

Flavobacterium johnsoniae as a Model Organism for Characterizing Biopolymer Utilization in Oligotrophic Freshwater Environments^{∇†}

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Biopolymers are important substrates for heterotrophic bacteria in oligotrophic freshwater environments, but information on bacterial growth kinetics with biopolymers is scarce. The objective of this study was to characterize bacterial biopolymer utilization in these environments by assessing the growth kinetics of *Flavobacterium johnsoniae* strain A3, which is specialized in utilizing biopolymers at $\mu\text{g liter}^{-1}$ levels. Growth of strain A3 with amylopectin, xyloglucan, gelatin, maltose, or fructose at 0 to 200 $\mu\text{g C liter}^{-1}$ in tap water followed Monod or Teissier kinetics, whereas growth with laminarin followed Teissier kinetics. Classification of the specific affinity of strain A3 for the tested substrates resulted in the following affinity order: laminarin ($7.9 \times 10^{-2} \text{ liter} \cdot \mu\text{g}^{-1} \text{ of C} \cdot \text{h}^{-1}$) \gg maltose $>$ amylopectin \approx gelatin \approx xyloglucan $>$ fructose ($0.69 \times 10^{-2} \text{ liter} \cdot \mu\text{g}^{-1} \text{ of C} \cdot \text{h}^{-1}$). No specific affinity could be determined for proline, but it appeared to be high. Extracellular degradation controlled growth with amylopectin, xyloglucan, or gelatin but not with laminarin, which could explain the higher affinity for laminarin. The main degradation products were oligosaccharides or oligopeptides, because only some individual monosaccharides and amino acids promoted growth. A higher yield and a lower ATP cell⁻¹ level was achieved at $\leq 10 \mu\text{g C liter}^{-1}$ than at $> 10 \mu\text{g C liter}^{-1}$ with every substrate except gelatin. The high specific affinities of strain A3 for different biopolymers confirm that some representatives of the classes *Cytophagia-Flavobacteria* are highly adapted to growth with these compounds at $\mu\text{g liter}^{-1}$ levels and support the hypothesis that *Cytophagia-Flavobacteria* play an important role in biopolymer degradation in (ultra)oligotrophic freshwater environments.

High-molecular-weight (HMW) compounds such as polysaccharides and proteins originating from phytoplankton and bacteria usually occur at concentrations in the $\mu\text{g liter}^{-1}$ range in oligotrophic aquatic environments (8, 34, 36, 38, 54). These biopolymers are considered to be important sources of carbon and energy for the heterotrophic bacteria in these ecosystems (2, 19). Low-molecular-weight (LMW) compounds (e.g., amino acids and monosaccharides) can diffuse directly into the cell, whereas biopolymers generally require extracellular enzymatic degradation and can be utilized only by bacteria that are capable of producing specific extracellular enzymes (4, 41).

Representatives of the classes *Cytophagia-Flavobacteria* seem to play a central role in the degradation of biopolymers in marine and freshwater environments (20, 24). A high abundance of *Cytophagia-Flavobacteria* was observed before and during phytoplankton blooms, when phytoplankton cells release large amounts of biopolymers (17, 18, 58). Furthermore, *Cytophagia-Flavobacteria* dominated the total bacterial community in culture-independent studies where natural bacterioplankton collected from aquatic environments was exposed to polymers such as starch, chitin, and bovine serum albumin (12, 39). Whole-genome sequencing of biopolymer-degrading bac-

terial isolates is increasingly applied to identify genes involved in biopolymer utilization processes (24, 32). These genome-based studies contribute to the enzymatic characterization of biopolymer-degrading bacterial strains. However, knowledge of nutritional versatility and growth kinetics is still essential for determining the role of these bacteria in the degradation of specific organic compounds in the environment. In contrast to the amount of kinetic data available in literature on oligotrophic aquatic bacteria consuming LMW compounds (9, 10, 27, 42, 48, 52), information on kinetic parameters of oligotrophic aquatic bacteria consuming HMW compounds is scarce.

In a recent study, *Flavobacterium johnsoniae* strain A3 was isolated from tap water supplemented with 100 μg of polysaccharide carbon liter⁻¹ and a river water inoculum (40). Strain A3 is particularly proficient in the utilization of a diverse group of oligo- and polysaccharides at $\mu\text{g liter}^{-1}$ levels in natural and treated water. Consequently, strain A3 may be a suitable model organism to study bacterial utilization of biopolymers in (ultra)oligotrophic freshwater environments. The genome of strain A3 has not been sequenced, but genome sequence information has recently been obtained for biopolymer-degrading *F. johnsoniae* strain UW101 and has allowed identification of proteins involved in biopolymer utilization (32). However, growth of strain UW101 with biopolymers has been demonstrated only at g liter⁻¹ levels (7, 32). Thus, whether the genome sequence data of strain UW101 can be used to elucidate the biopolymer utilization systems of strain A3 depends on the ability of strain UW101 to utilize biopolymers at $\mu\text{g liter}^{-1}$ levels.

The objective of our study was to characterize biopolymer

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TABLE 1. Amino acids, peptides, and proteins tested as growth substrates for strain A3 in tap water at 15°C^a

| Amino acid | Peptides and proteins |
|------------------|-------------------------------|
| L-Alanine | L-Alanyl-L-alanine |
| L-Aspartate | L-Alanyl-L-glutamine |
| L-Glutamine | Glycyl-L-aspartate |
| L-Glutamate | L-Glutamyl-L-glutamate |
| Glycine | Glycyl-L-leucyl-L-tyrosine |
| L-Isoleucine | Poly-DL-alanine ^b |
| L-Leucine | Poly-L-aspartate ^b |
| L-Lysine | Poly-L-glutamate ^b |
| DL-Phenylalanine | Casein ^c |
| L-Proline | Gelatin ^c |
| DL-Serine | Lectin ^c |
| L-Threonine | |
| L-Tyrosine | |
| L-Valine | |

^a All compounds were tested individually; the peptides and proteins were also tested simultaneously as constituents of the peptide-and-protein mixture.

^b Molecular masses: poly-DL-alanine, 1 to 5 kDa; poly-L-aspartate, 5 to 15 kDa; and poly-L-glutamate, 3 to 15 kDa (Sigma-Aldrich, Germany).

^c Casein sodium salt from bovine milk; gelatin from bovine skin, type B; and lectin from *Canavalia ensiformis* (jack bean) (Sigma-Aldrich, Germany).

utilization in oligotrophic freshwater environments by (i) assessing the kinetics and physiology of *F. johnsoniae* strain A3 during its growth with selected biopolymers at $\mu\text{g liter}^{-1}$ levels in tap water and (ii) comparing the putative biopolymer utilization systems of *F. johnsoniae* strains A3 and UW101 and their abilities to utilize selected biopolymers at $\mu\text{g liter}^{-1}$ levels.

MATERIALS AND METHODS

Assessment of growth of *F. johnsoniae* strain A3 with peptides and proteins.

The ability of strain A3 to utilize peptides and proteins was assessed using a mixture of five oligopeptides (L-alanyl-L-alanine, L-alanyl-L-glutamine, glycyl-L-aspartate, L-glutamyl-L-glutamate, glycyl-L-leucyl-L-tyrosine), three polypeptides (poly-DL-alanine, poly-L-aspartate, poly-L-glutamate), and three proteins (casein, gelatin, lectin) at a concentration of 10 $\mu\text{g C liter}^{-1}$ per compound in tap water (Table 1). Furthermore, the compounds included in the peptide-protein mixture and 14 amino acids were also tested as individual growth substrate for strain A3 at 10 $\mu\text{g C liter}^{-1}$ (Table 1). Tap water (600 ml), prepared from anaerobic groundwater by aeration and rapid sand filtration and containing 1.9 mg dissolved organic carbon (DOC) liter⁻¹, was collected and pasteurized for 30 min at 60°C in Pyrex glass Erlenmeyer flasks, which had been cleaned as previously described (44). The peptide-protein mixture and the individual compounds were added from solutions separately prepared in Milli-Q ultrapure water (Millipore) and heated for 30 min at 60°C. The tap water samples were supplemented with an excess of NO_3^- and PO_4^{3-} and inoculated with 50 to 200 CFU ml⁻¹ of strain A3 (50 to 150 μl of inoculum) precultured as previously described (40). All samples were prepared in duplicate flasks and incubated without shaking at 15°C until maximum colony counts (N_{max}) were reached. Colony counts of strain A3 were determined daily or every other day using triplicate Lab-Lemco agar (LLA) streak-plates (Oxoid), which were incubated for 3 days at 25°C.

Estimation of growth kinetics and yields of *F. johnsoniae* strain A3. Growth kinetics of strain A3 were determined with fructose, maltose, laminarin (from *Laminaria digitata* [Sigma-Aldrich, Germany]), xyloglucan (from tamarind seeds [Megazyme, Ireland]), amylopectin (from corn [Sigma-Aldrich, Germany]), gelatin, or proline as the growth substrate at 0, 1.0, 2.5, 5.0, 7.5, 10, 25, 50, 100, and 200 $\mu\text{g C liter}^{-1}$ in tap water. In addition, the growth rate of strain A3 was determined with laminaribiose, laminaripentaose (both from Megazyme, Ireland), lectin, or casein at 5 $\mu\text{g C liter}^{-1}$ and with alanine or glutamate at 100 $\mu\text{g C liter}^{-1}$. Duplicate sample flasks were supplemented with substrate, inoculated with precultured strain A3, and incubated without shaking at 15°C until N_{max} values were reached (40). The incubation period varied from 7 days (laminarin; 200 $\mu\text{g C liter}^{-1}$) to 28 days (proline; 200 $\mu\text{g C liter}^{-1}$). During the incubation period, the total ATP concentration was measured once or twice per day using a bioluminescence assay as described previously (53). When the maximum growth level was (about to be) reached based on the ATP concentration mea-

sured, the total direct cell (TDC) count was determined using acridine orange (22) and epifluorescence microscopy (DMRXA [Leica, The Netherlands]). Depending on the type of substrate and the added substrate concentration, the colony count was determined one to four times per day using the method described above. The mean plating efficiency and standard error of the mean were estimated from the ratios between N_{max} and TDC for a total of 53 samples. The Shapiro-Wilk test was used to test whether the 53 $N_{\text{max}}/\text{TDC}$ ratios were normally distributed (α level of significance = 0.05). Subsequently, the 95% confidence interval of the mean plating efficiency was calculated to determine with 95% certainty whether the mean plating efficiency was significantly different from 100%. The validity of using batch cultures for determining the growth kinetics of strain A3 is shown in Fig. S1 in the supplemental material.

The yield Y (CFU μg^{-1} of C) of strain A3 with each of the tested substrates was calculated from the linear relationship between the N_{max} value of strain A3 and substrate concentration. The growth rate V (h^{-1}) of strain A3 during the exponential growth phase at the various substrate concentrations was calculated using the following equation:

$$V = \log N_2 - \log N_1 / [\log 2 \times (t_2 - t_1)] \quad (1)$$

where N_2 and N_1 are the colony counts at time points t_2 and t_1 . The relationship between the growth rate of strain A3 and the substrate concentration was modeled according to Monod kinetics or Teissier kinetics. The Monod model (33) can be written as follows:

$$V = V_{\text{max}} \times [S/(K_s + S)] \quad (2)$$

and the Teissier model (43) can be written as follows:

$$V = V_{\text{max}} \times [1 - \exp(-S/K_s')] \quad (3)$$

In equations 2 and 3, V and V_{max} are the observed and maximum growth rates (h^{-1}) and S is the substrate concentration ($\mu\text{g C liter}^{-1}$). In each of the seven experiments conducted to determine the growth kinetics of strain A3 (i.e., one experiment per substrate), limited growth of strain A3 with the indigenous compounds in the blank (i.e., tap water) was observed. It was assumed that these indigenous compounds were utilized simultaneously with the substrate added to the tap water. Consequently, S in equations 2 and 3 is $\Delta S + S_b$, with ΔS representing the added substrate concentration and S_b the apparent indigenous substrate concentration, which was calculated from the N_{max} of strain A3 in the blank and its average yield of $1.43 (\pm 0.13) \times 10^7$ CFU μg^{-1} of C at $\leq 10 \mu\text{g}$ of added substrate C liter⁻¹. K_s is the saturation constant and represents S when V is $1/2 V_{\text{max}}$, whereas K_s' is the apparent saturation constant and equals $K_s/\ln 2$ (1, 3). The V_{max}/K_s ratio (liter μg^{-1} of C $\cdot \text{h}^{-1}$) is defined as the specific affinity of strain A3 for the substrate tested.

Assessment of growth of *F. johnsoniae* strain UW101 at low substrate concentrations. *F. johnsoniae* strain UW101 (ATCC 17061) was obtained from LGC Standards, United Kingdom. Strain UW101 was precultured in a previously described mineral salts medium (40) supplemented with 100 μg of laminarin C liter⁻¹ and 100 μg of $\text{NO}_3^- \text{N liter}^{-1}$. The preculture was incubated at 15°C and stored at 4°C when the stationary growth phase was reached. Subsequently, growth of strain UW101 was tested at 10 $\mu\text{g C liter}^{-1}$ of the following individual organic compounds: amylopectin, xyloglucan, pectin, laminarin, maltose, glucose, fructose, casein, gelatin, and lectin. Tap water samples and pasteurized solutions of the individual compounds were prepared as described above. Duplicate sample flasks were incubated at 15°C after inoculation with strain UW101. The colony count of strain UW101 was determined using LLA plates according to the method described above for strain A3.

RESULTS

Utilization of amino acids, peptides, and proteins by *F. johnsoniae* strain A3. Strain A3 can utilize various oligo- and polysaccharides (40). In the present study, the ability of strain A3 to utilize amino acids, peptides, and proteins was investigated. Of the 14 individually tested amino acids, alanine, glutamate, glutamine, isoleucine, proline, and threonine were utilized by strain A3, but the N_{max} values and growth rates reached with isoleucine and threonine were considerably lower than with alanine, glutamine, glutamate, and proline (Table 2). Strain A3 reached an N_{max} value of $8.1 (\pm 0.09) \times 10^5$ CFU ml⁻¹ in tap water supplemented with a mixture of 11 oligo- and

TABLE 2. Maximum colony counts (N_{max}) and growth rates (V) of *F. johnsoniae* strain A3 in tap water supplemented with individual amino acids, peptides, and proteins at 10 $\mu\text{g C liter}^{-1}$

| Amino acid, peptide, or protein | N_{max} ($\times 10^5$ CFU ml $^{-1} \pm$ SD) | V (h $^{-1}$) ^c |
|---------------------------------|---|----------------------------------|
| Amino acids | | |
| Blank I ^a | 0.04 (\pm 0.004) | 0.017 |
| Ala | 0.8 (\pm 0.01) | 0.029 |
| Asp | NG ^b | NG |
| Gln | 1.1 (\pm 0.07) | 0.039 |
| Glu | 1.1 (\pm 0.05) | 0.038 |
| Gly | NG | NG |
| Ile | 0.5 (\pm 0.1) | 0.019 |
| Leu | NG | NG |
| Lys | NG | NG |
| Phe | NG | NG |
| Pro | 1.1 (\pm 0.1) | 0.039 |
| Ser | NG | NG |
| Thr | 0.4 (\pm 0.2) | 0.016 |
| Tyr | NG | NG |
| Val | NG | NG |
| Peptides and proteins | | |
| Blank II ^a | 0.03 (\pm 0.002) | 0.013 |
| Ala-Ala | 0.6 (\pm 0.01) | 0.022 |
| Ala-Gln | 1.1 (\pm 0.2) | 0.046 |
| Gly-Asp | NG | NG |
| Glu-Glu | 1.1 (\pm 0.01) | 0.081 |
| Gly-Leu-Tyr | NG | NG |
| Poly-Ala | NG | NG |
| Poly-Asp | NG | NG |
| Poly-Glu | NG | NG |
| Casein | 1.3 (\pm 0.1) | 0.081 |
| Gelatin | 1.2 (\pm 0.02) | 0.081 |
| Lectin | 1.1 (\pm 0.06) | 0.034 |

^a Blank I (i.e., tap water in duplicate flasks) was included in the series of individually tested amino acids, and blank II in the series of individually tested peptides and proteins.

^b NG, growth not different from growth in the blank.

^c Standard deviation ≤ 0.005 h $^{-1}$ for all V values determined.

polypeptides and proteins at 10 $\mu\text{g C liter}^{-1}$ per compound, as compared to an N_{max} value of $6.4 (\pm 0.1) \times 10^3$ CFU ml $^{-1}$ in the blank. The dipeptides L-alanyl-L-alanine (Ala-Ala), L-alanyl-L-glutamine (Ala-Gln), and L-glutamyl-L-glutamate (Glu-Glu) and the proteins casein, gelatin, and lectin promoted growth of strain A3 when tested individually at 10 $\mu\text{g C liter}^{-1}$ (Table 2). The growth rate of strain A3 with casein, gelatin, Glu-Glu, or Ala-Gln at 10 $\mu\text{g C liter}^{-1}$ was higher than that with the individually growth-promoting amino acids. These results imply that strain A3 preferentially utilizes growth-promoting oligopeptides and proteins instead of individually growth-promoting amino acids.

Growth kinetics of strain A3 with carbohydrates and proteins. The growth kinetic parameters of strain A3 for each substrate tested were derived from the relationship between the growth rate of strain A3 and the substrate concentration. The data obtained for growth of strain A3 with laminarin fitted best to the Teissier model (Fig. 1A), whereas growth with fructose, maltose (Fig. 1B), xyloglucan, amylopectin, or gelatin could be equally well described by Monod or Teissier kinetics. The order of the substrates based on the specific affinity (V_{max}/K_s ratio) of strain A3 was as follows: laminarin \gg maltose $>$ amylopectin \approx gelatin \approx xyloglucan $>$ fructose (Table 3). A particularly high specific affinity of 7.9×10^{-2}

liter $\cdot \mu\text{g}^{-1}$ of C $\cdot \text{h}^{-1}$ was obtained for laminarin, and the specific affinities of strain A3 for xyloglucan, amylopectin, gelatin, and maltose ranged from approximately 1.1×10^{-2} to 2.3×10^{-2} liter $\cdot \mu\text{g}^{-1}$ of C $\cdot \text{h}^{-1}$. Strain A3 is clearly adapted to growth with these substrates at $\mu\text{g C liter}^{-1}$ levels. The V_{max} of strain A3 with fructose was comparable to the V_{max} with amylopectin and xyloglucan, but fructose did not promote growth of strain A3 at 2.5 and 5.0 $\mu\text{g C liter}^{-1}$, in contrast to the other substrates tested. As a result, the highest K_s value and lowest specific affinity were observed for fructose, demonstrating that strain A3 has a lower specific affinity for this monosaccharide than for the other carbohydrates tested.

The K_s value and specific affinity for proline could not be calculated, because the growth rate of strain A3 was the same at all substrate concentrations (2.5 to 200 $\mu\text{g C liter}^{-1}$) and growth was not tested at $<2.5 \mu\text{g C liter}^{-1}$ (Fig. 2). Apparently, strain A3 already attained its V_{max} at 2.5 $\mu\text{g C liter}^{-1}$, which implies that its K_s value with proline is lower than 2.5 $\mu\text{g C liter}^{-1}$. In addition, the growth curves revealed that the exponential growth of strain A3 in tap water with proline at 10, 25, 50, 100, and 200 $\mu\text{g C liter}^{-1}$ occurred in two

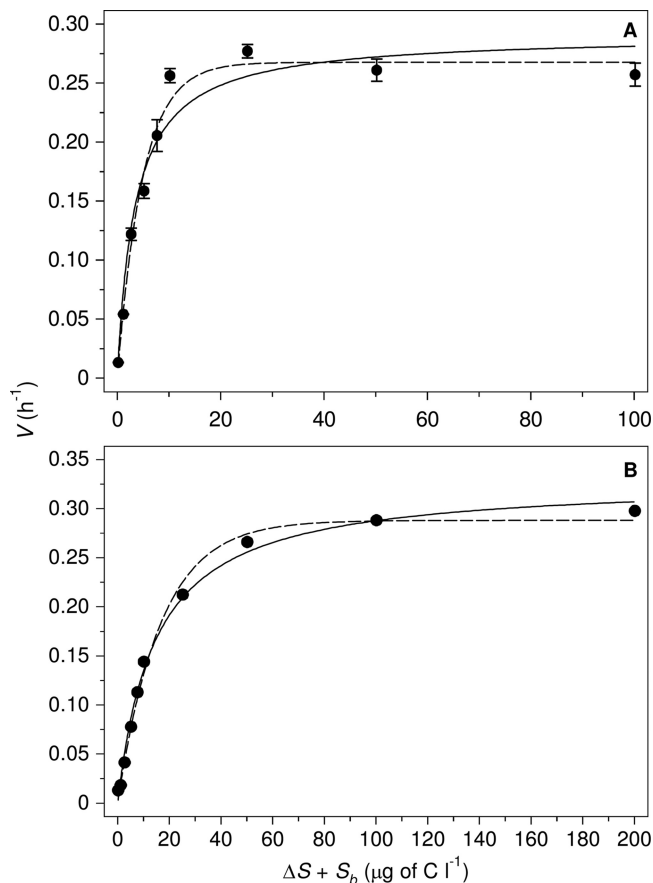


FIG. 1. Growth rate V (h $^{-1}$) of *F. johnsoniae* strain A3 at 15°C in relation to the concentration ΔS of laminarin (A) and maltose (B) added to pasteurized tap water with an apparent indigenous substrate concentration S_b of $0.2 (\pm 0.00) \mu\text{g biopolymer C equivalents liter}^{-1}$. Data modeled according to Monod kinetics (solid line) and Teissier kinetics (dashed line). Error bars represent standard deviation of V in duplicate flasks. In panel B, error bars are not visible because the standard deviation was ≤ 0.005 h $^{-1}$ for all V values determined.

TABLE 3. Kinetic parameters of *F. johnsoniae* strain A3 for various substrates tested at 15°C

| Substrate | Kinetic model | Kinetic parameter | | | R^2 |
|-------------|-----------------|---|--|--|-------|
| | | V_{\max} (h^{-1}) ^a | K_s ($\mu\text{g C liter}^{-1}$ \pm SD) | Specific affinity ($\times 10^{-2}$ liter \cdot μg^{-1} of C \cdot h^{-1} \pm SD) | |
| Fructose | Monod | 0.22 | 34.4 (\pm 1.1) | 0.69 (\pm 0.01) | 0.99 |
| | Teissier | 0.19 | 24.0 (\pm 0.6) | 0.81 (\pm 0.01) | 0.99 |
| Maltose | Monod | 0.33 | 14.4 (\pm 0.1) | 2.3 (\pm 0.002) | 0.99 |
| | Teissier | 0.29 | 11.5 (\pm 0.1) | 2.5 (\pm 0.02) | 1.00 |
| Laminarin | Monod | 0.29 | 3.4 (\pm 0.3) | 8.5 (\pm 0.5) | 0.95 |
| | Teissier | 0.27 | 3.4 (\pm 0.2) | 7.9 (\pm 0.01) | 0.98 |
| Amylopectin | Monod | 0.23 | 17.0 (\pm 0.2) | 1.4 (\pm 0.01) | 0.99 |
| | Teissier | 0.20 | 14.3 (\pm 1.3) | 1.4 (\pm 0.05) | 0.98 |
| Xyloglucan | Monod | 0.24 | 21.8 (\pm 1.4) | 1.1 (\pm 0.05) | 0.99 |
| | Teissier | 0.21 | 17.8 (\pm 0.8) | 1.2 (\pm 0.04) | 0.99 |
| Proline | ND ^b | 0.019 | <2.5 ^b | >0.76 ^b | |
| Gelatin | Monod | 0.22 | 18.5 (\pm 0.1) | 1.2 (\pm 0.01) | 0.99 |
| | Teissier | 0.19 | 14.5 (\pm 0.04) | 1.3 (\pm 0.01) | 1.00 |

^a Standard deviation $\leq 0.005 \text{ h}^{-1}$ for all V_{\max} values determined.

^b Actual K_s and specific affinity could not be determined (ND), because V_{\max} had already been reached at the lowest ΔS of $2.5 \mu\text{g C liter}^{-1}$.

phases (Fig. 2). During the first exponential growth phase (day 0 until day 9), strain A3 grew at a higher rate than during the second exponential growth phase (day 10 until stationary phase). The growth rate of strain A3 in tap water supplemented with proline was $0.039 (\pm 0.001) \text{ h}^{-1}$ during the first exponential growth phase and equaled the sum of the actual growth rate with this amino acid during the second exponential growth phase ($0.019 \pm 0.001 \text{ h}^{-1}$) and the growth rate in the blank ($0.022 \pm 0.001 \text{ h}^{-1}$). These results suggest simultaneous uptake of the added proline and the indigenous organic compounds present in the tap water during the first phase of exponential growth. The same phenomenon occurred when strain A3 was grown in tap water supplemented with alanine or glutamate at $100 \mu\text{g C liter}^{-1}$ (growth curves not shown). The actual growth rates of strain A3 with alanine or glutamate at $100 \mu\text{g C liter}^{-1}$ ($0.015 \pm 0.001 \text{ h}^{-1}$ and $0.020 \pm 0.000 \text{ h}^{-1}$) were comparable to those observed at $10 \mu\text{g C liter}^{-1}$ ($0.012 \pm 0.001 \text{ h}^{-1}$ and $0.021 \pm 0.001 \text{ h}^{-1}$; calculated from data in Table 2), indicating that strain A3 grew at its V_{\max} at both concentrations.

The nature of the compounds produced by strain A3 upon extracellular degradation of laminarin was assessed by testing its growth with laminaripentaose or laminaribiose at $5 \mu\text{g C liter}^{-1}$ in tap water (S_b of $0.6 \pm 0.05 \mu\text{g biopolymer C equivalents liter}^{-1}$). Laminaripentaose promoted growth of strain A3 at a slightly higher rate ($0.18 \pm 0.002 \text{ h}^{-1}$) than laminarin ($0.16 \pm 0.003 \text{ h}^{-1}$), but laminaribiose was not utilized by strain A3. Thus, strain A3 appears to produce laminari-oligosaccharides larger than laminaribiose upon laminarin degradation. To obtain more data about the specific affinity of strain A3 for individual proteins other than gelatin, growth of strain A3 with casein or lectin was also tested at $5 \mu\text{g C liter}^{-1}$ in tap water.

The growth rate of strain A3 with casein ($0.046 \pm 0.000 \text{ h}^{-1}$) was nearly the same as that with gelatin ($0.045 \pm 0.000 \text{ h}^{-1}$), whereas the growth of strain A3 with lectin was almost twice as slow ($0.026 \pm 0.001 \text{ h}^{-1}$). The nearly identical growth rates of strain A3 with casein and gelatin at $5 \mu\text{g C liter}^{-1}$ and at $10 \mu\text{g C liter}^{-1}$ (0.081 h^{-1} ; Table 2) suggest that the specific affinities for casein and gelatin approximate each other. Strain A3 seems to have a lower specific affinity for lectin than for casein and gelatin, because the growth rates with lectin at $5 \mu\text{g C liter}^{-1}$ and $10 \mu\text{g C liter}^{-1}$ (0.034 h^{-1} ; Table 2) were lower than with the other two proteins.

Yields of strain A3 with carbohydrates and proteins. Plotting the N_{\max} value of strain A3 as a function of maltose concentration revealed two linear relationships (Fig. 3). The first relationship is valid for ΔS values of $\leq 10 \mu\text{g C liter}^{-1}$ and the second for $>10 \mu\text{g C liter}^{-1}$. This phenomenon was also observed with the other individual substrates tested, except gelatin. Consequently, the yields (expressed in CFU μg^{-1} of C) of strain A3 estimated with maltose, laminarin, amylopectin, xyloglucan, and proline are higher at ΔS values of $\leq 10 \mu\text{g C liter}^{-1}$ than at ΔS values of $>10 \mu\text{g C liter}^{-1}$ (Table 4).

The 53 N_{\max} /TDC ratios used to calculate the mean plating efficiency came from a normal distribution ($P = 0.30$). The mean plating efficiency of strain A3 was 101.9% (SEM 1%; $n = 53$) with a 95% confidence interval from 99.8% to 103.8% efficiency. This 95% confidence interval includes 100%, and therefore it can be assumed with 95% certainty that the mean plating efficiency did not differ from 100% and that each cell of strain A3 formed a colony. Thus, the lower yield for ΔS values of $>10 \mu\text{g C liter}^{-1}$ did not result from a lower plating efficiency.

Two average yields were calculated from the yields obtained with the seven individually tested substrates: (i) Y_{mean} of $1.43 (\pm 0.13) \times 10^7 \text{ CFU } \mu\text{g}^{-1}$ of C, when the N_{\max} of strain A3 is $\leq 1.5 \times 10^5 \text{ CFU liter}^{-1}$ and thus represents

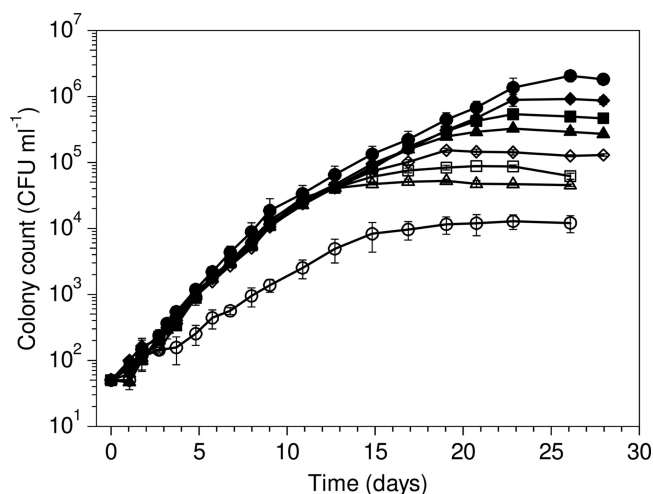


FIG. 2. Growth of *F. johnsoniae* strain A3 at 15°C in tap water supplemented with proline at various concentrations. Symbols: \circ , blank, no proline added; \triangle , $2.5 \mu\text{g proline C liter}^{-1}$ added; \square , $5.0 \mu\text{g proline C liter}^{-1}$ added; \diamond , $10 \mu\text{g proline C liter}^{-1}$ added; \blacktriangle , $25 \mu\text{g proline C liter}^{-1}$ added; \blacksquare , $50 \mu\text{g proline C liter}^{-1}$ added; \bullet , $100 \mu\text{g proline C liter}^{-1}$ added. Error bars indicate standard deviation of colony count in duplicate flasks.

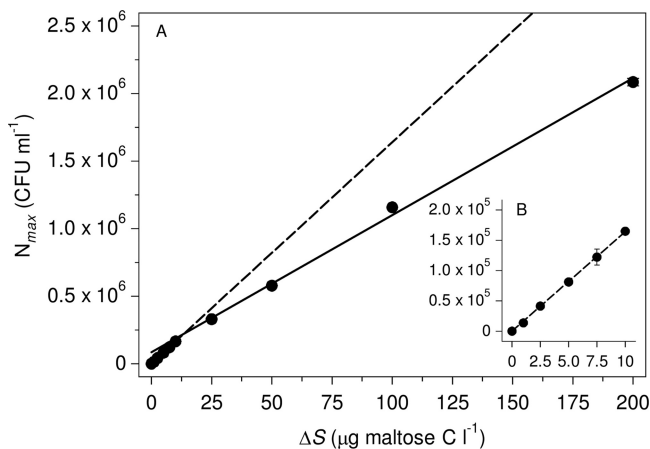


FIG. 3. Maximum colony count (N_{max}) of *F. johnsoniae* strain A3 at 15°C in relation to the concentration ΔS of maltose added to pasteurized tap water. (A) Dashed line represents the linear relationship between N_{max} and ΔS when $<10 \mu\text{g C liter}^{-1}$. Solid line shows the linear relationship between N_{max} and ΔS when $>10 \mu\text{g C liter}^{-1}$. Error bars indicate standard deviation of N_{max} in duplicate flasks. (B) Data points of the linear relationship between N_{max} and substrate concentration ΔS when $<10 \mu\text{g C liter}^{-1}$.

a concentration of $\leq 10 \mu\text{g biopolymer C liter}^{-1}$; and (ii) Y_{mean} of $0.98 (\pm 0.17) \times 10^7 \text{ CFU } \mu\text{g}^{-1}$ of C, when the N_{max} of strain A3 is $> 1.5 \times 10^5 \text{ CFU ml}^{-1}$ and indicates the presence of $> 10 \mu\text{g biopolymer C liter}^{-1}$.

Growth of *F. johnsoniae* strain UW101 at $\mu\text{g liter}^{-1}$ levels. Of the 10 carbohydrates and proteins tested, only laminarin and maltose promoted growth of strain UW101 at $10 \mu\text{g C liter}^{-1}$. Strain UW101 attained a higher growth rate with laminarin ($0.16 \pm 0.001 \text{ h}^{-1}$) than with maltose ($0.07 \pm 0.000 \text{ h}^{-1}$), but its N_{max} value with laminarin ($5.9 [\pm 0.3] \times 10^4 \text{ CFU ml}^{-1}$) was the same as with maltose ($6.2 [\pm 0.1] \times 10^4 \text{ CFU ml}^{-1}$). These growth parameters are significantly lower than the growth rate and N_{max} value reached by strain A3 when it was grown with laminarin ($0.26 \pm 0.001 \text{ h}^{-1}$; $1.6 [\pm 0.1] \times 10^5 \text{ CFU ml}^{-1}$) or maltose at $10 \mu\text{g C liter}^{-1}$ ($0.16 \pm 0.002 \text{ h}^{-1}$; $1.7 [\pm 0.0] \times 10^5 \text{ CFU ml}^{-1}$). In addition, unlike strain A3, strain UW101 did not grow in the blank during the incubation period. Hence, strain UW101 seems less well adapted to oligotrophic conditions than strain A3.

DISCUSSION

Biopolymer utilization by *F. johnsoniae* strains A3 and UW101. The growth rates of strain A3 with proline, glutamine, glutamate, or alanine at 10 and $100 \mu\text{g C liter}^{-1}$ in the present study were nearly identical to the growth rate of the strain ($0.016 \pm 0.000 \text{ h}^{-1}$) with a mixture of 20 different amino acids ($10 \mu\text{g C liter}^{-1}$ per compound) in a previous study (40). The higher growth rates of strain A3 with Ala-Gln, Glu-Glu, casein, gelatin, and lectin than with the amino acid mixture and the individually growth-promoting amino acids indicate the preference of strain A3 for utilizing oligopeptides and proteins as a source of energy and carbon. Casein, gelatin, and lectin, which were utilized by strain A3 at 10 and $5 \mu\text{g C liter}^{-1}$, differ in amino acid composition and sequence. The main constituents ($>10\% \text{ wt/wt}$) in casein are glutamate, leucine, and pro-

line; gelatin is rich in glycine, proline, hydroxyproline, and alanine; and aspartate and serine are predominant in lectin (14, 15, 28). In addition, more than 10 other types of amino acids are present in each of the three proteins at concentrations varying from 0.5 to 10%. The fact that strain A3 can utilize various complex proteins but only a limited number of individual amino acids as a sole energy source demonstrates that oligopeptides are the main extracellular products of protein degradation by the microorganism. These findings are consistent with previous observations indicating that strain A3 preferentially utilizes oligo- and polysaccharides instead of monosaccharides and produces oligosaccharides upon extracellular polysaccharide degradation that are not hydrolyzed before uptake into the cytoplasm (40). A comparable biopolymer degradation strategy has been suggested for *Flavobacterium* sp. strain S12 (45). Furthermore, the growth of strain A3 with the amino acid mixture and with the individual proteins suggests that amino acids and oligopeptides not serving as an individual energy source are utilized as a carbon source in the presence of an appropriate energy source(s).

Like strain A3, *F. johnsoniae* strain UW101 can degrade laminarin, amylopectin, pectin, xylan, xyloglucan, gelatin, and casein (7, 32). Genome sequence analysis has demonstrated that strain UW101 possesses proteins to bind specific biopolymers (e.g., α/β -glucans, hemicelluloses, chitin, pectins, peptides) to its outer membrane and outer membrane-associated enzymes to degrade the bound biopolymers into oligomers that pass the outer membrane via oligomer-specific porins (32). Based on its metabolic capacities, it seems likely that strain A3 has also included outer membrane-associated binding proteins and enzymes and oligomer-specific porins in its biopolymer utilization systems. However, growth of strain UW101 with the aforementioned biopolymers has been demonstrated only at high substrate concentrations of 5 or 10 g of biopolymer liter⁻¹ (7, 32). In the present study, it was shown that strain UW101

TABLE 4. Yields of *F. johnsoniae* strain A3 with various individual substrates tested at 15°C

| Substrate | Yield | |
|-------------|---|---|
| | ΔS range ($\mu\text{g C liter}^{-1}$) | $Y (\times 10^7 \text{ CFU } \mu\text{g}^{-1} \text{ of C } \pm \text{SD})$ |
| Fructose | 0-10 | — ^a |
| | 10-200 | 0.93 (± 0.02) |
| Maltose | 0-10 | 1.65 (± 0.03) |
| | 10-200 | 1.01 (± 0.02) |
| Laminarin | 0-10 | 1.30 (± 0.04) |
| | 10-200 | 0.75 (± 0.01) |
| Amylopectin | 0-10 | 1.47 (± 0.03) |
| | 10-100 | 0.98 (± 0.10) |
| Xyloglucan | 0-10 | 1.45 (± 0.01) |
| | 10-100 | 0.89 (± 0.02) |
| Proline | 0-10 | 1.42 (± 0.03) |
| | 10-200 | 0.99 (± 0.03) |
| Gelatin | 0-200 | 1.31 (± 0.07) |

^a —, no linear relationship between N_{max} and ΔS when $<10 \mu\text{g C liter}^{-1}$.

utilized only maltose and laminarin of the 10 carbohydrates and proteins tested at $10 \mu\text{g C liter}^{-1}$, whereas strain A3 utilized all 10 compounds, except glucose (Table 2) (40). Moreover, strain UW101 grew at significantly low rates with maltose and laminarin at $10 \mu\text{g C liter}^{-1}$ compared with strain A3. The N_{max} values reached by strain UW101 when grown with these compounds were almost thrice lower than those of strain A3, which suggests that cells of strain UW101 were larger than those of strain A3 during growth at $\mu\text{g C liter}^{-1}$ levels. These physiological differences between strains UW101 and A3 and their relatively low 16S rRNA gene similarity of 97% reduce the extent to which the whole-genome sequence data of strain UW101 can be used to elucidate biopolymer utilization by strain A3. Growth experiments with biopolymer-degrading bacteria at $\mu\text{g C liter}^{-1}$ levels clearly provide essential information in addition to genome sequence information.

Growth kinetics of *F. johnsoniae* strain A3 for biopolymers.

The Monod model is based on the theory that a single rate-limiting, saturation kinetics-exhibiting transport system at the cytoplasmic membrane controls bacterial growth (33), whereas the Teissier model assumes growth to depend on diffusion-controlled substrate supply through the outer membrane (43). However, the mathematical difference between these models is small at low substrate concentrations (26), which could explain why both were applicable to the growth of strain A3 with fructose, maltose, xyloglucan, amylopectin, and gelatin. The similarity of the two specific affinities obtained for growth of strain A3 with laminarin demonstrates that, despite the better fit of the growth data to the Teissier model, the Monod model could also be applied. The growth kinetic parameters of strain A3 have been determined by assuming that ΔS was utilized simultaneously with S_b . Simultaneous utilization is expected when ΔS values are close to S_b , but sequential utilization seems more likely when ΔS is high (i.e., the added substrate is used preferentially) (48). However, the specific affinities of strain A3 did not significantly change when preferential utilization of the added substrate at ΔS values of $\geq 25 \mu\text{g C liter}^{-1}$ was assumed (data not shown; $P < 0.01$, t test), which indicates that the low apparent S_b (0.2 to 2 biopolymer C equivalents liter^{-1}) did not significantly contribute to these high substrate concentrations.

The lower specific affinity of strain A3 for fructose than for the polysaccharides and gelatin confirms that strain A3 is specialized in biopolymer utilization at $\mu\text{g C liter}^{-1}$ levels. Few data are available on the growth kinetics of other biopolymer-consuming, oligotrophic bacteria for comparison with the growth kinetic parameters of strain A3. The high specific affinity of strain A3 for laminarin ($7.9 \times 10^{-2} \text{ liter} \cdot \mu\text{g}^{-1}$ of $\text{C} \cdot \text{h}^{-1}$) is close to the specific affinities reported for growth of *Flavobacterium* sp. strain S12 with maltodextrins (7.1×10^{-2} to $8.3 \times 10^{-2} \text{ liter} \cdot \mu\text{g}^{-1}$ of $\text{C} \cdot \text{h}^{-1}$) and to the specific affinity observed for growth of *Flavobacterium* sp. strain 166 with starch ($6.9 \times 10^{-2} \text{ liter} \cdot \mu\text{g}^{-1}$ of $\text{C} \cdot \text{h}^{-1}$) (45, 49). Higher specific affinities have been reported only for *Aeromonas hydrophila* M800 grown with either oleate ($11 \times 10^{-2} \text{ liter} \cdot \mu\text{g}^{-1}$ of $\text{C} \cdot \text{h}^{-1}$) or arginine ($28 \times 10^{-2} \text{ liter} \cdot \mu\text{g}^{-1}$ of $\text{C} \cdot \text{h}^{-1}$) and for *Polaromonas* strain P315 grown with acetate ($25 \times 10^{-2} \text{ liter} \cdot \mu\text{g}^{-1}$ of $\text{C} \cdot \text{h}^{-1}$) (30, 47). In review studies on other oligotrophic bacteria consuming LMW compounds, the highest reported specific affinity was $1.2 \times 10^{-2} \text{ liter} \cdot \mu\text{g}^{-1}$ of $\text{C} \cdot \text{h}^{-1}$ for the marine bacterium *Cycloclasticus oligotrophus*

grown with toluene (recalculated from a specific affinity of $47.4 \text{ liter} \cdot \text{mg}^{-1}$ of $\text{cells} \cdot \text{h}^{-1}$) (9–11, 42). Hence, the higher specific affinities of strain A3 for laminarin, maltose, gelatin, and amylopectin, along with those of strains S12, 166, M800, and P315, confirm that these strains are adapted to oligotrophic conditions.

Extracellular degradation is the first process in biopolymer utilization and could control bacterial growth with biopolymers (5, 31). The slightly higher growth rate of strain A3 with laminaripentaose ($0.18 \pm 0.002 \text{ h}^{-1}$) than with laminarin ($0.16 \pm 0.003 \text{ h}^{-1}$) at $5 \mu\text{g C liter}^{-1}$ indicates that extracellular degradation of laminarin was not rate limiting. However, the lower specific affinity of strain A3 for amylopectin than for laminarin and the higher specific affinity for maltose than for amylopectin reveal that extracellular degradation was rate limiting in amylopectin utilization by strain A3. The 10^4 - to 5×10^5 -kDa and extensively branched amylopectin molecule is clearly more difficult to degrade than the 5- to 6-kDa linear laminarin molecule (6, 37). In contrast to amylopectin, maltose can diffuse directly through the outer membrane of strain A3 via nonspecific porins and probably also via a maltodextrin-specific porin for amylopectin degradation products (35). The lower specific affinity of strain A3 for maltose than for laminarin suggests that maltose was transported across the cytoplasmic membrane at a lower rate than the oligosaccharides produced upon laminarin degradation, which were presumably larger than laminaribiose. Like *Flavobacterium* sp. strain S12, strain A3 may degrade amylopectin into maltodextrins instead of maltose (45), but additional research would be needed to assess if strain A3 has higher specific affinities for maltodextrins than for maltose.

Strain A3 has nearly the same specific affinity for xyloglucan as for amylopectin, despite the lower molecular mass of xyloglucan (200 kDa). The multiple types of monosaccharides and glycosidic linkages in xyloglucan probably complicate its degradation and utilization by strain A3 (56). Nevertheless, the specific affinity of strain A3 for xyloglucan is still significantly higher than for fructose, which promoted growth of strain A3 at $\mu\text{g C liter}^{-1}$ levels, in contrast to eight other individually tested monosaccharides (40). These eight individual monosaccharides were probably not taken up into its cytoplasm, and thus it seems likely that transport across the cytoplasmic membrane controlled the growth of strain A3 with fructose.

The apparently lower specific affinity of strain A3 for lectin than for casein and gelatin may be attributed to the fact that strain A3 cannot utilize the main amino acid constituents in lectin (e.g., aspartate and serine) as a sole energy source, in contrast to some of the main amino acid constituents in casein and/or gelatin (e.g., proline and glutamate) (Table 2). Consequently, it may be more difficult for strain A3 to degrade lectin into oligopeptides from which energy can be obtained. The lowest K_s of strain A3 ($< 2.5 \mu\text{g C liter}^{-1}$) was observed for growth with proline, but the V_{max} of strain A3 with proline (0.019 h^{-1}) was significantly lower than with the other substrates tested.

As mentioned in the first section of this discussion, the growth rates of strain A3 with proline, glutamine, glutamate, or alanine at 10 and $100 \mu\text{g C liter}^{-1}$ were comparable to its growth rate of $0.016 \pm 0.000 \text{ h}^{-1}$ with a mixture of 20 different amino acids ($10 \mu\text{g C liter}^{-1}$ per compound) (40). However, in

the presence of a mixture of 6 carbohydrates (10 $\mu\text{g C liter}^{-1}$ per compound) that promoted the growth of strain A3 at a rate of $0.29 \pm 0.003 \text{ h}^{-1}$, the amino acid mixture was utilized simultaneously with the carbohydrate mixture, indicating that the amino acids may have served as carbon sources (40). These observations suggest that metabolism in the cytoplasm was the rate-determining step in the growth of strain A3 with the aforementioned individual amino acids and the amino acid mixture.

Overall, the kinetic parameters determined in the present study demonstrate that strain A3 has high-affinity, high-capacity utilization systems for polysaccharides and proteins as individual energy sources, and a high-affinity, low-capacity utilization system that saturates at very low substrate concentrations for proline as the energy source.

Yields of *F. johnsoniae* strain A3 with biopolymers. The average cell yield of strain A3 with maltose, laminarin, amylopectin, and xyloglucan was 1.6 times higher at $\leq 10 \mu\text{g C liter}^{-1}$ ($1.47 \times 10^7 \text{ CFU } \mu\text{g}^{-1}$ of C) than at $>10 \mu\text{g C liter}^{-1}$ ($0.91 \times 10^7 \text{ CFU } \mu\text{g}^{-1}$ of C). The cell yields of *Flavobacterium* sp. strain S12 with maltose at $\leq 5 \mu\text{g C liter}^{-1}$ and with maltopentaose and maltohexaose at $\leq 10 \mu\text{g C liter}^{-1}$ were also higher than those obtained at >5 or $10 \mu\text{g C liter}^{-1}$ (45). From the ATP levels measured at the maximum growth level of strain A3 with maltose, laminarin, amylopectin, and xyloglucan (data not shown), the average ATP level cell^{-1} of strain A3 was calculated. The ATP level cell^{-1} was 2.5 times lower at $\leq 10 \mu\text{g C liter}^{-1}$ ($0.061 \pm 0.01 \text{ fg cell}^{-1}$) than at $>10 \mu\text{g C liter}^{-1}$ ($0.16 \pm 0.04 \text{ fg cell}^{-1}$). Thus, the ATP level cell^{-1} had increased more than the cell yield had decreased at $>10 \mu\text{g C liter}^{-1}$. It has been hypothesized that oligotrophic bacteria can release excess substrate C by overflow metabolism to prevent too-high internal carbon concentrations (10, 25). However, to our knowledge, there are no supporting data for this hypothesis and consequently it is unclear whether the higher ATP level cell^{-1} and lower cell yield at $>10 \mu\text{g C liter}^{-1}$ can be attributed to overflow metabolism. Another explanation is that strain A3 formed smaller cells and maintained a more than proportionally lower ATP level cell^{-1} during growth at $\leq 10 \mu\text{g C liter}^{-1}$ than at $>10 \mu\text{g C liter}^{-1}$. The larger surface area-to-volume ratio of small cells should provide strain A3 with a greater ability to compete for substrates in natural aquatic environments, because compounds can diffuse more efficiently into (e.g., nutrients and oxygen) and out of (e.g., waste, extracellular enzymes) the cell (25, 57). The strategy to maintain a lower ATP level cell^{-1} when grown under C-limiting batch conditions has been demonstrated for other heterotrophic bacteria (23).

It has also been reported that heterotrophic bacteria growing with glucose and an excess of nitrogen and phosphorus can accumulate glycogen as an energy reserve, for which additional ATP is required (55). Hence, the higher ATP level cell^{-1} and lower cell yield of strain A3 with maltose, laminarin, amylopectin, and xyloglucan at $>10 \mu\text{g C liter}^{-1}$ may also suggest that a certain amount of carbohydrate was converted into glycogen or another energy reserve. Bacteria generally do not convert proteins into energy reserve polymers (i.e., polysaccharides and lipids) (13), which could explain why strain A3 displayed only one cell yield and one ATP level cell^{-1} with gelatin ($0.086 \pm 0.001 \text{ fg CFU}^{-1}$ at $\leq 10 \mu\text{g C liter}^{-1}$; $0.087 \pm 0.01 \text{ fg CFU}^{-1}$ at $>10 \mu\text{g C liter}^{-1}$). Elucidation of the relation-

ship between substrate concentration and cell properties (e.g., size, ATP content, glycogen content) of strain A3 during growth with polysaccharides or proteins would have required research beyond the scope of our study.

Biopolymer utilization in the oligotrophic freshwater environment. It has been suggested that growth kinetics of oligotrophic bacteria should be assessed under mixed-substrate conditions, because natural oligotrophic environments contain complex mixtures of compounds (16, 27). Indeed, heterotrophic bacteria can utilize multiple LMW energy and carbon sources simultaneously and at lower threshold concentrations than during growth with single substrates (21, 27, 29). Furthermore, a variety of heterotrophic bacteria (including strain A3) can utilize LMW organic compounds that individually do not serve as the energy source when growth-promoting organic compounds are present (40, 47, 50, 52). The growth kinetic parameters of strain A3 with biopolymers have been determined only in the presence of a few $\mu\text{g liter}^{-1}$ of indigenous substrates in the blank and not in the presence of other added substrates. Nevertheless, the specific affinities obtained for strain A3 under these conditions still clearly demonstrate that strain A3 is highly proficient in the utilization of biopolymers under (ultra)oligotrophic conditions. The results of our study prove that biopolymers promote the growth of heterotrophic bacteria at a few $\mu\text{g C liter}^{-1}$ in (ultra)oligotrophic freshwater environments and that strain A3 is a suitable model organism to study the bacterial utilization of biopolymers at low concentrations in these environments.

Strain A3 can also take up amino acids with high affinity at $\mu\text{g C liter}^{-1}$ levels, but representatives of *Pseudomonas*, *Aeromonas*, and *Klebsiella* species have this ability as well (46, 50–52). Apparently, amino acid utilization at low concentrations is relatively common among oligotrophic freshwater bacteria. Biopolymer utilization in oligotrophic freshwater environments, however, seems to be dominated by *Cytophagia-Flavobacteria* (20, 24, 40). The high specific affinities of strain A3 for different biopolymers confirm that some planktonic *Cytophagia-Flavobacteria* are highly adapted to growth with these compounds at $\mu\text{g liter}^{-1}$ levels and support the hypothesis that *Cytophagia-Flavobacteria* play an important role in the degradation of biopolymers in (ultra)oligotrophic freshwater environments (24). Assessment of the role of attached heterotrophic bacteria in the degradation of biopolymers in these environments requires further investigation.

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