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The inhibitory effects of 15 hydrocarbons and halogenated hydrocarbons on  $NH<sub>3</sub>$  oxidation by ammonia monooxygenase (AMO) in intact cells of the nitrifying bacterium Nitrosomonas europaea were determined. Determination of AMO activity, measured as  $NO<sub>2</sub><sup>-</sup>$  production, required coupling of hydroxylamine oxidoreductase (HAO) activity with NH<sub>3</sub>-dependent NH<sub>2</sub>OH production by AMO. Hydrazine, an alternate substrate for HAO, was added to the reaction mixtures as <sup>a</sup> source of reductant for AMO. Most inhibitors exhibited competitive or noncompetitive inhibition patterns. The competitive character generally decreased  $(K_{IE}/K_{IES}$  increased) as the molecular size of the inhibitors increased. For example, CH<sub>4</sub> and C<sub>2</sub>H<sub>4</sub> were competitive inhibitors of NH<sub>3</sub> oxidation, whereas the remaining alkanes (up to  $C_4$ ) and monohalogenated (Cl, Br, I) alkanes were noncompetitive. Oxidation of  $C_2H_5Br$  (noncompetitive) increased as the NH<sub>4</sub><sup>+</sup> concentration increased up to 40 mM, whereas oxidations of inhibitors with competitive character ( $K_{iE} \ll K_{iES}$ ) were<br>diminished at 40 mM NH<sub>4</sub>+. Multichlorinated compounds produced nonlinear Lineweaver-Burk plots. Iodinated alkanes (CH<sub>3</sub>I, C<sub>2</sub>H<sub>5</sub>I) and C<sub>2</sub>Cl<sub>4</sub> were potent inhibitors of NH<sub>3</sub> oxidation. Maximum rates of NH<sub>3</sub>,  $C_2H_4$ , and  $C_2H_6$  oxidations were approximately equivalent, suggesting a common rate-determining step. These data support an active-site model for AMO consisting of an NH3-binding site and <sup>a</sup> second site that binds noncompetitive inhibitors, with oxidation occurring at either site.

The widely distributed soil bacterium Nitrosomonas europaea is an obligate chemolithoautotrophic aerobe which uses ammonia as its sole natural energy source (28). The oxidation of ammonia to nitrite in  $N$ . *europaea* is initiated by ammonia mono-oxygenase (AMO). Because of the broad substrate range of AMO (2, 19, 21, 24), attention has focused recently on the possibility of using nitrifiers such as N. europaea in the bioremediation of contaminated soils and aquifers and in the treatment of wastes. Exploitation of this potential of nitrifiers will require a thorough knowledge of AMO and its interaction with alternate substrates.

AMO catalyzes the oxidation of  $NH<sub>3</sub>$  to hydroxylamine All  $\sigma$  catalyzes the contained to  $NO_2$ <sup>-</sup> by hydroxylamine oxidoreductase (HAO) with the release of four electrons (28). Two of the four electrons must be transferred to AMO to activate  $O<sub>2</sub>$  and maintain steady-state rates of ammonia oxidation  $(28)$ . Free NH<sub>2</sub>OH concentrations are apparently very low during ammonia oxidation (28). The coupling of AMO and HAO activities is illustrated in the top half of Fig. 1. AMO in N. europaea also catalyzes the oxidation of several alternate substrates (including hydrocarbons and halogenated hydrocarbons) (19-21, 24). These oxidations, such as the oxidation of ethylene to ethylene oxide (Fig. 1, bottom half), require reductant, which can be supplied by the simultaneous oxidation of ammonia to provide NH<sub>2</sub>OH.

Previous studies of halogenated hydrocarbon oxidations by N. europaea focused on the substrate range of the enzyme (11, 19-21, 24), product identification (11, 19), and the toxicity associated with the oxidation of some compounds (21, 24). As potential substrates for AMO, hydrocarbons and halogenated hydrocarbons can be categorized into three classes as defined by Rasche et al. (21): class <sup>1</sup> (those not oxidized by AMO), class <sup>2</sup> (those oxidized by AMO with little or no resultant toxic effect on the cells), and class 3 (those oxidized by AMO but yielding reactive products that inactivate  $NH<sub>3</sub>$  oxidation). Two examples of class 1 compounds are carbon tetrachloride and tetrachloroethylene (21). Chloromethane (21) and monohaloethanes (19) are class 2 substrates, which yield formaldehyde and acetaldehyde as oxidation products, respectively. Chloroform and trichloroethylene are examples of class 3 compounds, although both are oxidatively dechlorinated (21).

Although previous studies have provided information on the substrate range and other aspects of alternate substrate oxidations by AMO, they have provided little information on how halogenated hydrocarbon substrates interact with the active site of AMO. Kinetic inhibition studies can provide such insights into the active site of AMO and should therefore have predictive value for biotransformations of compounds structurally related to those we have tested, as well as for in situ biotransformations of mixtures of compounds. With whole cells of N. europaea, the inhibition of  $NH<sub>3</sub>$ oxidation by CH<sub>4</sub> (13) and C<sub>2</sub>H<sub>4</sub> (14) is competitive, which indicates mutually exclusive binding of  $NH<sub>3</sub>$  and these alternate substrates. Benzene, which is oxidized to phenol and subsequently to  $p$ -hydroquinone, exhibits a noncompetitive pattern (12). At low  $NH_4$ <sup>+</sup> concentrations, the doublereciprocal plots for  $CH_4$  and  $C_2H_4$  deviate from the pattern expected for simple competitive inhibition; reductant depletion was cited as an explanation (14). Suzuki et al. (23) monitored AMO activity by measuring  $NH<sub>3</sub>$ -dependent  $O<sub>2</sub>$ consumption in cell extracts and obtained double-reciprocal plots for the inhibitors  $CH_4$ , CO, and  $CH_3OH$  which are also indicative of competitive inhibition. Their plots also deviate somewhat from simple competitive inhibition.

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FIG. 1. Reactions catalyzed by AMO and HAO. Reactants are shown in numbers required for a single catalytic turnover event.

We wished to investigate the interactions of hydrocarbons and halogenated hydrocarbons with AMO by determining the inhibition patterns and apparent inhibition constants associated with the inhibition of  $NH<sub>3</sub>$  oxidation by these compounds. Since bioremediation applications with  $N$ . europaea would involve whole cells, our experiments were carried out with intact cells. Active, purified preparations of AMO are not available. Furthermore, there is considerable difficulty involved in stabilizing and assaying cell extracts (6). The direct electron donor for AMO has not been identified, necessitating the use of a coupled enzyme system, as in our study. The efficiency of coupling of AMO and HAO activities is apparently greatly reduced when cells are lysed (6). Alternate substrates can influence AMO activity in intact cells by three distinct mechanisms: (i) direct binding and interaction with AMO, (ii) interference with the reductant supply to AMO (oxidation of alternate substrates requires reductant, but the products are not further oxidized to replenish the reductant as is the case with  $NH<sub>3</sub>$ ), or (iii) oxidation to highly reactive products that covalently bind and inactivate AMO and other enzymes. To avoid the cytotoxic effects associated with reactive products, we limited our study to class <sup>1</sup> and 2 compounds. To ensure a constant supply of reductant to AMO, we included hydrazine, an alternate substrate for HAO, in the reaction mixtures. In this way, we attempted to restrict the inhibitory effects of class 2 compounds to direct interactions with AMO. Fifteen hydrocarbon and halogenated hydrocarbon inhibitors produced a variety of inhibition patterns including competitive, noncompetitive, and nonlinear (concave-down)  $v^{-1}$ -versus-S<sup>-1</sup> plots (for definitions of v and S, see Materials and Methods). Within the selection of inhibitors, trends were noted in molecular size, identity of the halogen substituent, and number of halogen substituents. These trends should enhance the predictive value of the present work.

# MATERIALS AND METHODS

Cell growth and preparation. N. europaea ATCC <sup>19718</sup> was cultured in 1.5-liter batches at 30°C. The growth medium contained 25 mM  $(NH_4)_2SO_4$  and other constituents as described previously (21). Cultures were inoculated with 40 ml of a 2-day-old culture of  $N$ . europaea grown on the same medium. Nitrite concentrations were determined spectrophotometrically by using the formula  $(A_{352} - A_{400})/0.0225 =$  $[NO<sub>2</sub><sup>-</sup>]$  (millimolar concentration). When the NO<sub>2</sub><sup>-</sup> concentrations in the medium reached 15 to 21 mM ( $\sim$ 42 h), the cells were harvested by centrifugation. At this age, the cell culture is in the late exponential growth phase; AMO activity for a given cell density is maximal (9) and consistent (as

indicated by the day-to-day consistency of  $V_{\text{max}}$  and  $K_m$ values for control curves in  $v^{-1}$ -versus- $S^{-1}$  plots [see below]. The cells were washed once in assay buffer, consisting of 50 mM  $NaH<sub>2</sub>PO<sub>4</sub>$  (pH 7.7) and 2 mM  $MgCl<sub>2</sub>$ , and then sedimented and resuspended in assay buffer to a constant cell density (1.8 mg of protein per ml). Cell suspensions were prepared daily, stored on ice in the dark, and used within 15 h. Protein content was determined by using the biuret assay (7) after the cells were solubilized in <sup>3</sup> N NaOH for <sup>1</sup> <sup>h</sup> at  $65^{\circ}$ C.

Materials. Liquid inhibitors included  $CCl<sub>4</sub>$  (Fisher, Fair Lawn, N.J.);  $C_2H_5Cl$  (Kodak, Rochester, N.Y.); and  $C_2H_5Br$ ,  $C_2Cl_4$ ,  $C_2H_5I$ ,  $CH_3I$ ,  $CCl_3CH_2Cl$ , and  $n-CIC_3H_7$ (Aldrich Chemical Co., Milwaukee, Wis.). Gaseous inhibitors included  $CH_4$  and  $C_2H_4$  (Airco, Vancouver, Wash.);  $C_3H_8$  and n-C<sub>4</sub>H<sub>10</sub> (Aldrich); and CH<sub>3</sub>Br, CH<sub>3</sub>Cl, and C<sub>2</sub>H<sub>6</sub> (Liquid Carbonic, Chicago, Ill.). The purities of all compounds were  $\geq 99\%$  unless otherwise noted. Other reagents included 1-allyl-2-thiourea (Kodak),  $NH<sub>2</sub>OH$ . HCl (97.8%) pure; Fisher),  $N_2H_4 \cdot H_2SO_4$  (Fisher), and  $(NH_4)_2SO_4$ (Mallinckrodt, Paris, Ky.). All other chemicals were of reagent grade.

Kinetic inhibition assays. Stock solutions of the liquid inhibitors were prepared by adding the compounds to bufferfilled vials with microsyringes. Solutions were stirred magnetically to achieve equilibrium, and then appropriate volumes were added with microsyringes to glass serum vials (volume, 6.5 ml) sealed with butyl rubber stoppers (Teflonlined stoppers were used with  $C_2Cl_4$ ). Gaseous inhibitors were added directly to sealed serum vials with microsyringes. Serum vials contained 4.9 ml of assay buffer. Inhibitor concentrations in the liquid phase of the assay vials were calculated from dilutions (solutions of liquids in buffer) or volumes added (gases), accounting for partitioning between the gas and liquid phases (determined by gas chromatography). Cells  $(50 \mu l)$  of the aforementioned suspension) were added to the reaction vials, which were preincubated for 10 min in a water bath with shaking at 30°C. The reactions were initiated by addition of an aqueous solution  $(50 \mu l)$  containing  $(NH_4)_2SO_4$  and  $N_2H_4$  in concentrations appropriate to give the desired initial concentrations in the assay vials. The vials were shaken in a reciprocating water bath (three reciprocations per s) at  $30^{\circ}$ C. After 10 min, the reactions were stopped by addition of 1-allyl-2-thiourea (to 40  $\mu$ M), a potent, specific inhibitor of  $NH<sub>3</sub>$  oxidation (16). The amount of  $NO<sub>2</sub><sup>-</sup>$  produced in the reactions was determined colorimetrically (8). For the experiment whose results are shown in Table 1,  $NH<sub>3</sub>$  concentrations were determined colorimetrically as described previously (27).

To examine  $NH_3$  as an inhibitor of  $C_2H_4$  oxidation by AMO, we determined the inhibition pattern for several fixed  $NH_4$ <sup>+</sup> concentrations with variable  $C_2H_4$  concentrations. The production of ethylene oxide was quantified by gas chromatography as described previously (19) (see Fig. 5). The reaction conditions were as described above, including the addition of an optimized concentration of  $N_2H_4$  for each combination of  $NH_4^+$  and  $C_2H_4$  (see below).

Analysis of kinetic inhibition data. The rates of  $NO<sub>2</sub>$ formation (v) (or of  $C_2H_4O$  formation [see Fig. 5]) obtained at various  $NH_4$ <sup>+</sup> concentrations (S) at a fixed inhibitor concentration were fit to the equation  $v = (V_{\text{max}} \cdot S)(K_m +$  $S$ <sup>-1</sup> by using the unweighted least-squares method and the Marquardt-Levenberg algorithm for nonlinear curve fitting (SigmaPlot; Jandel Corp.). Data for tetrachlorinated inhibitors clearly exhibited more complex behavior than for the remaining inhibitors; therefore,  $K_i$  values were not determined for these compounds. The datum points in Fig. 7 are connected by straight lines to indicate that they correspond to a given inhibitor concentration. The kinetic inhibition data were plotted as  $v^{-1}$  versus  $S^{-1}$  at several inhibitor concentrations to facilitate visual analysis. The inhibition constants  $K_{iE}$  and  $K_{iES}$  were obtained by replotting the inhibitor concentrations versus the slopes or y intercepts obtained on the  $v^{-1}$ -versus-S<sup>-1</sup> plots, respectively. The constants were taken as the absolute values of the  $x$  intercepts on the appropriate replots. For purified enzymes with one substrate and an unreactive inhibitor,  $K_{iE}$  and  $K_{iES}$  are the dissociation constants for binding of the inhibitor to the free enzyme (E) and the enzyme-substrate complex (ES), respectively (4). Our system provides apparent  $\hat{K}_i$  values that cannot be considered true dissociation constants. However, these values should provide reasonable approximations for the relative affinities of these inhibitors for AMO in vivo.

Addition of hydrazine to circumvent reductant limitation. To eliminate reductant depletion caused by the oxidation of alternate substrates by AMO, we added hydrazine to the reaction mixture at a concentration that gave the maximum  $NO_2^-$  production rate. This optimum  $N_2H_4$  concentration was determined empirically for each combination of  $NH<sub>4</sub>$ <sup>+</sup> and inhibitor concentrations as follows. Hydrazine concentrations (0, 0.1, 0.2, 0.3, 0.5, 0.7, and 0.9 mM) were tested for 0.5, 1, and 5 mM  $NH<sub>4</sub><sup>+</sup>$  for each of the high, low, and intermediate inhibitor concentrations (five concentrations were used for most inhibitors). The optimum  $N_2H_4$  concentration was then interpolated for the remaining combinations of  $NH<sub>4</sub>$ <sup>+</sup> and inhibitor concentrations.

 $V_{\text{max}}$  and  $K_{\text{m}}$  determinations for  $C_2H_4$  and  $C_2H_6$ .  $V_{\text{max}}$  and  $K<sub>m</sub>$  values were determined for the alternate substrates  $C<sub>2</sub>H<sub>4</sub>$ and  $C_2H_6$  by using  $N_2H_4$  (added from aqueous stock solutions) to provide reductant. Oxidation rates of  $C_2H_4$  and  $C_2H_6$  were maximized with 0.8 mM N<sub>2</sub>H<sub>4</sub>; varying the N<sub>2</sub>H<sub>4</sub> concentration was unnecessary. The respective products ethylene oxide and ethanol were quantified by gas chromatography as described previously (19). All other reaction conditions were as described above.

Alternate substrate oxidations with  $NH<sub>3</sub>$  as the sole reductant source. The effects of increasing  $NH<sub>4</sub><sup>+</sup>$  concentrations on the oxidation rates of  $C_2H_4$ , CH<sub>3</sub>Br,  $C_2H_5Br$ , and CH<sub>3</sub>Cl were determined. The alternate substrates (300  $\mu$ M in the aqueous phase) were combined with cells, preincubated as above, and  $(NH_4)_2SO_4$  was added (final  $NH_4$ <sup>+</sup> concentrations, 1, 2, 5, 10, 20, and 40 mM) to initiate the reaction. Oxidation rates with endogenous reductant only were determined in the absence of  $NH_4$ <sup>+</sup> (see Table 4). Hydrocarbon and halogenated hydrocarbon oxidations were determined as the amount of product formed or the difference between the initial substrate concentrations and the substrate concentration that remained after a fixed period. Substrates and products were quantified with liquid-phase injections by using gas chromatography. All other reaction conditions were as described above.

#### RESULTS

Determination of the validity of a coupled assay to measure rates of NH<sub>3</sub> oxidation in the presence of AMO inhibitors. We sought to investigate the kinetic mechanisms of the interactions of hydrocarbon and halogenated hydrocarbon compounds with the physiological substrate  $NH<sub>3</sub>$ . AMO activity can be determined in a number of ways, including gaschromatographic analysis of organic substrate depletion and determination of the residual  $NH<sub>4</sub>$ <sup>+</sup> concentration by use of

TABLE 1. Comparison of ammonium consumed and nitrite produced by whole cells of N. europaea in the presence

of ethylene and/or hydrazine <sup>a</sup>					
<b>Addition</b>	Amt of ammonium consumed $(\mu \text{mol})$ produced $(\mu \text{mol})$	Amt of nitrite			
$0.5$ mM NH <sub>4</sub> <sup>+</sup>	1.52	1.58			
1 mM $NH4$ <sup>+</sup>	2.76	2.77			
$0.5$ mM NH <sub>4</sub> <sup>+</sup> + 0.7 mM N <sub>2</sub> H <sub>4</sub>	1.18	1.19			
1 mM $NH_4$ <sup>+</sup> + 0.7 mM $N_2H_4$	1.93	1.89			
0.5 mM NH <sub>4</sub> <sup>+</sup> + 690 $\mu$ M C <sub>2</sub> H <sub>4</sub> + $0.5$ mM $N_2H_4$	0.61	0.61			
1 mM NH <sub>4</sub> <sup>+</sup> + 690 $\mu$ M C <sub>2</sub> H <sub>4</sub> + $0.5$ mM $N_2H_4$	1.14	1.16			

<sup>a</sup> Reactions were stopped with  $C_2H_2$  after 1 h. Ammonium and nitrite concentrations were measured as described in Materials and Methods.

an ion-selective electrode or a colorimetric assay. However, these methods suffer from the need to accurately determine small changes in  $NH<sub>3</sub>$  or alternate substrate concentration. We chose to determine rates of  $NO<sub>2</sub><sup>-</sup>$  production from  $NH<sub>3</sub>$ as a measure of AMO activity; colorimetric  $NO<sub>2</sub>$ <sup>-</sup> quantification is <sup>a</sup> simple and sensitive assay. A shortcoming of this method is that  $NO_2^-$  production involves the coupling of two enzyme activities-AMO and HAO-through the intermediate NH<sub>2</sub>OH. Therefore, a number of assumptions are inherent in this assay. The first assumption was that all the oxidized NH<sub>3</sub> was converted to  $NO_2^-$ . To test this assumption, we performed an experiment in which the amounts of  $NH<sub>3</sub>$  consumed were determined and compared with the amounts of  $NO<sub>2</sub><sup>-</sup>$  produced under various experimental conditions. As shown in Table 1, the amount of  $NH<sub>3</sub>$ consumed after incubation for <sup>1</sup> h equaled the amount of  $NO<sub>2</sub><sup>-</sup>$  produced under all conditions tested, which included the presence of a representative inhibitor,  $C_2H_4$  (690  $\mu$ M), and/or the reductant  $N_2H_4$  (0.7 mM). This approach was not feasible for measuring small changes in  $NH<sub>4</sub>$ <sup>+</sup> concentration occurring during 10-min reaction periods, as used in the kinetic assays. However, when the highest concentration of an alternate substrate/inhibitor was used (with its optimal  $N_2H_4$  concentration [see below]) and AMO was specifically and rapidly inactivated with  $C_2H_2$  after 10-min reactions, no significant further increases in  $NO<sub>2</sub>$  concentration were measured after continued incubation of the reaction mixtures. Supraoptimal  $N_2H_4$  concentrations diminished  $NO_2^$ production over 10-min reactions but also correlated with significant increases in  $NO_2^-$  concentration with extended incubations. These observations can be explained if negligible NH<sub>2</sub>OH concentrations accumulate with optimal  $N_2H_4$ concentrations, whereas supraoptimal  $N_2H_4$  concentrations cause accumulation of  $NH<sub>2</sub>OH$ .

The second assumption was that changes in the concentrations of substrates, inhibitors, and products during the time course of the reaction (10 min) did not affect the observed rates of  $NO_2^-$  production. To test this assumption, we determined time courses of  $NO<sub>2</sub><sup>-</sup>$  production with the inhibitor  $C_2H_4$  under the conditions used for Fig. 2. The reaction rates were constant up to 16 min. In subsequent experiments, the rates were determined from the first 10 min of the reaction. Similar tests of rate constancy were conducted for all 15 compounds examined; rates of  $NO<sub>2</sub>$ production were constant over the time course of the experiments, with only  $C_2H_5Br$  and  $C_2H_5I$  causing slight rate decreases at the highest inhibitor concentrations.

The third assumption was that any inhibition of  $NH<sub>3</sub>$ 



FIG. 2. Time courses of  $NO<sub>2</sub><sup>-</sup>$  production by N. europaea. For each line, reactions in quintuplicate vials were initiated by addition of cells and individually stopped at 4-min intervals by addition of  $C_2H_2$ . For vials containing  $C_2H_4$ , N<sub>2</sub>H<sub>4</sub> concentrations providing maximum  $NO<sub>2</sub>$  production were determined (see Materials and Methods) and included in quintuplicate vials. Symbols:  $\blacksquare$ , 0.5 mM  $NH_4^+$ ;  $\bullet$ , 1 mM NH<sub>4</sub><sup>+</sup>;  $\blacktriangle$ , 5 mM NH<sub>4</sub><sup>+</sup>;  $\Box$ , 0.5 mM NH<sub>4</sub><sup>+</sup> + 690  $\mu$ M C<sub>2</sub>H<sub>4</sub> + 0.7 mM N<sub>2</sub>H<sub>4</sub>; 0, 1 mM NH<sub>4</sub><sup>+</sup> + 690  $\mu$ M C<sub>2</sub>H<sub>4</sub> + 0.7 mM  $N_2H_4$ ;  $\triangle$ , 5 mM  $NH_4^+$  + 690  $\mu$ M  $C_2H_4$  + 0.3 mM  $N_2H_4$ .

oxidation observed was specific for AMO and was not due to inhibition of HAO or other enzymes involved in the coupled reaction. To test this assumption, we investigated whether the oxidation of  $NH<sub>2</sub>OH$  to  $NO<sub>2</sub><sup>-</sup>$  by HAO was influenced by any of the <sup>15</sup> inhibitors tested. AMO was inactivated with  $C_2H_2$ , a mechanism-based inactivator of AMO (15). Reactions were stopped after 8 min by addition of an aliquot of the reaction mixture to the acidic reagent for the  $NO<sub>2</sub>$ assay. Even at the highest concentrations of the inhibitors used to obtain the kinetic data, the oxidation of  $NH<sub>2</sub>OH$  (200  $\mu$ M) was not inhibited by 14 of the compounds. Only  $CCl<sub>3</sub>CH<sub>2</sub>Cl$  (1.2 mM) inhibited the oxidation of NH<sub>2</sub>OH (by 18%). This indicates that HAO and other enzymes and proteins required in the oxidation of  $NH<sub>2</sub>OH$  to  $NO<sub>2</sub>$  in intact cells were not influenced by the inhibitors.

Because the reactions were carried out with intact cells, a fourth assumption was that  $NH<sub>4</sub>$ <sup>+</sup> diffusion gradients between the medium and the cell periplasm were not influenced by changes in AMO activity. To determine whether NH4' concentration gradients exist, we partially and specifically inactivated AMO in whole cells with light (10) and then adjusted the concentration of the cells to give the same maximum velocity of  $NO_2^-$  production as in untreated control cells (at 20 mM  $NH_4^+$ ). Rates of  $NO_2^-$  production as a function of  $NH_4$ <sup>+</sup> concentration (0.33 to 20 mM) were determined. AMO inactivation should allow any  $NH<sub>4</sub>$ <sup>+</sup> diffusion gradient to approach equilibrium, resulting in a decrease in the apparent  $K_m$  for  $NH_4^+$  (17). With 0, 52, 82, and 92% inactivation, the apparent  $K_{m}$ s were 1.21, 1.17, 1.11, and 1.02 mM, respectively. These results suggest that an NH4+ diffusion gradient, if it existed, was small. Therefore, any changes in the gradient as a result of addition of inhibitors would not be expected to have a significant impact on the kinetics of  $NO_2^-$  production. In summary, these results confirm the validity of determining rates of  $NO<sub>2</sub>$ production from intact cells as <sup>a</sup> measure of AMO activity.

Addition of hydrazine to circumvent reductant limitation. In previous studies, it was shown that the effects of alternate substrates on the rates of AMO activity cannot be accounted for solely by direct effects occurring at the active site of



FIG. 3. Influence of  $N_2H_4$  on  $NO_2^-$  production by N. europaea. (A) Inhibition of  $NH_4^+$ -dependent  $NO_2^-$  production by  $N_2H_4$  in the absence of an alternate substrate. Reactions were stopped by addition of aliquot to acidic NO<sub>2</sub><sup>-</sup> assay reagent immediately after a 10-min reaction. Symbols:  $\Box$ , 0.5 mM NH<sub>4</sub><sup>+</sup>;  $\blacksquare$ , 5 mM NH<sub>4</sub><sup>+</sup>. (B) Influence of  $NH_4^+$  on the optimum  $N_2H_4$  concentration required for maximum  $NO_2^-$  production with 690  $\mu$ M C<sub>2</sub>H<sub>4</sub> present. Symbols:<br>  $\bigcirc$ , 0.5 mM NH<sub>4</sub><sup>+</sup>;  $\bigcirc$ , 5 mM NH<sub>4</sub><sup>+</sup>. (C) Influence of C<sub>2</sub>H<sub>4</sub> on the optimum  $N_2H_4$  concentration required for maximum  $NO_2^-$  production from 1 mM NH<sub>4</sub><sup>+</sup>. Symbols:  $\triangle$ , 170  $\mu$ M C<sub>2</sub>H<sub>4</sub>;  $\blacktriangle$ , 1,040  $\mu$ M  $C_2H_4$ .

AMO (14, 19). Because the products of the alternate-substrate oxidations are not further oxidized, the oxidation of alternate substrates by AMO results in <sup>a</sup> net drain of reductant (Fig. 1). To discriminate between direct  $NH<sub>3</sub>$  and inhibitor interactions on AMO and any secondary effects due to reductant limitation, it was necessary to eliminate the latter effects. This was achieved by addition of hydrazine to the reaction mixtures. Hydrazine is an alternate substrate for HAO (18), is an effective electron donor for AMO-catalyzed oxidations (13), and is oxidized by HAO to produce  $N_2$ , which does not interfere with the colorimetric  $NO_2^-$  assay.

Addition of  $N_2H_4$  to cells in the presence of  $NH_4^+$  and the absence of a hydrocarbon inhibitor did not stimulate the rates of  $NO_2^-$  production, indicating that  $NH_3$  oxidation was not reductant limited under such conditions. Indeed, increasing concentrations of  $N_2H_4$  progressively inhibited the rates of  $NO_2^-$  production (Fig. 3A). Excess  $N_2H_4$  might prevent the oxidation of  $NH<sub>2</sub>OH$  generated from  $NH<sub>3</sub>$  and hence decrease the amount of  $NO<sub>2</sub>$ <sup>-</sup> detected. Furthermore, the subsequent increase in the intracellular concentration of  $NH<sub>2</sub>OH$  may lead to direct inhibition of AMO (1, 14). It seems unlikely that  $N_2H_4$  directly inhibited AMO activity at the concentrations used  $(<1$  mM) in the inhibition experiments, because, in the absence of  $NH<sub>4</sub>$ <sup>+</sup>, the rate of ethylene (920  $\mu$ M) oxidation was not diminished at 1.0 mM N<sub>2</sub>H<sub>4</sub> relative to lower concentrations (data not shown).

The effects of  $N_2H_4$  addition on the rates of  $NO_2^$ production in the presence of the inhibitor  $C_2H_4$  are shown



FIG. 4. Effect of  $N_2H_4$  on  $NH_4^+$ -dependent  $NO_2^-$  production rates by *N. europaea* in the presence of 345  $\mu$ M C<sub>2</sub>H<sub>4</sub> (and control).<br>Symbols:  $\Box$ , NH<sub>4</sub><sup>+</sup> only;  $\odot$ , C<sub>2</sub>H<sub>4</sub> without N<sub>2</sub>H<sub>4</sub>;  $\triangle$ , C<sub>2</sub>H<sub>4</sub> + 0.1 mM  $N_2H_4$ ;  $\bullet$ ,  $N_2H_4$  concentrations selected (for each  $NH_4^+$  concentration) which yielded maximum  $NO<sub>2</sub>$ <sup>-</sup> production.

in Fig. 3B and C. In contrast to the situation in the absence of  $C_2H_4$ , low concentrations of  $N_2H_4$  stimulated the rate of  $NO<sub>2</sub><sup>-</sup>$  production in the presence of  $C<sub>2</sub>H<sub>4</sub>$ . This stimulation was attributed to circumvention of the reductant limitation imposed by the oxidation of  $C_2H_4$ . As in the absence of an alternate substrate, higher concentrations of  $N_2H_4$  resulted in a decreased rate of  $NO<sub>2</sub><sup>-</sup>$  production, presumably for the reasons stated above. These results demonstrate that different concentrations of  $N_2H_4$  are required to achieve optimal rates of  $NO<sub>2</sub>$ <sup>-</sup> formation under different conditions. Since increasing concentrations of the same compound will cause greater depletion of the reductant supply (Fig. 3C), it is obvious that each set of experimental conditions is associated with a unique optimal  $N_2H_4$  concentration. Therefore, in all subsequent experiments, the concentration of  $N_2H_4$ supporting the maximum rate of  $NO<sub>2</sub>$  production was determined for each unique set of conditions. Throughout this text, "optimal  $N_2H_4$  concentration" refers to the concentration of  $N_2H_4$  required to maximize the rate of NO<sub>2</sub><sup>-</sup> production under the stated conditions.

Maximum  $NO_2^-$  production rates with optimal  $N_2H_4$ concentrations were constant for 16 min (Fig. 2). Also,  $NH_3$ -dependent  $NO_2^-$  production equaled  $NH_3$  consumption over 1 h when 0.7 mM  $N_2H_4$  was present (Table 1). These results show that the assumptions of the previous section were still valid when  $N_2H_4$  was included in the assay. We also assumed that optimal  $N_2H_4$  concentrations replenished the reductant to a constant level and that only the initial inhibitor and  $NH<sub>3</sub>$  concentrations varied significantly among reaction vials.

Saturation kinetics are observed in the coupled assay. The coupled assay (NH<sub>3</sub> to  $NO<sub>2</sub><sup>-</sup>$ ), with addition of optimized concentrations of  $N_2H_4$ , was used to determine the velocity of  $NH<sub>3</sub>$  oxidation as a function of  $NH<sub>3</sub>$  concentration. As shown in Fig. 4, saturation kinetics were observed for  $NH<sub>3</sub>$ alone. When  $C_2H_4$  was included in the reaction mixture, the rates of  $NO_2^-$  production decreased and the pattern was no longer typical of saturation kinetics. Addition of a single concentration of  $N_2H_4$  (0.1 mM) increased the rates, but the curve was not hyperbolic. However, when optimized concentrations of  $N_2H_4$  were added to the reaction mixture along with  $C_2H_4$ , the plot once again was typical of satura-



FIG. 5. Lineweaver-Burk plot for  $C_2H_4$  as an inhibitor of NH<sub>4</sub><sup>+</sup>dependent NO<sub>2</sub> production in N. europaea. Symbols:  $\Box$ , 0  $\mu$ M  $C_2H_4$ ;  $\bigcirc$ , 345  $\mu M C_2H_4$ ;  $\bigtriangleup$ , 520  $\mu M C_2H_4$ ;  $\blacksquare$ , 690  $\mu M C_2H_4$ ;  $\spadesuit$ , 860  $\mu$ M C<sub>2</sub>H<sub>4</sub>;  $\blacktriangle$ , 1,040  $\mu$ M C<sub>2</sub>H<sub>4</sub>. (Inset) Slope replot. Slopes of curves were plotted against inhibitor concentration to obtain  $K_{iE}$ , the absolute value of the  $x$  intercept.

tion kinetics, albeit with an apparently higher  $K_m$ . Thus, including optimal  $N_2H_4$  concentrations was necessary to obtain saturation kinetics.

Kinetic inhibition patterns and constants. By using the assay described above, we investigated the inhibition of  $NH<sub>3</sub>$ oxidation to  $NO<sub>2</sub><sup>-</sup>$  by the 15 hydrocarbons and halogenated hydrocarbons listed above. Except for  $CH<sub>3</sub>I$ , all of these inhibitors have been reported to be either substrates for AMO or class 1 nonsubstrates  $(C_2Cl_4$  and  $CCl_4$ ) (11, 20, 21). For each inhibitor, a series of  $v^{-1}$ -versus- $S^{-1}$  curves were obtained, with each curve representing a fixed concentration of inhibitor. Because each experiment included a control saturation curve with no inhibitor added, this provided a means of determining the day-to-day variability of the kinetic data. In 15 experiments, an average  $K_m$  for NH<sub>4</sub><sup>+</sup> of 1.34  $\pm$  0.22 mM and an average  $V_{\text{max}}$  of 1.59  $\pm$  0.17  $\mu$ mol · min<sup>-1</sup> · mg of protein<sup>-1</sup> were determined. This consistency facilitated comparison of results obtained on different days.

As an example of this approach, the results of the inhibition of NH<sub>3</sub> oxidation by  $C_2H_4$  are shown in Fig. 5. The double-reciprocal plot reveals a pattern typical of a competitive inhibitor. The replot of slopes versus inhibitor concentrations (slope replot) is linear and yields a  $K_{iE}$  of 660  $\mu$ M (Fig. <sup>5</sup> inset). We also determined the inhibition pattern with  $NH<sub>3</sub>$  as the inhibitor and  $C<sub>2</sub>H<sub>4</sub>$  as the variable substrate. The rate of ethylene oxide formation was determined. Again, the pattern was typical of a competitive inhibitor, although the slope replot was not linear (Fig. 6). For a competitive inhibitor which also acts as a substrate, the  $K_i$  for the compound as inhibitor should equal its  $K_m$  as substrate (4). The  $K_i$  for C<sub>2</sub>H<sub>4</sub> of 660  $\mu$ M compares favorably with the  $K_m$ for  $C_2H_4$  of 658  $\pm$  154  $\mu$ M (see Table 3). Methane was also a competitive inhibitor of  $NH<sub>3</sub>$  oxidation (see Table 2). The  $K_i$  for CH<sub>4</sub> (3,240  $\mu$ M) was about fivefold higher than the  $K_i$ for  $C_2H_4$ . The high  $K_i$  for CH<sub>4</sub> is consistent with the observation that  $CH<sub>4</sub>$  is a relatively poor substrate for AMO (13).

Most of the compounds we examined did not give inhibition patterns typical of competitive inhibitors. Indeed, non-



FIG. 6. Lineweaver-Burk plot for NH<sub>3</sub> as an inhibitor of  $C_2H_4$ oxidation by  $N$ . europaea. Ethylene oxide production as a function of  $C_2H_4$  concentration. Symbols:  $\Box$ , 0 mM NH<sub>4</sub><sup>+</sup>;  $\odot$ , 0.5 mM NH<sub>4</sub><sup>+</sup>;  $\triangle$ , 5 mM NH<sub>4</sub><sup>+</sup>; **.**, 15 mM NH<sub>4</sub><sup>+</sup>. (Inset) Slope replot.

competitive patterns were the most common. The doublereciprocal plot obtained for  $C_2H_5Cl$  (Fig. 7) exemplifies the noncompetitive pattern for inhibition of  $NH<sub>3</sub>$  oxidation. Replots (Fig. 7 inset) of inhibitor concentrations versus slopes or y intercepts of the curves in Fig. 7 provided values for  $K_{iE}$  (1.41 mM) and  $K_{iES}$  (1.42 mM), respectively. These similar values may have resulted from  $C_2H_5Cl$  having equal affinity to free enzyme (E) and to the ES complex (i.e., enzyme with  $NH<sub>3</sub>$  bound). All other noncompetitive inhibitors exhibited mixed noncompetitive patterns  $(K_{iE} \neq K_{iES})$ . These inhibitors were the hydrocarbons  $C_2H_6$ ,  $C_3H_8$ , and  $n\text{-}C_4H_{10}$  and the halogenated hydrocarbons CH<sub>3</sub>Cl,  $n$ -ClC<sub>3</sub>H<sub>7</sub>, CH<sub>3</sub>Br, C<sub>2</sub>H<sub>5</sub>Br, CH<sub>3</sub>I, and C<sub>2</sub>H<sub>5</sub>I. The iodinated compounds gave the lowest  $K_{iE}$  and  $K_{iE}$  values, which indicates strong binding to AMO. Ratios of  $K_{iE}/K_{iES}$  increased in the following sequence:  $CH_3Cl$  (0.20),  $C_2H_6$ (0.25), CH<sub>3</sub>Br (0.33), C<sub>2</sub>H<sub>5</sub>Cl (0.99), C<sub>2</sub>H<sub>5</sub>Br (2.23), n-C<sub>4</sub>H<sub>10</sub>  $(3.07)$ , C<sub>3</sub>H<sub>8</sub> (3.25), CH<sub>3</sub>I (4.33), n-ClC<sub>3</sub>H<sub>7</sub> (5.10), and C<sub>2</sub>H<sub>3</sub>I



FIG. 7. Lineweaver-Burk plot for  $C_2H_5Cl$  as an inhibitor of NH<sub>4</sub><sup>+</sup>-dependent NO<sub>2</sub><sup>-</sup> production in *N. europaea.* Symbols:  $\square$ , 0<br>mM C<sub>2</sub>H<sub>5</sub>Cl;  $\odot$ , 2.34 mM C<sub>2</sub>H<sub>5</sub>Cl;  $\triangle$ , 3.07 mM C<sub>2</sub>H<sub>5</sub>Cl; ■, 3.80 mM  $C_2H_5C1$ ;  $\bullet$ , 4.54 mM  $C_2H_5C1$ ;  $\bullet$ , 5.27 mM  $C_2H_5C1$ . (Inset) Slope and intercept replots. The inhibitor concentration was replotted against slopes (O) or y intercepts ( $\blacksquare$ ) to obtain  $K_{iE}$  and  $K_{iES}$ , respectively. Data from the 5.27 mM  $C_2H_5Cl$  curve were omitted from replots.



FIG. 8. Lineweaver-Burk plot for CCl<sub>4</sub> as an inhibitor of NH<sub>4</sub><sup>+</sup>dependent NO<sub>2</sub><sup>-</sup> production in *N. europaea*. Symbols:  $\Box$ , 0  $\mu$ M<br>CCl<sub>4</sub>;  $\bigcirc$ , 75  $\mu$ M CCl<sub>4</sub>;  $\bigtriangleup$ , 150  $\mu$ M CCl<sub>4</sub>;  $\blacksquare$ , 225  $\mu$ M CCl<sub>4</sub>;  $\blacksquare$ , 300  $\mu$ M CCl<sub>4</sub>;  $\blacktriangle$ , 375 µM CCl<sub>4</sub>.

(9.67). With the inhibitors propylene, trans-dichloroethylene,  $CH_2ClCH_2Cl$ , and  $CH_2BrCH_2Cl$ , the rates of  $NH_3$ oxidation as a function of time were constant only at inhibitor concentrations causing little inhibition of  $NH<sub>3</sub>$ oxidation. Nonetheless, all four inhibitors showed noncompetitive patterns at these low concentrations (data not shown).

Not all compounds gave inhibition patterns typical of either competitive or noncompetitive inhibitors. With the tetrachlorinated compounds  $C_2Cl_4$ , CCl<sub>4</sub>, and CCl<sub>3</sub>CH<sub>2</sub>Cl, the double-reciprocal plots were nonlinear. For example, the plot for  $\text{CCI}_4$  (Fig. 8) shows concave-down curves, especially at high inhibitor concentrations. This pattern does not allow determination of  $K_{iE}$  and  $K_{iES}$  values. For comparison with other inhibitors, Table 2 includes inhibitor concentrations causing 50% inhibition of  $NO_2^-$  production from 1 mM  $NH_4^+$ . By this measure,  $C_2Cl_4$  was the most potent inhibitor we examined.

For each inhibitor we investigated, the range of  $N_2H_4$ concentrations required to optimize the rates of  $NO<sub>2</sub>$ production is indicated in Table 2. For example, with  $C_2H_4$ the optimal  $N_2H_4$  concentrations varied from 0.1 to 0.7 mM and  $N_2H_4$  requirements were influenced by the NH<sub>4</sub><sup>+</sup> concentration (Fig. 3B). In general, the higher  $C_2H_4$  concentrations required higher  $N_2H_4$  concentrations to replace the reductant diverted to  $C_2\overline{H}_4$  oxidation (Fig. 3C). Other inhibitors previously shown to be oxidized rapidly (19) also required high concentrations of  $N_2H_4$  to replenish reductant and maximize  $NO<sub>2</sub><sup>-</sup>$  production, whereas slowly oxidized inhibitors required lower concentrations of  $N_2H_4$  (19, 21). For inhibitors with competitive character,  $(K_{iE}/K_{iES})$  ratios,  $\langle 1 \rangle$ , the optimal N<sub>2</sub>H<sub>4</sub> concentration decreased with increasing  $NH_4$ <sup>+</sup> concentration. This is consistent with a decreased diversion of reductant to the alternate substrate as its binding to AMO was outcompeted by  $NH<sub>3</sub>$ ; NH<sub>3</sub>-derived NH<sub>2</sub>OH would provide more of the total reductant at higher  $NH<sub>4</sub><sup>+</sup>$  concentrations. For noncompetitive oxidizable inhibitors with  $K_{iE}/K_{iES} \ge 1$  (including C<sub>2</sub>H<sub>5</sub>Cl), the optimal  $N_2H_4$  requirements increased with increasing inhibitor concentration but did not vary with the  $NH<sub>4</sub>$ <sup>+</sup> concentration for a given inhibitor concentration. In contrast, compounds that were oxidized only slowly (such as  $CH<sub>3</sub>I$ ,  $C<sub>2</sub>H<sub>5</sub>I$ , or  $CCl_3CH_2Cl$  (19, 21) or not at all  $(C_2Cl_4$  and  $\overline{CCl_4}$ ) (21)

Inhibitor	Inhibition pattern <sup>a</sup>	$K_{iE}$ $(\mu M)^b$	$K_{iES}$ $(\mu M)^b$	[ $\mu$ M I] <sub>50%</sub> $(1 \text{ mM})$ $NH4+)c$	$[N2H4]$ range used $(mM)^d$	$K_{iE}$ $K_{iES}$
Methane	$\mathbf C$	3,240		>1,800	$0.05 - 0.3$	
Ethane	NC	220	890 <sup>e</sup>	520	$0.1 - 0.5$	0.25
Propane	NC	1,430	440	840	$0.1 - 0.5$	3.25
$n$ -Butane	NC	920	300	450	$0.2 - 0.5$	3.07
Ethylene	$\mathbf C$	660		550	$0.1 - 0.7$	
Chloromethane	NC	300	1,470	550	$0.1 - 0.7$	0.20
Chloroethane	NC	$1,410^e$	1,420e	2,340	$0.3 - 0.7$	0.99
$n$ -Chloropropane	NC	$5,150^e$	1,010	2,000	$0.3 - 0.5$	5.10
<b>Bromomethane</b>	NC	500	1,490	770	$0.1 - 0.7$	0.33
<b>Bromoethane</b>	NC	490	220	550	$0.1 - 0.7$	2.23
Iodomethane	NC	130	30	80	0	4.33
Iodoethane	NC	290	30	80	0.1	9.67
Tetrachloroethylene	CD			5	0	
Carbon tetrachloride	CD			300	0	
1,1,1,2-Tetrachloroethane	CD			500	0.1	

TABLE 2. Apparent kinetic inhibition constants from slope and intercept replots of  $v^{-1}$  versus  $S^{-1}$  plots with N. europaea whole cells

<sup>a</sup> Patterns of curves on double-reciprocal plots were as follows: C, competitive; NC, noncompetitive; CD, concave-down.

 $b_{K_{\text{I}}E}$  and  $K_{\text{IES}}$  are apparent inhibition constants derived from slope and intercept replots, respectively. Data in replots were fit to the  $y = mx + b$  formula by the least-squares method.

These values represent the micromolar inhibitor concentrations required for 50% inhibition of NO<sub>2</sub><sup>-</sup> production from 1 mM NH<sub>4</sub><sup>+</sup>. The N<sub>2</sub>H<sub>4</sub> concentration

was optimized in each case.<br>  $\frac{d}{dx}$  These values include the N<sub>2</sub>H<sub>4</sub> concentrations used in the kinetic assays.

<sup>a</sup> These values include the N<sub>2</sub>H<sub>4</sub> concentrations used in the kinetic assays.<br>
<sup>e</sup> One (C<sub>2</sub>H<sub>5</sub>Cl and C<sub>2</sub>H<sub>6</sub>) or two (n-ClC<sub>3</sub>H<sub>7</sub>) datum points were omitted from these replots. The remaining replots included all (f 0.03).

required little (0.1 mM) or no  $N_2H_4$  to supplement  $NH_3$ derived reductant.

 $V_{\text{max}}$  values were obtained for the oxidation of C<sub>2</sub>H<sub>6</sub> to ethanol and of  $C_2H_4$  to ethylene oxide in the presence of  $N_2H_4$  and the absence of competing NH<sub>3</sub>. In Table 3 the values are compared with those obtained for  $NH<sub>3</sub>$ . All three  $V_{\text{max}}$  values are about 1.5  $\mu$ mol. min<sup>-1</sup>. mg of protein<sup>-1</sup>. The  $K_m$  values for  $C_2H_4$  and  $C_2H_6$  are similar and are lower than the value obtained for  $NH_4$ <sup>+</sup>. However, the substrate for AMO is considered to be  $NH<sub>3</sub>$ , not  $NH<sub>4</sub><sup>+</sup>$  (3). At pH 7.7, 1.35 mM  $NH_4$ <sup>+</sup> corresponds to an  $NH_3$  concentration of 54  $\mu$ M. Thus, the  $K_m$  for NH<sub>3</sub> is about 10-fold lower than the  $K<sub>m</sub>$ s for C<sub>2</sub>H<sub>4</sub> and C<sub>2</sub>H<sub>6</sub>. In these experiments, 0.8 mM N<sub>2</sub>H<sub>4</sub> did not inhibit the oxidation of  $C_2H_4$  and  $C_2H_6$  at their lowest concentrations and was adequate for their highest concentrations; therefore, 0.8 mM  $\rm N_2H_4$  was used at all substrate concentrations.

Alternate substrate oxidations with  $NH<sub>3</sub>$  as the sole reductant source. The effects of increasing the concentration of  $NH<sub>4</sub>$ <sup>+</sup> on the oxidations of alternate substrates were studied to corroborate the inhibition data by further characterizing the interactions of  $NH<sub>3</sub>$  with alternate substrate inhibitors. High concentrations of  $NH<sub>3</sub>$  (>10 mM) were found to inhibit the oxidation of  $C_2H_4$  (Table 4), with maximum  $C_2H_4O$ <br>production occurring at 5 mM  $NH_4^+$ . Oxidation of  $C_2H_5Br$ , a clearly noncompetitive inhibitor  $(K_{iE} > K_{iES})$ , was not diminished at high  $NH_4$ <sup>+</sup> concentrations; 40 mM  $NH_4$ <sup>+</sup> caused the greatest acetaldehyde production  $(0.44 \mu mol)$  in 10 min). However, some noncompetitive inhibitors showed competitive character ( $K_{iE} \ll K_{iES}$ ); CH<sub>3</sub>Cl and CH<sub>3</sub>Br were chosen as examples. Substrate depletion was used to monitor their oxidation; maximum substrate depletion occurred with 2 mM  $NH_4^+$  for CH<sub>3</sub>Cl and with 5 mM  $NH_4$ <sup>+</sup> for CH<sub>3</sub>Br. These results are comparable to those for  $C_2H_4$ .

## DISCUSSION

We studied the inhibition by hydrocarbons and halogenated hydrocarbons of  $NH<sub>3</sub>$  oxidation by AMO to learn more about the interaction of these compounds with this enzyme. Despite the complexity of the experimental system,  $\overline{NO_2}^$ production rates at various  $NH<sub>3</sub>$  and inhibitor concentrations yielded inhibition plots showing simple patterns. The patterns we observed can be interpreted in terms of direct inhibitor binding to the enzyme. We observed <sup>a</sup> variety of inhibition patterns ranging from competitive to nearly uncompetitive, as well as some nonclassical inhibition patterns. Our data suggest that some inhibitors bind predominantly to the site on AMO which also binds  $NH<sub>3</sub>$ , whereas other inhibitors are not excluded when  $NH<sub>3</sub>$  is bound to the enzyme. We propose an active-site model for AMO which consists of an  $N\hat{H}_3$ -binding site to which competitive inhibitors bind and an alternate site to which noncompetitive inhibitors bind. Additional binding sites would be required for  $O<sub>2</sub>$  and the site of electron donation.

Because CH<sub>4</sub> and C<sub>2</sub>H<sub>4</sub> competitively inhibit NH<sub>3</sub> oxidation, it seems reasonable that these compounds bind predominantly to the same specific site to which  $NH<sub>3</sub>$  binds. That  $C_2H_4$  and NH<sub>3</sub> bind to the same site is further evidenced by the observation that the  $K_{iE}$  (Table 2) and  $K_m$ 

TABLE 3. Apparent kinetic parameters from reaction rate studies with N. europaea

Substrate	Mean $V_{\text{max}} \pm SD^a$ (µmol of product/min/mg of protein)	Mean $K_m \pm SD^a$ $(\mu M)$	No. of trials
Ammonium	$1.68 \pm 0.15$	$1,353 \pm 109$	3
Ethylene	$1.56 \pm 0.23$	$658 \pm 154$	
Ethane	$1.44 \pm 0.08$	$522 \pm 27$	

<sup>a</sup> SD, standard deviation.





<sup>a</sup> All initial substrate concentrations in liquid medium were 300  $\mu$ M. Reaction times for oxidations of C<sub>2</sub>H<sub>4</sub>, C<sub>2</sub>H<sub>5</sub>Br, CH<sub>3</sub>Br, and CH<sub>3</sub>Cl were 10, 10, 25, and 30 min, respectively.

(Table 3) values for  $C_2H_4$  are both 660  $\mu$ M. This result is predicted for competing substrates, one of which is treated as the inhibitor  $(4)$ . Conversely, Fig. 6 shows that  $NH<sub>3</sub>$  is a competitive inhibitor of  $C_2H_4$  oxidation, which corroborates mutually exclusive binding between  $NH_3$  and  $C_2H_4$  at the NH3-binding site. Whole-cell kinetic studies with AMO in N. oceanus (26) showed that Michaelis-Menten kinetics are observed for the physiological substrate  $NH<sub>3</sub>$  alone but not when CH<sub>4</sub> is added as an inhibitor of NH<sub>3</sub> oxidation (25, 26). However, no supplemental reductant such as  $N_2H_4$  was added, and so the effects of inhibitor binding to AMO are difficult to separate from the problem of reductant limitation.

The competitive character (defined as  $K_{iE} \ll K_{iES}$ ) of inhibition by  $CH_4$ ,  $C_2H_4$ ,  $C_2H_6$ ,  $CH_3Cl$ , and  $CH_3Br$  is supported by the optimal  $N_2H_4$  requirements, which decreased with increasing  $NH_4$ <sup>+</sup> concentration for a given concentration of inhibitor. The competitive character is further corroborated by Table 4, which shows that oxidation of  $C_2H_4$ , CH<sub>3</sub>Cl, and CH<sub>3</sub>Br decreased at the highest concentrations of  $NH_4$ <sup>+</sup>. In each case, an optimum  $NH_4$ <sup>+</sup> concentration provided maximum oxidation of the alternate substrate, presumably because lower  $NH<sub>4</sub>$ <sup>+</sup> concentrations provided insufficient reductant whereas supraoptimal concentrations competitively prevented alternate substrate binding to AMO. Our data support not only the findings of Hyman and Wood for CH<sub>4</sub> (13) and C<sub>2</sub>H<sub>4</sub> (14) but also the competitive patterns obtained by Suzuki et al. for CH<sub>4</sub>, CO, and  $CH<sub>3</sub>OH$  (23). The curvature observed in the kinetic plots of the previous studies (inhibitor present) (13, 14, 23) disappeared in our plots when the optimal  $N_2H_4$  concentration was added. We thus confirm that reductant depletion in N. europaea by oxidation of (competitive) alternate substrates is a primary cause of nonlinear (concave-up) plots, as has been suggested (14). Reductant depletion probably influenced the lower  $K_{iE}$  values obtained for CH<sub>4</sub> (2 mM) and  $C_2H_4$  (80  $\mu$ M) (13, 14). Therefore, only some  $C_1$  and  $C_2$ compounds have been shown to competitively inhibit  $NH<sub>3</sub>$ oxidation by AMO.

Binding of noncompetitive inhibitors to the active site may occur at a hydrophobic region, since the inhibitors are all nonpolar. This region is likely to be less well defined than the NH3-binding site because of the greater structural diversity of alternate substrates that are noncompetitive inhibitors of NH<sub>3</sub> oxidation. Typically, noncompetitive patterns ( $K_{iE} \geq$  $K_{iES}$ ) were associated with a less variable optimal  $N_2H_4$ requirement for a given inhibitor concentration. Since inhibition was not relieved by a high  $NH<sub>4</sub>$ <sup>+</sup> concentration,  $NH<sub>3</sub>$ -derived NH<sub>2</sub>OH contributed to AMO reduction via  $HAO$  in smaller increments as the  $NH_4$ <sup>+</sup> concentration increased (relative to competitive inhibition). Also, as shown in Table 4, 40 mM  $NH<sub>4</sub><sup>+</sup>$  allowed the greatest production of

acetaldehyde from 300  $\mu$ M C<sub>2</sub>H<sub>5</sub>Br (0.50  $\mu$ mol min<sup>-1</sup> mg of protein-1). Apparently, some noncompetitive substrates can be oxidized at a site other than the  $NH<sub>3</sub>$ -binding site and at comparable rates. Rasche et al. found that  $C_2H_5Cl$  oxidation rates were undiminished or slightly increased at <sup>40</sup> mM  $NH<sub>4</sub>$ <sup>+</sup> relative to lower NH<sub>4</sub><sup>+</sup> concentrations over a range of  $C_2H_5Cl$  concentrations (19). This result supports noncompetitive binding and oxidation for  $C_2H_5Cl$ .

The similarity of  $V_{\text{max}}$  values for  $C_2H_4$ ,  $C_2H_6$ , and NH<sub>3</sub> is remarkable given that the oxidized bonds (or electron pair) differ in each case. The most plausible explanation is that a common rate-determining step limits oxidation rates for these substrates. It has been suggested that AMO reduction is rate determining in vivo (14). The similar  $V_{\text{max}}$  values indicate that  $C_2H_4$  and  $C_2H_6$  bind at the active site in an orientation allowing efficient turnover. In contrast,  $C_2H_5I$ was a poor substrate relative to other haloethanes but had high affinity for AMO (19). Apparently,  $C_2H_5I$  binds in an orientation which does not promote efficient catalysis, as well as inhibiting NH<sub>3</sub> oxidation. How  $C_2H_4$ ,  $C_2H_6$ , and NH<sub>3</sub> might bind to <sup>a</sup> common site is unknown, but it is interesting that lone electron pairs (NH<sub>3</sub>), pi electrons ( $C_2H_4$ ), and even C—H bonds  $(C_2H_6)$  may serve as metal ligands (5).

The inhibitors we chose allowed us to consider several series of structurally related compounds. The first trend in our data was an increase in the  $K_{iE}/K_{iES}$  ratio with increasing molecular size. This was observed for the alkane series  $\rm CH_4$  $\rm < C_2H_6 < C_3H_8 \approx n\text{-}C_4H_{10}$  and for halogenated hydrocarbons with increasingly longer alkyl chains but an identical halogen atom (e.g., CH<sub>3</sub>Cl, C<sub>2</sub>H<sub>5</sub>Cl, n-ClC<sub>3</sub>H<sub>7</sub>). This pattern also occurred for halomethanes (Cl, Br, I) as a group and also for haloethanes (Cl, Br, I) (halogen radii increase in the order  $Cl < Br < I$ ). This effect may have arisen from the increasing affinity of larger (and more hydrophobic) inhibitors to an alternate binding site. Also, larger inhibitors might cause greater steric hindrance of proper positioning of the active site (22).

The second trend involved the identity of the halogen substituent on monohalogenated hydrocarbons. The  $\tilde{K}_{iE}$ ,  $K_{iES}$ , and [µM I]<sub>50%</sub> values in Table 2 indicate that chlorinated compounds were generally less effective inhibitors than brominated compounds. The iodinated compounds were the most inhibitory of the monohalocarbons. This trend may have been related to increasing size or nucleophilicity of the halogen atoms (both orders were  $Cl < Br < I$ ). These data reflect the finding that haloethane reactivity (measured as acetaldehyde production in the presence of  $NH<sub>3</sub>$ ) decreased in the order  $C_2H_5Cl > C_2H_5Br > C_2H_5I$  (19).

Another observation was that concave-down reciprocal plots were obtained only for tetrachlorinated compounds. The multiple lone electron pairs on these compounds may constitute potential ligands that could allow some competition with  $NH<sub>3</sub>$  binding to the active site, whereas the molecular size of the compounds would predict a high  $K_{iE}/K_{iES}$  ratio. This would explain the concave-down curvature: a disproportionate increase in  $NO<sub>2</sub>$ <sup>-</sup> production rates with increasing  $NH<sub>4</sub>$ <sup>+</sup> concentration.

Our data support a model in which (i) the  $NH<sub>3</sub>$ -binding site can be occupied significantly only by  $C_1$  compounds and  $C_2$ hydrocarbons (including  $C_2H_2$  [15]); (ii) iodinated compounds,  $C_2$  (and larger) halogenated compounds, and most hydrocarbons  $(>C_2)$  would bind predominantly at a more hydrophobic site, to which  $NH<sub>3</sub>$  would not bind; and (iii) oxidation of an organic substrate at the alternate site could occur at a rate comparable to oxidation at the  $NH<sub>3</sub>$ -binding site. Binding at the alternate site could interfere with oxidation at the  $\text{NH}_3$ -binding site by competing for activated  $\text{O}_2$ (i.e., alternate substrate oxidation) or by interfering with turnover (e.g., by drawing the enzyme into a dead-end complex).

Vannelli et al. (24) proposed a model in which an alternate substrate such as trans-2-butene was bound to AMO through interactions at two sites. This model, which proposes a single oxidation site, was presented to explain the product ratios (alcohol/epoxide) for the substrates cis- and trans-2 butene (11) and the relative reactivities of cis- and transdibromoethylene (24). It should be noted that differing bond dissociation energies and the intrinsic steric inaccessibility of the pi bonds may have accounted for the product ratios (11, 24). Our model and the model of Vannelli et al. are not necessarily mutually exclusive; substrate binding orientations are not excluded by our model as a factor influencing bond reactivities, product ratios, or inhibition patterns.

Our model describes the experimental results in terms of the direct interactions of the inhibitors with AMO. However, given that the experiments were carried out with intact cells, other factors may have influenced the results. For example, the inhibitors could have altered the activities of enzymes other than AMO that are required for the coupled assay. This appeared not to be the case, given that the oxidation of  $NH<sub>2</sub>OH$  was not substantially altered by the inhibitors. If an  $NH<sub>4</sub>$ <sup>+</sup>/NH<sub>3</sub> diffusion gradient existed across the periplasmic membrane, addition of inhibitors could alter this gradient. Decreasing the activity of AMO would be expected to cause a shallowing of any diffusion gradient and a decrease in the apparent  $K_m$  for NH<sub>4</sub><sup>+</sup> (17). However, specific inactivation of AMO by light resulted in only small changes in the apparent  $K_m$  for NH<sub>4</sub><sup>+</sup>, which suggests that the diffusion gradient, if it existed, was small. Therefore, if the AMO inhibitors we used also diminished the apparently small gradient, only small decreases in curve slopes on the doublereciprocal plots would have resulted. It is also possible that AMO is part of <sup>a</sup> multienzyme complex in intact cells and that the kinetics we have measured are a reflection of the complex rather than the active site of AMO. Because of these and additional factors that could influence the values of measured kinetic constants, the values are referred to as apparent kinetic constants to distinguish them from the constants that would be determined if active, purified enzyme preparations were available.

In our experiments,  $N_2H_4$  was added as a source of reductant, so that reductant limitation was not a factor influencing the observed kinetics. The results provide a basis for predicting the outcome when  $N_2H_4$  is not included and  $NH<sub>4</sub><sup>+</sup>$  is the only source of reductant. For noncompetitive inhibitors ( $K_{iE} > K_{iES}$ ) which are also substrates, the rate of oxidation of the alternate substrate should not decrease substantially at high  $NH_4$ <sup>+</sup> concentrations (>20 mM). In contrast, for the alternate substrates that are competitive inhibitors of  $NH<sub>3</sub>$  oxidation or display competitive character  $(K_{iE} \ll K_{iES})$ , their rate of oxidation should decrease substantially at high  $NH_4$ <sup>+</sup> concentrations. In both cases, low concentrations of alternate substrates will inhibit AMO activity by depleting the NH<sub>3</sub>-derived reductant supply. The predicted results were observed for a competitive inhibitor  $(C_2H_4)$ , a distinctly noncompetitive inhibitor (C<sub>2</sub>H<sub>5</sub>Br), and two noncompetitive inhibitors with competitive character  $(CH_3Cl$  and  $CH_3Br$ ) (Table 4).

In summary, we have observed trends regarding hydrocarbon and halogenated hydrocarbon inhibition of  $NO<sub>2</sub>$ production by whole cells of N. europaea. The trends reflect structural relationships of the inhibitors: increasing molecular size produced increasing  $K_{iE}/K_{iES}$  ratios, and increasing halogen size was correlated with greater inhibitor effectiveness. Corroborating studies indicated that high  $NH<sub>3</sub>$  concentrations decreased oxidation rates for alternate substrates with competitive character ( $K_{iE} \ll K_{iES}$ ) as inhibitors of  $NO<sub>2</sub>$ <sup>-</sup> production but not for substrates with predominantly noncompetitive character ( $K_{iE} \ge K_{iES}$ ). These results support an active-site model for AMO consisting of (at least) two substrate-binding sites in addition to the  $O_2$ -binding site and the site of electron donation to AMO; oxidation may occur at either site. The correlation of structural relationships with the observed trends indicates that our data should allow predictions for structurally related compounds regarding their interactions with  $NH<sub>3</sub>$  at the active site of AMO.

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