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Evaluating continuum solvation models for the electrodeelectrolyte interface: challenges and strategies for improvement

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Abstract

Ab initio modeling of electrochemical systems is becoming a key tool for understanding and predicting electrochemical behavior. Development and careful benchmarking of computational electrochemical methods are essential to ensure their accuracy. Here, using charging curves for an electrode in the presence of an inert aqueous electrolyte, we demonstrate that most continuum models, which are parameterized and benchmarked for molecules, anions, and cations in solution, undersolvate metal surfaces, and underestimate the surface charge as a function of applied potential. We examine features of the electrolyte and interface that are captured by these models, and identify improvements necessary for realistic electrochemical calculations of metal surfaces. Finally, we reparameterize popular solvation models using the surface charge of Ag(100) as a function of voltage to find improved accuracy for metal surfaces without significant change in utility for molecular and ionic solvation.

Accurate modeling of the electrode-electrolyte interface is an active challenge for the computational electrochemical community, and solving it will enable rapid and systematic improvement of electrocatalysts, reactants, and electrolytes. Models for the electrode-electrolyte interface must not only describe the reactants and surface of interest with high chemical accuracy (using *ab initio* techniques such as density functional theory (DFT)), but also accurately describe the changing interfacial charge distribution with potential, to correctly predict mechanisms and kinetics (onset voltage, barrier heights) of electrochemical reactions. Calculation of the charge on a given surface at a given voltage requires both the surface capacitance, and the fluid contribution to the capacitance which is a thermodynamic average of solvent and electrolyte ion configurations. The number of necessary configurations, and the low relative concentration of electrolyte ions which necessitates inclusion of large numbers of solvent molecules for meaningful statistics, makes these calculations difficult and computationally expensive.

To make this problem more tractable, a number of approaches have been developed to perform *ab initio* modeling of the electrified interface, from canceling out the surface charge

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through a uniform opposite charge across the entire cell,¹ or through introducing localized classical counter-charges in the effective screening medium approach,² to including protons far away from the cell to cancel the charge on the surface.³ These approaches do not approximate the spatial distribution of charge in the electrolyte, which can significantly influence the structure and energetics of some adsorbates. An alternative is the solvation model approach with a dielectric continuum description of the solvent,⁴ wherein Debye screening due to the electrolyte cancels out the surface charge.^{5,6} These continuum approaches improve upon previous vacuum extrapolation techniques, and possibly also upon calculations including only one or two explicit water molecule layers,⁷ as they include the response of the electrolyte to the charged surface.

Solvation models for use in *ab initio* calculations were originally designed primarily for the solvation of non-periodic systems of small, neutral molecules. Fatte-bert and Gygi⁸ modified an isodensity continuum model (where the spatial extent of the continuum liquid is derived from the electron density) to make it numerically stable for periodic systems within a plane wave basis, hence allowing continuum solvation of surfaces. Treatment of charged species and interfaces in electrochemical systems additionally requires the inclusion of the response of ions in the electrolyte. The simplest approach for this is Poisson-Boltzmann (PB) theory,⁹ which treats the ions as point particles with mean-field interactions. The drastic approximation of treating the solvent and ions as a continuum lead to bound charge distributions that are closer to the solute than expected.⁵ Fitting the models to solvation energies results in good agreement for electrostatic interactions between solute and the solvent dielectric response despite differences in the spatial distributions. However, the ionic response is not constrained by fits and tends to be overestimated in the PB approach.

The ionic response plays a smaller role than the solvent dielectric in the overall energetics of the continuum solvation approach; nonetheless different approaches have been attempted to alter its spatial extent and intensity. Jinnouchi and Anderson restricted the ionic response to one solvation shell away from the solute, creating an approximation of the Stern layer.^{10,11} Modifications of the mean-field PB approach to incorporate Stern layer effects is also an area of active development.^{12–15} We introduced an alternate approach (NonlinearPCM) based on the classical density-functional theory of liquids¹⁶ that incorporates a packing limit to stabilize against large ionic response, but uses the same cavity for the liquid (dielectric) and ionic response.¹⁷ For high ionic concentrations, an even simpler approach is to use the linearized Poisson-Boltzmann equation (LinearPCM), which avoids these issues from the beginning by precluding large build-up of ionic charge.^{5,17} Here we focus on such singlecavity models of solvent and electrolyte response in this work, which have recently attracted attention as a way to perform routine, affordable electrochemical calculations. These models have been applied to examine electrochemical reactions including formic acid oxidation¹⁸ and underpotential hydrogen deposition¹⁹ on platinum, and CO₂ reduction on copper.^{20,21} They have also been applied to predict electrochemical capacitance in new classes of electrodes such as graphene and borophenes for supercapacitor applications.^{22,23}

Careful benchmarking of these models is crucial to understanding their accuracy for a variety of systems, but so far few comparisons with electrochemical experiments exist and hence the accuracy of these models is poorly understood. Prior efforts in this direction

include finding the potential at which specific processes such as changing molecular orientation occur,²⁴ but the indirect dependence on electrolyte model in these processes limit the information that can be derived about model accuracy.

A direct test of model accuracy for charging behavior of the electrode, with readily available corresponding experimental measurements, is the capacitance of the electrochemical interface. In particular, the capacitance of the single-crystalline Ag(100) surface is an ideal test case since it exhibits double-layer behavior without specific adsorption or surface reconstruction over a wide potential range. This is seen in at least two experiments in (nearly) non-adsorbing electrolytes: in aqueous NaClO₄ electrolyte by Hamelin25 and in aqueous KPF₆ electrolyte by Valette.²⁶ The experimental differential capacitance appears to be nearly symmetric as a function of potential around the potential of zero charge (PZC) – more so for KPF₆ than NaClO₄, suggesting that specific adsorption of ions (especially anions) is not a significant problem with these electrolytes. Consequently, here we use these Ag(100) capacitance measurements to test and refine solvation approaches for electrochemistry.

We perform DFT calculations with various solvation models using previously established methodology from Ref. 27. Briefly, we use the JDFTx code,²⁸ with the PBE exchange-correlation functional,²⁹ the GBRV ultrasoft pseudopotential set³⁰ at its recommended plane-wave cutoffs of 20 E_h for orbitals and 100 E_h for charge density. We utilize a larger fluid spacing of 60.8 Å between the metal slabs to capture the longer range response of the fluid models at lower ionic concentrations (such as 0.01M), and use truncated Coulomb potentials to minimize interactions between periodic images.³¹ We include DFT-D2 dispersion corrections³² for the calculations with explicit water molecules in DFT to correctly describe the binding energy and distance. Additionally, because of the increased computational expense of performing the calculations with explicit water molecules, for these calculations we use a smaller fluid spacing (14.7 Å), and limit our calculations to 1 M ionic concentration.

We compare surface charges calculated using different solvation models as a function of potential, with experimental estimates of the surface charge obtained by digitizing differential capacitance data from Refs. 25 and 26, and numerically integrating outwards from the PZC. Fig. 1 shows that most of the commonly used continuum solvation models in DFT calculations of electrochemical systems severely underestimate the surface charge of the Ag(100) surface. In fact, at 0.5 V above the PZC of Ag(100), the charge on the surface is already underestimated by more than a factor of two for all of the solvation models, and this worsens with increasing potential. We therefore expect that electrochemical reactions that involve transfer of charge will not be accurately described by any of these models, especially at potentials far from the PZC.

LinearPCM¹⁷ and SCCS,^{33,34} which approximate the electrolyte response with a linearized Poisson-Boltzmann equation, are the worst performers. Note that the commonly used VASPsol code³⁵ exactly implements the LinearPCM model. Therefore this underestimation is an issue in the primary solvation models available in all major plane-wave DFT software. NonlinearPCM, which solves the (full) Poisson-Boltzmann equation, accounting for

dielectric saturation in the solvent response, and nonlinear enhancement and packing effects in the ionic response,¹⁷ performs marginally better than the linearized models. All of these models have an ionic response that likely is too close to the solute, but this would lead to overestimation rather than underestimation of charge, and hence is not the reason for the incorrect capacitance. Instead, they all contain a parameter (or more) to define the spatial extent of the electrolyte, which is fit to molecular solvation energies, with no ions or metallic surfaces included in these parameterization datasets. This procedure of parameterizing solvation models to solely neutral molecules results in an undersolvation of metals, with charge underestimation as a consequence. (See Ref. 17 for a detailed discussion of the solvation models and their parametrization.)

The CANDLE solvation model also solves the linearized Poisson-Boltzmann equation, but it is fit to molecules and ions, and adjusts the spatial extent of the electrolyte depending on the local charge of the solute to describe differences in cationic and anionic solvation.²⁷ Fig. 1 shows that the CANDLE capacitance agrees well with experiment for potentials negative of the PZC, but underestimates it similarly to the other solvation models for positive potentials. The anionic parameterization, which yields a fluid cavity that is smaller than that for neutral molecules and cations, appears to be suitable for the metallic surfaces (regardless of charge), whereas the cationic/neutral parameterization undersolvates the surface.³⁶

While the bare solvated surface might be an ideal way to test the accuracy of the solvation model, in practice, DFT calculations frequently include a monolayer or more of explicit (DFT) water molecules. Fig. 2 compares the change in surface charge with voltage between a calculation performed with one explicit water molecule with nonlinearPCM adjacent and above it, with that of the bare solvated surface. A larger unit cell with two Ag atoms per surface was used for these calculations so that explicit water molecules are surrounded by the continuum solvent and we can avoid geometric issues such as hydrogen bond frustration between neighbouring water molecules (which would necessitate large unit cells and molecular dynamics). In this case, there are two free energy local-minimum configurations of the water molecule, with the water molecule dipole pointing towards or away from the surface, which differ significantly in surface charge at the same potential. The global free energy minimum changes from one of these configurations to the other at the PZC, resulting in a large change in the thermodynamically averaged surface charge (weighted by Boltzmann factors of the calculated Gibbs free energies). This average charge therefore exhibits a much steeper slope with potential than experiment within 0.4 eV of the PZC due to this change in dipole, and a smaller slope comparable to NonlinearPCM further away from the PZC due to the continuum model response.

The above thermodynamic averaging procedure between two water configurations grossly approximates features of the surface charging curve that are observed experimentally, but it is non-trivial to systematically extend this treatment to a larger number of configurations with multiple water molecules. With increasing number of molecules, the configurations would be less clearly defined, and expensive thermodynamic sampling using molecular dynamics will become necessary. Even if feasible computationally, hybrid treatments combining molecular dynamics in few explicit layers and continuum solvation above require further method development to ensure proper matching of the explicit and continuum

solvents, while preventing explicit solvent molecules from drifting into the continuum solvent.

Here, we explore an alternate practical approach of reparametrizing solvation models to potentially correct for the undersolvation of metal surfaces. In the LinearPCM / VASPsol and NonlinearPCM models, the distance from the solute at which the continuum solvent appears is controlled by an electron density threshold parameter n_c .¹⁷ (The SCCS model^{33,34} uses two electron density parameters ρ_{min} and ρ_{max} in a formally different but functionally equivalent parameterization.) To correct the surface charging behavior of Ag(100), we adjust the value of n_c for the nonlinear model to match the surface charge at the highest potential reported experimentally in Ref. 25 (0.6 V above PZC). For the linear model, we report the reparameterization of this model against the surface charge of the nonlinear model at 1M ionic strength. Fig. 3 illustrates that the resulting higher n_c (reported in Table III and discussed further below), which defines the continuum fluid as beginning closer to the metal leads to good agreement with the experimental charge/voltage relationship for this surface.

To examine how the reparameterized model performs for other metal surfaces, we next calculate and compare the differential capacitance of Pt(111). A single value for the capacitance of the Pt(111) surface has been estimated experimentally,³⁷ and previously reported for continuum and explicit solvation model approaches, as shown in Table I. The continuum models predict lower capacitance for the Pt(111) relative to the experimental estimate, while explicit solvation predicts a higher capacitance, with a similar magnitude of discrepancy. The refit NonlinearPCM model more closely agrees with the explicit solvation results. However, the degree to which we accurately predict the capacitance is difficult to determine, since we are comparing to a single experimental estimate reported with no error bars.

To understand the transferability of our refit models for use under other common electrochemical conditions, we next evaluate the behavior of the refit models as a function of ionic concentration. Figure 4 illustrates the success of the nonlinear model in capturing the surface charge characteristics as a function of decreasing ionic strength, and the drastic failures of the linear model. This is in agreement with previous qualitative explorations of the importance of nonlinear behavior⁶. We note limitations in the nonlinear model, however. Solely reparameterizing the solvation model does not capture all of the nonlinearity of the surface charging curve with voltage, and in particular underestimates the Gouy-Chapmann behavior seen experimentally at lower ionic strengths at voltages near the PZC, which requires further investigation.

While the refit models are promising for metal surfaces, the reparameterization of only the cavity threshold n_c results will necessarily oversolvate molecules and ions for which the original n_c was optimized. This can be mitigated somewhat by refitting the second parameter in these models which capture the non-electrostatic contribution to solvation, represented by a cavity surface tension parameter *t*. (See Ref. 17 for more details about the fit parameters.) Table II lists the mean absolute errors for the solvation energies of a set of molecular and ionic species for the original and refit models. The reparameterized nonlinearPCM performs better for cations, slightly worse for anions and neutral molecules, and overall marginally

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better for the combined set. The resulting improvements for metal surfaces though, makes this parameterization preferred over that of the original. Table III lists the original and refit parameters, so that these new values can be utilized for future calculations.

Table II shows that the reparametrization worsens the accuracy of LinearPCM for molecules and cations, while slightly improving it for anions, again a consequence of anions being undersolvated to start with. Table III reports the corresponding parameters which can be used for improving the predictions for metal surfaces in implementations of NonlinearPCM and LinearPCM, such as in VASPsol³⁵ and JDFTx.²⁸

This work illustrates that design of continuum solvation models for describing charged metal electrodes must include short-range cavity parameterization that simultaneously leads to correct molecular and ionic solvation energies, as well as differential capacitance curves for metal surfaces. Describing the nonlinearity in the ionic response is further important for describing these systems correctly at lower ionic strengths. Benchmarking against the surface charging for Ag(100) provides a way to compare performance of electrolyte models. Our reparameterization of both the linear and nonlinear solvation models provide better options for electrochemical calculations in which the charge of the surface might be important. Despite the fact that we have demonstrated the serious limitations of the LinearPCM model for lower ionic strengths, the linear model is currently more widely available (in codes other than JDFTx, for example). Therefore, we recommend using the reparameterized NonlinearPCM model for computational electrochemical calculations of metallic surfaces, but if that is not possible, we suggest utilizing the reparameterized LinearPCM model at 1 M ionic strength as a work around, regardless of the expected or actual experimental ionic strength.

Additionally, we note that further careful experimental measurements of the differential capacitance of several single-crystalline metal surfaces in non-adsorbing electrolytes are necessary to guide the development of the next generation of solvation models that can achieve simultaneous accuracy for molecules, ions and electrodes.

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FIG. 1.

Left: Surface charge as a function of electrode potential at 0.1 M ionic concentration for LinearPCM¹⁷, CANDLE²⁷, NonlinearPCM¹⁷, and the SCCS^{33,34} solvation models, compared to experimental data from Hamelin²⁵ for NaClO₄ and Valette²⁶ for KPF₆. Right: Bound charge in the NonlinearPCM continuum solvent at 0.6 V above PZC.



FIG. 2.

Left: Surface charge as a function of electrode potential for a Ag(100) surface with continuum solvation, and with a single (DFT) water molecule above the surface. The blue points are individual minimized configurations of the water, and the blue line is the thermodynamic average of the two configurations, using the Gibbs free energies of the configurations at a given potential. Right: Bound charge in the continuum solvent above the bare Ag(100) and surrounding the single explicit water molecule above Ag(100) at 0.6 V above PZC.



FIG. 3.

Left: NonlinearPCM with the density cutoff parameter n_c from a molecular fit, Ref. 17, and with a value for n_c that more accurately captures the differential capacitance of Ag(100), for 0.1 M ionic concentration. Right: Bound charge in the fluid for the original NonlinearPCM and the refit Non-linearPCM at 0.6 V above PZC.



FIG. 4.

Comparison of surface charge predicted by refit NonlinearPCM, and refit LinearPCM with experimental data from Hamelin²⁵ for NaClO₄ and Valette for KPF_6^{26} for different ionic concentrations: (a) 1M, (b) 0.1M and (c) 0.01M. NonlinearPCM qualitatively captures the variations in capacitance with potential and ionic concentration, whereas LinearPCM fails.

TABLE I

Capacitance for Pt(111) by different methods, including the reparameterization for the last two models described here.

Method	Source	Value (µF/cm ²)	
Experimental estimate	Ref. 37	20	
Calculated:			
Explicit H^+ and H_2O	Ref. 38	26	
LinearPCM	This work	14	
NonlinearPCM	This work	17	
CANDLE	This work	11	
Refit NonlinearPCM	This work	29	
Refit LinearPCM	This work	31	

TABLE II

Mean absolute errors in kcal/mol (1 kcal/mol is 0.0434 eV) for NonlinearPCM and LinearPCM with original parameterization, and with refit n_c and surface tension t, for the set of molecules, anions, and cations in Ref. 27.

Model	Neutrals	Cations	Anions	Combined
NonlinearPCM	1.28	16.08	27.03	7.55
Refit NonlinearPCM	1.44	14.40	27.61	7.51
LinearPCM	1.27	2.10	15.09	3.59
Refit LinearPCM	2.57	19.73	12.50	6.68

TABLE III

Parameters for the original and refit NonlinearPCM and LinearPCM models, and the corresponding reference electrode potential V_{SHE} calibrated to experimental potentials of zero charge of single-crystalline Ag, Au and Cu surfaces.

Parameters	$n_c [a_0^{-3}]$	$t\left[E_h/a_0^2\right]$	V _{SHE} [V]
NonlinearPCM	$1.0 imes 10^{-3}$	$9.5 imes10^{-6}$	4.62±0.0917
Refit NonlinearPCM	$2.2 imes 10^{-3}$	2.6×10^{-5}	4.33±0.09
LinearPCM	$3.7 imes 10^{-4}$	$5.4 imes10^{-6}$	$4.68{\pm}0.09^{17}$
Refit LinearPCM	$1.4 imes 10^{-3}$	4.2×10^{-5}	4.10 ± 0.05