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# Filtration and inactivation of aerosolized bacteriophage MS2 by a CNT air filter fabricated using electro-aerodynamic deposition



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#### ABSTRACT

Carbon nanotubes (CNTs) were coated on a sample of glass fiber air filter medium at atmospheric pressure and room temperature using electro-aerodynamic deposition (EAD). In the EAD method, CNTs (diameter: 50 nm, length: 2–3  $\mu$ m) were aerosolized, electrically charged, and injected through a nozzle. A voltage was applied externally between the ground nozzle and a planar electrode on which the sample was located. The charged CNTs were deposited on the sample in a vertically standing posture even at a low flow velocity. Before the deposition experiment, a calculation was performed to determine the applied voltage by simulating the electric field, flow field, and particle trajectory. Using CNT-coated filter samples, virus aerosol filtration and anti-viral tests were carried out using the aerosol number counting method and the plaque counting method, respectively. For this purpose, bacteriophage MS2 was aerosolized with an atomizer. The particle filtration efficiency was increased to 33.3% in the most penetration particle size zone (100 nm) and the antiviral efficiency of the CNT filter was 92% when the coating areal density was  $1.5 \times 10^9$ #/cm<sup>2</sup>. The susceptibility constant of virus to CNTs was 0.2 cm<sup>2</sup>/µg.

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# 1. Introduction

Biological aerosols generally include bacteria, fungi, viruses and their derivatives such as endotoxin, glucans and mycotoxin. Exposure has been shown to cause many adverse health effects including allergic, toxic, and infectious responses [1–3]. Aerosol transmission is known to play an important role in observed airborne microbial infections. Studies indicate that large scale outbreaks of severe acute respiratory syndrome (SARS) were mainly the result of airborne exposure routes [4,5]. Viruses are detected in air samples collected from hospital rooms [6,7] and also in human breath [8,9]. A study indicated that there was an approximately 23% possibility of influenza virus infections in people wearing surgical and N95 respiratory masks [10]. Therefore, development of efficient air control technology is important in combating inhalation-related diseases.

Over the years, a large volume of studies have been undertaken to develop air cleaning technologies. Among the various air cleaning techniques, filtration is widely applied to remove particles from air streams. However, recent research has demonstrated that some microorganisms are capable of colonizing the air filter surface in heating, ventilating, and air-conditioning systems (HVAC) [11–13], and the organic or inorganic materials deposited on the filter surface can contribute to microbial growth. Air filters contaminated by microorganisms lead to the release of microorganisms from the filter surface [14], and the emission of volatile organic

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compounds (VOCs) produced by microbial metabolism [11,12]. Biologically contaminated filter could pose a significant health hazard through reaerosolizing opportunistic pathogenic or allergenic aerosols [15]. Antimicrobial treatment could be a possible solution to these problems.

Carbon nanotubes (CNTs) have been increasingly used in environmental applications due to their high specific surface area, smooth surface, and adsorption capability [16]. Recently, multi-walled and single-walled CNT filters were developed and found to be effective for multilog microbial removal from contaminated water by physical straining, puncture and depth filtration [17–20]. CNTs were shown to inactivate the highest percentage of cells both in monocultures and diverse microbial communities of river water and wastewater effluents [21–23]. A CNT filter was successfully created and utilized to remove biological agents from water with filtration efficiency [17–21,24–26].

Even though carbon nanotube filters have been extensively studied for water purification, there are only a few reports in the literature on carbon nanotube use for air purification. Viswanathan et al. [27] presented the first investigation of the use of multi-walled carbon nanotubes (MWCNTs) as high efficient, airborne particulate filter media. High filtration efficiencies were achieved from films of MWCNTs deposited onto cellulose fiber filters. The MWCNT-coated filters exhibited low pressure drops and better filter quality than cellulose filters. Park and Lee [28] constructed a metal MWCNT filter in which carbon nanotubes were grown directly on the micron-sized metallic fibers of the air filter using the thermal chemical vapor deposition (CVD) method. The metal MWCNT filter had higher filtration efficiency than conventional filters without a significant decrease in pressure. Karwa and Tatarcuk [29] studied an enhancement in aerosol filtration by synthesizing carbon nanostructures including nanofibers within nickel sintered metal microfibrous matrices/filter media. Their study showed that carbon nanostructure synthesis led to significant improvement in the performance of filter media with large initial pore size because the pore diameters did not reduce significantly with synthesis. Yildiz and Bradford [30] prepared novel filters by drawing aligned CNTs sheets and embedding them between polypropylene melt-blown nonwoven fabrics using calendaring. The filters were prepared with an increasing number of CNT sheets. The filtration performance of the novel filters showed that when the number of CNTs layers increased, the filtration efficiency increased dramatically, while the pressure drop also increased. Guan and Yao [31] investigated the removal efficiencies of CNT filters for a collection of aerosolized biological and non-biological particles. In their preparation of the CNT filters, a predetermined volume of CNT suspension with a certain concentration was uniformly filtered through the membrane support. The removal efficiencies for aerosols and bacteria were shown to increase with increased loadings of CNTs regardless of membrane supports and pore size tested. Xu and Yao [32] fabricated a single walled carbon nanotube (SWCNT) filter with CNT solution, and investigated its anti-bacterial efficacy with CNT loading. Their results revealed that particle types and CNT loading had greater effects on anti-bacterial efficacy than other membrane types and pore sizes tested. Park et al.

[33] reported that a MWCNT-deposited glass fiber filter showed increased particle filtration efficiency and antibacterial activity. In the fabrication of CNT filters, samples of glass fiber filter media were catalytically activated with iron (Fe) nanoparticles generated by the spark discharge method. The catalytically activated filter samples were placed in a thermal CVD reactor in which MWCNT fibers were vertically grown on the activated spots after acetylene ( $C_2H_2$ ) gas was carried into the reactor.

However, the fabrication of a CNT filter using the spark discharge method followed by the CVD process requires time and effort in controlling the operation of a CVD reactor. In addition, the durability of a CNT filter made by the CVD process can be degraded in the high temperature environment associated with the CVD process. In this paper, we suggest an aerosol process of fabricating a CNT filter at atmospheric pressure and temperature using the electro-aerodynamic deposition (EAD) method, the details of which were introduced in our previous study [34]. In the EAD method, CNTs were aerosolized, electrically charged, and injected through a nozzle, where an external electric field was applied. The charged CNTs were vertically deposited on the glass fiber filter media even at a low flow velocity. Using CNT coated filter samples, virus aerosol filtration and anti-viral tests were carried out using the aerosol number counting technique and the plaque counting method, respectively.

Susceptibility has been used to explain the relative importance of various parameters affecting antimicrobial efficacy. Yoon et al. [35] used susceptibility to evaluate the antibacterial effects of silver and copper nanoparticles. Kim et al. [36] applied susceptibility to evaluate the antibacterial effects of corona discharge-generated ions in the air. In this paper, the susceptibility of a virus to CNTs was calculated to determine the inactivation efficacy with respect to CNT concentration.

# 2. Materials and methods

#### 2.1. CNT filter fabrication

Fig. 1 shows the process of coating CNTs on a substrate. The set-up consisted of CNT aerosolization (A), CNT charging (B), and CNT deposition (C) equipment. Commercial MWCNTs (Nanokarbon, Korea) with a diameter of 50 nm and a length of 2–3  $\mu$ m were used. After compressed air was passed through a clean air supply consisting of an oil trap, diffusion dryer, and high efficiency particulate air (HEPA) filter, the particle-free compressed air entered a Collison type atomizer (9302, TSI Inc., USA), which was filled with 9 ml of de-ionized water and 1 ml of 1% CNT solution. The aerosol flow rate was controlled by a rotameter. Dry, clean air at 3 lpm formed a high-velocity jet through an orifice in the atomizer. The pressure drop from this jet drew the CNT solution up through a tube. The solution was then broken up into droplets by the high-velocity air jet. The resultant larger droplets impinged on an impactor, while the smaller droplets made no contact and formed an aerosol that exited through an outlet. The aerosolized CNTs were passed through a diffusion dryer for water removal and a neutralizer (Soft X-ray charger 4530,



Fig. 1 – Schematic of the electro-aerodynamic deposition system used for CNT filter fabrication (A, B, C) and experimental setup (D) for filtration, pressure drop, and antiviral tests. (A color version of this figure can be viewed online.)

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HCT, Korea) to induce a Boltzmann charge distribution (Fig. 1(A)).

The neutralized CNTs entered a unipolar charger where a stainless steel needle (wire) electrode, located at the center, was used to generate a corona discharge on its sharp tip (Fig. 1B). The corona discharge generated air ions, which moved along the electric field to a grounded cylinder (made of Duralumin). The amount of charge per particle was controlled by DC voltage supplied from a high voltage power supply. A voltage of -8 kV was applied to the needle to charge the CNTs. Details of the charger are described in Park et al. [37].

The electrical current carried by the charged CNTs was measured with an aerosol electrometer (3068A, TSI, ISA) to obtain the average charge number of the CNTs, using the following equation:

$$h_p = \frac{I}{N \cdot e \cdot Q} \tag{1}$$

where  $n_p$  is the average charge number, e is the elementary charge, I is the measured current, Q is the flow rate, and N is the number concentration of the charged CNTs (Fig. 1B). An ion trap was used to remove free unattached ions and allow charged particles to pass through the ion trap zone. The ion trap voltage was 200 V [38].

The charged CNTs then entered a cylindrical nozzle (Fig. 1C) with a length of 30 cm and a diameter of 6 mm, which induced a fully developed flow and minimize the entrance effect at the nozzle (Re = 700). The nozzle filet had a finite radius of curvature (2 mm) at the tip so that the electric field applied to this tip was minimized [39]. After the charged CNTs were ejected from the nozzle, they were guided

by electrical force to deposit on a substrate located on an electrode to which a high voltage was applied. The distance between the nozzle and the substrate was 10 mm. A silicon wafer or glass fiber filter medium (Fabriano, Italy) was used as the substrate.

Before the deposition experiment, a calculation was performed to determine the voltage applied to the substrate. Commercial computational fluid dynamics (CFD) software, FLUENT, with external user defined function (UDF) code was used to simulate the electric field, flow field, and particle charging motion. FLUENT is a solver software package for various physics and engineering applications and utilizes the finite volume method (FVM). Even though FLUENT does not include an electric field solver, UDFs allow for the customization of FLUENT to fit particular modeling needs. The discrete phase model (DPM) and the Laminar model in FLUENT were used as the particle solver and the flow solver, respectively.

First, the continuity equation and Navier–Stokes equation were solved for the flow velocity. The electric field was then obtained by solving Poisson's equation with known particle concentration and particle charge  $(n_p)$  values. Finally, the particle trajectory was calculated using the following equation:

$$\frac{d\vec{u}_{p}}{dt} = \frac{18\mu}{d_{p}^{2}\rho_{p}C_{c}}(\vec{u} - \vec{u}_{p}) + \frac{\vec{g}(\rho_{p} - \rho)}{\rho_{p}} + \vec{F}_{p}$$
(2)

where  $\vec{u}$  is the flow velocity,  $\rho$  is the density of air,  $\vec{g}$  is the gravitational constant,  $d_p$  is the particle diameter,  $\vec{u}_p$  is the particle velocity,  $\rho_p$  is the particle density,  $C_c$  is the Cunningham slip correction factor, and  $\mu$  is the dynamic viscosity of air.  $\vec{F}_p$  in Eq. (2) describes the electrostatic forces on a particle (per unit mass) and can be expressed as follows:

$$\vec{F}_p = \vec{F}_E + \vec{F}_{Di} + \vec{F}_{Im} \tag{3}$$

where  $\vec{F}_E$  is the Coulombic force per unit mass that is induced by charges and electric fields,  $\vec{F}_{Di}$  is the dipole force per unit mass, and  $\vec{F}_{Im}$  is the image force acting on a particle per unit mass [40,41]. Simulation details can be found in Park et al. [34].

A scanning mobility particle sizer (SMPS) system consisting of a differential mobility analyzer (DMA, 3081, TSI, USA) and a condensation particle counter (CPC, 3025, TSI, USA) was utilized to evaluate the CNT coating efficiency (Fig. 1C). Aerosol sampling was carried out upstream of the nozzle (I) and also at the air outlet (II) from undeposited CNTs exited. The SMPS system was operated under a sampling flow rate of 0.3 lpm and a scan time of 180 s.

After fabrication of the CNT filter using glass fiber filter medium as the substrate, it was necessary to confirm whether the CNTs were firmly deposited on the glass fibers. For this purpose, clean air with a face velocity of 1.5 m/s was forced to flow through the CNT filter. A SMPS was located downstream of the CNT filter to measure the number of CNTs that detached from the filter.

#### 2.2. Preparation of virus solution

Bacteriophage MS2 (ATCC 15597-B1) and Escherichia coli strain C3000 (ATTCC 15597) were selected as the test virus and host bacteria, respectively. To recover bacterial cells from a freezedried state, 10 ml of tryptic soy broth (TSB) was mixed with the freeze-dried bacterial cells and the mixture was incubated with shaking for 24 h at 37 °C. A total of 0.1 ml of the incubated bacterial solution was injected into the 10 ml of TSB. The TSB solution containing the bacteria was used as the host bacterial solution after incubation with shaking for six hours at 37 °C.

One milliliter of TSB was injected into the freeze-dried MS2 virus, and 0.1 ml of the viral solution was extracted. The extracted solution was mixed with 0.3 ml of the host bacterial solution and 29 ml of soft tryptic soy agar (TSA) containing 8 g/l of agar. The resulting agar solution was poured into a Petri dish and incubated overnight at 37 °C. The surface of the agar was scraped off with 10 ml of phosphate buffer solution (PBS), pH 7.0. The solution was centrifuged for 20 min at 5000G, and the supernatant was used as the virus solution in subsequent experiments.

#### 2.3. Filtration test

Prior to filtration testing, the pressure drop across the CNT filter was measured using a differential pressure gauge (Magnehelic 2000, Dwyer Instruments Inc., USA) with various face velocities of clean air ranging from 0.0 m/s to 0.2 m/s.

After the pressure drop test, the filtration test was carried out using bacteriophage MS2. The experimental setup for the filtration test is shown in Fig. 1D. The system consisted of a test duct with a cross-sectional area of  $40 \text{ mm} \times 40 \text{ mm}$  and a length of 1000 mm, a test particle generation system, and a measurement system. A CNT filter sample was installed in the middle of the test duct. Two isokinetic stainless steel sampling probes were placed before and after the filter media for aerosol sampling. Aerosolized virus particles were supplied to the test duct by the same procedure used in the supply of aerosolized CNTs. The number concentration of the virus particles was measured using an SMPS before and after the filter. A stream of clean air was delivered to the test duct and mixed with the particle-laden air flow to adjust the flow velocity. The fractional particle filtration efficiency,  $\eta_F(d_p)$ , was defined using the following equation:

$$\eta_F(d_p) = 1 - \frac{C_{downstream}(d_p)}{C_{upstream}(d_p)}$$
(4)

where  $C(d_p)$  is the number concentration of aerosolized bacteriophage MS2 of size  $d_p$ . The filter quality factor was evaluated with various face velocities using following equation:

$$q_{\rm F} = \frac{\ln\left(\frac{1}{1-\eta_{\rm F}}\right)}{\Delta p} \tag{5}$$

where  $q_F$  is the quality factor,  $\Delta p$  is the pressure drop, and  $\eta_F$  is the integrated value of  $\eta_F(d_p)$  over the particle size  $d_p$ .

#### 2.4. Antiviral test

The experimental set-up for the antiviral test is also shown in Fig. 1D. To aerosolize the virus particles, 0.1 ml of the supernatant was diluted with 50 ml deionized (DI) water. The virus particles were aerosolized, and deposited onto each test filter for 30 min in the test duct. A pristine filter and CNT-coated filter were used for comparison. Each filter was put into the 10 ml of DI water and subjected to sonication for ten minutes with a batch-type sonicator (KMC1300V, Vision Scientific, Korea) to detach deposited virus particles from the filter. Then 0.1 ml of the water containing virus particles was mixed with 0.3 ml of host bacterial solution and 29 ml of soft TSA. The mixed solution was poured into a Petri dish and incubated overnight at 37 °C. The number of plaques that appeared on the plate was counted and the antiviral efficiency was calculated using the following equation:

$$\eta_{\rm A} = 1 - \frac{\rm PFU_{\rm CNT\ filter}}{\rm PFU_{\rm Pristine\ filter}} \tag{6}$$

where the numerator is the number of plaque forming units (PFU) on the nutrient agar plate after incubation when the CNT filter was used, and the denominator is the number of plaque forming units on the nutrient agar plate after incubation when the pristine glass fiber filter was used.

The susceptibility of virus to CNTs was determined by calculating the susceptibility constant Z defined by the following equation,

$$Z = \frac{-\ln(1 - \eta_A)}{C} \tag{7}$$

where C is the coating areal mass density of CNTs ( $\mu$ g/cm<sup>2</sup>). A higher Z value implies higher antiviral activity. Moreover, experiments were carried out to compare the viable viral count in the air before and after the filtration, with both pristine and modified filters under the same experimental condition with the filtration test (at face velocity: 0.2 m/s). We generated virus with an atomizer and sampled aerosolized virus at both upstream and downstream the test filter. The sampled virus was captured on a sampling filter and cultured for PFU counting.

# 3. Results and discussion

# 3.1. Fabrication of CNT filter

The process depositing of CNTs on a glass fiber filter sample required that the CNTs were highly charged by the corona charger. When a voltage of -8 kV was applied to the needle of the charger, the current carried by the charged CNTs was measured to estimate their average charge using Eq. (1). With measured values of I ( $=3.6 \times 10^{-12}$  A), Q (=3 lpm), and N ( $=4.52 \times 10^5$  #/cm<sup>3</sup>), we determined that the average charge number was 110, which was in good agreement with the value of 116 obtained from calculation using the classical charging theory [40]. In the calculation, we assumed that the CNTs had a shape factor of 1.91 [40]. The particle diameter calculated with this shape factor was 162 nm, which was very close to 160 nm measured using the SMPS system.

For a given CNT charge number, a calculation was carried out to determine the voltage applied to the substrate. Fig. 2 shows the (a) voltage distribution and (b) trajectories of CNTs near the substrate, under the electric field. When the applied voltage was less than 300 V, CNT particles would not deposit on the substrate. However, at a potential of 300 V, CNTs started to deposit on the substrate and the CNT deposition area decreased. The calculated results were in good agreement with those predicted by the following equation [34]:

$$\frac{W_p}{W} \simeq 0.96 \left(\frac{n_p e C_c V}{3\pi \mu U d_p h}\right)^{-0.41} \tag{8}$$

where W is the nozzle width, U is the flow velocity at the nozzle, V is the voltage applied to the substrate, h is the distance between the nozzle and the substrate, and  $W_p$  is the radius of the coated region.

CNT deposition experiments were conducted with a Si wafer substrate. Fig. 3 shows field emission scanning electron microscopy (FE-SEM) images of CNTs deposited on the substrate. When the charger was not operated, there were no CNTs observed on the substrate, regardless of the voltage applied (Fig. 3(a)). When charged CNTs were flowing toward the substrate where no electric field was applied, several particles were deposited as shown in Fig. 3(b), which was caused by an image force between the CNTs and the substrate (Eq. (3)). When the charged CNTs were delivered to a substrate of opposite polarity, many of them were successfully deposited on the



Fig. 2 – (a) Effect of applied voltage on the CNT coating width. (b) Spatial voltage distribution between the nozzle and the substrate (applied voltage of 7 kV). (c) Particle trajectory and coating width (applied voltage of 7 kV). (A color version of this figure can be viewed online.)



(a) Charger: 0 kV, Substrate:7 kV (Top view)





(c) Charger: -8 kV, Substrate: 7 kV (Top view)

(d) Charger: -8 kV, Substrate: 7 kV (Front view)

Fig. 3 - FE-SEM images of CNT deposition under various conditions.

surface (Fig. 3(c)). Fig. 3(d) shows a frontal view of the deposited CNTs. Note that the CNTs were vertically aligned. This phenomenon was due to characteristics of the charged CNTs. According to Keblinski et al. [42], CNTs have higher charge concentration on both tube ends than in the central part. Therefore, when they landed on the substrate the end of each CNT that was closer to the substrate than the other end was attracted to the substrate, resulting in the standing posture of the tubes.

The CNT deposition experiment was also carried out using glass fiber filter medium as the substrate. The cross-sectional size of the filter was 40 mm × 40 mm. Fig. 4 shows the size distribution of CNTs measured before the nozzle inlet (location I in Fig. 1) and away from the nozzle outlet (II), measured with the SMPS system. The total number concentrations of CNTs at locations I and II were  $4.52 \times 10^5$  #/cm<sup>3</sup> and  $7.5 \times 10^3$  #/cm<sup>3</sup>, respectively, resulting in a coating efficiency of 83%. With coating times of 3 min, 5 min, and 10 min, the coating areal densities of fabricated CNT filters were  $4.5 \times 10^8$  #/cm<sup>2</sup>,  $7.5 \times 10^8$  #/cm<sup>2</sup>, and  $1.5 \times 10^9$  #/cm<sup>2</sup>, respectively. Fig. 5 shows an FE-SEM image of the CNT-coated filter (coating time = 3 min). The CNTs were observed to be standing vertically on each filter fiber.

Experiments were carried out using forced clean air with a face velocity of 1.5 m/s in order to determine whether CNTs could be detached from the filter. The results in Fig. 6(a) show that no CNTs were detached from any of the three filter samples. The pressure drop across each test filter media was also



Fig. 4 – CNT coating efficiency. (A color version of this figure can be viewed online.)

measured at various face velocities of the clean air. The results are summarized in Fig. 6(b), which shows that CNT deposition did not affect the pressure drop, implying that the change in filter solidity due to the addition of the CNTs was negligible. For comparison, the following theoretical prediction of pressure drop was used [43]:

$$\Delta p = \frac{64\mu t U_0 \alpha^{1.5} (1 + 56\alpha^3)}{d_f^2} \tag{9}$$

where,  $U_0$  is the face velocity, t is the filter thickness (=0.2 mm),  $\alpha$  is the solidity (=0.11), and  $d_f$  is the diameter of



Fig. 5 – FE-SEM images of the CNT-coated filter. (A color version of this figure can be viewed online.)

filter fiber (=4  $\mu m$ ). The calculations were consistent with the data from the pristine test filter.

#### 3.2. Filtration test

The size distribution of the aerosolized viral particles (bacteriophage MS2) is shown in the inset of Fig. 7. The total concentration and mode diameter were  $8.6 \times 10^6$ #/cm<sup>3</sup> and 37.2 nm, respectively. Fig. 7 shows the effect of CNT coating on filtration efficiency as a function of particle diameter  $(\eta_{\rm F}(d_n))$ . The face velocity was 0.2 m/s. The results show that the filtration efficiency was improved overall by the presence of CNTs on the glass fiber filter. The overall filtration efficiencies ( $\eta_F$ ) were 54%, 66.2%, 70%, and 78.4% for the pristine filter and CNT filters with coating areal densities of  $4.5 \times 10^8$  #/cm<sup>2</sup>,  $7.5\times10^8$  #/cm², and  $1.5\times10^9$  #/cm², respectively. Particle sizes of 120 nm and 100 nm were the most abundant penetration particle size for the pristine filter and CNT-coated filter, respectively. The fractional filtration efficiency was 11%  $(d_p = 120 \text{ nm})$  with the pristine filter, but increased to 33.3%  $(d_p = 100 \text{ nm})$  with the CNT-coated filter (coating areal density:



Fig. 7 – Filtration of viral particles. (A color version of this figure can be viewed online.)



Fig. 8 – Antiviral test results. (A color version of this figure can be viewed online.)

 $1.5 \times 10^9$  #/cm<sup>2</sup>). For the pristine filter, the fractional filtration efficiency was also determined theoretically using the following equation [22]:



Fig. 6 - Experimental results. (A color version of this figure can be viewed online.)

$$\eta_p(d_p) = 1 - \exp\left[-\frac{4\alpha t E(d_p)}{\pi d_f(1-\alpha)}\right]$$
(10)

The single fiber (fractional) filtration efficiency  $E(d_p)$  is defined as

$$E(d_p) = 1 - (1 - E_{diff}(d_p)) \times (1 - E_{int}(d_p)) \times (1 - E_{imp}(d_p))$$
(11)

where  $E_{diff}$ ,  $E_{int}$ , and  $E_{imp}$  are the filtration efficiencies due to Brownian diffusion, interception, and inertial impaction, respectively [40]. The theoretical results were in good agreement with the experimental data.

Quality factors were evaluated using Eq. (5) for various face velocities. The quality factor increased with coating areal



Fig. 9 – Viable viral count ratios before and after filtration. (A color version of this figure can be viewed online.)

density for a given face velocity, but decreased with face velocity for a given coating areal density. The best quality factor of 0.13 (44% increase compared to the pristine filter) was obtained when the face velocity was 0.05 m/s and the coating areal density was  $1.5 \times 10^9$  #/cm<sup>2</sup>.

# 3.3. Antiviral efficiency

Fig. 8 shows the results of antiviral testing. As the coating areal density increased, the PFU value decreased exponentially (decay constant =  $-0.809 \text{ cm}^2$ ). The filter had higher antiviral efficiency with increasing CNT density. The antiviral efficiency was 92% with a coating areal density of  $1.5 \times 10^9 \text{ #/ cm}^2$ . The relationship between  $-\ln(1 - \eta_A)$  and *C* is the Z value, which is the slope of the line, was 0.1944 cm<sup>2</sup>/µg.

According to Fig. 9, the viable viral count ratio in the air before and after the filtration for a pristine filter (coating areal density = 0) was same as the penetration ratio  $(1 - \eta_F)$ . However, in case of CNT coated filters, the viable viral count ratio was lower than the penetration ratio and decreased with coating areal density, implicating that the virus could be physically damaged when they passed through the CNT coated filter.

Fig. 10(a) shows TEM images of viruses sampled from the viral solution which was prepared by filtration of the viruses on the pristine filter and subsequent detachment of the viruses from the pristine filter with sonication in de-ionized water. Their shape was close to circular with a diameter of approximately 40 nm, which was consistent with the value measured using the SMPS as shown in the inset of Fig. 7. Fig. 10(b) and (c) shows TEM images of viruses captured on the CNTs. Fig. 10(b) and (c) also shows viruses that were detached from the CNTs during the sonication process. The



Fig. 10 – (a) Viruses detached from the pristine filter. (b) and (c) TEM images of CNTs and viruses captured on the CNTs. (d) Damaged viruses. (A color version of this figure can be viewed online.)

morphology of the detached viruses changed to a dumbbelllike or tore shape, clearly seen in Fig. 10(d).

In previous studies [17–20], viruses were completely removed by a depth filtration mechanism, that is, capture by nanotube bundles inside the CNT layer. Liu et al. [44] also reported that the adsorption process of virus on CNTs follows the chemical adsorption mechanism and the process may be associated with electronic sharing or electronic exchange of covalent forces in the surface between nanomaterials and virus. The removal rate of virus became higher with the dosage of nanomaterial since the total adsorption effect is boosted as the dosage increases. In this study, Fig. 10 shows that mechanical damage due to puncture and straining by CNTs can be inferred as one of virus removal mechanisms.

In this paper, we introduced a methodology that CNT air filter can be fabricated by coating aerosolized CNTs on a filter at atmospheric pressure and room temperature condition. Conventionally, wet coating by solution process has been used to deposit any functional materials to a filter, followed by a drying process with heated air flow. CNT air filter also can be fabricated by CNT growth on a filter medium via CVD process [33], where a tube furnace need to be used. However, using heated air flow or tube furnace often causes deformation of filter materials. Since our methodology does not include any solution process and high temperature treatment on the filter, possible chances of filter deformation are avoided.

In this paper, CNT air filter was fabricated in a laboratory scale. If we want to scale up the fabrication process, we need to supply higher amount of CNTs, use a nozzle with bigger diameter, and increase the number of nozzles to cover large area deposition, and so on. CNT air filter can be used in a wide range of applications such as automobile air conditioning system, secondary sterilization system, and counter-terrorism mask.

# 4. Concluding remarks

This study is the first to report the fabrication of CNT filters at atmospheric pressure and room temperature using electroaerodynamic deposition of aerosolized CNTs. CNT filters had better filtration efficiencies for aerosolized bacteriophage MS2 than medium air filters with a negligible decrease in pressure. The particle filtration efficiency was increased to 33.3% in the most penetration particle size zone (100 nm) and the antiviral efficiency of the CNT filter was 92% when the coating areal density was  $1.5 \times 10^9 \text{ #/cm}^2$ . The susceptibility constant of virus to CNTs was  $0.2 \text{ cm}^2/\mu \text{g}$ . These CNT filters will be useful for both filtration and inactivation of viral aerosols.

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# Appendix A. Supplementary data

Supplementary data associated with this article can be found, in the online version, at http://dx.doi.org/10.1016/j.carbon. 2014.04.019.

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