

Operando Insights into CO Oxidation on Cobalt Oxide Catalysts by NAP-XPS, FTIR, and XRD

Liliana Lukashuk,^{†,‡} Nevzat Yigit,[†] Raffael Rameshan,[‡] Elisabeth Kolar,[†] Detre Teschner,^{§,||} Michael Hävecker,^{§,||} Axel Knop-Gericke,[§] Robert Schlögl,^{§,||} Karin Föttinger,^{*,†,||} and Günther Rupprechter^{*,†,||}

[†]Institute of Materials Chemistry, Technische Universität Wien, Getreidemarkt 9/BC/01, Vienna 1060, Austria

[‡]Institute of Physical Chemistry, University of Innsbruck, Innrain 80/82, Innsbruck A-6020, Austria

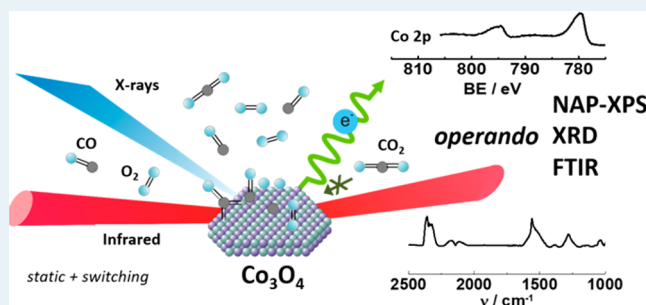
[§]Department of Inorganic Chemistry, Fritz-Haber-Institut der Max-Planck-Gesellschaft, Faradayweg 4-6, Berlin 14195, Germany

^{||}Department of Heterogeneous Reactions, Max Planck Institute for Chemical Energy Conversion, Stiftstraße 34-36, Mülheim an der Ruhr 45470, Germany

Supporting Information

ABSTRACT: Cobalt oxide Co_3O_4 has recently emerged as promising, noble metal-free catalyst for oxidation reactions but a better understanding of the active catalyst under working conditions is required for further development and potential commercialization. An operando approach has been applied, combining near ambient (atmospheric) pressure X-ray photoelectron spectroscopy (NAP-XPS), Fourier transform infrared spectroscopy (FTIR), or X-ray diffraction (XRD) with simultaneous catalytic tests of CO oxidation on Co_3O_4 , enabling one to monitor surface and bulk states under various reaction conditions (steady-state and dynamic conditions switching between CO and O_2). On the basis of the surface-specific chemical information a complex network of different reaction pathways unfolded: Mars-van-Krevelen (MvK), CO dissociation followed by carbon oxidation, and formation of carbonates. A possible Langmuir–Hinshelwood (LH) pathway cannot be excluded because of the good activity when no oxygen vacancies were detected. The combined NAP-XPS/FTIR results are in line with a MvK mechanism above 100 °C, involving the $\text{Co}^{3+}/\text{Co}^{2+}$ redox couple and oxygen vacancy formation. Under steady state, the Co_3O_4 surface appeared oxidized and the amount of reduced Co^{2+} species at/near the surface remained low up to 200 °C. Only in pure CO, about 15% of surface reduction were detected, suggesting that the active sites are a minority species. The operando spectroscopic studies also revealed additional reaction pathways: CO dissociation followed by carbon reoxidation and carbonate formation and its decomposition. However, due to their thermal stability in various atmospheres, the carbonates are rather spectators and also CO dissociation seems a minor route. This study thus highlights the benefits of combining operando surface sensitive techniques to gain insight into catalytically active surfaces.

KEYWORDS: CO oxidation, Co_3O_4 , operando, NAP-XPS, FTIR, XRD, surface spectroscopy



1. INTRODUCTION

Controlling automotive emissions during an engine's cold start is an unresolved issue, resulting from the strong CO adsorption on noble metals, poisoning the catalyst at low temperature (<200 °C).^{1,2} Due to their low-temperature CO oxidation ability, transition metal oxides,³ especially cobalt oxide, are promising.^{4,5} Despite intensive studies, the nature of the active sites of cobalt oxide catalysts as well as exact reaction mechanisms are still debated and contradicting results concerning the role of $\text{Co}^{3+}/\text{Co}^{2+}$, of different oxygen species, oxygen vacancies, and carbonates were reported.

The active sites are often attributed to the abundance of specific cobalt cations. In 2009, Xie et al. reported that Co_3O_4 nanorods, predominately exposing (110) planes and enriched in Co^{3+} cations, exhibit very high activity for low-temperature

CO oxidation. The high catalytic activity was ascribed to Co^{3+} cations,⁵ but no spectroscopic evidence was given. Two years later the same group reported that Co_3O_4 nanosheets with (111) planes, enriched in Co^{2+} cations, were the most active among nanorods, nanocubes, and nanoparticles,⁶ contrasting with the previous report. Jia et al. observed that a Co_3O_4 – SiO_2 nanocomposite catalyst, without ordered planes, but enriched in Co^{2+} , exhibited very high activity at low temperature.⁴ Recently, it was reported that CoO with octahedrally coordinated Co^{2+} had unexpectedly high activity due to the ease of surface oxidation of Co^{2+} to Co^{3+} .⁷ Nevertheless, all

Received: March 29, 2018

Revised: August 2, 2018

Published: August 7, 2018

conclusions were primarily based on catalytic studies and no direct spectroscopic evidence of the active surface oxidation state was provided.

A recent study by Iablokov et al. using different particle sizes (2 to 10 nm) showed a maximum rate between 5 and 8 nm. This was explained by a higher concentration of Co^{3+} 3d states, as revealed by XPS.⁸ Ding et al. reported an enhanced activity of flower-like Co_3O_4 with an increased number of surface Co^{3+} .⁹ All findings illustrate that there are still open questions concerning the nature of active sites, i.e., the abundance of $\text{Co}^{3+}/\text{Co}^{2+}$ and $\text{Co}_3\text{O}_4/\text{CoO}$.

With respect to the reaction mechanism, it was suggested that CO adsorbs to Co^{3+} cations, followed by abstracting surface lattice oxygen coordinated to three Co^{3+} cations, with the oxygen vacancy later replenished by gas phase oxygen (Mars-van-Krevelen mechanism).⁵ Studying the effect of pretreatment conditions, Yu et al. proposed a reaction between a molecularly adsorbed CO and molecularly adsorbed O–O peroxy species, but without spectroscopic evidence.¹⁰ However, Jia et al. did not detect peroxy O–O species by in situ Raman spectroscopy.⁴ In an in situ IR study, Pollard et al.¹¹ suggested that CO adsorbed on Co^{2+} sites reacted with an oxygen atom bonded to a neighboring Co^{3+} cation, and the oxygen vacancy was replenished by oxygen from the gas phase. In his early work on the CO oxidation mechanism, Jansson et al. had already proven lattice oxygen extraction using isotopes, i.e., the redox Mars-van-Krevelen mechanism.^{12–14} He also found that CO disproportionation takes place during CO oxidation. Mechanistic insights were also gained from reaction orders. The study of Perti et al. on CO oxidation kinetics on $\text{Co}_3\text{O}_4\text{--Al}_2\text{O}_3$ revealed reaction orders of CO and O_2 being 0 and 0.42, respectively^{15–17} and their study suggested two competitive mechanisms: reaction of CO with adsorbed oxygen (Langmuir–Hinshelwood LH) and with lattice oxygen (MvK).^{15–17}

The CO oxidation mechanism on cobalt oxide has also been examined by theoretical work,^{18–21} also showing divergences. For example, Jiang et al. suggested a MvK mechanism for Co_3O_4 (110).²¹ Pang et al. proposed two scenarios: direct reaction of CO with surface lattice oxygen atoms (MvK) but also direct reaction of preadsorbed molecular O_2 with molecular CO from the gas phase.^{20,22}

A better understanding of CO oxidation on cobalt oxide would clearly benefit from an evaluation of the surface oxidation state of the active catalyst, as well as of the surface species present. Applying operando (in situ) techniques for studying the catalyst surface under reaction conditions may enable to reveal the reaction network, which is required for setting up a mikrokinetic model that could eventually explain the macroscopic kinetics.^{23–25} The importance of surface composition changes of a cobalt oxide model catalyst during methanol oxidation was, e.g., revealed by operando near atmospheric pressure X-ray photoelectron spectroscopy (NAP-XPS).²⁶ The goal of the current study was to improve the understanding of the reaction pathways occurring during CO oxidation on Co_3O_4 . Thus, NAP-XPS and Fourier transform infrared (FTIR) spectroscopy monitoring the surface changes and surface species were applied with simultaneous catalytic activity tests by gas chromatography (GC) or mass spectroscopy (MS). Experiments were performed under steady-state conditions ($\text{CO} + \text{O}_2$), in CO atmosphere, and upon switching between CO and O_2 . In addition, the effect of pretreatment conditions on catalyst structure and activity was examined by

operando XRD/MS. Altogether, the operando studies provided new insight into the active catalyst surface, several possible reaction pathways, and the presence and stability of surface species.

2. EXPERIMENTAL SECTION

2.1. Catalyst. Co_3O_4 was used as received from Fluka (purity 99.5%). The average crystallite size of Co_3O_4 determined by X-ray diffraction was 28 nm, the BET specific surface area was $38 \text{ m}^2\text{g}^{-1}$. According to TEM measurements, the material was composed of nanospheres of 20 to 50 nm in size. A detailed catalyst characterization was reported previously.²⁷

2.2. Catalytic CO Oxidation. CO oxidation was performed in a continuous-flow fixed-bed quartz reactor under atmospheric pressure. The sample (ca. 20 mg, mixed with 100 mg quartz powder to avoid mass and heat transfer limitations) was loaded into the reactor and pretreated with synthetic air at 400 °C for 30 min (50 mL min^{-1} , heating rate of $10 \text{ }^\circ\text{C min}^{-1}$, standard pretreatment procedure). For studying the effect of pretreatment conditions, oxidation at 400 °C in synthetic air was followed by reduction at 100 °C, 200 °C, 300 °C, or 400 °C in 5 vol % H_2 in N_2 . After cooling to 30 °C, temperature-dependent CO oxidation was performed either with 5 vol % CO and 10 vol % O_2 in He or 5 vol % CO and 2.5 vol % O_2 in He. The total flow rate was 50 mL min^{-1} , and the heating rate was $2 \text{ }^\circ\text{C min}^{-1}$. The catalysts rapidly deactivate at room temperature (RT), why rather higher reaction temperatures were examined. The concentrations of CO and CO_2 in the outlet stream were monitored by gas chromatography (GC) using a HP-PLOT Q column and a flame-ionization detector (FID) with a methanizer.

2.3. Operando XRD Measurements. Operando XRD experiments were performed on a laboratory diffractometer (XPert III: PANalytical XPert Pro MPD) using $\text{Cu}\text{--}\text{K}\alpha$ radiation (1.54 \AA) operating in the Bragg–Brentano reflection geometry. The diffractometer is equipped with an Anton Paar XRK 900 high-temperature gas cell. In situ diffraction patterns were recorded in the scanning range from 25° to 70° (2θ) using a step scan mode with steps of 0.05° (2θ) and a time per step of 2 s. XRD data were analyzed with the HighScore Plus program.

The inlet of the Anton Paar XRK 900 high-temperature gas cell is connected to a gas manifold system with calibrated mass flow controllers; the outlet of the cell is connected to a quadrupole mass spectrometer (QMS) (PrismaPlus QMG 220, Pfeiffer Vacuum, SEM detector). The Co_3O_4 (ca. 20 mg) was placed into a sample holder, inserted into the cell and pretreated in synthetic air at 400 °C (30 min). Afterward, the reaction mixture of 5 vol % CO, 10 vol % O_2 , and 85 vol % He was introduced and XRD patterns were recorded at room temperature (RT), 100 °C, 150 °C, 200 °C, and 250 °C. The same experiment was done after pretreatment in synthetic air at 400 °C followed by reduction in 5 vol % H_2 in He at 400 °C (30 min). For in situ H_2 -temperature-programmed reduction, the samples were pretreated in synthetic air at 400 °C (30 min), then cooled to RT, purged with He, and then 5 vol % H_2 in He was introduced. XRD patterns were recorded at RT, 100 °C, 200 °C, 300 °C, and 400 °C. All experiments were performed at atmospheric pressure with a total flow of 50 mL min^{-1} .

2.4. Operando NAP-XPS Measurements. Operando near ambient (atmospheric) pressure X-ray photoelectron

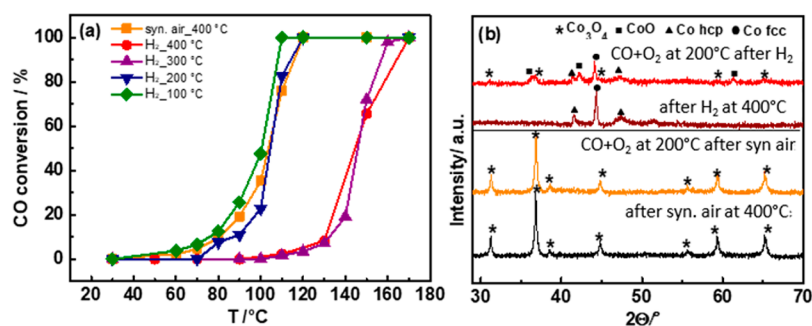


Figure 1. (a) Temperature-dependence of the CO oxidation activity for a reaction mixture of 5 vol % CO, 10 vol % O₂, and 85 vol % He (total flow 50 mL min⁻¹) for differently pretreated Co₃O₄; (b) operando XRD during CO oxidation at 200 °C after oxidation pretreatment of Co₃O₄ at 400 °C in synthetic air and after reduction of preoxidized Co₃O₄ in 5 vol % H₂ at 400 °C. The XRD patterns before starting the reaction are included for comparison.

spectroscopy (NAP-XPS) was performed at the ISSS beamline at the synchrotron radiation facility BESSY II of the Helmholtz-Zentrum Berlin, Germany. The setup consisted of a reaction cell attached to a set of differentially pumped electrostatic lenses and a separately pumped analyzer (Phoibos 150 Plus, SPECS GmbH), as described elsewhere.²⁸ Typically, the powder sample (ca. 30 mg) was pressed into a tantalum grid (to minimize potential charging effects) together with a K-type thermocouple, fixed to a sapphire sample holder and mounted inside the XPS reaction cell in front of the first aperture of the differentially pumped electrostatic lens system. The heating of the samples was done from the back using an infrared laser. Before the catalytic experiments, the sample was pretreated in the XPS reaction cell by oxidation (0.5 mbar O₂ at 400 °C) until all residual surface carbon and carbonates disappeared. After cooling the sample to RT, the CO + O₂ reaction mixture (1:2 ratio at 0.5 mbar) was introduced with the partial pressure of the gases controlled by calibrated mass flow controllers, and the photoemission spectra were recorded. Then, the sample was heated to 100 °C, 150 °C, and 200 °C with a heating rate of 5 °C min⁻¹, and photoemission spectra were again acquired at these temperatures. For CO vs O₂ switching experiments, CO (0.15 mbar) was introduced at RT and photoemission spectra were recorded for ~30 min, then the atmosphere was changed to O₂ (0.15 mbar), again collecting spectra for ~30 min. Then, Co₃O₄ was heated in O₂ to the next temperature and the procedure was repeated. Such experiments were performed at RT, 100, 150, and 200 °C. To ensure surface sensitivity, the Co 2p and C 1s core-level regions were recorded using selected photon energies that resulted in photoelectrons with 200 eV kinetic energy and a ~0.6 nm inelastic mean free path. The gas phase composition was monitored online by an electron impact quadrupole mass spectrometer, which was connected to the XPS cell via a gas dosing valve.

XPS spectra were analyzed using the CasaXPS package. All binding energies (BE) were calibrated using the second-order O 1s peak. The accuracy of the BE calibration was estimated to be around 0.05 eV. A Shirley-type function was used to remove the background arising from energy loss for Co 2p, and either a Shirley- or a linear-type function was used in the case of C 1s. The extracted spectra were then fitted with a combined Gaussian and Lorentzian line profile. The peak positions of Co 2p and C 1s, full width at half-maximum (fwhm), and constraints are presented in Tables S1 and S2 (Supporting Information, SI).

2.5. Operando FTIR Measurements. Operando FTIR studies were carried out in transmission mode using a Bruker Vertex 70 spectrometer (liquid N₂-cooled MCT detector, resolution of 4 cm⁻¹) in a stainless steel transmission flow cell equipped with CaF₂ windows. The inlet of the cell was connected to a gas manifold system with calibrated mass flow controllers. The sample (ca. 4–5 mg) was pressed into a pellet, which consisted of a thin catalyst layer supported on a KBr pellet, and placed in a small cylindrical stainless steel sample holder equipped with a ring-shaped furnace and a type-K thermocouple. All infrared spectra were collected in the 4000–900 cm⁻¹ range by averaging 256 scans to achieve good signal-to-noise ratio. A spectrum of the empty sample holder recorded in He was used for background subtraction for all spectra, which were evaluated with the OPUS 4.0 software. During operando FTIR measurements catalytic CO oxidation was *simultaneously* monitored by gas chromatography (Figure S5).

Before each experiment, the catalyst was pretreated in synthetic air (50 mL min⁻¹) at 400 °C for 30 min (heating rate 10 °C min⁻¹), cooled to 30 °C under a flow of synthetic air, and purged with He for 10 min.

CO Oxidation. the reaction mixtures, (i) 5 vol % CO, 10 vol % O₂ in He; (ii) 5 vol % CO, 5 vol % O₂ in He; or (iii) 5 vol % CO, 2.5 vol % O₂ in He were passed through the cell at 25 mL min⁻¹, and temperature-dependent spectra were recorded while heating to 250 °C with a heating rate of 2 °C min⁻¹.

CO-Temperature-Programmed Reduction Followed by Heating in O₂ or He. Five vol % CO in He (25 mL min⁻¹) was continuously introduced to the cell and temperature-dependent spectra were recorded while heating to 250 °C. Then, the sample was cooled to room temperature and temperature-dependent spectra were recorded during heating to 200 °C in 5 vol % O₂ in He or in pure He.

CO vs O₂ Switching Experiments. CO (5 vol % CO in He) was introduced and five IR spectra were consecutively recorded within 10 min, then the atmosphere was changed to O₂ (5 vol % O₂ in He) again collecting five IR spectra within 10 min. Then, Co₃O₄ was heated in O₂ to the next temperature and the procedure was repeated. Such experiments were performed at RT, 100 °C, 150 °C, 200 °C, and 250 °C.

CO₂ Adsorption. Five vol % CO₂ in He (25 mL min⁻¹) was continuously passed through the cell and temperature-dependent spectra were recorded while heating to 200 °C.

Table 1. CO Conversion for a Reaction Mixture of 5 vol.% CO, 10 vol.% O₂, and 85 vol.% He (total flow 50 mL min⁻¹, 20 mg Catalyst) for Co₃O₄ Pretreated in Synthetic Air (400 °C) or in Synthetic Air (400 °C) Followed by Hydrogen at the Indicated Temperatures

pretreatment	$T_{10\%}$ (°C) ^a	$T_{50\%}$ (°C) ^b	$T_{90\%}$ (°C) ^c	$r_{90\text{ °C}}$ (mol/s·g) ^d	TOF _{90 °C} (s ⁻¹) ^e
Syn_air_400 °C	79	104	115	1.64×10^{-5}	$1.9\text{--}3.8 \times 10^{-2}$
+H ₂ _100 °C	76	101	108	2.18×10^{-5}	$2.6\text{--}5.2 \times 10^{-2}$
+H ₂ _200 °C	88	105	114	9.37×10^{-6}	$1.1\text{--}2.2 \times 10^{-2}$
+H ₂ _300 °C	132	146	157	n.a.	n.a.
+H ₂ _400 °C	130	145	164	n.a.	n.a.

^aReaction temperature for 10% CO conversion. ^bReaction temperature for 50% CO conversion; ^cReaction temperature for 90% CO conversion. ^dReaction rate of CO oxidation at 90 °C per gram of a catalyst. ^eTurnover frequency of the Co³⁺ sites at 90 °C. This estimation is based on the procedure suggested by Xie et al. for nanoparticles of similar mean size and shape, assuming 5–10% of Co³⁺ in surface defects as active sites.⁵

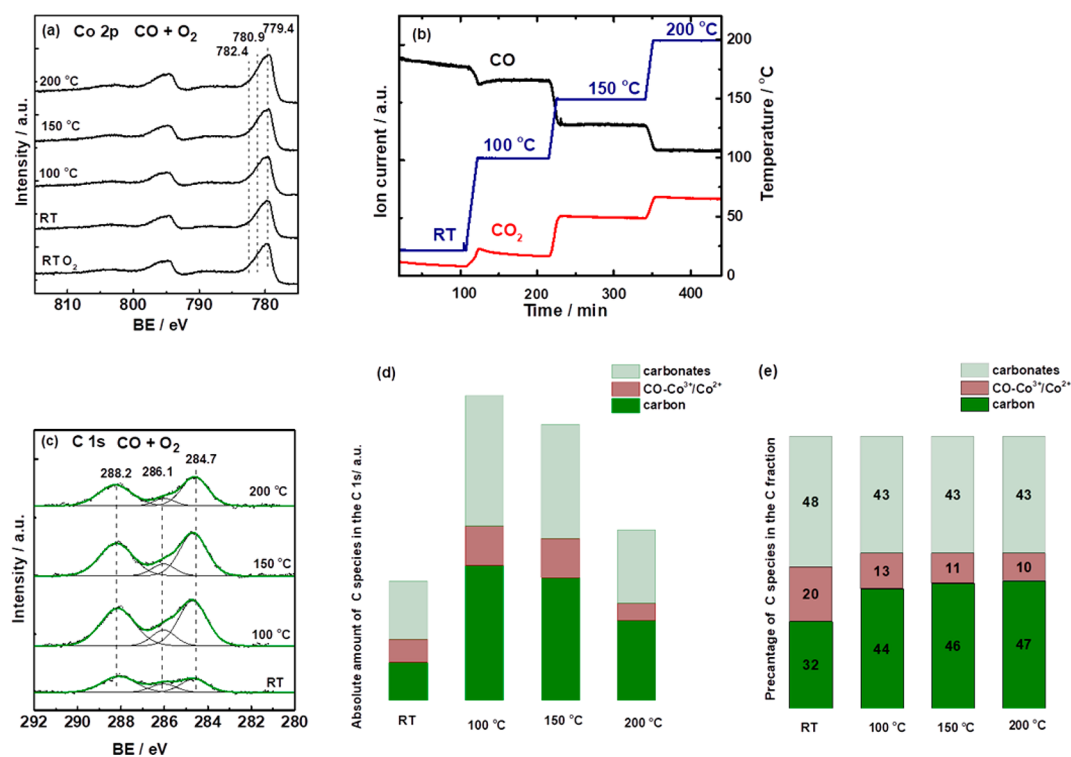


Figure 2. Operando NAP-XPS during CO oxidation on Co₃O₄ from RT to 200 °C (0.15 mbar CO and 0.3 mbar O₂): (a) the Co 2p region ($h\nu = 1015$ eV, KE = 200 eV); (b) MS catalytic data recorded during NAP-XPS; (c) the C 1s region ($h\nu = 465$ eV, KE = 200 eV); (d) the absolute amount of carbon species; and (e) the relative ratio between carbon species, both calculated from a linear peak fit.

3. RESULTS

3.1. Operando XRD under Steady State Conditions: Influence of Pretreatment on CO Oxidation Activity.

The CO oxidation activity strongly depended on the CO/O₂ ratio (Figure S1; as reported previously), why a 1:2 ratio was used for most experiments. To examine the influence of the (bulk) cobalt oxidation state, the Co₃O₄ catalyst was pretreated in different ways: by oxidation in synthetic air at 400 °C; or by oxidation at 400 °C followed by reduction in 5 vol % H₂ in N₂ at 100 °C, 200 °C, 300 °C, and 400 °C. After pretreatment, CO oxidation was carried out in 5 vol % CO and 10 vol % O₂ in He. The temperature-dependent CO conversion for differently pretreated Co₃O₄ is presented in Figure 1a and summarized in Table 1. Co₃O₄ pretreated in synthetic air or in synthetic air/H₂ (100 °C or 200 °C) was active already at ~80 °C, reaching 100% CO conversion at ~110–120 °C (apparent activation energy around 70 kJ/mol). In contrast, for preoxidized Co₃O₄ reduced in H₂ at 300 °C or 400 °C, CO conversion started at higher temperature (~120

°C) and reached 100% at 160 °C and 170 °C, respectively. This is accompanied by an increase in apparent activation energy to around 110 kJ/mol, suggesting a different rate-determining step and different active sites (Figure S2).

Operando XRD upon CO oxidation on Co₃O₄ pretreated in synthetic air and in synthetic air followed by 5 vol % H₂ at 400 °C are shown in Figure 1b for 200 °C, with more details in Figure S2. After standard preoxidation, Co₃O₄ remained Co₃O₄ at all reaction temperatures (Figure S2a), in agreement with the in situ XRD study of Jansson et al.¹⁴ Although the bulk structure of Co₃O₄ does not undergo structural changes during CO oxidation, the topmost surface layers could still be affected, as discussed below.

The low catalytic activity after reduction at 300 °C or 400 °C is due to the reduction of Co₃O₄ to metallic cobalt, as revealed by in situ XRD (Figures 1b and S3) and in situ XAS at the Co K edge reported in our previous study.²⁷ Upon heating in the 1:2 CO/O₂ mixture the metallic cobalt is gradually reoxidized and CO conversion increases at 150–200 °C. This

is evident from operando XRD (Figure 1b) indicating metallic cobalt, CoO and Co₃O₄ at 200 °C. At 250 °C the oxidation was still incomplete (Figure S2b). As mentioned, XRD is a bulk characterization technique, and the surface composition of the catalyst might be different, calling for surface sensitive techniques, such as X-ray photoelectron spectroscopy and infrared spectroscopy.

3.2. Operando Spectroscopy under Steady State Conditions.

3.2.1. Operando NAP-XPS. To gain spectroscopic insight into CO oxidation, we have utilized operando NAP-XPS, which provides surface-specific information on the cobalt oxidation state and formation of oxygen vacancies (by probing the Co 2p region), as well as on adsorbate species (by probing the C 1s region). Within our previous study of preferential CO oxidation (PROX),²⁷ CO-temperature-programmed reduction (CO-TPR) NAP-XPS indicated that CO reduced the top surface layers of Co₃O₄, forming CoO, Co, and oxygen vacancies, whereas elementary carbon, carbonates, and CO-Co³⁺/CO-Co²⁺ were observed in the C 1s region. Similarly, herein operando NAP-XPS (KE = 200 eV, probing depth ~0.6 nm) was carried out during CO oxidation (0.15 mbar CO and 0.3 mbar O₂), as a function of reaction temperature (Figure 2). The assignment of Co 2p peaks was based on literature:²⁹ the peak at 779.4 eV corresponds to Co³⁺, the peak at 780.9 eV to Co²⁺ in CoO, and that at 782.4 eV to Co²⁺ in Co(OH)₂.

At first, Co 2p XPS did not indicate any surface reduction of Co₃O₄ in CO+O₂, neither at RT nor at higher temperature (i.e., there were no shakeup satellites)^{29,30} (Figure 2a). To better reveal changes, all spectra were normalized, plotted together (Figure S4a) and a difference spectrum of spectra at 200 °C and RT was calculated (Figure S4b), which point to minor surface reduction at the detection level at 200 °C. Note that (pure) CO induced surface reduction and formation of oxygen vacancies particularly above 100 °C.²⁷ Thus, during CO oxidation (i.e., in the presence of an excess of O₂) only minute surface reduction occurred. This indicates a rapid dynamic reduction/reoxidation of the cobalt oxide surface in the CO+O₂ mixture under steady state. Catalytic data recorded in parallel to NAP-XPS (Figure 2b) agreed with those from the fixed-bed flow reactor.

The C 1s region revealed three peaks during CO oxidation (Figure 2c), characterizing carbonates (288.2 eV),^{31–33} elementary carbon (284.7 eV),³⁴ and CO adsorbed to cobalt (i.e., CO-Co³⁺/CO-Co²⁺) (286.1 eV).³⁵ The peak positions and fwhm are listed in Table S1. The absolute amount of elementary carbon, carbonates, and weakly adsorbed CO increased from RT to 100 °C, but decreased upon further heating (Figure 2d). The relative amount of C was 32% at RT and 44–47% at 100–200 °C (Figure 2e), assuming identical sensitivity for all species.

In contrast, during CO-TPR (O₂ absent) the intensity of carbon species increased with temperature.²⁷ The ratio of elementary carbon to carbonates and adsorbed CO was larger: the fraction of C was 52% at RT and 78% at 200 °C.²⁷ Also, increasing temperature in CO led to Co₃O₄ reduction to CoO_x and formation of oxygen vacancies. Since the C concentration was much higher in pure CO, the oxygen vacancies are likely the reaction sites of CO dissociation (cooperating with neighboring Co cations). In the presence of oxygen, vacancies are refilled and less carbon is produced. Thus, O₂ of the reaction mixture may hinder the growth of C by keeping the

surface oxidized and thus preventing CO dissociation, or O₂ just reoxidizes C deposited by CO dissociation.

3.2.2. Operando FTIR Spectroscopy. Operando FTIR spectroscopy enables studying adsorbed species, thus contributing in identifying reaction pathways. A number of IR studies have reported carbonates,^{4,13,14,32} but their exact role, whether being reaction intermediates, spectators, or poisons remained unclear. Carbonates have also frequently been observed for CO-containing reactions on oxide supported metals.^{36,37} Systematic operando FTIR studies were performed to unravel their role, applying three feed compositions (Figure 3): CO/O₂ = 1:2; 1:1; 2:1.

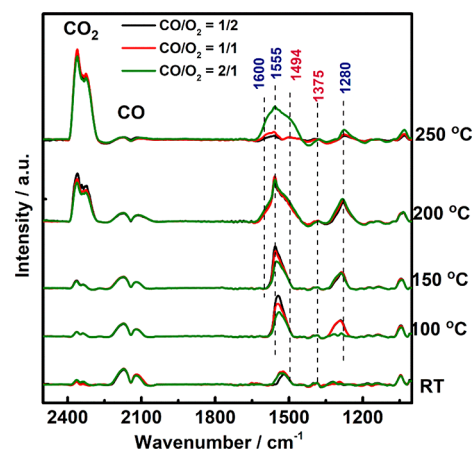


Figure 3. Operando FTIR spectra recorded during CO oxidation on Co₃O₄ in flow mode (25 mL min⁻¹) from RT to 250 °C in different gas mixtures: 50 mbar CO, 100 mbar O₂ (black); 50 mbar CO, 50 mbar O₂ (red); and 50 mbar CO, 25 mbar O₂ (green).

All operando FTIR spectra exhibited the characteristic gas-phase bands of CO (2110 and 2170 cm⁻¹) as well as bands in the 1000–1650 cm⁻¹ region, attributed to various carbonate vibrations. In contrast to NAP-XPS, operando FTIR did not show any bands of (linearly adsorbed) CO on Co²⁺ or Co³⁺. The CO stretching frequencies of cobalt carbonyls were reported at 2023–2025 cm⁻¹ for metallic cobalt, 2070–2110 cm⁻¹ for Co⁺, 2120–2170 cm⁻¹ for Co²⁺, and 2178–2180 cm⁻¹ for Co³⁺.¹⁴ Thus, the 2178–2180 cm⁻¹ on Co³⁺ band could be masked by gas-phase CO.

In the FTIR cell, carbonate formation started at RT whereas CO₂ production began around 150 °C, increasing with temperature. The assignment of surface carbonates is based on literature^{38,39} and IR stretching vibrations are presented in Table S3. The carbonates at RT were mainly monodentates (1494, 1375, 1320 cm⁻¹). Upon temperature increase, bidentates evolved (additional bands at 1620, 1555, and 1280 cm⁻¹). It is important to note that all FTIR spectra were recorded on the same pellet of Co₃O₄, allowing to quantitatively compare intensities and the amount of adsorbed species.

FTIR spectra of the three gas mixtures mainly differed in the stability of the carbonates. Under O₂-rich conditions (CO/O₂ = 1 to 2) the signal intensity increased from RT to 170 °C, between 170 °C and 200 °C additional bidentate carbonates were formed, but at 220 °C carbonates started to disappear and no carbonates were present above 220 °C (Figure 3). The appearance of bidentate carbonates was accompanied by an increase in CO conversion (CO₂ gas-phase peak; Figure 3).

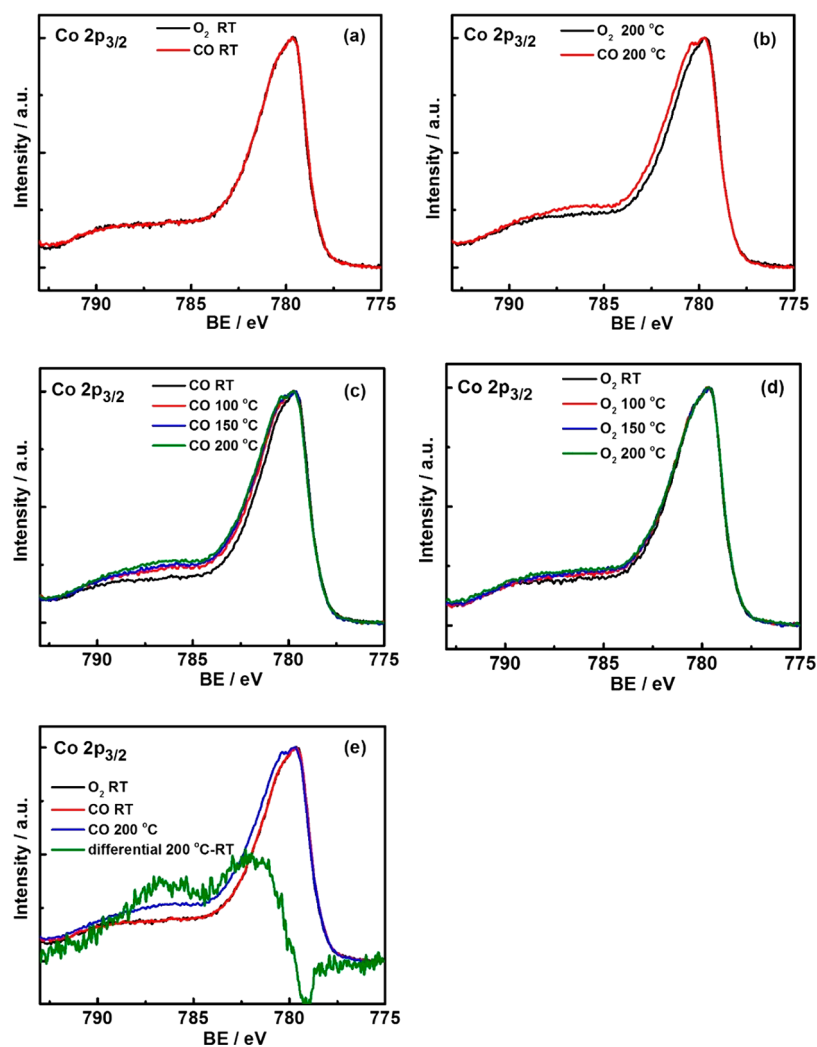


Figure 4. Operando NAP-XPS on Co_3O_4 during CO/ O_2 switching (0.15 mbar CO vs 0.15 mbar O_2), Co $2p_{3/2}$ region ($h\nu = 1015$ eV; KE = 200 eV): comparison in CO and O_2 at (a) RT and (b) 200 °C; the Co $2p_{3/2}$ region at various temperatures in (c) CO and (d) O_2 ; (e) difference spectrum (Co $2p_{3/2}$ 200 °C in CO-Co $2p_{3/2}$ RT in O_2).

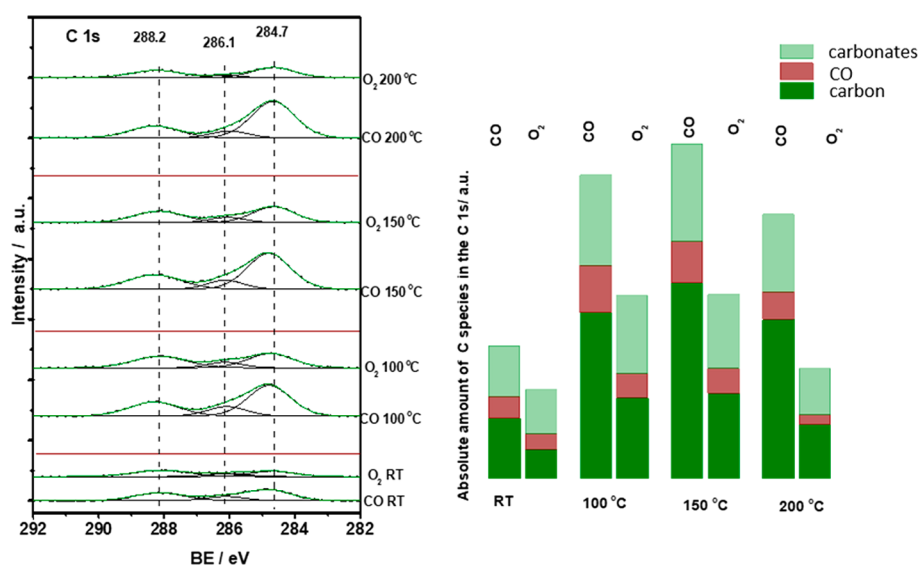


Figure 5. Operando NAP-XPS C 1s region ($h\nu = 465$ eV; KE = 200 eV) on Co_3O_4 during CO/ O_2 switching (0.15 mbar CO vs 0.15 mbar O_2). The absolute amount of carbon species was calculated from a linear peak fit.

The disappearance of carbonate peaks was accompanied by a further increase of the CO₂ gas-phase peak and an overall increase of CO conversion. The decreasing carbonate intensity above 220 °C is likely due to lower stability of carbonates in O₂ excess.

In the reaction mixture with an initial CO/O₂ ratio of 1:1, a relatively high amount of carbonates was still present at 220 °C and higher temperatures were required to make them disappear. When the CO to O₂ ratio was stoichiometric (CO/O₂ = 2:1), the amount of carbonates was even higher and the concentration of carbonates increased continuously up to 250 °C.

In summary, the more reducing (CO rich) the reaction atmosphere was, the higher the amount and stability of surface carbonates became. This suggests that upon temperature increase more sites were formed (likely by reduction of the Co₃O₄ surface), that were active for CO adsorption and carbonate formation. Whether excess O₂ reduces the amount of carbonates formed or just facilitates carbonate decomposition/desorption to CO₂ cannot be answered at this point. On the basis of static IR experiments, the potential contribution of carbonates to the overall activity cannot be assessed. Thus, gas switching experiments were performed both for NAP-XPS and FTIR.

3.3. Operando Spectroscopy upon Switching between CO and O₂. **3.3.1. NAP-XPS.** To lift the limitations of steady state spectroscopy, switching experiments were monitored by NAP-XPS (Figures 4, 5, S6, S7, and S8). CO/O₂ switching (each 0.15 mbar for ~50 min) was carried out at RT, 100 °C, 150 °C, and 200 °C, simultaneously recording Co 2p and C 1s spectra (KE = 200 eV; Figures 4, 5, and S7) and MS of reactants and CO₂ (Figure S6). Taking into account the attenuation of photoelectrons in the gas phase, a CO/O₂ ratio of 1 was used (0.15 mbar CO vs 0.15 mbar O₂; similar scattering was confirmed by comparing Co 2p peak intensities).

Figure S6b demonstrates that changing the atmosphere from O₂ to CO produced CO₂ already at RT, but increased with temperature. Note that before introducing the reacting gas (e.g., CO) into the NAP-XPS chamber, the other reacting gas (e.g., O₂) was evacuated from the chamber, in order to keep the Co₃O₄ catalyst free from physisorbed molecules.

A significant increase in CO₂ evolution at 200 °C and continuous CO₂ production for ~30 min upon switching to CO indicates that not only surface lattice oxygen may take part in CO₂ production, but also oxygen from the bulk. The shape of the MS curve, a sharp peak followed by a slow decrease, points to fast reaction with surface oxygen (decaying fast upon consumption) and a slower reaction with bulk oxygen, which needs to diffuse to the surface. If only surface oxygen would react, then CO₂ production should have dropped quickly. A gradual (slow) decrease in CO₂ evolution is observed at 200 °C, which may be caused by catalyst deactivation by carbon (C 1s region, Figure 5) or by slow diffusion of oxygen from deeper (bulk) layers.

CO disproportionation to C and CO₂ may also contribute to the slower pathway. The amount of CO₂ produced at 200 °C during steady state CO oxidation (0.15 mbar CO and 0.3 mbar O₂; Figure 2b) was 1.34×10^{-10} a.u. The amount of CO₂ produced at 200 °C in the presence of pure CO (0.15 mbar CO; Figure S6b) was 6.10×10^{-12} a.u. (after ~5 min) and 3.61×10^{-12} a.u. (after ~30 min) that is 22–37 times lower than the catalytic activity in CO + O₂.

In the opposite case, when O₂ was introduced after CO, there was only minor CO₂ production, likely due to surface carbonate decomposition (and then O₂ reoxidized the surface). The MS data were confirmed by analogous experiments in the catalytic flow reactor.

Figures 4 and 5 display the corresponding Co 2p_{3/2} and C 1s spectra. Upon switching to CO, the Co₃O₄ surface oxidation state did not change at RT (no satellites appeared in Co 2p), whereas more pronounced changes of Co³⁺/Co²⁺ were observed at higher temperature, especially at 200 °C (Figures 4a,b, and S7). In CO at 200 °C, the Co³⁺ concentration decreased by 15%, as compared to O₂. The amount of reduced sites upon switching was quantified via the spectral intensities (i.e., the ratio between Co₃O₄ and CoO). This indicates that CO reduces part of the surface, while O₂ reoxidizes it, as expected for the Mars-van-Krevelen mechanism (which has been proven by numerous experimental and theoretical studies.^{5,12,13,18–21}) Figure 4d suggests that reoxidation (0.15 mbar O₂) was not complete though, but a tiny amount of reduced Co²⁺ species persisted.

With respect to the C 1s region, elementary carbon increased with temperature in CO, whereas switching to O₂ strongly decreased the (amorphous) carbon (interestingly, O₂ partially oxidizes carbon even at RT) (Figures 5 and S8). Thus, it is possible that a (minor) reaction pathway toward CO₂ proceeds via CO dissociation followed by carbon oxidation to CO/CO₂. In contrast, the carbonates decreased to a considerably lower extent at higher temperature, indicating that carbonate decomposition was more difficult than the reoxidation of carbon.

Carbonate formation has been previously reported for Co₃O₄,^{4,13,14} but the observed carbon deposition has been scarcely discussed in literature (indirect investigations by Jansson^{12,13} in the course of isotope studies). The current C 1s NAP-XPS data directly indicate carbon formation on Co₃O₄ during CO exposure and CO oxidation.

The simultaneous NAP-XPS/MS observations are in line with the redox Mars-van-Krevelen mechanism, but also point to a possible contribution of CO dissociation, elementary carbon deposition, and carbon reoxidation, the extent of which is however unknown. The role of the various carbonates remains ambiguous, why “switching” operando FTIR spectroscopy was employed.

3.3.2. FTIR Spectroscopy. Figure 6 shows operando FTIR spectra upon CO/O₂ switching (50 mbar CO vs 50 mbar O₂) on Co₃O₄. CO was introduced first and consecutive IR spectra were acquired for 10 min (each spectrum taking about 2 min), then the atmosphere was changed to O₂ and IR spectra were acquired after 2 and 10 min. Then, Co₃O₄ was heated in O₂ to the next temperature before introducing CO again (performed at RT, 100 °C, 150 °C, 200 °C, and 250 °C). FTIR shows that neither at RT nor at 100 °C carbonate decomposition by O₂ took place, not even during 10 min O₂ exposure. Mainly monodentate carbonates, apparently being quite stable, were present. At 150 °C, the carbonate peak area decreased during the first 2 min, and higher temperature decreased both mono- and bidentate carbonates. At 200 °C and 250 °C, the carbonates strongly decreased after 2 min and after 10 min no carbonates were present anymore (Figure 6). Overall, the surface carbonates seemed rather stable spectators, with their intensity decreasing rather slowly and mostly at high temperature, which rather excludes carbonates as reaction intermediates of fast CO oxidation. Thus, carbonate

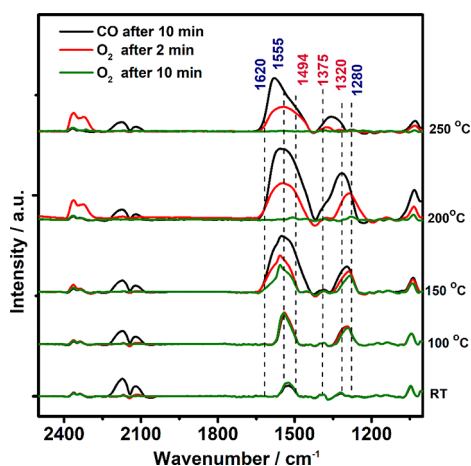


Figure 6. Operando FTIR on Co_3O_4 upon CO/O_2 switching experiments (50 mbar CO vs 50 mbar O_2): spectra recorded during the 10th minute of CO exposure (black), during the 2nd minute of O_2 exposure (red) and during the 10th minute of O_2 exposure (green).

formation/decomposition plays rather a minor role beside fast CO oxidation (MvK). Deactivation/site blocking by carbonates can also rather be excluded.

3.4. Carbonate Formation and Stability: FTIR Spectroscopy. 3.4.1. *Interaction of Co_3O_4 with Carbon Monoxide.* To further examine carbonate formation, reactivity

and stability, the interaction of CO with Co_3O_4 was studied by FTIR from RT to 350 °C (Figure 7a). Similar to $\text{CO}+\text{O}_2$, no adsorbed CO but only carbonates were observed. Mainly monodentate carbonates were formed at RT, bidentate carbonates emerged at 100 °C, and the overall carbonate intensity increased with temperature. This suggests that at higher temperature more reactive sites are formed that enable CO adsorption as a carbonate. Recall that NAP-XPS revealed partial reduction of the Co_3O_4 surface and surface oxygen vacancy formation in CO , especially from 100 °C to 200 °C.²⁷ When more vacancies were created, CO could adsorb as carbonate. Accordingly, heating in CO favors lattice oxygen extraction, increasing the concentration of carbonates. Note that in CO the amount of carbonates was significantly higher than that during CO oxidation (even in a stoichiometric mixture at low temperature) (Figure S9). The higher concentration of carbonates in CO as compared to O_2 -containing feed suggests that partial Co_3O_4 surface reduction is beneficial for carbonate formation. This will be discussed in the following.

3.4.2. *Investigation of Carbonate Stability in O_2 and He Atmosphere.* The thermal stability of carbonates was examined in O_2 and He atmospheres. FTIR spectra were recorded after exposing Co_3O_4 to CO at 200 °C and cooling in CO to RT (i.e., initial spectrum) and during heating in 50 mbar O_2 in He or in pure He. As evident from Figure 7b, introducing O_2 at RT already changed the carbonates, forming

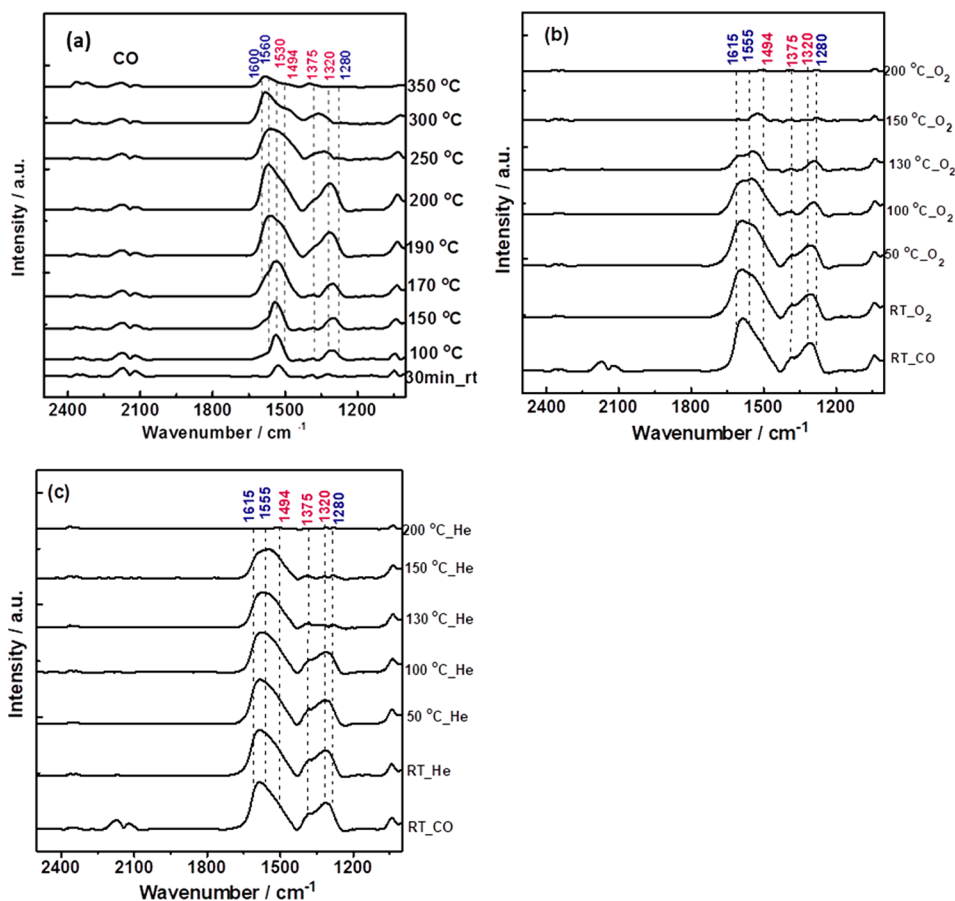


Figure 7. FTIR spectra on Co_3O_4 recorded during: (a) adsorption of CO (50 mbar) in flow mode (total flow 25 mL min^{-1}) from RT to 350 °C; (b) pretreatment with CO at 200 °C, cooling in CO to RT and heating in O_2 (100 mbar O_2 bar in He, total flow 25 mL min^{-1}); and (c) pretreatment with CO at 200 °C, cooling in CO to RT and heating in He (total flow 25 mL min^{-1}).

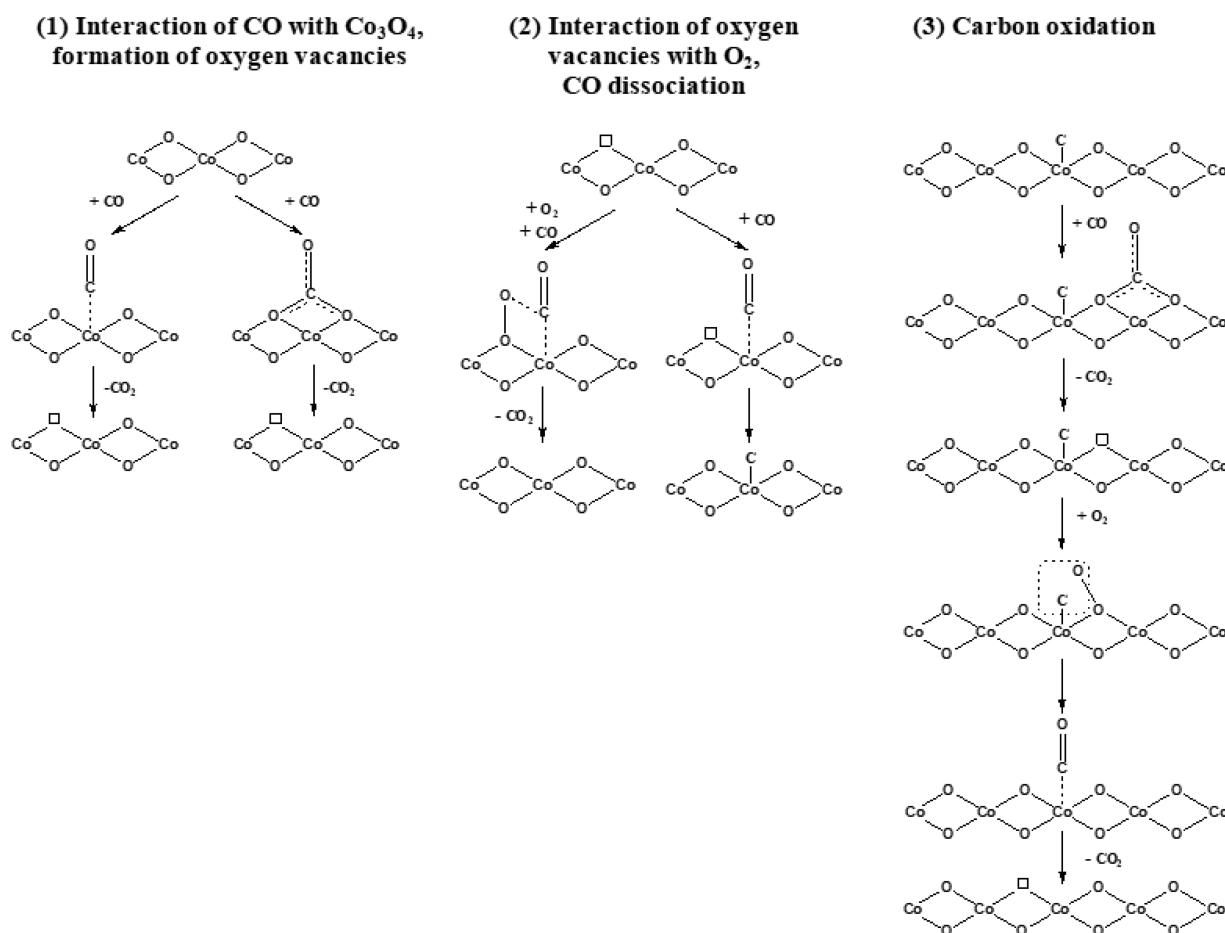


Figure 8. Schematic representation of CO oxidation on Co_3O_4 .

additional monodentate carbonates appearing as a shoulder at $\sim 1530\text{--}1470\text{ cm}^{-1}$. Heating in O_2 to $100\text{ }^\circ\text{C}$ decomposed both mono- and bidentate carbonates. At $130\text{ }^\circ\text{C}$, the intensity of carbonate bands decreased to 1/3 of its initial value. At $150\text{ }^\circ\text{C}$, only a small amount of monodentate carbonates were left on the cobalt oxide surface, while at $200\text{ }^\circ\text{C}$ it was free of carbonates.

The thermal stability of carbonates was also studied in He (Figure 7c). Again, FTIR spectra were recorded after exposing Co_3O_4 to CO at $200\text{ }^\circ\text{C}$, cooling down in CO to RT and heating in He. Up to $100\text{ }^\circ\text{C}$, no significant carbonate decomposition was observed. At $130\text{ }^\circ\text{C}$, carbonates started to decompose. However, the decrease was faster for the $1380\text{--}1280\text{ cm}^{-1}$ peaks than for the $1600\text{--}1430\text{ cm}^{-1}$ peaks, indicating different thermal stability and reactivity of surface carbonates. Importantly, at $150\text{ }^\circ\text{C}$ carbonates were still detected in He, whereas in O_2 only a small amount was present. The observation of carbonate peaks disappearing at about $200\text{ }^\circ\text{C}$ is in agreement with CO-TPD reported in our previous study (CO exposure at RT for 30 min followed by heating in He to $700\text{ }^\circ\text{C}$).²⁷ Only CO_2 evolved (and no CO) suggesting lattice oxygen extraction from cobalt oxide.

3.4.3. Interaction of Co_3O_4 with Carbon Dioxide. The results presented so far (CO vs CO/O_2) suggest that carbonate formation requires, or is at least facilitated, by partial surface reduction by CO. However, it is still unclear whether carbonates may also form by readsorption of the reaction product CO_2 . Thus, preoxidized Co_3O_4 was exposed to CO_2 at RT and heated to $200\text{ }^\circ\text{C}$ (Figure S10a).

Interestingly, neither at RT nor during heating any CO_2 adsorption/carbonate was observed; CO_2 remained in the gas phase (2336 and 2360 cm^{-1}). This is in contrast to CO_2 adsorption on many other oxides such as ZrO_2 ^{38,40} or Al_2O_3 ⁴¹ when CO_2 easily forms carbonates. The different affinity to CO_2 may be due to specific active sites or functional groups (i.e., OH, basic surface oxygen) that are missing on Co_3O_4 .

In another series of experiments, the interaction of CO_2 with Co_3O_4 prereduced by CO or H_2 (intended to create oxygen vacancies that seem required for CO_2 adsorption) was examined. (Figures S10b, S11, and S12). However, there was no CO_2 adsorption or carbonate formation under all conditions. Thus, it can be ruled out that the observed carbonates originate from CO_2 readsorption. Rather, they are only formed by direct interaction of Co_3O_4 with CO that partly reduces the Co_3O_4 surface. The higher concentration of surface carbonates in CO as compared to O_2 -containing feed also suggests this picture.

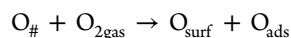
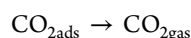
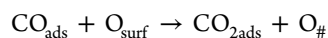
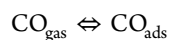
3.5. DISCUSSION

Using operando NAP-XPS, FTIR, and XRD we have examined the (surface) oxidation state of Co_3O_4 and adsorbates present during CO oxidation, and compared them with those in pure CO and upon switching between CO and O_2 . In particular, the comparison of static (steady-state) and switching experiments provided valuable information.

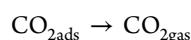
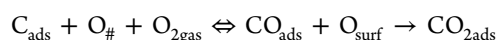
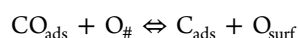
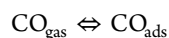
Combining information from NAP-XPS/FTIR and activity tests revealed a complex network of different reaction pathways contributing to CO oxidation on Co_3O_4 . In the following O_{surf}

$O_{\#}$, and O_{ads} refer to surface (lattice) oxygen, oxygen (surface) vacancies, and adsorbed atomic oxygen. Some pathways are reversible, others have been shown to be irreversible.

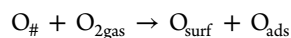
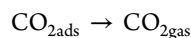
(1) Direct MvK pathway:



(2) via CO dissociation and carbon oxidation:



(3) via carbonates as intermediates:



Operando NAP-XPS and FTIR spectroscopy—in particular based on switching experiments—were in accordance with a fast CO oxidation route via a Mars-van-Krevelen mechanism (1), i.e., alternating reduction–oxidation of the Co_3O_4 surface by CO and O_2 . Carbon monoxide adsorbed to cobalt cations reacts with lattice surface oxygen, and the created oxygen vacancies ($\text{O}_{\#}$) are replenished by O_2 from the gas phase, further creating active O_{ads} species.

In addition, adsorbed CO (likely near $\text{O}_{\#}$) may undergo dissociation, filling an oxygen vacancy and depositing elementary carbon on the surface, which can be reoxidized by O_2 (once more near $\text{O}_{\#}$) (2). CO dissociation likely occurs at/near oxygen vacancies, as indicated by the larger amount of carbon present under more reducing conditions when more oxygen vacancies are formed. The carbon is quite reactive and is oxidized even at RT. Overall, CO dissociation and carbon reoxidation seems an (unavoidable) additional pathway of CO oxidation on Co_3O_4 .

The pronounced decline of surface carbonates appearing at higher temperature (at 200–250 °C the surface of Co_3O_4 is almost free of carbonates) suggests that the stable carbonates play a minor role, being rather spectators (3). Decomposition of carbonates to CO_2 is, however, facilitated by (excess) O_2 .

Below 100–150 °C, oxygen vacancies cannot be detected but Co_3O_4 exhibits considerable activity. A contribution via a Langmuir–Hinshelwood (LH) reaction can thus not be excluded. For methane oxidation on cobalt oxide spinel nanocubes Zasada et al.⁴² reported that at 300–450 °C the LH mechanism was dominant, whereas above 450 °C, LH and MvK coexisted.

The spectroscopically examined possible reaction pathways/elementary steps of CO oxidation on Co_3O_4 are summarized in Figure 8. Clearly, surface reduction by CO, reoxidation by O_2 , CO dissociation/reoxidation presumably at vacancies, and (to a lesser extent) carbonate formation/decomposition are key

processes, demonstrating the complexity of the seemingly simple CO oxidation.

4. CONCLUSIONS

Combining surface-specific chemical information from operando NAP-XPS and FTIR spectroscopy with activity tests revealed a complex network of four different reaction pathways of CO oxidation on Co_3O_4 : redox Mars-van-Krevelen, CO dissociation followed by carbon oxidation, formation of carbonate spectators, and possibly Langmuir–Hinshelwood at low temperature (which can currently not be excluded). Experiments performed under steady-state and dynamic conditions were in accordance with a MvK mechanism above 100 °C, involving the $\text{Co}^{3+}/\text{Co}^{2+}$ redox couple and oxygen vacancy formation. Under steady state, the Co_3O_4 surface appeared oxidized and only in pure CO about 15% Co^{2+} species at/near the surface were detected, suggesting the active sites being minority species. CO dissociation followed by carbon reoxidation and carbonate formation/decomposition are additional reaction pathways. Nevertheless, stable carbonates are rather spectators and also CO dissociation may be a minor route.

This work demonstrates the benefits of combining several operando techniques for studying catalysts under steady state and dynamic conditions, revealing a complex network of reaction pathways. Nevertheless, to assess the relative contributions of all pathways and to determine the rate limiting step, further studies would be required (e.g., by transient/concentration modulation IR spectroscopy⁴³ and detailed (micro)kinetic modeling).^{23–25}

■ ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge on the ACS Publications website at DOI: 10.1021/acscatal.8b01237.

CO conversion at different CO/ O_2 ratios, in situ XRD during CO oxidation, temperature-programmed reduction in H_2 followed by XRD, NAP-XPS during CO oxidation at different (additional) temperatures, MS data and Co 2p XP spectra obtained in the switching experiments, supplementary FTIR spectra of CO adsorption and CO oxidation, FTIR spectra of CO_2 adsorption, C 1s spectral fitting parameters, spectral ranges, and assignment of surface carbonates (PDF)

■ AUTHOR INFORMATION

Corresponding Authors

*E-mail: karin.foettinger@tuwien.ac.at (K.F.).

*E-mail: guenther.ruppachter@tuwien.ac.at (G.R.).

ORCID

Karin Föttinger: 0000-0002-2193-0755

Günther Ruppachter: 0000-0002-8040-1677

Present Address

[†]Johnson Matthey, PO Box 1, Belasis Avenue, Billingham, Cleveland, TS23 1LB, U.K.

Author Contributions

The manuscript was written through contributions of all authors. All authors have given approval to the final version of the manuscript.

Funding

This work was supported by the Austrian Science Fund (FWF) in the framework of the Doctoral School “Building Solids for Function (“Solids4Fun”) [project W1243] and the ComCat Project [I 1041-N28].

Notes

The authors declare no competing financial interest.

ACKNOWLEDGMENTS

We acknowledge the Helmholtz-Zentrum Berlin for synchrotron radiation beamtime at ISSS beamline of BESSY II. The research leading to these results has received funding from the European Community's Seventh Framework Programme (FP7/2007-2013) under grant agreement no. 312284. We are grateful to Dr. Klaudia Hradil and DI Werner Artner for assistance with the in situ XRD measurements. L.L. is grateful to Dr. Leon van de Water from Johnson Matthey for useful discussions.

REFERENCES

- (1) Ertl, G. Reactions at Surfaces: From Atoms to Complexity (Nobel Lecture). *Angew. Chem., Int. Ed.* **2008**, *47*, 3524–3535.
- (2) Zorn, K.; Giorgio, S.; Halwax, E.; Henry, C. R.; Gronbeck, H.; Rupprechter, G. CO Oxidation on Technological Pd-Al₂O₃ Catalysts: Oxidation State and Activity. *J. Phys. Chem. C* **2011**, *115*, 1103–1111.
- (3) Royer, S.; Duprez, D. Catalytic Oxidation of Carbon Monoxide over Transition Metal Oxides. *ChemCatChem* **2011**, *3*, 24–65.
- (4) Jia, C.-J.; Schwickardi, M.; Weidenthaler, C.; Schmidt, W.; Korhonen, S.; Weckhuysen, B. M.; Schüth, F. Co₃O₄-SiO₂ Nanocomposite: A Very Active Catalyst for CO Oxidation with Unusual Catalytic Behavior. *J. Am. Chem. Soc.* **2011**, *133*, 11279–11288.
- (5) Xie, X.; Li, Y.; Liu, Z.-Q.; Haruta, M.; Shen, W. Low-temperature oxidation of CO catalysed by Co₃O₄ nanorods. *Nature* **2009**, *458*, 746–749.
- (6) Teng, Y.; Kusano, Y.; Azuma, M.; Haruta, M.; Shimakawa, Y. Morphology effects of Co₃O₄ nanocrystals catalyzing CO oxidation in a dry reactant gas stream. *Catal. Sci. Technol.* **2011**, *1*, 920–922.
- (7) Gu, D.; Jia, C.-J.; Weidenthaler, C.; Bongard, H.-J.; Spliethoff, B.; Schmidt, W.; Schüth, F. Highly Ordered Mesoporous Cobalt-Containing Oxides: Structure, Catalytic Properties, and Active Sites in Oxidation of Carbon Monoxide. *J. Am. Chem. Soc.* **2015**, *137*, 11407–11418.
- (8) Iablokov, V.; Barbosa, R.; Pollefeyt, G.; Van Driessche, I.; Chenakin, S.; Kruse, N. Catalytic CO Oxidation over Well-Defined Cobalt Oxide Nanoparticles: Size-Reactivity Correlation. *ACS Catal.* **2015**, *5*, 5714–5718.
- (9) Ding, K.; Wang, D.; Yang, P.; Hou, P.; Cheng, X. Enhanced CO catalytic oxidation of flower-like Co₃O₄ composed of small nanoparticles. *RSC Adv.* **2016**, *6*, 16208–16214.
- (10) Yu, Y.; Takei, T.; Ohashi, H.; He, H.; Zhang, X.; Haruta, M. Pretreatments of Co₃O₄ at moderate temperature for CO oxidation at – 80 °C. *J. Catal.* **2009**, *267*, 121–128.
- (11) Pollard, M. J.; Weinstock, B. A.; Bitterwolf, T. E.; Griffiths, P. R.; Piers Newbery, A.; Paine Iii, J. B. A mechanistic study of the low-temperature conversion of carbon monoxide to carbon dioxide over a cobalt oxide catalyst. *J. Catal.* **2008**, *254*, 218–225.
- (12) Jansson, J. Low-Temperature CO Oxidation over Co₃O₄/Al₂O₃. *J. Catal.* **2000**, *194*, 55–60.
- (13) Jansson, J.; Skoglundh, M.; Fridell, E.; Thormählen, P. A Mechanistic Study of Low Temperature CO Oxidation over Cobalt Oxide. *Top. Catal.* **2001**, *16*, 385–389.
- (14) Jansson, J.; Palmqvist, A. E. C.; Fridell, E.; Skoglundh, M.; Österlund, L.; Thormählen, P.; Langer, V. On the Catalytic Activity of Co₃O₄ in Low-Temperature CO Oxidation. *J. Catal.* **2002**, *211*, 387–397.
- (15) Perti, D.; Kabel, R. L. Kinetics of CO oxidation over Co₃O₄/γ-Al₂O₃. Part I: Steady state. *AIChE J.* **1985**, *31*, 1420–1426.
- (16) Perti, D.; Kabel, R. L. Kinetics of CO oxidation over Co₃O₄/γ-Al₂O₃. Part II: Reactor dynamics. *AIChE J.* **1985**, *31*, 1427–1434.
- (17) Perti, D.; Kabel, R. L.; McCarthy, G. J. Kinetics of CO oxidation over Co₃O₄/γ-Al₂O₃. *AIChE J.* **1985**, *31*, 1435–1440.
- (18) Broqvist, P.; Panas, I.; Persson, H. A DFT Study on CO Oxidation over Co₃O₄. *J. Catal.* **2002**, *210*, 198–206.
- (19) Wang, H.-F.; Kavanagh, R.; Guo, Y.-L.; Guo, Y.; Lu, G.; Hu, P. Origin of extraordinarily high catalytic activity of Co₃O₄ and its morphological chemistry for CO oxidation at low temperature. *J. Catal.* **2012**, *296*, 110–119.
- (20) Pang, X.-Y.; Liu, C.; Li, D.-C.; Lv, C.-Q.; Wang, G.-C. Structure Sensitivity of CO Oxidation on Co₃O₄: A DFT Study. *ChemPhysChem* **2013**, *14*, 204–212.
- (21) Jiang, D.-e.; Dai, S. The role of low-coordinate oxygen on Co₃O₄(110) in catalytic CO oxidation. *Phys. Chem. Chem. Phys.* **2011**, *13*, 978–984.
- (22) Luo, J.-Y.; Meng, M.; Li, X.; Li, X.-G.; Zha, Y.-Q.; Hu, T.-D.; Xie, Y.-N.; Zhang, J. Mesoporous Co₃O₄-CeO₂ and Pd/Co₃O₄-CeO₂ catalysts: Synthesis, characterization and mechanistic study of their catalytic properties for low-temperature CO oxidation. *J. Catal.* **2008**, *254*, 310–324.
- (23) Vogel, D.; Spiel, C.; Suchorski, Y.; Trinchero, A.; Schlögl, R.; Grönbeck, H.; Rupprechter, G. Local Catalytic Ignition during CO Oxidation on Low-Index Pt and Pd Surfaces: A Combined PEEM, MS, and DFT Study. *Angew. Chem., Int. Ed.* **2012**, *51*, 10041–10044.
- (24) Markova, V. K.; Philbin, J. P.; Zhao, W.; Genest, A.; Silvestre-Albero, J.; Rupprechter, G.; Rösch, N. Catalytic Transformations of 1-Butene over Palladium. A Combined Experimental and Theoretical Study. *ACS Catal.* **2018**, *8*, 5675–5685.
- (25) Suchorski, Y.; Datler, M.; Bespalov, I.; Zeininger, J.; Stöger-Pollach, M.; Bernardi, J.; Grönbeck, H.; Rupprechter, G. Visualizing catalyst heterogeneity by a multifrequency oscillating reaction. *Nat. Commun.* **2018**, *9*, 600.
- (26) Zafeiratos, S.; Dintzer, T.; Teschner, D.; Blume, R.; Hävecker, M.; Knop-Gericke, A.; Schlögl, R. Methanol oxidation over model cobalt catalysts: Influence of the cobalt oxidation state on the reactivity. *J. Catal.* **2010**, *269*, 309–317.
- (27) Lukashuk, L.; Föttinger, K.; Kolar, E.; Rameshan, C.; Teschner, D.; Hävecker, M.; Knop-Gericke, A.; Yigit, N.; Li, H.; McDermott, E.; Stöger-Pollach, M.; Rupprechter, G. Operando XAS and NAP-XPS studies of preferential CO oxidation on Co₃O₄ and CeO₂-Co₃O₄ catalysts. *J. Catal.* **2016**, *344*, 1–15.
- (28) Knop-Gericke, A.; Kleimenov, E.; Hävecker, M.; Blume, R.; Teschner, D.; Zafeiratos, S.; Schlögl, R.; Bukhtiyarov, V. I.; Kaichev, V. V.; Prosvirni, I. P.; Nizovskii, A. I.; Bluhm, H.; Barinov, A.; Dudin, P.; Kiskinova, M. X-Ray Photoelectron Spectroscopy for Investigation of Heterogeneous Catalytic Processes. In *Advances in Catalysis*; Academic Press, 2009; Vol. 52; pp 213–272.
- (29) Biesinger, M. C.; Payne, B. P.; Grosvenor, A. P.; Lau, L. W. M.; Gerson, A. R.; Smart, R. S. C. Resolving surface chemical states in XPS analysis of first row transition metals, oxides and hydroxides: Cr, Mn, Fe, Co and Ni. *Appl. Surf. Sci.* **2011**, *257*, 2717–2730.
- (30) Grosvenor, A. P.; Wik, S. D.; Cavell, R. G.; Mar, A. Examination of the Bonding in Binary Transition-Metal Monophosphides MP (M = Cr, Mn, Fe, Co) by X-Ray Photoelectron Spectroscopy. *Inorg. Chem.* **2005**, *44*, 8988–8998.
- (31) Feng, Z. A.; Machala, M. L.; Chueh, W. C. Surface electrochemistry of CO₂ reduction and CO oxidation on Sm-doped CeO_{2-x}: coupling between Ce³⁺ and carbonate adsorbates. *Phys. Chem. Chem. Phys.* **2015**, *17*, 12273–12281.
- (32) Ferstl, P.; Mehl, S.; Arman, M. A.; Schuler, M.; Toghan, A.; Laszlo, B.; Lykhach, Y.; Brummel, O.; Lundgren, E.; Knudsen, J.; Hammer, L.; Schneider, M. A.; Libuda, J. Adsorption and Activation of CO on Co₃O₄(111) Thin Films. *J. Phys. Chem. C* **2015**, *119*, 16688–16699.
- (33) Shchukarev, A. V.; Korolkov, D. V. XPS Study of group IA carbonates. *cent.eur.j.chem.* **2004**, *2*, 347–362.

(34) Wolfbeisser, A.; Klotzer, B.; Mayr, L.; Rameshan, R.; Zemlyanov, D.; Bernardi, J.; Föttinger, K.; Rupprechter, G. Surface modification processes during methane decomposition on Cu-promoted Ni-ZrO₂ catalysts. *Catal. Sci. Technol.* **2015**, *5*, 967–978.

(35) Ramsvik, T.; Borg, A.; Kildemo, M.; Raaen, S.; Matsuura, A.; Jaworowski, A. J.; Worren, T.; Leandersson, M. Molecular vibrations in core-ionised CO adsorbed on Co(0 0 0 1) and Rh(1 0 0). *Surf. Sci.* **2001**, *492*, 152–160.

(36) Diemant, T.; Bansmann, J.; Behm, R. J. CO oxidation on planar Au/TiO₂ model catalysts: Deactivation and the influence of water. *Vacuum* **2009**, *84*, 193–196.

(37) Denkwitz, Y.; Zhao, Z.; Hörmann, U.; Kaiser, U.; Plzak, V.; Behm, R. J. Stability and deactivation of unconditioned Au/TiO₂ catalysts during CO oxidation in a near-stoichiometric and O₂-rich reaction atmosphere. *J. Catal.* **2007**, *251*, 363–373.

(38) Köck, E.-M.; Kogler, M.; Bielz, T.; Klötzer, B.; Penner, S. In Situ FT-IR Spectroscopic Study of CO₂ and CO Adsorption on Y₂O₃, ZrO₂, and Ytria-Stabilized ZrO₂. *J. Phys. Chem. C* **2013**, *117*, 17666–17673.

(39) Davydov, A. *Molecular Spectroscopy of Oxide Catalyst Surfaces*; John Wiley & Sons Ltd: The Atrium, Southern Gate, Chichester, West Sussex PO19 8SQ, England, 2003; pp 95–136.

(40) Pokrovski, K.; Jung, K. T.; Bell, A. T. Investigation of CO and CO₂ Adsorption on Tetragonal and Monoclinic Zirconia. *Langmuir* **2001**, *17*, 4297–4303.

(41) Föttinger, K.; Schlogl, R.; Rupprechter, G. The mechanism of carbonate formation on Pd-Al₂O₃ catalysts. *Chem. Commun.* **2008**, 320–322.

(42) Zasada, F.; Janas, J.; Piskorz, W.; Gorczyńska, M.; Sojka, Z. Total Oxidation of Lean Methane over Cobalt Spinel Nanocubes Controlled by the Self-Adjusted Redox State of the Catalyst: Experimental and Theoretical Account for Interplay between the Langmuir–Hinshelwood and Mars-Van-Krevelen Mechanisms. *ACS Catal.* **2017**, *7*, 2853–2867.

(43) Haghofar, A.; Ferri, D.; Föttinger, K.; Rupprechter, G. Who Is Doing the Job? Unraveling the Role of Ga₂O₃ in Methanol Steam Reforming on Pd₂Ga/Ga₂O₃. *ACS Catal.* **2012**, *2*, 2305–2315.