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Reduction of aerobic fermentation on sugars by altering the fermentative/oxidative balance is of significant interest for optimization of industrial production of *Saccharomyces cerevisiae***. Glucose control of oxidative metabolism in baker's yeast is partly mediated through transcriptional regulation of the Hap4p subunit of the Hap2/3/4/5p transcriptional activator complex. To alleviate glucose repression of oxidative metabolism, we constructed a yeast strain with constitutively elevated levels of Hap4p. Genetic analysis of expression levels of glucose-repressed genes and analysis of respiratory capacity showed that Hap4p overexpression (partly) relieves glucose repression of respiration. Analysis of the physiological properties of the Hap4p overproducer in batch cultures in fermentors (aerobic, glucose excess) has shown that the metabolism of this strain is more oxidative than in the wild-type strain, resulting in a significant reduced ethanol production and improvement of growth rate and a 40% gain in biomass yield. Our results show that modification of one or more transcriptional regulators can be a powerful and a widely applicable tool for redirection of metabolic fluxes in microorganisms.**

Modification and control of metabolic fluxes is an important goal in most industrial applications of microorganisms. This is the case for baker's yeast, which has applications in production of heterologous proteins, brewing, and baking. Maximization of biomass yields of baker's yeast growing on sugars is hampered by the cell's strong tendency to produce ethanol, even under aerobic conditions when sugars are present in excess. This alcoholic fermentation might be prevented by manipulation of the carbon flux distribution between fermentation and respiration.

Attempts at redirection of carbon fluxes by interference in expression levels of single enzymes of glycolytic or fermentative pathways have so far not been successful (24, 25). Reduced activities of fermentative enzymes such as pyruvate decarboxylase result in impaired growth on glucose (8, 9) and deprive the cells of their fermentative capacity necessary for raising of dough. Increasing respiratory activity seems to be a better approach, but numerous studies have shown that overproduction of a single enzyme results in either little or no increase of flux through a metabolic pathway (20). This is because flux control is usually not exerted by only a single enzyme (2, 20, 28). A more rational approach would therefore be to manipulate the activity of a regulatory protein involved in control of all key enzymes of one or more specific metabolic pathways. The potential of this approach is illustrated by the partial alleviation of glucose control of sucrose and galactose metabolism as a result of disruption of the glucose repressor Mig1p alone or in combination with Mig2p (16, 17). These modifications do not, however, result in a significant change in respiratory functions, ethanol production, or biomass yield.

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Aiming at redirection of fermentative flux toward oxidative carbon flux, we focused on the Hap4p activator subunit of the transcriptional complex involved in carbon source-dependent regulation of respiratory function (3, 6, 11). Transcription of this subunit is glucose repressible (11), suggesting that Hap4p is the key component of the complex in terms of its control of transcriptional activity in response to carbon source. This study shows that raising the expression level of Hap4p on glucose results in a partial alleviation of glucose repression of respiratory genes and function. The resulting significant changes in carbon metabolism, growth rate, and biomass yield demonstrate the pivotal role of the transcriptional regulator Hap4p in control of respiro-fermentative metabolism in *S. cerevisiae*.

MATERIALS AND METHODS

Overexpression of *HAP4* **in** *Saccharomyces cerevisiae* **strain DL1.** A 1.7-kb fragment containing the coding region of *HAP4* was isolated from pSLF406 (11) by digestion with $BspHI$ (which cleaves $HAP4$ at position -1 relative to the start codon the coding sequence), blunting, and subsequent digestion with *Pst*I. YCplac111::*ADH1* (which was derived from Ycplac111 [12] and contains a 723-bp *Eco*RV *ADH1* promoter fragment from pBPH1 [28]) was cleaved with *Sma*I and *Pst*I and ligated with the *HAP4* fragment to generate YCplac111::*ADH1-HAP4*. Yeast strain DL1 (30) was transformed by the lithium acetate method (14). Transformants were selected on plates containing 2% glucose, 2% agar, and 0.67% yeast nitrogen base (Difco) supplied with the required amino acids but lacking leucine.

Growth of yeast in flask-batch cultures. For shake flask cultivation, yeast cells were grown in either YPD (1% yeast extract, 1% Bacto Peptone, 3% D-glucose), YPEG (yeast extract, 1% Bacto Peptone, 2% ethanol, 2% glycerol), YPL [lactate medium; 1.5% lactic acid, 2% sodium lactate, 0.1% glucose, 8 mM MgSO₄, 45 $\text{mM (NH)}_{2}\text{HPO}_{4}$, 0.5% yeast extract], or selective mineral medium (0.67% yeast nitrogen base) containing 3% D-glucose.

Growth of yeast in fermentor-batch cultures. Transformed yeast cells were grown in selective mineral Evans medium (7) containing 30 g of D-glucose per liter and supplemented with filter-sterilized 40 mg each of uracil and L-histidine per liter. Instead of citrate, nitrilotriacetic acid (2 mM) was used as a chelator, and silicone antifoaming agent (1 ml/20 liters) was added to the medium. After heat sterilization of the medium at 120°C (glucose sterilized separately at 110°C), filter-sterilized vitamins were added to final concentrations per liter as follows: myoinositol, 0.55 mM; nicotinic acid, 0.16 mM; Ca-D- $(+)$ -panthothenate, 0.02

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mM; pyridoxine-HCl, 0.013 mM; thiamine-HCl, 0.006 mM; biotin, 0.02 μ.Μ. Cultivation was performed at 28°C in New Brunswick Scientific Bioflow fermentors, at a stirrer speed of 900 rpm. The pH was kept constant at 5.0 via the automatic addition of 2 mol of NaOH per liter. Antifoam (BDH) was added automatically at fixed time intervals. An airflow of 0.8 liter min^{-1} maintained the dissolved oxygen tension above 40% of air saturation. The starting working volume of the cultures was 1.0 or 1.4 liters. Samples of 30 ml were taken every hour for analysis of culture purity, optical cell density (OD; spectrophotometrically at 600 nm), substrate and product concentrations, and dry biomass weight (by centrifugation of 10.0 ml of culture, washing cells with demineralized H_2O , and drying the cell pellet overnight at 80°C; parallel samples varied by less than 1%). The dissolved carbon dioxide concentration was continuously monitored by a Servomex IR PA404 gas analyzer and oxygen was measured by a Taylor Servomex OA 272 gas analyzer. The absolute amounts of gas consumption/ production during the time course of the experiment were calculated by the mean of the gas concentration, corrected for the decreasing volume of the culture. Specific consumption/production rates of metabolites (*q*; millimoles consumed or produced per gram of dry yeast biomass per hour) were calculated from the slope of a plot of metabolite concentration versus dry biomass concentration, amplified by the specific growth rate. The correlation of metabolite concentration versus dry biomass concentration was linear for all metabolites during the independent experiments.

Substrate consumption and product formation in liquid medium. Concentrations of extracellular carbon compounds were determined by high-pressure liquid chromatography analysis using an Aminex HPX87H organic acids column (Bio-Rad) at 65° C. The column was eluted with 5 mM H₂SO₄. Detection was by means of a 2142 refractive index detector (LKB) and SP4270 integrator (SpectraPhysics).

Analysis of $O₂$ consumption. For oxygen consumption capacity measurements of flask-batch-grown cells, the cells were harvested, washed three times with ice-cold demineralized H_2O , and resuspended in oxygraph buffer [1% yeast extract, 0.1% KH₂PO₄, 0.12% (NH4)₂SO₄ (pH 4.5)] at 200 OD units ml⁻¹. Oxygen consumption capacity of the cells was measured with a Clark-type oxygen electrode, with 0.1 mM ethanol as substrate. Rates were determined from the slope of a plot of $O₂$ concentration versus time.

RNA isolation, Northern analysis, and labeling of DNA fragments. Cells were harvested, and RNA was isolated, separated, on a nondenaturing 1.2% agarose gel, and transferred to a nitrocellulose filter as described previously (5). Prehybridization was performed in hybridization buffer (50% formamide, 25 mM NaPi [pH 6.5], 5 \times SSC [1 \times SSC is 0.15 M NaCl plus 0.015 M sodium citrate], 5 \times Denhardt's solution) containing 50 μ g of single-stranded salmon sperm DNA per ml. DNA fragments used as probes in this study include an 840-bp *Hin*dIII-*Sal*I fragment from pJH1 (5), a 1.6-kb *Bam*HI-*Kpn*I fragment containing the yeast actin gene (19), a 2.5-kb *Hin*dIII-*Sal*I fragment from YE23SH containing the *QCR2* gene (22), a 1,333-bp *Nco*I-*Hin*dIII fragment from pAZ6 containing the yeast *PDA1* gene (32), and a 1.2-kb *Bam*HI-*Hin*dIII fragment from YE23R-SOD/SUC containing the *SUC2* gene (31). Fragments were ³²P labeled by nick translation as described by Maniatis et al. (18). Labeled probes were added to the prehybridization buffer, and hybridization was performed overnight at 42°C. Blots were washed once with $2 \times$ SSC–0.1% sodium dodecyl sulfate (SDS), twice with $1\times$ SSC–0.1% SDS, and finally with 0.5 \times SSC–0.1% SDS. Blots were air dried completely, and autoradiography was performed with Kodak X-Omat 100 film or analyzed by a Storm 840 Phosphorimager (Molecular Dynamics).

RESULTS

Hap4p overexpression on glucose results in derepression of respiratory chain components. To elevate the repressed endogenous level of Hap4p in *S. cerevisiae* growing on glucose, we introduced a centromeric plasmid containing the coding region of *HAP4* under control of the glucose-inducible *ADH1* promoter in a laboratory *S. cerevisiae* strain. As a reference to this Hap4p overproducer (DL1HAP), a wild-type strain was transformed with the same plasmid but lacking the *HAP4* gene (DL1). The expression level of *HAP4* mRNA in both strains under fermentative and nonfermentative growth conditions is depicted in Fig. 1. Expression of *HAP4* in wild-type cells is strongly repressed by glucose. Introduction of the plasmid with *HAP4* under control of the *ADH1* promoter leads to an approximately 10-fold increased expression level of *HAP4* in DL1HAP which is grown on medium containing 2% glucose. This level is comparable to the expression level of *HAP4* in wild-type cells when grown on medium containing ethanolglycerol, which induces transcription of *HAP4* about ninefold (Fig. 1 and reference 4).

To study the effect of *HAP4* overexpression on transcrip-

FIG. 1. Expression of several mRNAs in a Hap4p overexpression strain. DL1 and DL1HAP were grown to mid-logarithmic phase in medium containing 2% glucose (D) or 2% ethanol–2% glycerol (EG); 20 μ g of total RNA was hybridized with probes specific for *HAP4*, *ACT* (actin), *QCR8*, or *SUC2* mRNA.

tional control of respiratory function, we first studied the mRNA levels of different genes encoding components of the respiratory chain. As shown in Fig. 1, the elevated level of Hap4p in glucose-containing medium leads to derepression of transcription of *QCR8*, the gene encoding the 11-kDa subunit of the yeast ubiquinol-cytochrome *c* oxidoreductase (QCR) complex of the respiratory chain. Hap4p overexpression does not result in full induction levels of *QCR8* as found on nonfermentable carbon sources such as ethanol-glycerol, which is probably due to the involvement of other factors in transcriptional control of *QCR8*. Comparable results were obtained for a number of other genes encoding respiratory components, such as *QCR2*, *QCR7*, and *CYC1* (not shown). The sustained glucose repression of *SUC2*, without a Hap2/3/4/5p binding box in the promoter region, shows that Hap4p overproduction does not alleviate glucose repression in general.

Respiratory capacity is increased in Hap4p overproducer. To test whether the increased level of mRNAs of respiratory components results in an higher respiratory capacity of the Hap4p-overproducing strain, we measured oxygen consumption rates of cells grown to mid-logarithmic phase in shake flask cultures. Respiratory capacity of DL1HAP cells collected from media containing glucose was nearly twofold greater than that of wild-type cells (18.1 versus 9.4 nmol of glucose produced/min/mg [dry weight] of yeast biomass). When Hap4pproducing strains were grown in the presence of the nonfermentable carbon source lactate, the respiratory capacity is further increased approximately fivefold, to a level similar to that for the wild-type strain grown on lactate (86.7 versus 88.1 nmol/min/mg of yeast biomass). This indicates that an elevated level of Hap4p only partially relieves repression of respiratory function, which is in agreement with the partially derepressed transcript levels of respiratory genes.

In vivo carbon catabolism is shifted from fermentation toward respiration. To follow a possible change from fermentative toward a more oxidative catabolism during growth on excess glucose, we further characterized the physiological properties of the Hap4p-overproducing strain. Since cultivation in shake flask cultures is subject to oxygen limitations and variable pH conditions that can influence carbon metabolism, cells were grown under controlled conditions in fermentors (constant pH, aeration, and stirring) in well-defined mineral media. Aerobic growth of the wild-type strain carrying the

FIG. 2. Growth characteristics and glucose consumption and ethanol production profile in fermentor batch cultivations. Shown are dry yeast biomass formation (\Box, \blacksquare) and glucose $(\Diamond, \blacklozenge)$ and ethanol $(\triangle, \blacktriangle)$ concentrations present in the culture supernatant of the wild-type strain DL1 (A) and the Hap4p overproducer DL1HAP (B) and glucose consumption (C) and ethanol production (D) relative to the amount of dry yeast biomass formed in wild-type DL1 (closed symbols) and DL1HAP (open symbols) strains.

empty plasmid was compared with growth of DL1HAP cells in a defined mineral salts medium containing glucose (30 g/liter [3%]). As calculated from three independent growth curves (one example shown in Fig. 2), the wild type grew exponentially with a specific growth rate of 0.17 ± 0.01 h⁻¹, whereas the growth rate of DL1HAP was 0.20 ± 0.01 h⁻¹. Overproduction of Hap4p thus results in an increased growth rate of approximately 17%, which was also observed during early logarithmic flask-batch growth (data not shown).

During a 6-h period of exponential growth, samples were taken at hourly intervals to measure substrate consumption and biomass and product formation. Exponential growth (biomass formation) of both the wild-type (Fig. 2A) and Hap4poverproducing (Fig. 2B) strain are shown, along with the concentrations of residual glucose and produced ethanol present in the culture supernatant. Although from this figure only the difference in growth between the two strains seems apparent, the difference in carbon catabolism becomes evident when the data are presented relative to the amount of biomass formed (Fig. 2C and D). Calculation of the specific ethanol production and glucose consumption rates (Table 1) showed that Hap4p overexpression results in a significant reduction in the specific glucose consumption rate (q_{glucose} ; 15% reduction) and spe-

TABLE 1. Effect of HAP4 overexpression on carbon flux distribution*^a*

| q | $Flux^a$ | |
|-----------------------|----------|---------|
| | DL1 | DL1HAP |
| q_{glucose} | -9.84 | -8.08 |
| q_{ethanol} | 14.49 | 10.84 |
| q_{glycerol} | 2.31 | 0.62 |
| q_{acetate} | 0.28 | 0.64 |
| q_{CO_2} | 17.4 | 17.4 |
| q_{O_2} | 3.3 | 6.9 |

^a Determined as described in Materials and Methods; calculated from the linear correlations of metabolite concentration versus dry biomass formed during 6 h of exponential growth in a fermentor-batch cultivation, amplified by the specific growth rate. Data are presented as the average of calculations based on duplicate metabolite and biomass determinations from two independent experiments. Data varied by less than 5%.

cific ethanol production rate $(q_{\text{ethanol}}; 25\%$ reduction). As a consequence, the biomass yield, i.e., the amount of biomass formed per 100 g of consumed glucose, is 39% higher in the Hap4p overproducer: 9.9 ± 0.4 g for DL1 and 13.7 ± 0.4 g for DL1HAP.

Analysis of production rates of other carbon compounds present in the fermentor effluent (Table 1) showed that the specific glycerol production rate is significantly decreased in the Hap4p overproducer (27% of the wild-type level), whereas the amount of produced acetate is 2.2-fold increased in DL1HAP cells. The change in product pattern of these compounds is directly attributable to an increased ability to reoxidize redox equivalents via respiration. In accordance with this, the carbon flux through the trichloroacetic acid cycle was increased approximately twofold as calculated directly from either the oxygen consumption rate or from the total $CO₂$ production rate corrected for ethanol production. The respiratory coefficient (q_{CO_2}/q_{O_2}) ratio) of the DL1HAP strain is hence significantly lower than that of the wild-type strain, which is also indicative for a less fermentative catabolism of the Hap4poverproducing strain. All data are thus consistent with a shift of carbon metabolism from fermentative toward oxidative metabolism due to an increased expression level of *HAP4*.

DISCUSSION

Interference in molecular regulatory circuits can be used as a powerful tool for redirection of metabolic fluxes in order to optimize industrial use of microorganisms. We have exemplified this by redirection of the fermentative-oxidative carbon balance in baker's yeast in order to reduce aerobic alcoholic fermentation triggered by the presence of glucose. This has been achieved by raising the expression level of Hap4p, the major regulatory protein of the Hap2/3/4/5p complex required for transcriptional induction of respiratory components. Although previously it has been suggested that regulation of the transcript level of *HAP4* would be the main determinant for the activity of the Hap complex $(3, 11)$, we now present the first experimental evidence for this hypothesis. Our results also show that the DNA binding factors of the complex, Hap2p, Hap3p, and Hap5p, are constitutively present at sufficient levels and that posttranslational modifications do not play an important role in glucose control of the Hap complex, in contrast to other transcriptional regulators like Cat8p (23) and Mig1p (21). Hence, an artificially elevated expression level of Hap4p is sufficient to increase mRNA levels of respiratory genes on glucose. This resulted in an increased respiratory capacity and in vivo carbon flux through the tricarboxylic acid cycle and respiration. The alleviation of repression of respiration and redirection of respiro-fermentative carbon flux is only partial, which can be explained by the control of other factors and mechanisms on regulation of oxidative function. Nevertheless, this partial effect results in a significant gain in specific growth rate and biomass yield during growth on an excess of glucose due to the large difference in the energetic efficiency between respiration and fermentation.

When grown under anaerobic conditions, Hap4p-overexpressing strains are identical to wild-type cells with respect to growth rate, ethanol production, and biomass yield (data not shown). This implies that overexpression of *HAP4* exhibits its effect only during aerobic growth of yeast. Processes depending on anaerobic alcoholic fermentation, like brewing or dough leavening, will be unaffected by *HAP4* overexpression. *HAP4* modified strains should therefore be suited to optimize biomass yields in the aerobic production phase of industrial yeast strains. Experiments are in progress to test whether *HAP4*

overexpression has an effect on the rapid triggering of alcoholic fermentation, which occurs during local and transient exposure to an excess of glucose due to imperfect mixing in sugarlimited, aerobic industrial fed-batch cultivations.

The profound effect of Hap4p overproduction on cell physiology during growth on excess of glucose suggest a broad spectrum of effects on different functional groups of genes involved in carbon and energy metabolism. A switch from fermentative to respiratory growth, which normally occurs during the diauxic shift upon depletion of glucose, is correlated with widespread changes in the expression of genes involved in fundamental cellular processes such as carbon metabolism, mitochondrial assembly, stress response, protein synthesis, and carbohydrate storage (4, 15). Although many genes contain Hap2/3/4/5p consensus binding sites in their promoter regions (10), only few have been reported to be regulated by the HAP complex (3, 6). We are currently performing genome-wide transcript profiling studies that will reveal the total spectrum of gene families that are directly or indirectly affected by Hap4p overexpression. Insight into gene families that are affected or unaffected by Hap4p overproduction may provide clues toward modification of other regulatory proteins. The use of transcript-profiling analysis techniques (1, 26) will be invaluable in the exploration of regulators of metabolic pathways that should be modified for biotechnological applications.

We have presented a clear example of how modification of a transcriptional regulator may serve as a powerful tool for manipulation of the cell's physiology and as an attractive alternative to the unsuccessful alteration of expression levels of single enzymes. It should, however, be realized that overexpression of transcriptional activators can have a deleterious effect on growth which is attributable to squelching of general transcription factors, as observed for GAL4 (13) and GCN4 (27), but also in studies with $GAL4-HAP4$ fusions on 2μ m plasmids (J. Stebbins and S. Triezenberg, Abstr. Yeast Genet. Mol. Biol. Meet., abstr. 517, p. 307, 1998). Undesired pleiotropic effects can also occur in case of interference in factors with a central role high in signaling cascades, such as the general repressor complex Tup1/Ssn6 or the Snf1/Snf4 kinase with a central role in the glucose response (reviewed in reference 15). Our study involving a modest change of a familyspecific transcriptional regulator is one of the first successful and promising examples of genetic engineering of metabolic fluxes in yeast.

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