Endo-exo Synergism in Cellulose Hydrolysis Revisited*5

Received for publication, May 14, 2012, and in revised form, June 22, 2012 Published, JBC Papers in Press, June 25, 2012, DOI 10.1074/jbc.M112.381624

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Background: Synergism between enzymes is a prerequisite for the efficient degradation of cellulose, but its molecular mechanisms are not fully understood.

Results: Endoglucanase increased the rate constant of cellobiohydrolase-catalyzed cellulose hydrolysis.

Conclusion: A mechanism whereby endoglucanase avoids the stalling of processive cellobiohydrolase is proposed.

Significance: Understanding the mechanisms of synergism helps to design more efficient enzyme mixtures for cellulose degradation.

Synergistic cooperation of different enzymes is a prerequisite for efficient degradation of cellulose. The conventional mechanistic interpretation of the synergism between randomly acting endoglucanases (EGs) and chain end-specific processive cellobiohydrolases (CBHs) is that EG-generated new chain ends on cellulose surface serve as starting points for CBHs. Here we studied the hydrolysis of bacterial cellulose (BC) by CBH TrCel7A and EG TrCel5A from Trichoderma reesei under both single-turnover and "steady state" conditions. Unaccountable by conventional interpretation, the presence of EG increased the rate constant of TrCel7A-catalyzed hydrolysis of BC in steady state. At optimal enzyme/substrate ratios, the "steady state" rate of synergistic hydrolysis became limited by the velocity of processive movement of TrCel7A on BC. A processivity value of 66 \pm 7 cellobiose units measured for *Tr*Cel7A on ¹⁴Clabeled BC was close to the leveling off degree of polymerization of BC, suggesting that TrCel7A cannot pass through the amorphous regions on BC and stalls. We propose a mechanism of endo-exo synergism whereby the degradation of amorphous regions by EG avoids the stalling of TrCel7A and leads to its accelerated recruitment. Hydrolysis of pretreated wheat straw suggested that this mechanism of synergism is operative also in the degradation of lignocellulose. Although both mechanisms of synergism are used in parallel, the contribution of conventional mechanism is significant only at high enzyme/substrate ratios.

Cellulose is the most abundant biopolymer on Earth and has great potential as a renewable energy source (1). Cellulose is the main component of plant cell walls, but it is also produced by some animals and microorganisms like bacteria and algae. Cellulose consists of linear chains of anhydroglucose units linked through β -1-4 glycosidic bonds. Degree of polymerization (DP)² in native celluloses ranges from a few thousand to tens of



EG Cel5A from *T. reesei*; CD_{*TrC*el7A}, catalytic domain of *Tr*Cel7A; DSE, degree of synergistic effect; EG, endoglucanase; MU, 4-methylumbelliferone; MUL, 4-methylumbelliferyl- β -lactoside; pNP, *para*-nitrophenol; pNPL, *para*-nitrophenol- β -lactoside.



^{*} This work was supported by the European Union Commission (FP7/2007– 2013, Grant 213139) and Estonian Science Foundation (Grant 9227).

This article contains supplemental Tables S1–S6, Figs. S1–S3, and Equation S1.

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² The abbreviations used are: DP, degree of polymerization; AC, amorphous cellulose; BC, bacterial cellulose; CB, cellobiose; ¹⁴CB, ¹⁴C-labeled cellobiose; ¹⁴C-BC, ¹⁴C-labeled bacterial cellulose; CBH, cellobiohydrolase; CBM, carbohydrate binding module; *Tr*CeI7A, CBH CeI7A from *T. reesei*; *Tr*CeI5A,

cient in degradation of crystalline cellulose, whereas EGs preferentially target less ordered amorphous regions.

Synergistic cooperation between cellulases is a prerequisite for efficient degradation of cellulose (18, 19). The first mechanistic explanation of synergism was put forward by Reese et al. (20) more than 50 years ago. The first, unknown component (C_1) was supposed to carry out so-called amorphogenesis of crystalline cellulose, exposing single cellulose chains and cellooligosaccharides that were then degraded by the C_x component, identified as EG (20). Although numerous non-hydrolytic proteins that can induce amorphogenesis and act synergistically with cellulases have been identified (21), their contribution to lignocellulose degradation remains elusive. After discovery of CBHs (referred to as C_1 for some time) (22, 23), the mechanistic explanation of endo-exo synergy was put forward, whereby randomly acting EG generates new chain ends on cellulose that serve as starting points for processive CBHs (24). Although alternative explanations like removal of obstacles by EG (surface "cleaning") to aid the processive movement of CBH have also been proposed (25, 26), the conventional "starting point generation" mechanism is still the most widely accepted one. Synergistic action has been shown to be reciprocal, meaning that not only does CBH benefit from the action of EG, but also the action of CBH renders the substrate more accessible to EG (25, 27). Synergism between two CBHs (exo-exo synergism) has also been reported (28-32). Because one of the CBH components has been proposed to employ also the endo-mode of initiation (endo-processive CBH), the mechanistic interpretation of the conventional endo-exo synergism was adopted (30-32). Recently, a new type of synergism between enzymes that employ oxidative chemistry to break glycosidic bonds and hydrolytic enzymes was reported in chitin degradation (33). The enigmatic synergism between non-hydrolytic glycoside hydrolase family 61 proteins and cellulases has since found a mechanistic interpretation (34-37). This has lead to the resurgence of C_1 - C_x theory with the oxidative enzyme identified as C_1 (19, 35, 38). To make it all more complex and challenging, Gao et al. (39) demonstrated that synergism was dependent on the glycosylation pattern of CBH.

For the quantitative description of synergism, the degree of synergistic effect (DSE) is often used. DSE is the ratio of the activity of synergistic mixture to the sum of the activities of individual components. Besides the nature of synergistic components, DSE has also been shown to depend on the molar ratio of the components (31, 40); surface density of bound cellulases (30, 41, 42); and properties of cellulose like DP (25, 43), crystallinity (44), and allomorph composition (45). Because cellulose properties can change with hydrolysis, the dependence of DSE on hydrolysis time has also been reported (25, 31, 46). Usually, a small molar fraction (a few percent) of EG results in the highest DSE (31, 40), but the optimal fraction of EG depends on the nature of the EG as well as the substrate used (25, 31). Data on the effect of the surface density of bound enzymes on DSE are controversial. Some studies have shown that DSE is highest in the case of low surface coverage (41), whereas others support the importance of proximity (*i.e.* high surface density) of synergistic components (30, 42, 47, 48). Among cellulose substrates, the highest DSE is observed on substrates with high DP and

intermediate crystallinity (45) like filter paper or bacterial cellulose (BC), whereas low or moderate DSE is observed on highly crystalline substrates (25, 46, 49). All of these findings indicate that endo-exo synergism is far more complex than appears from the conventional, "starting point generation" mechanism.

Here we studied the hydrolysis of BC by CBH *Tr*Cel7A and EG *Tr*Cel5A under both single-turnover and "steady state" conditions. EG was found to increase the rate constant of CBH-catalyzed cellulose hydrolysis in "steady state." A mechanism of endo-exo synergism is proposed, whereby the degradation of amorphous regions of BC by EG avoids the stalling of processive CBH and leads to its accelerated recruitment.

EXPERIMENTAL PROCEDURES

Materials—Glucose, cellobiose, 4-methylumbelliferyl- β -lactoside (MUL), *para*-nitrophenyl- β -lactoside (pNPL), bovine serum albumin (BSA), and papain were purchased from Sigma-Aldrich. D-U-¹⁴C-Labeled glucose with a specific activity of 262 mCi/mmol was from Hartmann Analytic GmbH. Scintillation mixture was from Merck. All chemicals were used as purchased.

Enzymes—*Tr*Cel7A and *Tr*Cel5A were purified from the culture filtrate of *T. reesei* QM 9414 as described previously (50, 51). Catalytic domain of *Tr*Cel7A (CD_{*Tr*Cel7A}) was prepared by limited proteolysis of intact *Tr*Cel7A with papain according to Ref. 10. *Aspergillus* β -glucosidase was purified from Novozyme[®] 188 (C6105, Sigma) as described before (52). Enzyme concentration was determined from absorbance at 280 nm using molar extinction coefficients of 84,400, 78,000, 78,250, and 180,000 M⁻¹ cm⁻¹ for *Tr*Cel7A, *Tr*Cel5A, CD_{*Tr*Cel7A}, and β -glucosidase, respectively.

Celluloses-BC was prepared by laboratory fermentation of the Gluconobacter xylinum strain ATCC 53582 as described (53). ¹⁴C-Labeled bacterial cellulose (¹⁴C-BC) was prepared as BC, but the glucose carbon source was supplemented with ¹⁴Cglucose. In the case of ¹⁴C-BC, the cultivation flasks were also provided with a CO₂ trap, and O₂ was supplied by slowly pumping the air through the culture medium. ¹⁴C-BC had a specific activity of 450,000 dpm/mg. Amorphous cellulose (AC) was prepared from Avicel according to Ref. 53. The total concentration of cellulose was determined by the anthrone sulfuric acid method. Pretreated wheat straw (hereafter referred to as lignocellulose) was from Inbicon (Skærbæk, Denmark). Hydrothermal pretreatment of wheat straw was performed in the Inbicon IBUS pilot plant (54). Glucan, Klason lignin, xylan, and ash content of lignocellulose on a dry weight basis was 58.5, 26.4, 5.3, and 2.6%, respectively. For purification and handling of lignocellulose, see Ref. 55.

Hydrolysis of Cellulose under Single-turnover Conditions— Experiments were performed in 50 mM sodium acetate buffer, pH 5.0, containing BSA (0.1 mg ml⁻¹) at 25 °C. Cellulases (supplemented with 0.12 μ M β -glucosidase) were mixed with uniformly ¹⁴C-labeled bacterial cellulose (¹⁴C-BC, 0.5 mg ml⁻¹) to start the hydrolysis. At the selected time, an equal volume of non-labeled AC (10 mg ml⁻¹) was added to trap all unbound cellulases. Under these conditions, each bound cellulase was allowed to perform only a single processive run on ¹⁴C-BC. For time points, 0.2-ml aliquots were withdrawn and added to 20 μ l



of 1 M NaOH to stop the reaction. After separation of cellulose by centrifugation, the radioactivity in the supernatant was quantified using a liquid scintillation counter. For the background measurements ("leakage" of trap), separate experiments were performed where AC was added to ¹⁴C-BC before cellulases. Because of the dynamic exchange between cellulases bound to ¹⁴C-BC and the AC trap, there will always be a small number of attacks on ¹⁴C-BC after the addition of an AC trap. This is represented by the leakage of trap, and all hydrolysis data were corrected for the corresponding leakage (56). The magnitude of leakage was dependent on the concentration and composition of the enzyme mixture, but in most cases it remained within 10% of the radioactivity reading of the corresponding hydrolysis experiments. In the experiments performed in the presence of EG, the radioactivity released by EG for the moment of the trap addition (no detectable release of radioactivity by EG was observed after the AC trap addition) was also subtracted. Thus, the data represent the radioactivity released by CBH.

Determination of [ES]_{trap}—The concentration of cellulasecellulose complex at the moment of the trap addition $([ES]_{trap})$ was measured by quantification of the inhibition of the hydrolysis of MUL by BC (56). For that, BC (0.5 mg ml⁻¹) was incubated with cellulases in the presence of 5 μ M MUL in 50 mM sodium acetate buffer, pH 5.0, containing BSA (0.1 mg ml) at 25 °C. Reactions were supplemented with 0.85 μ M β -glucosidase to avoid the inhibition of MUL hydrolysis by cellobiose released from BC. Hydrolysis was stopped by the addition of an equal volume of 0.2 M ammonium hydroxide. After separation of cellulose by centrifugation, the released 4-methylumbelliferone (MU) was guantified from the fluorescence of the supernatant. Excitation and emission wavelengths were set to 360 and 450 nm, respectively. The concentration of the population of TrCel7A with the free active site (*i.e.* free to hydrolyze MUL; $[TrCel7A]_{FA}$) was found from the calibration curves of MUL hydrolysis made in the absence of cellulose. [ES]_{trap} was found as the difference of total concentration of TrCel7A $([TrCel7A]_{Total})$ and $[TrCel7A]_{FA}$ (56).

Hydrolysis of Cellulose under "Steady State" Conditions-All experiments were performed in 50 mM sodium acetate buffer, pH 5.0, containing BSA (0.1 mg ml $^{-1})$ and β -glucosidase (0.85 μ M) at 25 °C. BC (0.1–2.5 mg ml $^{-1}$) was incubated with 0.5 μ M TrCel7A or $CD_{TrCel7A}$. If present, the concentration of EG (TrCel5A) was 0.1 µm. At selected times (between 1 and 30 min), 0.45-ml aliquots were withdrawn and added to 5 μ l of 10 mм MUL. After 30 s, 0.45 ml of 0.2 м ammonium hydroxide was added to stop the reaction. Cellulose was separated by centrifugation, and the concentration of MU was found from the fluorescence of the supernatant. After fluorescence measurements, 0.105 ml of 1 M acetic acid was added to 0.8 ml of supernatant, and the concentration of glucose was measured using a glucose oxidase peroxidase assay as described (55). Zero data points were treated identically, but the enzymes were added after ammonium hydroxide. [TrCel7A]_{FA} was found from the released [MU] using calibration curves of MUL hydrolysis made in the absence of cellulose. The concentration of TrCel7A with the active site occupied by the cellulose chain $([TrCel7A]_{OA})$ was found from the difference $[TrCel7A]_{OA} = [TrCel7A]_{Total} - [TrCel7A]_{FA}$.

In the case of lignocellulose, lignocellulose $(1.0-10 \text{ mg ml}^{-1})$ dry matter) was incubated (shaking at 500 rpm) with 2.5 μ M TrCel7A or CD_{TrCel7A} in the presence of 0.5 mM pNPL. If present, the concentration of EG (TrCel5A) was 0.25 μ M. After 30 min of hydrolysis, the reaction mixtures were rapidly pressed through a glass fiber filter (GF/D from Whatman) mounted to a 1-ml syringe. The filtrate was centrifuged (1 min, 10,000 \times g), and 0.4 ml of supernatant was added to 0.4 ml of 0.2 M ammonium hydroxide. Released para-nitrophenol (pNP) was quantified from the absorbance at 414 nm. $[TrCel7A]_{FA}$ ($[TrCel7A]_{OA}$ = [*Tr*Cel7A]_{Total} – [*Tr*Cel7A]_{FA}) was found from [pNP] using the calibration curves of pNPL hydrolysis made in the absence of cellulose. After absorbance measurements, 0.105 ml of 1 M acetic acid was added to 0.8 ml of supernatant, and the concentration of glucose was measured using the hexokinase assay as described (55). Control experiments without pNPL were run in parallel to account for the background absorbance from lignocellulose. Zero data points were treated identically, but the enzymes were added after ammonium hydroxide.

Determination of the Values of the Observed Rate Constant (k_{obs}) —This was performed essentially as described (55). The time courses of glucose formation in hydrolysis of BC under "steady state" conditions were first converted to the rates of glucose formation. For that, the hydrolysis data were fitted to an empirical function that explicitly and without systematic deviation described the data. Rates of glucose formation were calculated using the values of parameters obtained from the above mentioned fitting of the data and the first order derivative of the rates of cellobiose formation (taken as a half of the corresponding rate of glucose formation) and $[TrCel7A]_{OA}$ according to Equation 6. Values of $[TrCel7A]_{OA}$ were found from the inhibition of the hydrolysis of MUL by BC.

In the case of lignocellulose substrate, average velocities after 30 min of hydrolysis were used to calculate $k_{\rm obs}$ values. Here the $[TrCel7A]_{OA}$ values were found from the inhibition of the hydrolysis of pNPL by lignocellulose.

Determination of the DSE in Hydrolysis of Cellulose—The values of DSE were found at three different levels. (i) DSE at the level of glucose formation (DSE_{Glc}) represents the ratio of glucose produced by the mixture of *Tr*Cel7A and *Tr*Cel5A to glucose produced by individual *Tr*Cel7A. Low levels of glucose produced by individual *Tr*Cel7A, Low levels of glucose produced by individual *Tr*Cel7A are not accounted for in calculating DSE_{Glc}. (ii) DSE at the level of [*Tr*Cel7A]_{OA} (DSE_{OA}) represents the ratio of [*Tr*Cel7A]_{OA} measured for the mixture of *Tr*Cel7A. (iii) DSE at the level of *k*_{obs} (DSE_k) represents the ratio of *k*_{obs} measured for the mixture of *Tr*Cel7A and *Tr*Cel5A to *k*_{obs} measured for individual *Tr*Cel7A.

Inhibition of TrCel7A by Cellobiose—All experiments were performed in 50 mM sodium acetate buffer, pH 5.0, containing BSA (0.1 mg ml⁻¹) at 25 °C. In the case of the single-turnover approach ¹⁴C-BC (0.5 mg ml⁻¹) was incubated with 1.0 μ M TrCel7A in the presence of added cellobiose (0–20 mM). If present, the concentration of TrCel5A was 0.1 μ M. Series made without added cellobiose were provided with 0.125 μ M β -glu-

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FIGURE 1. **Hydrolysis of** ¹⁴**C-BC by** *Tr***Cel7A under single-turnover conditions.** *A*, ¹⁴C-BC (0.5 mg ml⁻¹) was incubated with 1.0 μ M *Tr*Cel7A. An AC trap was added after 10 s (\Box), 30 s (\diamond), or 60 s (\bigtriangleup) of hydrolysis, and the release of ¹⁴CB in time was followed. *B*, [*Tr*Cel7A]_{OA} was measured from the inhibition of the hydrolysis of MUL by BC (0.5 mg ml⁻¹). [*Tr*Cel7A] was 0.1 μ M (\bigcirc), 0.25 μ M (\diamond), or 1.0 μ M (\square). *Solid lines* are from the non-linear regression according to Equation 2. C, data from *A* divided by the corresponding concentration of *Tr*Cel7A at the moment of the AC trap addition ([*ES*]_{trap}). Values of [*ES*]_{trap} were taken from *B* using an assumption that [*ES*]_{trap} = [*Tr*Cel7A]_{OA}. *D*, average [¹⁴CB]/[*ES*]_{trap} ratios over experiments with different *Tr*Cel7A contentrations and different times of trap addition. Shown is non-linear regression according to the single exponent (Equation 3; *dotted line*) or to the sum of two exponents (Equation 4; *solid line*). The *dashed line* and the *dashed and dotted line* represent the fast and slow components of Equation 4, respectively. *Error bars* show S.D. and are from at least three independent measurements.

cosidase. The AC trap was added after 10 or 30 s from the initiation of the hydrolysis of ¹⁴C-BC for the series made with or without the presence of *Tr*Cel5A, respectively. Suspensions of AC were also supplemented with cellobiose at appropriate concentrations.

To study the cellobiose inhibition of *Tr*Cel7A in "steady state," the hydrolysis of ¹⁴C-BC (0.25 mg ml⁻¹) by *Tr*Cel7A (0.25 μ M) in the presence of added cellobiose was followed. If present, the concentration of *Tr*Cel5A was 0.025 μ M. Series without added cellobiose were provided with 0.125 μ M β -glucosidase. Hydrolysis was started with the addition of enzymes, and at selected times, 0.2-ml aliquots were withdrawn and added to 20 μ l of 1 M NaOH to stop the reaction. After separation of cellulose by centrifugation, the radioactivity in the supernatant was quantified using a liquid scintillation counter. In making zero time points, NaOH was added to ¹⁴C-BC before enzymes.

RESULTS

Hydrolysis of Cellulose under Single-turnover Conditions— Recently, we described a method for the measurement of the apparent processivity ($P_{\rm app}$) of CBHs under single-turnover conditions (56). The method relies on the hydrolysis of uniformly ¹⁴C-labeled bacterial cellulose (¹⁴C-BC). Cellulases are mixed with ¹⁴C-BC to start the hydrolysis, and after a short interval, an excess of non-labeled AC is added to trap all unbound cellulases. Under these conditions, each bound cellulase is allowed to perform only a single processive run on ^{14}C -BC. The time course of the formation of ^{14}C -cellobiose (^{14}CB) should follow the exponent in the form,

$$\begin{bmatrix} {}^{14}\text{CB} \end{bmatrix} = \begin{bmatrix} {}^{14}\text{CB} \end{bmatrix}_{\max} (1 - e^{-kt})$$
(Eq. 1)

where $[^{14}CB]_{max}$ is the leveling off value of $[^{14}CB]$, and *k* is the pseudo first order rate constant for passing through one processive run. The value of [¹⁴CB]_{max} depends on (i) the concentration of productive cellulase-cellulose complexes at the moment of the trap addition ([ES]_{trap}) and (ii) an average number of cellobiose units released during a single run (*i.e.* the P_{app} of cellulase) (56). To meet single-turnover conditions, the trap must be added before the enzyme has dissociated after completion of a processive run. Fig. 1A shows the release of ¹⁴C-cellobiose in hydrolysis of ¹⁴C-BC by TrCel7A with different times of the addition of trap. Hydrolysis data were fitted to Equation 1 to obtain $[{}^{14}CB]_{max}$ and k values. Higher $[{}^{14}CB]_{max}$ values were observed with increasing the time of the trap addition, whereas the values of k were unaffected (supplemental Table S1). The increase in $\left[^{14}\text{CB}\right]_{max}$ values with increasing time of the trap addition can be a result of repeated initiations and/or an increased number of first initiations (higher $[ES]_{trap}$). In the latter case, P_{app} should be independent of the time of the trap addition, whereas in the former case, $P_{\rm app}$ is expected to increase with increasing time of the trap addition. To find $P_{\rm app}$ from the value of $[^{14}CB]_{max}$, the value of $[ES]_{trap}$ must be avail-





FIGURE 2. Synergism in hydrolysis of ¹⁴C-BC by *TrCeI7A* and EG *TrCeI5A* under single-turnover conditions. \diamond , *TrCeI7A*; \blacklozenge , *TrCeI7A* + EG; \triangle , CD_{*TrCeI7A*; \blacklozenge , CD_{*TrCeI7A*} + EG. Concentration of *TrCeI7A* or CD_{*TrCeI7A*} was 1.0 μ M. If present, the concentration of EG (*TrCeI5A*) was 0.1 μ M. *A*, release of ¹⁴CB in hydrolysis of ¹⁴C-BC (0.5 mg ml⁻¹). AC trap was added after 10 s of hydrolysis. *B*, concentration of *TrCeI7A* with the active site occupied by the cellulose chain ([*TrCeI7A*]_{OA}) was measured from the inhibition of the hydrolysis of MUL by BC (0.5 mg ml⁻¹). *Solid lines* are from the non-linear regression according to Equation 2. *Error bars* show S.D. and are from at least three independent measurements.}

able. For TrCel7A, a recently developed method for the quantification of the TrCel7A population with the active site occupied by the cellulose chain ($[TrCel7A]_{OA}$) can be applied to find the values of $[ES]_{trap}$ (55, 56). Assuming that initial binding through the active site is productive, we can use [TrCel7A]_{OA} to account for $[ES]_{trap}$. Although this seems a plausible assumption for TrCel7A in the early stage of the reaction (first 30 s) (55), it cannot be generalized. This is the reason for the mixed use of the terms [ES]_{trap} and [TrCel7A]_{OA} here. Whereas [ES]_{trap} is the correct term to appear in the equations, the use of $[TrCel7A]_{OA}$ to account for $[ES]_{trap}$ assumes that all complexes that prevent the hydrolysis of MUL are productive cellulase cellulose complexes. Fig. 1B shows the build-up of $[TrCel7A]_{OA}$ in time measured using the hydrolysis of MUL as a reporter reaction. Binding kinetics was consistent with a simple exponential function (solid lines in Figs. 1B and 2B),

$$[TrCeI7A]_{OA} = [TrCeI7A]_{OA-max}(1 - e^{-k_{ON(obs)}t})$$
(Eq. 2)

where $[TrCel7A]_{OA-max}$ is the plateau value of TrCel7A bound to BC via the active site, and $k_{on(obs)}$ is the pseudo first order rate constant for binding that depends on cellulose concentration. Transit times for binding $(1/k_{on(obs)})$ measured at a BC concentration of 0.5 mg ml⁻¹ were between 5 and 10 s. For the values of $[TrCel7A]_{OA-max}$ and $k_{on(obs)}$ at different TrCel7A concentrations, see supplemental Table S2. Provided with $[ES]_{trap}$, Equation 1 can now be expressed in the following form.

$$\frac{[{}^{14}\text{CB}]}{[ES]_{trap}} = \frac{[{}^{14}\text{CB}]_{max}}{[ES]_{trap}} (1 - e^{-kt}) = P_{app}(1 - e^{-kt}) \quad (Eq. 3)$$

After dividing the released [¹⁴CB] with corresponding $[ES]_{trap}$, all curves made with different times of the trap addition merge (Fig. 1*C*) and result in the same P_{app} value within the error limits (supplemental Table S1). This confirms that the number of repeated initiations was not significant within the studied conditions. Increasing the concentration of *Tr*Cel7A resulted in increased [¹⁴CB]_{max}, but the P_{app} was independent of [*Tr*Cel7A] (supplemental Fig. S1 and Table S1). However, obvious systematic deviation was observed in fitting the data (up to 1800 s) to Equation 3 (Fig. 1*D*), and an equation consisting of a sum of two exponents was necessary to fit the data (Equation 4),

$$\frac{\begin{bmatrix}1^{4}\mathsf{C}\mathsf{B}\end{bmatrix}}{[\mathsf{E}\mathsf{S}]_{\mathsf{trap}}} = \left(\frac{\begin{bmatrix}1^{4}\mathsf{C}\mathsf{B}\end{bmatrix}_{\mathsf{max}}}{[\mathsf{E}\mathsf{S}]_{\mathsf{trap}}}\right)_{1}(1 - e^{-k_{1}t}) + \left(\frac{\begin{bmatrix}1^{4}\mathsf{C}\mathsf{B}\end{bmatrix}_{\mathsf{max}}}{[\mathsf{E}\mathsf{S}]_{\mathsf{trap}}}\right)_{2}(1 - e^{-k_{2}t})$$
(Eq. 4)

where subscripts 1 and 2 denote the parameters for the first and the second exponent, respectively. The second exponent had an about 10-fold longer transit time and smaller amplitude than the first exponent (Fig. 1*D*). We propose that the second exponent represents the small population of enzymes that progress with higher $P_{\rm app}$. Another possibility is that the two populations have the same $P_{\rm app}$ but different velocity of the processive movement. Because $[TrCel7A]_{OA}$ accounts only for total $[ES]_{\rm trap}$, it is not possible to discriminate between these two possibilities experimentally. Therefore, we further focused on the first 180 s of the time course where the systematic deviation from Equation 3 was negligible. Combining the data obtained using different times of the trap addition and different TrCel7A concentrations (supplemental Table S1) resulted in an average $P_{\rm app}$ value of 66 \pm 7 (Table 1).

The rate constant k in Equations 1 and 3 is related to the catalytic constant (k_{cat}) that represents the rate constant leading from one productive complex through catalytic events to another productive complex 1 cellobiose unit further on the cellulose chain according to Equation 5,

$$k = \frac{k_{\text{cat}}}{P_{\text{app}}} = \frac{k_{\text{cat}}}{n_{\text{free}}} + \frac{k_{\text{cat}}}{\text{DP}} + k_{\text{off}}$$
(Eq. 5)

where $n_{\rm free}$ is the average length of the obstacle-free path (in cellobiose units) on cellulose (55), DP is the degree of polymerization of cellulose (in cellobiose units), and $k_{\rm off}$ is the dissociation rate constant of *Tr*Cel7A from cellulose (s⁻¹). $k_{\rm off}$ is related to $k_{\rm cat}$ and intrinsic processivity ($P_{\rm Intr}$) according to $k_{\rm off} = k_{\rm cat}/(P_{\rm Intr} - 1)$ (57). Depending of the values of $n_{\rm free}$, DP, and $P_{\rm Intr}$, the value of $P_{\rm app}$ may be governed by the properties of the substrate (low $n_{\rm free}$ or DP) or the properties of the enzyme (low $P_{\rm Intr}$, *i.e.* high $k_{\rm off}$). An average DP of ¹⁴C-BC is around 1000 cellobiose units. In our previous study, we have estimated a $P_{\rm Intr}$ value of 4000 \pm 570 cellobiose units ($k_{\rm off}$ value of 0.0007 \pm 0.0001 s⁻¹) for *Tr*Cel7A on reduced BC and proposed that $P_{\rm app}$



TABLE 1
Values of kinetic parameters for <i>Tr</i> Cel7A from single-turnover experiments

Enzyme(s) ^a	$\begin{bmatrix} {}^{14}\text{CB} \end{bmatrix}_{\max}^{b}$	$[ES]_{trap}^{c}$	$P_{\rm app}^{\ \ d}$	k ^b	$k_{\rm cat}^{\ e}$		
	μ_M	μ_M	CB units	s^{-1}	s ⁻¹		
TrCel7A	15 ± 2	0.22 ± 0.10	66 ± 7^{f}	0.033 ± 0.006^{f}	2.2 ± 0.5^{f}		
TrCel7A + EG	34 ± 2	0.67 ± 0.01	50 ± 3	0.030 ± 0.005	1.5 ± 0.2		
CD _{TrCel7A}	4.9 ± 0.5			0.089 ± 0.05			
$CD_{TrCel7A} + EG$	11 ± 2	0.28 ± 0.02	40 ± 6	0.031 ± 0.025	1.2 ± 0.4		
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^{*a*} Experimental conditions were as follows: [¹⁴C-BC] = 0.5 mg ml⁻¹, [*Tr*Cel7A] or [CD_{*Tr*Cel7A}] = 1.0 μ M, [β -glucosidase] = 0.125 μ M, 25 °C, pH 5.0. If present, the concentration of tration of EG (TrCel5A) was 0.1 µm. An AC trap was added after 10 s of hydrolysis.

 b Values of $[^{14}CB]_{max}$ and k were found by non-linear regression of $[^{14}C$ -cellobiose] released under single-turnover conditions according to Equation 1.

 c Concentration of TrCel7A at the moment of trap addition ([ES]_{trap}) represents the population of TrCel7A with the active site occupied by the cellulose chain ([TrCel7A]_{OA}) after 10 s of hydrolysis

^d Apparent processivity of TrCel7A ($P_{app'}$ in cellobiose units) was found from the values of $[^{14}CB]_{max}$ and $[ES]_{trap}$ according to Equation 3. ^e The value of k_{cat} was found from the values of k and P_{app} according to Equation 5. ^f These values are averages over values obtained at different TrCel7A concentrations and at different times of trap addition (supplemental Table S1).

was limited by $n_{\rm free}$ (57). The results presented here are in accord with this. Combining the values of $k (0.033 \pm 0.006 \text{ s}^{-1})$ and P_{app} (66 ± 7) resulted in a k_{cat} value of 2.2 ± 0.5 s⁻¹ for TrCel7Å on ¹⁴C-BC (Table 1). This value is well in line with earlier estimates of k_{cat} derived either from the rate measurements (57-60) or direct observations of the processive movement of TrCel7A along the cellulose chain (32, 61). Using the rate measurements over the period of 1-3 h, Fox et al. (62) concluded that the steady state rate of the hydrolysis is limited by the slow complex formation between BC and Cel7A from Trichoderma longibrachiatum. However, cellulose hydrolysis is more complicated because it displays burst kinetics where the steady state is preceded by the transient burst of activity (59, 60, 63, 64). As a result of the burst kinetics, the values of observed rate constants are primarily dependent on the measurement period (60, 64). Recent pre-steady state measurements of the activity of TrCel7A on cellulose demonstrated that the rates must be measured within first few s of hydrolysis to reveal the $k_{\rm cat}$ value (60). Because of the specific reaction conditions, a single-turnover approach employed here allows us to measure $k_{\rm cat}$ values without the need of a special apparatus for transient kinetics.

The performance of CD_{TrCel7A}, the truncated form of TrCel7A that lacks CBM, was also tested under single-turnover conditions. CD_{TrCel7A} displayed an about 3-fold lower $[^{14}CB]_{max}$ than intact *Tr*Cel7A (Fig. 2 and Table 1). The low $[^{14}CB]_{max}$ value resulted in a large uncertainty in the estimate of k for CD_{TrCel7A} (Table 1). Because of the low level of binding, we were not able to measure the $[ES]_{trap}$ value and, therefore, also $P_{\rm app}$ and $k_{\rm cat}$ values for CD_{TrCel7A}.

Synergism between Endoglucanase and Cellobiohydrolase-First we studied the effect of EG on the performance of TrCel7A under single-turnover conditions. Supplementation of 1.0 μ M *Tr*Cel7A with 0.1 μ M EG *Tr*Cel5A resulted in an about 2-fold increase in $[^{14}CB]_{max}$, whereas the value of k remained unaffected (Fig. 2 and Table 1). Because TrCel5A has no MUL hydrolyzing activity, $[TrCel7A]_{OA}$ and hence $[ES]_{trap}$ can be measured also in the presence of TrCel5A. EG resulted in an about 3-fold increase in $[ES]_{trap}$. Because the increase in $[ES]_{trap}$ exceeded the increase in $[^{14}CB]_{max}$, somewhat lower P_{app} and k_{cat} values were observed in the presence of EG (Table 1). The addition of EG promoted the binding of CD_{TrCel7A} to the level that allowed the quantification of $[ES]_{trap}$, P_{app} , and k_{cat} also for $CD_{TrCel7A}$ (Fig. 2 and Table 1).

If the AC trap is omitted, "steady state" is established in hydrolysis of BC by TrCel7A (Fig. 3A). Note that in most parts of this study, we use the term "steady state" merely to distinguish between experimental conditions (*i.e.* "steady state" versus single-turnover conditions). The term is enclosed in quotation marks to indicate this use. The addition of 0.1 μ M TrCel5A to 0.5 μ M TrCel7A resulted in an about 8-fold increase in the "steady state" rate of hydrolysis. A synergistic effect between TrCel5A and CD_{TrCel7A} was also evident, but the activity of the $CD_{TrCel7A}$ -containing mixture was far lower (Fig. 3A). In the case of individual enzymes, about 70 and 20% of TrCel7A and $CD_{TrCel7A}$, respectively, were bound via the active site, and these values were fairly constant in time (Fig. 3B). Somewhat higher [TrCel7A]_{OA} values were observed in the presence of EG. The situation was more complicated with synergistic mixture containing $CD_{TrCel7A}$. In this case, an initial increase in $[CD_{TrCel7A}]_{OA}$ was followed by its rapid decrease, and after 30 min of hydrolysis, the amount of $\mathrm{CD}_{\mathit{TrCel7A}}$ bound through the active site was negligible (Fig. 3B). Provided with the rate of cellobiose formation (v_{CB}) and [*Tr*Cel7A]_{OA}, one can calculate the value of the observed rate constant for cellulose hydrolysis $(k_{\rm obs})$ using Equation 6 (55).

$$k_{\rm obs} = \frac{v_{\rm CB}}{[Tr {\rm Cel7A}]_{\rm OA}}$$
(Eq. 6)

Note that although the experiments were performed in the presence of excess β -glucosidase activity and the formation of glucose was measured, it is more appropriate to express the rates and $k_{\rm obs}$ values on the basis of cellobiose formation, which is the main product of the TrCel7A-catalyzed hydrolysis of cellulose. As seen in Fig. 3C, the presence of EG caused a significant increase in $k_{\rm obs}$ values in the case of both $Tr{\rm Cel7A}$ and CD_{TrCel7A}.

All of the measurements described above (Fig. 3, A-C) were performed at a BC concentration of 0.5 mg ml^{-1} . Because the synergistic hydrolysis of BC is inhibited by the substrate (42), we next measured $[TrCel7A]_{OA}$ and k_{obs} values at different BC concentrations. At the level of glucose formation, the substrate inhibition was revealed only in the case of a synergistic mixture containing intact TrCel7A (Fig. 3D). Although TrCel7A clearly outperformed CD_{TrCel7A} at low [BC] values, their activities were the same at the highest [BC] tested (Fig. 3D). Plotting [*Tr*Cel7A]_{OA} as a function of [BC] demonstrates higher binding





FIGURE 3. Synergism in hydrolysis of BC by *TrCel7A* and EG *TrCel5A*. *TrC*el7A (\Diamond), *TrC*el7A + EG (\blacklozenge), CD_{*TrCel7A*} (\triangle), CD_{*TrCel7A*} + EG (\blacklozenge). Concentration of *TrCel7A* or CD_{*TrCel7A*} was 0.5 μ M, and that of β -glucosidase was 0.85 μ M. If present, the concentration of EG was 0.1 μ M. *Error bars* show S.D. and are from three independent measurements. In *A*-*C*, concentration of BC was 0.5 mg ml⁻¹. *A*, glucose formation. *B*, concentration of *TrCel7A* with the active site occupied by the cellulose chain ([*TrCel7A*]_{OA}) was measured from the inhibition of the hydrolysis of MUL by BC (0.5 mg ml⁻¹). *C*, values of the observed rate constant (k_{obs}) were found from the rates of cellobiose formation (recalculated from the rates of glucose formation) and values of [*TrCel7A*]_{OA} according to Equation 6. *D*-*F*, data points were taken after 2, 5, and 10 min of hydrolysis. *D*, glucose formation after 10 min of hydrolysis. *E*, average values over all time points are plotted. DSE values at different BC concentrations are listed in Table 2.

TABLE 2 DSE between CBH TrCeI7A and EG TrCeI5A in hydrolysis of BC

	TrCel7A and TrCel5A ^a			CD _{<i>Tr</i>Cel7A} and <i>Tr</i> Cel5A ^{<i>a</i>}			
BC	DSE _{Glc} ^b	DSE _{OA} ^c	DSE_k^d	DSE _{Glc} ^b	DSE _{OA} ^c	$\text{DSE}_k^{\ d}$	
$mg m l^{-1}$							
0.1	23 ± 7.9	1.7 ± 0.70	14.5 ± 5.3				
0.25	12 ± 1.6	1.5 ± 0.32	7.8 ± 2.4	5.3 ± 1.9	0.25 ± 1.30	12.5 ± 2.4	
0.5	7.7 ± 0.8	1.3 ± 0.15	5.6 ± 1.2	4.8 ± 1.3	0.64 ± 0.33	5.9 ± 1.3	
1.0	4.5 ± 0.5	1.1 ± 0.04	4.0 ± 1.3	4.4 ± 0.9	0.63 ± 0.03	5.2 ± 2.4	
2.5	3.0 ± 0.7	1.1 ± 0.03	2.7 ± 1.0	2.6 ± 0.4	0.81 ± 0.14	2.6 ± 0.8	

^{*a*} Experimental conditions were as follows: [*Tr*Cel7A] or [CD_{*Tr*}Cel7A] = 0.5 μM, [β-glucosidase] = 0.85 μM, 25 °C, pH 5.0. If present, the concentration of EG (*Tr*Cel5A) was 0.1 μM. Samples were withdrawn after 2, 5, and 10 min of hydrolysis and analyzed for glucose formation and [*Tr*Cel7A]_{OA}.

^b DSE on the level of glucose formation (DSE_{Glc}) represents the ratio of glucose produced by the mixture of *TrC*el7A and *TrC*el5A to glucose produced by individual *TrC*el7A. Glucose formation after 10 min of hydrolysis was used in calculations of DSE_{Glc}. Low levels of glucose produced by individual 0.1 μ M *TrC*el5A were not accounted for in calculating DSE_{Glc}.

^c DSE on the level of [*Tr*Cel7A]_{OA} (DSE_{OA}) represents the ratio of [*Tr*Cel7A]_{OA} measured for the mixture of *Tr*Cel7A and *Tr*Cel5A to [*Tr*Cel7A]_{OA} measured for individual *Tr*Cel7A. For series with intact *Tr*Cel7A, an average value of [*Tr*Cel7A]_{OA} taken over all time points was used in calculations of DSE_{OA}, whereas for CD_{*Tr*Cel7A}, a [CD_{*Tr*Cel7A]_{OA} measured after 10 min of hydrolysis was used.}

^d DSE on the level of observed rate constant (k_{obs}) (DSE_k) represents the ratio of k_{obs} measured for the mixture of *Tr*Cel7A and *Tr*Cel5A to k_{obs} measured for individual *Tr*Cel7A. An average value of k_{obs} taken over all time points was used in calculations of DSE_k.

affinity of intact TrCel7A compared with CD_{TrCel7A}. The addition of EG resulted in an increase in $[TrCel7A]_{OA}$, whereas the opposite was observed in the case of $CD_{TrCel7A}$ (Fig. 3E). The dependence of k_{obs} on [BC] reveals different patterns for individual enzymes and synergistic mixtures (Fig. 3F). Synergistic mixtures displayed a significant decrease in $k_{\rm obs}$ values with increasing [BC], whereas for individual enzymes, k_{obs} values were virtually independent of [BC]. About the same k_{obs} values were found for intact TrCel7A and CD_{TrCel7A} in the case of both individual enzymes and synergistic mixtures (Fig. 3F). For the quantitative description of synergism, the DSE values were calculated. Table 2 lists the DSE values at three different levels: glucose formation (DSE_{Glc}), [*Tr*Cel7A]_{OA} (DSE_{OA}), and k_{obs} (DSE_k) . For intact *Tr*Cel7A, the highest DSE values were observed at the level of glucose formation, whereas for $CD_{TrCel7A}$, the highest DSE was observed at the level of k_{obs} . Because the rate of glucose (or cellobiose) formation is the product of $[TrCel7A]_{OA}$ and k_{obs} (Equation 6), the DSE_{Glc}

should also be the product of DSE_{OA} and DSE_k . The highest DSE values on the level of k_{obs} found for $CD_{TrCel7A}$ are due to the negative effect of EG on $[CD_{TrCel7A}]_{OA}$ (DSE_{OA} values less than 1; Table 2). With the DSE_{OA} for $CD_{TrCel7A}$ as an exception, the DSE values at all levels decreased with increasing [BC] (Table 2).

Synergism was also assessed on lignocellulose as substrate. As in the case of BC, the affinity of intact *Tr*Cel7A toward lignocellulose was higher than that of $\text{CD}_{TrCel7A}$, but no substrate inhibition was observed within the concentration range of lignocellulose studied (Fig. 4*A*). The addition of EG (10% on a molar basis) resulted in a significant synergistic effect (Fig. 4*A*), with average DSE_{Glc} values of 3.2 ± 0.3 and 2.5 ± 0.2 for *Tr*Cel7A and CD_{*Tr*Cel7A}, respectively. EG did not increase the amount of *Tr*Cel7A_{OA} (Fig. 4*B*), suggesting that the availability of chain ends on lignocellulose was not limiting under the study conditions, and the synergistic effect was caused by the increase in k_{obs} values. It must be





FIGURE 4. **Synergism in hydrolysis of lignocellulose by TrCel7A and EG TrCel5A.** \diamond , $TrCel7A; \blacklozenge$, $TrCel7A + EG; <math>\triangle$, $CD_{TrCel7A}; \blacklozenge$, $CD_{TrCel7A}; \blacklozenge$, $CD_{TrCel7A}; \blacklozenge$, $DT_{TrCel7A}; \bullet$, DT_{T



FIGURE 5. **Cellobiose inhibition of TrCeI7A on** ¹⁴**C-BC under single-turnover conditions.** *Error bars* show S.D. and are from three independent measurements. *A*, release of ¹⁴CB in the presence of added cellobiose at 0 mm (\diamond), 0.5 mm (\triangle), 2.0 mm (\bigcirc), 5.0 mm (\bigcirc), or 20 mm (\bigcirc). Concentration of ¹⁴C-BC and *Tr*CeI7A was 0.5 mg ml⁻¹ and 1.0 μ M, respectively. Series without added cellobiose were provided with 0.125 μ M β -glucosidase. An AC trap was added after 30 s of hydrolysis. *B* and *C*, effect of added cellobiose on parameters of single-turnover kinetics, [¹⁴CB]_{max} and *k*. Values of parameters (listed in supplemental Table S4) were found by non-linear regression of the hydrolysis data in *A* (for *Tr*CeI7A) or supplemental Fig. S2 (for *Tr*CeI7A + EG) according to Equation 1. Subscripts CB and CB = 0 refer to the parameters measured in the presence and absence of cellobiose, respectively. \diamond , *Tr*CeI7A; \blacklozenge , *Tr*CeI7A + EG.

noted, however, that we observed the binding of pNP (the product of the hydrolysis of pNPL used as a reporter molecule for [*Tr*Cel7A_{OA}]) to lignocellulose. Binding of MU to lignocellulose was even stronger, and this was the reason why pNPL was used instead of MUL here. Because of the binding of pNP to lignocellulose, the measured [*Tr*Cel7A_{OA}] and k_{obs} values are somewhat over- and underestimated, respectively. For this reason, the DSE_{OA} and DSE_k values on lignocellulose must also be treated with caution. For the DSE_{Glc}, DSE_{OA}, and DSE_k values at different lignocellulose concentrations, see supplemental Table S3.

Inhibition of TrCel7A by Cellobiose-Inhibition of TrCel7A by cellobiose was studied using both single-turnover and "steady state" conditions. The addition of cellobiose clearly reduced the amount of ¹⁴C-cellobiose released under singleturnover conditions (Fig. 5A). Fitting of the data to Equation 1 revealed that the values of both [¹⁴CB]_{max} and k decreased with increasing concentration of added cellobiose (Fig. 5, B and C). Because the method for quantification of $[TrCel7A]_{OA}$ is not applicable in the presence of cellobiose (55), it is not possible to address the effect of cellobiose on $P_{\rm app}$ and $k_{\rm cat}$ experimentally. However, strong limitation of P_{app} of *Tr*Cel7A by n_{free} on BC (57) suggests that the decrease in [¹⁴CB]_{max} is caused by the decrease in $[ES]_{trap}$ rather than in P_{app} . The inhibition of *Tr*Cel7A by cellobiose was also studied in the presence of EG (supplemental Fig. S2). The effect of cellobiose on [14CB]_{max} and k observed in the presence of EG was similar to that for individual *Tr*Cel7A (Fig. 5, *B* and *C*). IC_{50} values for cellobiose inhibition were found by fitting the data to the hyperbolic functions,

and

$$\frac{k_{CB}}{k_{CB=0}} = \frac{1}{1 + \frac{[CB]}{IC_{50}}}$$
(Eq. 8)

(Eq. 7)

where [CB] is the concentration of added cellobiose (mM), and subscripts CB and CB = 0 refer to the parameters measured in the presence and the absence of added cellobiose, respectively. Because of the scattering of data points, the data obtained for the individual *Tr*Cel7A and for the mixture of *Tr*Cel7A and *Tr*Cel5A were combined and analyzed together to estimate IC₅₀ values. In this way, the IC₅₀ values of 3.2 ± 0.8 mM and 2.2 ± 0.7 mM were found for cellobiose inhibition of [¹⁴CB]_{max} and *k*, respectively. For the numerical values of [¹⁴CB]_{max} and *k* measured in the presence of cellobiose, see supplemental Table S4.

 $\frac{\begin{bmatrix} 1^{4}CB \end{bmatrix}_{max CB}}{\begin{bmatrix} 1^{4}CB \end{bmatrix}_{max CB} = 0} = \frac{1}{1 + \frac{\begin{bmatrix} CB \end{bmatrix}}{1 + \frac{\begin{bmatrix} CB \end{bmatrix}}{1 + \frac{\begin{bmatrix} CB \end{bmatrix}}{1 + \frac{\begin{bmatrix} CB \end{bmatrix}}{1 + \frac{CB}{1 + \frac{CB}{1$

To study cellobiose inhibition of TrCel7A in "steady state," the hydrolysis of ¹⁴C-BC (0.25 mg ml⁻¹) was followed over a longer time (2 min to 3 h). The final degree of degradation of ¹⁴C-BC ranged from 10 to 80%, depending on the experimental conditions. Fig. 6, *A* and *B*, shows the time courses of degradation of ¹⁴C-BC by individual *Tr*Cel7A and by the mixture of *Tr*Cel7A and *Tr*Cel5A in the presence of cellobiose at different concentrations. In the case of series without added cellobiose, the experiments were provided with β -glucosidase to prevent the inhibition of *Tr*Cel7A by cellobiose released during hydro-





FIGURE 6. **Cellobiose inhibition of TrCeI7A on** ¹⁴**C-BC in** "**steady state**." *A* and *B*, release of ¹⁴CB in hydrolysis of ¹⁴C-BC by individual TrCeI7A (A) or TrCeI7A + EG (B). The concentration of ¹⁴C-BC and TrCeI7A was 0.25 mg ml⁻¹ and 0.25 μ M, respectively. If present, the concentration of EG (TrCeI5A) was 0.025 μ M. Series without added cellobiose were provided with 0.125 μ M β -glucosidase (\diamond). Concentration of added cellobiose was 0 mM (\diamond), 0 mM without β -glucosidase (\diamond), 0.2 mM (*), 0.5 mM (\triangle), 1.0 mM (+), 2.0 mM (\bigcirc), 5.0 mM (>), or 10 mM (\square). C and *D*, hydrolysis data were rearranged to obtain the ratio of ([¹⁴CB]_{CB}/[¹⁴CB]_{CB} = 0) for each time point. Subscripts CB and CB = 0 refer to the measurements in the presence and absence of cellobiose, respectively. Plotted are average values over all time points (except TrCeI7A + EG) with corresponding *error bars* (S.D.). *Solid lines* are from the non-linear regression according to supplemental Equation S1 (individual enzymes) or Equation 9 (synergistic mixtures). *C*, TrCeI7A (\diamond) and TrCeI7A + EG (\blacklozenge). D, CD_{TrCeI7A} (\triangle) and CD_{TrCeI7A} + EG (\blacklozenge).

lysis. The strength of cellobiose inhibition was analyzed using the plots in coordinates ($[^{14}CB]_{CB}/[^{14}CB]_{CB = 0}$) versus [cellobiose], where $[^{14}CB]_{CB}$ and $[^{14}CB]_{CB = 0}$ are the concentrations of released ^{14}C -cellobiose in the experiments with and without added cellobiose, respectively (Fig. 6*C*). The ratio of $[^{14}CB]_{CB}/[^{14}CB]_{CB} = _0$ at a certain concentration of added cellobiose was first found for each time point in Fig. 6, *A* and *B*, and Fig. 6*C* plots the average values taken over all time points. No or little systematic variation of $[^{14}CB]_{CB}/[^{14}CB]_{CB = 0}$ with hydrolysis time was observed (*e.g.* see supplemental Table S5). In the case of a synergistic mixture of *TrC*el7A and *TrC*el5A, the amount of cellobiose released during hydrolysis was significant (the curve with no added cellobiose and β -glucosidase in Fig. 6*B*) and was accounted for in generating the plot in Fig. 6*C*.

For calculation of IC_{50} values (listed in Table 3), the data for synergistic hydrolysis were first fitted to simple hyperbolae for competitive inhibition,

$$\frac{[{}^{14}CB]_{CB}}{[{}^{14}CB]_{CB=0}} = \frac{([{}^{14}C\text{-BC}] + K_m)(1 - H)}{[{}^{14}C\text{-BC}] + K_m\left(1 + \frac{[CB]}{K_i}\right)} + H \qquad (Eq. 9)$$

where [CB] is the concentration of added cellobiose, [¹⁴C-BC] is cellulose concentration (mg ml⁻¹), K_m is the Michaelis constant for cellulose (mg ml⁻¹), K_i is the inhibition constant for cellobiose (mM), and H is a parameter that accounts for the background radioactivity (*i.e.* the radioactivity reading that is independent of *Tr*Cel7A). In the non-linear regression analysis, the value of [¹⁴C-BC] was fixed to a value used in the experiments. The values of K_m , K_i , and H obtained from the fitting of

TABLE 3

CB inhibition of TrCel7A in "steady state"

Enzyme(s) ^a	IC_{50} for CB^b
	тм
<i>Tr</i> Cel7A	0.65 ± 0.15
TrCel7A + EG	0.38 ± 0.03
$CD_{TrCel7A}$	0.72 ± 0.28
$CD_{TrCel7A} + EG$	0.46 ± 0.07

^{*a*} Experiment conditions were as follows: [¹⁴C-BC] = 0.25 mg ml⁻¹, [*Tr*Cel7A] or $[CD_{TrCel7A}] = 0.25 \ \mu$ M, 25 °C, pH 5.0. If present, the concentration of EG (*Tr*Cel5A) was 0.025 \ \muM.

 b IC₅₀ for cellobiose was found from the data in Fig. 6, *C* and *D*, using non-linear regression according to supplemental Equation S1 (for individual *Tr*Cel7A or its CD) or Equation 9 (for synergistic mixture).

the data to Equation 9 were further used to calculate the values of $\rm IC_{50}$ using Equation 10.

$$IC_{50} = \frac{\left[{}^{14}\text{C-BC}\right] + K_m}{\frac{K_m}{K_i}(1 - 2H)}$$
(Eq. 10)

It must be noted that, although we used equations for competitive inhibition (Equations 9 and 10), the assumption about the type of inhibition is not important in the context of deriving IC_{50} values. The equations for other types of reversible inhibition like non-competitive, uncompetitive, or mixed type of inhibition are equally well suited for this purpose. Likewise, the values of individual parameters, K_m , K_i , and H, are not important. Important is their combination (Equation 10) that defines the value of IC_{50} . Although this simplified approach does not permit one to distinguish between different types of inhibition, slightly higher IC_{50} values obtained at higher TrCel7A concen-





FIGURE 7. **Hydrolysis of cellulose by processive CBH** (*A* and *B*) and possible mechanism of synergism with EG (*C*). *A*, processive cycle of CBH consists of at least six putative steps as follows (65). *a*, CBM-mediated binding to the cellulose surface; *b*, finding and recognition of cellulose chain end; *c*, threading of cellulose chain into active site tunnel and formation of productive enzyme-substrate complex; *d*, hydrolysis of glycosidic bond; *e*, expulsion of product CB; *f*, threading another cellobiose unit to reform productive complex. Steps *d*-*f* are repeated until enzyme happens to dissociate or stops behind an obstacle (55). Transit times were found from the values of rate constants for the corresponding step(s). *B*, hydrolysis of cellulose by individual CBH. CBH cannot pass through the amorphous regions (*wavy lines*) and stalls. The length of the crystalline regions between amorphous parts defines the length of obstacle-free path (*n*_{free}), which also limits the apparent processivity (*P*_{app}) of CBH. The steady state rate of cellobiose formation is governed by the slow dissociation (*k*_{off} value was taken from Ref. 57) of stalled CBH. *C*, synergistic hydrolysis of cellulose. EG accelerates the recruitment of CBH by degrading amorphous regions. *P*_{app} of CBH is determined by the DP of EG-fragmented cellulose surface (DP_{surface}), and the steady state rate of cellobiose formation approaches the limit set by the velocity of processive movement of CBH. Transit times correspond to the steps taken by the CBH depicted to the *left* of the cellulose. Conventional mechanism of endo-exo synergism is depicted to the *right* of the cellulose.

trations (supplemental Table S6) suggest non-competitive or mixed type inhibition. Unlike with the inhibition of synergistic mixture, a simple hyperbola (Equation 9) was not sufficient to describe the inhibition of individual TrCel7A. In the latter case, an equation accounting for two different modes of action was necessary to fit the data (supplemental Equation S1). The cellobiose inhibition of individual TrCel7A was somewhat weaker than the inhibition of the synergistic mixture (Table 3). Because the cellobiose inhibition of TrCel5A is more than an order of magnitude weaker than that of TrCel7A (58), the cellobiose inhibition of the synergistic mixture apparently represents the inhibition of the CBH component. The strength (Table 3) and pattern (Fig. 6D and supplemental Fig. S3) of cellobiose inhibition of $CD_{TrCel7A}$ and intact TrCel7A was similar in the case of both individual enzymes and synergistic mixtures.

DISCUSSION

Processive CBHs are the key components of the efficient fungal cellulase systems. However, the molecular mechanisms of their mode of action are still not fully understood. The major obstacle in advancing our knowledge has been the lack of biochemical methods for assessing different molecular steps of the hydrolysis of the insoluble and heterogeneous substrate. Here we attempted to fill this gap by introducing a single-turnover approach that was used in parallel with "steady state" measurements of *Tr*Cel7A-catalyzed hydrolysis of cellulose. A processive cycle of *Tr*Cel7A consists of at least six putative steps (Fig. 7*A*) (65). Measurement of the formation of [*Tr*Cel7A]_{OA} in time (Figs. 1*B* and 2*B*) revealed that the binding through the active site was fast, with the transit times for steps a-c in Fig. 7*A* around 10 s. A recent study of transient kinetics also supports the fast complex formation between *Tr*Cel7A and cellulose



(60). The k_{cat} value $2.2 \pm 0.5 \text{ s}^{-1}$ (Table 1) predicts a transit time of about 0.45 s for passing through steps d–f in Fig. 7A. Transit times for single processive runs (P_{app} times steps d–f in Fig. 7A) found from the values of rate constants k (Table 1) were in the range of 30 s, and during this time, an average of 66 ± 7 cellobiose units were released (Table 1). Although different scenarios for CBM-assisted catalysis have been proposed (15, 16), the supporting biochemical evidence has remained elusive (17). Here we measured somewhat lower P_{app} and k_{cat} values for CD_{TrCel7A} compared with the intact enzyme, but the differences may not be significant, considering the error limits (Table 1). Thus, our data rather support the observations that CD_{TrCel7A} moves along cellulose chain with the same velocity as intact TrCel7A (61).

Our understanding of the mechanisms of synergism between EG and CBH cannot be in advance of our understanding of the rate limitations in CBH-catalyzed cellulose hydrolysis. Considering the crystalline nature of the substrate, the number of reducing chain ends available for CBH is expected to be low. The conventional explanation of endo-exo synergism assumes that the chain end availability is rate-limiting for CBH so that generation of new chain ends by EG will increase the population of productive CBH cellulose complexes (24). Consistent with that, we also found an increase in $[TrCel7A]_{OA}$ in the presence of EG under both single-turnover (Fig. 2B and Table 1) and "steady state" (Fig. 3 and Table 2) conditions. However, the increase in [TrCel7A]_{OA} was far from being sufficient to account for the EG-caused increase in "steady state" rates. The majority of the synergistic effect came from the EG-caused increase in the rate constant (k_{obs}) of the hydrolysis of BC by *Tr*Cel7A instead (Fig. 3 and Table 2). The increase in k_{obs} points to the presence of an additional mechanism of synergy between TrCel7A and EG that is used in parallel with the conventional mechanism. At optimal enzyme/substrate ratios, the synergistic "steady state" k_{obs} values (Fig. 3) approached the k_{cat} value measured using single-turnover conditions (Table 1), meaning that in the presence of EG, the steady state rate becomes limited by the velocity of processive movement of TrCel7A. Recently, we proposed an obstacle model to describe the rate retardation in CBH-catalyzed cellulose hydrolysis (55). According to this, the retardation in hydrolysis rate is caused by the accumulation of stalled, non-productive CBH cellulose complexes (Fig. 7B). The comparison of transit times measured here for binding (10 s) and processive movement (30 s) and for the recruitment of TrCel7A (\sim 25 min) measured before (57) supports this model. Although the exact nature of obstacles remains elusive, our data suggest that they are related to the amorphous parts of BC. It is worth mentioning that the $P_{\rm app}$ value for *Tr*Cel7A was close to the leveling off DP value of BC, the DP value that cellulose preparation approaches during heterogeneous acid hydrolysis (25). Heterogeneous acid hydrolysis, like HCl-catalyzed hydrolysis, is limited with the degradation of easily accessible amorphous regions, whereas crystalline regions remain intact. Although difficult to address experimentally, the regularity of amorphous parts that disrupt the crystalline structure has been demonstrated in ramie cellulose (66, 67). We propose that TrCel7A cannot pass through and stalls after encountering amorphous parts on BC (Fig. 7*B*). The P_{app} of *Tr*Cel7A is thus

limited by the length of crystalline regions between amorphous parts on BC, and this distance also defines the length of the obstacle-free path (n_{free}) for *Tr*Cel7A on this substrate (Fig. 7*B*). Because dissociation is much slower than association and processive run, the k_{obs} of cellobiose formation in steady state becomes limited by $n_{\text{free}}k_{\text{off}}$. On the other hand, by preferentially targeting and degrading amorphous regions, EG removes the obstacles, and TrCel7A does not stall (Fig. 7C). In this way, EG accelerates the recruitment of TrCel7A, and the steady state $k_{\rm obs}$ value of cellobiose formation approaches the value of true $k_{\rm cat}.$ In the presence of EG, the $P_{\rm app}$ of $Tr{\rm Cel7A}$ will be apparently limited by the DP of cellulose chains on EG-fragmented cellulose surface (Fig. 7*C*). Similar k_{obs} values found for synergistic hydrolysis with the mixtures containing intact TrCel7A or $CD_{TrCel7A}$ confirmed that the mechanism of synergy depicted in Fig. 7C is operative also in the case of CD_{TrCel7A}. However, in synergistic hydrolysis, CD_{TrCel7A} appeared to be inefficient in binding to cellulose through the active site (low levels of [CD_{TrCel7A}]_{OA} in Fig. 3B). This suggests that in the case of $CD_{TrCel7A}$ passing through steps *ab* and/or *c* in Fig. 7*A* are impaired on EG-generated chain ends.

The relative contribution of the conventional (characterized by DSE_{OA}) and the novel (characterized by DSE_k) mechanism of synergism was dependent on the enzyme/substrate ratio (Table 2). The relative contribution of the conventional mechanism was higher at high enzyme/substrate ratios. At low enzyme/substrate ratios, most of the TrCel7A molecules were bound through the active site even in the absence of EG and synergism revealed only at the level of k_{obs} . Hydrolysis of BC is interesting in that it displays a phenomenon of substrate inhibition (42). However, substrate inhibition is revealed only in synergistic hydrolysis by the EG/CBH mixtures containing intact CBH (42). In our early study, we proposed that at a constant concentration of enzymes, an increase in BC concentration will result in lower surface density of EG-generated chain ends and therefore longer distances of lateral diffusion used by intact TrCel7A to catch the chain ends (step b in Fig. 7A) (42). However, we did not observe a decrease in the [TrCel7A]_{OA} with increasing concentration of BC, and it was k_{obs} of synergistic hydrolysis instead that decreased with increasing [BC] (Fig. 3). Decrease in k_{obs} can still be described by the lower surface density of EG-generated chain ends at high BC concentrations. To avoid the stalling of TrCel7A, it is necessary that the EG-degraded amorphous region would be on the same cellulose chain and in front of the processively moving TrCel7A (Fig. 7*C*). The probability of the latter is expected to decrease with decreasing surface density of EG-degraded amorphous regions on BC. Because of the lower affinity of CD_{TrCel7A} toward cellulose, in the case of synergistic mixtures containing $CD_{TrCel7A}$, the decrease in k_{obs} is apparently compensated for by the increase in population of bound CD_{TrCel7A} with increasing BC concentration, and substrate inhibition at the level of glucose formation is not revealed (Fig. 3).

Cellobiose inhibition also reflects the mode of action and rate limitation of *Tr*Cel7A. Under single-turnover conditions, cellobiose reduced the number of initiations by competing with cellulose chain for binding to *Tr*Cel7A (reduced [¹⁴CB]_{max} values) and also slowed the processive movement of *Tr*Cel7A



(reduced k values). The strongest binding of cellobiose, with the K_d value of 20 μ M, takes place in the product sites (glucose unit binding sites +1/+2 in Fig. 7A) of the active site tunnel of *Tr*Cel7A (68, 69). However, binding of cellobiose to the sites +1/+2 permits the formation of non-productive complex with cellulose chain bound to the sites -7/-1. Such a complex is expected because it also forms after the cleavage of the glycosidic bond in cellulose (step d in Fig. 7A). The IC₅₀ value of $3.2 \pm$ 0.8 mM found for cellobiose inhibition of [¹⁴CB]_{max} apparently reflects the binding of cellobiose somewhere into minus sites of the active site tunnel, and this competes with the binding of the cellulose chain. Because the product sites must be empty before *Tr*Cel7A can step further on the cellulose chain (step *f* in Fig. 7*A*), the binding of cellobiose to the sites +1/+2 is expected to restrict the processive movement. This non-competitive component of inhibition is apparently responsible for the slower movement of TrCel7A in the presence of cellobiose. A recent computational study suggested that the product expulsion may be a rate-limiting factor in the processive cycle of TrCel7A (5). The about 100-fold higher IC_{50} value of cellobiose for k compared with the K_d value for its binding to the sites +1/+2, however, suggests that the product expulsion (step e in Fig. 7A) is not limiting for k_{cat} (steps d-f in Fig. 7A). Cellobiose inhibition of TrCel7A in "steady state" (Table 3) was stronger than that observed for $[^{14}CB]_{max}$ and k in single-turnover experiments. The competitive component of inhibition should decrease the number of initiations by the same factor in the case of both "steady state" and single-turnover conditions. Thus, our data indicate that both competitive and non-competitive components of inhibition are involved in cellobiose inhibition of the cellulose hydrolysis in the "steady state" resulting in an overall mixed type of inhibition. Somewhat stronger cellobiose inhibition observed in the case of synergistic mixture can now be explained by the increased contribution of the processive movement in controlling the "steady state" rate of the synergistic hydrolysis and therefore also increased contribution of the non-competitive component of inhibition compared with individual TrCel7A.

Our data suggest that the novel mechanism of synergy depicted in Fig. 7*C* is also operative in lignocellulose hydrolysis. Besides amorphous parts, lignocellulose also contains lignin and residual hemicellulose, which may serve as obstacles for processive TrCel7A (55). Removal of these apparently requires more accessory enzymes like hemicellulases and oxidative enzymes and explains the complex nature of the synergism in lignocellulose degradation.

Acknowledgments—We thank Jan Larsen (Inbicon, Skærbæk, Denmark) for lignocellulose and Dr. Silja Kuusk (University of Tartu) for critical reading.

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