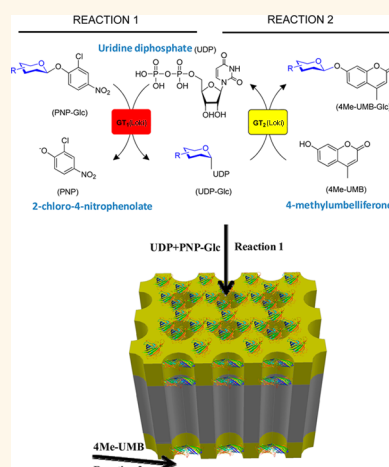


Functionalized Anodic Aluminum Oxide Membrane–Electrode System for Enzyme Immobilization

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ABSTRACT A nanoporous membrane system with directed flow carrying reagents to sequentially attached enzymes to mimic nature's enzyme complex system was demonstrated. Genetically modified glycosylation enzyme, OleD Loki variant, was immobilized onto nanometer-scale electrodes at the pore entrances/exits of anodic aluminum oxide membranes through His₆-tag affinity binding. The enzyme activity was assessed in two reactions—a one-step “reverse” sugar nucleotide formation reaction (UDP-Glc) and a two-step sequential sugar nucleotide formation and sugar nucleotide-based glycosylation reaction. For the one-step reaction, enzyme specific activity of 6–20 min⁻¹ on membrane supports was seen to be comparable to solution enzyme specific activity of 10 min⁻¹. UDP-Glc production efficiencies as high as 98% were observed at a flow rate of 0.5 mL/min, at which the substrate residence time over the electrode length down pore entrances was matched to the enzyme activity rate. This flow geometry also prevented an unwanted secondary product hydrolysis reaction, as observed in the test homogeneous solution. Enzyme utilization increased by a factor of 280 compared to test homogeneous conditions due to the continuous flow of fresh substrate over the enzyme. To mimic enzyme complex systems, a two-step sequential reaction using OleD Loki enzyme was performed at membrane pore entrances then exits. After UDP-Glc formation at the entrance electrode, aglycon 4-methylumbelliferone was supplied at the exit face of the reactor, affording overall 80% glycosylation efficiency. The membrane platform showed the ability to be regenerated with purified enzyme as well as directly from expression crude, thus demonstrating a single-step immobilization and purification process.



KEYWORDS: biomimetic enzyme immobilization · membrane–electrode · glycosyltransferase · glycosylation · enzyme purification · sequential reactions

Enzymes are biocatalysts capable of accelerating a range of chemical transformations relevant to materials production, pharmaceutical development, and renewable energy and often present an attractive “green” alternative to conventional synthetic strategies.¹ In their natural cellular/tissue environment, enzymes often assemble and/or colocalize to form multi-enzyme complexes or serial networks to expedite multistep processes in part *via* minimization of substrate/product loss *via* diffusion^{2–5} and/or to maintain exquisite control of highly reactive intermediate species.^{6–8} Additionally, the reliance upon sequential multienzyme processes and/or enzyme complexes enables metabolic control

of an overall process *via* focused allosteric and/or competitive regulation of key gate-keeper enzymes within the process by substrate/product/cofactor concentrations.⁹ Inspired, in part, by nature's logic, enzyme immobilization platforms offer the potential to mimic natural multienzyme systems,^{10–15} particularly in systems where convective flow can be used to efficiently direct products and intermediates in a sequential manner rather than depending upon Fickian diffusion.

A variety of immobilization formats for multienzyme processes have been developed. For example, simple nitrilotriacetate immobilization of His₆-tagged enzymes, as exemplified by the “superbead” approach reported by Wang and co-workers, offered

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improvements in enzyme stability and product isolation in the context of multienzyme sugar nucleotide synthesis and utilization processes.^{16,17} However, such random immobilization strategies lack systematic control and rely on stochastic transport within the dense surface layer that is mechanistically analogous to homogeneous solution. Kunitake and co-workers¹⁸ constructed alternating layers of glucose oxidase and peroxidase with layer-by-layer film adsorption on a quartz slide and subsequently demonstrated sequential activity. Though discrete enzymatic reactions were spatially separated into layers in this example, the system lacked convective flow for directing the overall sequence of reactions. Bhattacharyya and co-workers recently developed reactive stacked membranes with a top membrane containing immobilized glucose oxidase and bottom membrane containing ferrihydrite/iron oxide nanoparticles for the degradation of toxic organics in water.¹⁹ This membrane system has the advantage of using convective flow to direct the potentially damaging peroxide produced at the enzyme away to the Fe catalyst activation sites in the lower membrane layer. Building from these examples, we anticipate an idealized structure to derive from membrane pore bearing immobilized enzymes in a sequential order at nanometer-scale proximity. In this context, porous anodic aluminum oxide (AAO) membranes offer an attractive platform for enzyme immobilization and biosensor applications^{20–25} due to its high pore density, uniform pore size, and good resistance to nonspecific protein adsorption. The precise placement of gold electrodes on an AAO membrane would also make it possible for tunable immobilization of sequential enzyme cascades. Gold plating has been successfully used to tune pore size and add surface chemistry on track-etched and AAO membranes.^{26,27} Thus, multiple enzymes could feasibly be immobilized, in a sequential manner, on these two nanometer-scale electrodes to perform multistep reactions at the membrane entrance and exit respectively to mimic natural multienzyme sequential processes.

As a simple model to demonstrate multistep immobilized enzyme-catalyzed catalysis using AAO membranes, we have selected the recently reported glycosyltransferase (GT)-catalyzed transglycosylation process reported by Thorson and co-workers.^{28–34} This system is based upon the development of simple aromatic glycosides as efficient donors in glycosyltransferase-catalyzed reactions for both sugar nucleotide formation (*i.e.*, the “reverse” of a conventional GT-catalyzed reaction) and subsequent sugar nucleotide-mediated glycoside formation, wherein the use of 2-chloro-4-nitrophenyl glycoside donors also offered a convenient colorimetric screen to enable the directed evolution of enhanced GTs with broad substrate permissivity.^{31–34} Thus, this system offers a convenient model of a simple two-step enzyme-catalyzed

process—2-chloro-4-nitrophenyl glycoside-driven sugar nucleotide formation and sugar nucleotide-mediated glycoside formation—for immobilization studies. Herein we report the successful immobilization of the His₆-tagged engineered glycosyltransferase OleD Loki variant on nanometer-scale electrodes at the pore entrance and exit of AAO membrane through Ni-NTA,³⁵ which improves both enzyme activity and stability while eliminating unwanted hydrolytic side reactions known to occur at higher enzyme concentrations in the solution phase. In addition, discrete control of each independent step of the two-step sequential reaction was demonstrated *via* selective reagent feedstock composition exposure of the top and/or bottom surface of an immobilized membrane/electrode system. Finally, a convenient one-step immobilization and purification of *N*-His₆-OleD Loki variant directly from crude *Escherichia coli* Loki heterologous overproduction extract was demonstrated to enable rapid immobilized catalyzed regeneration. Cumulatively, this study highlights the utility of the AAO membrane/electrode system as a support architecture for controlling multistep enzymatic processes.

RESULTS AND DISCUSSION

The primary membrane design challenge is to localize enzyme functionality at pore entrances and exits to enable directional flow of substrates/products over the enzyme active sites in an efficient manner. Commercially available 20 nm nominal diameter AAO membranes are asymmetric with a thin porous layer at the top with a diameter of 27 nm and a bulk pore structure mainly composed of 200 nm diameter straight channel monoliths. The depth that gold sputtering can reach within the top pore neck is around 20 nm, and gold electroless plating occurs only on that deposited gold seed layer. The pore diameter of AAO membranes can be controlled by changing electroless plating time, as shown in Figure 1. Fifty minutes of electroless plating time gave the desired average pore diameter of 10 nm, matching the GT dimer length of 9.2 nm.³⁹ With this geometry GT₁ (the first GT as shown in Figure 3), the 10 nm pore entrance will block the pore, thus excess solution GT₁ cannot pass through the pore to the other side of the AAO membrane after binding.³⁸ This allows a second distinct enzyme, GT₂, to be immobilized on the 200 nm pore side of the AAO membrane to enable a directional sequential series of reactions. The process for *N*-His₆-OleD immobilization on a gold surface (Figure 2) enabled immobilization of a total amount of 30 μg of enzyme per monolayer coating based upon Bradford assay to afford a surface “concentration” of 3 g/mL immobilized enzyme within the 9.8×10^{-6} mL electrode volume.

To demonstrate the immobilized activity of the enzyme on the membrane system, we first compared GT-catalyzed UDP-Glc production (Figure 3, reaction 1) in a standard solution-phase reaction^{31,33,34} to that of

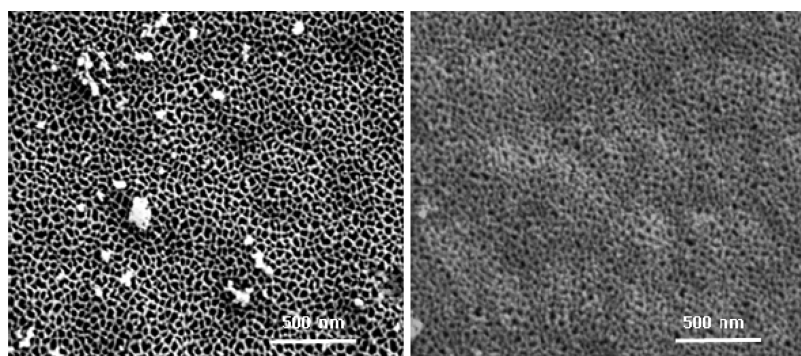


Figure 1. SEM images of bare AAO membrane and electroless-plated AAO membrane on top surface sputtered seed layer. AAO membrane pore size was controlled by gold electroless plating to match enzyme dimensions to increase efficiency of convective flow over the enzyme.

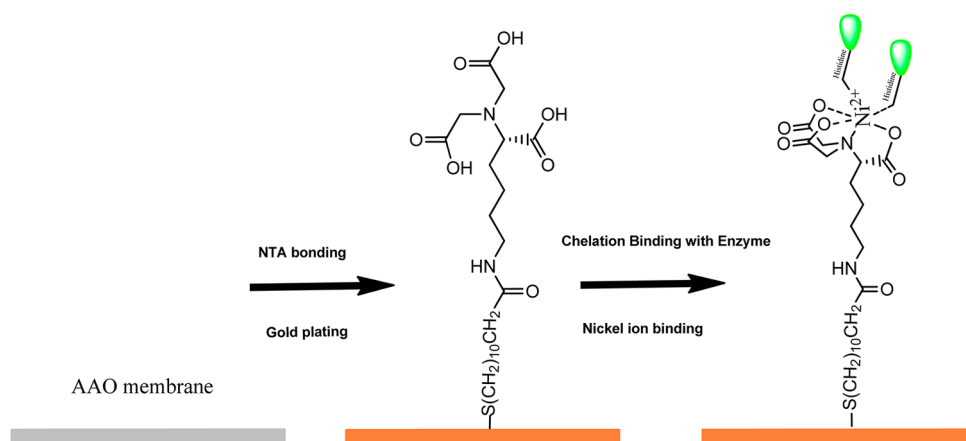


Figure 2. Enzyme immobilization process onto Au electrodes at AAO pore entrances. In the presence of excess *N*-His₆-enzyme for 24 h (see Experimental Section), the 20 nm pore size surface is routinely coated with 30 μg of enzyme, affording a local surface concentration of 3 g/mL.

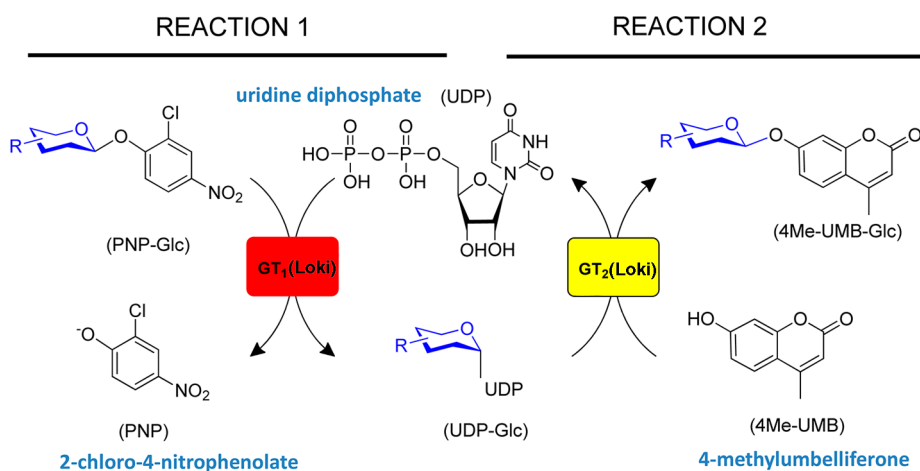


Figure 3. Model reactions utilized to assess the immobilized platform. Reaction 1 is a 2-chloro-4-nitrophenyl glucose (PNP-Glc)-driven glycosyltransferase-catalyzed "reverse" reaction to produce the desired sugar nucleotide UDP-Glc. Reaction 2 is a standard glycosyltransferase-catalyzed glycosylation of the model acceptor 4Me-UMB, where the UDP-Glc from reaction 1 serves as the sugar donor in a sequential reaction. For the current study, reaction 1 occurs on the top face while reaction 2 occurs at the bottom face of the reactor membrane.

the membrane-supported format. The solution-phase reaction contained 2.6 mM glycoside donor, 1 mM UDP, and 100 $\mu\text{g}/\text{mL}$ OleD Loki in a total volume of 200 μL of Tris-HCl (50 mM, pH 8.5) and was incubated at

25 $^{\circ}\text{C}$ for 12 h. The much higher than standard (typically 0.5–2.0 $\mu\text{g}/\text{mL}$) enzyme concentrations employed in this solution-phase comparator reaction were utilized to better reflect the high local concentration of the

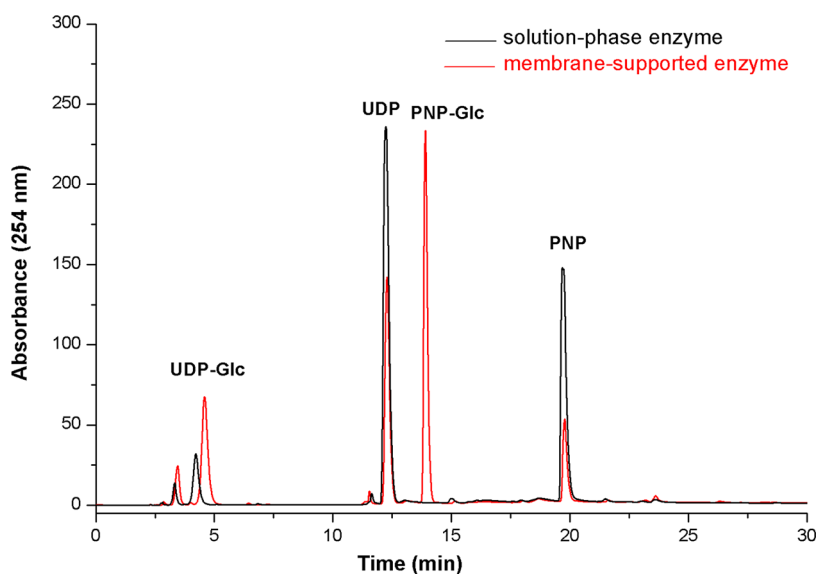


Figure 4. Representative HPLC analysis of UDP-Glc production (reaction 1) using solution-phase enzyme and membrane-supported enzyme. The solution-phase reaction mixture contained 2.6 mM glycoside donor, 1 mM UDP, 100 $\mu\text{g}/\text{mL}$ OleD Loki in a total volume of 200 μL 50 mM Tris-HCl, pH 8.5 and was incubated at 25 $^{\circ}\text{C}$ for 12 h. The immobilized reaction contained 4 mL of the same reagent mix (lacking solution-phase OleD Loki) injected through the membrane containing a total of 30 μg of immobilized OleD Loki at a flow rate of 1 mL/h at 25 $^{\circ}\text{C}$ for 4 h. Resulting reactions were subsequently analyzed by HPLC.

immobilized system (estimated as 3 g/mL as previously described). The corresponding immobilized reaction utilized an identical reagent/reaction mixture (lacking enzyme) pumped through the OleD Loki-loaded membrane at 1 mL/h over 4 h at 25 $^{\circ}\text{C}$. UDP-Glc production in the solution-phase reaction and the collected eluent from the membrane-supported reaction was determined by HPLC (Supporting Information Figure S7 and Figure 4). As controls, identical reactions wherein OleD Loki was replaced by *N*-His₆-tagged CalC (an enediyne self-resistance protein devoid of GT activity)^{40,41} were utilized to distinguish any potential non-enzymatic contributions to UDP-Glc production.

Figure 4 highlights the outcome of this initial reaction 1 comparison and reveals a total 40% yield of UDP-Glc in the membrane-bound enzyme format compared to 12% in the solution phase and no reaction in the comparator CalC-based negative controls. Interestingly, significant amounts of PNP-Glc were still present in the membrane-bound eluent, suggesting the 1 mL/h flow rate to be too fast for optimal residence time. In contrast, PNP-Glc was exhausted in the solution-phase reaction, and corresponding low UDP-Glc yield was attributed to undesired PNP-Glc and UDP-Glc hydrolysis that unexpectedly occurred at high enzyme concentrations and extended reactions times. Supporting Information Figure S2 shows the direct hydrolysis of a solution of desired product (UDP-Glc) being hydrolyzed by the enzyme to UDP (reaction conditions: 0.5 mM UDP-Glc, 100 $\mu\text{g}/\text{mL}$ Loki, 100 μL of Tris-HCl, pH 8.0, 25 $^{\circ}\text{C}$). Supporting Information Figures S3 shows the formation of hydrolysis product under the conditions for the first reaction (reaction conditions: 0.5 mM UDP-Glc, 100 $\mu\text{g}/\text{mL}$ Loki, 100 μL of Tris-HCl,

pH 8.0, 25 $^{\circ}\text{C}$). While a reduction of enzyme concentration and shorter reaction times in the solution-phase format can circumvent this unwanted effect, the immobilized format offers the opportunity to fine-tune residence time *via* adjusting the flow rate to afford optimal UDP-Glc production in reaction 1 at high concentrations/throughput without allowing the subsequent hydrolysis reaction. Within this context, the substrate residence time can be calculated based upon [(pore area \times electrode thickness)/volume flow rate]. Thus, we expect to achieve the best reaction yields by matching an optimal flow rate with an enzyme's specific kinetics where slower enzymes would require an additional increase in path length.

For the current model system, the kinetics of the solid-phase system can be estimated based upon enzyme loading per surface area (*i.e.*, concentration) and flow rates. Specifically, the loading of OleD Loki on the nanometer-scale electrode was 30 μg , giving a local concentration of about 3 g/mL based on the pore volume of the solution adjacent to the 20 nm thick gold electrode. Using the average turnover number of OleD Loki (10 min^{-1}),^{31,33,34} the theoretical calculated UDP-Glc yield *versus* flow rate (Figure 5) predicts 0.4 mL/h as the optimal flow rate for continuous UDP-Glc production. Consistent with this model, Figure 5 illustrates the impact of flow rate upon UDP-Glc formation with a maximum yield observed experimentally at a flow rate of 0.5 mL/h. This is also consistent with a model wherein unwanted hydrolysis, which occurs under very high enzyme concentrations in the solution phase over extended periods, does not significantly impact product formation under optimal solid-phase conditions. Specifically, nearly quantitative

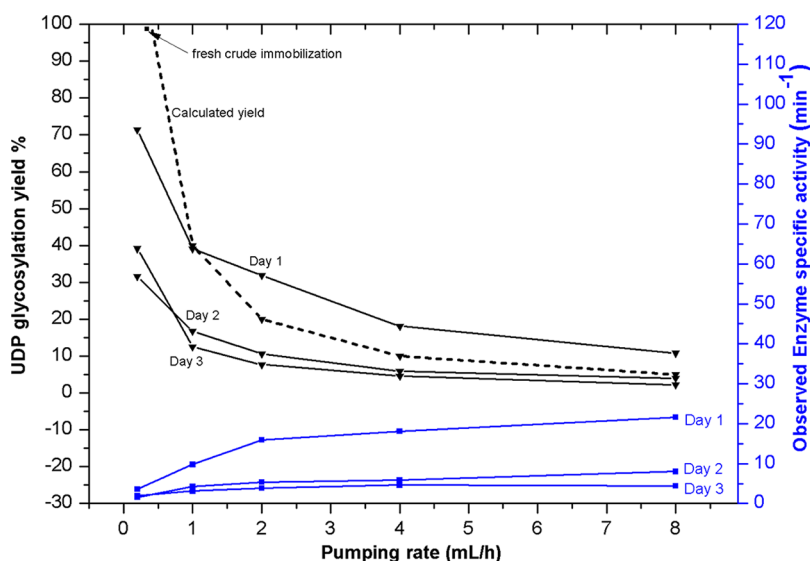


Figure 5. Calculated (dotted line) and observed UDP-Glc production as a function of flow rate; for a pumping rate of 0.2, 1, and 2 mL/h, the pumping time was 4 h, and for a pumping rate 4 and 8 mL/h, the pumping time was 1 h. Day 1 refers to a complete series of runs at specified pumping rates, followed by repeating a second complete series on day 2 to show enzyme stability. Square marker was for an experiment performed at optimal flow rates with fresh enzyme separated directly from cell crude.

UDP-Glc formation (98%, square marker shown in Figure 5) was observed experimentally at a flow rate of 0.5 mL/h, illustrating the potential of the immobilized system to reduce unwanted side reactions and thereby optimize product output.

Continuous production is another important merit of an immobilized platform. As part of the study illustrated in Figure 5, a total volume of 84.4 mL of substrate solution was processed using 30 μg of Loki immobilized on the membrane with a total production of 10 μmol UDP-Glc. Using optimal solution-phase conditions (0.5–2 $\mu\text{g}/\text{mL}$), the same reaction volume would require up to 5-fold more enzyme and, if incubated for the same time frame, is expected to suffer a significant reduction in yield due to product hydrolysis. In this particular case, the membrane flow reactor gave a 280-fold improvement in enzyme utilization compared to 0.2 mL of the homogeneous solution protocol with 20 μg of Loki for a total of 2.4×10^{-8} mol UDP-Glc.

Two-step sequential reactions on the membrane-immobilized enzyme system were then carried out to mimic multienzyme processes and compare their performance to solution-based single-glycosyltransferase-coupled reactions. We selected two model GTs (GtfE and OleD Loki) that catalyze glucosyltransfer from UDP-Glc to model acceptors [vancomycin aglycon and 4-methylumbelliferone (4Me-UMB), respectively] with differing proficiencies. Specifically, the turnover rates for GtfE⁴² and Loki³⁴ are 0.005 and 10 min^{-1} . For the sequential reaction platform, the reaction sequence was physically separated into two discrete steps with the first (UDP-Glc formation, reaction 1) occurring on the top face of the membrane (entry) and the second (aglycon glycosylation, reaction 2) on

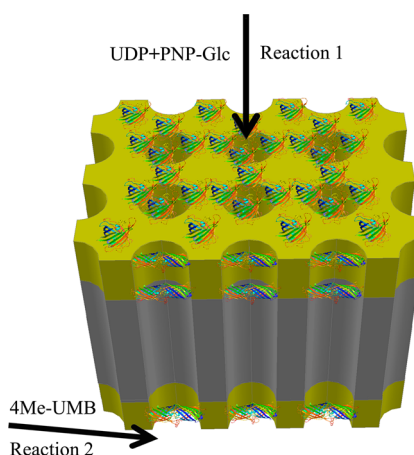


Figure 6. Configuration for the solid-phase two-step sequential reaction process (Figure 3 reaction 1, top face; reaction 2, bottom face) catalyzed by AAO membrane-immobilized OleD Loki. Reaction 1 is carried out on the top membrane entrance to produce UDP-Glc, which is then directed to the bottom membrane exit for the glycosylation of 4Me-UMB (reaction 2).

the bottom face (exit). To afford this physical separation of reactions, the required reagents for reaction 2 were introduced by cross-flow to the bottom surface, as illustrated in Figure 6. This format allows for sequential transfer of intermediates by having separate reagents flowing through the top and supplied orthogonally to the bottom of the membrane. Thus, for the kinetically matched pairing where both GT₁ and GT₂ (Figure 3) are OleD Loki, the UDP-Glc formed in reaction 1 enters the reaction 2 sequence *via* directional flow wherein the acceptor 4Me-UMB is only present in the lower reaction vessel at the membrane exit.

For this analysis, solution-phase and membrane-supported reactions were conducted in parallel using

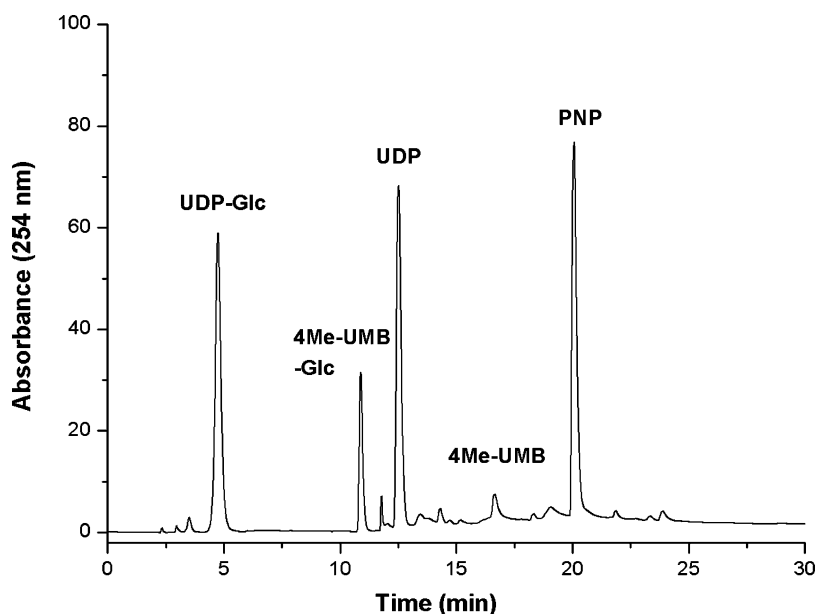


Figure 7. HPLC analysis of a representative immobilized sequential reaction containing 2.56 mM PNP-Glc and 1 mM UDP in 50 mM Tris-HCl, pH 8.5, in the upper reactant chamber injected through the membrane carrying immobilized OleD Loki on the top and bottom face into a bottom reaction chamber containing 0.56 mM 4Me-UMB in the same buffer. Flow rate for this sequential reaction was 0.5 mL/h at 25 °C for 4 h, and the bottom reaction chamber contents were subsequently analyzed by HPLC. For comparison, Figure S4 highlights a representative solution-phase sequential reaction.

similar conditions to offer a potential comparison of overall utility to afford the desired glycosylated product. For the kinetically matched pairing where both GT₁ and GT₂ (Figure 3) were OleD Loki, the solution-phase reaction contained 2.56 mM PNP-Glc, 1 mM UDP, 0.56 mM 4Me-UMB, and 100 μ g/mL OleD Loki variant in a total volume of 200 μ L 50 mM Tris-HCl (pH 8.5) incubated for 12 h at 25 °C. The corresponding immobilized system employed the same reagents/concentrations where PNP-Glc and UDP were introduced from the top of the membrane using a syringe pump (reaction 1) while 4Me-UMB was separately fed across the bottom of the membrane in orthogonal cross-flow using a second syringe pump (Figure S1), both at a flow rate of 0.5 mL/h. Product formation in the solution-phase reaction and the eluent from the bottom solid-phase reactor face were analyzed by HPLC.

Figure 7 highlights the distribution of reactants/products in the lower eluent of the solid-phase OleD Loki-based sequential reaction series revealing a 71% yield of the desired product (4Me-UMB glucoside). The corresponding solution-phase yield of 4Me-UMB was 16% (Figure S4) wherein potential GT-catalyzed reaction reversibility and UDP-Glc hydrolysis under longer reaction times are likely major contributors to the reduction of the overall yield. While this supports our initial premise that the membrane-immobilized format serves as a potential platform for mimicking Nature's control of multienzyme sequential reactions, one limitation derives from a need to pair the corresponding enzyme catalytic efficiencies with flow rates. Consistent with this, while a solution-phase sequential

OleD/GtfE-catalyzed reaction was previously demonstrated,²⁸ the kinetically mismatched (10 min⁻¹ vs 0.005 min⁻¹) OleD Loki (top)/GtfE (bottom) pair failed to afford the final desired product potentially due to an inability to reduce the flow rate to sufficiently compensate for the slow turnover rate of GtfE without succumbing to back diffusion and unwanted OleD Loki-catalyzed hydrolysis of UDP-Glc (Figure S9). In such cases, a possible solution may be to increase the active path length (membrane/electrode thickness) to increase residence time or increase enzyme loading of the slower enzyme.

The design of the membrane platform presented suggests that, like a standard nickel nitrilotriacetic acid resin-based column, this membrane should be able to "capture" active enzyme directly from crude lysates, thereby circumventing the need for protein purification as part of membrane preparation. To assess this, membrane was exposed to 5 mL of crude lysate from a standard OleD Loki *E. coli* heterologous overproduction culture for 24 h, subsequently washed with Tris-HCl buffer three times, and the purity of the captured protein upon release *via* treatment with 500 mM imidazole in Tris-HCl buffer solution was determined *via* SDS-PAGE (Figure S5), which revealed captured protein with a purity of $\geq 99\%$ (Figure S6). Importantly, the membrane loaded *via* the crude extract capture method catalyzed nearly quantitative single-step UDP glycosylation (98%) and a corresponding notable two-step 4Me-UMB glycosylation yield (80%) at optimal volume flow rates (Figure S7 and Figure S8).

Finally, the membrane-immobilized enzyme also displayed notable stability even after 2 months of cold

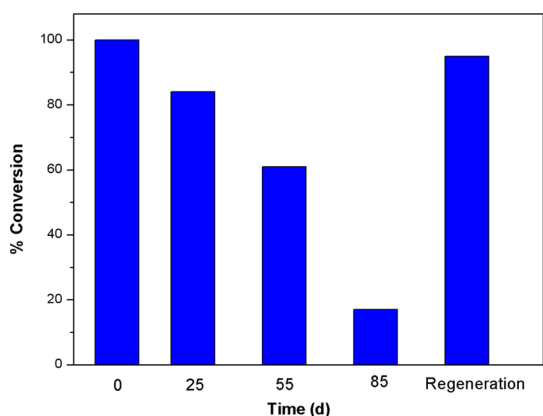


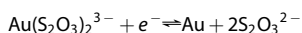
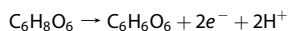
Figure 8. Stability of immobilized enzyme stored at 4 °C where percent conversion is based upon UDP-Glc formation (reaction 1) as determined *via* HPLC. Regeneration was carried out after 85 days storage of immobilized enzyme at 4 °C.

storage at 4 °C. Specifically, the immobilized enzyme $T_{1/2}$ based upon UDP-Glc formation was more than 55 days (Figure 8). In addition, the membrane platform is robust and could be reused multiple times *via* a simple regeneration process (removal of protein with 500 mM imidazole, rinsing with Tris-HCl buffer, and subsequent protein reloading).

EXPERIMENTAL SECTION

Materials. AAO membranes were purchased from Whatman. Gold(I) thiosulfate was purchased from Alfa Aesar (Ward Hill, MA), and ascorbic acid was purchased from EM Science (Gibbstown, NJ). Vancomycin aglycon^{31,33} and 2-chloro-4-nitrophenyl glucoside³¹ were prepared as previously reported. All other chemicals were purchased from Sigma-Aldrich (Milwaukee, WI), and all chemicals were used as received unless otherwise noted. Swinnex 47 mm filter holders were purchased from Millipore (Billerica, MA).

Membrane/Electrode Fabrication. Sputtering was performed with a Cressington Coating System (Ted-Pella) with calibrated quartz crystal monitor with background pressure of 0.02 mbar. No intermediate wetting layer (*i.e.*, Ti/TiO₂) on Al₂O₃ was needed for seeding the Au layer. Gold (5 nm) was sputtered on the top and bottom of the AAO membranes followed by electroless plating. Electroless plating³⁶ was performed in 50 mM phosphate buffer, pH 7.0, containing 1.6 mM sodium gold(I) thiosulfate and 2.68 mM ascorbic acid. The oxidation and reduction reactions were given by



Pore size before and after electroless plating was analyzed *via* scanning electron microscopy (SEM) using a Hitachi S-4300 scanning electron microscope.

Enzyme Immobilization and Regeneration. *N*-[*N*α,*N*α-Bis(carboxymethyl)-L-lysine]-12-mercaptododecanamide (NTA) self-assembled monolayer³⁷ was prepared by incubation of gold with 10 mL of 1 mM NTA ethanol solution at 25 °C for 24 h followed by rinsing with 10 mL of ethanol for 3 min and drying under a N₂ stream. The membrane was incubated with 10 mL of 0.5 M NiCl₂ aqueous solution for 24 h at 25 °C followed by rinsing with 10 mL of Milli-Q water for 3 min and dried under a N₂ stream. The production and

CONCLUSION

In conclusion, we have demonstrated a design for a robust sequential enzyme reaction system immobilized on nanoscale electrodes at the entrance and exit of AAO membranes. The local enzyme concentration at the nanoscale electrodes is much higher compared to homogeneous solution and allows precise control of the enzyme residence time of substrates, translating to improvements in overall output *via* the reduction of unwanted side reactions (hydrolysis) and/or potential product inhibitors. Model sequential reactions using the same format revealed similar advantages wherein a main limitation stems from the need to pair enzymes of similar catalytic efficiencies with overall flow rate. In situations where catalytic efficiencies of catalysts dramatically differ, it is expected that extending the path length (*i.e.*, surface area) for slower catalysts could enable pairing with faster catalytic partners. Additional advantages observed in this study include the ability to rapidly capture target catalysts from crude *E. coli* lysates and the relatively long-term stability of target catalysts and corresponding membrane architecture. As such, this membrane platform offers an opportunity to expand the study and biocatalytic utility of multi-enzyme cascades with directed mass transport.

purification of OleD Loki³⁴ and GtfE⁴² followed previously reported methods. One side or both sides of the membranes were incubated with an excess of purified enzyme in 10 mL of 50 mM tris(hydroxymethyl)aminomethane hydrochloride (Tris-HCl) buffer, pH 8.5, for 24 h at 4 °C and washed three times with an equal volume of buffer to remove unbound protein prior to use. Immobilized protein was released by 500 mM imidazole (10 mL, 50 mM Tris-HCl buffer, pH 8.5) followed by filtering to remove imidazole. The amount of released protein was determined *via* standard Bradford assay. The OleD Loki-loaded membrane can be regenerated by simply soaking in 500 mM imidazole solution to remove the bound protein, rinsing with Tris-HCl buffer, and subsequent protein reloading.

Protein Capture from *E. coli* Lysates. Following standard protocol,³⁴ cell pellets from standard heterologous overproduction of OleD Loki in *E. coli* were collected by centrifugation (6000 *g* at 4 °C for 20 min), resuspended in 2.5 mL of chilled lysis buffer (20 mM phosphate buffer, pH 7.4, 0.5 M NaCl, 10 mM imidazole), and lysed by sonication (5 pulses of 1 min each) in an ice bath. Cell debris was removed by centrifugation (10 000 *g* at 4 °C for 20 min), and NTA-Ni-modified membranes were then incubated in the resulting crude extracts (10 mL) for 24 h at 4 °C; the membranes were subsequently washed with 5 mL of 50 mM Tris-HCl buffer, pH 8.5, three times to remove unbound protein.

HPLC Analysis. HPLC was conducted with an Agilent 1260 system equipped with a DAD detector with a 250 mm × 4.6 mm Gemini-NX 5μ C18 column (Phenomenex, Torrance, CA) and using a linear gradient [1% B to 71% B over 30 min, 71% B for 5 min, 71% B to 1% B over 1 min, 1% B for 4 min (solvent A = 50 mM PO₄²⁻, 5 mM tetrabutylammonium bisulfate, 2% acetonitrile, pH 6.0; solvent B = acetonitrile); flow rate = 1 mL min⁻¹; A254]. HPLC peak areas were integrated with an Agilent (Santa Clara, CA) 1260 workstation, and the percent conversion was calculated based upon peak area of the products and unreacted starting materials. For all reactions, 30 μL aliquots were quenched with an equal volume of MeOH and analyzed *via* HPLC.

Conflict of Interest: The authors declare no competing financial interest.

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Supporting Information Available: Membrane-based sequential reaction setup, enzyme-induced hydrolysis reactions, HPLC of solution-phase sequential reactions, SDS-PAGE of Loli released from AAO membrane, HPLC of enzymatic reactions using membrane-supported enzyme prepared *via* crude extract capture method, OleD Loli/GtFE sequential reaction scheme. This material is available free of charge *via* the Internet at <http://pubs.acs.org>.

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