

# Preparation of a Polypyrrole/Graphene Oxide Composite Electrode by Electrochemical Codeposition for Capacitor Deionization

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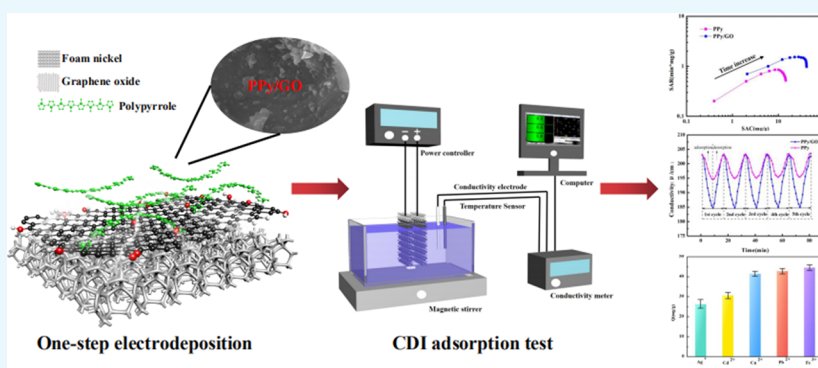


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**ABSTRACT:** In this paper, a polypyrrole/graphene oxide (PPy/GO) composite electrode, applied to the capacitive deionization process for removing heavy metal ions, was prepared by one-step electrochemical codeposition. The PPy/GO composite electrode has a dense sheet structure, and PPy is spherical and uniformly distributed on the surface of GO sheets. The experimental results show that the PPy/GO composite electrode has a higher capacitance (186.67 F/g) and a lower charge transfer resistance ( $1.626 \Omega \cdot \text{cm}^2$ ) than the PPy electrode. The adsorption capacity of the PPy/GO composite electrode is 41.51 mg/g, which is about 2.67 times (15.52 mg/g) that of the PPy electrode. After five adsorption/desorption treatments, the adsorption capacity was maintained at about 98.0%, and the regeneration rate was 94.7%. Therefore, the electrode has good cycle stability and regenerability. In addition, the adsorption capacity of different metal ions follows the order  $\text{Ag}^+ < \text{Cd}^{2+} < \text{Cu}^{2+} < \text{Pb}^{2+} < \text{Fe}^{3+}$ , indicating that the PPy/GO composite electrode has stronger adsorption capacity for the added state, and the adsorption capacity for ions with the same valence state decreases with the increase in ion hydration radius. The PPy/GO composite electrode has a good prospect for the removal of heavy metal ions in industrial wastewater.

## 1. INTRODUCTION

The increasing global demand for metals has led to a rapid expansion of the mining and metallurgical industries, where the risk of environmental pollution caused by heavy metal ion wastewater is increased.<sup>1</sup> Metallurgical wastewater containing copper, aluminum, zinc, nickel, and lead has obvious toxicity and carcinogenic effects.<sup>2,3</sup> Therefore, the removal and reuse of heavy metal wastewater have received extensive attention.

Traditional heavy metal ion wastewater treatment processes include chemical precipitation, membrane filtration, use of biological organisms (algae and fungi), adsorption, ion exchange, reverse osmosis, etc.<sup>4–9</sup> However, these technologies have some problems in the removal of heavy metal ions, for example, secondary pollution, short service life, high operating costs, and poor cyclability.<sup>10–12</sup>

Capacitive deionization (CDI) technology has become a promising technology for the treatment of heavy metal wastewater due to its low operating cost, environmental friendliness, and high ion recovery rate.<sup>13–15</sup> The CDI

technique applies a voltage between the electrodes, and the anions/cations in the solution are adsorbed on the anode/cathode, respectively. When the electrode is saturated, the ions are released into the solution by electrode reversal, electrode shorting, or breaking voltage, and electrodes and ions were regenerated.<sup>16,17</sup>

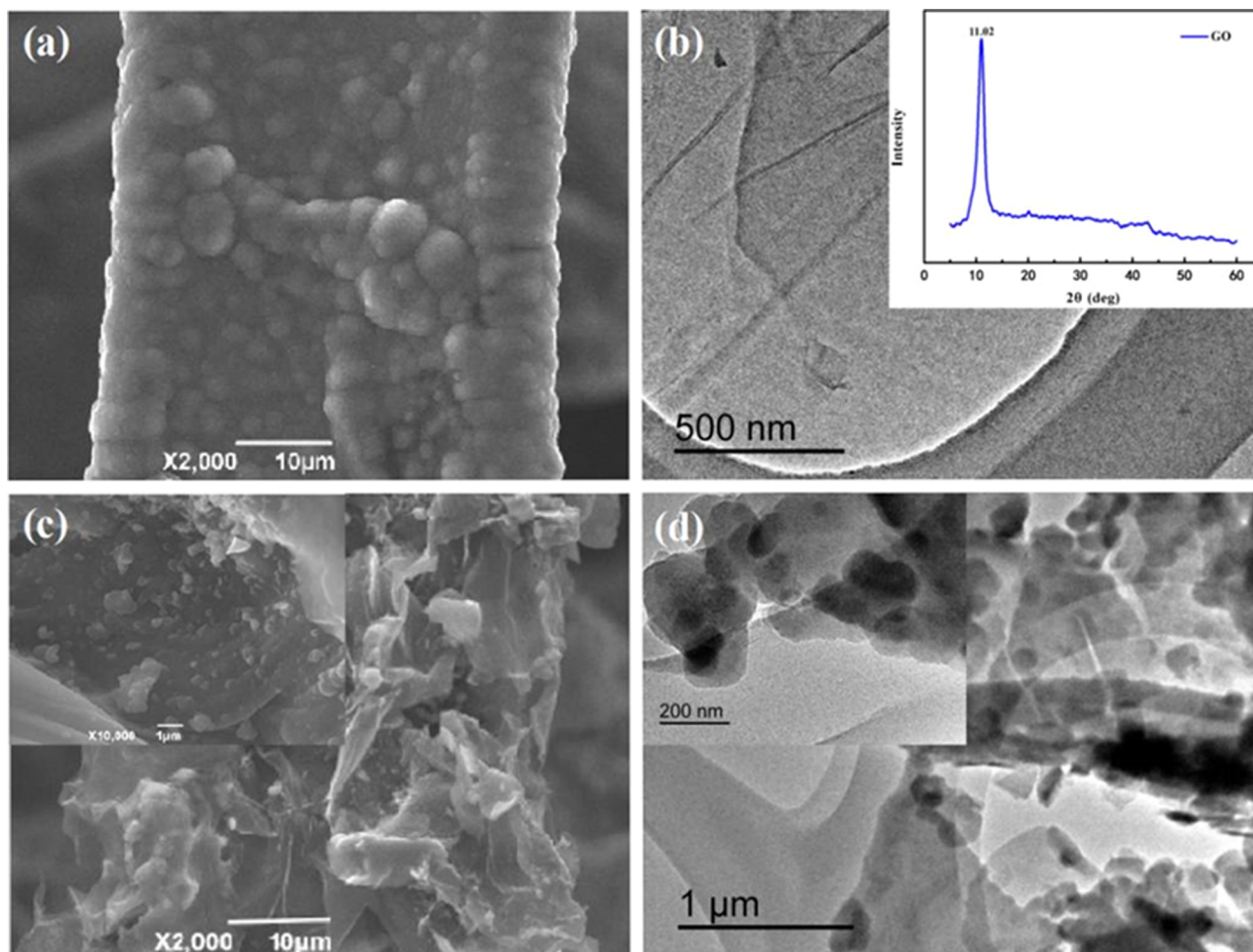
The ion adsorption performances of the electrode, decided by the prepared process, are the core of the CDI technology. At present, the preparation of composite electrode materials with carbon materials, metal oxide materials, and conductive polymer materials has become a research hotspot.<sup>15,18–21</sup> As a

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**Figure 1.** (a, c) SEM images of PPy and PPy/GO composites. (b, d) TEM images of GO and PPy/GO composites.

typical conductive polymer, polypyrrole (PPy) has the advantages of high specific capacitance, low cost, and good chemical stability.<sup>22–24</sup> It has been reported that polypyrrole can be used to adsorb heavy metals such as  $\text{Ag}^+$ ,  $\text{Cd}^{2+}$ ,  $\text{Pb}^{2+}$ ,  $\text{Cu}^{2+}$ ,  $\text{Cr}^{6+}$ , etc.<sup>25–28</sup>

To further improve the CDI performances of the PPy electrode, carbon-based material graphene oxide (GO) was selected for the composite. GO has the advantages of good mechanical toughness, good mechanical properties, and good thermal stability and chemical stability.<sup>29,30</sup> Moreover, GO can effectively disperse the PPy formed and limit the aggregation of PPy.<sup>31</sup> Zhang et al.<sup>32–35</sup> have used graphene to prepare a variety of composite materials for capacitive deionization, which have good deionization performance, stability, and regeneration performance. The synergistic effect of GO and PPy can improve the conductivity of the electrode material and make the electrode material have more adsorption sites.

At present, the forming process of the conductive polymer composite electrode is generally through the forming method of the high-pressure pressing composite material and the coating method using adhesive and conductive agents.<sup>36,37</sup> The PPy/CS/CNT composite nanoelectrode with good adsorption performances has been prepared by the compression method by our working group.<sup>38</sup> However, this forming method will narrow the ion channel of the electrode, resulting in high resistance of charge transfer.<sup>39</sup> Moreover, the electrode easily deforms in the solution due to the die forming, which will have

a negative impact on the adsorption performance of the electrode. As a kind of forming process, electrodeposition is green and simple, which can form a uniform and compact film. The variable electrode substrate shape and low cost provide the possibility of expanding the scale. The CNT electrode prepared by the deposition process has a specific capacitance of 33.36 F/g and an adsorption capacity of 23.93 mg/g, which are 1.62 times and 1.85 times that of the coated electrode, respectively.<sup>40</sup> Electrochemical deposition has a good prospect in the field of CDI electrode material preparation.

In this paper, one-step electrochemical codeposition of PPy/GO composites was carried out on a foamed nickel substrate by the potentiostatic method. Pure PPy was prepared by the same method as a comparison. The composites were characterized by scanning electron microscopy (SEM), transmission electron microscopy (TEM), X-ray photoelectron spectroscopy (XPS), and Fourier transform infrared spectroscopy (FTIR). The electrochemical behavior of the prepared electrode was investigated by cyclic voltammetry (CV) and electrochemical impedance spectroscopy (EIS). The adsorption performance of the PPy/GO composite electrode was tested and analyzed by electroadsorption experiments.

## 2. RESULTS AND DISCUSSION

### 2.1. Morphology Analysis of PPy/GO Composites.

The SEM image of the pure PPy electrode is shown in Figure 1a. Pure PPy is spherical and has a rough surface, and dense films

are formed on the surface of the nickel foam. Figure 1b shows the TEM image of the prepared GO from which the flake morphology of GO can be clearly seen. Moreover, it can be seen from the XRD pattern of GO that there is an obvious peak at  $11.02^\circ$ , which is a typical diffraction peak of GO,<sup>41</sup> indicating that graphite is completely oxidized and GO has been successfully prepared under experimental conditions. Figure 1c shows the SEM image of PPy/GO. It can be seen that after adding GO, the surface of the nickel foam has changed obviously. PPy was spherical and evenly distributed in GO sheets. This result is consistent with the TEM image observation of PPy/GO in Figure 1d. It can be speculated that the interconnection of GO sheets can help the diffusion of ions to the active center of electrode materials.

The nitrogen adsorption/desorption isotherm of the PPy/GO composite electrode is shown in Figure 2. The PPy/GO

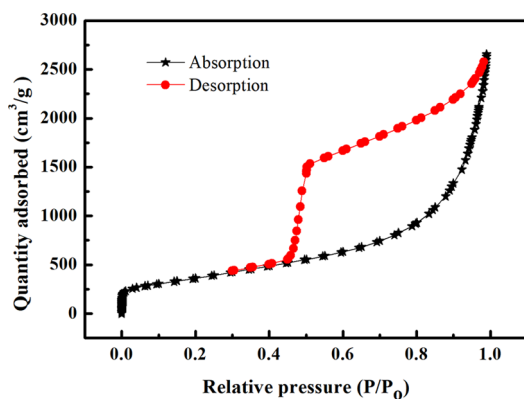


Figure 2. Nitrogen adsorption/desorption isotherms of PPy/GO composite electrodes.

composite electrode has a type IV isotherm and an H3-type hysteresis ring, indicating that the PPy/GO composite electrode exhibited mesoporous adsorption.<sup>42</sup> According to the adsorption/desorption isotherm, it can be seen that the PPy/GO composite electrode has a large specific surface area of  $1325.4 \text{ m}^2/\text{g}$ . The total pore volume of the PPy/GO composite electrode was  $4.10 \text{ m}^3/\text{g}$ , and the average pore diameter was  $12.39 \text{ nm}$ . It can be seen from the adsorption curve that it started as monolayer adsorption and then became multimolecular layer adsorption. It can be seen from the desorption curve that the mesopore diameter distribution of the composite is uniform. The addition of GO greatly improved the specific surface area of the composite electrode and enhanced the adsorption performance of the composite electrode.

**2.2. FTIR Analysis and XPS Analysis.** Figure 3a shows the FTIR spectrum of the PPy/GO composite electrode. It can be seen from the FTIR spectrum that the peak values of PPy/GO at  $1170$ ,  $1460$ , and  $1538 \text{ cm}^{-1}$  are related to the tensile vibration and aggregation of C–H, C=C, and CN in PPy, respectively.<sup>43</sup> The new peak of PPy/GO at  $1040 \text{ cm}^{-1}$  is caused by the C–O stretching vibration at  $1058 \text{ cm}^{-1}$  in GO. The peak of PPy/GO at  $3430 \text{ cm}^{-1}$  is significantly enhanced compared to the peak at  $3421 \text{ cm}^{-1}$  in GO due to the stretching vibration of H–N and O–H. In the FTIR spectrum of GO, the stretching vibration peak of the O–H bond at  $1400 \text{ cm}^{-1}$  and the stretching vibration peak of the C–OH bond at  $1247 \text{ cm}^{-1}$  indicate that the surface of the prepared GO carries more oxygen-containing functional groups.<sup>44</sup> Compared with

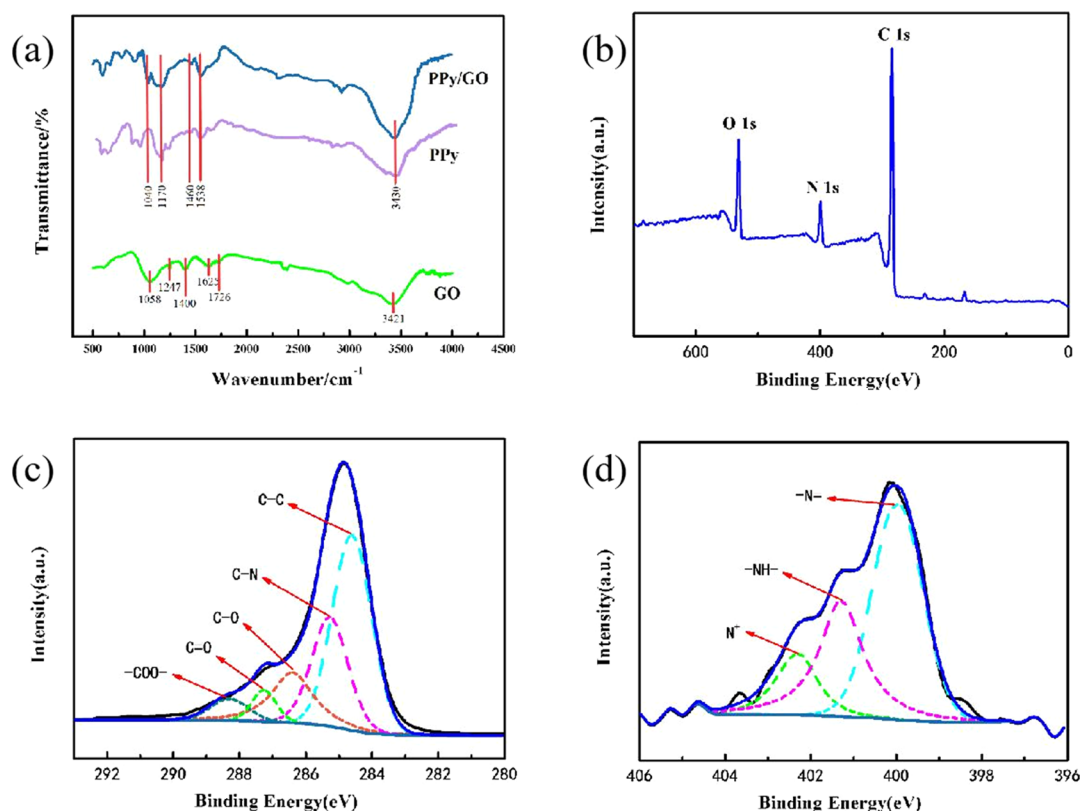
the infrared spectra of GO and PPy, the peak positions of C–N, C–H, and H–N of PPy/GO move toward high or low wavenumbers, indicating the formation of PPy/GO.

Figure 3b–d shows the XPS measurement spectrum and the C 1s and N 1s spectra of the PPy/GO composite, respectively. XPS measurement spectra of PPy/GO composites indicate the presence of O, N, and C elements in the composite. The C 1s spectrum of PPy/GO has five peaks: the peaks at  $284.6$  and  $285.3 \text{ eV}$  are attributed to the combination of C–C and C–N in the PPy framework, and the peaks at  $286.6$ ,  $287.3$ , and  $288.3 \text{ eV}$  are attributed to the C–O in GO, C=O, and –COO–, respectively.<sup>45</sup> The composite material contains many oxygen-containing functional groups and can ionize the –COO– and –O– groups, which can improve the adsorption of the composite material. It is consistent with the FTIR analysis results of PPy/GO. Figure 3d shows the N 1s spectrum of the PPy/GO composite. The peak at  $402.2 \text{ eV}$  is attributed to the positive nitrogen ( $\text{N}^+$ ) doped with PPy, while the characteristic peak at  $400.4 \text{ eV}$  is attributed to –NH–, and the characteristic peak at  $399.9 \text{ eV}$  is attributed to –N=.<sup>46,47</sup> The doping level of PPy can be estimated by the ratio of  $\text{N}^+$  to total nitrogen content ( $\text{N}_{\text{total}}$ ).<sup>48</sup> The  $\text{N}^+/\text{N}_{\text{total}}$  value of PPy/GO is  $0.39$ , and the  $\text{N}^+/\text{N}_{\text{total}}$  value of pure PPy is  $0.46$ . This is due to the formation of hydrogen bonds between –NH– and –COOH in GO during the polymerization of pyrrole.

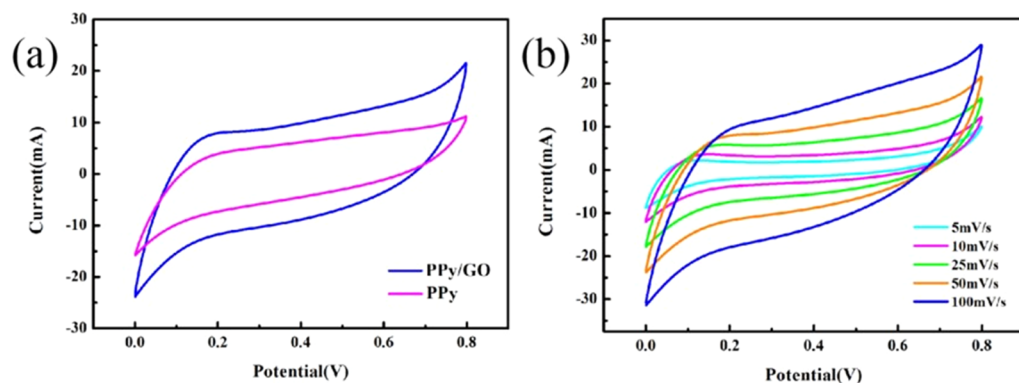
**2.3. Electrochemical Properties of PPy/GO Composites.** CV curves of PPy and PPy/GO electrodes in  $1.0 \text{ mol/L}$   $\text{CuSO}_4$  solution are shown in Figure 4. It can be seen from Figure 4a that the shape of the CV curve is rectangle-like with good symmetry, indicating that the composite material has good capacitance performance. The specific capacitance of the PPy/GO composite, calculated by eq 1, is  $186.67 \text{ F/g}$ , which is higher than that of PPy ( $104.45 \text{ F/g}$ ). This can be explained by the fact that when the GO layer is intercalated in PPy, the loose structure of the composite material creates conditions for ion transport storage and improves the electrochemical performance of PPy. The slope of the PPy/GO composite CV curve is larger than the PPy slope, which indicates that the PPy/GO composite has a larger ion diffusion velocity and a smaller resistance.

It can be seen from Figure 4b that the specific capacitance value of the PPy/GO composite material is reduced from  $186.67 \text{ F/g}$  at  $5 \text{ mV/s}$  to  $60.33 \text{ F/g}$  at  $100 \text{ mV/s}$ . This is because the increase in the scanning rate leads to an increase in the ion diffusion rate in the electrolyte, some of the ions cannot effectively make contact with the adsorbed sites, the amount of actively adsorbed ions on the composite electrode is decreased, and the specific capacitance of the final composite electrode is reduced.

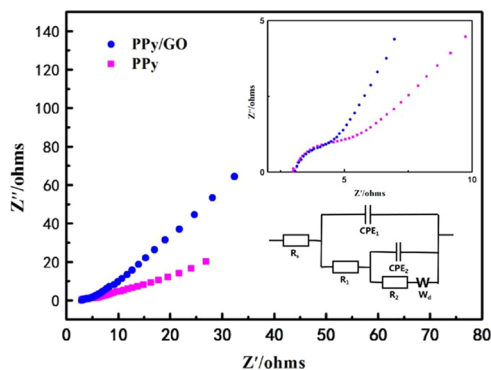
The Nyquist curves of the PPy/GO composite electrode are shown in Figure 5. As shown in Figure 5, the PPy and PPy/GO electrodes have similar Nyquist curves, forming a semicircle in the high-frequency region, and the semicircle diameter represents the charge-transfer resistance ( $R_{\text{ct}}$ ).<sup>49</sup> In the low-frequency region, they are lines close to  $45^\circ$ , and the slope of the PPy/GO electrode is slightly larger than the slope of the PPy electrode, indicating that the PPy/GO composite electrode is more favorable for ion diffusion. By fitting the equivalent circuit, the fitting results are given in Table 1. The charge-transfer resistance values of PPy and PPy/GO materials are  $3.441$  and  $1.626 \Omega\cdot\text{cm}^2$ , respectively, indicating that the PPy/GO material has a lower charge-transfer resistance. The CPE value of the PPy/GO material is  $3.783 \times 10^{-3} \text{ mF}$ , which



**Figure 3.** (a) FTIR spectra of the prepared pristine GO, PPy, and PPy/GO composites. (b) XPS survey spectrum and (c) C 1s and (d) N 1s XPS spectra of the PPy/GO composite.



**Figure 4.** (a) CV curves of PPy and PPy/GO electrodes at a scanning rate of 50 mV/s. (b) CV curves of the PPy/GO electrode at different scanning rates vs SCE in 1.0 mol/L.



**Figure 5.** EIS spectrum and equivalent circuit diagram of PPy and PPy/GO electrodes.

is larger than that of PPy by an order of magnitude. Therefore, the PPy/GO electrode has better CDI performance than that of the PPy electrode.

**2.4. Adsorption Performances.** **2.4.1. Initial Concentration.** Figure 6 shows the effect of initial concentration of Cu<sup>2+</sup> solution on the adsorption capacity and adsorption efficiency of the PPy/GO composite electrode. It can be seen from the figure that as the initial concentration of the solution increases, the adsorption capacity of the PPy/GO composite electrode increases, and the adsorption efficiency decreases. This is because the adsorbed sites of the electrode material are constant, and when the amount of Cu<sup>2+</sup> is larger than the number of adsorbed sites of the electrode material, the adsorption efficiency is decreased.

Table 1. Fitting Parameters of Equivalent Circuit<sup>a</sup>

electrode	$R_s$ ( $\Omega\cdot\text{cm}^2$ )	$R_1$ ( $\Omega\cdot\text{cm}^2$ )	$R_2$ ( $\Omega\cdot\text{cm}^2$ )	$\text{CPE}_1$ (mF)	$\text{CPE}_2$ (mF)	$W_d$ ( $\Omega\cdot\text{cm}^2$ )	errors (%)
PPy	0.6117	3.441	0.9217	$5.066 \times 10^{-4}$	$2.766 \times 10^{-3}$	0.0932	6.135
PPy/GO	0.3104	1.626	0.9449	$3.783 \times 10^{-3}$	$3.641 \times 10^{-3}$	0.0850	4.519

<sup>a</sup> $R_s$  is the solution resistance,  $R_1$  is the charge-transfer resistance of the electrode material,  $\text{CPE}_1$  is the specific capacitance value of the electrode material,  $R_2$  is the charge-transfer resistance of the nickel foam,  $\text{CPE}_2$  is the specific capacitance value of foamed nickel, and  $W_d$  is for the diffusion resistor.

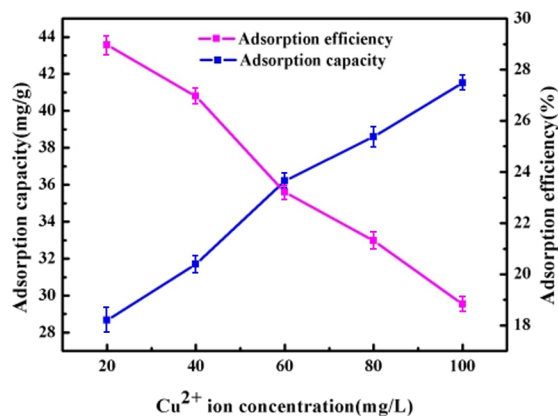


Figure 6. Effect of  $\text{Cu}^{2+}$  concentration on adsorption capacity and adsorption efficiency of the PPy/GO composite electrode.

**2.4.2. Working Voltage.** When the initial concentration of  $\text{Cu}^{2+}$  was 80 mg/L, the effect of voltage on the adsorption amount of PPy/GO composite electrode was investigated. Figure 7 shows the saturation adsorption of  $\text{Cu}^{2+}$  on the PPy/

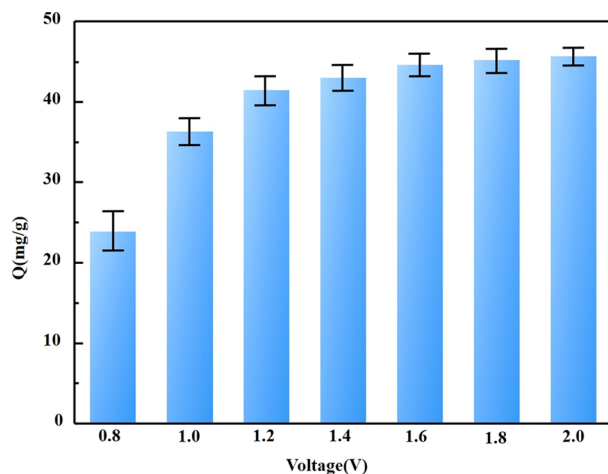


Figure 7.  $\text{Cu}^{2+}$  adsorption capacity of the PPy/GO composite electrode at different voltages.

GO composite electrode at different voltages. As the voltage gradually increases, the adsorption capacity of the PPy/GO composite electrode increases. When the voltage reaches 1.6 V, the adsorption amount of the PPy/GO composite electrode is no longer obvious. With the increase in voltage, the migration rate of ions in the electric field increases, and more ions diffuse onto the surface and into the electrode. Therefore, the adsorption capacity of the electrode increases with the increase in voltage.

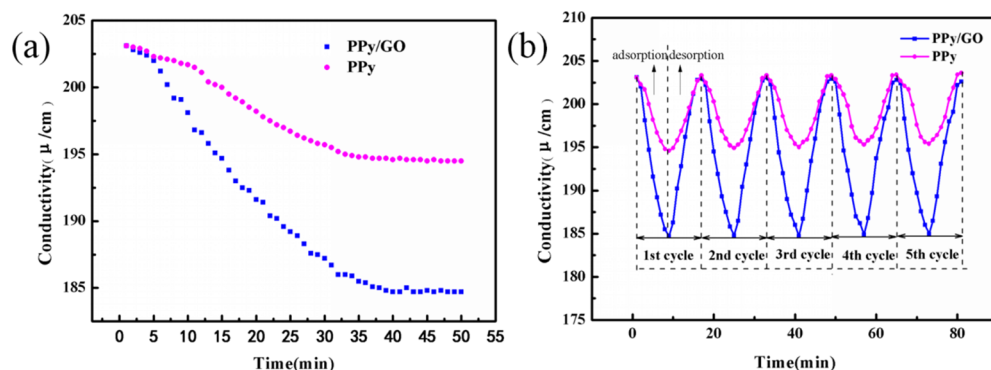
**2.4.3. Cycle Adsorption Process.** Figure 8a shows the saturation adsorption curves of PPy and PPy/GO composite electrodes at a voltage of 1.2 V and an initial concentration of

100 mg/L  $\text{Cu}^{2+}$ . It was found that the conductivity of the solution showed a rapid decrease at the beginning of the adsorption. The solution conductivity of the PPy/GO composite electrode decreased more significantly than that of the PPy electrode. The PPy/GO composite electrode reaches adsorption saturation after adsorption for about 40 min. The saturated adsorption capacity of the PPy/GO composite electrode, calculated by eq 2, is 41.51 mg/g, which is about 2.67 times (15.52 mg/g) that of the PPy electrode. It can be explained by the fact that the addition of GO increases the diffusion of ions into the material, thereby increasing the adsorption properties of the composite and functional groups and improving the adsorption performance of the electrode.

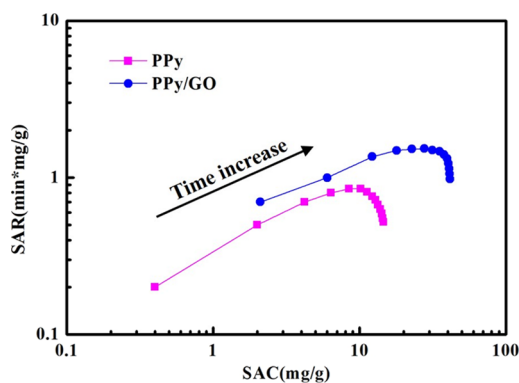
To further investigate the cycle performance of the PPy/GO composite electrode, multiple adsorption/desorption cycles were performed. As can be seen from Figure 8b, the adsorption capacity of the composite electrode decreased from 41.51 to 40.67 mg/g during five cycles, and this means that the adsorption capacity only decreased by about 2.0% during five cycles, which indicated that the electrode prepared by one-step deposition has better adsorption stability than that prepared by molding.<sup>50</sup> Compared with some reported materials for  $\text{Cu}^{2+}$  electrosorption, PPy/GO composites have good adsorption capacity and cycle performance in terms of adsorption. Moreover, in the preparation of electrodes, the one-step electrodeposition method avoids the use of binders, and the preparation process is also simpler.<sup>51–53</sup>

The relationship between the salt adsorption capacity (SAC) and salt adsorption rate (SAR) of PPy and PPy/GO composite electrodes was investigated. Figure 9 shows the Ragone diagram of PPy and PPy/GO composite electrodes at a voltage of 1.2 V and a concentration of 100 mg/L  $\text{Cu}^{2+}$ . The results show that the Ragone curve of the PPy/GO composite electrode is at the upper right, which indicates that the PPy/GO composite electrode has higher SAR and SAC compared to PPy. This is because of it having a higher specific surface area and more adsorption sites, which make ions be transported and adsorbed quickly.

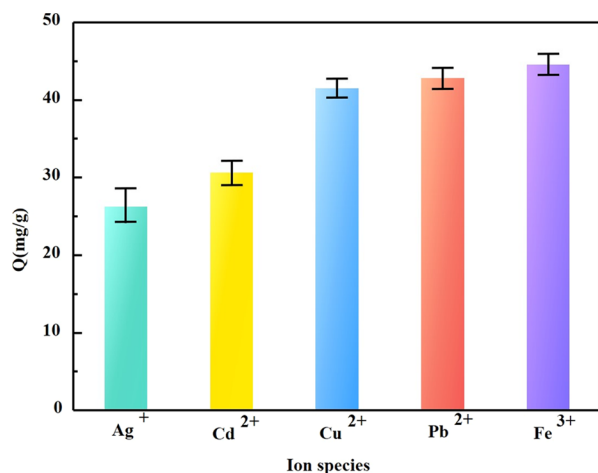
**2.4.4. Metal Ions.** Figure 10 shows the adsorption performance of five metal ions ( $\text{Ag}^+$ ,  $\text{Cu}^{2+}$ ,  $\text{Pb}^{2+}$ ,  $\text{Cd}^{2+}$ , and  $\text{Fe}^{3+}$ ) on the PPy/GO composite electrode, which was investigated at conditions of 1.2 V working voltage, 100 mg/L initial concentration, and 50 min adsorption time. Also, the adsorption capacity of the composite electrode for different ions and the hydration radii of ions are listed in Table 2. From these data, it can be seen that the adsorption capacity of the PPy/GO composite electrode for the five ions follows the order  $\text{Ag}^+ < \text{Cd}^{2+} < \text{Cu}^{2+} < \text{Pb}^{2+} < \text{Fe}^{3+}$ , which means that the higher the valence state is, the larger the adsorption capacity. It can be seen that the adsorption amount of the composite electrode with the same valence state decreases with the increase in the ion hydration radius, indicating that the ion hydration radius also affects the adsorption capacity of the electrode. Also, for the ions with the same valence state, the



**Figure 8.** (a) Saturated adsorption curves of PPy and PPy/GO composite electrodes; (b) five cycles of adsorption/desorption curves of PPy and PPy/GO composite electrodes.



**Figure 9.** Ragone plots of SAR and SAC of PPy and PPy/GO composite electrodes.



**Figure 10.** Adsorption of different ions by the PPy/GO composite electrode.

**Table 2.** Adsorption of Different Ions by the PPy/GO Composite Electrode

ions	Ag <sup>+</sup>	Cd <sup>2+</sup>	Cu <sup>2+</sup>	Pb <sup>2+</sup>	Fe <sup>3+</sup>
adsorption capacity (mg/g)	26.26	30.59	41.51	42.82	44.57
hydration radius (nm)	3.41	4.26	4.19	4.01	4.28

order of adsorption capacity of the composite electrode is  $\text{Cd}^{2+} < \text{Cu}^{2+} < \text{Pb}^{2+}$ , and that for the hydration radius is  $\text{Cd}^{2+} > \text{Cu}^{2+} > \text{Pb}^{2+}$ . It can be said that the smaller the ion hydration radius is, the higher the adsorption capacity obtained, which can be

explained by the transfer resistance. Thus, both the valence state and hydration radius have an impact on the adsorption capacity of the CDI process.

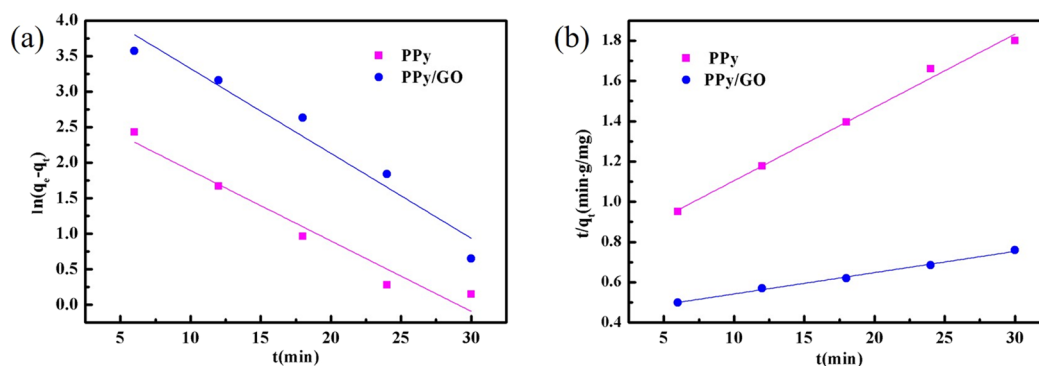
**2.4.5. Adsorption Kinetics Analysis.** To study the adsorption behavior of the PPy/GO composite electrode on metal ions, the Lagergren equation was used to calculate the first-order and second-order linearity of electrode adsorption. Figure 11 shows that the data for the adsorption of  $\text{Cu}^{2+}$  on PPy and PPy/GO composite electrodes were fitted by the Lagergren first-order equation and Lagergren second-order equation models. The fitting parameters are listed in Table 3. It can be seen from the value of  $R^2$  that the adsorption process of PPy and PPy/GO composite electrodes is fitted by the Lagergren second-order equation model, and the correlation coefficient is close to 1. The results indicate that the adsorption process of  $\text{Cu}^{2+}$  on PPy and PPy/GO composite electrodes is chemisorption, and the Faraday tantalum capacitor plays a major role in the adsorption process on the PPy/GO composite electrode.

### 3. CONCLUSIONS

In this paper, PPy/GO composites were successfully prepared by one-step electrochemical codeposition and used as the cathode of CDI. The experimental results show that the PPy/GO composite electrode has a higher capacitance (186.67 F/g) and a lower charge-transfer resistance ( $1.626 \Omega \cdot \text{cm}^2$ ) than the PPy electrode. The adsorption capacity of the PPy/GO composite electrode is 41.51 mg/g. After five adsorption/desorption treatments, the adsorption capacity was maintained at about 98.0%, and the regeneration rate was 94.7%. Therefore, the electrode has good cycle stability and regenerability. In addition, the adsorption capacity of different metal ions follows the order  $\text{Ag}^+ < \text{Cd}^{2+} < \text{Cu}^{2+} < \text{Pb}^{2+} < \text{Fe}^{3+}$ , indicating that the PPy/GO composite electrode has stronger adsorption capacity for the added state, and the adsorption amount of the same valence state decreases with the increase in the ion hydration radius. Therefore, the PPy/GO composite electrode is a promising CDI high-performance material.

### 4. EXPERIMENTAL PROCEDURES

**4.1. Materials.** Pyrrole (Py, chemically pure, Shanghai Kefeng Industrial Co., Ltd.), sodium dodecyl benzene sulfonate (SDBS, analytical grade, Tianjin Fuyu Fine Chemical Co., Ltd.), absolute ethanol (analytical grade, Tianjin Fuyu Fine Chemical Co., Ltd.), natural graphite (spectral pure, Shanghai Kefeng Industrial Co., Ltd.), concentrated sulfuric



**Figure 11.** Kinetics fitting curve of PPy and PPy/GO composite electrodes: (a) Lagergren first-order equation and (b) Lagergren second-order equation.

**Table 3.** Kinetics of Adsorption of  $\text{Cu}^{2+}$  on PPy and PPy/GO Composite Electrodes<sup>a</sup>

adsorption equation	material	fitting straight line	$R^2$
Lagergren first-order equation $\ln(q_e - q_t) = \ln q_e - k_1 t$	PPy	$y = 2.883 - 0.0992x$	0.9599
	PPy/ GO	$y = 4.518 - 0.1193x$	0.9545
Lagergren second-order equation $t/q_t = 1/(k_2 \times q_e^2) + t/q_e$	PPy	$y = 0.7410 + 0.3640t$	0.9932
	PPy/ GO	$y = 0.4365 + 0.0106t$	0.9961

<sup>a</sup> $q_e$  is the amount of adsorbed ions at equilibrium, mg/g;  $q_t$  is the amount of adsorbed ions at time  $t$ , mg/g;  $k_1$  is the first adsorption rate constant,  $\text{min}^{-1}$ ; and  $k_2$  is the secondary adsorption rate constant, g/(mg·min).

acid ( $\text{H}_2\text{SO}_4$ , analytical grade, Tianjin Fuyu Fine Chemical Co., Ltd.), sodium nitrate ( $\text{NaNO}_3$ , analytical grade, Guangdong Guanghua Technology Co., Ltd.), potassium permanganate ( $\text{KMnO}_4$ , analytical grade, Tianjin Fuyu Fine Chemical Co., Ltd.), hydrogen peroxide ( $\text{H}_2\text{O}_2$ , 30%, analytical grade, Tianjin Fuyu Fine Chemical Co., Ltd.), copper sulfate ( $\text{CuSO}_4$ , analytical grade, Tianjin Fuyu Fine Chemical Co., Ltd.), and deionized water (conductivity  $\leq 2 \mu\text{S}/\text{cm}$ , laboratory preparation) were used.

**4.2. Instruments.** A conductivity meter (DDSJ-308A, Shanghai Yidian Scientific Instrument Co., Ltd.), an electronic analytical balance (CP224S, ACCULAB, Germany), an electrochemical workstation (PARSTAT 4000, AMETEK, USA), a vacuum drying oven (DZ-2 BC type, Tianjin Taisite Instrument Co., Ltd.), a scanning electron microscope (JSM-6700F, JEOL Ltd.), a transmission electron microscope (JSM-2100, JEOL Ltd.), a Fourier transform infrared spectrometer (Magna-IR 550 type, Shimadzu Corporation, Japan), and an X-ray photoelectron spectrometer (ESCALAB 250Xi, Thermo Fisher Scientific, Inc.) were used.

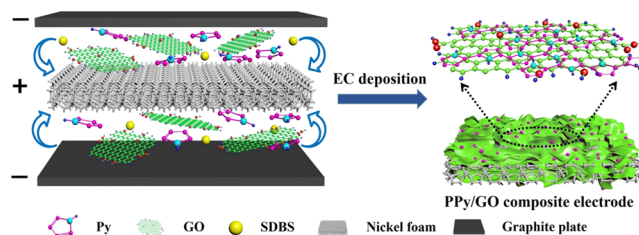
**4.3. Preparation of Graphene Oxide.** Graphene oxide was prepared by the modified Hummers method where  $\text{NaNO}_3$  (3 g), graphite (3 g), and concentrated  $\text{H}_2\text{SO}_4$  (100 mL) were placed in a 500 mL round-bottom flask, and the reaction was continuously stirred in an ice water bath for 30 min.  $\text{KMnO}_4$  (9 g) was slowly added to the flask with vigorous stirring. The ice bath was then removed, the mixture was stirred at  $35^\circ\text{C}$  for 1 h, and then double distilled water (100 mL) was added. The temperature of the mixed solution was kept below  $90^\circ\text{C}$ ,  $\text{H}_2\text{O}_2$  (80 mL) was added until no bubbles were generated in the flask, and the reaction was completed. The color of the reaction product gradually changed from dark brown to bright yellow, and a mixed solution was obtained.

The mixed solution was separated by centrifugation, the centrifugation time was 4 min, the rotation speed was 7000 rpm, and after solid–liquid separation, a small amount of deionized water was added and the obtained product was added to a dialysis bag (pretreatment of dialysis bag: the dialysis bag is processed into a 20 cm length unit, heated in hot water for 10 min, and cooled for standby). The upper and lower seals were sealed, and then the bag was placed in a water bath filled with deionized water for dialysis and examined using a pH meter. When  $\text{pH} = 7$ , the dialysis was completed. The dialyzed graphene oxide was added to an appropriate amount of deionized water and freeze-dried to prepare 1 g/L graphene oxide dispersion. Finally, the prepared GO was subjected to X-ray diffraction (XRD) analysis.

**4.4. Electrodeposition of PPy and PPy/GO on a Nickel Foam (NF).** An NF ( $1.5 \text{ mm}$ ,  $30 \times 50 \text{ mm}^2$ ) was soaked in acetone for 10 min before use, washed with deionized water, then soaked in absolute ethanol for 20 min, then soaked in hydrochloric acid, then thoroughly cleaned with deionized water, and then dried at  $60^\circ\text{C}$  for 1 h. An electrochemical cell was assembled using the NF as the working electrode and a graphite plate as the counter electrode.

The GO dispersion (1 g/L) was mixed with pyrrole (0.1 mol/L), and SDBS (1 mol/L) was added as an anionic dopant. The mixture was then sonicated for 1 h at room temperature. The composite material was electrodeposited on the NF for 25 min at 3.5 V by a potentiostatic method (Figure 12). A pure PPy electrode was prepared while maintaining other preparation conditions. The obtained sample was washed with deionized water and dried at  $60^\circ\text{C}$  for 1 h.

**4.5. PPy/GO Composite Characterization.** The morphology of the PPy/GO composite electrode was characterized by scanning electron microscopy (SEM) and transmission electron microscopy (TEM). The functional groups of the composites were analyzed by Fourier transform infrared spectroscopy (FTIR) and X-ray photoelectron spectroscopy



**Figure 12.** Preparation flow chart of the PPy/GO composite material.

(XPS). The electrochemical performances of the composite electrode were tested by cyclic voltammetry (CV) and electrochemical impedance spectroscopy (EIS). For the CV and EIS methods, the electrochemical cell configuration uses a three-electrode system with a PPy/GO composite electrode as the working electrode, a Pt electrode as the counter electrode, a saturated calomel electrode (SCE) as the reference electrode, and 1 mol/L CuSO<sub>4</sub> solution as the electrolyte solution.

The specific capacitance value of the PPy/GO composite electrode is calculated by eq 1

$$C = \frac{1}{m \times \nu \times (V_2 - V_1)} \int_{V_1}^{V_2} I \, dV \quad (1)$$

where  $C$  is the capacitance value of the composite nano-electrode, F/g;  $m$  is the mass of the composite nano-electrode, g;  $\nu$  is the scanning rate, mV/s;  $V_1$  is the lower limit of the scanning potential, V;  $V_2$  is the upper limit of the scanning potential, V; and  $I$  is the current value on the cyclic voltammetry curve, A.

**4.6. CDI Process.** The PPy/GO composite electrode was used as the cathode, and the PPy electrode was used as the anode. The adsorption performance of the PPy/GO composite electrode was tested in a Cu<sup>2+</sup> solution with initial concentrations of 20, 40, 60, 80, and 100 mg/L. Figure 13

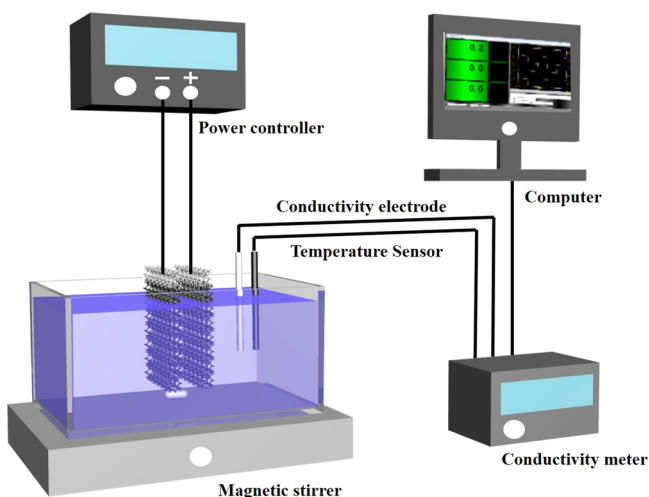


Figure 13. Schematic diagram of the adsorption experiment device.

shows the experimental flow chart. Here, the operating voltage is set to 1.2 V, provided by the power controller. The conductivity of the Cu<sup>2+</sup> solution was monitored and collected in real time during the experiment to characterize the change in solution concentration. To determine the linear relationship between concentration and conductivity, different concentrations of the solution to be tested are configured with Cu<sup>2+</sup> standard solution, and then the conductivity value of the solution to be tested is determined. Finally, the concentration–conductivity relationship is plotted based on the measured data. The curve is shown in Table 4.

The capacity for electrode adsorption is calculated by eq 2.

$$Q = \frac{(C_0 - C_1)V}{m} \quad (2)$$

where  $Q$  is the electrode adsorption capacity, mg/g;  $C_0$  is the initial concentration of solution, mg/L;  $C_1$  is the solution

Table 4. Different Ion Concentration–Conductivity Curves<sup>a</sup>

species	curve	R <sup>2</sup>
Cu <sup>2+</sup>	$y = 0.5414x - 9.9073$	0.9994
Pb <sup>2+</sup>	$y = 1.0829x - 9.4815$	0.9947
Cd <sup>2+</sup>	$y = 0.6702x - 7.1321$	0.9992
Ag <sup>+</sup>	$y = 0.5247x - 5.7204$	0.9991
Fe <sup>3+</sup>	$y = 0.4129x - 12.7221$	0.9995

<sup>a</sup> $x$  is the solution conductivity value,  $\mu\text{S}/\text{cm}$ ; and  $y$  is the solution ion concentration value, mg/L.

equilibrium concentration, mg/L;  $V$  is the volume of solution, L; and  $m$  is the mass of composite electrodes, g.

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### Notes

The authors declare no competing financial interest.

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