

Evidence for a Key Role of Cytochrome bo_3 Oxidase in Respiratory Energy Metabolism of *Gluconobacter oxydans*

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The obligatory aerobic acetic acid bacterium *Gluconobacter oxydans* oxidizes a variety of substrates in the periplasm by membrane-bound dehydrogenases, which transfer the reducing equivalents to ubiquinone. Two quinol oxidases, cytochrome bo_3 and cytochrome bd , then catalyze transfer of the electrons from ubiquinol to molecular oxygen. In this study, mutants lacking either of these terminal oxidases were characterized. Deletion of the *cydAB* genes for cytochrome bd had no obvious influence on growth, whereas the lack of the *cyoBACD* genes for cytochrome bo_3 severely reduced the growth rate and the cell yield. Using a respiration activity monitoring system and adjusting different levels of oxygen availability, hints of a low-oxygen affinity of cytochrome bd oxidase were obtained, which were supported by measurements of oxygen consumption in a respirometer. The H^+/O ratio of the $\Delta cyoBACD$ mutant with mannitol as the substrate was 0.56 ± 0.11 and more than 50% lower than that of the reference strain (1.26 ± 0.06) and the $\Delta cydAB$ mutant (1.31 ± 0.16), indicating that cytochrome bo_3 oxidase is the main component for proton extrusion via the respiratory chain. Plasmid-based overexpression of *cyoBACD* led to increased growth rates and growth yields, both in the wild type and the $\Delta cyoBACD$ mutant, suggesting that cytochrome bo_3 might be a rate-limiting factor of the respiratory chain.

Gluconobacter oxydans is a Gram-negative, obligate aerobic, rod-shaped alphaproteobacterium belonging to the family of acetic acid bacteria (1). Due to its many membrane-bound dehydrogenases that incompletely oxidize sugars, sugar alcohols, and other compounds stereo- and regioselectively in the periplasm, *G. oxydans* has been used for decades in industrial biotechnology (2). Important applications are in the production of vitamin C and of 6-amino-L-sorbose, an intermediate in the synthesis of the antidiabetic drug miglitol (3). Only small fractions of the carbon and energy sources are metabolized in the cytoplasm, either via the pentose phosphate pathway or via the Entner-Doudoroff pathway, and it was demonstrated that the former one is of major importance for growth on mannitol and glucose (4, 5). Moreover, it was recently shown that the pentose phosphate pathway has partially cyclic operation during growth on glucose (6).

G. oxydans possesses 32 membrane-bound dehydrogenases, 11 with known and 21 with unknown substrate specificity (Fig. 1) (7, 8). Electrons are transferred to ubiquinone from the various dehydrogenases via pyrroloquinoline quinone (PQQ), PQQ plus cytochrome *c*, or flavin adenine dinucleotide (FAD). Electron transfer from ubiquinol to oxygen is catalyzed by two terminal oxidases, cytochrome bd and cytochrome bo_3 (9) (Fig. 1). Interestingly, the genome sequence of *G. oxydans* 621H revealed the presence of the *qcrABC* genes for a cytochrome bc_1 complex and of a *cyoA* gene for a soluble cytochrome *c*, whereas genes for a cytochrome *c* oxidase were absent (8). Furthermore, genome sequencing revealed that *G. oxydans* possesses only a non-proton-pumping single subunit NADH dehydrogenase encoded by the *ndh* gene. Whereas genes for succinate:quinone oxidoreductase were absent, an *mgo* gene for malate:quinone oxidoreductase was present.

The cytochrome bo_3 quinol oxidase of *Gluconobacter suboxydans* IFO 12528 (now *G. oxydans*) has been purified and characterized (10). It belongs to the superfamily of heme-copper oxygen reductases and contains heme *b*, heme *o*, and a copper ion as

prosthetic groups. The reaction catalyzed by cytochrome bo_3 quinol oxidase contributes to the generation of proton motive force in two ways. On the one hand, ubiquinol is oxidized at the periplasmic side of the membrane, with the protons released in the periplasm and the electrons transferred to the binuclear heme o_3 -Cu center. As the protons for water formation stem from the cytoplasm, an electrochemical proton gradient is established. On the other hand, heme-copper oxygen reductases use the free energy associated with electron transfer from ubiquinol to dioxygen to pump protons across the membrane, further contributing to the establishment of proton motive force (11). In *Escherichia coli* the bo_3 oxidase is synthesized under conditions of high aeration.

Cytochrome bd oxidase of *G. oxydans* was characterized as a cyanide-insensitive oxidase (9). Biochemical and spectroscopic studies of overexpression strains revealed the presence of heme b_{558} , b_{595} , and *d* (12, 13). Cytochrome bd oxidases do not pump protons but can generate proton motive force by oxidizing ubiquinol at the periplasmic side of the membrane and taking up protons for water formation from the cytoplasm (14, 15). In *Escherichia coli* maximal synthesis of cytochrome bd occurs under microaerobic conditions (16).

The use of *G. oxydans* in biotechnological production processes, which are often whole-cell biotransformations, is limited

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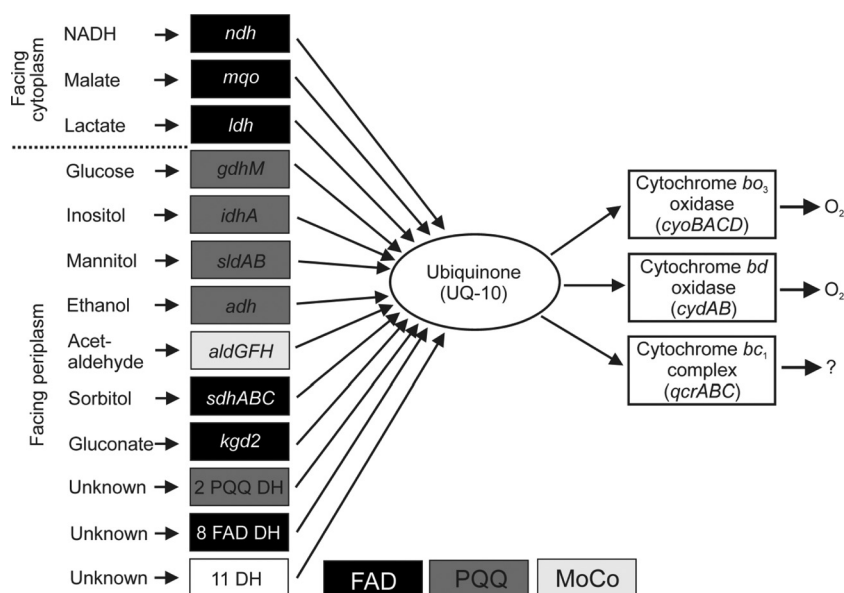


FIG 1 Overview of the components of the respiratory chain of *G. oxydans*. DH, dehydrogenase; FAD, flavin adenine dinucleotide; PQQ, pyrroloquinoline quinone; MoCo, molybdopterin.

due to its poor cell yield, which results in a cost-intensive formation of biomass. *G. oxydans* IFO3293 and *G. oxydans* 621H cells cultivated with glucose as the carbon source in a bioreactor reach a cell yield of 0.09 g of cells (dry weight) [$\text{g}_{\text{cdw}}/\text{g}$ of glucose (4, 17)]. In comparison to these values, *E. coli* reaches a value of 0.49 $\text{g}_{\text{cdw}}/\text{g}$ of glucose, and *Bacillus subtilis* reaches a yield of 0.32 $\text{g}_{\text{cdw}}/\text{g}$ of glucose (18, 19). It has been shown for several respiring bacteria that the cell yield correlates with the H^+/O ratio measured by the oxygen pulse method (20, 21). *Acetobacter pasteurianus* for example has a H^+/O ratio of 1.9 ± 0.1 and a cell yield of 13.1 $\text{g}_{\text{cdw}}/\text{mol}$ of ethanol, whereas *Paracoccus pantotrophus* shows a H^+/O ratio of 4.9 ± 0.3 and reaches a cell yield of 25.2 $\text{g}_{\text{cdw}}/\text{mol}$ of ethanol (21).

To gain further insights into the respiratory energy metabolism of *G. oxydans*, in-frame deletion mutants of the terminal oxidases were constructed and characterized with respect to growth, respiration activity, and H^+/O ratio. The results show that cytochrome bo_3 oxidase is of major importance for growth of *G. oxydans*, whereas cytochrome bd oxidase is dispensable under the tested conditions.

MATERIALS AND METHODS

Materials. Chemicals were obtained from Sigma-Aldrich (Taufkirchen, Germany), Qiagen (Hilden, Germany), Merck (Darmstadt, Germany), and Roche Diagnostics (Mannheim, Germany).

Bacterial strains, plasmids, and media. The bacterial strains and plasmids used in this study are listed in Table 1. *Escherichia coli* strains were cultivated in lysogeny broth (LB) medium (22, 23) or on LB agar plates at 37°C. When required, kanamycin was added to a final concentration of 50 $\mu\text{g ml}^{-1}$. *G. oxydans* ATCC 621H Δupp (ATCC 621H is identical to DSM 2343) strains were cultivated on mannitol medium containing 220 mM (4%, wt/vol) mannitol, 5 g liter $^{-1}$ yeast extract, 2.5 g liter $^{-1}$ $\text{MgSO}_4 \cdot 7 \text{H}_2\text{O}$, 1 g liter $^{-1}$ $(\text{NH}_4)_2\text{SO}_4$, and 1 g liter $^{-1}$ KH_2PO_4 . The initial pH value of the medium was 6.0. *G. oxydans* possesses a natural resistance against cefoxitin. As a precaution to prevent bacterial contaminations, 50 $\mu\text{g ml}^{-1}$ cefoxitin was added to the preculture medium. When required, kanamycin was added (50 $\mu\text{g ml}^{-1}$).

Cloning and DNA techniques. For DNA manipulation standard methods were used as described by Sambrook and Russell (24). For PCRs, genomic DNA isolated from *G. oxydans* 621H Δupp was used as the template. Competent cells of *E. coli* were prepared with CaCl_2 and transformed as described by Hanahan et al. (25). DNA sequencing was performed by Agowa (Berlin, Germany) and Eurofins MWG Operon (Ebersberg, Germany). Oligonucleotides were synthesized by Biolegio (Nijmegen, Netherlands) and are listed in Table 1.

Construction of in-frame deletion mutants. Construction of *G. oxydans* Δupp in-frame deletion mutants of the genes *cydAB* and *cyoBACD* was performed using a recently described method in which fluorouracil is used to select for the second homologous recombination event leading to chromosomal excision of the plasmid vector (26). For the deletion of *cyoBACD*, plasmid pAJ-*cyoBACD* was constructed as follows. A total of 500 bp of the upstream region of *cyoA* and 500 bp of the downstream region of *cyoD* were amplified using the oligonucleotide pairs *cyoBACD_forw_FIA/cyoBACD_rev_FIA* and *cyoBACD_forw_FIB/cyoBACD_rev_FIB* and Phusion DNA polymerase (Fisher Scientific, Schwerte, Germany). The two PCR products were fused by overlap extension PCR with Platinum Pfx DNA polymerase (Invitrogen, Darmstadt, Germany) using the oligonucleotides *cyoBACD_forw_FIA/cyoBACD_rev_FIB*. The resulting 1-kb PCR product was cloned into the *SmaI*-restricted plasmid pAJ63a that is nonreplicative in *G. oxydans*. After conjugative transfer of pAJ-*cyoBACD* from *E. coli* S17-1 to *G. oxydans* Δupp , colonies were screened by PCR for chromosomal integration of pAJ-*cyoBACD* via a single homologous crossover event using the oligonucleotides *cyoBACD_mut_forw* and *cyoBACD_mut_rev*. Positive clones were inoculated overnight in 20 ml of mannitol medium containing cefoxitin and kanamycin and used as a preculture for fluorouracil-enforced vector excision, as described previously (5). Fluorouracil-resistant colonies were screened by PCR for the chromosomal deletion of *cyoBACD* using the oligonucleotide pair *cyoBACD_mut_forw/cyoBACD_mut_rev* and *cyoBACD_forw/cyoBACD_rev*. The up- and downstream regions of the deleted genes were sequenced, and the corresponding strain was named *G. oxydans* $\Delta\text{upp} \Delta\text{cyoBACD}$. Deletion of the *cydAB* genes was performed analogously with the help of plasmid pAJ-*cydAB*, which contains the upstream region of *cydA* fused to the downstream region of *cydB*. The desired strain obtained after allelic exchange was called *G. oxydans* $\Delta\text{upp} \Delta\text{cydAB}$.

TABLE 1 Bacterial strains, plasmids, and oligonucleotides used in this work

Strain, plasmid, or oligonucleotide	Characteristic(s) or primer sequence ^a	Source and/or reference
Strains		
<i>E. coli</i> DH5αF'	F' ϕ 80dlacZΔM15 Δ(<i>lacZYA-argF</i>)U169 <i>deoR recA1 endA1 hsdR17</i> (r _K ⁻ m _K ⁺) <i>supE44 thi-1 gyrA96 relA1</i>	25
<i>E. coli</i> S17-1	Δ <i>recA endA1 hsdR17 supE44 thi-1 tra</i> ⁺	51
<i>G. oxydans</i> Δ <i>upp</i>	<i>G. oxydans</i> 621H derivative with a deletion of GOX0327 coding for uracil phosphoribosyltransferase; reference strain in this study	26
<i>G. oxydans</i> Δ <i>upp</i> Δ <i>cydAB</i>	<i>G. oxydans</i> Δ <i>upp</i> derivative with a deletion of the genes <i>cydA</i> (GOX0278) and <i>cydB</i> (GOX0279) coding for cytochrome <i>bd</i> oxidase	This work
<i>G. oxydans</i> Δ <i>upp</i> Δ <i>cyoBACD</i>	<i>G. oxydans</i> Δ <i>upp</i> derivative with a deletion of the genes <i>cyoBACD</i> (GOX1911 to GOX1914) coding for cytochrome <i>bo</i> ₃ oxidase	This work
Plasmids		
pAJ63a	Kan ^r ; pK18mobGII derivative; <i>lacZ mob oriV</i> ; contains GOX0327 for uracil phosphoribosyltransferase including its promoter region	26
pAJ- <i>cydAB</i>	Kan ^r ; pAJ63a derivative used for marker-free deletion of the <i>cydAB</i> genes; contains an overlap extension PCR product covering the 20-bp upstream region of <i>edd</i> and the 36-bp downstream region of <i>eda</i>	This work
pAJ- <i>cyoBACD</i>	Kan ^r ; pAJ63a derivative used for marker-free deletion of the <i>cyoBACD</i> genes; contains an overlap extension PCR product covering 20-bp upstream region and the 67-bp downstream region of <i>gnd</i>	This work
pBBR1p384	Kan ^r ; pBBR1MCS-2 derivative containing the promoter region of <i>gox0384</i> for target gene expression	52; U. Deppenmeier, University of Bonn, Germany
pBBR1p384- <i>cyoBACD</i>	Kan ^r ; pBBR1p384 derivative expressing <i>cyoBACD</i>	This work
pBBR1p384- <i>cydAB</i>	Kan ^r ; pBBR1p384 derivative expressing <i>cydAB</i>	This work
pBBR1p384- <i>cydABCD</i>	Kan ^r ; pBBR1p384 derivative expressing <i>cydABCD</i>	This work
Oligonucleotides		
cydAB_forw_FIA	TCTCCGGACAACCGGATCAC	
cydAB_rev_FIA	GTAGTGATGTCGGCCATGTCGATTGCCTTCTGGGTAGATGGCGAAAACGC	
cydAB_forw_FIB	AAGGCAATCGACATGGCCGGACATCACTACCCTGAGAACAGGGAGGCCG	
cydAB_rev_FIB	CTGTTCGACAGTCTGCATCGC	
cydAB_mut_forw	ATCGCTCTCACAGCATCG	
cydAB_mut_rev	GGGCATGTGTCGTATGTC	
cydAB_screen_forw	TGAACACGCTGGAATACC	
cydAB_screen_rev	CATCGTGTCTGTCAGTTC	
cyoBACD_forw_FIA	GGGTTTCGCTCAGATAACAAG	
cyoBACD_rev_FIA	GGACATCATGTTGATCATCCGTTCCGGCTTGCAGTAGTCGCCGGGAAACG	
cyoBACD_forw_FIB	AAGCCGGAACGGATGATCAACATGATGTCGCCGCTAAGGTTTCTTTGAAA	
cyoBACD_rev_FIB	ACGGATTGCGTGGAAATC	
cyoBACD_mut_forw	GTCATGATGCGCTGACG	
cyoBACD_mut_rev	CGATCGGAGACGTCAATG	
cyoBACD_forw	CTGGCGAAGAACAAGAAG	
cyoBACD_rev	GGTGCTGGTGTTCATGTG	
cydAB_compl_forw_XhoI	AGTTCGCTCGAGCTACCCAGAAGGCAATCGAC ^b	
cydAB_compl_rev_KpnI	TGACTTGGTACCCAGCCCAGATCGCCACGAAC ^c	
cydCD_compl_forw_EcoRI	GGCACGGAATTCTGTCGGGCTTTGCGACCTAT ^d	
cydCD_compl_rev_XhoI	GCGTAGCTCGAGCAGGATAGAGAGGTGTGAAG ^b	
cyoBACD_compl_forw_XhoI	TGCGATCTCGAGACTACTGCAAGCCGGAACGG ^b	
cyoBACD_compl_rev_KpnI	GTACTGGGTACCAAGGGCTGGCAGGATTTCTC ^c	

^a The sequence is given 5' to 3'. Underlined sequences indicate the regions used for overlap extension PCR or restriction enzyme sites.

^b Contains an XhoI site.

^c Contains a KpnI site.

^d Contains an EcoRI site.

Complementation studies. For complementation of the deletion mutants, the broad-host-range plasmid pBBR1p384 was used to construct three expression plasmids. The *cyoBACD* region (GOX1911 to GOX1914) including 20 bp upstream of the predicted start codon of *cyoB* was amplified using Phusion DNA polymerase (Fisher Scientific, Schwerte, Germany) with the oligonucleotides *cyoBACD_compl_forw_XhoI* and *cyoBACD_compl_rev_KpnI*. The *cydAB* region (GOX0278 to GOX0279)

including 20 bp upstream of the predicted start codon of *cydA* was amplified with the oligonucleotides *cydAB_compl_forw_XhoI* and *cydAB_compl_rev_KpnI*. The PCR products were digested with XhoI and KpnI and cloned into pBBR1p384 restricted with the same enzymes, resulting in plasmids pBBR1p384-*cyoBACD* and pBBR1p384-*cydAB*. The *cydCD* region (GOX2409 to GOX2410) including 31 bp upstream of the predicted start codon was amplified using Phusion DNA polymerase (Fisher Scien-

tific, Schwerte, Germany) with the oligonucleotides *cydCD_compl_forw_EcoRI* and *cydCD_compl_rev_XhoI*. The PCR product was digested with *EcoRI* and *XhoI* and cloned into pBBR1p384-*cydAB* restricted with the same enzymes, resulting in plasmid pBBR1p384-*cydABCD*. Using *E. coli* S17-1 as host, these plasmids and as a control pBBR1p384 vector were transferred into the desired *G. oxydans* strains by conjugation.

For growth experiments with the plasmid-carrying strains, 20 ml of mannitol medium in a 100-ml baffled shake flask (three baffles, 1 by 2.5 cm each) was inoculated with cells from agar plates and incubated for 24 h at 30°C and 140 rpm. A second preculture (80 ml of mannitol medium in a 500-ml baffled shake flask with three baffles, 1.5 by 5 cm each) was inoculated with 1% (vol/vol) of the first preculture and incubated for 16 h at 30°C and 140 rpm. This preculture was then used for inoculation of the main culture (100 ml of mannitol medium in a 500-ml baffled shake flask) to an optical density at 600 nm (OD_{600}) of 0.3. At selected time points, samples for the measurement of the optical density and for high-performance liquid chromatography (HPLC) analysis were taken. All cultivations were carried out in a Minitron incubation shaker (Infors HT, Basel, Switzerland).

Characterization of respiration activity and growth. Cultivations of *G. oxydans* 621H Δupp and deletion mutants were performed using a self-made respiration activity monitoring system, RAMOS, which enables the online measurement of the oxygen transfer rate (OTR), carbon dioxide transfer rate (CTR), and respiratory quotient (RQ) in eight parallel flasks (27). The OTR describes the total molar flow of oxygen per time from the gas phase to the liquid volume. Since the microorganisms in the liquid phase consume this oxygen, OTR is equal to oxygen uptake rate. To determine the OTR, modified 250-ml shake flasks were used, each with four additional ports in the headspace. These ports are necessary for supplying gas, purging exhaust gas, inoculating the culture, and connecting an electrochemical oxygen sensor located in the headspace of the flasks. The aeration of 10 ml min^{-1} per flask is adjusted by a thermal mass flow controller to guarantee similar aeration conditions as in normal shake flasks with a cotton plug (28, 29). To determine the OTR, the valves for gas inlet and outlet for each flask were periodically closed (5 min closed and 15 min open). Due to the interruption of the air supply and the continued respiration activity of the microorganisms, the oxygen partial pressure in the headspace of the flasks decreases while the carbon dioxide partial pressure decreases. The partial pressures are monitored by an oxygen sensor and a total pressure sensor. Based on the slope of the decrease of the oxygen partial pressure over time, the OTR is calculated. CTR can be calculated by the difference of the total pressure and the oxygen partial pressure, and RQ is calculated as the ratio of CTR/OTR (27). During the experiments the temperature was kept constant at 30°C by placing the RAMOS device in an incubation hood. Commercial versions of RAMOS are available from Kuhner (Birsfelden, Switzerland) or Hitech Zang (Herzogenrath, Germany). This device has already been intensively in other investigations to study and characterize microbial systems (30–32). Off-line sampling was conducted with the help of parallel 250-ml unbaffled shake flasks running simultaneously under identical conditions (30°C; 50-mm shake diameter) as the RAMOS cultivations in a ISF-4-W Kuhner shaker (Birsfelden, Switzerland). Each sample flask was used for only one sampling in order to avoid a change of the flask filling volume. For the preculture, mannitol medium was inoculated with *G. oxydans* cells from a glycerol stock and incubated overnight at 30°C. The main culture was inoculated with the preculture to an OD_{600} of 0.1. Nonlimiting oxygen supply was achieved by using 10 ml of mannitol medium and a shaking frequency of 350 rpm. For oxygen-limiting conditions, different volumes (20 to 60 ml) of mannitol medium were used with a shaking frequency of 200 rpm. Samples of the cultures grown in parallel to the RAMOS cultures were taken at selected time points and analyzed regarding pH, optical density, and sugar concentrations.

H⁺/O measurements. For determination of H⁺/O ratios, 50 ml of mannitol medium (*G. oxydans*) or LB medium (*E. coli*) was inoculated to an OD_{600} of 0.3. Cells were grown to an OD_{600} of 1.5 at 30°C (*G. oxydans*)

or 37°C (*E. coli*) at 140 rpm in baffled 500-ml shake flasks (three baffles, 1.5 by 5 cm each) in a Minitron incubation shaker (Infors HT, Basel, Switzerland). Cells were harvested by centrifugation at $10,414 \times g$ for 3 min at 4°C and washed twice with 25 ml of 200 mM KCl each. Cells were resuspended in 1 ml of 200 mM KCl and centrifuged for 5 min at $16,100 \times g$ and 4°C. The supernatant was discarded, and the cells were resuspended in 200 μl of 200 mM KCl. Fifty microliters of the cell suspension was added into a closed reaction vessel containing 2.5 ml of an anaerobic buffer composed of 1 mM morpholineethanesulfonic acid (MES), pH 6.0, 200 mM KCl, 50 mM potassium thiocyanate (KSCN), 10 mM mannitol, and 24 $\mu\text{g ml}^{-1}$ valinomycin, leading to a final OD_{600} of about 7 (33). The vessel was thermostatted at 30°C and kept anaerobic by a flow of argon. The cell suspension in the vessel was continuously mixed with a magnetic stirrer. The pH of the medium was recorded using a micro-pH electrode (Mettler Toledo, Gießen, Germany) in combination with a Seven Easy pH meter (Mettler Toledo, Gießen, Germany) and the software LabX direct pH (Mettler Toledo, Gießen, Germany). After the pH remained constant, defined volumes (12.5 μl to 50 μl) of air-saturated 150 mM KCl solution were added. The solubility of O₂ in 150 mM KCl at 30°C was 223 μM (corresponding to 0.223 nmol O₂/ μl or 0.446 ng-atoms of O/ μl). Calibration of the pH electrode was performed using 2.5 μl , 5 μl , and 10 μl of an anaerobic 5 mM HCl solution (5 μl of 5 mM HCl is equivalent to 25 ng-ions of H⁺). The maximal acidification observed after addition of air-saturated KCl was used for calculation of the H⁺/O ratio without correction for the proton influx into the cells that occurred during the acidification (34). The determined H⁺/O ratios therefore represent minimal values. Doubling of the concentrations of valinomycin or thiocyanate did not significantly affect the measured H⁺/O values, indicating that proton translocation was not limited by insufficient charge compensation.

Respirometry. A respirometer with an electrochemical oxygen electrode was used to characterize the oxygen affinity of the reference strain and the deletion mutants. Two milliliters of an overnight culture was centrifuged (5 min at $10,000 \times g$ at room temperature), and the supernatant was removed. The cell pellet was resuspended in fresh mannitol medium to obtain a cell suspension with an OD_{600} of 15. To calibrate the respirometer, 4.9 ml of mannitol medium was added to the measuring chamber, which was constantly mixed by a magnetic stirrer. Air saturation of the medium was achieved via surface aeration until a constant value was reached. Then, 100 μl of the concentrated cell suspension was transferred to the measuring chamber, and the chamber was immediately closed. Bubbles inside the measuring chamber had to be avoided since they would act as an oxygen source during the measurement. The voltage corresponding to the dissolved oxygen tension (DOT) was recorded continuously by a computer. The oxygen solubility of the mannitol medium at 22.5°C was 244 μM , calculated as described previously (35–37).

Determination of substrate and product concentrations by HPLC analysis. One milliliter of culture was centrifuged for 5 min at $10,000 \times g$, and the supernatant was filtered through a 0.2- μm -pore-size polyvinylidene difluoride (PVDF) filter (Carl Roth, Karlsruhe, Germany) prior to HPLC analysis. Mannitol and fructose were quantified using a Carbohydrate Pb²⁺ column (300 by 8 mm) including a precolumn (CS-Chromatographie Service, Langerwehe, Germany) at 80°C in the experiments accompanying RAMOS cultivations. H₂O was used as eluent at a flow rate of 0.6 ml min^{-1} . Retention times for fructose and mannitol were 20 and 30 min, respectively. 5-Ketofructose as well as fructose and mannitol (complementation experiments) were quantified with a Rezex RCM-Monosaccharide 300- by 7.8-mm column (Phenomenex, Aschaffenburg, Germany) at 60°C using H₂O as the eluent at a flow rate of 0.6 ml min^{-1} . The above-mentioned metabolites were detected by a refractive index detector. Retention times for 5-ketofructose, fructose, and mannitol were 13.47, 15.23, and 19.95 min, respectively. Calibration curves were made using a series of standards ranging from 0 to 10 g liter⁻¹ mannitol, 0 to 15 g liter⁻¹ fructose, and from 0 to 5 g liter⁻¹ for 5-ketofructose.

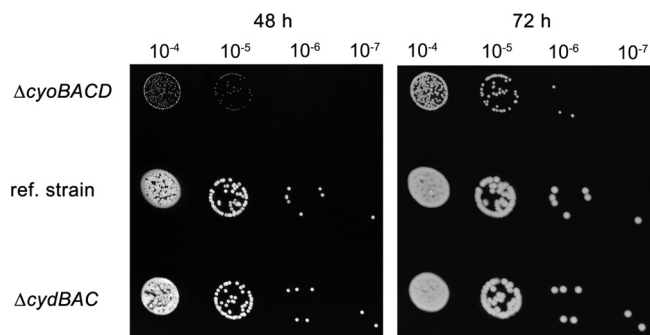


FIG 2 Growth of the indicated *G. oxydans* strains on agar plates containing mannitol medium with 1.5% agar. The plates were incubated for 48 h or 72 h at 30°C. A preculture was grown in 20 ml of mannitol medium for 24 h. After adjusting the OD₆₀₀ of all precultures to 1, the suspension was diluted 10⁻⁴- to 10⁻⁷-fold in mannitol medium. Ten microliters of each dilution was dropped on the agar plates. Three biological replicates were performed with comparable results, and one representative experiment is shown here. ref, reference.

DNA microarrays. For DNA microarray analysis of strain *G. oxydans* $\Delta upp \Delta cyoBACD$ versus the reference strain *G. oxydans* Δupp , cells were cultivated in baffled shake flasks with mannitol as the carbon source and harvested at an OD₆₀₀ of 1.5. RNA extraction, cDNA labeling and DNA microarray analysis were performed as described previously (38).

Microarray data accession number. The DNA microarray data have been deposited in NCBI's Gene Expression Omnibus and are accessible through GEO series accession number GSE47782.

RESULTS

Construction of *G. oxydans* mutants lacking terminal oxidases.

In order to investigate the role of the two terminal oxidases in *G. oxydans*, deletion mutants lacking either the *cydAB* genes for cytochrome *bd* oxidase or the *cyoBACD* genes for cytochrome *bo*₃

oxidase were constructed. To obtain the *cyd* deletion mutant, 12 fluorouracil-resistant colonies obtained after the second homologous recombination event were analyzed by PCR, and three of them were found to have the *cydAB* deletion. *G. oxydans* $\Delta upp \Delta cydAB$ clone 1 was used for further experiments. To identify a strain lacking cytochrome *bo*₃ oxidase, more than 500 fluorouracil-resistant colonies had to be analyzed after the second homologous recombination event, and only one of them contained the desired *cyoBACD* deletion. The strain was named *G. oxydans* $\Delta upp \Delta cyoBACD$. The 100-fold difference in the appearance of *cydAB* and *cyoBACD* mutants already indicates that cytochrome *bo*₃ oxidase is important for growth.

Growth and respiration activity of terminal oxidase mutants. Growth experiments on agar plates containing mannitol medium revealed a severe growth defect of strain *G. oxydans* $\Delta upp \Delta cyoBACD$ as the colonies grew much more slowly and reached a much smaller size than those of the reference strain. In contrast, strain *G. oxydans* $\Delta upp \Delta cydAB$ behaved like the reference strain (Fig. 2). Growth and respiration activity of the terminal oxidase deletion mutants were analyzed in more detail using RAMOS and shake flask cultivations, both under oxygen-excess and oxygen-limited conditions (Fig. 3 and 4 and Table 2). The results obtained confirmed the findings obtained on agar plates. The final OD₆₀₀ values reached by *G. oxydans* $\Delta upp \Delta cyoBACD$ were 39 to 43% lower than those of the wild type, whereas the $\Delta upp \Delta cydAB$ strain reached 100 to 103% of the wild-type level.

Under oxygen excess, *G. oxydans* Δupp and *G. oxydans* $\Delta upp \Delta cydAB$ reached their maximal OTRs of about 37 mmol liter⁻¹ h⁻¹ after 7 h. The time points of maximal OTR correlated with the time points at which more than 60% of mannitol had been consumed, which is predominantly oxidized in the periplasm to fructose (5). *G. oxydans* $\Delta upp \Delta cyoBACD$ reached a maximal OTR of

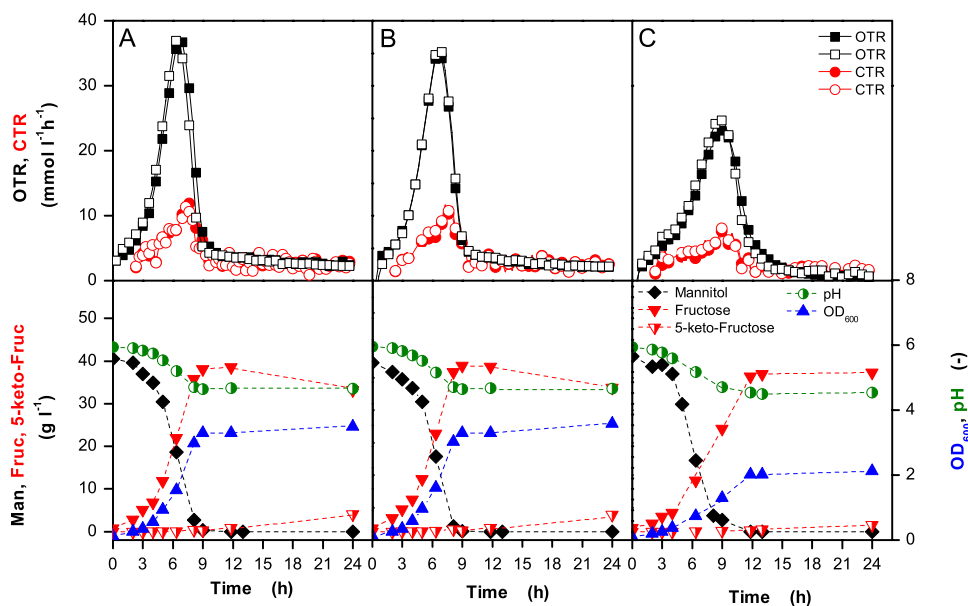


FIG 3 Growth of *G. oxydans* Δupp (A), *G. oxydans* $\Delta upp \Delta cydAB$ (B), and *G. oxydans* $\Delta upp \Delta cyoBACD$ (C) in mannitol medium at 30°C under oxygen excess. The 250-ml flasks contained 10 ml of medium and were shaken at 350 rpm with a shaking diameter of 50 mm. In the upper panels, the oxygen transfer rates (OTRs) and the carbon dioxide transfer rates (CTRs) of two independent cultures are shown. In the lower panels, the OD₆₀₀, the pH of the medium, and the concentrations of mannitol (Man), fructose (Fruc), and 5-keto-fructose (5-keto-Fruc) are shown. RAMOS experiments were conducted as duplicates and showed excellent reproducibility.

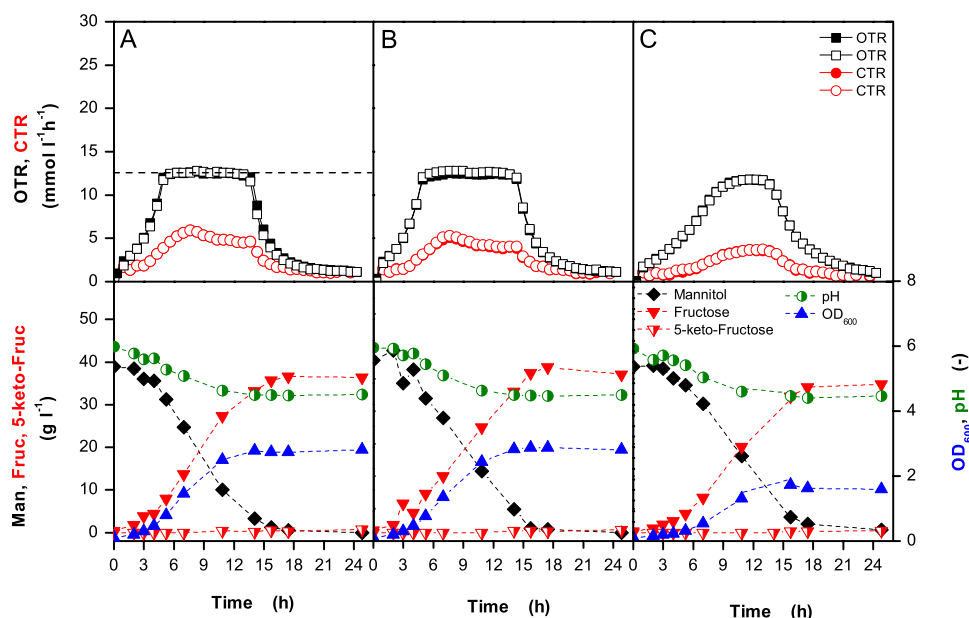


FIG 4 Growth of *G. oxydans* Δupp (A), *G. oxydans* $\Delta upp \Delta cydAB$ (B), and *G. oxydans* $\Delta upp \Delta cyoBACD$ (C) in mannitol medium at 30°C under oxygen limitation. The 250-ml flasks contained 40 ml of medium and were shaken at 200 rpm with a shaking diameter of 50 mm. In the upper panels, the oxygen transfer rates (OTRs) and the carbon dioxide transfer rates (CTRs) of two independent cultures are shown. In the lower panels, the OD_{600} , the pH of the medium, and the concentrations of mannitol (Man), fructose (Fruc), and 5-keto-fructose (5-keto-Fruc) are shown. RAMOS experiments were conducted as duplicates and showed an excellent reproducibility. In panel A the maximal oxygen transfer capacity is illustrated as an example by a dashed horizontal line.

24 mmol liter⁻¹ h⁻¹ after 9 h and had a 27% reduced growth rate. The specific maximal oxygen consumption rate of the *cyo* deletion mutant was reduced by 25% compared to that of the reference strain, whereas that of the *cyd* deletion mutant was almost identical to that of the reference strain. The specific maximal CO₂ production rate of the *cyo* deletion mutant was decreased by 16% compared to the reference strain, whereas that of the *cyd* deletion mutant was decreased by 8%. After complete consumption of mannitol, the OTRs of all three strains decreased to 2 to 5 mmol liter⁻¹ h⁻¹, showing that only a small fraction of fructose was either oxidized in the periplasm to ketofructose or in the cyto-

plasm to CO₂ and acetate. During the cultivations, the pH dropped from 6 to 4.5, presumably due to acetate formation (5).

The results of the oxygen-limited cultivations of the *G. oxydans* Δupp , $\Delta upp \Delta cydAB$, and $\Delta upp \Delta cyoBACD$ strains are shown in Fig. 4 and Table 2. In the case of the reference strain and the *cyd* deletion mutant, the OTR initially increased and then abruptly reached a plateau when oxygen became limiting. The height of this plateau, known as maximum oxygen transfer capacity, represents the maximum OTR provided by the bioreactor under these operating conditions. As soon as the maximum oxygen transfer capacity is reached, the microorganisms are oxygen limited. For the *G.*

TABLE 2 Growth-related parameters and respiration activities obtained during cultivation of the indicated *G. oxydans* strains under a nonlimiting oxygen supply and under oxygen limitation^a

Condition and <i>G. oxydans</i> strain	μ_{max} (h ⁻¹)	OD_{600}	OTR _{max} (mM h ⁻¹)	Specific maximal O ₂ consumption rate (μmol min ⁻¹ mg protein ⁻¹) ^b	Total O ₂ consumption (mM) ^c	CTR _{max} (mM h ⁻¹)	Specific maximal CO ₂ production rate (μmol min ⁻¹ mg protein ⁻¹) ^b	Total CO ₂ formed (mM) ^c
Nonlimiting oxygen supply								
Δupp strain	0.40	3.49	37	2.08 (100)	194	12	0.62 (100)	100
$\Delta upp \Delta cydAB$ strain	0.41	3.58	36	2.05 (99)	183	11	0.57 (92)	91
$\Delta upp \Delta cyoBACD$ strain	0.30	2.12	24	1.56 (75)	154	8	0.52 (84)	66
Oxygen limitation								
Δupp strain	0.38	2.81	13	0.93 (100)	162	6	0.38 (100)	66
$\Delta upp \Delta cydAB$ strain	0.37	2.81	13	0.93 (100)	171	5.5	0.35 (92)	65
$\Delta upp \Delta cyoBACD$ strain	0.23	1.59	12	0.76 (82)	142	3.5	0.22 (58)	44

^a Dry cell weight (DCW) per liter was obtained using following empirical correlation: DCW = 0.1675 ln (OD_{600}) + 0.4684 ($R^2 = 0.9593$); protein was calculated as 50% of DCW. Mean values of two independent cultures are shown which deviated by less than 5%. max, maximum.

^b Calculated using the OD_{600} values at the time of maximal OTR and CTR, respectively. Values in parentheses are percentages for consumption and production relative to the corresponding values for the Δupp strain, set at 100%.

^c These values refer to an initial mannitol concentration of 40 g liter⁻¹ (220 mM) and were obtained by integrating the OTR and CTR curves in Fig. 3 and 4 over time.

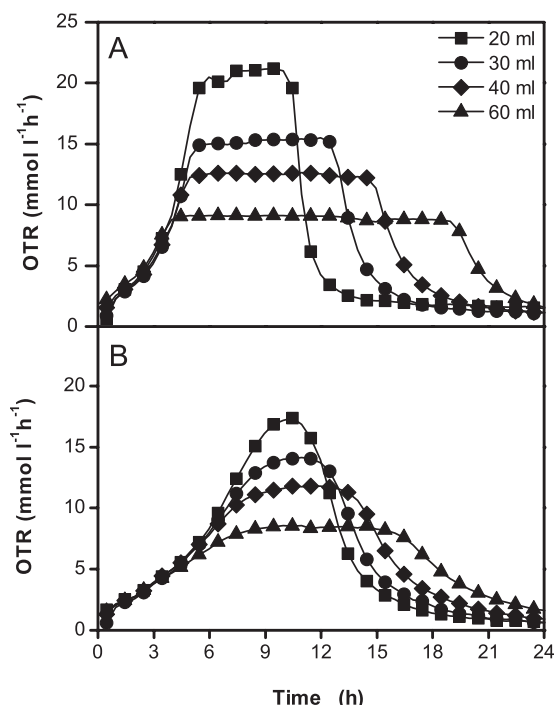


FIG 5 Comparison of OTRs of strains *G. oxydans* Δupp (A) and *G. oxydans* $\Delta upp \Delta cyoBACD$ (B) in mannitol medium at 30°C under oxygen-limited conditions. The 250-ml unbaffled flasks contained 20 ml, 30 ml, 40 ml, or 60 ml of medium and were shaken at 200 rpm with a shaking diameter of 50 mm. The maximal OTR values obtained for the reference strain were 21.0, 15.0, 12.5, and 9.0 mmol liter⁻¹ h⁻¹, and those for the *cyo* deletion mutant were 18.5, 14.5, 11.5, 8.5 mmol liter⁻¹ h⁻¹, respectively.

oxydans Δupp and $\Delta upp \Delta cydAB$ strains, this plateau remained constant over several hours until mannitol was completely oxidized, and then the OTR decreased again. In the case of the *cyo* deletion mutant, the OTR kinetics was different as the OTR was diminished long before the cells reached the maximum oxygen transfer capacity. As a consequence, there was no abrupt transition from oxygen excess to oxygen limitation, and the plateau phase was much shorter. To further investigate this phenomenon, RAMOS experiments were conducted with the reference strain and the *cyo* deletion mutant using various medium volumes (20 to 60 ml) to achieve different degrees of oxygen limitation (Fig. 5). In all cases, the OTR kinetics of the reference strain and the *cyo* deletion mutant were comparable to those shown in Fig. 4. Thus, the reference strain and the *cyd* deletion mutant are capable of high respiration rates also when oxygen becomes limiting, whereas the *cyo* deletion mutant lacks this ability. This suggests that cytochrome *bo*₃ oxidase has a high-oxygen affinity, whereas cytochrome *bd* oxidase has a low-oxygen affinity. Similar results as shown here for mannitol-grown cells were also observed for glucose-grown cells (data not shown), confirming that they are not dependent on the carbon source.

Respirometry. To further analyze the respiration activities of the reference strain and the terminal oxidase deletion mutants, oxygen consumption was measured in a respirometer (Fig. 6). Oxygen consumption by the strain lacking cytochrome *bo*₃ oxidase occurred significantly more slowly than that of the reference strain and the *bd* oxidase deletion mutant. Comparison of the slope of DOT curves, which is equivalent to the oxygen transfer

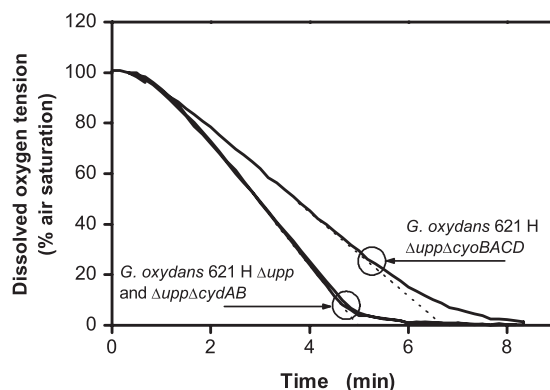


FIG 6 Oxygen consumption of *G. oxydans* Δupp , *G. oxydans* $\Delta upp \Delta cyoBACD$, and *G. oxydans* $\Delta upp \Delta cydAB$ in a respirometer with an electrochemical oxygen electrode. Experimental conditions were as follows: complex medium with 40 g liter⁻¹ mannitol; room temperature. The OD₆₀₀ was adjusted to 0.3 for all strains. The circles show the dissolved oxygen tension where the oxygen consumption rate started to decrease. The experiments were conducted in triplicate with comparable results, and one experiment for each strain is shown here.

rates, demonstrated a 30% lower value for the *cyo* deletion mutant (2.3 ± 0.06 mM h⁻¹ for the $\Delta upp \Delta cyoBACD$ strain, 3.55 ± 0.11 mM h⁻¹ for the $\Delta upp \Delta cydAB$ strain, and 3.26 ± 0.03 mM h⁻¹ for the Δupp strain). The oxygen consumption rates of the reference strain and the *cyd* deletion mutant decreased when DOT ran below ~10%, whereas oxygen consumption rate of the *cyo* deletion mutant had already decreased when the DOT ran below 25%. Based on the data shown in Fig. 6, half-maximum oxygen consumption rates were estimated at 7 μ M oxygen for the Δupp and $\Delta upp \Delta cydAB$ strains and at 21 μ M oxygen for the $\Delta upp \Delta cyoBACD$ strain. These values are roughly comparable to the K_M values for oxygen of purified *bo*₃ oxidase (2 to 3 μ M) and purified *bd* oxidase (21 μ M) as determined from the deoxygenation kinetics of oxymyoglobin (13).

H⁺/O ratio measurements. The deletion mutants constructed in this work allowed us to determine the H⁺/O ratios in the presence of only one terminal oxidase. The experiments were performed with mannitol as an energy source, which is oxidized in the periplasm by the major polyol dehydrogenase SldAB to fructose, with concomitant reduction of ubiquinone. The average H⁺/O ratio of the reference strain *G. oxydans* Δupp containing both terminal oxidases determined from 10 independent experiments was 1.26 ± 0.06 (Table 3). Control experiments under identical conditions (30°C, pH 6) using *E. coli* DH5 α F' showed an average H⁺/O ratio of 3.04 ± 0.11 , indicating that the low values measured for *G. oxydans* were not an artifact of the experimental setup. The *G. oxydans* $\Delta upp \Delta cydAB$ strain lacking cytochrome *bd* oxidase showed a H⁺/O ratio (1.31 ± 0.16) comparable to that of the reference strain, which agrees with the unimpaired growth of the mutant under the tested conditions. The $\Delta upp \Delta cyoBACD$ mutant, on the other hand, showed a 56% reduction of the H⁺/O ratio (0.56 ± 0.11) compared to the reference strain, indicating that cytochrome *bo*₃ oxidase is predominantly responsible for respiratory proton translocation in *G. oxydans*. The low H⁺/O ratio of the *cyo* deletion mutant correlates with its poor growth on agar medium and in shake flask experiments.

Complementation of terminal oxidases. For complementation studies, the genes *cyoBACD*, *cydAB*, and *cydABCD* with their

TABLE 3 H⁺/O ratio of three *G. oxydans* strains and *E. coli* as a reference with mannitol as the carbon source

Strain	H ⁺ /O ratio at the indicated vol of air-saturated 150 mM KCl solution (no. of expts) ^a			Avg H ⁺ /O ratio
	12.5 μl	25 μl	50 μl	
<i>G. oxydans</i> strains				
Δ <i>upp</i> strain	1.19 ± 0.11 (10)	1.34 ± 0.10 (10)	1.24 ± 0.10 (10)	1.26 ± 0.10
Δ <i>upp</i> Δ <i>cydAB</i> strain	ND	1.31 ± 0.16 (8)	ND	1.31 ± 0.16
Δ <i>upp</i> Δ <i>cyoBACD</i> strain	ND	0.56 ± 0.11 (8)	ND	0.56 ± 0.11
<i>E. coli</i> DH5αF ^b				
	2.89 ± 0.23 (10)	3.16 ± 0.21 (10)	3.05 ± 0.17 (10)	3.04 ± 0.11

^a The H⁺/O ratio measured by the oxygen pulse method. ND, not determined.

^b *E. coli* was used as a control strain for the experimental setup.

native ribosomal binding sites were cloned into the expression vector pBBR1p384, resulting in plasmids pBBRp384-*cyoBACD*, pBBRp384-*cydAB*, and pBBRp384-*cydABCD*, respectively. After transfer of the plasmids into the desired *G. oxydans* strains, growth of the recombinants in mannitol medium was tested. Plasmid-based expression of either *cydAB* or *cydABCD* in the reference Δ*upp* strain and in the Δ*upp* Δ*cydAB* mutant had no influence on the growth properties (data not shown). In contrast, plasmid-based expression of the *cyoBACD* genes led to improved growth (Fig. 7). The Δ*upp* strain carrying pBBRp384-*cyoBACD* showed

an 8% higher growth rate than the Δ*upp* strain carrying pBBRp384 (from 0.39 ± 0.01 h⁻¹ to 0.42 ± 0.00 h⁻¹), and the final OD₆₀₀ was increased by 20% (from 4.05 ± 0.13 to 4.88 ± 0.09). In the Δ*upp* Δ*cyoBACD* mutant strain carrying pBBRp384-*cyoBACD*, the growth rate was increased by 60% compared to the strain carrying pBBRp384 (from 0.27 ± 0.03 h⁻¹ to 0.43 ± 0.00 h⁻¹), and the final OD₆₀₀ increased by 69% (from 2.92 ± 0.05 to 4.93 ± 0.05). The delay observed in Fig. 7 for mannitol oxidation and fructose formation by strain *G. oxydans* Δ*upp*(pBBRp384-*cyoBACD*) compared to the Δ*upp* Δ*cyoBACD*(pBBRp384-*cyoBACD*) strain is probably due to a higher initial mannitol concentration of the former culture.

DISCUSSION

In this study, the roles of the two terminal oxidases of *G. oxydans* 621H, cytochrome *bd* oxidase and cytochrome *bo*₃ oxidase, were investigated. Deletion of the corresponding genes revealed that neither of these oxidases is essential for growth in a mannitol-yeast extract medium but that the *bo*₃ oxidase is of major importance for the build-up of proton motive force and biomass formation.

Shake flask and RAMOS cultivations demonstrated that the absence of cytochrome *bd* oxidase had no influence on growth and respiration activity under either oxygen excess or oxygen limitation conditions. The reference strain and the *bd* oxidase deletion mutant consumed comparable quantities of oxygen (oxygen excess condition, 194 and 182 mM; oxygen limitation condition, 162 and 171 mM) (Table 2). For complete oxidation of 220 mM mannitol to fructose, 110 mM O₂ is required, and the rest is used for oxidation of mannitol or fructose to CO₂ and acetate in the cytoplasm, for partial oxidation of fructose to ketofructose in the periplasm, and for oxidation of components of the yeast extract (Table 2). The strain lacking cytochrome *bo*₃ oxidase showed reduced oxygen consumption (oxygen excess condition, 154 mM; oxygen limitation condition, 142 mM), which is in agreement with the reduced formation of CO₂, 5-ketofructose, and biomass.

The oxygen consumption rates of the *cyo* deletion mutant in the RAMOS and respirometer studies was about 25 to 30% lower than those of the reference strain and the *cyd* deletion mutant. This relatively small reduction is presumably due to an increased synthesis of cytochrome *bd* oxidase in the *cyo* deletion mutant, which was indicated by an increased peak at 630 nm in reduced-minus-oxidized difference spectra of purified membranes of this mutant and by a 3.6- to 5.4-fold increased mRNA level of this mutant and by a 3.6- to 5.4-fold increased mRNA level of the *cydAB* genes (GOX0278-GOX0279) in DNA microarray experiments comparing the mRNA levels of the Δ*upp* Δ*cyoBACD* and Δ*upp* strains (see Table S1 and Fig. S1 in the supplemental mate-

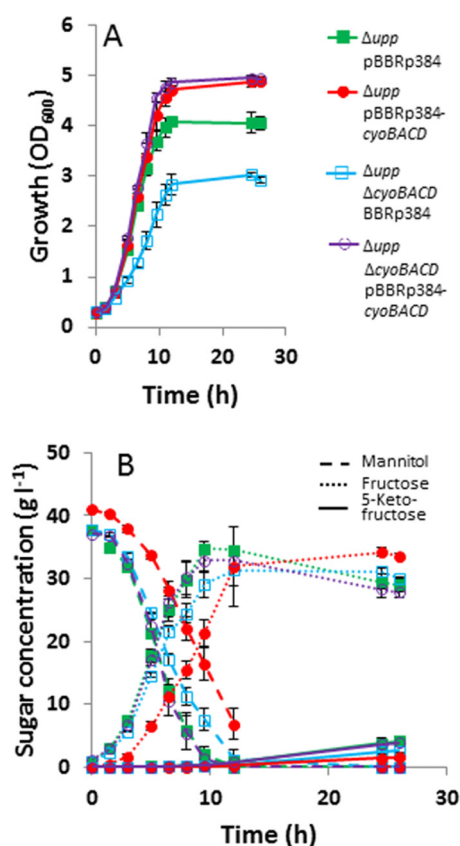


FIG 7 Growth (A), substrate consumption and product formation (B) of the *G. oxydans* Δ*upp*(pBBRp384), Δ*upp*(pBBRp384-*cyoBACD*), Δ*upp* Δ*cyoBACD* (pBBRp384), and Δ*upp* Δ*cyoBACD*(pBBRp384-*cyoBACD*) strains. The strains were cultivated in 100-ml baffled shake flasks with mannitol medium at 30°C and 140 rpm. Mean values and standard deviations of three independent cultures are shown.

rial). This suggests that synthesis of the *bd* oxidase is increased in the *cyo* deletion mutant and that *G. oxydans* is capable of sensing and responding to a deficiency in its respiratory capacity.

When the RAMOS cultivations were performed under conditions leading to oxygen limitation during growth, the OTR of the *cyo* deletion mutant hardly reached the horizontal plateau that was observed for the reference strain and the *cyd* deletion mutant (Fig. 5). Instead, the OTR of the *cyo* deletion mutant slowly approached the maximal value possible under the chosen conditions. This behavior might be caused by a low-oxygen affinity of cytochrome *bd*, the only remaining terminal oxidase in the *cyo* deletion mutant. Support for this assumption was obtained by the respirometer measurements of the *cyo* deletion mutant, in which the initially linear oxygen consumption rate had already decreased when the dissolved oxygen tension (DOT) fell below 25%, whereas in case of the wild type and the *cyd* deletion mutant, it did not decrease until the DOT fell below 10% (Fig. 6).

Our evidence that cytochrome *bd* oxidase of *G. oxydans* has a significantly lower oxygen affinity than cytochrome *bo*₃ oxidase is in agreement with recent biochemical data. Based on the cyanide insensitivity of *G. oxydans* cytochrome *bd*, Matsushita and co-workers designated this enzyme cyanide-insensitive oxidase (CIO) and the corresponding genes *cioA* and *cioB* instead of *cydA* and *cydB* (12). In a recent study, they purified and characterized the terminal oxidases of *G. oxydans* and, for comparison, cytochrome *bd* of *E. coli* (13). Their results indicated significant differences between CIO and *E. coli* cytochrome *bd*: besides a much lower sensitivity to cyanide (50% inhibitory concentration [IC₅₀] of 118 mM versus 4.2 mM for *E. coli bd*), the CIO enzyme has a higher sensitivity to azide (IC₅₀ of 0.8 mM versus 4.8 mM), an exceptionally high turnover number, and a *K_M* value for oxygen (21 μM) which is 10-fold higher than the one of *E. coli* cytochrome *bd* (2 μM) and about 7-fold higher than the one measured for *G. oxydans* cytochrome *bo*₃ (3 μM). A phylogenetic analysis supported the idea that the cytochrome *bd* oxidase superfamily includes a specific CIO clade with members from the alpha, beta-, and gammaproteobacteria (13). Based on these data, the use of a different designation for members of the CIO clade appears reasonable and will be used by us in future studies.

In agreement with the growth properties of the *G. oxydans cyd* and *cyo* deletion mutants, the absence of cytochrome *bd* oxidase did not affect respiration-driven proton extrusion (H⁺/O ratio of 1.3), whereas the lack of cytochrome *bo*₃ oxidase caused a reduction of more than 50% (H⁺/O ratio of 0.56). That the absence of the non-proton-pumping cytochrome *bd* oxidase did not improve the H⁺/O ratio might be due to a much lower content of the *bd* oxidase than of the *bo*₃ enzyme and to the proposed lower oxygen affinity of the *bd* oxidase, which should favor oxygen reduction by the higher-affinity *bo*₃ oxidase under the experimental conditions of an oxygen pulse. In previous studies, H⁺/O ratios of 1.7 to 2.2 were reported for *G. oxydans* cells supplied with glycerol, glucose, lactate, or ethanol at pH 6 (39). These values are higher than those determined by us, which could be due to the use of other substrates or differences in the experimental conditions.

The H⁺/O ratio of 1.3 measured for *G. oxydans* is more than 2-fold lower than the ratio of 3.0 determined for *E. coli* using a nonoptimized system. In the literature, H⁺/O ratios reported for *E. coli* vary between 3.4 and 4.9 (20, 34, 40). A major difference between the respiratory chains of the two species is the lack of the multisubunit proton-pumping NADH dehydrogenase I (NDH-I)

in *G. oxydans*. However, NDH-I is preferentially synthesized during anaerobic growth in the presence of alternate electron acceptors, whereas during aerobic growth the non-proton-pumping single-subunit NDH-II is the dominant NADH:Q oxidoreductase (41). Therefore, it is unclear to what extent NDH-I (H⁺/e⁻ stoichiometry of 2; [42]) contributes to the H⁺/O ratios measured for *E. coli*. For cytochrome *bo*₃ oxidase, a H⁺/e stoichiometry of 2, and therefore a H⁺/O ratio of 4, can be assumed (11), and for cytochrome *bd* oxidase a H⁺/e stoichiometry of 1 and a H⁺/O ratio of 2 are assumed (43, 44). As the *bd* oxidase was not relevant for growth of *G. oxydans* and proton translocation under the conditions used in our study, a H⁺/O ratio approaching 4 might be expected for *G. oxydans*. However, both our results as well as those presented by Matsushita et al. (39) are much lower than a value of 4. There are a number of very speculative hypotheses to explain the low H⁺/O ratios determined for *G. oxydans*. (i) The cytoplasmic membrane of *G. oxydans* might be leakier for protons than the one of *E. coli*, causing a non-energy-conserving backflow of protons into the cells (45). (ii) The respiratory chain could involve a reverse electron transfer coupled to an influx of protons (46). (iii) Cytochrome *bo*₃ oxidase might not function as a primary proton pump but as a Na⁺ pump, as has been described for cytochrome *bo*₃ oxidase of *Vitreoscilla* sp. (47, 48). In this context it is interesting that *G. oxydans* possesses two different F₁F_o-type ATP synthases (49), one of which might use Na⁺ as coupling ion (8, 38). The comparative DNA microarray analysis of the *cyo* deletion mutant versus the reference strain showed an upregulation of genes (GOX2167 to GOX2175) coding for the putative Na⁺-dependent F₁F_o-ATPase (see Table S1 in the supplemental material).

Surprisingly, complementation of the *G. oxydans cyo* deletion mutant with the expression plasmid pBBR1p384-*cyoBACD* resulted not only in a reversal to wild-type-like growth but also to an increased growth rate and an increased final OD₆₀₀. A comparable growth behavior was observed when the Δ *upp* reference strain was transformed with this plasmid (Fig. 7). An increased cell yield was also observed for an *E. coli* mutant deficient in the *bo*₃ and the *bd*-I oxidase when the *bo*₃ oxidase gene was overexpressed by a plasmid (20). The possibility that an increased level of *bo*₃ oxidase in *G. oxydans* causes a shift of the electron flux from the non-proton-pumping *bd* oxidase to the proton-pumping *bo*₃ oxidase appears unlikely as the *G. oxydans cyd* deletion mutant did not show improved growth although only the *bo*₃ oxidase remained as a terminal oxidase. Another explanation for the improved growth is the assumption that the oxidative capacity of *G. oxydans* under the experimental conditions used is limited by the activity of the *bo*₃ oxidase and can be increased by its overproduction. A limitation of oxygen consumption by the activity of the terminal oxidases was recently reported for membranes of a *G. oxydans* strain with an increased membrane-bound glucose dehydrogenase activity (50). Although the major polyol dehydrogenase SldAB responsible for mannitol oxidation to fructose was not overproduced in our strain, its activity might be high enough to satisfy an increased capacity for oxygen reduction due an elevated level of *bo*₃ oxidase. In addition, the oxidation of components of the yeast extract can also contribute to the electron flux to the *bo*₃ oxidase. An increased rate of oxygen reduction by the *bo*₃ oxidase is coupled to an increased rate of proton motive force generation and oxidative phosphorylation, which can explain the increased growth rate and maybe also the increased cell yield. Although additional studies are required to clarify the positive effect of *bo*₃ overproduction, the

result shows that respiratory chain components are a promising starting point for further optimization of *G. oxydans* for its use in biotechnological applications. For the development of strains with a higher biomass yield, studies are planned that are directed at the repair of defective metabolic pathways by genomic integration of heterologous genes, such as succinate dehydrogenase, and at an increased cytoplasmic rather than periplasmic metabolism of the carbon source by deleting suitable membrane-bound dehydrogenases. If these approaches are successful, the possibilities for using *G. oxydans* as a broadly applicable host for oxidative biotransformations in industry will be considerably improved.

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