

## H<sub>2</sub>-Dependent Mixotrophic Growth of N<sub>2</sub>-Fixing *Azotobacter vinelandii*†

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*Azotobacter vinelandii* can grow with a variety of organic carbon sources and fix N<sub>2</sub> without the need for added H<sub>2</sub>. However, due to an active H<sub>2</sub>-oxidizing system, H<sub>2</sub>-dependent mixotrophic growth in an N-free medium was demonstrated when mannose was provided as the carbon source. There was no appreciable growth with either H<sub>2</sub> or mannose alone. Both the growth rate and the cell yield were dependent on the concentrations of both substrates, H<sub>2</sub> and mannose. Cultures growing mixotrophically with H<sub>2</sub> and mannose consumed approximately 4.8 mmol of O<sub>2</sub> and produced 4.6 mmol of CO<sub>2</sub> per mmol of mannose consumed. In the absence of H<sub>2</sub>, less CO<sub>2</sub> was produced, less O<sub>2</sub> was consumed, and cell growth was negligible. The rate of acetylene reduction in mixotrophic cultures was comparable to the rate in cultures grown in N-free sucrose medium. The rate of [<sup>14</sup>C]mannose uptake of cultures with H<sub>2</sub> was greater than with argon, whereas [<sup>14</sup>C]sucrose uptake was unaffected by the addition of H<sub>2</sub>; therefore, the role of H<sub>2</sub> in mixotrophic metabolism may be to provide energy for mannose uptake. *A. vinelandii* is not an autotroph, as attempts to grow the organism chemoautotrophically with H<sub>2</sub> or to detect ribulose biphosphate carboxylase activity were unsuccessful.

*Azotobacter vinelandii* is an obligate aerobic common soil bacterium "capable of fixing nitrogen in a nitrogen-free medium with an organic carbon source" (1). Due to its rapid growth and high N<sub>2</sub> fixation rate, *A. vinelandii* is commonly used to study the physiology and biochemistry of N<sub>2</sub> fixation. Even though *A. vinelandii* is capable of oxidizing a wide variety of organic substrates, growth of *A. vinelandii* in most natural environments is thought to be severely limited by organic carbon (8). In addition to the production of NH<sub>4</sub><sup>+</sup>, nitrogenase evolves H<sub>2</sub>. An enzyme that apparently aids in the efficiency of the N<sub>2</sub> fixation process is hydrogenase. When fixing N<sub>2</sub>, *Azotobacter* hydrogenase oxidizes the nitrogenase-evolved H<sub>2</sub> at high rates, and the electrons from H<sub>2</sub> are carried through an electron transport chain to O<sub>2</sub>, yielding H<sub>2</sub>O as the final product. H<sub>2</sub> oxidation is thought to serve primarily two beneficial purposes for N<sub>2</sub>-fixing *Azotobacter* species (21, 27). These are to provide ATP, which could then be used in the nitrogenase reaction, and to augment respiratory protection by removal of O<sub>2</sub>, thereby preventing damage to the O<sub>2</sub>-labile nitrogenase.

Due to an active H<sub>2</sub> oxidation system, some N<sub>2</sub>-fixing bacteria, such as *Rhizobium japonicum* (11), *Azospirillum* spp. (22), and *Derxia gummosa* (16), are capable of growing chemoautotrophically with H<sub>2</sub> and CO<sub>2</sub>. However, *Azotobacter* species are not autotrophic, as attempts to grow *A. vinelandii* and *Azotobacter chroococcum* this way have been unsuccessful (16; unpublished data). Nevertheless, we thought that H<sub>2</sub> might, in energy-limited conditions, supply sufficient energy for growth of this heterotrophic bacterium. In this report, we demonstrate growth and N<sub>2</sub> fixation of *A. vinelandii* that require both an inorganic energy source (H<sub>2</sub>) and an organic carbon source. This type of growth is characteristic of mixotrophy (4, 19).

(A preliminary account of this work has been presented [Abstr. Annu. Meet. Am. Soc. Microbiol. 1985, K32, p. 177].)

### MATERIALS AND METHODS

**Screening carbon sources for ability to support H<sub>2</sub>-dependent growth.** *A. vinelandii* OP was grown in nitrogen-free Burk (7) liquid medium containing 2% sucrose. A drop of mid-log-phase cells (approximately 2 × 10<sup>7</sup> cells) was spread evenly onto a carbon-free Burk agar plate. A Taxo carbohydrate disk (BBL Microbiology Systems, Cockeysville, Md.) was placed onto the agar plate for the following carbon sources (see Table 1): adonitol, arabinose, glucose, dulcitol, galactose, inositol, inulin, lactose, levulose, maltose, mannitol, mannose, melibiose, raffinose, rhamnose, salicin, sorbitol, sucrose, trehalose, and xylose. A sterile blank disk was also included as a control. Sterile saturated solutions of the other carbon sources used (see Table 1) were prepared. A sterile disk was saturated with the solution and placed onto the plate. The plates were then transferred to an anaerobic vented jar (product no. 60608; BBL). An amount equal to about 20% of the jar volume of either H<sub>2</sub> or Ar was injected into the container. The plates were incubated at 30°C for at least 3 days, and the plates were removed and checked for growth. For liquid growth, side-armed flasks (volume, 180 ml) containing 20 ml of N-free Burk medium with the indicated organic compound were autoclaved for 15 min. An aliquot (0.05 ml) of early-log-phase cells grown on Burk medium with 2% sucrose was then inoculated into each flask. The flasks were tightly stoppered with sterile rubber stoppers, and 50 ml of H<sub>2</sub> or Ar gas that had been filtered through a sterile membrane filter (pore size, 0.22 μm; Millipore Corp., Bedford, Mass.) was injected into the flasks. Excess pressure inside the flasks was then released by injecting a sterile needle through the stopper for 2 to 5 s. The flasks were then placed in a water bath shaker (30°C) at 250 rpm.

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TABLE 1. Growth of *A. vinelandii* in the presence of hydrogen or argon<sup>a</sup>

Carbon source	Growth of culture under:	
	H <sub>2</sub>	Ar
Acetate	+	+
Adonitol	-	-
D(+)-Arabinose	+/-	+/-
Benzoate	+	+
D(+)-Cellobiose	-	-
<i>i</i> -Erythritol	+	+
$\alpha$ -L(-)-Fucose	-	-
D(+)-Galactose	+	+
Methylglucoside	-	-
<i>myo</i> -Inositol	-	-
Itaconic acid	-	-
$\beta$ -D(-)-Levulose	+	+
D-Mannitol	+	+
Phenol	+	+
Propionate	+	+
D(+)-Raffinose	+	+
2-Deoxyribose	-	-
Salicin	-	-
Sucrose	+	+
Xylose	-	-
D(+)-Mannose	+	-
Aconitate	+	+
Adipic acid	-	-
Azelaic acid	-	-
<i>n</i> -Butyrate	+	+
Dulcitol	-	-
Ethanol	+	+
$\beta$ -D(-)-Fructose	+	+
D(+)-Glucose	+	+
Glutamate	+	+
Inulin	+	+
$\alpha$ -Lactose	-	-
Maltose	+	+
$\alpha$ -D(+)-Melibiose	+	+
Pimelate	-	-
Pyruvate	+	+
D(-)-Ribose	-	-
$\alpha$ -L-Rhamnose	+	+
D-Sorbitol	+	+
Trehalose	+/-	+/-

<sup>a</sup> Procedures are described in the text. Symbols: +, growth; -, no growth; +/-, very little growth.

Optical density at 540 nm was monitored; 0.1 optical density unit was equivalent to approximately  $2.2 \times 10^7$  viable cells per ml. All growth experiments were performed in this closed gas system; therefore, concentrations of gases such as H<sub>2</sub> and O<sub>2</sub> decreased during the course of these experiments. All carbon sources were obtained from Sigma Chemical Co., St. Louis, Mo., with the exception of glucose and acetate, which were obtained from J. T. Baker Chemical Co., Phillipsburg, N.J.

**Sugar uptake experiments.** D-[U-<sup>14</sup>C]mannose and D-[U-<sup>14</sup>C]sucrose were purchased from Amersham Corp., Arlington Heights, Ill., and had specific activities of 300 and 552 mCi/mmol, respectively. *A. vinelandii* cells were grown in Burk medium with 2% mannose plus H<sub>2</sub> for 24 h. The cells were harvested and then washed three times with 50 mM phosphate buffer (pH 7.5). The cells were then suspended in carbon-free Burk medium to about  $2 \times 10^8$  cells per ml. The culture was then incubated at 30°C for approximately 2 h to deplete the endogenous substrate. A 2-ml portion of the substrate-depleted sample was then transferred to a 15-ml

bottle, which was then tightly stoppered with a sleeve-type rubber stopper. Three milliliters of either H<sub>2</sub> or Ar was then injected into the bottle. A 30- $\mu$ l volume of [<sup>14</sup>C]mannose solution (0.5  $\mu$ Ci) was injected along with cold mannose into the sample to give a final mannose concentration of 150  $\mu$ M. At the times indicated (see Fig. 3), 0.1 ml of the sample was withdrawn from the bottle and then diluted into 4 ml of ice-cold phosphate buffer. A 2-ml portion of this diluted sample was filtered through a membrane filter (pore size, 0.22  $\mu$ m; GSWP 024 00; Millipore), and the filter was washed twice with 10 ml of ice-cold phosphate buffer. The filters were then placed in 5 ml of Aquasol-2 (New England Nuclear Corp., Boston, Mass.), and radioactivity was counted in a Packard 3375 liquid scintillation spectrometer. Counting efficiency was 0.55. For [<sup>14</sup>C]sucrose uptake experiments, the same procedure as described above for mannose was used, except that the cells were grown in 2% sucrose instead of mannose before harvest. Control experiments on boiled cells demonstrated that there was no mannose or sucrose uptake in nonviable cells. Radioactivity counts in these experiments were less than 80 cpm, whereas similar experiments with viable cells gave counts of over 1,000 cpm after 5 min.

**Other assays.** Whole-cell N<sub>2</sub> fixation by *A. vinelandii* was performed as described by Bishop et al. (2). Gas chromatography conditions for monitoring C<sub>2</sub>H<sub>4</sub> production were as described previously (9). Carbon dioxide production was determined by measuring thermal conductivity with a Perkin Elmer Sigma 3B gas chromatograph. A column (2 m by 2 mm [inner diameter]) with Porapak N (80-100 mesh) was used. The carrier flow rate was 20 ml of helium per min, the detector and injector temperatures were 175°C, and the oven temperature was 50°C. For measuring the CO<sub>2</sub> produced during the 9-h incubation period (see Table 3), the culture was acidified with trichloroacetic acid, to ensure elimination of dissolved CO<sub>2</sub>, before removal of the gas sample.

## RESULTS

Forty carbon sources were tested for their ability to support growth of *A. vinelandii* on N-free agar plates in a closed gas system with either H<sub>2</sub> or Ar added at a partial pressure of 20%. The results are shown in Table 1. With the carbon sources that supported some growth, added H<sub>2</sub> did not facilitate growth. However, growth of *A. vinelandii* was observed on the mannose-containing plates in an atmosphere containing H<sub>2</sub> (Table 1), whereas no growth was observed when argon was substituted for H<sub>2</sub>.

The effect of added H<sub>2</sub> on the growth rate of *A. vinelandii* in carbon-containing N-free media was subsequently tested.

TABLE 2. Doubling time of *A. vinelandii* grown with different carbon sources with either H<sub>2</sub> or Ar added<sup>a</sup>

Substrate	Doubling time (h) for culture grown under	
	H <sub>2</sub>	Ar
Acetate	4.0	3.3
Glucose	2.8	3.0
Sucrose	3.0	3.0
Mannose	3.8	>14.0
Xylose	NG <sup>b</sup>	NG
Trehalose	NG	NG

<sup>a</sup> Procedures are described in the text.

<sup>b</sup> NG, No growth.

The cell doubling times on mannose and other carbon sources were compared (Table 2). The addition of  $H_2$  did not stimulate the growth rate in any of the carbon substrates tested, with the exception of mannose. Therefore,  $H_2$ -dependent mixotrophic growth was dependent on the use of mannose as a carbon source. The doubling time of *A. vinelandii* in mannose decreased from more than 14 h (without  $H_2$ ) to 3.8 h (with  $H_2$ ). This difference in growth rate due to added  $H_2$  was observed only when cells were fixing  $N_2$ . In the presence of  $NH_4^+$  (0.05%  $NH_4Cl$  in the medium) doubling times were 4.8 h (with  $H_2$ ) and 4.5 h (without  $H_2$ ).

We studied the effects of the  $H_2$  concentration on the growth rate in mannose-containing medium. Figure 1 shows the growth curves of  $N_2$ -fixing *A. vinelandii* in 2% mannose plus various amounts of  $H_2$ . Both the growth rate and the cell yield increased with increasing amounts of  $H_2$ . Maximum growth was achieved by the addition of 25% partial pressure  $H_2$ . Further addition of  $H_2$  above 25% partial pressure did not increase growth rate or yield. Figure 2 shows the dependence of cell growth on the carbon source mannose, in the presence of saturating (25% partial pressure)  $H_2$ . In this experiment,  $H_2$  was added after 24 h of incubation with mannose (Fig. 2, arrow) to show the dependence of growth on the added  $H_2$ ; there was no appreciable growth before  $H_2$  addition (Fig. 2). The results show a concentration dependence effect on mannose for both growth rate and yield. Maximum growth occurred at 2% mannose concentration;

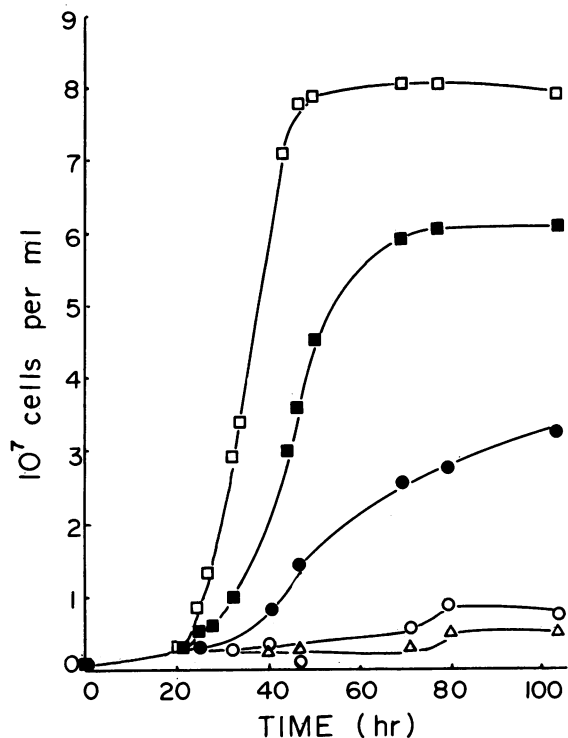


FIG. 1. Growth curves of  $N_2$ -fixing *A. vinelandii* in 2% mannose and various concentrations of  $H_2$ .  $H_2$  was injected into the 150-ml stoppered flask 18 h after inoculation, and the cells were incubated and growth was monitored as described in the text. Cultures were grown under 50 ml of  $H_2$  ( $\square$ ), 30 ml of  $H_2$  plus 20 ml of Ar ( $\blacksquare$ ), 10 ml of  $H_2$  plus 40 ml of Ar ( $\bullet$ ), 5 ml of  $H_2$  plus 45 ml of Ar ( $\circ$ ), or 50 ml of Ar ( $\triangle$ ).

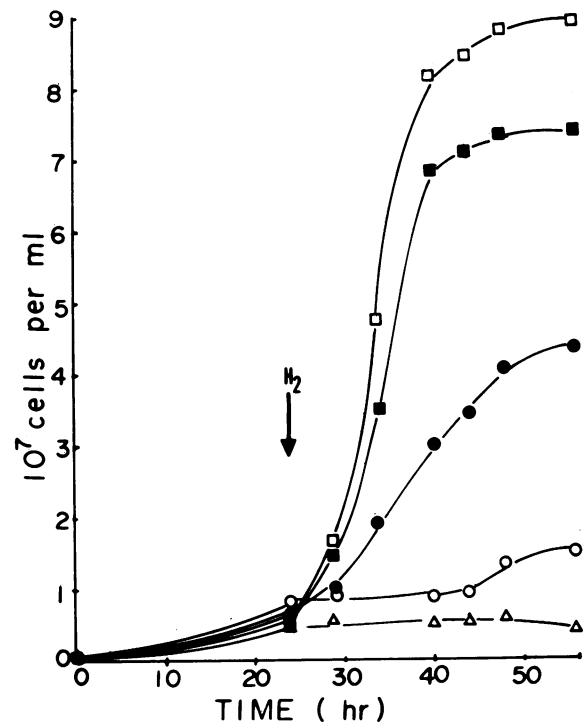


FIG. 2. Growth curves of  $N_2$ -fixing *A. vinelandii* with added  $H_2$  plus 2% mannose ( $\square$ ), 1% mannose ( $\blacksquare$ ), 0.5% mannose ( $\bullet$ ), 0.125% mannose ( $\circ$ ), or no mannose ( $\triangle$ ). Arrow shows the time at which  $H_2$  (final 25% partial pressure) was added. Other conditions were as described in the legend to Fig. 1.

higher concentrations (3 and 6% [wt/vol]) were also tested (data not shown).

To confirm  $H_2$ - and mannose-dependent mixotrophic metabolism in *A. vinelandii*, we measured cell yield,  $CO_2$  production, mannose consumption, and oxygen consumption in cultures with  $H_2$  or argon added (Table 3). The cultures with added  $H_2$  exhibited high rates of  $H_2$  uptake

TABLE 3. Cell yield,  $CO_2$  production, and mannose and  $O_2$  consumption during mixotrophic growth of *A. vinelandii*<sup>a</sup>

Experiment no.	Addition	Total $CO_2$ production (mmol)	Mannose consumption (mmol)	Oxygen consumption (mmol)	Cell yield (viable cell number [ $10^7$ ])
1	$H_2$	0.63	0.147	0.67	4.4
2	$H_2$	0.83	0.168	0.86	6.0
3	Ar	0.32	0.07	0.29	<0.5
4	Ar	0.40	0.05	0.35	<0.5

<sup>a</sup> The  $H_2$  consumption rate for experiments 1 and 2 at the time of harvest was approximately  $2.4 \mu\text{mol of } H_2 \text{ per h per } 10^8 \text{ cells}$ . All four cultures (10 ml of medium in a 180-ml flask) were initially inoculated with  $2 \times 10^6$  cells and then incubated in a closed-flask system as described in the text. Gas samples (0.2 ml) were removed at the time of inoculation of each flask and again (9 h later) when cell yield was determined; the total amount of  $O_2$  consumed or  $CO_2$  produced was then calculated. Carbon dioxide was determined by gas chromatography as described in the text. Oxygen was determined polarographically as described previously (15). Mannose (the only organic carbon source in the medium) was also determined initially and at 9 h on 0.5-ml liquid samples after cells were removed by centrifugation. Mannose was quantitated by the phenol sulfuric acid method for hexose determination as described previously (12). Appropriate standards of  $CO_2$ ,  $O_2$ , and mannose were made which included concentrations both above and below the concentrations of the experimental samples.

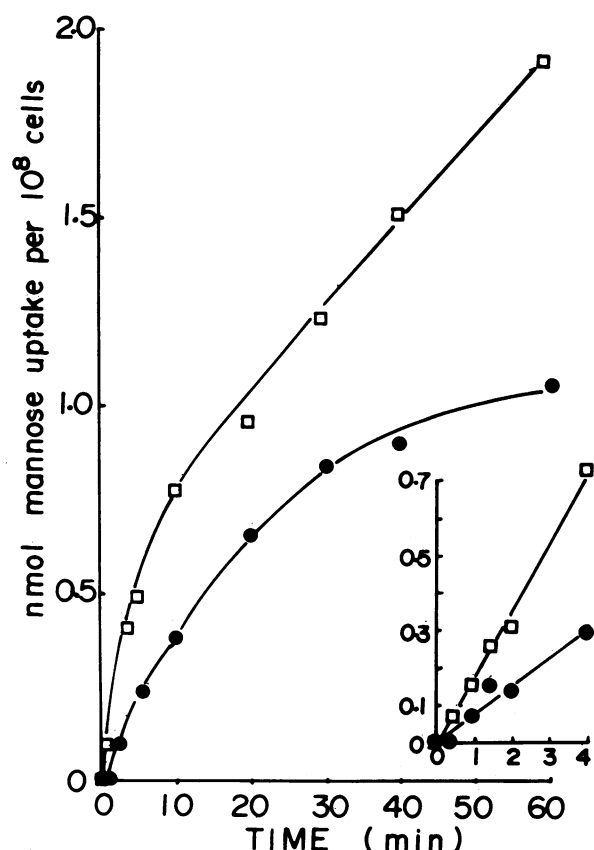


FIG. 3. [<sup>14</sup>C]mannose uptake of *A. vinelandii* with added H<sub>2</sub> (□) or Ar (●). Cultures were incubated with [<sup>14</sup>C]mannose for the indicated time with either H<sub>2</sub> or Ar, the cultures were rapidly filtered and washed on the filter, and radioactivity was determined as described in the text. The radioactivity count for the zero time culture (the sample of cells removed immediately after inoculation into the [<sup>14</sup>C]mannose solution) was subtracted from all the other counts before the data were processed. Each point is the average of two independent determinations. (Inset) a similar experiment performed over a 4-min total time period.

activity (see the legend to Table 3) and grew from an inoculum of  $2 \times 10^6$  cells to over  $4 \times 10^7$  cells (Table 3, experiments 1 and 2). In contrast, the cultures without H<sub>2</sub> grew very little (to less than  $5 \times 10^6$  cells). The cultures incubated with H<sub>2</sub> also consumed mannose, used an average of 4.8 mmol of O<sub>2</sub>, and produced 4.6 mmol of CO<sub>2</sub> per mmol of mannose used for the two experiments with H<sub>2</sub> added. These are reasonable stoichiometries for O<sub>2</sub> production and CO<sub>2</sub> production via sugar metabolism by aerobic bacteria (10, 20).

The cultures incubated with Ar rather than H<sub>2</sub> still used mannose, produced some CO<sub>2</sub>, and respired oxygen (Table 3, experiments 3 and 4). Therefore, these cultures are capable of some mannose-dependent metabolism, yet this must not be sufficient for growth. Even though no growth was observed in this condition, the fact that substrate was used and O<sub>2</sub> was consumed is still consistent with current views on maintenance metabolism requirements of bacteria (23). The lack of growth with mannose plus argon is not inconsistent with previous work on mannose metabolism in *A. vinelandii*; previous researchers have noticed that N<sub>2</sub>-fixing *A. vinelandii* utilizes mannose for the production of acid, yet the cells are not capable of growth (24). Apparently, they did not test the effect of adding H<sub>2</sub>.

To study the roles of mannose and H<sub>2</sub> in mixotrophic growth, we performed sugar uptake experiments. We compared the accumulated <sup>14</sup>C from mannose over a 60-min period in cells supplied with H<sub>2</sub> versus that in cells supplied with Ar (Fig. 3). The amount of <sup>14</sup>C accumulated in cells was greater in the presence of H<sub>2</sub> than without H<sub>2</sub>. CO<sub>2</sub> measurements ruled out the possibility that mannose merely accumulated unchanged in the cells during transport studies. Little CO<sub>2</sub> production was observed until the substrate mannose was added, and CO<sub>2</sub> production was twofold greater in the presence of H<sub>2</sub> compared with that observed in the presence of argon; this indicates that the mannose transported is actually metabolized. Since sugars are rapidly metabolized after they enter cells, it is important to determine sugar uptake in the first few minutes. This gives a more accurate determination of the real uptake rate of the labeled sugar. The uptake rates of [<sup>14</sup>C]mannose over a 4-min period in cultures grown with and without H<sub>2</sub> are also shown in Fig. 3 (inset). The uptake rate with H<sub>2</sub> provided was greater than that without H<sub>2</sub>; after 4 min, the cells with H<sub>2</sub> accumulated more than two times as much <sup>14</sup>C-sugar as did cells without H<sub>2</sub>. The results (Fig. 3) suggest that one role of H<sub>2</sub> may be to provide energy for mannose uptake. Also, the results demonstrate that the probable role of mannose is indeed as an intracellular carbon substrate for cells, rather than another role, such as providing a suitable osmotic environment for H<sub>2</sub>-dependent growth. As a control, we also determined the effect of H<sub>2</sub> and Ar on [<sup>14</sup>C]sucrose uptake. In this case, there was no difference in <sup>14</sup>C accumulation in cells with and without H<sub>2</sub> provided (data not shown).

Even though *A. vinelandii* took up mannose, it is important to rule out CO<sub>2</sub> as a major carbon source under H<sub>2</sub>-dependent growth conditions. Attempts to detect appreciable whole-cell CO<sub>2</sub> fixation or ribulose biphosphate carboxylase activity in permeabilized cells in H<sub>2</sub> plus mannose growth conditions were unsuccessful. Likewise, many attempts to grow *A. vinelandii* chemoautotrophically with H<sub>2</sub> were unsuccessful.

The rate of acetylene reduction by cells growing exponentially in mannose plus H<sub>2</sub> was 412 nmol of C<sub>2</sub>H<sub>4</sub> produced per h per 10<sup>8</sup> cells. This value is comparable to the rates of N<sub>2</sub> fixation for this bacterium in N-free medium reported by others (3, 17). It is also comparable to the N<sub>2</sub> fixation rate we have observed in N-free sucrose medium (up to 550 nmol of C<sub>2</sub>H<sub>4</sub> per h per 10<sup>8</sup> cells). Therefore, *A. vinelandii* growing mixotrophically presumably has no difficulty producing the energy and reductant needed for N<sub>2</sub> fixation.

## DISCUSSION

Mixotrophy is the term used to describe the ability of an organism to use inorganic and organic compounds concomitantly as energy sources or carbon sources or both (4). We have demonstrated that the heterotrophic N<sub>2</sub>-fixing bacterium *A. vinelandii* can grow mixotrophically. This type of growth in *A. vinelandii* was dependent on H<sub>2</sub> as the inorganic energy source and mannose as the organic carbon substrate. Most of the thiobacilli, hydrogen bacteria, nitrifying bacteria, and iron-oxidizing bacteria use the Calvin cycle to fix CO<sub>2</sub> and are chemolithoautotrophic. Mixotrophic growth is thought to be common among these chemolithoautotrophic bacteria (13, 18, 19). However, mixotrophy has been demonstrated in only a few heterotrophic bacteria. The anaerobe *Desulfovibrio* sp. can use either H<sub>2</sub> or organic compounds as the energy source and couples the electrons through cytochrome-dependent, energy-conserving reactions. Al-

though *Desulfovibrio* sp. can use  $H_2$  as an energy source, it is not autotrophic, as it lacks the enzymes unique to autotrophy, namely phosphoribulokinase and ribulose diphosphate carboxylase. The mixotrophic mode of metabolism we describe for *A. vinelandii* is probably closest to the aerobic chemolithotrophic heterotroph metabolism of *Thiobacillus perometabolis* (14). This bacterium grows solely on organic compounds, but it can also oxidize sulfur compounds for energy generation. Also, some iron-oxidizing bacteria have been described that couple the oxidation of iron to organic substrate utilization (5, 6). Like *A. vinelandii*, these bacteria are heterotrophs; they do not fix  $CO_2$  via the Calvin cycle.

Even though there are only these few reports of mixotrophy among heterotrophs, it has been considered that mixotrophy, even among nonautotrophic bacteria, may actually be widespread in natural environments (4, 13, 25). Since *A. vinelandii* is a common soil bacterium and  $H_2$  is available in soil, mixotrophic growth of this heterotrophic bacterium may occur in nature. The metabolic flexibility of *A. vinelandii* may be of survival significance to the organism during competition in natural environments.

The basis for the requirement for  $H_2$  to obtain growth on mannose is not known. However, since cells were able to grow on mannose plus  $NH_4^+$  (non- $N_2$ -fixing conditions),  $H_2$  is required only when cells are fixing  $N_2$ . We suggest that the added energy demand for  $N_2$  fixation requires the additional energy source, namely  $H_2$ . It may be important that under  $N_2$ -fixing conditions, the activity of hydrogenase markedly increases (compared with cells grown with  $NH_4^+$ ), facilitating input of energy from  $H_2$ . Another possible role for  $H_2$  is suggested by sugar transport studies. These studies showed that added  $H_2$  can help support mannose uptake by *A. vinelandii*. Therefore, the role of  $H_2$  probably includes not only production of ATP for  $N_2$  fixation but also energy for mannose uptake.

*A. vinelandii* can grow in a variety of organic carbon sources and fix  $N_2$  without the need for added  $H_2$ . However,  $H_2$ -dependent mixotrophic growth in N-free media by this organism was dependent on the use of mannose. Mannose must be a poor energy source for *A. vinelandii*; no growth was observed in mannose alone (without  $H_2$ ). We have found a specific condition under which hydrogenase, with its associated electron transport pathway (26), can supply enough energy to permit  $N_2$  fixation and growth in the presence of a poor carbon substrate. It is very important to rule out the possibility that *A. vinelandii* is an autotroph. Our attempts as well as attempts by others (16) to grow *A. vinelandii* autotrophically with  $H_2$  have not been successful. Also, we have been unable to detect appreciable  $CO_2$  fixation or the key  $CO_2$ -fixing enzyme, ribulose biphosphate carboxylase, in cultures grown in  $H_2$ .

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