



# Production of Ophthalmic Acid Using Engineered Escherichia coli

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**ABSTRACT** Ophthalmic acid (OA; L- $\gamma$ -glutamyl-L-2-aminobutyryl-glycine) is an analog of glutathione (GSH; L- $\gamma$ -glutamyl-L-cysteinyl-glycine) in which the cysteine moiety is replaced by L-2-aminobutyrate. OA is a useful peptide for the pharmaceutical and/or food industries. Herein, we report a method for the production of OA using engineered *Escherichia coli* cells. *yggS*-deficient *E. coli*, which lacks the highly conserved pyridoxal 5'-phosphate-binding protein YggS and naturally accumulates OA, was selected as the starting strain. To increase the production of OA, we overexpressed the OA biosynthetic enzymes glutamate-cysteine ligase (GshA) and glutathione synthase (GshB), desensitized the product inhibition of GshA, and eliminated the OA catabolic enzyme  $\gamma$ -glutamyltranspeptidase. The production of OA was further enhanced by the deletion of *miaA* and *ridA* with the aim of increasing the availability of ATP and attenuating the unwanted degradation of amino acids, respectively. The final strain developed in this study successfully produced 277  $\mu$ mol/liter of OA in 24 h without the formation of by-products in a minimal synthetic medium containing 1 mM each glutamate, 2-aminobutyrate, and glycine.

**IMPORTANCE** Ophthalmic acid (OA) is a peptide that has the potential for use in the pharmaceutical and/or food industries. An efficient method for the production of OA would allow us to expand our knowledge about its physiological functions and enable the industrial/pharmaceutical application of this compound. We demonstrated the production of OA using *Escherichia coli* cells in which OA biosynthetic enzymes and degradation enymes were engineered. We also showed that unique approaches, including the use of a  $\Delta yggS$  mutant as a starting strain, the establishment of an S495F mutation in GshA, and the deletion of *ridA* or *miaA*, facilitated the efficient production of OA in *E. coli*.

**KEYWORDS** ophthalmic acid, pyridoxal 5'-phosphate, glutathione, YggS

Ophthalmic acid (OA; L- $\gamma$ -glutamyl-L-2-aminobutyryl-glycine) was initially identified to be a glutathione (GSH; L- $\gamma$ -glutamyl-L-cysteinyl-glycine) analog in calf lens (1) and was later detected in the lenses of many higher animals (2) and in microorganisms (3–5). OA is produced through the consecutive reactions of glutamate (Glu)-cysteine (Cys) ligase (GshA) and glutathione synthase (GshB), which are the same enzymes involved in the synthesis of GSH (Fig. 1). Owing to the structural similarity between OA and GSH, OA is used as a non-thiol-containing analog of GSH (6, 7). OA is known to inhibit both the degradation of insulin in sections of rat adipose tissue (8) and the activity of glyoxalase I (9). A recent study that profiled liver metabolites following acetaminophen-induced hepatotoxicity reported that the concentration of OA is closely correlated with GSH consumption in mouse serum and liver. This observation has raised the possibility that OA can be used as an oxidative stress biomarker to indicate hepatic GSH consumption (10). In *Synechocystis* sp. strain PCC6803, OA was proposed to be a stress-induced marker of L-Cys depletion, which is triggered by the Received 19 December 2017 Accepted 13 January 2018

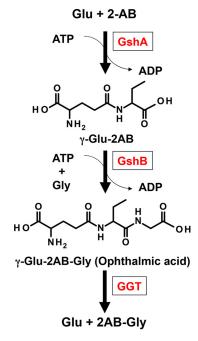
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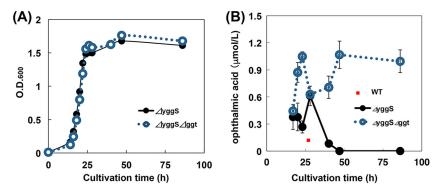


**FIG 1** Biosynthesis and degradation pathway of OA. Abbreviations: GshA, glutamate-cysteine ligase; GshB, glutathione synthase; GGT, γ-glutamyltranspeptidase; 2-AB, 2-aminobutyrate.

increased demand for GSH biosynthesis under conditions of stress (4). In addition, recent studies have revealed that GSH, OA,  $L-\gamma$ -glutamyl-L-valyl-glycine, and their analogs activate the calcium-sensing receptors of humans and act as kokumi substances that modify the five basic tastes (11, 12).

Although OA has potential applications in the pharmaceutical and/or food industries, it is currently a highly expensive substance. The development of an efficient method to produce OA will enable us to perform further research on this molecule and investigate its potential applications in the pharmaceutical and/or food industries. In the present study, we developed a method for the production of OA using engineered Escherichia coli cells. To this end, we utilized a yggS-deficient E. coli strain (E. coli  $\Delta yggS$ ) reported to accumulate OA as a starting strain (5). YggS is a highly conserved pyridoxal 5'-phosphate (PLP)-binding protein that plays important roles in the homeostasis of amino acids and/or B6 vitamers (13, 14). In addition, we deleted y-glutamyltranspeptidase (GGT), which is the primary enzyme that degrades GSH, and investigated its contribution to the degradation of OA. To enhance the OA biosynthetic pathway, we cooverexpressed GshA and GshB, eliminated the feedback inhibition ability of GshA, and evaluated their effects on the production of OA. The enamine intermediates 2-aminoacrylate/2crotonate, which are generated by the action of Ser/Thr dehydratase and transiently accumulate in enamine intermediate deaminase (RidA)-deficient cells, have been reported to inactivate several PLP-dependent enzymes involved in amino acid metabolism (15–17). To attenuate the unwanted catabolism of OA's constituent amino acids by PLP-dependent enzymes, we deleted ridA and investigated the effect on the production of OA. Hara et al., using a single-gene deletion library of E. coli strains (Keio Collection), identified some genes that, when deleted, resulted in a higher efficiency of ATP regeneration and a higher level of production of GSH in the deletion mutant than in the parental strain (18, 19). Among them, we selected two genes, ptsG and miaA, and examined the effects of deleting those genes on the production of OA.

In the present paper, we report the results of an investigation using the abovedescribed strategies to develop an efficient method for the production of OA in *E. coli*. The engineered *E. coli* strain constructed by combining these approaches specifically produced ~80 mg/liter of OA with a yield of 28% in 24 h.



**FIG 2** Effect of *ggt* deletion on growth (A) and cultivation time-dependent changes of the OA content (B).  $\Delta yggS$  and  $\Delta yggS \Delta ggt$  cells were cultivated by cultivation method A in the absence of Cam and IPTG (without amino acid supplementation). Samples were collected at the indicated times, and the cultivation time-dependent changes of the OA content were analyzed by amino acid analyses. All results are expressed as means  $\pm$  standard deviations of the data obtained from at least 3 independent experiments. WT, wild type.

## **RESULTS AND DISCUSSION**

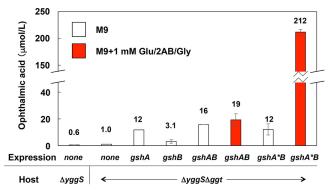
**The deletion of GGT effectively reduces the degradation of OA.** With the aim of increasing the production of OA, we sought to identify and disrupt the enzymes responsible for OA degradation in *E. coli*. Previous studies have demonstrated that both GGT and tripeptidase (PepT) play important roles in GSH degradation and that GGT contributes to GSH degradation to a greater extent than PepT in *E. coli* (20, 21).

Thus, we constructed a *yggS* and *ggt* double-knockout strain (*E. coli*  $\Delta yggS$   $\Delta ggt$ ) and examined the effect on OA degradation. The deletion of *ggt* did not significantly affect the growth rate of the *E. coli* cells in M9 medium (Fig. 2A). With the parental strain (*E. coli*  $\Delta yggS$ ), the highest concentration of OA during the cultivation period was observed at 28 h (0.6  $\mu$ mol/liter). The concentration of OA subsequently decreased with prolonged cultivation and was below the detection limit at 86 h. With the  $\Delta yggS$   $\Delta ggt$  strain, the highest concentration of OA was 1.0  $\mu$ mol/liter and the OA content did not decrease with prolonged cultivation (Fig. 2B). These results demonstrate that GGT is crucial for the catabolism of OA and that the deletion of OA with prolonged cultivation. The reason for the transient decrease in the content of OA during the cultivation period is currently unclear.

**GshA-GshB coexpression increases the production of OA.** OA is synthesized by the actions of GshA and GshB (Fig. 1). Our previous study showed that the overexpression of GshA or GshB effectively increased the content of OA in  $\Delta yggS$  cells in the log phase (5). We thus overexpressed GshA or GshB in the *ggt*-deficient strain (*E. coli*  $\Delta yggS$   $\Delta ggt$ ), which we cultivated in M9 medium until the cells reached the stationary phase of growth (88 h), and examined the effects on the production of OA. As expected, the overexpression of GshA or GshB increased the production of OA by 7.9- or 3.8-fold, respectively, compared to that for the control harboring the empty vector (Fig. 3). This result suggests that the simultaneous expression of these two enzymes may further enhance the production of OA.

To test that possibility, we constructed a GshA-GshB coexpression plasmid (pGshAB), which was then introduced into the  $\Delta yggS \Delta ggt$  strain, thereby generating  $\Delta yggS \Delta ggt$ -GshAB. The overexpression of the two enzymes was verified by sodium dodecyl sulfate-polyacrylamide gel electrophoresis and Western blotting using an anti-His tag antibody (data not shown).  $\Delta yggS \Delta ggt$ -GshAB cells produced 15.7  $\mu$ mol/liter of OA, which was an amount 10 times greater than the amount produced by the  $\Delta yggS \Delta ggt$  strain harboring the empty vector (Fig. 3).

Although  $\Delta yggS\Delta ggt$ -GshAB cells exhibited the highest levels of production of OA, the concentration was only 30% higher than the amount produced by the GshA-overexpressing strain ( $\Delta yggS\Delta ggt$ -GshA, 11.8  $\mu$ mol/liter) (Fig. 3). We speculated that the



**FIG 3** Effect of GshA and/or GshB overexpression on OA production. The  $\Delta yggS$  and  $\Delta yggS \Delta ggt$  strains harboring empty vector pCA24N (none), pCA24N-gshA (*gshA*), pCA24N-gshB (*gshB*), pGshAB (*gshAB*), or pGshA\*B (*gshA\*B*) were grown to the stationary phase by cultivation method A for 88 h with 1 mM each Glu, 2-AB, and Gly or without amino acids. The total amount of OA in the cultivation system was analyzed by amino acid analysis as described in Materials and Methods. All data are expressed as means  $\pm$  standard deviations of the data obtained after at least 3 repetitions of each assay.

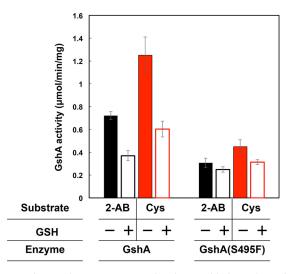
limited increase in the production of OA by  $\Delta ygg \Delta ggt$ -GshAB cells was partially due to the limited availability of certain constituent amino acids. However, when we supplemented the cells with three constituent amino acids, namely, Glu, L-2-aminobutyrate (2-AB), and glycine (Gly) (1 mM each), the production of OA was not noticeably altered (Fig. 3). This result suggests that the limited availability of an amino acid(s) was not the primary reason for the limited increase in the concentration of OA in the  $\Delta yggS\Delta ggt$ -GshAB strain.

The S495F mutation in GshA significantly increases the production of OA in the presence of amino acids. GshA exhibits strong product inhibition, which is mediated by the reduced form of GSH and limits the biosynthesis of GSH (22–24). The production of OA may also be limited by this product inhibition. The 494th and/or 495th amino acid residue in GshA has been reported to be involved in the product inhibition ability of GSH (25, 26). In addition, the S495F mutation of GshA confers resistance to its product inhibition ability (H. Suzuki, Kyoto Institute of Technology [KIT], unpublished data).

We therefore introduced the S495F mutation into GshA (referred to as GshA\*) and examined the effect on product inhibition by analyzing the activities of the Glu–2-AB and Glu-Cys ligases in the cell extracts in the presence or absence of GSH. As shown in Fig. 4, the Glu–2-AB ligase activity catalyzed by wild-type GshA was inhibited by 50% in the presence of GSH. In contrast, the activity of the GshA(S495F) mutant was not significantly affected by the presence of GSH, although its activity decreased by approximately 20%. Similar results regarding Glu-Cys ligase activity were observed. The data validate the suggestion that the S495F mutation of GshA confers desensitization of its product inhibition ability. Considering the structural similarity between GSH and OA, the S495F mutation was also expected to confer resistance to product inhibition by OA.

In the absence of amino acid supplements, the  $\Delta yggS \Delta ggt$  strain harboring pGshA\*B ( $\Delta yggS\Delta ggt$ -GshA\*B) produced 12.2  $\mu$ mol/liter of OA, which was similar to the amount produced by  $\Delta yggS\Delta ggt$ -GshAB cells (15.7  $\mu$ mol/liter) (Fig. 3). In contrast, in the presence of 1 mM each Glu, 2-AB, and Gly, the  $\Delta yggS\Delta ggt$ -GshA\*B cells produced 213  $\mu$ mol/liter of OA, which represented an 11-fold increase in the level of production compared with that by  $\Delta yggS\Delta ggt$ -GshAB cells (19.2  $\mu$ mol/liter) (Fig. 3). The production of OA by  $\Delta yggS\Delta ggt$ -GshA\*B cells was significantly stimulated by supplementation with amino acids. Eliminating the product inhibition ability of GshA and supplementing the engineered cells with amino acids was an effective way to increase the production of OA.

**Effects of varying the culture conditions.** In the production system described above, we used cultivation method A (see the Materials and Methods section). This



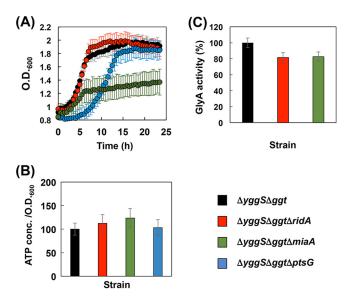
**FIG 4** Effect of GSH on GshA or GshA(S495F) activity. The Glu-2-AB (black) or Glu-Cys ligase activity (red) catalyzed by GshA or GshA(S495F) was determined as described in Materials and Methods. The reduced form of GSH significantly inhibited the enzyme activity catalyzed by GshA. All data are expressed as means  $\pm$  standard deviations of the data obtained after at least 3 repetitions of each assay.

method was time-consuming, and the cells took 4 days to reach the stationary phase, probably because the overexpression of GshA and GshB significantly inhibited cell growth. We therefore varied the cultivation conditions to shorten the cultivation time. When we used cultivation method B, in which the cell growth medium was supplemented with 1 mM each constituent amino acid of OA,  $\Delta yqqS \Delta qqt$ -GshA\*B cells produced 200  $\mu$ mol/liter of OA in 24 h, which was almost the same as the level of production under cultivation method A (212 µmol/liter; Table 1). Thus, we subsequently used cultivation method B for the production of OA. In the new cultivation method, the *E. coli* cells were used like a whole-cell biocatalyst. ΔyggSΔggt-GshA\*B cells reached the stationary phase (optical density at 600 nm  $[\mathrm{OD}_{600}],\,\sim 1.8)$  in 7 h, and the cell density was unchanged by further cultivation (Fig. 5A). A lack of supplementation with 2-AB resulted in a low level of OA production. Culturing of the cells for 24 h without shaking resulted in a low level of production of OA, indicating the importance of the oxygen supply and/or control in OA production. When we used 2.5  $\!\times$  M9 medium containing 2.5 mM each Glu, 2-AB, and Gly, the cells produced 377  $\mu$ mol/liter of OA. In M9 medium containing 5 mM each Glu, 2-AB, and Gly,  $\Delta yqgS\Delta qqt$ -GshA\*B cells produced 281  $\mu$ mol/liter and 331  $\mu$ mol/liter of OA within 24 h and 64 h, respectively

TABLE 1 Effect of cultivation conditions on OA production<sup>a</sup>

Medium	Cultivation method	Cultivation time (h)	OA concn (µmol/liter)	Yield (%)
M9	Α	88	$12 \pm 5$	
M9 plus 1 mM each Glu, 2-AB, and Gly	A	88	$212\pm5$	21
M9 plus 1 mM each Gln, 2-AB, and Gly	A	88	186 ± 7	19
M9 plus 1 mM each Glu, 2-AB, and Gly	В	24	$200 \pm 3$	20
M9 plus 1 mM each Glu, 2-AB, and Gly (without shaking)	В	24	$39\pm3$	3.9
M9 plus 1 mM each Glu and Gly	В	24	$10 \pm 1$	1.0
2.5× M9 plus 2.5 mM each Glu, 2-AB, and Gly	В	24	376 ± 60	15
M9 plus 5 mM each Glu, 2-AB, and Gly	В	24	$281 \pm 36$	5.6
M9 plus 5 mM each Glu, 2-AB, and Gly	В	64	$331 \pm 17$	6.6

 $a \Delta ygg S \Delta ggt$ -GshA\*B cells were grown by cultivation method A or B with M9 medium (or 2.5× M9 medium) containing Cam, IPTG, and the indicated concentrations of amino acids. The total amount of OA in the cultivation system was determined at the indicated cultivation times. Yield indicates the level of OA production based on the concentrations of the added amino acids. All results are expressed as means ± standard deviation of the data obtained from at least 3 independent experiments.



**FIG 5** Effect of the *ptsG*, *miaA*, or *ridA* deletion on growth, ATP level, and GlyA activity. (A) The  $\Delta yggS$ ,  $\Delta ggt$ ,  $\Delta yggS \Delta ggt \Delta ptsG$ ,  $\Delta yggS \Delta ggt \Delta ptsA^*B$  was grown for 24 h by cultivation method B with 1 mM each Glu, 2-AB, and Gly. The OD<sub>600</sub> of the cultures was monitored every 30 min using an OD-Monitor C&T apparatus (Taitec Co., Ltd.). The  $\Delta yggS \Delta ggt \Delta ptsG$ ,  $\Delta yggS \Delta ggt \Delta miaA$ , or  $\Delta yggS \Delta ggt \Delta ptsG$ ,  $\Delta yggS \Delta ggt \Delta miaA$ , or  $\Delta yggS \Delta ggt \Delta ridA$  strain harboring pGshA\*B was grown for 4 h by cultivation method B with 1 mM each Glu, 2-AB, and Gly. (B and C) The ATP concentrations in the culture medium (B) and the GlyA activity in the cell extract (C) were determined as described in Materials and Methods. Data are expressed as the means  $\pm$  standard deviations of the data obtained after 3 repetitions of each assay.

(Table 1). Increasing the concentrations of the amino acids in the medium seemed to increase the production of OA. However, the yield of OA (i.e., the efficiency of OA production) decreased as the concentrations of exogenous amino acids increased (Table 1).

**The RidA mutation alleviates the unwanted metabolism of amino acids.** Table 2 shows the concentrations of amino acids after the cultivation of  $\Delta yggS\Delta ggt$ -GshA\*B cells for 24 h by cultivation method B with 1 mM each Glu, 2-AB, and Gly. After the 24-h cultivation period, the system contained significant amounts of OA and 2-AB but less than 10  $\mu$ mol/liter each of Glu and Gly. This result indicates that approximately 80% of the supplemented Glu and Gly was consumed by pathways other than those involved in OA production. The reduction of this unwanted catabolism of the constituent amino acids will be required to obtain further increases in the production of OA.

In *E. coli*, Glu is metabolized by several PLP-dependent aminotransferases. Branchedchain amino acid aminotransferase (IIvE) and alanine-valine transaminase metabolize 2-AB, while Gly is degraded by the actions of serine hydroxymethyltransferase (GlyA)

TABLE 2 Concentrations of OA and amino acids after cultivation<sup>a</sup>

	Concn (μmol/liter)				
Component	ΔyggS Δggt strain	Δ <i>yggS Δggt</i> Δ <i>rid</i> A strain	ΔyggS Δggt ΔptsG strain	ΔyggS Δggt ΔmiaA strain	
OA	200 ± 3	231 ± 4	182 ± 18	277 ± 7	
Glu	$8.4\pm0.2$	$16 \pm 3$	$0.6\pm0.8$	ND	
2-AB	$210\pm24$	$485\pm29$	$3.4\pm0.7$	$321 \pm 21$	
Gly	$5.6\pm0.8$	$525\pm7$	$6.3\pm0.7$	583 ± 11	

<sup>*a*</sup>The  $\Delta yggS \Delta ggt$ ,  $\Delta yggS \Delta ggt \Delta ridA$ ,  $\Delta yggS \Delta ggt \Delta ptsG$ , or  $\Delta yggS \Delta ggt \Delta miaA$  strains, all of which harbored pGshA\*B, were grown by cultivation method B with 1 mM each Glu, 2-AB, and Gly. After the 24-h cultivation, the concentrations of OA and amino acids in the cultivation system were determined. Data are expressed as the means  $\pm$  standard deviations obtained from at least 3 independent experiments. ND, not detected.

and the glycine cleavage system (27, 28). Thus, PLP-dependent enzymes play primary roles in the catabolism of the constituent amino acids of OA.

In this study, we focused on RidA (reactive intermediate/imine deaminase A), which deaminates the 3- and 4-carbon enamines (2-aminoacrylate and 2-aminocapronate, respectively) that are generated as intermediates by the L-Ser/L-Thr dehydratases. In *ridA*-deficient *Salmonella enterica*, 2-aminoacrylate inactivates certain PLP enzymes, such as IlvE (29), GlyA (15, 16), and alanine racemase (17), by forming a covalent adduct in the active site. GlyA is suggested to be the most physiologically sensitive target of inactivation by 2-aminoacrylate in *S. enterica* (16). We hypothesized that the deletion of *ridA* would lead to the accumulation of 2-aminoacrylate/2-aminocapronate, resulting in the inactivation of various PLP enzymes and the attenuation of the unwanted degradation of amino acids in *E. coli* cells.

The  $\Delta yggS \Delta ggt \Delta ridA$  strain was generated, and the effect on the production of OA was examined.  $\Delta yggS \Delta ggt \Delta ridA$ -pGshA\*B cells produced 231  $\mu$ mol/liter of OA in M9 medium containing 1 mM each Glu, 2-AB, and Gly, which represented an approximately 15% increase in the level of production compared with that of the parental strain ( $\Delta yggS \Delta ggt$ -GshA\*B). Amino acid analysis revealed that the cultivation medium of the *ridA*-deficient strain retained a significant amount of Gly after fermentation (525  $\mu$ mol/liter). The residual amounts of 2-AB or Glu were also slightly increased in the *ridA*-deficient mutant compared to those in the parental strain (Table 2). These data suggest that the deletion of *ridA* especially affects the enzyme activities of GlyA, as observed in *S. enterica* (15, 16). We therefore determined the GlyA activity in the cell extracts of  $\Delta yggS\Delta ggt$ -GshA\*B and  $\Delta yggS\Delta ggt\Delta ridA$ -GshA\*B than that in the cell extract of  $\Delta yggS\Delta ggt$ -GshA\*B. The inactivation of RidA was a useful strategy for the suppression of Gly catabolism.

Exogenous Ser/Thr may further elevate the production of 2-aminoacrylate/2aminocrotonate in *ridA*-deficient cells and further increase the production of OA. We examined this possibility, but no clear correlation between the addition of exogenous Ser/Thr and the production of OA was observed (data not shown).

**The deletion of** *miaA* **increases the production of OA.** OA is produced by the sequential action of two ATP-requiring enzymes (Fig. 1). The elevation of the availability of ATP probably enables a further increase in the production of OA. Previously, Hara et al. (18) investigated the efficiency of cellular ATP regeneration in permeable *E. coli* cells using a genome-wide single-gene-deletion *E. coli* K-12 library (the Keio Collection [30]). They identified several genes to be suppressors of ATP generation, since their deletion resulted in an increase in the rate of cellular ATP synthetic activity (18). Importantly, most of the mutant strains exhibited a higher rate of ATP-driven GSH synthesis than the parental strain (19).

We selected two genes, *miaA* and *ptsG*, from the list of genes whose mutation increases ATP-driven GSH synthesis (19) and investigated whether the deletion of those two genes could similarly increase the amount of OA synthesized. The deletion of *miaA* or *ptsG* was previously reported to increase total cellular ATP synthetic activities by 371% or 218%, respectively. Moreover,  $\Delta ptsG$  or  $\Delta miaA$  cells expressing  $\gamma$ -glutamylcysteine synthase (GSH I) and glutathione synthase (GSH II) exhibited ~400% more GSH production than the corresponding wild-type cells (19). *ptsG* encodes a subunit of a glucose phosphotransferase system permease and participates in the transport of glucose (31). *miaA* encodes dimethylallyl diphosphate:tRNA dimethylallyltransferase, which catalyzes the addition of a 5-carbon isopentenyl moiety to the exocyclic amine of A37 to yield *N*<sup>6</sup>-isopentenyladenosine (32, 33).

As shown in Table 2,  $\Delta yggS\Delta ggt\Delta ptsG$ -GshA\*B produced 182  $\mu$ mol/liter of OA when using cultivation method B, in which the growth medium was supplemented with 1 mM each of the constituent amino acids of OA. This value was slightly lower than that observed for the parental strain ( $\Delta yggS\Delta ggt$ -GshA\*B). The ATP levels in the cultivation system of  $\Delta yggS\Delta ggt\Delta ptsG$ -GshA\*B was comparable to that in the cultivation system of  $\Delta ygg \Delta ggt$ -GshA\*B under the conditions examined (Fig. 5B). In addition, we found that the strains with the *ptsG* deletion showed significantly lower growth rates and OD<sub>600</sub> values in the stationary phase than the parental strain (Fig. 5A). The deletion of *ptsG* may hamper the glucose uptake of the cells and suppress their ability to consume glucose, and the *ptsG* mutant cells might consume other nutrients, such as Glu, 2-AB, and Gly, at a higher rate.

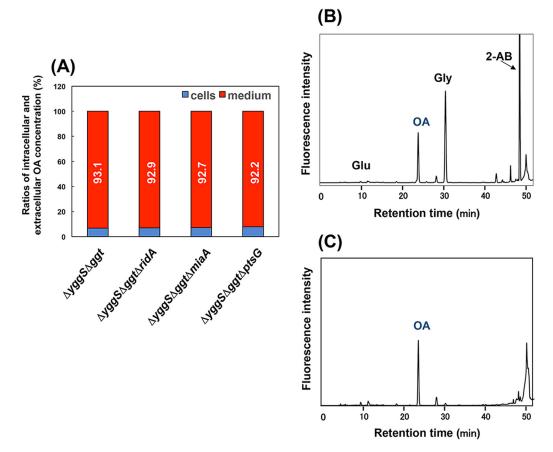
Under similar conditions,  $\Delta yqgS\Delta qqt\Delta miaA$ -GshA\*B cells produced 277  $\mu$ mol/liter of OA, which was a 39% increase compared with the amount produced by the parental strain (Table 2). The yield of OA on the basis of the amounts of exogenous amino acids added was 28%, which was the highest yield of OA production detected in the present study. The ATP levels in the cultivation system of  $\Delta yqgS\Delta qqt\Delta miaA$ -GshA\*B were  $\sim 20\%$ higher than those in the cultivation system of  $\Delta yqqS\Delta qqt$ -GshA\*B under the cultivation conditions examined (Fig. 5B), which probably contributed to the increase in the level of the OA production in the miaA-deficient strain. Interestingly, we noticed after 24 h of cultivation of  $\Delta y q g \Delta q g t \Delta m i a A$ -GshA\*B that the culture medium contained substantial amounts of Gly (Table 2). Assays of GlyA activity identified a decrease in GlyA activity in the cell-free extract of  $\Delta yqqS\Delta qqt\Delta miaA$ -GshA\*B, which probably explains the reduced consumption of Gly in the cultivation system of  $\Delta y q g \Delta q d \Delta m a A$ -GshA\*B. The deletion of miaA is known to affect the expression of several genes, including operons of phenylalanine biosynthesis (34), tryptophanase (35), and phenylalanine-tRNA synthase (36). The expression of glyA may be decreased in the miaA background. In addition, *ΔyggSΔgqtΔmiaA*-GshA\*B exhibited slow growth under the cultivation conditions examined (Fig. 5A). All these effects that appeared with the miaA deletion may contribute to the increase in the level of OA production.

OA specifically accumulates in the culture media of the engineered *E. coli* strains. Using the four engineered *E. coli* strains ( $\Delta yggS\Delta ggt$ -GshA\*B,  $\Delta yggS\Delta ggt\Delta ridA$ -GshA\*B,  $\Delta yggS\Delta ggt\Delta miaA$ -GshA\*B, and  $\Delta yggS\Delta ggt\Delta ptsG$ -GshA\*B), the OA contents of the culture media and the cells were separately determined. The intracellular concentrations of OA in  $\Delta yggS\Delta ggt$ -GshA\*B,  $\Delta yggS\Delta ggt\Delta ridA$ -GshA\*B, and  $\Delta yggS\Delta ggt\Delta ridA$ -GshA\*B, and  $\Delta yggS\Delta ggt\Delta ridA$ -GshA\*B, and  $\Delta yggS\Delta ggt\Delta ptsG$ -GshA\*B,  $\Delta yggS\Delta ggt\Delta miaA$ -GshA\*B, and  $\Delta yggS\Delta ggt\Delta ptsG$ -GshA\*B,  $\Delta yggS\Delta ggt\Delta miaA$ -GshA\*B, and  $\Delta yggS\Delta ggt\Delta ptsG$ -GshA\*B were 5.3, 4.8, 3.5, and 5.0 nmol/mg cell, respectively, indicating that the intracellular concentrations of OA did not significantly differ among these strains. The determination of the OA content in the culture medium confirmed that most of the OA was present in the medium (Fig. 6A). Importantly, as shown in Fig. 6B and C, OA was the major amino acid and/or amine in the medium of the  $\Delta yggS\Delta ggt\Delta miaA$ -GshA\*B cells. Similar results were obtained using the other three strains (data not shown). These results indicate that our engineered *E. coli* system is suitable for the production and purification of OA.

**Conclusions.** This study reports a method for the production of OA using engineered *E. coli*, in which *E. coli*  $\Delta yggS$  was used as the starting strain. The deletion of *ggt*, which encodes the enzyme responsible for the degradation of OA, as well as the cooverexpression of the OA synthetic enzymes GshA and GshB and the reduction of the product inhibition ability of GshA by the S495F mutation, all effectively increased the level of production of OA by *E. coli*. Additionally, we propose a new finding that the inactivation of *ridA* may be an effective strategy to attenuate the unwanted catabolism of certain amino acids in *E. coli*. The deletion of *miaA* may also further elevate the production of OA. The strain developed in the present study specifically produced ~80 mg/liter of OA in 24 h with a yield of 28%.

## **MATERIALS AND METHODS**

**Bacterial strains and media.** The bacterial strains used in this study were generated from *Escherichia coli* BW25113 (Table 3). The M9 medium consisted of 0.6% Na<sub>2</sub>HPO<sub>4</sub>, 0.3% KH<sub>2</sub>PO<sub>4</sub>, 0.1% NH<sub>4</sub>Cl, 0.05% NaCl, 0.2% glucose, 1 mM MgSO<sub>4</sub>, 10  $\mu$ M FeSO<sub>4</sub>, 10  $\mu$ M CaCl<sub>2</sub>, and 0.001% thiamine-HCl. The 2.5× M9 medium contained 1.5% Na<sub>2</sub>HPO<sub>4</sub>, 0.75% KH<sub>2</sub>PO<sub>4</sub>, 0.25% NH<sub>4</sub>Cl, 0.125% NaCl, 0.5% glucose, 2.5 mM MgSO<sub>4</sub>, 25  $\mu$ M FeSO<sub>4</sub>, 25  $\mu$ M CaCl<sub>2</sub>, and 0.025% thiamine-HCl. LB medium was 1% tryptone, 0.5% yeast extract, and 1% NaCl. Solid medium was made by adding 1.5% agar. Antibiotics were added as needed at the following concentrations: kanamycin (Kan), 30  $\mu$ g/ml; chloramphenicol (Cam), 30  $\mu$ g/ml; ampicillin (Amp), 100  $\mu$ g/ml. Isopropyl- $\beta$ -D-thiogalactoside (IPTG) was added to the M9 medium at a final concentration of 0.1 mM. L-Glutamic acid, DL-2-aminobutyric acid, and glycine were purchased from Wako or



**FIG 6** OA is specifically accumulated in the medium. (A) Ratio of the OA content in cells and medium. The  $\Delta yggS \Delta ggt$ ,  $\Delta yggS \Delta ggt \Delta ridA$ ,  $\Delta yggS \Delta ggt \Delta miaA$ , or  $\Delta yggS \Delta ggt \Delta ptsG$  strain harboring pGshA\*B was grown for 24 h by cultivation method B with 1 mM each Glu, 2-AB, and Gly, and the OA contents in the cells and the medium were separately determined. The data represent the extracellular levels of OA. (B, C) Elution profiles of amino acids in the medium after cultivation.  $\Delta yggS \Delta ggt \Delta miaA$ -GshA\*B was grown by cultivation method B with 1 mM each Glu, 2-AB, and Gly for 24 h (B) or 48 h (C).

Kanto Chemical and supplemented into the M9 medium at the final concentrations indicated above and below.

**Molecular methods.** Deletion of target genes was performed using the bacteriophage  $\lambda$  Red recombinase system described by Datsenko and Wanner (37). For the construction of the  $\Delta yggS \Delta ggt$  strain, a PCR product was generated with Tks Gflex DNA polymerase (TaKaRa), primers yggS-H1 and yggS-H2 (Table 4), and pKD13 as a template. The purified PCR product (500 ng) was electroporated into the  $\Delta ggt(kan)$  strain, which lacks the Kan resistance gene (*kan*). The  $\Delta ggt(kan)$  mutant was generated from the  $\Delta ggt$  strain using plasmid pCP20 expressing FLP recombinase (38). The resultant colonies that appeared on LB solid medium were picked up, and the gene knockout was confirmed by direct colony PCR with primers yggS-300up and yggS-200dwn. Deletion of the genes *ridA*, *miaA*, and *ptsG* was performed in a similar way using the  $\Delta yggS \Delta ggt(kan)$  mutant as the parental strain. The  $\Delta yggS \Delta ggt(kan)$  strain was generated from the  $\Delta yggS \Delta ggt$  strain using the pCP20 plasmid.

The construction of pGshAB and pGshA\*B was as follows. The *gshB* gene from pCA24N-gshB was amplified by PCR with primers pCA24N-gshB-F and pCA24N-gshB-R. The PCR product was digested with Sall and HindlII, gel purified, and ligated into pCA24N-gshA, which had previously been digested with the same restriction enzymes, forming pGshAB. The constructs were introduced into *E. coli* KRX (Promega), and the sequence of the insert was confirmed by sequence analysis. The *gshA* gene carried by pGshAB was mutated by site-directed mutagenic PCR using the primers gshA-S495F-F and gshA-S495F-R and KOD FX *neo* DNA polymerase (Toyobo), forming pGshA\*B. The pGshAB in the reaction mixture was eliminated by Dpnl treatment. In pGshA\*B, the Ser495 codon (TCT) was altered to Phe (TTT).

**Cultivation methods. (i) Cultivation method A.** *E. coli* cells were precultured in LB medium containing Cam at 30°C with shaking (160 rpm) for 12 to 16 h. Cells were collected by centrifugation (3,500  $\times$  *g*, 5 min) and washed twice with phosphate-buffered saline (PBS; 10 mM Na<sub>2</sub>HPO<sub>4</sub>, 1.8 mM KH<sub>2</sub>PO<sub>4</sub>, 140 mM NaCl, 2.7 mM KCl, pH 7.5). The cell suspension in PBS was seeded into 5 ml M9 medium containing Cam and IPTG at an initial optical density at 600 nm (OD<sub>600</sub>) of 0.01. The cells were grown at 30°C with shaking (160 rpm) using glass test tubes (16.5 mm in diameter by 165 mm in height) for several days. If required, amino acids were added to the culture media at the concentrations indicated above.

# TABLE 3 Strains and plasmids used in this study

Strain or plasmid	Parental strain	Characteristic	Source or reference
Strains			
KRX		[F' traD36 ΔompP proA <sup>+</sup> B <sup>+</sup> lacl <sup>q</sup> Δ(lacZ)M15] ΔompT endA1 recA1 gyrA96 (Nal <sup>i</sup> ), thi-1 hsdR17( $r_{K}^{-}$ m <sub>K</sub> <sup>+</sup> ) e14 (mcrA) relA1 supE44 Δ(lac-proAB) Δ(rha <sub>RAD</sub> )::T7 RNA polymerase	Promega
BW25113		Wild type of E. coli [Δ(araD-araB)567 Δ(rhaD-rhaB)568 ΔlacZ4787 (::rrnB3) hsdR514 rph-1]	Keio Collection
ΔyggS	BW25113	BW25113 Δ <i>yggS::kan</i> (Keio collection JW2918-KC)	Keio Collection
∆ggt	BW25113	BW25113 Δggt::kan (Keio Collection JW3412-KC)	Keio Collection
$\Delta ggt(kan)$	JW3412-KC	BW25113 $\Delta ggt$	This study
ΔyggS Δggt	∆ggt(kan)	BW25113 Δggt ΔyggS::kan	This study
ΔyggS Δggt-GshA	$\Delta yggS \Delta ggt$	ΔyggS Δggt/pCA24N-gshA	This study
Δ <i>yggS Δggt-</i> GshB	ΔyggS Δggt	Δ <i>yggS</i> Δ <i>ggt/</i> pCA24N-gshB	This study
∆ <i>yggS∆ggt</i> -GshAB	ΔyggS Δggt	ΔyggS Δggt/pGshAB	This study
∆yggS∆ggt-GshA*B	ΔyggS Δggt	ΔyggS Δggt/pGshA*B	This study
ΔyggS Δggt(kan)	ΔyggS Δggt	BW25113 ΔyggS Δggt	This study
ΔyggS Δggt ΔptsG	ΔyggS Δggt(kan)	BW25113 ΔyggS Δggt ΔptsG::kan	This study
∆ <i>yggS∆ggt∆ptsG</i> -GshA*B	ΔyggS Δggt ΔptsG	ΔyggS Δggt ΔptsG/pGshA*B	This study
ΔyggS Δggt ΔridA	ΔyggS Δggt(kan)	BW25113 ΔyggS Δggt ΔridA::kan	This study
∆ <i>yggS∆ggt∆ridA-</i> GshA*B	ΔyggS Δggt ΔridA	Δ <i>yggS</i> Δ <i>ggt</i> Δ <i>ridA</i> /pGshA*B	This study
ΔyggS Δggt ΔmiaA	ΔyggS Δggt(kan)	BW25113/ΔyggS Δggt ΔmiaA::kan	This study
∆yggS∆ggt∆miaA-GshA*B	$\Delta yggS \Delta ggt \Delta miaA$	ΔyggS Δggt ΔmiaA/pGshA*B	This study
Plasmids			
pCP20		Expresses FLP recombinase, ori(Ts <sup>a</sup> ) Amp <sup>r</sup> Cam <sup>r</sup>	38
pKD13		Kan <sup>r</sup> gene flanking FLP recombination target sequence, Amp <sup>r</sup>	37
pKD46		Expresses bacteriophage $\lambda$ Red recombinase by arabinose- inducible promoter, <i>ori</i> (Ts) Amp <sup>r</sup>	37
pCA24N-gshA		Expresses His-tagged GshA (ASKA library, JW2663-AM)	40
pCA24N-gshB		Expresses His-tagged GshB (ASKA library, JW2914-AM)	40
pCA24N-foID		Expresses His-tagged FoID (ASKA library, JW0518-AM)	40
pGshAB		Expresses His-tagged GshA and GshB, PT5-lac promoter	This study
, pGshA*B		Expresses His-tagged GshA(S495F) and GshB, PT5-lac promoter	This study

<sup>a</sup>Ts, temperature sensitive.

(ii) Cultivation method B. *E. coli* cells were precultured in LB medium containing Cam at 30°C with shaking (160 rpm) for 12 to 16 h. Cell pellets were washed twice with PBS and resuspended in PBS. The cell suspension in PBS was seeded into 5 ml M9 medium containing Cam and IPTG at an initial OD<sub>600</sub> of 1.0. The cells were cultivated at 30°C with shaking (160 rpm) for 24 h using glass test tubes (16.5 mm in diameter by 165 mm in height). If required, the culture media were supplemented with amino acids at the concentrations indicated above.

# **TABLE 4** Primers used in this study

Primer	Sequence (5'–3')
pCA24N-gshB-F	AGGGTCGACTTTGCTTTGTGAGCGGATAAC
pCA24N-gshB-R	ATTAAGCTTACTGCTGCTGTAAACGTGC
gshA-S495F-F	GAGCGCGAGGCGTTTGAACGCCGTCAGC
gshA-S495F-R	GCTGACGGCGTTCAAACGCCTCGCGCTC
yggS-H1	AGCGCCATCGCAGAAGCCATTGATGCCGGGCAGCGTCAATGTGTAGGCTGGAGCTGCTTC
yggS-H2	TCGTCCGACATTCCCAGAGAGAGCGTGTCGATATGCGGGTATTCCGGGGATCCGTCGACC
ptsG-H1	TATCGCATGTTATGGCAGAAGCAGGCGGTTCCGTCTTTGCAAACAGTGTAGGCTGGAGCTGCTTC
ptsG-H2	GTGATACCGGTCAGGAACGAGGTCAGCGCCGCGGAGATCATAATAATTCCGGGGATCCGTCGACC
miaA-H1	GAGCCTGCCTAAGGCGATTTTTTGATGGGGCCGACGGCCTCCGGATTCCGGGGATCCGTCGACC
miaA-H2	CTTCGCCAACTGTCTCGTGGCGCAAACACCTCGATAAACCATTTCGTGTAGGCTGGAGCTGCTTC
ridA-H1	CTATCGCGACGGAAAATGCACCGGCAGCTATCGGTCCTTACGTACG
ridA-H2	ACGAACAGCGATCGCTTCGATCTCAATCTTCACGTCTTTCGGCAGATTCCGGGGATCCGTCGACC
yggS-300up	GTGCGAAGGTAACAGCCGTAAG
yggS-200dwn	TTGGCCCCATTGCCGGAATAAC
ptsG-300up	AACGAGTAAAGTTCACCGCC
ptsG-200dwn	TCGTTACAGGGGAACGTCAA
miaA-300up	TCCAGTCAGATGCACAGCAT
miaA-200dwn	AGACTCGATTTGCCCTTGCA
ridA-300up	TATCGACAACTATGAAGTGG
ridA-200dwn	CCCGATTCAGATTGTAGACA

Determination of OA and amino acid concentrations. The concentrations of OA and some amino acids were determined by high-performance liquid chromatography (HPLC) as described previously (5, 13), with slight modification. For analysis of the OA content in the cell culture (cells and medium), medium was collected and the same volume of 10% trichloroacetic acid (TCA) was added. Samples were vortexed for 10 min, incubated for 30 min at 4°C, and centrifuged for 20 min at 20,000  $\times$  q. The TCA was removed from the supernatant by extraction three times with water-saturated diethyl ether. Samples were dried with a centrifugal evaporator and resuspended in water. They were diluted with water, and a 10- $\mu$ l portion was mixed with 25  $\mu$ l of the *o*-phthalaldehyde (OPA)–*N*-acetyl-L-cysteine (NAC)–borate reagent (a 1:9 mixture of the NAC-OPA reagent and 0.4 M borate buffer [pH 9.5]). The NAC-OPA reagent contains 10 mg of NAC and 20 mg of OPA in 1 ml methanol. After incubation for 15 min at 4°C, 215  $\mu l$ of distilled water was added. The mixture was centrifuged for 15 min at 20,000  $\times$  g at 4°C, and the supernatant (15  $\mu$ l) was analyzed using a Shimadzu HPLC system. A Mightysil RP-18 GPII column (4.6 [inside diameter {i.d.}] by 250 mm; particle size, 5 µm; Kanto Chemical) and a Mightysil RP-18 GPII guard column (4.6 by 5 mm [i.d.]; particle size, 5  $\mu$ m; Kanto Chemical) preequilibrated with mobile phase A (10 mM Na<sub>2</sub>HPO<sub>4</sub>, 10% methanol, pH 6.5) were used for the analyses. The columns were maintained at 24°C, and the flow rate was 0.8 ml/min. Separation was achieved by increasing the concentration of mobile phase B (10 mM Na<sub>2</sub>HPO<sub>4</sub>, 60% methanol, pH 6.5) in mobile phase A from 0% to 30% over 34 min. Fluorescence was monitored with a Shimadzu RF-20A fluorescence detector (excitation wavelength, 340 nm; emission wavelength, 450 nm). The ophthalmic acid standard was purchased from PH Japan.

**Determination of GshA and GlyA activities.**  $\Delta yggS\Delta ggt$ -GshAB,  $\Delta yggS\Delta ggt$ -GshA\*B,  $\Delta yggS\Delta ggt\Delta ridA$ -GshA\*B, or  $\Delta yggS\Delta ggt\Delta miaA$ -GshA\*B cells were cultivated for 4 h by cultivation method B with 1 mM each Glu, 2-AB, and Gly. The cells were collected by centrifugation (3,500  $\times$  g, 5 min) and washed once with PBS. The cell pellet was stored at  $-80^{\circ}$ C until use.

(i) **GshA activity.** The cell pellet was suspended in a buffer containing 50 mM Tris-HCl, 5 mM MgCl, and 20% glycerol, pH 7.4, and disrupted by sonication. The cell debris was removed by centrifugation (20 min, 20,000  $\times$  g, 4°C), and the supernatants were used for analyses. The Glu–2-AB or Glu-Cys ligase activity was determined at 30°C by a coupling assay with pyruvate kinase and lactic dehydrogenase as described previously (24). The reaction mixture (1 ml) was 100 mM Tris-HCl (pH 8.2), 1 mM each Glu, 1 mM 2-AB, or Cys, 20 mM MgCl<sub>2</sub>, 5 mM ATP, 2 mM phosphoenol pyruvate, 150 mM KCl, 0.3 mM NADH, 9.4 U pyruvate kinase, 10 U lactic dehydrogenase, and the cell extract. When required, the reduced form of GSH was added at a final concentration of 10 mM. Protein concentrations were determined using a Bio-Rad protein assay with bovine serum albumin as the standard.

(ii) GlyA activity. GlyA activity was determined as described by Schirch and Gross (39), with slight modification. The cell pellet was suspended in PBS containing 10% glycerol, sonicated, and centrifuged (20,000  $\times$  g, 4°C) for 30 min. The resultant cell extract (50  $\mu$ l) was added to a reaction mixture (1 ml) containing 50 mM HEPES-NaOH, pH 7.5, 0.2 mM tetrahydrofolate, 0.2 mM NADP<sup>+</sup>, 5 mM L-Ser, 20  $\mu$ M PLP, 0.1% 2-mercaptoethanol and incubated at 37°C for 10 min. After termination of the reaction by adding 100  $\mu$ l of 1 M K<sub>2</sub>CO<sub>3</sub> (pH 9.5), purified FoID (2 mg/ml, 10  $\mu$ l) was added to the reaction mixture, and the change in the absorbance at 340 nm was determined. FoID was purified from the *E. coli* cells harboring pCA24N-foID by Ni-affinity chromatography and stored in a buffer consisting of 12.5 mM Tris-HCl, pH 7.5, 75 mM KCl, 12.5 mM 2-mercaptoethanol, and 50% glycerol at  $-80^{\circ}$ C until it was used.

**Determination of ATP levels.**  $\Delta yggS \Delta ggt$ -GshA\*B,  $\Delta yggS \Delta ggt \Delta ridA$ -GshA\*B,  $\Delta yggS \Delta ggt \Delta ridA$ -GshA\*B, and  $\Delta yggS \Delta ggt \Delta ptsG$ -GshA\*B cells were cultivated for 4 h by cultivation method B with 1 mM each Glu, 2-AB, and Gly. Twelve microliters of the culture medium (cells and medium) was withdrawn, and ATP levels were measured by use of a Lucifer 250 kit (Kikkoman Co., Japan) according to the manufacturer's protocol.

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