

Machine Learning-Boosted Design of Ionic Liquids for CO₂ Absorption and Experimental Verification

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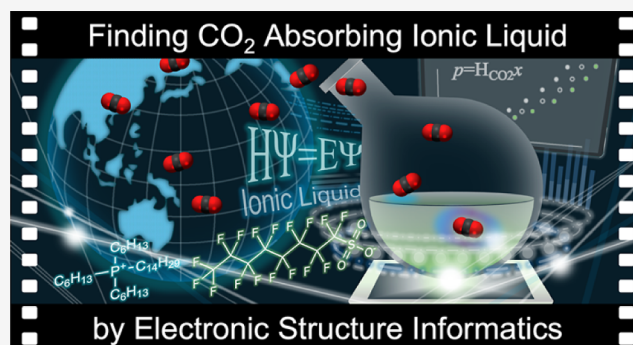
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ABSTRACT: Efficient CO₂ capture is indispensable for achieving a carbon-neutral society while maintaining a high quality of life. Since the discovery that ionic liquids (ILs; room-temperature molten salts) can absorb CO₂, various solvents composed of molecular ions have been studied. However, it is challenging to observe the properties of each isolated ion component to control the function of ILs as they are mixtures of ions. Finding the optimal cation–anion combination for the CO₂ absorbent from their enormous chemical space had been impossible in a practical sense. This study applied electronic structure informatics to explore ILs with high CO₂ solubility from 402,114 IL candidates. The feature variables were determined by a set of cheap quantum chemistry calculations for isolated small-ion fragments, and the importance of molecular geometries and electronic states governing molecular interactions was identified via the wrapper method. As a result, it was clearly shown that the electronic states of ionic species must have essential roles in the CO₂ physisorption capacity of ILs. Considering synthetic easiness for the candidates narrowed by the machine learning model, trihexyl(tetradecyl)phosphonium perfluorooctanesulfonate was synthesized. Using a magnetic suspension balance, it was experimentally confirmed that this IL has higher CO₂ solubility than trihexyl(tetradecyl)phosphonium bis(trifluoromethanesulfonyl)amide, which is the previous best IL for CO₂ absorption.



INTRODUCTION

Developing CO₂-absorbing materials with better performance is a critical step toward achieving efficient CCUS (carbon dioxide capture, utilization, and storage), which has been proposed as a strategy to address global warming.¹ While there are several types of CO₂ absorbers, the intensive study of ionic liquids (ILs; room-temperature molten salts) would give basic science contributing to environmental engineering toward the development of a safe and sustainable society. ILs are highly stable (with low volatility and high heat resistance) and can be chemically designed with a wide variety of ion combinations.^{2–5} ILs have been applied to various gas-fixing technologies, such as temperature/pressure swing, chemical/physical absorption, and cryogenic-/membrane-based separation.^{6,7}

A major limitation to the development of ILs for applications is the combinatorial explosion of the ion species, i.e., there are 10¹⁸ ILs in theory.² Even when ILs are limited to physical absorption (those not causing the CO₂ chemisorption), optimization of the CO₂ absorption capacity is experimentally challenging. The synthesis of ILs and characterization of their physical properties are more labor intensive than for electrically neutral molecular liquids due to their high

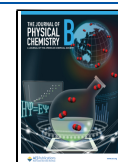
viscosities. To the best of our knowledge, [P₆₆₆₁₄][TFSA] (trihexyl(tetradecyl)phosphonium bis(trifluoromethanesulfonyl)amide) has the highest CO₂ solubility per molar fraction.⁸ Despite the vast number of candidates, even though many previous experimental and theoretical studies have designed CO₂-absorbing ILs, there has been no report of a material superior to [P₆₆₆₁₄][TFSA] in the last decade.

Machine learning has proven to be an excellent approach for overcoming such combinatorial problems if proper data sets are available. However, the synthesis and purification of ILs are typically complex, and it is difficult to consistently measure their physical properties with the same accuracy. Therefore, in the field of novel IL design, using experimental information may unintentionally bias the machine learning process. For example, the measured data of imidazolium cations are far greater than those for other cations. There have been several

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attempts to optimize the gas absorption properties of ILs for a narrow chemical space involving specific ionic skeletons using a machine learning approach,^{9–13} but a nonbiased (based on the number of ionic species) evaluation of the general chemical space has not been developed. Moreover, slight differences in the electronic states of ionic species can have critical effects on the properties of ILs. Since classical structure-based fingerprints cannot uniquely define charge delocalization, a comprehensive chemical space search by machine learning has not been achieved.

This study aimed to identify ILs with high CO₂ absorption capacities with minimal experimental processes. To this end, a materials informatics approach based on quantum chemistry calculations was implemented (Figure 1). Guided by the

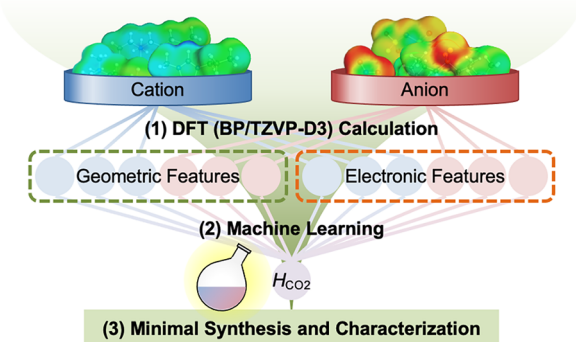


Figure 1. Proposed approach. By performing machine learning, synthesis, and precision measurement, ILs with excellent CO₂ solubilities were developed in a short period.

results of a machine learning evaluation, promising IL candidates were targeted and synthesized. Their CO₂ solubilities were also measured. This study focused on the simple ILs (cation–anion binary mixtures); however, it should be noted that the method has transferability to the functional design of further multicomponent systems.

METHODS

First, a theoretical screening was performed based on quantum chemistry calculations and machine learning. 6,991 stable ion structures (6,933 cations and 58 anions; see Figure S1 and Table S1) were explored by density functional theory calculations at the BP/TZVP-D3 level of theory, which has been successfully used for organic compounds, including ILs.^{14–22} Using geometry optimized structures and surface-charge-density distributions (σ -profiles),^{23–26} the geometric and electronic features listed in Table S2 were calculated for each ion.

Then, a set of Henry's law constant (H_{CO_2}) values at 298.15 K was evaluated by applying the COSMO-RS theory^{23–25} to 20,000 ILs (randomly selected from the total 402,114 candidates). It has been reported that calculated H_{CO_2} reproduces measured values well.^{21,22} Half of this set was used to train a machine learning model to predict H_{CO_2} for the other IL candidates. Using a cycle of feature selection, model creation, and performance evaluation, the essential molecular (ion) features for CO₂ absorption were systematically identified (wrapper method).²⁷ For model creation, the Gaussian process regression (GPR; kernel = ARDMatern 5/2) method²⁸ was applied to the standardized data with the quasi-Newton optimizer and five-fold cross-validation. The

performance of the created model was evaluated with 10,000 test data sets based on the coefficient of determination (R^2), root mean square error (RMSE), and mean absolute error (MAE). These operations were repeated five times. The quantum chemistry and statistical thermodynamics calculations and machine learning were performed with the TURBOMOLE 7.0,²⁹ COSMOtherm C30_1705,³⁰ and MATLAB³¹ packages, respectively.

Guided by the electronic structure informatics results, a set of automatically recommended (i.e., minimal) experiments was performed. Three representative [P₆₆₆₁₄][A] IL candidates were investigated, where A = [PFOS][−] (perfluorooctanesulfonate), [PF₆][−] (hexafluorophosphate), and [TFSA][−]. These ILs were synthesized (see Table S3 and Figures S2) according to the literature procedures^{32,33} (For details, see Synthesis Section in Supporting Information). No unexpected or unusually high safety hazards were encountered. The density and viscosity under atmospheric to high-pressure conditions were measured for the ILs according to the literature procedures^{34–40} (For details, see Measurements Section in Supporting Information).

The CO₂ solubility of an IL was measured using a magnetic suspension balance (Rubotherm GmbH), as detailed in our previous papers.^{39,40} The resolution and repeatability of the microbalance were 10 mg and ± 30 mg, respectively. Before the measurement, the weight and volume of a blank sample basket were measured at 313.15 or 333.15 K, respectively, up to 6 MPa. The volume of the blank sample basket was determined using the buoyancy method. CO₂ solubility measurements were then conducted as follows. 1 g of an IL was loaded in the sample basket, and then, the high-pressure cell was subjected to vacuum for approximately 24 h at 313.15 or 333.15 K. After evacuation, the weight of the pure IL under vacuum was recorded. A desired amount of CO₂ was loaded into the high-pressure cell, and the temperature was maintained to within ± 0.01 K. When the changes in weight, temperature, and pressure were less than ± 0.1 mg h^{−1}, ± 0.01 K h^{−1}, and 0.001 MPa h^{−1}, respectively, it was assumed that the IL was saturated with CO₂, and the weight was recorded. Subsequent measurements were repeated to obtain isothermal solubility data at pressures up to 6 MPa.

The amount of dissolved gas, W_g , was obtained as^{39,40}

$$W_g = W_F(p, T) - W_0(0, T) + \rho_{\text{CO}_2}(p, T) [V_{\text{IL}}(p, T) \{1 + S_W(p, T) + V_B\}] \quad (1)$$

where W_F and W_0 are the readouts of the balance at pressure p and vacuum, respectively. ρ_{CO_2} is the CO₂ density obtained using the Span–Wagner equation of state.⁴¹ V_{IL} and V_B are the volumes of the IL and the sample basket (including a hook), respectively. V_{IL} was obtained from the sample mass and specific volume of the IL at each pressure. Based on the experimental density data for the ILs, the specific volume of the IL at high pressure was calculated using the Tait equation of state.⁴² The volume expansion (swelling) of the IL, S_W , caused by gas absorption was calculated using the Sanchez–Lacombe equation of state.^{43,44} The coefficients of these equations were obtained by fitting the experimental densities of the ILs (temperature: 313.15 or 333.15 K; pressure: 0.1–6 MPa).

H_{CO_2} was evaluated for the ILs as the solubility gradients ($\partial p / \partial x_{\text{CO}_2}$) in the region of $x_{\text{CO}_2} < 0.1$. Finally, the Gibbs energy ($\Delta_{\text{abs}}G^\infty$), enthalpy ($\Delta_{\text{abs}}H^\infty$), and entropy ($\Delta_{\text{abs}}S^\infty$) of

CO₂ absorption by the ILs were experimentally obtained using the thermodynamic relations⁴⁵

$$\Delta_{\text{abs}}G^{\infty} = RT \ln \left(\frac{H_{\text{CO}_2}}{f_{\text{CO}_2}} \right) \quad (2)$$

$$\Delta_{\text{abs}}H^{\infty} = -T^2 \left[\frac{\partial}{\partial T} \left(\frac{\Delta_{\text{abs}}G^{\infty}}{T} \right) \right] = -RT^2 \left[\frac{\partial \ln \left(\frac{H_{\text{CO}_2}}{f_{\text{CO}_2}} \right)}{\partial T} \right] \quad (3)$$

$$\begin{aligned} \Delta_{\text{abs}}S^{\infty} &= \frac{\Delta_{\text{abs}}H^{\infty} - \Delta_{\text{abs}}G^{\infty}}{T} \\ &= -RT \left[\frac{\partial \ln \left(\frac{H_{\text{CO}_2}}{f_{\text{CO}_2}} \right)}{\partial T} \right] - R \ln \left(\frac{H_{\text{CO}_2}}{f_{\text{CO}_2}} \right) \end{aligned} \quad (4)$$

where f_{CO_2} is the fugacity coefficient of CO₂. $\Delta_{\text{abs}}H^{\infty}$ and $\Delta_{\text{abs}}S^{\infty}$ are closely related to the solute–solvent interaction strength and the free volume of the solvent, respectively.

RESULTS AND DISCUSSION

The correlation matrixes of cation and anion features are shown in Figures S3 and S4, respectively. These figures clearly

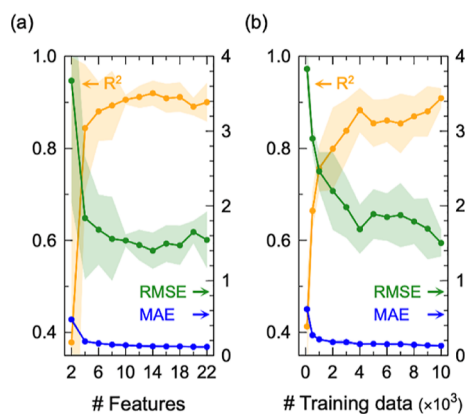


Figure 2. Learning curves for the test data not used for training the model with respect to the (a) number of features and (b) size of the training data set. For (a), the order of the features to add was determined by the wrapper method to maximize accuracy. For (b), V , M_2 , MW , M_3 , M_6 , and A were used for the features (see Tables S2 and S4–S6).

show that the geometric and electronic structures of ions are independent of each other. Sets of the logarithm of H_{CO_2} were normally distributed (Figures S5).

The accuracy of the machine learning procedure was confirmed by the learning curves for the test data not used for training the model and the correlation between the predicted and calculated H_{CO_2} values. According to a wrapper cycle, the features for CO₂ absorption were systematically identified. Highly accurate H_{CO_2} predictions ($R^2 > 0.90$, $\text{RMSE} < 1.5$ MPa, and $\text{MAE} < 0.13$ MPa) were achieved when 12 features were applied (Figure 2a). As summarized in Tables S4–S6, the wrapper method clarified that the first- and second-

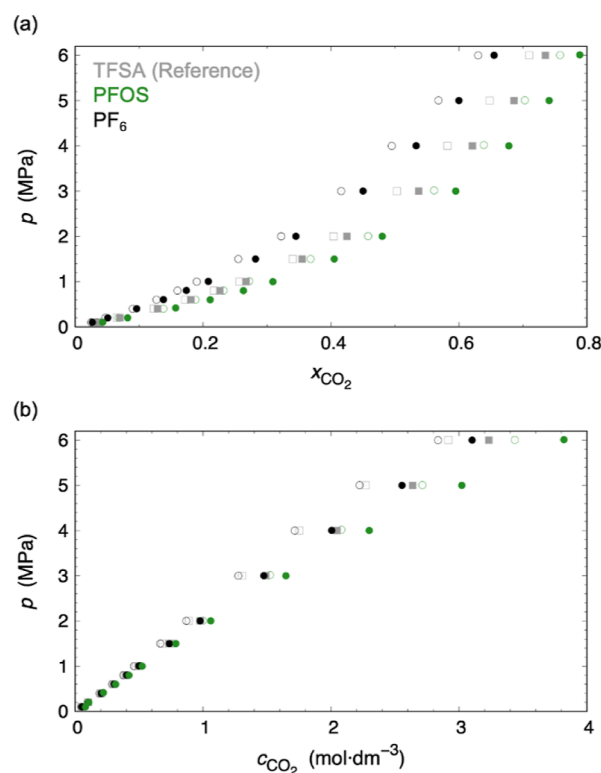


Figure 3. CO₂ solubility scaled by (a) mole fraction x_{CO_2} and (b) molarity c_{CO_2} (mol·dm⁻³) in [P₆₆₁₄][A] (A = TFSA, PFOS, and PF₆). Using the molar mass M_{CO_2} and the mass fraction X_{CO_2} of CO₂, c_{CO_2} was calculated by $c_{\text{CO}_2} = \rho_L \times X_{\text{CO}_2} / M_{\text{CO}_2}$. Closed and opened points are at 313.15 and 333.15 K, respectively.

most important features were geometric V (volume) and electronic M_2 (2nd σ -moment). This is considered reasonable because CO₂ molecules are physically absorbed in polar voids surrounded by ions in the ILs. It was clearly shown that the electronic state differences of ions have essential roles in the CO₂ physisorption capacity of ILs. It was also confirmed that a training data set size of 10,000 (2% of the candidates) was sufficient for obtaining an accurate model (Figure 2b). The constructed GPR model could predict H_{CO_2} values with high accuracy (Figure S6). Other algorithms (linear, XGBoost, and random forest regression) were also tried; however, they did not exceed GPR's performance (Figure S7).

Then, the GPR model was applied to predict H_{CO_2} for all 402,114 IL candidates. Using the well-trained model, superior ILs for CO₂ absorption could be predicted within a minute for these candidate ILs. A set of H_{CO_2} values regressed by the model are listed in Table S7. Considering machine learning results and synthetic possibilities (likely to yield the liquid state by a simple synthetic route), we decided to investigate two phosphonium-based ILs ([P₆₆₁₄][PFOS] and [P₆₆₁₄][PF₆]) which had better predicted H_{CO_2} values (2.78 and 2.91 MPa, respectively) than [P₆₆₁₄][TFSA] (3.06 MPa).

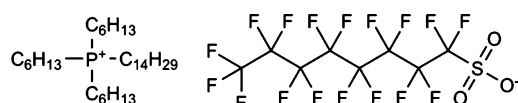
For the three ILs, the densities and the viscosities were determined to evaluate the specific volumes of the ILs (Figures S8–S10 and Tables S8–S11). Both densities and viscosities of all three ILs showed a negative correlation with increasing temperature, and high-pressure densities showed a positive correlation with increasing pressure. Here, the order of viscosity (TFSA⁻ < PFOS⁻ < PF₆⁻) did not correspond with the one of density (PF₆⁻ < TFSA⁻ < PFOS⁻). It has been

Table 1. CO₂ Solubility Scaled by Mole Fraction x_{CO_2} and Molarity c_{CO_2} (mol·dm⁻³) as a Function of Equilibrium Pressure p (MPa) in [P₆₆₆₁₄][A] (A = TFSA, PFOS, and PF₆)^a

p	x_{CO_2}	c_{CO_2}	p	x_{CO_2}	c_{CO_2}	p	x_{CO_2}	c_{CO_2}
$T = 313.15 \text{ K}$								
	TFSA			PFOS			PF ₆	
0.100	0.037	0.052	0.100	0.043	0.080	0.100	0.027	0.053
0.201	0.070	0.103	0.200	0.082	0.106	0.200	0.051	0.104
0.401	0.129	0.203	0.416	0.157	0.220	0.400	0.096	0.204
0.600	0.181	0.301	0.599	0.211	0.316	0.604	0.138	0.305
0.800	0.226	0.397	0.800	0.263	0.420	0.803	0.174	0.402
1.000	0.267	0.493	0.999	0.309	0.523	1.004	0.208	0.499
1.500	0.355	0.734	1.499	0.405	0.787	1.499	0.282	0.736
2.000	0.425	0.977	2.000	0.480	1.060	2.000	0.345	0.976
3.001	0.537	1.491	3.000	0.595	1.647	3.001	0.450	1.475
3.999	0.621	2.046	4.000	0.678	2.299	4.002	0.533	2.005
4.999	0.686	2.638	4.999	0.741	3.022	5.000	0.600	2.555
5.998	0.735	3.234	6.011	0.789	3.820	6.000	0.655	3.103
$T = 333.15 \text{ K}$								
	TFSA			PFOS			PF ₆	
0.101	0.035	0.050	0.100	0.033	0.066	0.100	0.025	0.049
0.201	0.065	0.099	0.199	0.068	0.101	0.200	0.047	0.099
0.400	0.123	0.199	0.400	0.138	0.213	0.399	0.090	0.191
0.600	0.172	0.295	0.600	0.188	0.305	0.600	0.127	0.290
0.800	0.217	0.386	0.802	0.232	0.412	0.800	0.160	0.377
1.000	0.257	0.473	1.010	0.272	0.510	1.000	0.190	0.460
1.500	0.340	0.682	1.500	0.368	0.762	1.499	0.255	0.666
2.000	0.404	0.888	2.006	0.458	0.999	2.000	0.322	0.869
3.000	0.503	1.304	3.014	0.561	1.523	2.999	0.416	1.276
4.000	0.582	1.753	4.018	0.639	2.081	3.998	0.495	1.716
5.000	0.648	2.271	5.007	0.703	2.714	5.004	0.568	2.224
6.000	0.710	2.917	6.004	0.758	3.436	5.997	0.630	2.836

^aStandard uncertainties are $u(T) = 0.01 \text{ K}$ and $u(p) = 0.0005 \text{ MPa}$. Relative expanded uncertainties of U_i are $u(x_{\text{CO}_2}) = 0.001$ and $u(c_{\text{CO}_2}) = 0.001$.

Chart 1. IL [P₆₆₆₁₄][PFOS] with the Best CO₂ Physisorption Capacity Achieved by Machine Learning

**Table 2.** Henry's Law Constants H_{CO_2} (MPa), Gibbs Energy $\Delta_{\text{abs}}G^\infty$ (kJ·mol⁻¹), Enthalpy $\Delta_{\text{abs}}H^\infty$ (kJ·mol⁻¹), and Entropy $\Delta_{\text{abs}}S^\infty$ (J·mol⁻¹·K⁻¹) of CO₂ Absorption Evaluated Experimentally for [P₆₆₆₁₄][A] (A = TFSA, PFOS, and PF₆)^a

	H_{CO_2}	$\Delta_{\text{abs}}G^\infty$	$\Delta_{\text{abs}}H^\infty$	$\Delta_{\text{abs}}S^\infty$
TFSA	2.85 (3.04)	2.72	-2.62	-17.1
PFOS	2.41 (2.71)	2.29	-8.11	-33.2
PF ₆	4.09 (4.39)	3.67	-2.88	-20.9

^aThe data outside/inside the parenthesis are at 313.15/333.15 K.

reported that [P₆₆₆₁₄][TFSA] has lower viscosity than [P₆₆₆₁₄][PF₆],⁴⁶ and our results confirm this fact. These results suggest that the cation–anion electrostatic interaction of [P₆₆₆₁₄][PF₆] is particularly strong. The measured densities well agreed with the calculated values fitted by the quadratic equation (average relative deviation: ARD < 0.02%). The measured viscosities correlated well with the Vogel–Fulcher–Tammann (VFT) equation (ARD < 0.46%) rather than the Arrhenius equation (ARD < 1.79%) because ILs have glass transition points. From the well-fitted high-pressure densities in the Tait equation of state (ARD < 0.01%) and the Sanchez–

Lacombe equation of state (ARD < 0.14%), the volume expansions (swelling) of the ILs were obtained.

Both the mole fraction and molarity-scaled CO₂ solubilities were also measured (Figure 3 and Table 1). The former does not consider the effect of molecular volume, while the latter does. Thus, the molarity-scaled CO₂ solubilities are important for gas absorption process design. The solubilities proportional to pressure means that the ILs absorb CO₂ by a physisorption mechanism. The CO₂ solubility increased in the anion order of PF₆⁻ < TFSA⁻ < PFOS⁻ (with increasing fluorine atoms in the anions). The reason for the results can be considered as due to the fact that the large numbers of fluorine atoms and S=O bonds in PFOS⁻ can develop strong interactions between the anion and CO₂. From the COSMO-RS validation, it was found that PFOS⁻ has the largest anion–CO₂ contact probability (PFOS⁻: 0.318, TFSA⁻: 0.232, and PF₆⁻: 0.151). The fact could also be explained experimentally: the absorption Gibbs energy of [P₆₆₆₁₄][PFOS] (Chart 1) was the most stable among the three ILs due to the large negative enthalpy (Table 2).

CONCLUSIONS

This study proposed an electronic structure informatics approach to predict and develop ILs with high CO₂ solubility based on geometric and electronic factors of the constituent cations and anions. With a machine learning-assisted search for the best cation/anion combination, targeted organic syntheses, and precision measurements, the IL [P₆₆₆₁₄][PFOS] was experimentally proven to have a higher CO₂ solubility than

[P₆₆₆₁₄][TFSA]. The wrapper cycle analysis of molecular features clearly showed that the electronic features of ions have essential roles in the CO₂ physisorption capacity. In other words, precisely designing electronic states of the ionic species by quantum chemistry calculation is mandatory for further tuning of the gas absorption nature. New ionic species with functional group introductions, elemental substitutions, and other modifications could also be systematically considered to accelerate research without being hindered by the enormous chemical space of ILs. The method for developing functional liquids proposed in this study can be applied to other gas-absorbing liquids, such as deep eutectic solvents (hydrogen-bonded mixed organic solvents in a broad sense) or general functional materials composed of multicomponent systems with an extension for weak intermolecular interaction. We believe our method will significantly contribute to developing a carbon-neutral society.

■ ASSOCIATED CONTENT

Data Availability Statement

All the experimental data are available in the main text or Supporting Information.

Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acs.jpcb.2c07305>.

Supporting methods including chemical space and features for machine learning, synthesis, and measurements; results including machine learning and densities and viscosities under atmospheric to high-pressure conditions; and references (PDF)

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Author Contributions

N.K. and H.M. conceived the project. N.K. generated the molecular library and performed machine learning with guidance from H.M. F.A.C. and H.Y. synthesized the three ILs. Y.S. and D.K. measured the basic properties of the ILs. The manuscript was written through contributions from all authors. All authors have given their approval to the final version of the manuscript.

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Notes

The authors declare no competing financial interest.

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