



# Modeling and optimization of Photocatalytic Decolorization of binary dye solution using graphite electrode modified with Graphene oxide and TiO<sub>2</sub>

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## Abstract

In this paper, the experimental design methodology was employed for modeling and optimizing the operational parameters of the photocatalytic degradation of a binary dye solution using a fixed photocatalytic compound. The compound used was modified graphite electrode (GE) with graphene oxide (GO) on which TiO<sub>2</sub> nanoparticles were immobilized. GO nanoparticle was deposited on graphite electrode (GO-GE) using electrochemical approach. TiO<sub>2</sub> nanoparticles were immobilized on GO-GE by solvent evaporation method. A binary solution containing mixture of methylene blue (MB) and acid red 14 (AR14) was chosen as dye model. The degradation intermediates were detected and analyzed using gas chromatography. Effect of different factors on the photocatalytic decolorization efficiency was investigated and optimized using response surface methodology (RSM). The obtained results indicated that the prepared TiO<sub>2</sub>-GO-CE can decolorize MB with high efficiency (93.43%) at pH 11, dye concentration of 10 mg/L and 0.04 g of immobilized TiO<sub>2</sub> on the GO fabricated plates after 120 min of photocatalytic process. It was demonstrated that by modifying GE with GO the stability of the electrode was remarkably enhanced. The ANOVA results ( $R^2 = 0.97$  and  $P$  value  $<0.0001$  for MB,  $R^2 = 0.96$  and  $P$  value  $<0.0001$  for AR14) and numerical optimization showed that it is possible to make good prediction on decoloration behavior and save time and energy with less number of experiments using design of experiments (DoE) like the RSM.

**Keywords** Modified graphite electrode · Binary dye solution · RSM optimization · Wastewater · Photocatalytic dye degradation

## Introduction

Nowadays, the pollution of groundwater resources is one of the most important global issues (1). The water streams can be contaminated by discharging of colored wastewaters from

various industries such as textile, paper, food, printing, cosmetics, pharmaceutical, etc., which causes an eco-toxic dangerous situation and threat human health by causing allergies, tumors and cancers (2, 3). Consequently, it is necessary to remove dyes from wastewaters before releasing them into water streams.

Photocatalysis technique is one of the advanced oxidation processes (AOPs) that can degrade various organic pollutants especially dyes (4–6). Semiconductors are the most interested materials as photocatalysts due to their effectiveness in UV region. In this regard, TiO<sub>2</sub> is a popular semiconductor material because of its outstanding features such as cheap price, abundance, biocompatibility, chemical stability, non-toxicity, high bandgap energy (3.2 eV for anatase) (7–9). In photocatalysis phenomenon, semiconductor produces an electron-hole pair which can migrate to the photocatalyst surface and participate in the oxidation-reduction reactions via producing free radicals (Eqs. 1–4) (10).

## Highlights

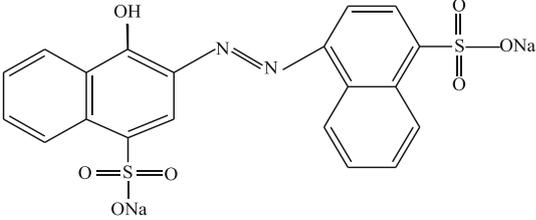
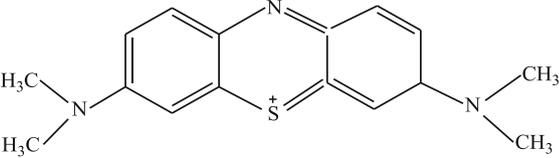
- Photocatalytic degradation of binary dye solution using TiO<sub>2</sub>-GO-GE.
- Binary solution was consist of two different dyes including AR14 and MB.
- RSM was used to examine effect of independent factors on dye removal as response.
- The degradation intermediates were detected and analyzed using gas chromatography method.
- Stability and adsorption tests were employed to enhance photocatalytic degradation of MB using GO.

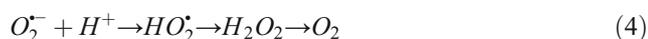
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**Table 1** Characteristics of treated dyes

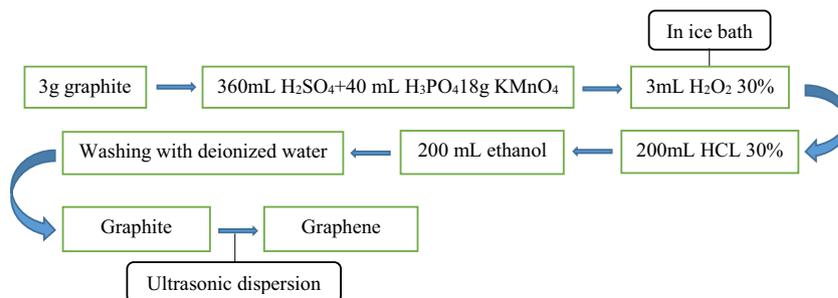
Chemical structure	Molecular formula	Color index name	$\lambda_{\max}$ (nm)	Molecular weight (g/mol)
	$C_{20}H_{12}N_2Na_2O_7S_2$	C.I. Acid Red 14 (AR14)	515	319.85
	$C_{16}H_{18}N_3SCl$	C.I. Basic Blue 9	665	502.42



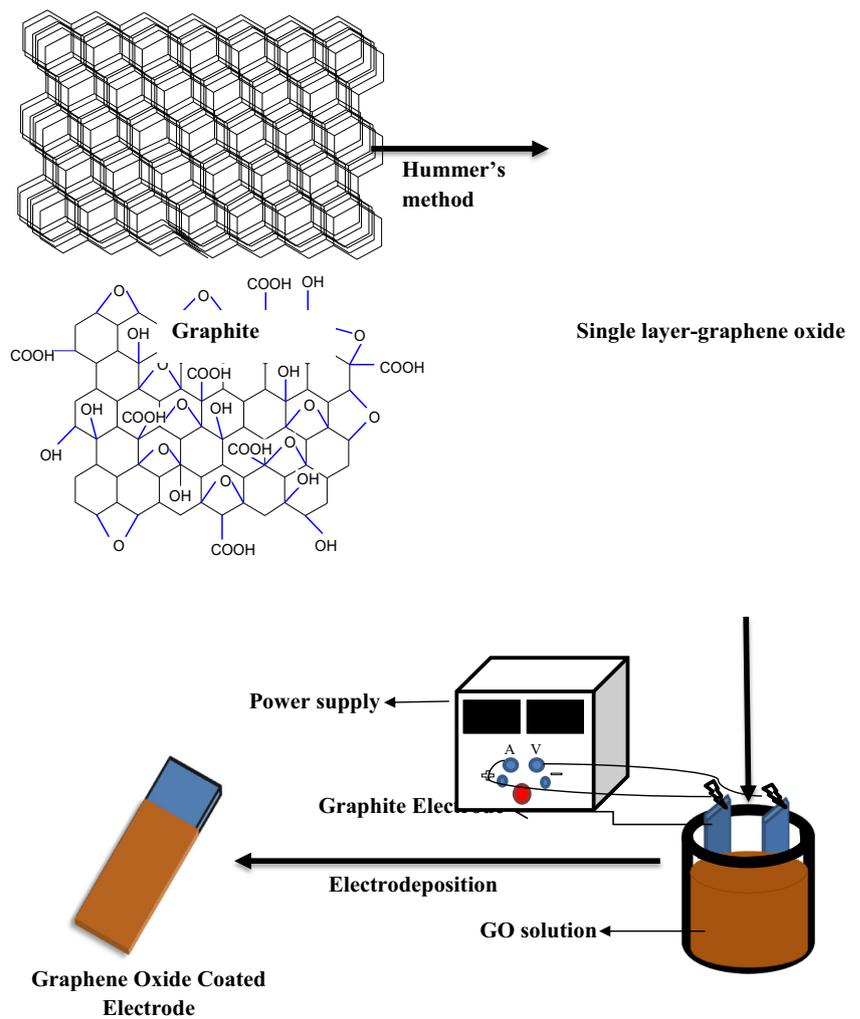
Separation and recycling of dispersed photocatalyst nanoparticles are costly, difficult and need extra time. Besides, the existence of these nanoparticles in solution may cause secondary pollution since complete recycling is impossible (11). Therefore, an efficient solution to overcome this problem is needed to immobilize the photocatalyst nanoparticles on suitable substrate by proper methods such as thermal treatment (12), membrane (13) and electro-spinning method (14).

To overcome shortcomings such as time-consuming of conventional and empirical methods RSM approach can be used. RSM is mathematical and statistical modeling approach which is used to examine the effect of independent working factors on the response and also is used to optimize the factors value with a low number of experiments to reach desirable responses (15). RSM uses a second order polynomial model to predict optimum condition to get best response (16).

A good selection of design and optimization model makes it possible to simultaneously evaluate the variables contribution (main and interaction) on photocatalytic process which in present study was obtained by experimental design (17, 18). In this study, a new and simple photocatalytic discoloration of binary system using immobilized  $TiO_2$  on graphene oxide (GO) substrate (GE-GO- $TiO_2$ ) is reported. A real colored wastewater (industrial wastewater) usually consists of the mixture of dyes along with other additives such as salts, surfactants etc. (19). Thus, the removal of the mixture of dyes from industrial wastewater is too important. Performance of photocatalytic activity depends on the number of pollutants present in the solution and their concentration (20, 21). To date, the number of literature on adsorption processes for simultaneous dye and heavy metal ions removal from water in multicomponent systems is rather limited (22). To simulate real wastewater a binary system was chosen which was consisted of two different dyes with an anionic dye (AR 14) and a cationic dye (MB). The photocatalytic effect of the immobilized composite and effects of pH, initial dye concentration and photocatalyst dosage on binary discoloration efficiency were studied and optimized using RSM. ANOVA table and

**Fig. 1** The synthesis of GO by modified Hummer's method

**Fig. 2** Fabrication of graphite electrode by GO



numerical optimization were performed to confirm validity of the model.

## Material and method

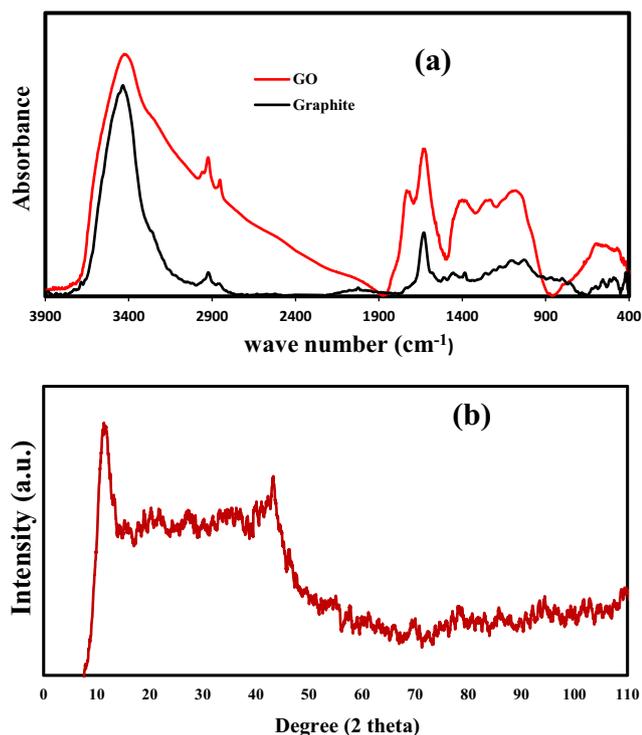
### Chemicals

Graphite powder (purity >95%, length 10–20 μm and diameter 30–50 nm) was purchased from Seraj Co. Titania

nanoparticle (Degussa P25) was used as the photocatalyst (average particle size: 30 nm, purity >97% with 80:20 anatase to rutile). A 9 watt UV lamp (Philips, 9 W (UV-c), Poland) was used as a light source and was jacketed with a Pyrex tube. The dyes were purchased from Ciba Co. and their information are shown in Table 1. The other chemicals were prepared from Merck Co.

**Table 2** Experimental Range and Levels of the Independent Variables

variables	code	ranges and levels				
		-2	-1	0	+1	+2
pH	A	3	5	7	9	11
initial dye concentration (mg/L)	B	10	20	30	40	50
TiO <sub>2</sub> concentration(g/L)	C	0.01	0.02	0.03	0.04	0.05
time(min)	D	40	50	60	70	80

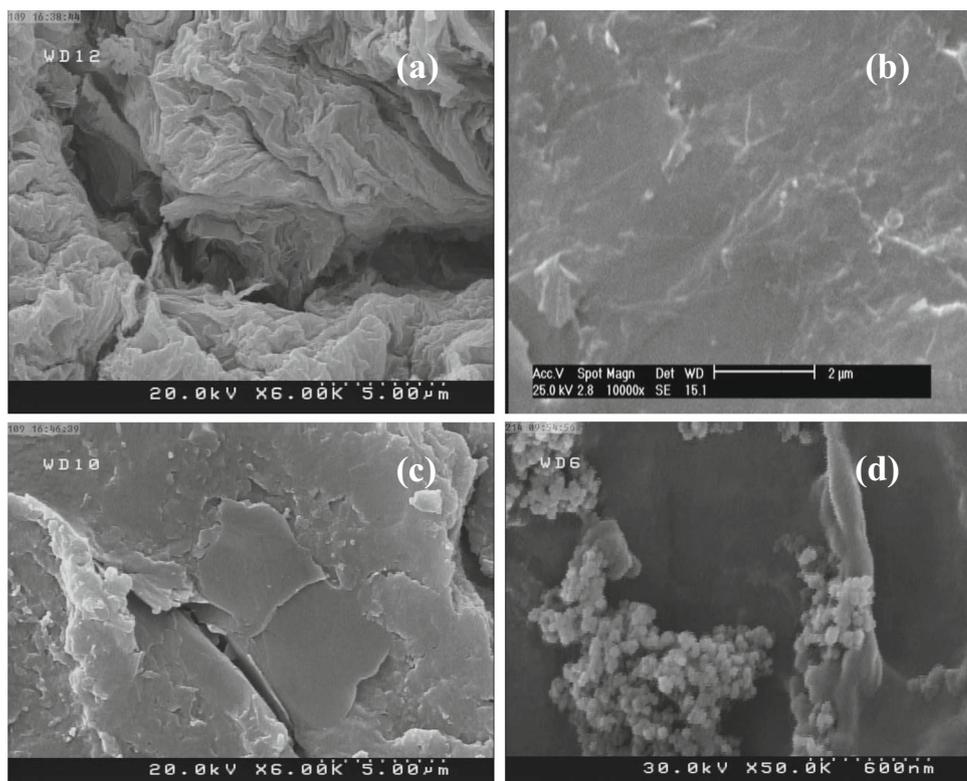


**Fig. 3** Characterization of GO: **a** FTIR, and **b** XRD

### Preparation of GO-GE-TiO<sub>2</sub>

GO was synthesized by the modified Hummer's method. The synthesis steps are schematically shown in Fig. 1. In brief,

**Fig. 4** FESEM images of GO powder (a), polished graphite electrode surface (b), GO-GE (c), and TiO<sub>2</sub>-GO-GE (d)



graphite powder (3 g) was added in a solution of H<sub>2</sub>SO<sub>4</sub> (360 mL), H<sub>3</sub>PO<sub>4</sub> (40 mL) and KMnO<sub>4</sub> (18 g). Then, H<sub>2</sub>O<sub>2</sub> (30%, 3 mL) was dispersed in the prepared solution at room temperature and filtered by a nylon filter. The solid material was washed with 200 mL HCL 30% and ethanol, respectively. The resulting solid was graphite oxide and in order to obtain graphene oxide, the solution was dispersed using ultrasonic bath for 1 h (23).

Fabrication of GO on graphite electrode (with the dimension of 3 × 50 × 110 mm<sup>3</sup>) was done with GO (0.2 g/L) and CTAB (1.3 g/L) dispersed in water using Delta D68H ultrasonic at room temperature. Direct current (DC) with the voltage of 25 V were applied by ESCORT power supply (3060 TD Dual Tracking, Taiwan) to the solution containing GO and CTAB for 20 min (Fig. 2). Dispersion with the cationic surfactant (CTAB), makes the GO sheets positively charged, which will move them toward the cathode in the deposition process.

In a typical experiment, TiO<sub>2</sub> (0.005 g) nanoparticles were dispersed in 10 mL of distilled water. The solution was placed in ultrasonic instrument to form a homogeneous mixture. Then this mixture was poured gradually on the surface of GO fabricated electrodes which had been placed in an oven at 120 °C for 1 h. It can be described that a lasting physical bonding could take place between GO-GE and TiO<sub>2</sub> nanoparticles.

**Table 3** Design of experiment suggested by CCD algorithm and final removal of blue and red dyes

Run	independent variable				dependent variable	
	A	B	C	D	AR14 removal (%)	MB Removal (%)
1	0	-2	0	0	72.78	74.02
2	0	0	0	0	55.85	32.57
3	1	-1	-1	-1	49.72	55.74
4	-1	-1	-1	-1	45.66	30.78
5	2	0	0	0	81.89	54.27
6	-1	-1	1	-1	72.02	32.33
7	0	0	2	0	61.35	45.37
8	1	-1	1	-1	60.68	67.24
9	0	0	0	-2	40.48	27.11
10	0	0	0	0	54.96	33.62
11	0	0	0	2	57.01	39.78
12	-1	1	-1	-1	50.00	17.45
13	-1	-1	1	1	79.44	41.62
14	0	2	0	0	49.79	27.32
15	0	0	-2	0	41.75	31.64
16	1	1	1	-1	51.86	27.59
17	-1	1	1	1	57.34	18.77
18	-1	-1	-1	1	54.13	40.61
19	0	0	0	0	55.23	32.45
20	0	0	0	0	56.09	34.18
21	0	0	0	0	55.12	31.89
22	1	1	1	1	59.00	36.13
23	-2	0	0	0	70.27	25.89
24	0	0	0	0	54.42	37.29
25	-1	1	1	-1	54.63	15.86
26	1	1	-1	1	56.44	29.59
27	1	1	-1	-1	47.32	29.38
28	1	-1	1	1	76.97	78.52
29	1	-1	-1	1	68.01	72.01
30	-1	1	-1	1	51.56	19.87

**Characterization techniques**

The morphology of the synthesized GO, GO-GE and TiO<sub>2</sub>-GO-GE was studied using a field emission scanning electron microscope ((FESEM) JSM-6700F, JEOL, Japan)).

The Fourier transform infrared (FTIR) spectra of all materials were recorded by a Thermo Nicolet Avatar 360 FTIR Spectrometer in the 500–4000 cm<sup>-1</sup> region with the resolution of 4 cm<sup>-1</sup>. X-ray diffraction (XRD) analysis was carried out by (Equinox 3000) X-ray diffractometer using (Cu K $\alpha$ ) X-ray source ( $\lambda = 1.5418 \text{ \AA}$ ) the operating conditions (generator voltage 40 kV and generator current 30 mA) were in the scanning range from (10° to 110°) at rate of (2°/min). Degradation products were analyzed using GC-MS (SHIMADZU QP2010 gas chromatography coupled with JEOL JMS-700 mass

**Table 4** ANOVA for MB removal Response Surface Quadratic Model

Source	df	Mean square	F-values	P value	R <sup>2</sup>
A	1	2315.949	158.4084	< 0.0001	–
B	1	4205.554	287.6554	< 0.0001	–
C	1	104.918	7.17628	0.0172	–
D	1	308.1667	21.07827	0.0004	–
AB	1	373.8422	25.57041	0.0001	–
AC	1	32.49	2.222281	0.1568	–
AD	1	8.910225	0.60945	0.4471	–
BC	1	21.20602	1.450469	0.2471	–
BD	1	66.7489	4.565554	0.0495	–
CD	1	0.714025	0.048839	0.8281	–
A <sup>2</sup>	1	40.40747	2.763828	0.1172	–
B <sup>2</sup>	1	408.9395	27.97102	< 0.0001	–
C <sup>2</sup>	1	18.44297	1.26148	0.2790	–
D <sup>2</sup>	1	5.431543	0.371512	0.5513	–
Model	14	563.9673	38.57476	< 0.0001	97%

spectrometry). The carrier gas was helium and the flow rate of elute was 2.11 ml min<sup>-1</sup>. A capillary column Terra C-18 (5 $\mu$ m  $\times$  100 mm length) was used for separation of product intermediates.

**Photocatalytic wastewater treatment**

The photocatalytic reactions were carried out in a cylindrical glass batch (CGB) with the total volume of 500 mL which was placed in a dark chamber. Two TiO<sub>2</sub>-GO-GEs were fixed at the inner wall of CGB, 8 cm away from each other and each GO-GE was contained 0.01 g TiO<sub>2</sub> nanoparticles. Aeration

**Table 5** ANOVA for AR14 removal Response Surface Quadratic Model

Source	df	Mean square	F-values	P value	R <sup>2</sup>
A	1	33.74882	4.856967	0.0436	–
B	1	645.4288	92.88701	< 0.0001	–
C	1	685.8704	98.70717	< 0.0001	–
D	1	451.1868	64.93264	< 0.0001	–
AB	1	0.5776	0.083125	0.7771	–
AC	1	76.82523	11.05632	0.0046	–
AD	1	58.8289	8.466373	0.0108	–
BC	1	182.7904	26.30632	0.0001	–
BD	1	56.02523	8.062881	0.0124	–
CD	1	0.9409	0.13541	0.7180	–
A <sup>2</sup>	1	695.4054	100.0794	< 0.0001	–
B <sup>2</sup>	1	48.99074	7.050512	0.0180	–
C <sup>2</sup>	1	33.02534	4.752849	0.0456	–
D <sup>2</sup>	1	88.72463	12.76882	0.0028	–
Model	14	226.0047	32.52552	< 0.0001	96%

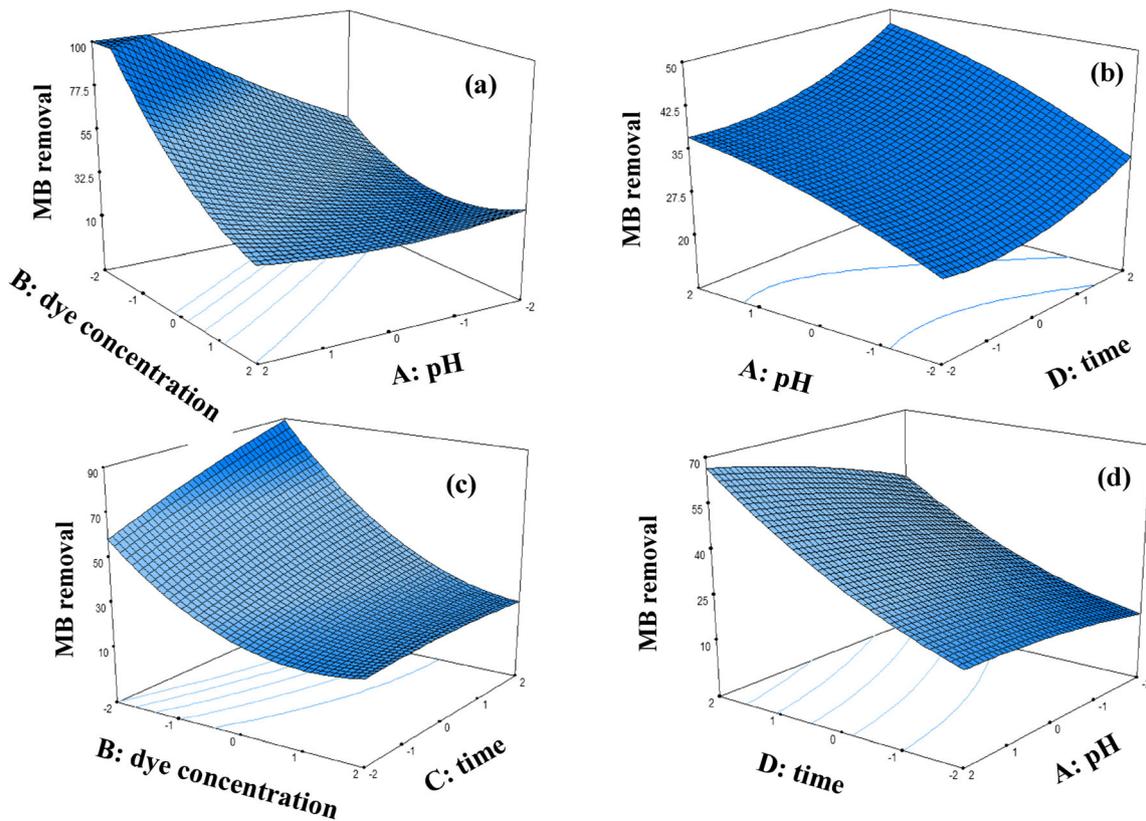


Fig. 5 3D plots for the removal of MB binary solutions

operation was exerted at the center bottom of the CGB using an air pump. The UV lamp was placed at the center top of the reactor. A starting solution containing initial dye concentrations of 10–50 mg.L<sup>-1</sup> for both blue and red dyes were fed to the reactor chamber. Samples were collected at time intervals that will be discussed later in statistical studies. The initial dye concentration for both dyes were same in the binary system. The dye concentration of the dye was evaluated using Beer-Lambert law; absorbance of the dye solution is measured at maximum wavelength and the dye concentration can be calculated by the following equation:

$$A_{\lambda_i} = \varepsilon_{\lambda_i} b C \quad (6)$$

Where,  $A_{\lambda_i}$  is the absorbance of the sample at maximum wavelength of sample,  $C$  is dye concentration in solution (mol L<sup>-1</sup>) and  $\varepsilon_{\lambda_i}$  is coefficient of molar attenuation (molar absorptivity (L mol<sup>-1</sup> cm<sup>-1</sup>)).

For binary system, absorbance of the binary sample was measured at maximum wavelengths of blue and red dye separately using UNICO 2100 spectrophotometer. The dye concentration can be calculated using two sets of linear equations (Eq. 7), each of those corresponds to absorbance at maximum wavelengths for blue and red dyes.

$$\begin{bmatrix} A_{\lambda_B} \\ A_{\lambda_R} \end{bmatrix} = \begin{bmatrix} \varepsilon_{B,\lambda_B} & \varepsilon_{R,\lambda_B} \\ \varepsilon_{B,\lambda_R} & \varepsilon_{R,\lambda_R} \end{bmatrix} \times \begin{bmatrix} C_B \\ C_R \end{bmatrix} \quad (7)$$

$$\begin{bmatrix} A'_{\lambda_B} \\ A'_{\lambda_R} \end{bmatrix} = \begin{bmatrix} \varepsilon'_{B,\lambda_B} & \varepsilon'_{R,\lambda_B} \\ \varepsilon'_{B,\lambda_R} & \varepsilon'_{R,\lambda_R} \end{bmatrix} \times \begin{bmatrix} C'_B \\ C'_R \end{bmatrix}$$

Where, B and R lowercases are representative for blue and red dyes, and two wavelengths were indicated with prime uppercase.

The initial dye concentrations are known ( $C_0$ ) and the final dye concentrations at time  $t$  ( $C_t$ ) were calculated using Eq. 7. The removal efficiency for each dye was measured by Eq. 8 (24).

$$\text{Dye removal (AR14 or MB) (\%)} = \frac{C_0 - C_t}{C_0} \times 100 \quad (8)$$

### Statistical studies

In the present study the TiO<sub>2</sub>-GO-GE was used for binary dye solution photocatalytic treatment as a simulated real wastewater in a reactor which contains two different dyes (methylene blue (MB) and acid red 14 (AR14)). Response surface methodology (RSM) was used for evaluating and optimizing the

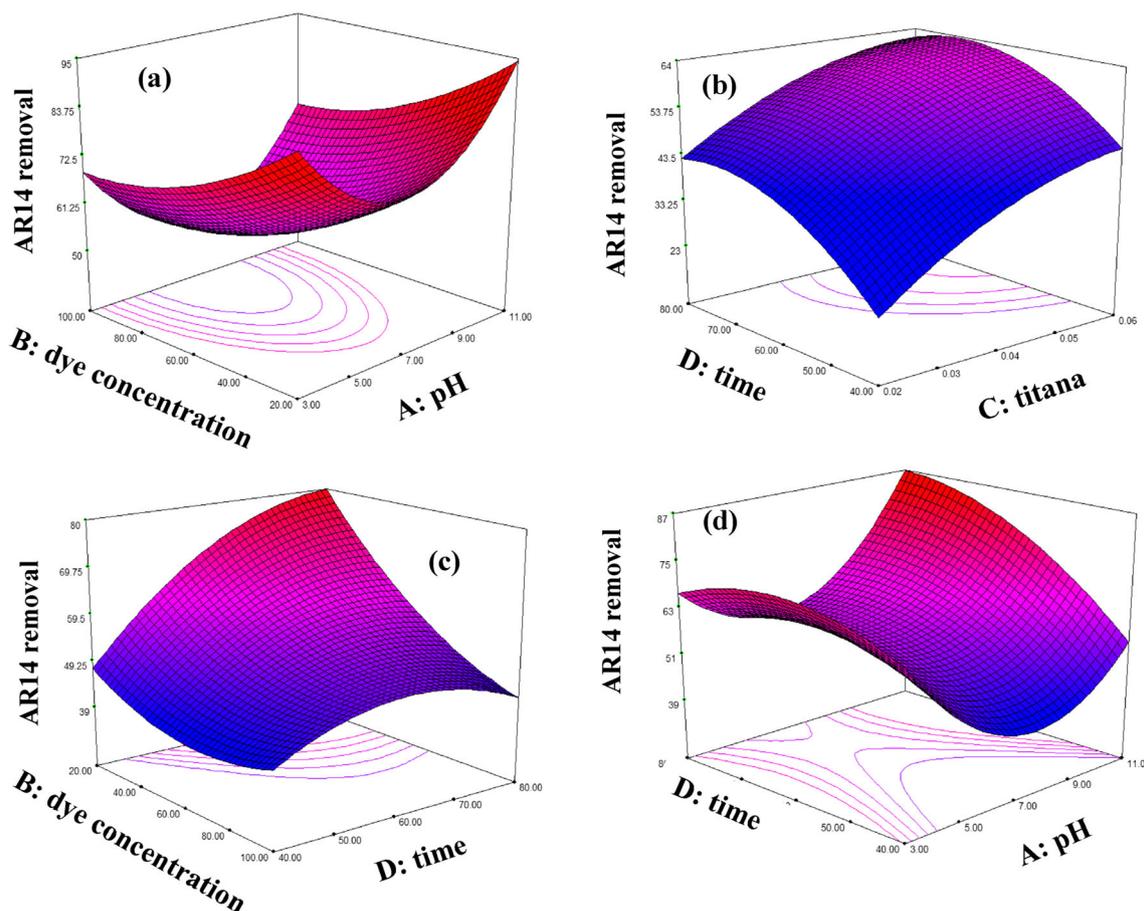


Fig. 6 3D plots for the removal of AR14 from binary solutions

photocatalytic activity of the immobilized TiO<sub>2</sub>. According to the earlier articles it has been reported that the pH of the solution, initial dye concentration, TiO<sub>2</sub> loading and reaction time were the most significant water treatment factors. In this work these parameters were taken as independent variables at five levels which are shown in Table 2. Since the final goal of the water treatment process is the extent of decoloration, the dye removals (%) were considered as dependent variables. Design Expert 7.0 software were used for experiment design and statistical analysis.

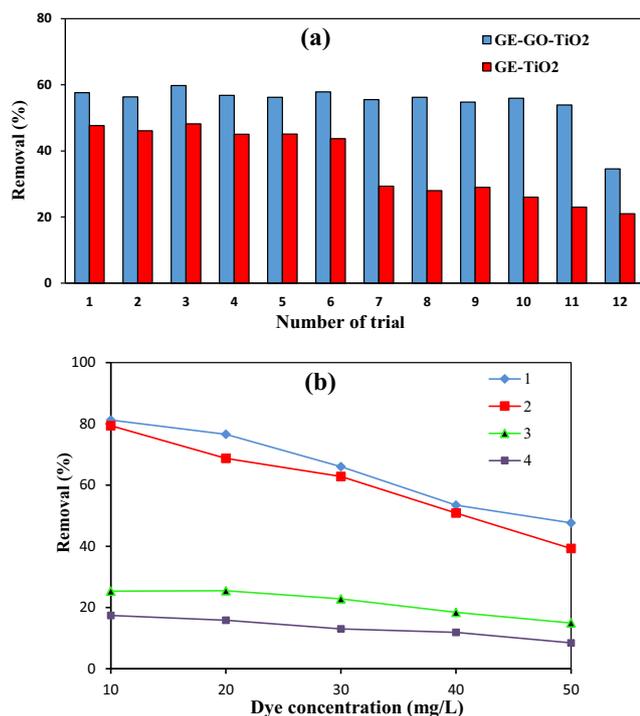
## Result and discussion

### GO, GE-GO and GE-GO-TiO<sub>2</sub> characterization

FT-IR spectra of GO and graphite is shown in Fig. 3a. The spectrum of graphite showed a main peak at 1623 cm<sup>-1</sup> and 3400 cm<sup>-1</sup> which are due to C=C and OH, respectively. In case of GO, the presence of bands at 1732 cm<sup>-1</sup> (C=O stretching), 1397 cm<sup>-1</sup> (C-OH stretching), 1223 cm<sup>-1</sup> (C-O-C (epoxy)) and 1627 cm<sup>-1</sup> (C=C stretching) clearly proved the presence of oxygenated groups which suggested synthesis of GO (25). In addition, broad peak 2400–3600 cm<sup>-1</sup> is because of

Table 6 Optimum Value for the Process Parameters

variables	optimum value	MB degradation (%)		AR14 degradation (%)	
		predictive	experimental	predictive	experimental
A	10				
B	40	85.51	86.74	83.55	82.48
C	0.03				
D	67				



**Fig. 7** **a** Effect of modification and electrode on photocatalyst stability, **b** difference between adsorption and photocatalytic performance of TiO<sub>2</sub>-GO-GE in various dye concentrations. **(1):** Photocatalytic activity of TiO<sub>2</sub>-GO-GE on AR 14 removal. **(2):** Photocatalytic activity of TiO<sub>2</sub>-GO-GE on MB removal. **(3):** Adsorption value of MB removal using TiO<sub>2</sub>-GO-GE. **(4):** Adsorption value of AR 14 removal using TiO<sub>2</sub>-GO-GE

formation of carboxylic acid (COOH) on graphite surface which cannot be seen on graphite or graphene surface.

The results of XRD test are shown in Fig. 3b. The peak existed at  $2\theta = 11.8^\circ$  (d-spacing = 7.8 Å with plane of (002) indicated formation of GO sheets (26). The peak at  $2\theta = 43.3^\circ$  may be due to the turbostratic band of the disordered carbon materials (27).

Figure 4 exhibits the morphology of GO powder (a), polished graphite electrode surface (b), GOG (c), and TiO<sub>2</sub>-GO-GE (d). The FESEM images display that the GO sheets are stacked together. Moreover, it is indicated that TiO<sub>2</sub> nanoparticles are attached to bare and modified electrode surface.

### Water treatment statistical analysis

Design Expert 7.0 suggested 30 sets of random experiments using central composite design (CCD) algorithm which are shown in Table 3. Moreover, the final dye removal for each dye as calculated using the equations given in the experimental section and a summary of them are reported in Table 3.

Two sets of second order polynomial equations by Design Expert 7.0 based on the theory of multiple

regression analysis. These models predict the final dye removal according to the experimental results (28), which are shown in Eq. 9 and 10.

$$R_{MB} = 33.67 + 9.81A - 13.23B + 2.09C + 3.59D + 1.21A^2 + 3.86B^2 + 0.82C^2 - 0.44D^2 - 4.84AB + 1.43AC + 0.74AD - 1.16BC - 2.04BD + 0.21CD \quad (9)$$

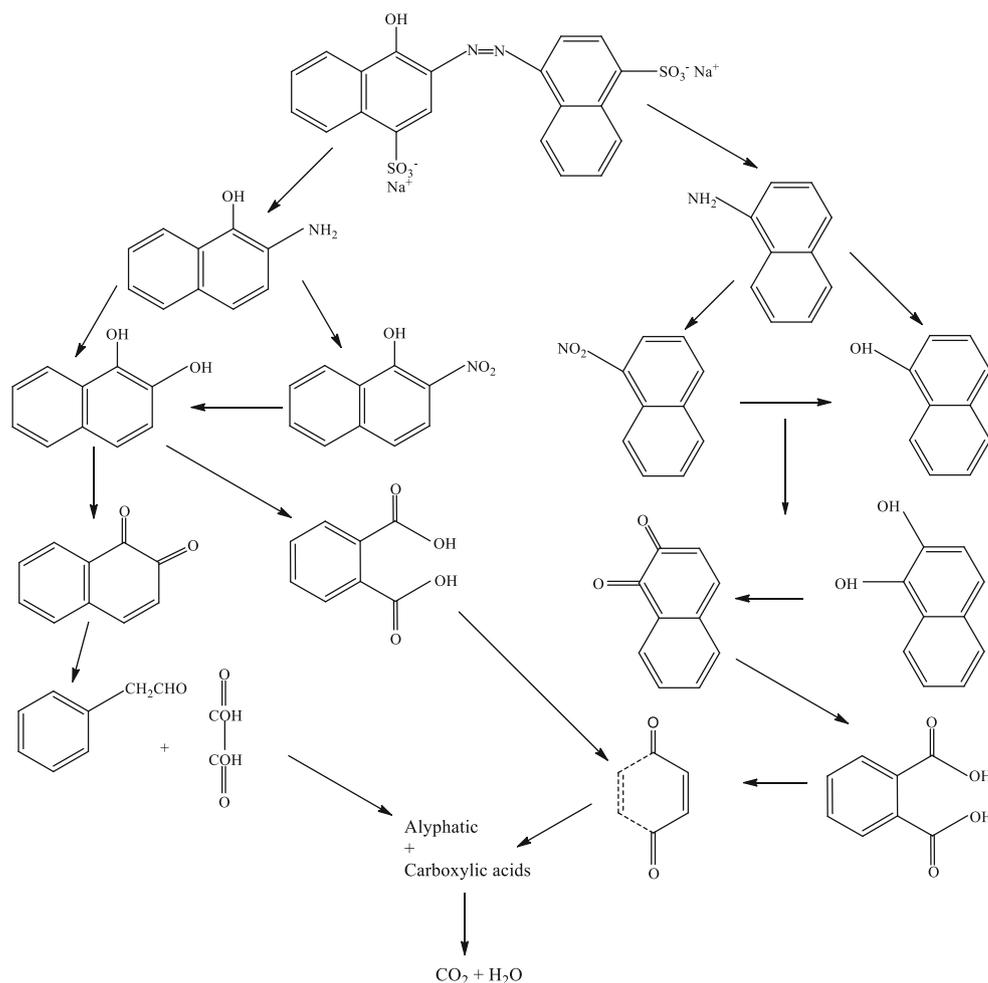
$$R_{AR14} = 55.28 + 1.18A - 5.19B + 5.35C + 4.33D + 5.04A^2 + 1.34B^2 - 1.10C^2 - 1.80D^2 - 0.19AB - 2.19AC + 1.92AD - 3.38BC - 1.87BD - 0.25CD \quad (10)$$

The analysis of variance (ANOVA) and R<sup>2</sup> (coefficient of regression) were also reported to analyze significance and adequacy of the models. According to low P values ( $P < 0.05$ ), the models can sufficiently predict the experimental data. Also, high R<sup>2</sup> values shows great fitness of proposed models with experiment results (29–31).

Regarding Tables 4 and 5 it can be seen that all corresponding factors significantly affected the photocatalytic degradation of both red and blue dyes in binary solution at 95% confidence level (31, 32).

### Effect of independent variables on dye removal

Figure 5 and 6 report the relationship between the independent variables (A, B and C) and the response (MB and AR14 removal) using the 3-D surface plots. Each plot shows simultaneous effect of two factors on dye removal while two other factors are kept constant in zero level (coded level). As shown in the Fig. 6a with increase in pH and decrease in dye concentration, dye removal (%) increase so that it is upper than 100% in level (-2) for dye concentration and level (+2) for pH. This is due to the fact that with increase in pH from 3 to 11 the amount of anionic surface charges of GO sheets increases because of the existence of OH<sup>-</sup> in the solution which results in more binding sites on the surface of GO-GE plates. As a result, cationic dye molecules will be adsorbed on GO sheets surface by electrostatic attractions. Therefore, in alkaline pH both GO sheets surface and TiO<sub>2</sub> nanoparticles are negatively charged, which cause an intense photocatalytic activity due to the adsorption of cationic dye molecules (MB) on the photocatalyst surface, which leads to efficient degradation of MB. In case of AR14 with increasing pH from 3 to 7, dye degradation efficiency decreases. But with increasing pH from 9 to 11, dye degradation increase as seen in Fig. 5a. At neutral pH, lowest adsorption of the dye on positively charged nano TiO<sub>2</sub> occurs. With increasing pH the adsorption of anionic dye molecules on the surface of the electrodes decreases. Same results are achieved in noor mohammadi et al. in 2018. They found that in pH 9 and 11 maximum MB removal is achieved due to maximum electrostatic attraction forces between the positively charged MB dye molecules and negative catalyst

**Fig. 8** Proposed degradation products of AR 14

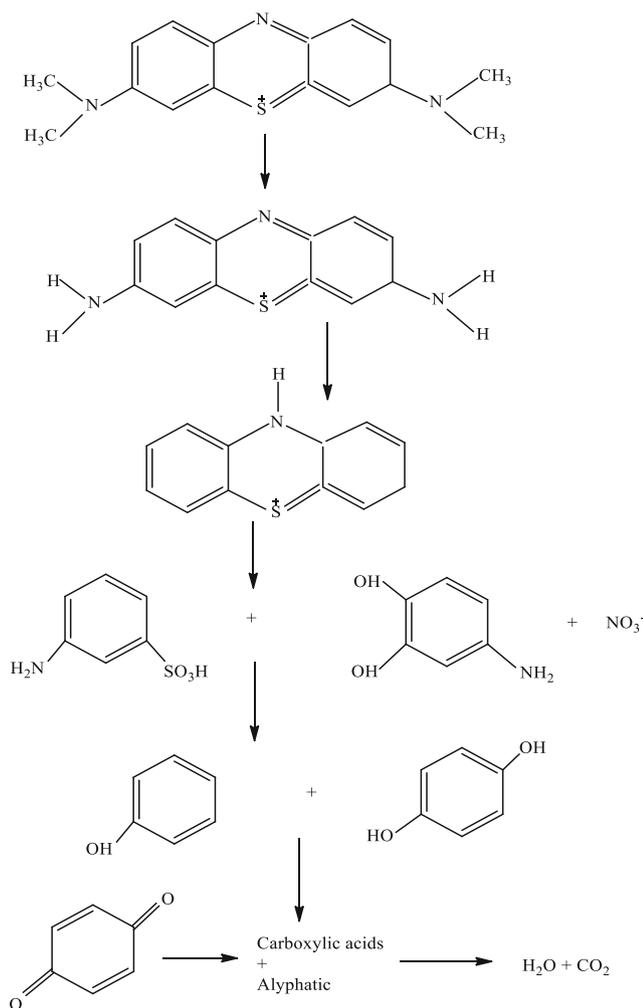
(2). However, when the pH of the dye solution is acidic the repulsion between negatively charged AR 14 and the negatively charged of the GO decreases. Therefore, adsorption of the dye on the TiO<sub>2</sub> and surface of the graphene oxide is increased and this will cause increasing the dye degradation. But at higher pH (higher than 7) increase in the removal could be due to conversion of  $OH$  to  $OH^{\bullet}$  in the presence of UV photons (33).

As seen in Fig. 5b and efficiency of MB removal increase with increase in pH. In Figs. 5d and 6d it can be seen that for all dye concentration, dye removal (%) increased by increasing the TiO<sub>2</sub> concentration. This phenomenon may be explained as follows with an increase in the semiconductor concentration, the amount of site density for the surface electrons, holes, and oxidizing species increases, which leads to the higher decolorization efficiency (34). In some cases it is reported that catalyst loading has an optimum point. For example, bansal et al. found that to reach maximum dye removal, optimum value of 1 g L<sup>-1</sup> for ZnO and 1.5 g L<sup>-1</sup> for TiO<sub>2</sub> is needed. They showed that addition of more catalyst lead to decrease in dye removal efficiency. It is because of aggregation phenomena which leads to decrease in active sites (35). In

this study, no optimum value was not observed due to no aggregation in the chosen TiO<sub>2</sub> loading range.

Figures 5c and 6c show that increasing time and dye concentration result in more dye degradation. With increase in MB and AR14 concentrations, the capability of photon access through the dye molecules to reach the catalyst surface or its vicinity decreases. But, at lower concentrations more photons strike on catalyst surface, which results in higher degradation efficiency by the generation of more hydroxyl radicals ( $OH^{\bullet}$ ) which attack the dye molecules. Ilinoiu et al. showed that by increasing dye concentration form 25 mg/L to 100 mg/L, removal percentage was decreased from 90 to 50. They inferred that this is because of two main reason. First, high concentration of the dye affects negatively the UV light penetrability in the dye solution. Second, the dye molecules may absorb a significant amount of light required for the catalyst surface irradiation, which diminishes the catalytic activity (36).

Numerical optimization (Design Expert software) was employed to determine optimal conditions for maximum MB and AR14 decolorization. This makes it possible to realize the validity of the model for good predicting of dye degradation (37). The optimum values which were



**Fig. 9** Proposed degradation of MB

suggested for desirable MB removal (84.51%) and AR14 removal (83.55%) are given in Table 6. Capability of the model for simulating of MB and AR14 removal was examined experimentally and found to be in good agreement with the proposed values ((Table 6) 86.74% for MB and 82.48% for AR14)).

### Stability of GE-TiO<sub>2</sub> and GE-GO-TiO<sub>2</sub>

In order to determine stability and reusability of immobilized GO-GE-TiO<sub>2</sub> and important role of GO, a repetitive test with working condition was carried out in binary system. The tests were performed with dye concentration of 50 mg/L, TiO<sub>2</sub> content of 0.02 g/L and pH = 7 at 120 min in presence of UV light. The results which are shown in Fig. 7a indicate that when immobilized GO-GE-TiO<sub>2</sub> used in decolorization process, the MB removals in 11 trials were almost the same. But, when synthesized GO sheets were not used in the electrode bed (GE-TiO<sub>2</sub>), the MB removals in 6 trials were almost the same but after

that the removals reduced. This results show that GO has important effect in photocatalyst system stability. It can be described that a physical bonding could occur between GO-GE and TiO<sub>2</sub> nanoparticles. In addition, high temperature in the Immobilization step of TiO<sub>2</sub> on GO-GE, may also help for a proper and lasting physical bonding and makes nanoparticles anchored properly with GO. In addition, there is an increase in MB removal when GO was used as bed in comparison with GE-TiO<sub>2</sub>. The increase in dye removal can be due to dye adsorption of dye on the GO surface. Because of the two positive points (stability and adsorption), GO can improve photocatalytic removal of dyes.

Figure 7b shows the difference between photocatalytic removal and adsorption values of dyes using TiO<sub>2</sub>-GO-GE. The experiments were performed with given conditions in above with various concentration of AR 14 and MB binary solution (10, 20, 30, 40 and 50 mg/L). The difference in removal percentage between photocatalytic and adsorption process for each dye can be indicative of degradation extent.

### Determination of the photocatalytic oxidation intermediates

Figure 8 and 9 summarize the oxidation pathway of MB and AR14 based on the detection of by-products from GC-MS analysis. Sites with a high electron density are more available for attacking by hydroxyl radicals. Dye degradation is initiated by *OH*<sup>•</sup> attack. The attack of *OH*<sup>•</sup> radical as first step of photocatalyst induced process is well established (38). As shown in Fig. 8 C-S (SO<sub>3</sub>H) and -N=N- bonds are initially broken at initiation of photocatalytic degradation. In the following, -N=N- convert to -NH<sub>2</sub> and -NO<sub>2</sub>. Among various intermediates and oxidative products, the aromatic products as naphthylamine, nitronaphthyl and naphthol compounds were commonly detected as the major oxidative products. It was found from Fig. 8 that the breakage of benzene and naphthalene ring formed some intermediates of formic acid, oxalic acid, acetic acid and carboxylic acids. The intermediates finally can be converted to H<sub>2</sub>O and CO<sub>2</sub>.

Dealkylation of dyes containing alkylamine groups is an important step to fade the color of the dyes. Demethylation of MB occurs as showed in the Fig. 9. N-C and S-C are the most active bonds of thionin molecule and are further broken down (ring opening) (39), and finally MB converts into H<sub>2</sub>O, CO<sub>2</sub>, and other inorganic molecules.

### Conclusion

In the present study, the photocatalytic discoloration of MB and AR14 dye molecules simultaneously was investigated by the immobilized TiO<sub>2</sub> nanoparticles on electrode. The

immobilized TiO<sub>2</sub> nanoparticles were used in a photocatalytic batch reactor and the important parameters including pH, initial dye concentration and TiO<sub>2</sub> dosage was studied. The plates containing photocatalyst particles were successfully used to decolorize mixture of dyes with the advantage of no further separation and recycling of the used photocatalyst nanoparticles. The stability test showed that synthesized GO has important role in stability of fixed TiO<sub>2</sub> nanoparticles. The effect of working factors on responses were examined and optimized using response surface methodology. A quadratic model and 3-dimension plots was obtained to predict relationship between independent coded variables and MB and AR14 removal (%). The results ( $R^2 = 0.97$  and  $P$  value  $<0.0001$  for MB,  $R^2 = 0.96$  and  $P$  value  $<0.0001$  for AR14) and numerical optimization suggest that the model was adequate to predict binary dye solution degradation. Numerical optimization indicate that to reach optimum removal for AR14 (90.92%) and MB (84.53%) the adequate conditions should be pH = 10, initial dye concentration = 40 mg/L and TiO<sub>2</sub> dosage = 0.03 g/L at 67 min.

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## Compliance with ethical standards

**Conflict of interest** There is not any conflict of interest in this manuscript.

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