

# Sucrose Catabolism in *Clostridium pasteurianum* and Its Relation to N<sub>2</sub> Fixation

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Received for publication 20 April 1968

The growth constant and Y (sucrose) (grams of cells per mole of sucrose) for NH<sub>3</sub>-grown cultures of *Clostridium pasteurianum* were 1.7 times those of N<sub>2</sub>-grown cultures, whereas the rate of sucrose utilized per gram of cells per hour was similar for both conditions. The Y (sucrose) of chemostat cultures grown on limiting NH<sub>3</sub> under argon at generation times equal to those of N<sub>2</sub>-fixing cultures was less than that of cultures grown on excess NH<sub>3</sub>, but cells of NH<sub>3</sub>-limited cultures contained the N<sub>2</sub>-fixing system in high concentration. The concentration of the N<sub>2</sub>-fixing system in whole cells, when measured with adenosine triphosphate (ATP) nonlimiting, was more than twofold greater than the amount needed for the N<sub>2</sub> actually fixed. Thus, energy production from sucrose, and not the concentration of the N<sub>2</sub>-fixing system nor the maximal rate at which N<sub>2</sub> could be fixed, was the limiting factor for growth of N<sub>2</sub>-fixing cells. Either NH<sub>3</sub> or some product of NH<sub>3</sub> metabolism partially regulated the rate of sucrose metabolism since, when cultures fixing N<sub>2</sub>, growing on NH<sub>3</sub>, or growing on limiting NH<sub>3</sub> in the absence of N<sub>2</sub> were deprived of their nitrogen source, the rate of sucrose catabolism decreased. Calculations showed that the rate of ATP production was the growth rate-limiting factor in cells grown on N<sub>2</sub>, and that the increased sucrose requirement of N<sub>2</sub>-fixing cultures in part reflected the energy demand of N<sub>2</sub> fixation. Calculations indicated that whole cells require about 20 moles of ATP for the fixation of 1 mole of N<sub>2</sub> to 2 moles of NH<sub>3</sub>.

N<sub>2</sub>-fixation in cell-free extracts of *Clostridium pasteurianum* is an energy-requiring process. It has been reported that two adenosine triphosphate (ATP) molecules are consumed per electron transferred in *C. pasteurianum* (9) and five ATP molecules are consumed per electron pair in *Azotobacter vinelandii* (5). N<sub>2</sub>-fixing cultures should have a significantly higher requirement for energy than do cultures growing on NH<sub>3</sub>, and the anaerobe *C. pasteurianum* may require more than two sucrose molecules for each molecule of N<sub>2</sub> fixed.

In this paper, the difference in sucrose utilization between N<sub>2</sub>-fixing and nonfixing cultures is quantitated, and the regulation of catabolic activity is studied in relation to nitrogen metabolism.

## MATERIALS AND METHODS

The medium used for the continuous cultures was  $2 \times 10^{-4}$  M in MgSO<sub>4</sub> and FeCl<sub>3</sub>,  $2 \times 10^{-5}$  M in MnSO<sub>4</sub> and CaCl<sub>2</sub>,  $2 \times 10^{-6}$  M in ZnSO<sub>4</sub>, CuSO<sub>4</sub>, and CoCl<sub>2</sub>, and 0.15 M in potassium phosphate, pH 6.9. Except for those experiments on the effects of sucrose limitation, the medium was made 1% in sucrose;

0.1 mg of biotin was added before autoclaving. Eight liters of this medium was autoclaved in 9-liter serum bottles. Since the medium contained some insoluble salts, it was stirred throughout the experiments. A 500-ml vacuum flask was used as the growth vessel; media were introduced through glass tubing fitted in a rubber stopper and connected to a tygon tubing inlet from the reservoir. The flow of medium through the tygon tubing was regulated by use of a Sigmamotor adjustable pump. The side arm of the growth vessel provided the exit for the effluent culture. Argon or N<sub>2</sub> was introduced through a sintered-glass sparger fitted through the rubber stopper of the flask; the gas flow was monitored with a flow meter and kept below 200 ml/min. The culture was kept in suspension by magnetic stirring. The growth vessel was kept in a constant temperature water bath at 30 C. Ammonium sulfate was used as the NH<sub>3</sub> source in all experiments.

The effluent medium of the continuous cultures could not be chemically assayed for N<sub>2</sub> content; thus, to show that N<sub>2</sub> was not a limiting nutrient in these experiments, growth was used as an index. Since the N<sub>2</sub>-fixing cultures contained sucrose in excess, the cells were allowed to increase in concentration by stopping the flow of the medium until the density was twice that of the experimental cell concentration but with no change in the flow rate of N<sub>2</sub> through the

growth flask. The flow of the medium was resumed and, if the culture equilibrated at the higher population density with the same growth constant it had at the lower density, it was assumed that at the lower density the external supply of  $N_2$  (as well as other components in the medium) was nonlimiting.

In the experiments with  $^{14}C$ -labeled sucrose, the growth medium was the same as just described, except that the phosphate concentration was  $6.6 \times 10^{-3} M$ , the  $CaCl_2$  was omitted, and 3 g of  $CaCO_3$  per liter was used to buffer the system. Initial concentration of sucrose varied from 27 to 35 mM for the three experiments performed. Total  $^{14}C$  as uniformly labeled sucrose varied from  $10^6$  to  $10^7$  counts/min per growth flask. Cultures (100 ml) were grown in 500-ml aspirator bottles, the tubulation of which was fitted with heavy-walled rubber tubing closed with a screw clamp from which samples were withdrawn. The cultures were grown under flowing  $N_2$  for at least three generations in the presence of the labeled sucrose, and the experiment was terminated by centrifugation of the cultures at  $500 \times g$ . The cells were washed with cold 1% sucrose in 0.1 M phosphate (pH 7.0), centrifuged, suspended in a small volume of distilled water, and disrupted by sonic treatment. Appropriate amounts of the solubilized cells and the supernatant medium were placed in Bray's solution (4) and counted in a Tri-Carb liquid scintillation spectrometer (Packard Instrument Co., Inc., Downers Grove, Ill.).

Anthrone reagent was used for all sucrose analyses (1). Determination of the rate of sucrose used per gram of cells in the chemostat was accomplished by methods previously established (7).  $Y$  (sucrose) (grams of cells produced/mole of sucrose) and  $Y$  (ATP) (grams of cells produced/mole of ATP) were determined as suggested by Beauchop and Elsdon (3). Ammonia was determined by the microdiffusion technique of Conway (6) and nitrogen was determined by Kjeldahl digestion (2). To determine the nitrogen content of  $NH_3$ -grown cells in the continuous culture, the amount ( $\mu$ moles) of  $NH_3$  per ml of the reservoir and effluent mediums was measured, the difference was multiplied by the volume of the culture, and the result was divided by the amount (grams) of cells in the culture. The result from 14 independent determinations was  $7.5 \pm 1.1$  mmole of  $NH_3$  per g of dry cells or 105 mg of nitrogen per g of cells. For batch cultures, the differences in  $NH_3$  content of samples taken at different times was divided by the corresponding change in mass of the cells. No significant difference between continuous and batch cultures was observed, and no significant differences were found between cultures grown under an atmosphere of argon or  $N_2$ . Cells from chemostat cultures grown on limiting  $NH_3$  had the same nitrogen content per gram (dry weight) as did nonlimited cultures.

The nitrogen content of  $N_2$ -fixing cells determined by Kjeldahl digestion averaged (four determinations)  $6.6 \pm 0.5$  mmoles per g of dry cells or 92 mg of nitrogen per g of cells.

Acetic and butyric acids in cultures, culture filtrates, and standard solutions were measured by gas chromatography with a Varian Aerograph (model

600-B) with a free fatty acid phase (FFAP) column supplied by the Wilkens Co.

Estimation of  $N_2$  fixed by measuring acetylene reduction was based on a modification (10) of the method of Koch and Evans (8).

Optical density (OD) measurements of cultures were made at  $660 m\mu$  in 1-cm cuvettes; a Spectronic-20 colorimeter (Bausch & Lomb, Inc., Rochester, N.Y.) was used. The samples were diluted in 4% acetic acid (to dissolve basic salts) so that readings between 0.10 and 0.31 were always obtained. One liter of culture at an OD of 1.00 contained 380 mg of cells (dry weight).

## RESULTS

*Sucrose utilization by cells grown on  $N_2$  and on  $NH_3$ .* Sucrose utilization was studied under three different conditions: (i) optimally growing  $N_2$ -fixing cultures, with sucrose present at all times in the effluent medium; (ii) optimally growing  $NH_3$ -supplemented cultures grown under an atmosphere of argon, with both  $NH_3$  and sucrose present in the effluent medium; and (iii)  $NH_3$ -limited cultures grown under argon, with sucrose but without  $NH_3$  present in the effluent medium and with the growth rate of the culture regulated by the rate of supply of  $NH_3$  to equal that of the  $N_2$ -fixing culture. The results of these experiments, in Table 1, show that the rate of sucrose utilization per gram of cells was similar under all three conditions, whereas the  $Y$  (sucrose) and the growth constant for  $NH_3$ -grown cultures were 1.7 times those of  $N_2$ -fixing cultures. Under the third condition, the  $Y$  (sucrose) was similar to that of a  $N_2$ -fixing culture. In addition, under the third condition, the bacteria apparently consumed up to 40% of the sucrose in reactions other than those of normal biosynthesis, since, because of nitrogen limitation, only 60% of the total sucrose consumed would be required to produce the same amount of  $NH_3$ -grown cells under  $NH_3$ -sufficient conditions. This could be taken as evidence that the cell's catabolic activity is not regulated to its biosynthetic needs. Further investigations, however, have shown that cultures grown on limiting  $NH_3$  in the absence of  $N_2$  possess a highly active  $N_2$ -fixing system and behave more like " $N_2$ -fixing" cultures (*in preparation*). ATP consumed by the nonfunctioning nitrogenase (5, 9) could be responsible for at least part of the excess sucrose utilization.

The above results were reexamined with radioactive sucrose to determine how much carbon of the sucrose fermented was incorporated into the cells under the two conditions. When paired cultures, one growing on  $N_2$  and one growing on  $NH_3$ , were grown in the presence of uniformly labeled  $^{14}C$ -sucrose, the percentage carbon incorporated into cellular material averaged 9.8 for

TABLE 1. Rate of sucrose utilization and cell yield of *Clostridium pasteurianum* grown in a chemostat on excess sucrose under  $N_2$ -fixing and nonfixing conditions<sup>a</sup>

Nitrogen source	Growth constant	Y (sucrose) (g of cells/mole of sucrose)	Amt (mmoles) of sucrose used per g of cells per hr
$N_2$ (excess) . . . . .	0.40	36.6	10.9
$NH_3$ (excess) . . . . .	0.69	63.0	10.9
$NH_3$ (limited) <sup>b</sup> . . . . .	0.41	38.0	10.6

<sup>a</sup> The figures given for the  $N_2$ -fixing state are averages of six independent determinations; those for the optimally growing  $NH_3$ -dependent state are averages of two independent determinations; and those for the  $NH_3$ -limited state are averages of three independent determinations.

<sup>b</sup> Chemostat with cells growing on  $NH_3$ -limited medium so that the doubling time is the same as in the  $N_2$ -fixing continuous culture. Gas phase was argon.

the  $N_2$ -fixing culture and 17.1 for the  $NH_3$ -grown culture. In an experiment with  $N_2$ -fixing cells, of a total of  $1.58 \times 10^6$  counts/min of the sucrose- $U-^{14}C$  used,  $1.56 \times 10^5$  counts/min was found in the cells, whereas with  $NH_3$ -grown cells, of a total of  $1.24 \times 10^6$  counts/min of sucrose- $U-^{14}C$  used,  $2.12 \times 10^5$  counts/min was found in the cells. The remainder was accounted for in  $CO_2$  and butyric and acetic acids. Since 9.8% and 17.1% sucrose carbon incorporated correspond to Y sucrose values of approximately 31 and 55, respectively (assuming the cells are 45% carbon), these results are in reasonable agreement with those of Table 1.

Two hypotheses are consistent with the results in Table 1. (i) Catabolism is not a regulated process and the rate of  $N_2$ -fixation is the growth rate-limiting factor in  $N_2$ -fixing cultures; and (ii) the rate of energy supply is the growth rate-limiting factor in both conditions and is simply at its maximum in both states. Senez (11) gave the former interpretation to results obtained with *Desulfovibrio desulfuricans*. To test the first hypothesis with *C. pasteurianum*, a situation was created in which energy supply was clearly the factor limiting growth. By regulating the flow rate (limiting sucrose), two  $N_2$ -fixing growth conditions were compared, one in which the bacteria had a growth rate just slightly less than maximum and one in which the growth rate was decreased to 50% of that of the nonlimited culture. Y (sucrose) results obtained were compared with those of similarly regulated cultures on media supplemented with excess  $NH_3$  (Table 2). Since (i)

TABLE 2. Cell yield and rates of sucrose utilization for sucrose-limited cultures under  $N_2$ -fixing and nonfixing conditions<sup>a</sup>

Nitrogen source	Concn of sucrose in the reservoir	Growth constant	Y (sucrose) (g of cells/mole of sucrose)	Amt (mmoles) of sucrose used per g of cells per hr
$N_2$ <sup>b</sup>	<i>mM</i>			
	5.95	0.385	43.2	8.95
	5.95	0.217	39.4	5.34
	11.2	0.365	46.2	7.70
	11.2	0.389	43.4	8.68
$NH_3$ (excess)	11.2	0.217	46.2	4.55
	5.95	0.568	73.1	7.58
	5.95	0.217	70.2	2.76
	11.2	0.555	76.0	6.50
	11.2	0.389	69.5	6.00

<sup>a</sup> All measurements were made in a chemostat culture originally derived from a  $N_2$ -fixing inoculum of *C. pasteurianum*. Growth constants were changed by adjusting the flow rate of medium into the chemostat. All cultures were limited in sucrose but to varying degrees.

<sup>b</sup> The maximal possible rate of  $N_2$  fixation by  $N_2$ -fixing cells was estimated by acetylene reduction and found to be two or more times that required to maintain the maximal growth constant.

there was no significant increase in efficiency of sucrose utilization [Y (sucrose)] when the maximal possible rate of  $N_2$  fixation was clearly not the growth rate-limiting factor and (ii) the addition of  $NH_3$  increased the Y (sucrose) at least part of the increased sucrose requirement of  $N_2$ -fixing cultures reflected the ATP demand for  $N_2$  reduction.

In addition, it was shown that if ATP available to  $N_2$  fixation was made less limiting by measuring  $N_2$  fixation in nongrowing cultures, such cultures could fix over twice the amount of  $N_2$  needed to maintain their normal rate of growth (*in preparation*).

When the growth rates of  $N_2$ -fixing and  $NH_3$ -grown cultures were controlled by sucrose limitation, a plot of mmoles sucrose used per gram of cells per hr against growth rate (Fig. 1) showed that the ratio of the rates ( $N_2$ -fixing to  $NH_3$ -grown) increased from 1.5 at a growth rate of 0.40 to 2.8 at a growth rate of zero. At the extrapolated zero growth rate, the  $N_2$ -fixing and  $NH_3$ -grown cultures consumed sucrose at rates of approximately 1.4 and 0.5 mmoles per g of cells per hr, respectively. Whether the sucrose consumed at zero growth rate is a result of uncoupled ATP hydrolysis or use in "maintenance" is unknown. The difference between the two conditions of 0.9 mmoles per g of cells per hr could be a result of

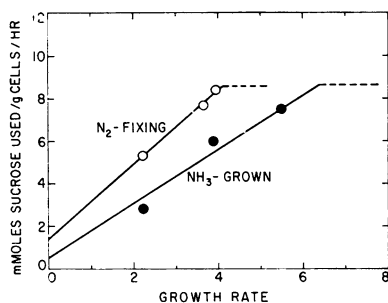


FIG. 1. Rate of sucrose used as a function of growth rate for  $N_2$ -fixing and  $NH_3$ -grown cultures. For conditions, see Table 2 and Materials and Methods.

ATP consumed by the  $N_2$ -fixing system producing  $H_2$  in the absence of  $N_2$ .

**Energy yield from sucrose by *C. pasteurianum*.** Before meaningful comparisons between sucrose utilization by  $N_2$ -fixing and  $NH_3$ -grown cells could be made, it was necessary to establish that the ratio of ATP to sucrose used was the same in both cell types. Since the enzymes for typical glycolysis are present in extracts of *C. pasteurianum*, the principal pathway of hexose catabolism and energy production was assumed to be the Embden-Meyerhoff-Parnas pathway, and at this stage the energy yields would be similar. Further metabolism of pyruvate involves two additional energy-yielding steps involving ATP:acetate phosphotransferase and ATP:butyrate phosphotransferase. Since butyric and acetic acids are the fermentation products of these energy-yielding steps, any change in their ratio to each other and to the sucrose consumed would be an index of any differences in the energy yield (ATP) from sucrose. The results of several experiments (Table 3) show that, within experimental error, these ratios were the same under all conditions.

**Does sucrose catabolism decrease during  $N_2$  starvation?** The question of whether sucrose catabolism is a regulated process was investigated since the answer would have direct bearing on whether  $N_2$  fixation is the only other energy-consuming process after biosynthesis. A  $N_2$ -fixing continuous culture was maintained at a steady state (OD of 1.15 for 12 hr) and the rate of sucrose utilization was measured; the flow of medium through the growth vessel was stopped and the gas phase was changed to argon. Measurement of OD and sucrose at 15-min intervals over 2 hr showed that the rate of sucrose catabolism decreased to less than 25% of the control rate (Fig. 2). To show that this was not a result of cell death during the period of nitrogen deprivation, an  $N_2$  atmosphere was restored at the end

TABLE 3. End products of sucrose fermentation by *Clostridium pasteurianum*

Nitrogen source	pH of medium	A/S (μmoles/μmoles)	B/S (μmoles/μmoles)	A/B	Carbon recovered as A and B <sup>b</sup>
$N_2$	4.6	1.18	1.36	0.90	%
	4.7	1.12	1.30	0.86	64
	6.1	1.34	1.39	0.95	62
	6.4	1.24	1.37	0.91	69
$NH_3$	4.6	1.29	1.54	0.84	66
	6.5	1.34	1.44	0.93	73
	6.7	1.11	1.38	0.87	70
					64

<sup>a</sup> A (acetate), B (butyrate), S (sucrose).

<sup>b</sup> The remainder of the carbon is in the  $CO_2$  evolved and the cells produced.

of 2 hr and sucrose metabolism and growth returned to their former rates.

The same experiment was performed with a culture equilibrated under an atmosphere of argon with the  $NH_3$  concentration of the medium such that less than 1 μmole/ml remained in the effluent. At the beginning of the nitrogen deprivation period, the reservoir was changed to  $NH_3$ -free medium and the flow was stopped. The results in Fig. 3 show that, after the residual  $NH_3$  was consumed, the OD remained constant and the rate of sucrose catabolism decreased to less than 25% of the control rate.

If the low Y (sucrose) observed with cultures grown on limiting  $NH_3$  (Table 1) resulted from ATP utilization by a nonfunctioning  $N_2$ -fixing enzyme system, then it might be expected that  $N_2$ -fixing cells and  $NH_3$ -limited cells (cells possessing the  $N_2$ -fixing system but growing on limiting  $NH_3$  in the absence of  $N_2$ ) would consume more sucrose in a period of nitrogen deprivation than nitrogenase-free cells (cells grown on excess  $NH_3$ ). A comparison of sucrose consumption between growing and nongrowing cultures of  $N_2$ -fixing,  $NH_3$ -grown, and  $NH_3$ -limited cells showed that under all conditions sucrose consumption was depressed by nitrogen starvation. With sucrose in excess, sucrose catabolism in  $N_2$ -fixing and  $NH_3$ -grown cultures averaged about 13.6 and 12.6 mmoles per g of cells per hr under the nitrogen-sufficient conditions, and 6.3 and 4.3 mmoles per g of cells per hr when no nitrogen was present. These results, which are higher than those of Fig. 1 at zero growth rate with sucrose as the limiting substrate, suggested that, when sucrose is in excess and nitrogen is limiting, more uncoupled ATP hydrolysis occurs. The results with several cultures grown on limiting  $NH_3$

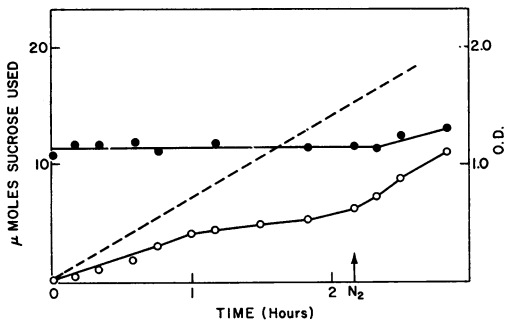


FIG. 2. Rate of sucrose utilization by a  $N_2$ -fixing culture during nitrogen starvation. Symbols: ○,  $\mu$ moles of sucrose used per ml; ●, optical density; and dotted line,  $\mu$ moles of sucrose used per ml by a growing culture.

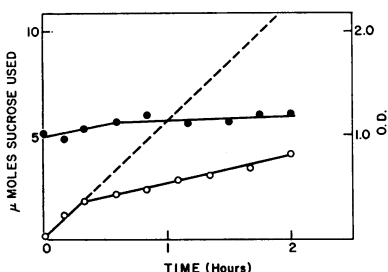


FIG. 3. Rate of sucrose utilization by an  $NH_3$ -grown culture during nitrogen starvation. Symbols: ○,  $\mu$ moles of sucrose used per ml; ●, optical density; and dotted line,  $\mu$ moles of sucrose used per ml by a growing culture.

showed a decrease in sucrose catabolized, but the decrease was variable, possibly because of the different composition of the  $N_2$ -fixing system. This is now under investigation.

#### DISCUSSION

Since each molecule of sucrose catabolized by *C. pasteurianum* yields four molecules of pyruvate and four molecules of ATP via the Embden-Meyerhoff-Parnas pathway, and the four pyruvate molecules in turn are catabolized to yield 1.26 molecules of acetate, 1.26 molecules of ATP, and 1.38 molecules of butyrate, the minimal gain of ATP per sucrose molecule would be 5.26 molecules. If an ATP molecule is also produced via phosphotransbutyrylase for each molecule of butyrate formed from butyryl-S-coenzyme A (12), the energy yield would be 6.64 ATP molecules per sucrose molecule. Finally, if the utilization of sucrose is initiated by phosphorolysis instead of by hydrolysis, the maximal yield of ATP per sucrose molecule would be 7.64 (unless there are other unknown sources of ATP). Since the maximal Y (sucrose) for  $NH_3$ -grown cultures is approximately 79, if the yield of ATP is 7.64/sucrose, then the Y (ATP) (3) would be 10.3.

Similarly, since the maximal Y (sucrose) for  $N_2$ -fixing cultures is 48, the Y (ATP) would be 6.3. If the energy demands for biosynthesis and assimilation of common material in both  $N_2$ -fixing and  $NH_3$ -grown cultures are the same and if the efficiency of ATP utilization were not decreased because of the slower growth rate imposed by nitrogen limitation, the ATP available for  $N_2$ -fixation would be 65 mmoles per g of cells. Since 1 g of cells contains 6.6 mmoles of nitrogen which corresponds to 3.3 mmoles of  $N_2$  fixed, the ATP to  $N_2$  ratio would be about 20. When compared to the best efficiency found in cell-free extracts (12 ATP per  $N_2$  fixed), this ratio suggested that some energy is lost as a result of the slower growth rate. If this is corrected for the difference in the rate of sucrose used at zero growth rate (Fig. 1), the ratio would be about 13 ATP per  $N_2$ .

Since the maximal growth rate constant for  $N_2$ -fixing cells is 0.40 and the nitrogen content of these cells is 6.6 mmoles per g of cells, the maximal rate of  $N_2$  fixation would be 1.32 mmoles of  $N_2$  fixed per g of dry cells per hr ( $1.32 \div 3.3 = 0.40$ ). This would correspond to a requirement of 15.9 mmoles of ATP per g of dry cells per hr if 12 ATP are required per  $N_2$  fixed (10) or of 26.4 mmoles of ATP per g of dry cells per hr if 20 ATP are used per  $N_2$  fixed. The average minimal amount (mmoles) of sucrose used per gram of cells per hour (8.5; Fig. 1) with sucrose limiting is equivalent to 65 mmoles of ATP per gram of dry cells per hr. Based on the ATP needed for the production of  $NH_3$ -grown cells, up to 40% of 65 mmoles of ATP per g of dry cells per hr, or 26.0 mmoles of ATP per g of dry cells per hr, is not needed for cellular biosynthesis. This agrees with the value of 26.4 based on 20 ATP molecules used per  $N_2$  molecule fixed. Since the  $N_2$  fixed based on 12 ATP per  $N_2$  would require a rate of 15.9 mmoles of ATP per g of dry cells per hr, 10.1 mmoles of ATP per g of dry cells per hr either was used for "maintenance" or was lost through hydrolysis, possibly via the  $N_2$ -fixing system.

The minimal rate of  $N_2$  fixation estimated by measuring acetylene reduction by intact cells of *C. pasteurianum* (in preparation) is 58  $\mu$ moles of  $N_2$  fixed per g of dry weight per min or 3.5 mmoles of  $N_2$  fixed per g of dry weight per hr. If this were the factor limiting the growth rate of the culture, the growth rate constant would be 1.06. Since the growth rate of the  $N_2$ -fixing culture is 0.40, this is not the limiting factor and over a twofold excess of enzyme is present ( $1.06/0.40$  or 3.5 mmoles of  $N_2$  fixed per g of dry weight per hr  $\div$  1.32 mmoles  $N_2$  fixed per g of dry cells per hr). In measuring the highest rate at which  $N_2$  could be fixed, we assumed, because only acetylene and argon were present in the reaction

vessel, that the cells were not growing and that the energy supply to the N<sub>2</sub>-fixing system was nonlimiting. If it were limiting, the maximal rate of N<sub>2</sub> fixation would be even greater.

One possible mechanism through which ATP could be wasted by cells containing the N<sub>2</sub>-fixing system could be through ATP utilization and H<sub>2</sub> production by an inefficient N<sub>2</sub>-fixing system (5). N<sub>2</sub> fixation by purified nitrogenase components of this organism has always been accompanied by H<sub>2</sub> evolution; in fact, between 20 and 50% of the ATP source supplied in the presence of N<sub>2</sub> can be consumed through this "ancillary" function of the N<sub>2</sub>-fixing system. The results reported here suggest that about 10% of the ATP may be consumed by this mechanism.

When sucrose and the nitrogen source are in excess, NH<sub>3</sub>-grown and N<sub>2</sub>-fixing cells have similar rates of sucrose catabolism. Of the ATP available from this sucrose catabolism, NH<sub>3</sub>-grown cells appear to use 94% in biosynthesis and the remainder (6%) either is used in other functions or is lost to the cell through uncoupled ATP hydrolysis. N<sub>2</sub>-fixing cells under the same conditions appear to use 55% of the energy in biosynthesis, 6% in the same unknown functions as NH<sub>3</sub>-grown cells, 11% through the N<sub>2</sub>-fixing system uncoupled to N<sub>2</sub> fixation, and 28% through the N<sub>2</sub>-fixing system coupled to N<sub>2</sub> fixation.

#### ACKNOWLEDGMENTS

This investigation was supported by National Science Foundation grant GB-05004.

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