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# **Electrochemical biofilm control: mechanism of action**

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# **Abstract**

Although it has been previously demonstrated that an electrical current can be used to control biofilm growth on metal surfaces, the literature results are conflicting and there is no accepted mechanism of action. One of the suggested mechanisms is the production of hydrogen peroxide  $(H<sub>2</sub>O<sub>2</sub>)$  on metal surfaces. However, there are literature studies in which  $H<sub>2</sub>O<sub>2</sub>$  could not be detected in the bulk solution. This is most likely because  $H_2O_2$  was produced at a low concentration near the surface and could not be detected in the bulk solution. The goals of this research were (1) to develop a well-controlled system to explain the mechanism of action of the bioelectrochemical effect on 316L stainless steel (SS) surfaces and (2) to test whether the produced  $H_2O_2$  can reduce cell growth on metal surfaces. It was found that  $H_2O_2$  was produced near 316L SS surfaces when a negative potential was applied. The  $H_2O_2$  concentration increased towards the surface, while the dissolved oxygen decreased when the SS surface was polarized to −600 mVAg/AgCl. When polarized and non-polarized surfaces with identical *Pseudomonas aeruginosa* PAO1 biofilms were continuously fed with air-saturated growth medium, the polarized surfaces showed minimal biofilm growth while there was significant biofilm growth on the nonpolarized surfaces. Although there was no detectable  $H_2O_2$  in the bulk solution, it was found that the surface concentration of  $H_2O_2$  was able to prevent biofilm growth.

# **Keywords**

biofilm; bioelectrochemical; biofilm control; hydrogen peroxide; cathode

# **Introduction**

Although electrical current has been previously demonstrated to control biofilm growth on metal surfaces, the literature results are conflicting and there is no single accepted mechanism of action (Del Pozo et al. 2008). Some of the mechanisms proposed in the literature are (1) electrochemical generation of oxidants on the surface (Costerton et al. 1994), (2) contraction or expansion of biofilm structure (Stoodley et al. 1997), (3) electrolytic generation of oxygen during water electrolysis (Stewart et al. 1999), and (4) electrostatic and electrophoretic repulsive forces (Hong et al. 2008). However, none of these mechanisms is widely accepted because of conflicting results in the literature and the

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impossibility of comparing the different electrochemical systems. This may be partly due to the oversimplification that the magnitude of the electrical current itself determines the effect on biofilm growth. Because the research group responsible for the study reported here works with bioelectrochemical systems, information on current, potential, and internal resistances is needed to characterize the system, similar to microbial fuel cells (Logan et al. 2006). Thus, the term 'bioelectrochemical effect' is used to describe the electrochemical control of biofilm growth on metal surfaces.

To control biofilm growth using the bioelectrochemical effect, the minimum electrochemical system that can be used is a two-electrode cell in which a current or potential is applied to the metal surface with biofilm against another electrode. Shirtliff et al. (2005) used an annular reactor with a stainless steel surface to evaluate the bioelectrochemical effect. They applied a 370-*μ*A cm−2 current and found that the applied current did not have any bactericidal effect. Similarly, Hong et al. (2008) used a flow chamber and applied a 15- *μ*A cm−2 current and found that the applied current caused detachment of the biofilm on the indium tin oxide surface. They hypothesized that this was due to electrostatic and electrophoretic repulsive forces. Similar observations were made by van der Borden et al. (2004), who applied a current between 2.86 and  $4.76 \mu A \text{ cm}^{-2}$ . Liu et al. (1997) inserted two electrodes into agar in a plate and found a zone where biofilm growth was inhibited. They found that this was due to hydrogen peroxide  $(H_2O_2)$  production. On the other hand, Del Pozo et al. (2009) applied a current between  $1.626 \times 10^3$  and  $1.626 \times 10^6$   $\mu$ A cm<sup>-2</sup> and did not detect  $H_2O_2$ ; instead, they concluded that pH was the cause of decreased biofilm growth.

Other researchers have controlled the potential of surfaces to prevent cell growth. For example, Busalmen and de Sanchez (2001) poised a gold surface at negative potentials and observed a reduction in biofilm growth. They hypothesized that this was a result of electrostatic repulsion and pH changes caused by oxygen reduction. Similarly, Matsunaga and Lim (2000) poised nylon fishnets coated with conductive paint at negative potentials and observed biofilm detachment. Toxic substances such as  $H_2O_2$ , oxidizing radicals, and chlorine molecules were not detected. Since the work reported here focused on the bioelectrochemical effect only, the literature related to the combined use of antibiotics and electrical current known as the 'bioelectric effect' is not discussed (Del Pozo et al. 2008). The use of combined antibiotics and electrical current could involve different mechanisms than those discussed in this paper.

It is important to note that the literature studies discussed above used different electrochemical cells with different geometries and operated using either a controlled potential-potentiostatic system or a controlled current-galvanostatic system to achieve the bioelectrochemical effect. Regardless of the type of system, a specified current is required to understand the rate of reaction and a specified potential is required to assess the thermodynamic state of the system. To have reproducible or comparable data, both the potential (galvanostatic) and current (potentiostatic) data must be presented. Additionally, the potential of the electrode must be defined against a well-known reference electrode. Therefore, it is critical to use a well-defined electrochemical system to understand the mechanisms of action of the bioelectrochemical effect.

(2)) (Bard and Faulkner 2001).

 $O_2 + 4H^+ + 4e^- \rightleftarrows 2H_2O$   $(E^{0'} = +618 mV_{Aq/AqCI})$  (1)

$$
O_2 + 2H^+ + 2e^- \rightleftarrows H_2O_2 \quad (E^{0'} = +85 \, mV_{Aq/AqCI}) \quad (2)
$$

Although the standard reduction potential of  $H_2O_2$  is +85 mV<sub>Ag/AgCl</sub>, it is common to observe the onset of  $H_2O_2$  production at negative polarization potentials because of large activation overpotentials (Vetter 1967). In bioelectrochemical systems where oxygen is the only cathodic reactant, cathodic current will most likely result in the production of  $H_2O_2$ .

By controlling the potential of the electrode, it is possible to generate  $H_2O_2$  on 316L stainless steel (SS) surfaces. To the best of the authors' knowledge, such generation of  $H_2O_2$ on SS surfaces has not been experimentally demonstrated to be a mechanism of the bioelectrochemical effect. The goals of this research were (1) to develop a well-controlled system to explain the mechanism of action of the bioelectrochemical effect on SS surfaces and (2) to test whether electrochemically generated  $H_2O_2$  can reduce biofilm growth on metal surfaces. A flat plate flow cell was designed to monitor *in situ* biofilm formation. Previously developed  $H_2O_2$  microelectrodes were modified to measure  $H_2O_2$  on SS surfaces. In addition, dissolved oxygen (DO) microelectrodes were used to measure the variation of DO near the SS surface. Since  $H_2O_2$  production was only found near the SS surface, its biocidal efficacy on *Pseudomonas aeruginosa* PAO1 biofilms was tested. *P. aeruginosa* PAO1 biofilms were grown on SS surfaces and biofilm growth was quantified on polarized and non-polarized surfaces.

# **Materials and methods**

#### **Preparation of growth medium and inoculum**

*P. aeruginosa* PAO1 tagged with green fluorescent protein was obtained from Dr Michael Franklin, Center for Biofilm Engineering, Montana State University. A defined medium with the following composition was used: Na<sub>2</sub>HPO<sub>4</sub>, 1830 mg l<sup>-1</sup> (J.T. Baker®); KH<sub>2</sub>PO<sub>4</sub>, 1350 mg l−1 (J.T. Baker®); MgSO4 · 7H2O, 10 mg l−1 (J.T. Baker®); yeast extract, 10 mg  $1^{-1}$  (Bacto®); glucose, 1000 mg  $1^{-1}$  (Fisher®); (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub>, 100 mg  $1^{-1}$  (J.T. Baker®). The medium was autoclaved at 121°C for 15 min l<sup>-1</sup> of solution. The ammonium sulfate and yeast extract were autoclaved separately and then added to the growth medium. The glucose was filter-sterilized. After the medium was allowed to cool to room temperature, a trace elements solution (1 ml  $l^{-1}$ ) was filtered and added to it. The trace elements solution was prepared by adding MnCl<sub>2</sub> · 4H<sub>2</sub>O, 357 mg l<sup>-1</sup>; CuCl<sub>2</sub> · 2H<sub>2</sub>O, 228 mg l<sup>-1</sup>; CoCl<sub>2</sub> · 2H<sub>2</sub>O, 317 mg l<sup>-1</sup>; (NH<sub>4</sub>)Mo<sub>7</sub>O<sub>4</sub> ·H<sub>2</sub>O, 231 mg l<sup>-1</sup>; Na<sub>2</sub>B<sub>4</sub>0<sub>7</sub> · 10H<sub>2</sub>O, 127 mg l<sup>-1</sup>; ZnCl<sub>2</sub>, 363 mg

l<sup>-1</sup>; FeCl<sub>3</sub>, 2160 mg l<sup>-1</sup>; and CaCl<sub>2</sub>, 3700 mg l<sup>-1</sup>. Carbenicillin (150 μg ml<sup>-1</sup> of USP grade disodium salt, Teknova) was added to the medium. A 1-ml vial of frozen (−85°C) *P. aeruginosa* PAO1 stock was thawed at room temperature. The stock was then used to inoculate 100 ml of the sterile defined medium, which was incubated on a shaker at 150 rpm at 30°C for 24 h. The optical density (OD) was measured at 600 nm and adjusted to 0.05 before the biofilm reactor was inoculated. An OD of 0.05 was chosen as optimal for obtaining a single layer of cells during initial attachment and quantifiable cell counts on the SS surface subsequently. The biofilm reactor was inoculated with 10 ml of inoculum using a sterile syringe.

#### **Preparing the biofilm reactor**

The experimental setup is shown in Figure 1. A custom-made flat plate flow cell was used to grow biofilms on SS surfaces. The reactor was designed in such a way that the SS working electrode and the graphite counter electrode (Glassmate grade GM-10, Poco Graphite, Inc., Decatur, TX, USA) were separated by a cation exchange membrane (Membranes International Inc., CMI-7000,  $6 \times 8$  cm). The membrane isolated the reactions at the counter electrode from the SS working electrode. The reactor bottom was made of microscope cover glass (Thermo Scientific<sup>®</sup> Gold Seal Cover Glasses, Rectangles  $48 \times 60$  mm, #1), which served as a viewing window for epifluorescence microscopy. In this way, the cells on the SS surface were imaged directly. Five autoclavable rubber separators were used between each two layers to prevent leakage. A graphite  $(1 \times 2 \text{ cm})$  counter electrode and a custom-made Ag/AgCl reference electrode (Lewandowski and Beyenal 2007) were used in the upper compartment. Two SS coupons  $(1.18 \times 1.18 \text{ cm})$  were used in the lower cells. The first SS coupon was the control surface (non-polarized) and the second SS coupon was polarized against the Ag/AgCl reference electrode. Platinum wires (CA Fine Wire Company, Pure TC Grade, MO, #M159850) were used to connect the SS coupons to external cables, which were connected to a custom-built potentiostat (Renslow et al. 2011). The connection resistances were always less than 5 $\Omega$ .

#### **Operating the biofilm reactor**

The assembled flat plate flow cell (Figure 1) and tubing were autoclaved at  $121^{\circ}$ C for 15 min. After cooling to room temperature, the 316L SS working electrode and the counter and reference electrodes were connected to a custom-built potentiostat (Renslow et al. 2011). A two-channel peristaltic pump (Masterflex<sup>®</sup> L/S<sup>®</sup> Cole-Parmer Instrument Company) was used at a flow rate of 0.4 ml min−1 for the feed and 3M NaCl solution. The flow cell was inoculated aseptically from its inoculation port with 10 ml of inoculum. After 2 h of initial attachment (no flow), the flow was started and planktonic cells were washed out of the flow cell. Before polarization, it was verified that there were no bubbles in the reactor. For biofilm experiments, the polarization potential was set to  $-600 \text{ mV}_{Ag/AgCl}$ .

#### **Biofilm imaging and analysis**

During operation, the flat plate flow cell was placed on an inverted epifluorescence microscope (Nikon® Eclipse Ti-S inverted microscope); a Nikon® DS-Qi1Mc camera was mounted on the microscope for imaging. A CFI Plan Fluor ELWD  $40 \times$  objective (N.A.

0.60, W.D. 3.7-2.7 mm) was used to image the cells. Every 8 h, at least 20 images were taken to obtain statistically representative data (Ica et al. 2012). The surface coverage was calculated from these images using NIS® software (Laboratory Imaging s.r.o., Praha, CZ). Surface coverage is the ratio of the area of biomass to the total area of the image. The higher the surface coverage, the higher the coverage of the surface by biomass.

#### **Scanning electron microscopy**

After treatment for 40 h, both the polarized and the non-polarized 316L SS surfaces were removed aseptically from the flat plate flow cell. The SS coupons were fixed overnight with 2.5% glutaraldehyde and 2%. paraformaldehyde in 0.1 M phosphate buffer followed by rinsing with 0.1 M phosphate buffer  $(3 \times 10 \text{ min each})$ . The SS coupons were then dehydrated gradually using 30%, 50%, 70%, and 95% alcohol (10 min each) and 100% alcohol ( $3 \times 10$  min each). Hexamethyldisilizane (HMDS) was used for overnight drying. The SS coupons were sputter-coated with gold prior to FEISEM (FEI 200F) imaging.

#### **Microelectrode construction**

The  $H_2O_2$  and oxygen microelectrodes were constructed following the procedures given in Lewandowski and Beyenal (2007) except that the  $H_2O_2$  microelectrode was modified so that it could operate on polarized surfaces. Briefly, an etched platinum wire was encased in a glass capillary which was pulled at a high temperature to seal the wire. The platinum tip was then exposed by grinding away the sealed tip using a diamond grinding wheel (Narishige<sup>®</sup>, model EG-4). The exposed tip was  $10-15 \mu m$  in diameter. Platinum was electrochemically deposited onto the exposed platinum tip, which resulted in a porous platinum ball that increased the effective surface area and, consequently, the sensitivity of the microelectrode. A 5% cellulose acetate (Sigma-Aldrich®) membrane was then deposited on the platinum ball. The final tip diameter was  $\sim$ 20  $\mu$ m. The H<sub>2</sub>O<sub>2</sub> microelectrode was placed in a glass outer casing with the tip exposed to the solution. The glass junction was sealed with an agar (1.812-g l<sup>-1</sup> R-2A Agar, Fluka<sup>®</sup>) salt bridge containing 1 mM sodium sulfate (Fisher<sup>®</sup>) and the outer case was filled with saturated KCl and Ag/AgCl reference filling solution (SP135-500, Fisher®). A Ag/AgCl reference electrode was inserted into the glass outer casing. The procedures given in the literature were followed to construct the dissolved oxygen microelectrode (Lewandowski and Beyenal 2007). The final tip diameter of the DO microelectrode was ~15 *μ*m.

#### **Operation of microelectrodes**

The H<sub>2</sub>O<sub>2</sub> and oxygen microelectrodes are amperometric sensors. A Keithley<sup>®</sup> 6517A Electrometer/High Resistance Meter was used as both the voltage source and a picoammeter. The  $H_2O_2$  microelectrode was polarized to +600 mV<sub>Ag/AgCl</sub> and the DO microelectrode was polarized to -800 mV<sub>Ag/AgCl</sub>. The H<sub>2</sub>O<sub>2</sub> microelectrode was calibrated in solutions of known H<sub>2</sub>O<sub>2</sub> concentration ranging from 0  $\mu$ m to 150  $\mu$ m. The calibration curve was always linear in this concentration range. The oxygen microelectrode was calibrated in a solution with zero oxygen concentration and in air-saturated sterile growth medium. Each microelectrode was calibrated immediately before use and the calibrations were also verified after the measurements.

#### **Reactor used for microelectrode measurements**

Since the reactor shown in Figure 1 did not have a port for microelectrode measurements, a flat plate reactor with recycle was used (Nguyen et al. 2012). The SS coupons were placed at the bottom of this reactor so that it was possible to measure DO or  $H_2O_2$  profiles on the SS surface. For control experiments, a clean SS coupon was used. For experiments with biofilms, *P. aeruginosa* PAO1 cells were allowed to attach to a SS surface using the procedure described earlier. After initial attachment, the growth medium was replaced several times to remove suspended cells. Air-saturated growth medium was continuously fed into the reactor. Microelectrode measurements with biofilm were conducted in a biosafety level II hood.

#### **Microelectrode measurements**

To determine the polarization potential at which  $H_2O_2$  was produced at the SS surface, the H2O2 microelectrode was positioned approximately 100 *μ*m from the SS surface and the potential was scanned from +200 mV<sub>Ag/AgCl</sub> to −650mV<sub>Ag/AgCl</sub>. The H<sub>2</sub>O<sub>2</sub> concentration was monitored as a function of the potential of the SS. A distance of 100 *μ*m from the SS surface was maintained to reduce the likelihood of breaking the microelectrode tip. The current values during the potential sweep were collected automatically by the potentiostat.

To measure depth profiles of  $H_2O_2$  or DO, the tip of the microelectrode was positioned approximately 800 *μ*m above the SS surface using micromanipulators (Narishige®). The microelectrode tip was then stepped down in 5-*μ*m increments using custom microprofiler software until the tip was 100 *μ*m from the SS surface. Concentrations were measured at each step. The measurement of profiles was stopped 100 *μ*m from the SS surface to ensure that the tip of the microelectrode was not broken for repeated measurements. Each measurement was repeated at least three times in total. The locations of the microelectrode tip and the SS surface were monitored using a stereomicroscope (Zeiss® Stemi 2000 stereomicroscope). A Gamry<sup>®</sup> Series G<sup>™</sup> 300 potentiostat (Gamry Instruments, Warminster, PA, USA) was used to polarize the SS coupon to  $-600$  mV<sub>Ag/AgCl</sub> during depth profile measurements. Subsequently, depth profiles were taken in the same position under non-polarized and polarized conditions by controlling the potentiostat. A graphite rod counter electrode (10 cm in length and 0.5 cm in diameter) and a Ag/AgCl reference electrode were used. Note that the current was allowed to stabilize before each depth profile was measured.

To find the SS surface, the tip of the microelectrode had to be broken by touching the surface, which did not allow replicate measurements with the same microelectrode. Therefore, depth profile measurements were stopped before the microelectrode tip touched the surface, except during the last measurement, when the tip was broken to determine the location of the SS surface. It was found that the profiles near the SS surface were always linear.

#### **Results and discussion**

The microelectrode measurements were conducted twice (two replicates) and repeated at least three times at each location. The biofilm experiments were conducted in replicates and

repeated at three different times. The results were all statistically similar and led to identical conclusions. Selected representative measurements are shown here.

#### **Quantifying H2O2 generation and oxygen consumption at the 316L SS surfaces**

Figure 2 shows the variation in  $H_2O_2$  concentration with potential at a position 100  $\mu$ m from the SS surface. During the potential scan between +200 mV<sub>Ag/AgCl</sub> and −650 mV<sub>Ag/AgCl</sub>, the H<sub>2</sub>O<sub>2</sub> concentration reached a transient concentration of 5.9 μm. The onset of detectable H<sub>2</sub>O<sub>2</sub> at the microelectrode tip was at  $\sim$  –400 mV<sub>Ag/AgCl</sub>, although it was expected to correspond with the onset of cathodic current at  $-200$  mV<sub>Ag/AgCl</sub>. The delay in detection of  $H<sub>2</sub>O<sub>2</sub>$  at the microelectrode tip can be attributed to a combination of diffusion, catalytic decomposition of  $H_2O_2$ , and further reduction of  $H_2O_2$  to water. According to Vetter (1967), oxygen reduction at metal electrodes proceeds initially with Equation (2). At more negative potentials,  $H_2O_2$  is further reduced to water, which results in the complete reduction of oxygen to water as shown in Equation (1) (Vetter 1967). On iron electrodes, the transition from Equation (2) to Equation (1) occurs between  $-400$  mV<sub>Ag/AgCl</sub> and  $-800$  mV<sub>Ag/AgCl</sub> (Vetter 1967). Beyond –800 mV<sub>Ag/AgCl</sub>, Equation (1) dominates and H<sub>2</sub>O<sub>2</sub> production is minimal. Figure 2 shows the onset of the transition at  $-400 \text{ mV}_{Ag/AgCl}$  and its continuation through  $-650$  mV<sub>Ag/AgCl</sub>. The observation of a potential range for H<sub>2</sub>O<sub>2</sub> production provides a key point for the bioelectrochemical effect. The production of  $H_2O_2$  cannot be understood by considering current values, alone. The limitation of reporting only the current values could explain the conflicting evidence on the role of  $H_2O_2$  in inhibiting biofilm growth (Costerton et al. 1994; Busalmen and de Sanchez 2001; Shirtliff et al. 2005; Hong et al. 2008). At sufficiently negative potentials,  $H_2O_2$  could go undetected by methods sampling the bulk solution.

Figure 3A shows the  $H_2O_2$  profiles that were measured above the SS surface, from the bulk to within 100  $\mu$ m of the surface. The H<sub>2</sub>O<sub>2</sub> concentration was 15.5  $\mu$ m near the SS surface at a potential of −600 mV<sub>Ag/AgCl</sub>. When the SS was not polarized, there was no detectable H<sub>2</sub>O<sub>2</sub>. However, Figure 3A shows that H<sub>2</sub>O<sub>2</sub> was not detectable at a distance of 500 μm from the SS surface while it was polarized to −600 mV<sub>Ag/AgCl</sub>. Considering that H<sub>2</sub>O<sub>2</sub> degrades in water and that the flow cell was operated in continuous flow mode,  $H_2O_2$  was unlikely to be found in the bulk solution. This result highlights the limitation of  $H_2O_2$ measurements using bulk sampling methods in this type of system. However, it also emphasizes the suitability of the system for preventing biofilm growth near the surface. Based on the results presented here, it is expected that cells attached on the SS surface are exposed to  $H_2O_2$  concentrations of at least 15.5  $\mu$ m. The concentration of  $H_2O_2$  could be enough to prevent monolayer cell coverage ( $\sim 1 \mu$ m thick) from growing into a mature biofilm.

Figure 3B shows the oxygen profiles that were measured above the SS, from the bulk to within 100  $\mu$ m of the surface. The oxygen concentration decreased to ~ 3.5 mg l<sup>-1</sup> near the SS surface from a bulk concentration of ~ 7.0 mg  $l^{-1}$  when the SS was polarized to –600  $mV_{Ag/AgCl}$ . When the SS was not polarized, there was a slight decrease in oxygen concentration, suggesting that cells were utilizing oxygen to respire. The consumption of oxygen while a cathodic current was measured confirms oxygen reduction as the source of

 $H_2O_2$ . The reduced DO at the SS surface also shows that the production of  $H_2O_2$  at the surface drives the environment from an oxic to a suboxic condition. Thus, if  $H_2O_2$  exposure is the primary mechanism of action of the bioelectrochemical effect, a simultaneous decrease in oxygen may also play a role. Since one of the proposed mechanisms of action, as described in the literature, is pH changes caused by the passing of current, pH variation also was quantified in the current study; there were no detectable pH changes near the SS surface (results not shown). This was expected, since the measured current was too low for the detection of significant pH changes at this buffer strength (Babauta et al. 2011).

One of the major limitations of this method of controlling biofilm growth is the requirement that oxygen be present at the SS surface. If a thick biofilm initially covered the SS surface, the DO concentration would be expected to be zero near the bottom of the biofilm, which would prevent  $H_2O_2$  production (Renslow et al. 2011). Perhaps this, too, is a reason for the conflicting data in the literature. The method could be optimized for thicker biofilms by increasing the delivery of oxygen to the surface, but the added energy input would still make this method less efficient for thicker biofilms. Since the biofilm in the current study was a single layer of cells, there was oxygen available on the surface. Using these thin biofilms, it was possible to assess the effect of  $H_2O_2$  production on biofilm growth.

#### **Biofilm formation on the non-polarized and polarized SS coupons**

To assess the effect of the H<sub>2</sub>O<sub>2</sub> generated by applying a potential of −600 mV<sub>Ag/AgCl</sub>, a monolayer of cells was exposed for 40 h, as shown in Figure 4. The initial cell surface coverage was  $\sim 1.9 \pm 0.5$ % for both nonpolarized and polarized SS surfaces. There was no statistical difference in initial surface coverage by biofilms ( $P = 0.808$ ). The surface coverage increased on the non-polarized SS surface to  $99 \pm 0.6\%$  after 40 h, whereas the surface coverage remained almost constant for the polarized SS surface. The differences between the non-polarized and polarized SS surfaces were statistically significant (*P* 0.001). It was clear that uncontrolled cell growth on the non-polarized SS surfaces resulted in large biofilm clusters. In contrast, dim patches of light intensity behind a sparsely populated SS surface characterized the polarized SS surface. No small or large biofilm clusters were observable, signifying that biofilm growth was delayed. In a similar experiment, initially attached cells were treated with 50  $\mu$ m H<sub>2</sub>O<sub>2</sub> in the bulk solution and the surface coverage was monitored. Nearly identical results were observed for externally added  $H_2O_2$  as for electrochemically produced  $H_2O_2$  (data not shown). The addition of  $H<sub>2</sub>O<sub>2</sub>$  to the bulk solution resulted in delaying biofilm growth. Interestingly, this suggests that the decrease in DO during oxygen reduction at the SS surface played only a minor role in delaying biofilm growth.

Figure 5A plots this time series and shows the variation with time of surface coverage of the SS surface. The non-polarized SS surface showed an exponential increase in surface coverage similar to the exponential growth measured by optical density. The polarized SS surface showed no measurable increase in surface coverage over time, which demonstrates the effectiveness of polarization in controlling biofilm growth. Over the length of the 40-h exposure, the current reached a steady state value of  $\sim 60 \mu A$ . Thus, it is thought that the monolayer of cells was exposed to at least  $15.5 \mu m H_2O_2$  under the polarized condition and

a subsequent decrease in DO. Although seemingly small, these  $H_2O_2$  concentrations have been shown to cause DNA damage (Linley et al. 2012).

#### **SEM analysis of biofilm growth on SS surfaces**

To confirm the images presented in Figure 4, SEM images were taken of the SS coupons after fluorescent imaging. The SEM images in Figure 6 show that the non-polarized surface was covered with cells (Figure 6A), while fewer cells colonized the polarized surface (Figure 6B). Higher magnification of individual cells on the non-polarized SS surface showed intact cell walls (Figure 6C). On the polarized SS surface, membrane-compromised cells surrounded by scattered deposits of material were observed (Figure 6D). It has been shown that cell walls and cell membranes of *P. aeruginosa* 19142 are deformed when treated with  $H_2O_2$  (DeQueiroz and Day 2007). This is because  $H_2O_2$  targets thiol groups of enzymes on the cell wall (Denyer and Stewart 1998). Intracellular contents are lost and, as a result, cell volume decreases (Linley et al. 2012). Similar images were also obtained by Diao et al. (2004) when cells were treated with  $H_2O_2$ . The scattered deposits observed in Figure 6D were identified as cell debris. These two observations provide further evidence that the electrochemical production of  $H_2O_2$  at the SS surface was the cause of the delayed biofilm growth.

Figures 4 and Figure 6B show that despite the 40-h polarization treatment, some cells were able to survive and persist on the polarized SS surface. This could be the result of heterogeneous current distribution on the SS surface, increased catalase production by these surviving cells, or a combination of both. Since these cells expressed GFP, they were most likely alive as demonstrated in the literature (Nancharaiah et al. 2005). Interestingly, catalase actively degrading  $H_2O_2$  could be another reason for  $H_2O_2$  not being detected in the bulk solution. This possibly explains why some of the previously published studies found  $H_2O_2$ , while others did not. Regardless of the mechanism that these cells used to survive, the bioelectrochemical effect did not kill all the cells on the polarized SS surfaces observed in this study. Thus, it is important to note that, although  $H_2O_2$  has a biocidal effect on cells, the bioelectrochemical effect as a whole should be considered biostatic rather than biocidal.

#### **Practical implications**

In this research, it was demonstrated that  $H_2O_2$  is produced on SS surfaces and that it can be used to prevent biofilm growth. However, for  $H_2O_2$  production, the biofilm must be thin and allow oxygen penetration to the bottom.  $H_2O_2$  cannot be produced when there is no DO on the SS surface. Thus, the thickness of the biofilm could be a critical factor when controlling biofilm growth electrochemically. Perhaps the best method of preventing cell growth on SS surfaces is to keep the potential of the surface at  $-600 \text{ mV}_{Ag/AgCl}$  as soon as the process starts. Continuous  $H_2O_2$  production may delay biofilm growth but may not eliminate longterm biofilm growth. Fewer cells might colonize but be able to survive and persist. Although a catalase-positive bacterium that can actively decompose  $H_2O_2$  was used in this study, electrochemically produced  $H_2O_2$  showed the biocidal effect. This technique could be more effective on catalase-negative bacteria. The presence of catalase could be critical in some systems if the biofilm producing catalase decomposes the produced  $H_2O_2$  to oxygen. This

could potentially prevent the biocidal effect of  $H_2O_2$ , as demonstrated by others (Liu et al. 1998; Stewart et al. 2000).

# **Conclusions**

In this work,  $H_2O_2$  production and dissolved oxygen consumption were quantified on polarized 316L SS surfaces using microelectrodes. The produced  $H_2O_2$  was used to control *P. aeruginosa* PAO1 biofilm growth on the SS surfaces. The following conclusions have been reached: (1) H<sub>2</sub>O<sub>2</sub> is produced at potentials below  $-400 \text{ mV}_{Ag/AgCl}$  on SS surfaces. (2) When the SS surface is polarized to –600 mV<sub>Ag/AgCl</sub>, the H<sub>2</sub>O<sub>2</sub> concentration increases towards the surface, while the dissolved oxygen concentration decreases. There was no H2O2 production or dissolved oxygen consumption on non-polarized clean surfaces. (3) When polarized and non-polarized surfaces with identical biofilms continued to be fed with fresh medium, polarization prevented biofilm growth, while there was significant biofilm growth on non-polarized surfaces. (4) There was cell debris deposited on the polarized surfaces, while there was no cell debris on non-polarized surfaces, indicating the biocidal effect of  $H_2O_2$ . (5) Overall,  $H_2O_2$  produced on a SS surface can be used to control biofilm growth. However, this requires a continuous flux of dissolved oxygen to the surface.

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#### **Figure 1.**

Schematic configuration of experimental setup and flat plate flow cell. The figure is not drawn to scale



# **Figure 2.**

Transient H2O2 concentration variation with potential 100 *μ*m from the SS surface. The black solid line represents the zero concentration line. The dashed line is the current measured during the potential sweep.



#### **Figure 3.**

(A)  $H_2O_2$  profiles above both non-polarized SS surfaces ( $O$ ) and polarized SS surfaces ( $\bullet$ ). The black dashed line is fitted to points between 100 and 215  $\mu$ m ( $R^2 = 0.997$ ). (B) Oxygen profiles above both non-polarized SS surfaces (○) and polarized SS surfaces (●). The current density was  $25.14 \mu A \text{ cm}^{-2}$ .

# Non-polarized Polarized  $t=0$  h  $t=40$  h

#### **Figure 4.**

Images of *P. aeruginosa* PAO1 on non-polarized and polarized surfaces at  $t = 0$  and  $t = 40$  h (four images shown for each condition). The initial surface coverages were identical (1.9  $\pm$ 0.5). However, the final surface coverages were statistically different (*P* 0.001). The image size is 204.8 *μ*m × 163.83 *μ*m.



#### **Figure 5.**

(A) The variation in surface coverage of polarized ( $\bigcirc$ ) and non-polarized ( $\bigcirc$ ) 316L SS surfaces over time. (B) The variation in current over time for the polarized 316L SS.



