

Optimization of Nutrient Requirements and Culture Conditions for the Production of Rhamnolipid from *Pseudomonas aeruginosa* (MTCC 7815) using *Mesua ferrea* Seed Oil

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Abstract Environmental awareness has led to a serious consideration for biological surfactants and hence non-edible vegetable oils may serve as a substitute carbon source for bio-surfactant production (rhamnolipid) which might be an alternative to complex synthetic surfactants. There are reports of rhamnolipid production from plant based oil giving higher production than that of glucose because of their hydrophobicity and high carbon content. Therefore the contribution of non-edible oil such as *Mesua ferrea* seed oil could serve as a good carbon source for rhamnolipid production. Moreover the use of rhamnolipid production from non-edible plant based seed oil has not been reported elsewhere. The present work focus on the optimal production of rhamnolipid by considering both micro and macro nutrients and culture conditions using response surface methodology. The study observes that micronutrients play a significant role in rhamnolipid production from *Pseudomonas aeruginosa* (MTCC 7815). The investigation results with the statistically optimize parameters able to produce a higher rhamnolipid production and this methodology could be used to optimize the nutrients requirements and culture conditions. The present findings would assist in bioremediation of crude oil contaminated ecosystems.

Keywords Rhamnolipid · Non-edible oil · Response surface methodology · Carbon source

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Introduction

Environmental awareness has led to a serious circumstance realizing biological surfactants as an alternative to synthetic surfactants [1]. Biosurfactants have higher specificity, low toxicity, higher biodegradability, stability at extreme pH, salinity and temperature compared to synthetic surfactants. Their unique structures provide unique properties that lacks in commercial surfactants [2]. Moreover, it has application in petroleum industry which includes enhanced oil recovery (EOR), bioremediation and waste treatment to remove hazardous materials, pharmaceutical-cosmetics formulas, agriculture, food processing industries, detergents, laundry supplies and paint industries [3–6]. Recently, biosurfactants have received much attention in nanobiotechnology too [7, 8].

Despite their potential applications, they are not employed extensively in industry because of its high production cost associated with inefficient methods for product recovery and expensive substrates that limit their commercialization. The use of cheap raw substrates is an important factor for the overall economic recovery as they account for 50 % of the total production cost [9, 10]. Also, the possible way for cost reduction is the use of an alternate substrates such as agro-industrial wastes which include molasses, whey milk, distillery waste, olive oil mill effluent, soap stock, cassava waste, potato substrates etc. [10, 11].

Alternate carbon substrates such as palm seed oil, olive oil, sunflower oil, safflower oil, canola oil, soybean oil and corn oil were evaluated for rhamnolipid production [12–18]. There are reports of rhamnolipid production from plant oil which is much higher than that of glucose because of their hydrophobicity and high carbon content per weight [10]. However, based on cost and global food supply, the use of food-grade oils for producing rhamnolipid is economically not remarkable. This may cause imbalance and depletion of

food sources. It is both extravagant and unethical to use food source for rhamnolipid production. Besides, the recent food storage crisis, limited land availability for crop cultivation and food industry with increasing food demand have persuaded the price of edible plant based oil to increase [19]. In this perspective, non-edible vegetable oils may be an alternate substrate for rhamnolipid production. Therefore, contributing non-edible oils such as *Mesua ferrea* seed oil could be a good carbon source for producing rhamnolipid. *Mesua ferrea* (Family: *Calophyllaceae*) is a slow-growing tree confined mainly to the wet and tropical parts of South-East Asia [20]. *Mesua ferrea* seed oil is typical triacylglycerols, consists of fatty acid and glycerol moieties. The major composition of fatty acids in its oil is myristic acid (2.13 %), palmitic acid (10.87 %), linoleic acid (13.68 %), oleic acid (55.93 %), stearic acid (14.19 %) and arachidic acid (2.92 %) [21].

Till date there are no reports for the use of non-edible *Mesua ferrea* seed oil for rhamnolipid production (Supplementary material Figs. S1, S2, S3, S4). It is easy to extract from the seed and available throughout the year. The present work aims to optimize the factors (nutrition and culture conditions) directly responsible for rhamnolipid production using statistical designs and response surface methodology (RSM) for higher yield. RSM is used in various experiments for optimization of products such as bacterial medium composition [22], enzymatic activity [23, 24] algal growth [25] etc.

A few works on synthesis and rhamnolipid production from *Pseudomonas aeruginosa* was reported earlier [26–29] however we are reporting for the first time the optimal production of rhamnolipid from *Mesua ferrea* seed oil. The present finding would assist in bioremediation of crude oil contaminated ecosystems and since rhamnolipid is known to be stable at extreme condition it will help in microbial enhanced oil recovery process (MEOR).

Materials and Method

Microorganism

Professor B. K. Konwar, Department of Molecular Biology and Biotechnology, Tezpur University, Assam, India provided the *Pseudomonas aeruginosa* (MTCC 7815) used in the present investigation. The strain was maintained in nutrient agar slants and plates with proper sub-culturing at an interval of 30 days (Supplementary material Fig. S5). The strain was preserved in 50 % glycerol and stored at -80°C for future work.

Culture Conditions

The inoculum was prepared using bacterial cells transferred from the storage culture to a test tube containing 10 ml of the nutrient broth and incubated at 37°C in an orbital incubator

shaker at 180 rpm. The optical density of bacterial suspension was adjusted to 0.65×10^8 cfu/ml. 1.0 ml of the culture was inoculated into a 250 ml Erlenmeyer flask containing 100 ml of mineral salt medium (MSM).

The MSM (g/l) consists of: 5.0 g urea, 5.0 g $(\text{NH}_4)_2\text{SO}_4$, 4.8 g Na_2HPO_4 , 4.75 g KH_2PO_4 , 1.0 g $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$, 10 mg $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$, 3.6 mg $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$, 4.4 mg $\text{CuSO}_4 \cdot 7\text{H}_2\text{O}$, 9.0 mg $\text{MnSO}_4 \cdot 5\text{H}_2\text{O}$, 7.6 mg H_3BO_3 , 3.6 mg $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$, 3.0 mg MnO_3 and 30 ml of the test carbon source (sterilized by passing through $0.2 \mu\text{m}$ membrane filter) and the volume was adjusted up to 1,000 ml of distilled water.

The initial pH of the broth was adjusted to 6.8 using 6 N HCl and incubated at 37°C for 9 days in an orbital incubator shaker at 180 rpm. Cell growth was monitored by measuring the protein content [30] and the increase in biomass was monitored by gravimetric method [31] continuously at an interval of 12 h for 9 days.

Oil Samples

Mesua ferrea seed oil (Supplementary material Fig. S4) was extracted using petroleum ether in a Soxhlet apparatus. The solvent part was evaporated under vacuum at 40°C in a rotary evaporator (Eyela, CCAS-1110, Tokyo, Rikakikai Co. Ltd.). The extracted oil was used in the culture medium as the sole source of carbon and energy. The physical and chemical characteristics of *Mesua ferrea* seed oil is shown in Table 1 as reported by Sayeed et al. [21].

Extraction of Rhamnolipid

The bacterial culture was centrifuged at $12,000 \times \text{rpm}$ for 20 min at 4°C and the bacterial cell mass was removed. Also, the unused vegetable oil remained in the supernatant was removed with the help of a separating funnel. The pH of the culture supernatant was adjusted to 2 using 6 N HCl and kept overnight at 4°C to precipitate the rhamnolipid. The precipitate was harvested by centrifugation at $10,000 \times \text{rpm}$ for 20 min at the same temperature. The precipitate was further extracted thrice with ethyl acetate. The organic phase was collected and dried in a rotary evaporator (Eyela, CCAS-1110, Tokyo, Rikakikai Co. Ltd.) to remove the solvent (Supplementary material Fig. S6). Further, the viscous honey-coloured residue was washed twice with *n*-hexane and the final product was dissolved in ethyl acetate, filtered and concentrated using a rotary evaporator [15].

Statistical Designs

Plackett–Burman Design

A Plackett–Burman experimental design was used to screen the significant variables that influenced the rhamnolipid

Table 1 Physical and chemical characteristics of *Mesua ferrea* seed oil as reported by Sayeed et al. [21]

Physical characteristics	Characteristics value	Chemical characteristics	Characteristics value
Specific gravity at 31 °C	0.929	Iodine value	91.17
Refractive index at 30 °C	1.474	Saponification value	200.82
Solidification point (°C)	−4.0	Saponification equivalent	279.35
Pour point (°C)	−1.3	Acid value	11.87
Cloud point (°C)	5.8	Free fatty acids (%) as oleic	5.96
Flash point (°C)	98	Ester value	188.95
Fire point (°C)	116	Unsaponifiable matter (%)	1.50
Smoke point (°C)	44	Acetyl value	2.70
		Peroxide value	3.58
		Reichert-Meissl value	5.961
		Polenske number	0.7891

production in two levels: −1 for a low-level and +1 for a high-level. In the present investigation, 16 assigned variables were screened in 20 experimental designs. All experiments were carried out in triplicates and the average rhamnolipid production is taken as the response. Such design is practically useful when there are many factors and these prevails uncertainty on nearer setting to the optimum response [32]. Factors under investigation as well as levels of each factor used in the experimental design are shown in Table 2 and the design matrix was illustrated in Table 3. From the results obtained by the Plackett–Burman design, the fitted first order model is

$$Y = \beta_0 + \sum \beta_i \chi_i \tag{1}$$

where Y is the predicted response, β_0 and β_i are constant coefficients, and χ_i are the coded independent variables or factors.

Box–Behnken Design

Response surface method is an empirical modelling scheme used to assess the relationship between experimental variables and their corresponding responses [33]. In the present investigation, Box–Behnken design was used for four independent variables viz. oil (X_1), urea (X_2), $\text{NH}_4(\text{SO}_4)$ (X_3) and phosphates (X_4) (Table 4) The ranges of the four variables studied in the present investigation are shown in Table 5. The factors of the highest confidence levels were represented in three levels, coded −1 for low, 0 for middle and +1 for high.

The actual design matrix of 27 trials of experiments is given in Table 5. Experiments were performed in triplicates and the mean values were taken. The behaviour of the system is explained by the following quadratic equation

$$Y = \beta_0 + \beta_1 \chi_1 + \beta_2 \chi_2 + \beta_3 \chi_3 + \beta_4 \chi_4 + \beta_{12} \chi_1 \chi_2 + \beta_{13} \chi_1 \chi_3 + \beta_{14} \chi_1 \chi_4 + \beta_{23} \chi_2 \chi_3 + \beta_{24} \chi_2 \chi_4 + \beta_{34} \chi_3 \chi_4 \tag{2}$$

Table 2 Media components, culture condition and test levels for Plackett–Burman experiment

Variable	Variable code	Low-level (−1)	High-level (+1)
Culture volume (ml)	X_1	50	25
Culture pH	X_2	5	8
Aeration (rpm)	X_3	150	200
Carbon source (% v/v)	X_4	0.5	3
Urea (%)	X_5	0.05	0.5
$(\text{NH}_4)_2\text{SO}_4$	X_6	0.1	0.5
KH_2PO_4	X_7	0.05	0.5
Na_2HPO_4	X_8	0.05	0.5
$\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$	X_9	0.005	0.1
$\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$	X_{10}	0.001	0.01
$\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$	X_{11}	0	0.001
$\text{CuSO}_4 \cdot 7\text{H}_2\text{O}$	X_{12}	0	0.001
$\text{MnSO}_4 \cdot 5\text{H}_2\text{O}$	X_{13}	0	0.001
H_3BO_3 (M)	X_{14}	0	0.001
$\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$ (M)	X_{15}	0	0.001
MnO_3 (M)	X_{16}	0	0.001

where Y is the predicted response, β_0 model constant; χ_1, χ_2, χ_3 and χ_4 independent variables; $\beta_1, \beta_2, \beta_3$ and β_4 are linear coefficients; $\beta_{12}, \beta_{13}, \beta_{14}$ and β_{23} are cross product coefficients and β_{11}, β_{22} and β_{33} are the quadratic coefficients.

Statistical Analysis of Data

The experimental data obtained were studied and interpreted using Minitab 15 statistical software [34] to estimate the response of the dependent variable. Each experiment was performed in triplicates and the mean values were taken. The quality of fitness of the polynomial model equation was expressed by the coefficient of determination (R^2), and its statistical significance was checked by an F test and the significance of the regression coefficient was tested by a t test.

Results and Discussion

Rhamnolipid Production

The performance of rhamnolipid production with the carbon sources used in the present investigation depicted in Table 5, clearly explained an alternate potential carbon substrate for rhamnolipid production. There are certain reports that mark the type and concentration of carbon substrates which affect the production of rhamnolipid yield [18, 35]. Wei et al. (2005) reported using major types of carbon sources such as carbohydrate, hydrocarbon and vegetable oils for rhamnolipid production by *P. aeruginosa* J4 strain.

Additionally, there are reports of vegetable oils depicting as more effective substrate in rhamnolipid production from *P. aeruginosa* compared to glucose, glycerol and hydrocarbons [15, 35–37]. However, in contrast to these findings *Pseudomonas* EMI strain used by Benincasa et al. [14] showed that carbon sources such as glucose and glycerol were superior over the vegetable oils like olive and soya bean oil when tested with rhamnolipid yield and productivity. This report clearly suggests that the carbon source preference for rhamnolipid production mainly depends on the behaviour of *P. aeruginosa* strain.

Additionally, the authors would like to highlight the point that the use of two nitrogen sources enhanced the rhamnolipid production and yield. In the present investigation a combination of urea and $(\text{NH}_4)_2\text{SO}_4$ (both nitrogen sources) was found to be more productive. This is because *P. aeruginosa* (MTCC 7815) is able to use these nitrogen sources. However, in order to obtain high concentrations of rhamnolipid, it is necessary to have restrained conditions of this macro-nutrient [38]. Also, there are several reports where two different nitrogen sources were used for the rhamnolipid production. Bordoloi and Konwar [39] used $(\text{NH}_4)_2\text{SO}_4$ as inorganic and urea as organic nitrogen sources. While Xia et al. [40] used $(\text{NH}_4)_2\text{SO}_4$ as inorganic and yeast extract as an organic nitrogen sources.

Evaluation of the Factors that Influence Features on Producing Rhamnolipid Biosurfactant

For explanation of various fermentation factors affecting the rhamnolipid production from *P. aeruginosa* (MTCC 7815), the independent variables examined in the Plackett–Burman experiments and their settings are shown in Table 2. Sixteen different variables including medium constituents and fermentation conditions were selected to perform the optimization process. The mean of rhamnolipid production for the different trials are listed in Table 3.

The main effect of each variable was calculated according to the difference between averages of measurements made on high-level (+1) and low-level (−1) of that variable which is shown in Table 3. The variation suggests

the need of the importance for optimized medium to reach for a higher productivity. The data in Table 3 showed a wide variation of rhamnolipid yield ranging from 0.1 to 6.9 g/l out of the 20 experimental run conditions.

Further, the Plackett–Burman experimental design used in the present investigation which is based on the first order model for the analysis of the data (main effects) is graphically represented in Fig. 1. From Fig. 1 and Table 6, i.e. the regression analysis coefficient data suggest that the culture volume (ml), aeration (rpm), carbon source (*Mesua ferrea* seed oil), urea, $(\text{NH}_4)_2\text{SO}_4$, KH_2PO_4 , $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$, $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$, $\text{MnSO}_4 \cdot 5\text{H}_2\text{O}$ and H_3BO_3 affect the rhamnolipid production positively. While, culture pH, Na_2HPO_4 , $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$, $\text{CuSO}_4 \cdot 7\text{H}_2\text{O}$, $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$ and MnO_3 contributed negatively. However the confidence level of the culture volume (ml), $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$, $\text{CuSO}_4 \cdot 7\text{H}_2\text{O}$, $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$ (M) is comparatively low (shown in Fig. 1; Table 6) compared to other factors. Additionally, the complementary factors i.e. aeration (rpm) and culture volume (ml) showed positive affect for rhamnolipid production which might be a major factor for the optimal production. Also from the Pareto chart from Fig. 1, for these physical parameters, the effect of aeration (rpm) contribute to a much higher level compared to culture volume (ml).

The correlation between the sixteen variables and the rhamnolipid production based on the calculated *t* values and confidence level (%) which is shown in Table 6 can be described by the polynomial model:

$$Y_{\text{activity}} = 2.682 + 0.102X_1 - 0.458X_2 + 0.428X_3 + 0.848X_4 + 0.998X_5 + 0.458X_6 + 0.622X_7 - 0.192X_8 + 0.072X_9 + 0.418X_{10} - 0.638X_{11} - 0.138X_{12} + 0.402X_{13} + 0.182X_{14} - 0.122X_{15} - 0.492X_{16}$$

From Table 3, it is depicted that the presence of high-level of urea (0.5 g/l), *Mesua ferrea* seed oil (30 ml/l), KH_2PO_4 (0.5 g/l), $(\text{NH}_4)_2\text{SO}_4$ (0.5 g/l), aeration (200 rpm), $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$ (0.01 g/l), $\text{MnSO}_4 \cdot 5\text{H}_2\text{O}$ (0.001 g/l), H_3BO_3 (0.001 g/l), culture volume (25 ml), $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$ (0.1 g/l) were found to be the most significant factors affecting the rhamnolipid production positively. Whereas low-level of Na_2HPO_4 (0.05 g/l), incubation at low pH (5) and without adding $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$, $\text{CuSO}_4 \cdot 7\text{H}_2\text{O}$, MnO_3 , $\text{FeSO}_4 \cdot 7\text{H}_2\text{O}$ will enhance the rhamnolipid production. To evaluate the accuracy of the Plackett–Burman design, a verification experiment was conducted in triplicate. By applying the Plackett–Burman design, the experiment was carried out with the following composition (g/l): urea, 0.5; KH_2PO_4 , 0.5; $(\text{NH}_4)_2\text{SO}_4$, 0.5; $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$, 0.01; $\text{MnSO}_4 \cdot 5\text{H}_2\text{O}$, 0.001; H_3BO_3 , 0.001; $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$, 0.1; Na_2HPO_4 , 0.05; *Mesua ferrea* seed oil, 30 ml (v/v), while pH is 5 incubated at a constant shaking of 200 rpm and the culture volume of 25 ml. The production of rhamnolipid increases about

Table 3 Randomized Plackett–Burman experimental design for evaluating factors influencing rhamnolipid production (g/l) from *Pseudomonas aeruginosa* (MTCC 7815)

Runs	Physical variables			Carbon source		Nitrogen source		Energy source		Metal ions							Rhamnolipid yield (g/l) ^a
	Culture volume (ml)	Culture pH	Aeration (rpm)	Carbon source (%)	(NH ₄) ₂ SO ₄	Urea (%)	KH ₂ PO ₄	Na ₂ HPO ₄	MgSO ₄ ·7H ₂ O	CaCl ₂ ·2H ₂ O	FeSO ₄ ·7H ₂ O	CuSO ₄ ·7H ₂ O	MnSO ₄ ·5H ₂ O	H ₃ BO ₃ (M)	ZnSO ₄ ·7H ₂ O (M)	MnO ₃ (M)	
1	1	1	-1	-1	-1	-1	1	-1	1	-1	1	1	1	1	-1	-1	0.24
2	-1	1	-1	1	1	1	1	1	-1	-1	-1	1	1	-1	1	1	2.1
3	-1	1	1	1	-1	-1	-1	1	1	-1	1	1	-1	-1	-1	-1	2.5
4	1	-1	1	1	1	1	-1	-1	1	1	-1	1	1	-1	-1	-1	6.9
5	-1	-1	-1	1	1	1	-1	1	1	1	-1	-1	-1	1	1	-1	2.0
6	1	-1	-1	1	1	-1	1	1	1	-1	-1	-1	1	-1	1	-1	5.6
7	-1	1	1	1	1	-1	-1	-1	-1	-1	-1	1	-1	1	-1	1	4.1
8	-1	-1	-1	-1	-1	-1	-1	-1	-1	-1	-1	-1	-1	-1	-1	-1	0.1
9	-1	-1	-1	-1	-1	1	1	1	1	1	1	1	-1	1	1	1	1.5
10	1	-1	1	1	1	1	1	1	1	-1	1	1	-1	1	1	-1	3.5
11	-1	-1	1	1	-1	-1	1	1	1	1	-1	-1	1	1	-1	1	5.2
12	1	1	-1	1	1	1	-1	-1	-1	-1	-1	-1	-1	-1	-1	1	1.4
13	1	1	1	1	-1	-1	1	1	1	1	1	-1	-1	-1	-1	1	1
14	-1	1	1	1	-1	-1	-1	-1	-1	-1	-1	1	1	1	1	-1	1.1
15	1	-1	1	1	-1	-1	-1	-1	-1	-1	1	1	1	1	1	1	2
16	-1	1	1	1	1	1	-1	-1	-1	-1	-1	-1	-1	-1	-1	-1	1.1
17	-1	1	-1	1	1	1	1	1	1	1	1	-1	1	1	1	-1	6.1
18	1	1	1	1	-1	-1	1	1	1	1	-1	-1	-1	-1	-1	-1	3.7
19	1	1	-1	1	1	-1	-1	-1	-1	-1	-1	1	1	1	1	1	3
20	1	-1	-1	-1	-1	-1	-1	1	1	1	1	1	-1	-1	-1	1	0.5

-1 low-level, +1 high-level

^a Rhamnolipid production (g/l) was determined after 9 days of incubation at 37 °C

Table 4 The levels of variables chosen for the Box–Behnken optimization experiment

Variables	Variable code	−1	0	+1
Oil	X_1	5.00	10.00	30
Urea	X_2	0.25	0.75	4
$\text{NH}_4(\text{SO}_4)$	X_3	0.50	1.00	5
Phosphates	X_4	1.00	3.00	8

6.95 g/l which is nearly equals to 2.0 times higher than that produced from basal medium (3.54 g/l). Based on t-statistic value thus obtained (Table 6), concentration of urea in the culture medium was considered to be the highly considerable variable for rhamnolipid production by the bacterial strain.

Optimization of the Rhamnolipid Production by Box–Behnken Design

Plackett–Burman design is based on the first order model and it doesn't show the interaction within the variables and

used for screening and evaluation of important variables that influence the response [41]. Therefore, Box–Behnken design was used as complementary step [42]. In this step of optimization, the level of four independent variables viz. oil (X_1), urea (X_2), $\text{NH}_4(\text{SO}_4)_2$ (X_3) and phosphates (X_4) were further investigated at three different level which is listed in Table 4. While the design matrix of the variables with their experimental results for rhamnolipid production is shown in Table 5. All experiments were carried out in triplicates and the mean values were taken for observation. The experimental results were displayed in the form of three-dimensional response surface plots. Figure 2a showed that gradual increase in urea concentration with the high-level of oil (g/l) that will promote the rhamnolipid production, while further increase in urea concentration beyond the optimum level will decrease rhamnolipid production. According to Fig. 2b, the NH_4SO_4 concentration affects the rhamnolipid production more significantly than urea. Figure 2b also suggest that with the increase in $\text{NH}_4(\text{SO}_4)$ the increase in rhamnolipid production and with the increase in urea concentration the increase in rhamnolipid production.

Table 5 Box–Behnken factorial experimental design, representing the response of rhamnolipid production (g/l) as influenced by oil, urea, $\text{NH}_4(\text{SO}_4)$ and phosphates

Runs	Oil	Urea	$\text{NH}_4(\text{SO}_4)$	Phosphates	Rhamnolipid production	Predicted value
1	−1	−1	0	0	3.01	2.20125
2	1	0	−1	0	2.16	1.64625
3	0	0	0	0	5.67	5.51000
4	1	0	0	1	3.86	3.98583
5	0	0	−1	1	2.06	1.82625
6	0	−1	1	0	3.14	3.35083
7	1	−1	0	0	3.09	2.80458
8	0	0	1	1	6.95	5.94458
9	0	0	0	0	5.74	5.51000
10	−1	0	1	0	3.35	4.52125
11	−1	0	0	−1	2.89	3.16917
12	1	1	0	0	4.37	4.11625
13	0	1	1	0	7.41	6.98250
14	0	0	−1	−1	2.31	2.25292
15	0	0	0	0	5.12	5.51000
16	−1	0	0	1	2.89	3.24750
17	0	1	0	−1	3.25	3.83292
18	0	0	1	−1	5.04	4.21125
19	−1	0	−1	0	2.41	2.18792
20	0	1	0	1	4.24	4.92125
21	−1	1	0	0	5.17	4.39292
22	0	1	−1	0	1.87	2.06417
23	1	0	1	0	4.51	5.38958
24	0	−1	−1	0	1.36	2.19250
25	0	−1	0	−1	2.54	2.51625
26	0	−1	0	1	2.66	2.73458
27	1	0	0	−1	2.71	2.75750

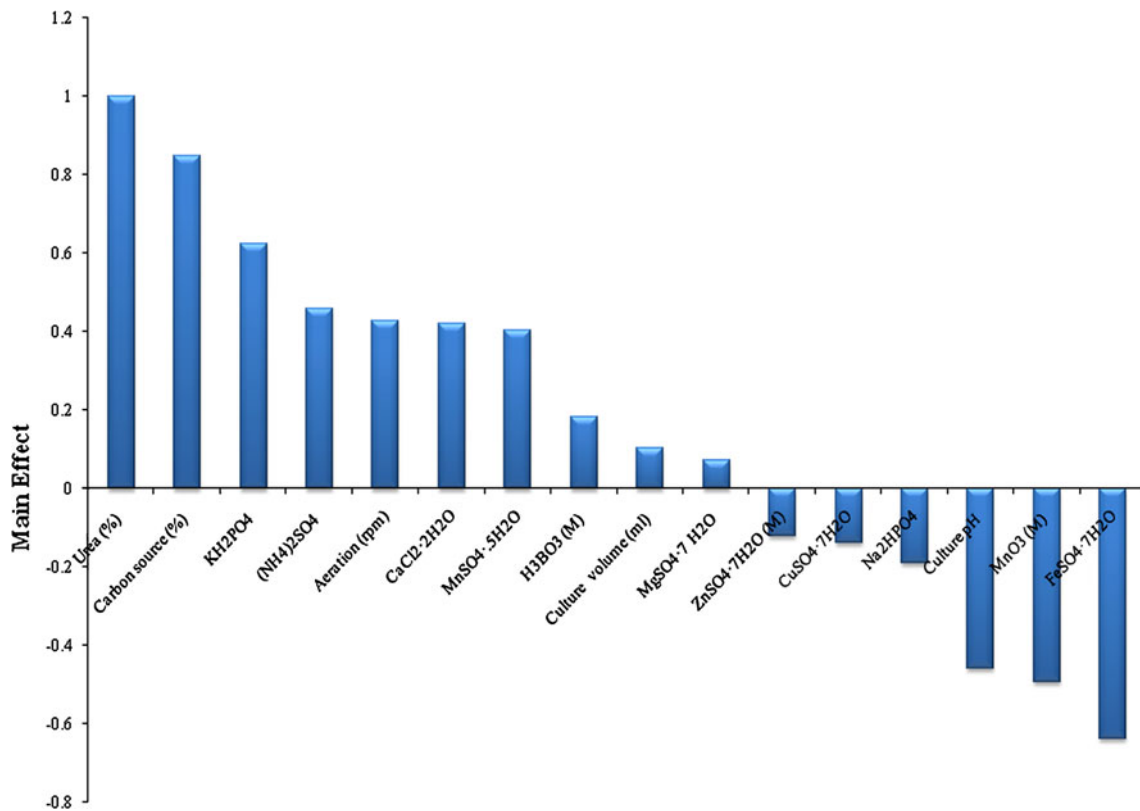


Fig. 1 Effect of nutrients and culture condition factors on the production of rhamnolipid by *Pseudomonas aeruginosa* (MTCC 7815)

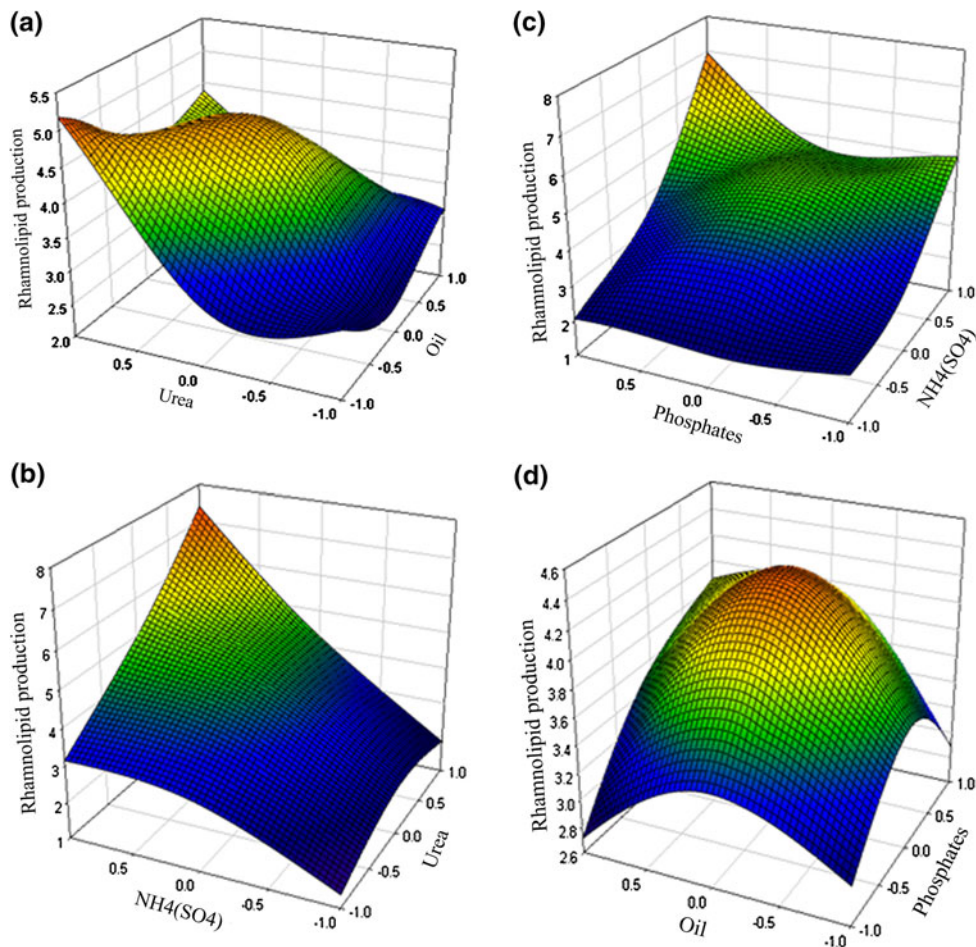
Table 6 Statistical analysis of Plackett–Burman design showing coefficient values, *t* and *p* values for each variable on rhamnolipid production (g/l)

Variables	Coefficient	<i>t</i> statistics	<i>p</i> value	Confidence level (%)
Intercept	2.682	–	–	(1– <i>p</i> value) × 100
Culture volume (ml)	0.102	0.640	0.567	43.3
Culture pH	–0.458	–2.875	0.064	93.6
Aeration (rpm)	0.428	2.687	0.075	92.5
Carbon source (%)	0.848	5.324	0.013	98.7
Urea (%)	0.998	6.266	0.008	99.2
(NH ₄) ₂ SO ₄	0.458	2.875	0.064	93.6
KH ₂ PO ₄	0.622	3.905	0.030	97
Na ₂ HPO ₄	–0.192	–1.205	0.314	68.6
MgSO ₄ ·7 H ₂ O	0.072	0.452	0.682	31.8
CaCl ₂ ·2H ₂ O	0.418	2.624	0.079	92.1
FeSO ₄ ·7H ₂ O	–0.638	–4.005	0.028	97.2
CuSO ₄ ·7H ₂ O	–0.138	–0.866	0.450	55
MnSO ₄ ·5H ₂ O	0.402	2.524	0.086	91.4
H ₃ BO ₃ (M)	0.182	1.143	0.336	66.4
ZnSO ₄ ·7H ₂ O (M)	–0.122	–0.766	0.499	50.1
MnO ₃ (M)	–0.492	–3.089	0.054	94.6

The interaction between phosphates and NH₄SO₄ concentration (g/l), where a maximum peak of rhamnolipid production was appeared which is shown in Fig. 2c. While Fig. 2c also suggest with the increase in NH₄SO₄, the higher yield of rhamnolipid while the phosphate concentration

remains the same. Lastly Fig. 2d showed the concentration of oil (g/l) and phosphates (g/l) that affects the rhamnolipid production. It also suggests that the rhamnolipid production increases with the optimal amount of oil concentration and phosphate concentration. Such experimental design is a very

Fig. 2 Rhamnolipid production (g/l) response surface from *Pseudomonas aeruginosa* (MTCC 7815) as affected by (a) urea and oil (b) $\text{NH}_4(\text{SO}_4)$ and urea (c) phosphates and $\text{NH}_4(\text{SO}_4)$ and (d) oil and phosphates



useful tool for media optimization for enhanced rhamnolipid production.

For predicting the optimal point, a second order polynomial function was fitted to the experimental results of rhamnolipid production:

$$\begin{aligned}
 Y_{\text{activity}} = & 5.5100 + 0.0816667X_1 + 0.875833X_2 + 1.51917X_3 \\
 & + 0.326667X_4 + 0.220000X_1X_2 + 0.352500X_1X_3 \\
 & + 0.287500X_1X_4 + 0.940000X_2X_3 \\
 & + 0.217500X_2X_4 + 0.540000X_3X_4
 \end{aligned}
 \quad (3)$$

where, X_1 , X_2 , X_3 and X_4 are the oil, urea, $\text{NH}_4(\text{SO}_4)_2$ and phosphates respectively.

The regression model Eq. (3) fits the experimental data well with a high R^2 (coefficient of determination) value of 0.87. The value of R^2 thus obtained suggests a high degree of correlation between the experimental and the predicted values.

Verification of the Model

To find out the optimum condition and to confirm the accuracy of the model, an experiment was carried out under basal

and predicted optimal conditions where rhamnolipid production was monitored compared to the calculated data from the model. The estimated rhamnolipid production was 5.012 g/l compared to 7.22 g/l of the predicted value from the polynomial model. Thus, it points out the accuracy of the model with more than 69.42 %, which is an evidence for the model validation. However this variance of rhamnolipid production might be because of slight variation in the experimental conditions.

Conclusion

Statistical experiment design was applied to find out the optimal concentration of each media components for the better production of rhamnolipid. The experimental design was found to be a valuable tool for improving medium composition that leads to a higher degree of rhamnolipid production. Hence pointing out statistical design as a tool for media optimization for enhanced productivity and yield. The results also suggest the optimized conditions improve the rhamnolipid production rate. As a concluding remark, the authors would like to point that, using the method of

experimental factorial design and RSM analysis, it was possible to find out the optimal handling conditions which would obtain a higher growth, thus a higher rhamnolipid production. Additionally, the validity of the model was proven by fitting the values of the variables in the model equation and by actually carrying out the experiment with those values of the variables resulting with a good accuracy of the statistical design. The present findings would aid in higher rhamnolipid yield which would assist in bioremediation of crude oil contaminated ecosystems such as soil and water bodies.

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Conflict of interest The authors have declared that no competing interests exist.

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