

Article

# Investigating the Influence of Infrared Drying Method on Linden (*Tilia platyphyllos Scop.*) Leaves: Kinetics, Color, Projected Area, Modeling, Total Phenolic, and Flavonoid Content

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Abstract: The Linden (*Tilia platyphyllos Scop.*) is a highly popular herbal plant due to its central nervous system properties. In this study, thin layer drying kinetics of linden leave samples were experimentally investigated in an infrared (IR) dryer. In order to select the appropriate model for predicting the drying kinetics of linden leaves, eleven thin layer semi theoretical, theoretical, and empirical models, widely used in describing the drying behavior of agricultural products, were fitted to the experimental data. Moreover, the color, projected area (PA), total phenolic content (TPC), and total flavonoid content (TFC) were investigated. The results showed that the drying time decreased from 50 min to 20 min. with increased IR temperature from 50–70 °C. Therewithal, the Midilli model gave the most suitable data for 50 °C, 60 °C. Moreover, Verma et al. and Diffusion approximation models showed good results for 70 °C. The lightness and greenness of the dried linden leaves were significantly changed compared with fresh samples. The PA of dried sample decreased similar to the drying time. In addition, the drying temperature effect on the effective diffusion diffusivity ( $D_{eff}$ ) and activation energy ( $E_a$ ) were also computed. The  $D_{eff}$  ranges from  $4.13 \times 10^{-12}$  to  $5.89 \times 10^{-12}$  and  $E_a$  coefficient was 16.339 kJ/mol. Considering these results, the Midilli et al. model is above the 50 °C, 60 °C, and the Verma et al. and Diffusion to 70 °C, for explaining the drying behavior of linden leaves under IR drying. Moreover, it can be said that the Page model can be used, if it is desired, to express the drying behaviors, partially with the help of a simple equation material by drying. TPC and TFC values were statistically < 0.001 higher in dried samples compared to fresh samples; however, no change has been recorded of TPC and TFC values at different temperatures (50 °C, 60 °C, 70 °C).

**Keywords:** linden leaves; infrared drying; color parameters; projected area; modeling; effective moisture diffusivity; activation energy; total phenolic content; total flavonoid content

# 1. Introduction

The usage of herbal medicinal products and supplements has increased tremendously over the past three decades. This is especially due to their health benefits (as a result of their peculiar chemical composition) [1,2]. Therefore, due to the increasing commercial importance of these products, determination of their drying properties is necessary for preservation and storage in longer periods [3]. From this point of view, Linden (*Tilia platyphyllos Scop.*) is highly popular as a herbal plant because of its central nervous system properties; Linden (Tiliaceae) consists of 44 species [4]. It is also consumed as tea, and known for its tranquilizing and analgesic effects [5]. In addition, fresh herbs (such as linden, thyme, mint etc.) are a splendid source of phenolic components (as flavonoids, phenolic, and others) [6]. Moreover, linden has been considered as diaphoretic although it has not been supported by scientific



evidence yet [7]. Moreover, the linden belongs to woody plants that shed their leaves in winter, and their leaves, are rich in a glycoside called Tiliacin, and manganese in ash. Primarily in Turkey, there are only three species in the natural environment: *Tilia tomentosa Moench, Tilia platyphyllos Scop., and Tilia rubra DC* [8].

The most common way used technology can guarantee food safety and develop its quality is through thermal processing. It has not only been successfully applied to food products due to reduction of moisture content to desirable levels, but it also leads to safe storage over a long period [9,10]. In general, conventional drying methods require much time and energy during drying of the products [11–13]. It is also reported that some structural properties of the products may be damaged with traditional drying methods, such excessive shrinkage, discoloration, loss of nutrients [14], and severe deterioration of nutritional and sensorial belongings [15].

For this reason, there is a reasonable need to introduce new drying methods to accomplish these problems. Infrared (IR) processing is one of them. To reduce the water content [16], the IR radiation had been implemented in food processing, reducing energy consumption and time spent in the process, securing and ensuring the quality of food stuffs processed [17,18]. That IR is predominantly responsible for the heating effect of the sun is a part of the electromagnetic spectrum [19]. Only if IR is used to heat—or dry—wet products (the radiation penetrates inside the material) does it become heat. The penetration deepness of radiation relies on the properties of the material and wavelength of radiation 3]. In addition, the surface of dried material emits IR radiation without heating the surrounding air. No medium heating is needed between the IR energy source and the material being dried [20]. IR is often more convenient for thin material layers having a large surface subject to radiation. There are some studies, related to the IR drying process, reported in the literature on mint [3], pepper [20], onion slices [21], strawberry [22], kiwifruit slices, [23].

It is widely known that the drying process occurs simultaneously by different mechanisms due to the complexity of food [20]. Owing to the fact that the ability to guess the IR drying system performance, modeling of the IR heating of food products is a crucial approach in the drying industry [19].

When a detailed literature search is carried out, there is no work found on the application of IR drying on Linden leaves as a thin layer. This is a topic of pivotal importance in the literature about drying linden. The objective of the study was (1) to have an observation on the impact of drying temperature, (2) to specify the color changes and projected area changes of linden leaves, (3) to find the best convenient drying model during IR drying of linden leaves together with the effective moisture diffusion coefficients and activation energies, and (4) to find the temperature effects on total phenolic content (TPC) and total flavonoid content (TFC) of the linden leaves.

#### 2. Materials and Methods

# 2.1. Materials

Linden leaves (T. platyphyllos Scop.) were harvested from the Samsun city coastline, Black Sea region, located in the north part of Turkey, particularly from the campus area of Ondokuz Mayıs University under open-air conditions. This leaf is considered one of the popular varieties in Samsun province. Its flowers have 5 petals around the flower; it is fragrant, and pale, greenish-yellow. The flower has plenty of stamens and an ovary, grouped in corymbose corymbs inflorescences, in which peduncle is partially connected to a membranous, lanceolate bract of approximately 8 cm long, rounded at the apex [7]. After the leaves collection, the samples were stored at 4 °C before drying and analysis. The destroyed and dark leaves were picked manually; only healthy structures and appearance samples were carefully selected and put into the infrared dryer as a thin layer (5 g).

#### 2.2. Experimental Drying Device

MA.R IR dryer and moisture analyzer (Radwag balances and scales, Warsaw, Poland) transmitting electromagnetic radiation in the range medium to shortwave IR (radiator) was used as drying equipment

(Figure 1). The drying temperature was fixed in keyboard of the equipment as 50, 60, 70 °C in each experiment. In the IR drying process, the sample was distributed uniformly over the entire pan in order to prevent the reflection of the IR radiation back from the not covered area by the sample. During drying, the amount of evaporating water was designated in about 3-min intervals in each drying temperature. Trials were replicated three times and average weight loss was reported.



**Figure 1.** MA.R infrared (IR) dryer and moisture analyzer. 1. Drying chamber base insert. 2. Drying pan shield. 3. Drying pan handle. 4. Cross-shaped holder. 5. Disposable pan.

#### 2.3. Color Measurements

Leaves of linden color (fresh and dried samples) were measured using the pixel method in the ImageJ program. ImageJ, developed by the National Institutes of Health (NIH), is a Java-based, readily available, open source platform, independent, and public domain software (Bethesda, Maryland USA) [24]. Before and after the drying process, this technique can be used due to being available and being free of charge to be accepted for indexed journals. The software can measure many parameters of the image analysis including the color differences, projected and surface area of leafy plants, such as linden leaves. The program uses a Lab stack to measure linden leaves. Figure 2 illustrates the flowchart using ImageJ to measure the color changing [25]. Moreover, the images were taken with the Huawei P20 16 MP camera before and after the drying process in the experiment.

$$C = (a^2 + b^2)^{1/2}$$
(1)

$$h^{o} = \tan^{-1} (b/a) \tag{2}$$

According to Diziki, D., et al. [28], total color difference ( $\Delta E$ ) was determined as follows:

$$\Delta E = [(L - L_o)^2 + (a - a_o)^2 + (b - b_o)^2]^{1/2}$$
(3)

where L<sub>o</sub>, a<sub>o</sub> and b<sub>o</sub> indicate the brightness, redness, and yellowness of dried samples, respectively.



**Figure 2.** Flowchart of the ImageJ using to obtain color parameter (L\*, a\*, and b\*). Descriptive variables (L\* a\* and b\*) related to color were achieved with the ImageJ software. L\* variant shows the degree of lightness to darkness, a\* value indicates the degree of redness (+) to greenness (-), and b\* value is the degree of yellowness (+) to blueness (-) [26]. The color value of L\* have shown the brightness and it ranges from 0 to 100. The color coordinates a\* and b\* variants do not have a particular reading range. The average values of color parameters and standard errors were calculated (L\*, a\*, b\*, C, and H) [27].

# 2.4. Image Analysis to Projected Area

Image analysis can be easily applied to measure the changes of area, perimeter, and equilibrium diameter of food [29]. The determination of the projected area (PA) of thin layer linden leaves was measured using the pixel method in the ImageJ program. This method was held at two-dimensional axes (x and y) with reference to the pixel colors. The program uses a threshold-based pixel count measurement and converts their digital units (pixels) into Reference object (REF) units (cm) to calculate the leaves area [30]. Figure 3 illustrates the flowchart using the ImageJ to measure the projected area [25,26]. Nevertheless, the images were taken with the Huawei P20 16 MP camera before and after drying the process in the experiment.



Figure 3. Flowchart of the ImageJ using to measure the projected area.

Mathematical modeling of thin-layer drying is currently the widest accepted method for investigation and optimization of dehydration characteristics in the drying process. The most frequently used moisture ratio equations were taken into account for determining the most suitable model in the thin-layer drying of Linden leaves (Table 1).

	Model Name	Model Equation	References
1	Newton	$MR = \exp(-kt)$	[31]
2	Page	$MR = \exp(-kt^n)$	[32]
3	Henderson and Pabis	$MR = a \exp(-kt)$	[31]
4	Logarithmic	$MR = a \exp(-kt) + b$	[33]
5	Midilli et al.	$MR = a \exp(-kt^n) + bt$	[34]
6	Wang and Singh	$MR = 1 + at + bt^2$	[35]
7	Logistic	$MR = b/(1 + a\exp(kt))$	[36]
8	Two term	$MR = a \exp(-kt) + b \exp(-k_1 t)$	[36]
9	Verma et al.	$MR = a \exp(-kt) + (1-a) \exp(-bt)$	[37]
10	Two term exponential	$MR = a \exp(-kt) + (1-a) \exp(-kat)$	[38]
11	Diffusion approximation	$MR = a \exp(-kt) + (1-a) \exp(-kbt)$	[39]

Table 1. Mathematical models applied to the drying curves in the study.

*MR*: moisture ratio; *k* and *k*<sub>1</sub>: drying coefficients; *n*: exponent; *t*: time in min; *a* and *b*: coefficients.

The equilibrium moisture content (*Me*) was reputed to be zero for IR drying [3] and, therefore, the moisture ratio (*MR*) was abbreviated to  $M/M_0$  instead of  $(M - Me)/M_0 - Me)$ ; where M is the moisture content in decimal dry basis at any time t,  $M_0$  is the initial moisture content in decimal dry basis, and *Me* is the equilibrium moisture content in decimal dry basis.

Non-linear regression analyses for these models were carried out by using SigmaPlot program (Version 12). The determination coefficient ( $R^2$ ), residual sum of squares (RSS) and standard error of estimate (SEE) were used as the primary parameters to select the best equation. These statistical values were calculated as follows:

$$R^{2} = \frac{\sum_{i=1}^{N} \left( MR_{exp,i} - MR_{pre,i} \right)^{2}}{N - n}$$
(4)

$$RSS = \left[\frac{1}{N}\sum_{i=1}^{N}MR_{pre,i} - MR_{exp,i}\right]^{\frac{1}{2}}$$
(5)

$$SEE = \sqrt{\frac{\sum_{1}^{N} (MR_{exp,i} - MR_{pre,i})}{N-2}}$$
(6)

where  $MR_{exp,i}$  is the *i*th experimental moisture ratio,  $MR_{pre,i}$  is the *i*th predicted moisture ratio,  $R^2$  is the coefficient of determination, and N is the number of observations [20,40].

## 2.6. The Effective Moisture Diffusivity and Activation Energy

Fick's diffusion equation for particles with slab geometry was used for calculation of effective moisture diffusivity. General solution of Fick's second law in slab geometry with the assumptions of moisture migration by diffusion, negligible shrinkage, constant diffusion coefficients, and temperature was as [41].

$$MR = \frac{8}{\pi^2} \exp\left(-\frac{\pi^2 D_{eff} t}{4L^2}\right) \tag{7}$$

$$D_{eff} = L^2 \times (-0.101 \ln MR - 0.0213)/t \tag{8}$$

where  $D_{eff}$  is the effective moisture diffusivity (m<sup>2</sup>/s), L is the thickness of linden leaves (m), *t* is the time (s).

The relationship between the effective moisture diffusivity and drying temperature was described using the Arrhenius-type equation [42–44]:

$$D_{eff} = D_0 \exp(-E_a / (RT_a)) \tag{9}$$

Many researchers considered that this is a convenient and frequently used method, as well as a simplified one, and it allows calculating a constant value for the whole process. Then, taking natural logarithm of the both sides, it can be written in a linear form as follows:

$$\ln(D_{eff}) = \ln(D_0) - [(E_a/R)(1/T_a)]$$
(10)

where  $E_a$  is the energy of activation (kJ/mol), R is the universal gas constant (8.3143 × 10<sup>-3</sup> kJ/mol),  $T_a$  is the absolute temperature (K), and  $D_0$  is the pre-exponential factor of the Arrhenius equation (m<sup>2</sup>/s). The activation energy can be calculated from the slope of the Equation (10) by plotting  $\ln(D_{eff})$  versus  $1/T_a$  ( $K_1 = E_a/R$ ).

#### 2.7. Extracts Preparation

The powdered sample (0.3 g) was extracted with methanol/distilled water (80:20, v/v) for 12 h at room temperature by the maceration method, and centrifuged for 20 min. The supernatant was used for the estimation of antioxidants and antioxidant activity.

# 2.8. Total Phenolic Content (TPC) Assay

The TPC was determined based on the Folin–Ciocalteu method [45]. A volume of 0.5 mL of the extract mixed with 2.5 mL of Folin–Ciocalteu reagent. After 5 min, 2 mL of 20% Na<sub>2</sub>CO<sub>3</sub> solution was added with the mix, then allowed to stand for 120 min. in the dark. The absorbance was measured at 760 nm. A calibration curve was established using gallic acid as a standard, and used between 1.5–100 ppm ( $R^2 = 0.9922$ ). TPC of the samples was expressed as gallic acid equivalents (g) per 100 g dry weight (DW) (g of GAE/ 100 g DW).

## 2.9. Total Flavonoids Assay (TFC)

The TFC was measured using an AlCl<sub>3</sub> colorimetric assay according to [46]. A volume of 0.25 mL of the extract was added to a test tube containing 0.75 mL of distilled water. Moreover, 0.15 mL of 5% sodium nitrite solution was added to the mix and reacted for 5 min followed by the addition of 0.3 mL of 10% aluminum chloride. After 5 min, 1 mL of 1 M sodium hydroxide solution was added. The absorbance was measured at 510 nm. A calibration curve was established using catechin as a standard. TFC was expressed as mg catechin equivalent (CE)/g of the samples.

#### 2.10. Statistical Analysis

Descriptive statistics were given as average and standard error of mean. Kolmogorov Smirnov test showed that the data has normally distributed (P = 0.862) and variances were homogeneous (P = 0.534), according to the Levene test. One-Way ANOVA was used to analyze the data [47]. Power of the test found 0.976; it showed that the sample size was adequate. Duncan multiple comparison was used to compare the means tests [48].

# 3. Results and Discussion

# 3.1. Moisture Contents

The moisture ratio vs. drying time at different temperatures is shown in Figure 4. The results show that the temperature had a significant effect on the drying of linden leaves. Depending on the drying temperature, the moisture content decreased to 0.10 g [H<sub>2</sub>O] kg<sup>-1</sup> [DM] in about 20 to 50 min (Figure 4)

for linden leaves. Drying time reduced dramatically with increased IR temperature. Moreover, results showed that higher drying temperature resulted in greater slope and the drying time is reduced by about 250%. The data obtained from many other studies in this field support this result [3,43,44,49–51]. Drying rate curves became steeper as drying temperature increased. This finding is in agreement with observations of several studies on IR drying [21,22,44].



Figure 4. Moisture ratio changes at different air temperatures.

# 3.2. Color

Indicators of fresh and dried leaves of linden at 50 °C, 60 °C, and 70 °C is presented in Table 2. The L\*, a\*, and b\* values mentioned in the Table 2, represent lightness (L\*), greenness (a\*), and yellowness (b\*) of linden leaves respectively.

Table 2. Color indicators of linden leaves at different temperature.

	<b>L</b> *	a*	b*	С	Н	ΔΕ
Fresh	$38.98 \pm 1.05$ <sup>b</sup>	$1.03 \pm 0.11$ <sup>b</sup>	$28.81 \pm 0.53$ <sup>a</sup>	$28.83 \pm 0.54$ <sup>a</sup>	$88.81 \pm 0.61$ <sup>a</sup>	-
IR-50 °C	38.86 ± 0.66 <sup>b</sup>	$-1.84 \pm 0.02$ <sup>c</sup>	$29.03 \pm 0.86$ <sup>a</sup>	$29.09 \pm 0.86$ <sup>a</sup>	$-86.36 \pm 0.14$ <sup>c</sup>	$3.617 \pm 0.20$
IR-60 °C	$42.36 \pm 0.63$ <sup>a</sup>	$1.22 \pm 0.06$ <sup>b</sup>	$30.56 \pm 0.35$ <sup>a</sup>	$30.59 \pm 0.35$ <sup>a</sup>	$88.34 \pm 0.66$ <sup>a</sup>	$4.11 \pm 1.32$
IR-70 °C	$40.95 \pm 1.11$ <sup>ab</sup>	$3.33 \pm 0.10^{a}$	$29.63 \pm 1.18$ <sup>a</sup>	29.81 ± 1.17 <sup>a</sup>	$83.4 \pm 0.93$ <sup>b</sup>	$3.81 \pm 0.54$
<i>p</i> -value	0.047	< 0.001	0.455	0.447	< 0.001	0.917

L\*, a\*, and b\* values represent fresh linden leaves; The resemblance of the defined colors (red, green, blue, and yellow) is called Hue (H); Chromatic deviation (C); Total chromatic deviation ( $\Delta E$ ); Different letters in same column indicate statistical difference (p < 0.05).

L\*, a\*, and b\* values of fresh linden leaves were 38.98, 1.03 and 28.81. As shown in Table 2, the L\* and b\* values of the dried linden leaves were increased partially, this may be due to the degradation of chlorophyll. The degree of color change was affected from oxygen level, drying temperature, and time. The magnesium in the chlorophyll structure can be replaced by hydrogen at high temperature. This displacement turns chlorophylls to pheophytins [52]. Observed a\* and b\* values were in the –1.84 and 3.33, 28.81, and 30.56 for dried linden leaves respectively. The a\* and b\* values of this study are consisted with the values found in study of Ertekin and Heybeli, ref. [31] for mint leaves. To determine the color difference, total chromatic deviation ( $\Delta$ E) and chromatic deviation ( $\Delta$ C) are not good indicators [3]. On the other hand, the resemblance of the defined colors (red, green, blue, and yellow) is called Hue (H) [53], and chrome value shows the vividness of color. Table 2 demonstrates that the color of dried linden leaves changed when the drying temperature changed.

The highest Hue value was 88.81 in fresh leaves. A similar finding was found in a study by Adak et al. [22]. The limit values of  $\Delta E$  were changed from 3.617 to 4.11. There were no significant differences from the point of  $\Delta E$  among the temperature effects, as well as C values. Zielinska and Markowski [54] found the highest L\* values at 60 °C under spout-fluidized bed drying and determined that a\* and b\* decreased at higher temperatures for the carrots slices.

Concerning color parameters, lightness (L\*) and (a\*) values increased together with temperature rise. Moreover,  $\Delta E$  and C values were not affected from temperature statistically with Type I error rates (P) of 0.917 and 0.447, respectively.

# 3.3. Projected Area (PA)

The effect of the IR process by using different temperatures on linden leaves were examined for changing of PA (Figure 5). Decreases from the PA were observed during drying of the leaves in all temperature treatments. In light of this result, it can be said that the changing of the drying temperature is the main effect on reducing the projection area of linden leaves. Statistical results (p < 0.05) also showed significant difference between the PA changes of dried linden leaves using IR, according to temperature (Table 3).



**Figure 5.** Demonstration of projected area (PA) changing at different temperatures process, (**a**) before IR drying, (**b**) after IR drying, and (**c**) calculate PA in ImageJ.

Table 3. Projection area changing of linden leave	s under IR processing a	at different temperatures
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	Projection Area (cm <sup>2</sup> )		
Fresh	$81.00 \pm 0.00$ <sup>a</sup>		
50 °C	$79.38 \pm 0.14$ <sup>b</sup>		
60 °C	$78.26 \pm 0.09$ <sup>c</sup>		
70 °C	$75.93 \pm 0.14$ <sup>d</sup>		
<i>p</i> -value	< 0.001		

Different letters in same column indicate statistical difference (p < 0.001).

Depending on the temperature values (50, 60, 70 °C), the initial projection area of fresh sample leaves was 81 cm<sup>2</sup>. There was a 1.067 times decreasing, compared to the projection area of fresh samples. The largest PA was observed as 79.38 cm<sup>2</sup> (50 °C) among treatments. At the end of the drying process, based on 50, 60, and 70 °C, the losses in the projection areas of the thin layer rose petals were 98.00%, 96.62%, and 93.74% for 50, 60, and 70 °C, respectively. The very fine structure of the leaves and the rapid removal of moisture as a result of this may have caused the shrinkage to occur at the beginning of the drying process. Briefly, this can be due to the effect of temperature on shrinkage. Similar statements (that drying reduces the PA of leaves [55]), and similar effects of drying air temperature, and time on the PA for different agricultural crops, have been reported in the literature [54].

## 3.4. Modeling of Drying Curves

For modeling purposes, the experimental moisture content data were used on the dry weight basis. These moisture content data at any time of drying process obtained under different IR drying temperatures were converted to moisture ratio values and fitted against the drying time. The 11 thin layer-drying models were compared according to their statistical parameters, such as the RSS, SEE, and  $R^2$  for adequacy of the model fit. The best model describing the thin layer drying characteristics of linden leaves was chosen as the one with the highest  $R^2$  value and lowest RSS and SEE values.

Among the eleven drying models used in this study, the Midilli et al. [34] model gave the best results for 50 °C and 60 °C data points with values for the R<sup>2</sup> greater than 0.9992, the SEE of lower than 0.0102 and the RSS of lower than 0.008 (Table 4 and Figure 6). This model was used for the linden leaves and can be shown as:

$$MR = a \exp(-kt^n) + bt \tag{11}$$

		5	Statistical N	Iodel and I	ts Constan	ts	
Temperature °C	Midilli et al. Model						
C	<i>R</i> <sup>2</sup>	SEE	RSS	k	п	а	b
50	0.9999	0.0025	0.0001	0.0413	1.0933	0.9998	0.0003
60	0.9992	0.0102	0.0008	0.0716	1.1305	0.9984	0.0009
70	0.9984	0.0152	0.0014	0.1300	1.1340	0.9914	0.0013
			Ver	ma et al. mo	odel		
50	0.9991	0.0095	0.0011	-0.1453	-	$6.64 \times 10^{-7}$	0.0534
60	0.9978	0.0159	0.0023	-0.0567	-	0.0020	0.0963
70	0.9999	0.0041	0.0001	-0.0121	-	0.0267	0.1814
			Diffusion	approximat	ion model		
50	0.9994	0.008	2.4640	2.1067	-	-0.0385	0.0262
60	0.9936	0.0269	0.0065	1.4003	-	-0.0229	0.0682
70	0.9999	0.0041	0.0001	0.1814	-	0.9733	-0.067
				Page model			
50	0.9992	0.009	0.0011	0.0472	1.0381	-	-
60	0.9935	0.0257	0.0066	0.0955	0.9915	-	-
70	0.9931	0.0269	0.0058	0.2584	0.7815	-	-

Table 4. Statistical models and its constant values for the thin layer drying models.

The determination coefficient ( $\mathbb{R}^2$ ), residual sum of squares ( $\mathbb{R}SS$ ) and standard error of estimate ( $\mathbb{S}EE$ ); *k*, the drying rate constant (h - 1), *a*, *n* and *b* are experimental constants.

On the other hand, when a comparison was made between the models for 70 °C, it was seen that the Verma et al. ( $R^2 = 0.9999$ ) and Diffusion approximation models ( $R^2 = 0.9999$ ) could represent the real values with higher accuracy than the other models. In addition, it can be said that the page model can be used if it is desired to express the drying behaviors partially with the help of a simple equation. Park et al. [58] compared Page and Fick's model and found that Page's model was a better fit to experimental mint drying data except for convective drying at a drying air temperature of 50 °C. In addition, the Onwude et al. study, in the pumpkin, similarly, Page model was best suited for predicting the drying kinetics of pumpkin for 60 °C, 70 °C, and 80 °C for the slices of 3 mm thickness [59]. As a result, the four different models, especially the Midilli et al model [34], predicted well the moisture ratio (MR) at three drying temperatures 50 °C, 60 °C, 70 °C for the linden leaves.



**Figure 6.** Statistical parameters of each model for different infrared (IR) drying temperatures. Where MR is the moisture ratio (dimensionless); *k*, the drying rate constant ( $h^{-1}$ ); *t*, the time (h) and *a*, *n* and *b* are experimental constants. The determination coefficient ( $R^2$ ), residual sum of squares (RSS) and standard error of estimate (SEE). Thus, the Midilli et al. [34] model may be assumed to represent the drying behavior of Linden leaves for 50 °C and 60 °C temperatures. It was emphasized that the Midilli et al. model [34] exhibited similar results in many other studies such as eggplant [31], kaffir lime leaves [51], carrot slices [56], Moroccan rosemary leaves [40], and pepper [20]. In addition, two- term and Logarithmic models gave relatively good results (Table 2 and Figure 6). Doymaz, I [57] surveyed four different thin-layer drying models (Lewis, Henderson, and Pabis, Modified Page, and logarithmic) and used determination coefficient, reduced  $R^2$ , and RMSE for comparing. According to the results, logarithmic model showed a good fit than the other models.

## 3.5. Effective Moisture Diffusivity and Activation Energy

The drying process of linden leaves can be easily modeled as a diffusion process as the entire drying process occurs in the falling rate period. Table 5 shows the effective moisture diffusivity ( $D_{eff}$ ) and activation energy ( $E_a$ ) values for linden leaves under different drying temperatures.

Table 5.  $D_{eff}$  coefficients and  $E_a$  of linden leaves under different IR drying temperatures.

Drying Temperature (°C)	$D_{eff}$ (m <sup>2</sup> s <sup>-1</sup> )	$D_0 \ ({ m m}^2 { m s}^{-1})$	E <sub>a</sub> (kJ/mol)
50	$4.13\times10^{-12}$		
60	$4.47\times10^{-12}$	$1.746 \times 10^{-09}$	16.339
70	$5.89\times10^{-12}$		

 $D_{eff}$  stands for the effective moisture diffusivity,  $D_0$  is the pre-exponential factor of the Arrhenius equation (m<sup>2</sup>/s) and  $E_a$  is activation energy.

The  $D_{eff}$  values varied from  $4.13 \times 10^{-12}$  to  $5.89 \times 10^{-12}$  m<sup>2</sup>/s and over the temperature range studied for biological materials [60]. According to Hii et al. [60] and Zogzas et al. [61], the values of moisture diffusivity of food products lies in the range of  $10^{-7}$  to  $10^{-12}$  m<sup>2</sup>/s. The variations in the present study might be because of  $D_{eff}$  is substantially hinged on drying conditions, features of drying equipment, recommended models used for calculation, product specifications as physico-chemical properties, such as compound, texture characteristics, layer thickness, cultivar and ripening stage, and other uncontrolled parameters [17,62]. The observations also agree with the results reported by Abraham et al. [63], Guine et al. [64], and Madan et al [65]. Noteworthy rises were acquired in the effective moisture diffusivity values with the increase in IR drying temperature (p < 0.001). This was because higher drying temperatures expedites the water molecules in the product and, as a result, rapid moisture loss occurs at higher temperatures as compared to lower temperatures. Moreover, rapid decline of the product moisture content corresponds to higher value of effective moisture diffusivity [66]. The logarithm of  $D_{eff}$  as a function of bivious of absolute temperature (T) is also demonstrated in Figure 7. The results show a linear relationship between ( $\ln D_{eff}$ ) and (1/T) or an Arrhenius-type relationship.



**Figure 7.**  $\ln D_{eff}$  versus absolute temperature inverses (T).

On the other hand, the diffusivity constant in other words "pre-exponential factor" of the Arrhenius equation ( $D_0$ ) was predicted as  $1.746 \times 10^{-09}$  m<sup>2</sup>/s for linden leaves. Activation energy ( $E_a$ ) was also estimated using exponential regression as a 16.339 kJ/mol for the linden leaves (Table 5).

This result is within the range of 15–40 kJ/mol for various foods [20]. When activation energies of fruits and vegetables are evaluated, more than 90% of the activation energy values that were found in previous studies ranged between 14.42 and 43.26 kJ/mol, for example; 28.60 kJ/mol for bamboo [66], 38.34 kJ/mol for sliced lemongrass [44], 28.36 kJ/mol for thin layer carrot [67]. The activation energy of present study for linden leaves is relatively low. The  $E_a$  value shows the sensitivity of diffusivity

against temperature [68]. This means that the lower the  $E_a$  values, the less sensitivity of the diffusivity to the temperature and, so, a lower value indicates high moisture diffusivity [67]. Hence, in the present study, about 16.339 kJ/mol of energy is required for the moisture diffusion and subsequent evaporation from the surface of the leaves.

## 3.6. Total Phenolic Content (TPC) and Flavonoids (TFC)

The results are given by calculating on dry matter values to prevent errors arising from dry matter difference. The total phenolic content (TPC) of fresh leaves material was significantly (p < 0.05) higher than dried leaves. Similarly, some recent searches have signified that dried plant materials include higher polyphenolics as antioxidants compared to fresh plant materials [68]. Table 6 presents the TPC and TFC content of the linden leaves under different temperatures process.

Temperature (°C)	TPC (mg/g, DW)	TFC (mg/g, DW)
Fresh	$127.73 \pm 0.76$ <sup>b</sup>	$0.567 \pm 0.015$ <sup>b</sup>
50	$95.184 \pm 0.47$ <sup>a</sup>	$2.790 \pm 0.150^{a}$
60	$99.756 \pm 0.63^{a}$	$2.631 \pm 0.084$ <sup>a</sup>
70	$98.929 \pm 0.43$ <sup>a</sup>	$2.583 \pm 0.145$ <sup>a</sup>
Significance	< 0.001	< 0.001

Table 6. Total phenolic and flavonoids content of the fresh and dried linden leaves.

The total phenolic content (TPC), total flavonoid content (TFC), a, b: Different letters within same column shows the statistical difference (p < 0.01).

To analyze the data, non-parametric permutation test was used because of heteroscedasticity [69]. TPC and TFC values were corrected and evaluated based on dry matter values to prevent errors arising from dry matter differences. Table 6 shows that, TPC of linden leaves were significantly different between fresh and dried samples and the values ranged from 99.756  $\pm$  0.63 mg/g to 127.73  $\pm$  0.76 mg/g. The TPC in the dried leaves (for 50 °C, 60 °C, 70 °C) were significantly (p < 0.001) lower than that in the fresh. TPC decreasing after IR drying may be caused by enzymatic processes. Moreover, a noteworthy decrease of total phenols concentration between fresh and dried samples, probably by the reason of generation of different antioxidant compounds having a varying degree of antioxidant activity. The same results were observed by Rababah, Al-u'datt, Alhamad, Al-Mahasneh, Ereifej, Andrade, Altarifi, Almajwal, and Yang [5] for sage, lemon balm, and thyme; Lopez et al. [70] for blueberry. When they evaluated the content of phenolic compounds after drying, higher TPC values in the fresh leaves than in the dried samples it have been found. It has also been reported by Felipe et al. [71] that the drying process can cause up to, approximately, a 30% decrease in total phenol content.

On the other hand, as can be seen in Table 6, the Duncan test indicates no statistical difference among temperatures (50 °C, 60 °C, and 70 °C). This means that linden leaves seem to be thermostable in the studied temperature range. This may indicate that linden leaves are thermostable in terms of the phenolic components they contain. Based on the drying process, similar observations were reported by Zlotek et al. [72]. Moreover, some researchers proposed that—not only the amount of antioxidants, but also a synergy occurring between them and the other leaves—ingredients might influence the differences in the antioxidant ability of material extracts [73].

Similarly, when the TFC were evaluated, a tendency to be directly proportional to the phenol contents was observed. The TFC in linden leaves are shown in Table 6; it varied significantly between fresh and dried samples and ranged from  $0.567 \pm 0.015$  mg/g to  $2.790 \pm 0.150$  mg/g. The reason for this may be the decrease of the solution viscosity due to the increase in temperature as the lime leaves change from a wet state to dry state, and the increase of solubility, accordingly [74]. Roshanak et al. [75] reported the high amount of TFC in dried green tea compared to fresh samples. In another study, Azad et al. [76] examined the effects of the IR drying process on Angelica gigas Nakai Powder and found that there was a decrease in total flavonoid content due to the temperature increase compared to the fresh sample. On the other hand, although the greatest TFC value among temperature applications

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was achieved at 50 °C, no statistically significant change (<0.001) was observed in the values due to the increase in temperature. As with the total phenol content values, the TFC values remained stable due to the temperature increase. The stability of the flavonoids depends on the type and number of substituents; sugar moiety and methoxyl groups protected flavonoids from different drying processes, such as IR, microwave, ultrasonic-induces degradation, hydroxyl groups, and the presence of non-phenolic compounds promoted it [77]. In this study, depending on the type of flavonoids and the number of substituents, there could be no change in the flavonoid contents. In addition, the TFC results obtained in the present study correlated with Olsson et al. [78]. They reported that heating has no causes—significant differences—in total flavonol content in sweet cultivars and in red onion cultivars.

Drying treatments have various effects on TPC and TFC, as stated by these observations. This finding suggests that besides the Midilli drying model, a simpler Page model can also be preferred for linden leaves under an IR thin layer drying process. In addition, 50 °C will be sufficient in terms of phenol content and flavonoids content in a thin layer lime leaf drying process with IR. In terms of energy saving, higher temperatures, such as 60 °C or 70 °C, can be avoided. The functional properties of food drying that influenced were by the intricate chemical interactions are still under research.

# 4. Conclusions

This study investigated the potential of using the thin layer as a modeling tool for predicting the drying process of linden leaves samples. The performance of IR drying technique for drying linden leaves samples was evaluated. This study also identified changing of color parameters, PA, and a suitable mathematical model to describe the behavior of thin layer linden leaves subject to IR drying. In addition, the moisture diffusion coefficient and the activation energy of the linden leaves were also estimated. Experiments for linden leaves were managed at specific drying temperatures of 50 °C, 60 °C, 70 °C.

The results showed that significant changes in color values occurred due to temperature change. The highest color parameters were achieved at 60 °C, except a\* and H values.  $\Delta E$  was not significantly affected from temperature change. The PAs of the dried linden leaves decreased 98.00%, 96.62%, and 93.74% for 50, 60, and 70 °C respectively. Moreover, the findings demonstrate that higher drying temperature is associated with shorter drying time and faster moisture removal rate. Drying time is reduced by about 250% with the effect of the IR process under different temperatures. The Midilli model (R<sup>2</sup> = 0.9999) was found to be the most suitable model describing thin-layer drying by IR for 50 °C, 60 °C, while the Verma et al. (R<sup>2</sup> = 0.9999) and Diffusion approximation models (R<sup>2</sup> = 0.9999) for the 70 °C. Effective moisture diffusivity varied from 4.13 × 10<sup>-12</sup> to 5.89 × 10<sup>-12</sup> over the temperature range studied, with activation energy of 16.339 kJ/mol.

Moreover, the effects of temperature on TPC and TFC by IR drying demonstrated that both values increased together with increasing temperatures. Drying temperature of 50 °C degrees in the thin layer IR drying process for these type of linden leaves could be recommended in terms of TPC and TFC. In addition, considering the further investigation in terms of TPC, more detailed results could be obtained with HPLC analysis instead of the Folin–Ciocalteu method. In this study, three different temperature effects on color, PA, some drying models, TPC, and TFC values were evaluated. Further study is recommended to understand the moisture diffusion mechanism, and any other properties changing at different drying processes, together with IR for linden leaves.

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# Abbreviations

C—degree (°), PA—projected area (mm<sup>2</sup>), TPC—total phenolic content (mg/g), TFC—total flavonoid content (mg/g), L\*—lightness, a\*—redness, b\*—blueness, C\*—chrome, H\*—hue angle,  $\Delta E$ —color difference,  $D_{eff}$ —effective moisture diffusivity (m<sup>2</sup>s<sup>-1</sup>),  $E_a$ —activation energy (kJ/mol).

# References

- 1. Ekor, M. The growing use of herbal medicines: Issues relating to adverse reactions and challenges in monitoring safety. *Front. Pharmacol.* **2014**, *4*, 1–10. [CrossRef] [PubMed]
- Certo, G.; Costa, R.; D'Angelo, V.; Russo, M.; Albergamo, A.; Dugo, G.; Germanò, M.P. Anti-angiogenic activity and phytochemical screening of fruit fractions from *Vitex agnus castus*. *Nat. Prod. Res.* 2017, 31, 2850–2856. [CrossRef] [PubMed]
- 3. Ertekin, C.; Heybeli, N. Thin-layer infrared drying of mint leaves. *J. Food Process. Preserv.* 2014, *38*, 1480–1490. [CrossRef]
- 4. Wissam, Z.; Nour, A.A.; Bushra, J.; Zein, N.; Saleh, D. Extracting and studying the antioxidant capacity of polyphenols in dry linden leaves (*Tilia cordata*). *J. Pharmacogn. Phytochem.* **2017**, *6*, 258–262.
- 5. Rodríguez, N.C.; Trujano, M.E.G.; Hernández, E.A.; García, M.R.; Sampieri, A.; Urrutia, E.C.; Aparicio, L.C. Anticonvulsant and antioxidant effects of *Tilia americana* var. *mexicana* and flavonoids constituents in the pentylenetetrazole-induced seizures. *Oxid. Med. Cell. Longev.* **2014**, 2014, 10.
- Rababah, T.M.; Al-u'datt, M.; Alhamad, M.; Al-Mahasneh, M.; Ereifej, K.; Andrade, J.; Altarifi, B.; Almajwal, A.; Yang, W. Effects of drying process on total phenolics, antioxidant activity and flavonoid contents of common Mediterranean herbs. *Int. J. Agric. Biol. Eng.* 2015, *8*, 145–150.
- 7. Delnavazi, M.R.; Shahabi, M.; Yassa, N. Flavonoids from the leaves of Iranian Linden; *Tilia rubra* subsp. *Caucasica. Res. J. Pharmacogn.* **2015**, *2*, 17–22.
- 8. Tuttu, G.; Ursavaş, S.; Soyler, R. Harvest amounts and ethnobotanical uses of the linden flowers in Turkey. *Anatol. J. Forest Res.* **2017**, *3*, 60–66.
- 9. Lao, Y.; Zhanga, M.; Chitrakar, B.; Bhandari, B.; Fan, D. Efficient plant foods processing based on infrared heating. *Food Rev. Int.* **2019**, *35*, 640–663. [CrossRef]
- 10. Khaled, A.Y.; Kabutey, A.; Selvi, K.Ç.; Mizera, C.; Hrabe, P.; Herak, D. Application of computational intelligence in describing the drying kinetics of persimmon fruit (*Diospyros kaki*) during vacuum and hot air drying process. *Processes* **2020**, *8*, 544. [CrossRef]
- 11. Soysal, Y.; Ayhan, Z.; Esturk, O.; Arikan, M.F. Intermittent microwave–convective drying of red pepper: Drying kinetics, physical (colour and texture) and sensory quality. *Biosyst. Eng.* **2009**, *103*, 455–463. [CrossRef]
- 12. Łechtanska, J.M.; Szadzinska, J.; Kowalski, S.J. Microwave- and infrared-assisted convective drying of green pepper: Quality and energy considerations. *Chem. Eng. Process.* **2015**, *98*, 155–164. [CrossRef]
- 13. Pawar, S.B.; Pratape, V.M. Fundamentals of infrared heating and its application in drying of food materials: A review. *J. Food Process. Eng.* **2017**, *40*, e12308. [CrossRef]
- 14. Guiné, R. The drying of foods and its effect on the physical-chemical, sensorial and nutritional properties. *Int. J. Food Eng.* **2018**, *4*, 93–100. [CrossRef]
- Orikasa, T.; Ono, N.; Watanabe, T.; Ando, Y.; Shiina, T.; Koide, S. Impact of blanching pretreatment on the drying rate and energy consumption during far-infrared drying of Paprika (*Capsicum annuum* L.). *Food Qual. Saf.* 2018, *2*, 97–103. [CrossRef]
- 16. Aboud, S.A.; Altemimi, A.B.; Al-Hilpy, A.R.S.; Chen, L.Y.; Cacciola, F. A comprehensive review on infrared heating applications in food processing. *Molecules* **2019**, *24*, 4125. [CrossRef] [PubMed]
- Deng, L.Z.; Yang, X.H.; Mujumdar, A.S.; Zhao, J.H.; Wang, D.; Zhang, Q.; Wang, J.; Gao, Z.J.; Xiao, H.W. Red pepper (*Capsicum annuum L.*) drying: Effects of different drying methods on drying kinetics, physicochemical properties, antioxidant capacity, and microstructure. *Dry Technol.* 2018, *36*, 893–907. [CrossRef]
- 18. Rahmawati, L.; Saputra, D.; Sahim, K.; Priyanto, G. Effect of infrared radiation on chemical and physical properties on duku's peel. *Potravin. Slovak J. Food Sci.* **2018**, *12*, 744–755.
- 19. Riadh, M.H.; Ahmad, S.A.B.; Marhaban, M.H.; Soh, A.C. Infrared heating in food drying: An overview. *Dry Technol.* **2015**, *33*, 322–335. [CrossRef]

- Soysal, Y.; Keskin, M.; Arslan, A.; Sekerli, Y.E. Infrared drying characteristics of pepper at different maturity stages. In Proceedings of the International Conference on Energy Research, Alanya, Turkey, 1–2 November 2018; pp. 293–304.
- 21. Sharma, G.P.; Verma, R.C.; Pathare, P.B. Thin-layer infrared radiation drying of onion slices. *J. Food Eng.* **2005**, *67*, 361–366. [CrossRef]
- 22. Adak, N.; Heybeli, N.; Ertekin, C. Infrared drying of strawberry. *Food Chem.* **2017**, *219*, 109–116. [CrossRef] [PubMed]
- 23. Doymaz, I. Infrared drying of kiwifruit slices. Int. J. Green Energy 2018, 15, 622–628. [CrossRef]
- 24. Igathinathane, C.; Pordesimo, L.O.; Batchelor, W.D. Major orthogonal dimensions measurement of food grains by machine vision using ImageJ. *Food Res. Int.* **2009**, *42*, 76–84. [CrossRef]
- 25. Juneau, K.J.; Tarasoff, C.S. Leaf area and water content changes after permanent and temporary storage. *PLoS ONE* **2012**, *7*, e42604. [CrossRef]
- 26. Easlon, H.M.; Bloom, A.J. Easy leaf area: Automated digital image analysis for rapid and accurate measurement of leaf area. *Appl. Plant Sci.* **2014**, *2*, 1–4. [CrossRef] [PubMed]
- Wang, D.C.; Fon, D.S.; Fang, W.; Sokhansanj, S. Development of a visual method to test the range of applicability of thin layer drying equations using MATLAB tools. *Dry Technol.* 2004, 22, 1921–1948. [CrossRef]
- 28. Dziki, D.; Kowalska, E.H.; Dziki, U.G.; Mis, A.; Rozylo, R.; Krzysiak, Z.; Hasson, W. Drying kinetics, grinding characteristics and physicochemical properties of broccoli sprouts. *Processes* **2019**, *8*, 97. [CrossRef]
- Nadian, M.H.; Shahin, R.; Seyed, S.M.; Soleiman, H.; Majid, K. Determination of shrinkage and shape change of apple slices during drying. In Proceedings of the 7th Asia-Pacific Drying Conference, Tianjin, China, 18–20 September 2011.
- Nahimana, H.; Zhang, M. Shrinkage and color change during microwave vacuum drying of carrot. *Dry Technol.* 2011, 29, 836–847. [CrossRef]
- Ertekin, C.; Yaldiz, O. Drying of eggplant and selection of a suitable thin layer drying model. *J. Food Eng.* 2004, *63*, 349–359. [CrossRef]
- 32. Diamente, L.M.; Munro, P.A. Mathematical modeling of the thin layer solar drying of sweet potato slices. *Solar Energy* **1993**, *51*, 271–276. [CrossRef]
- 33. Saçılık, K.; Keskin, R.; Eliçin, A.K. Mathematical modeling of solar tunnel drying of thin layer organic tomato. *J. Food Eng.* **2006**, *73*, 231–238. [CrossRef]
- 34. Midilli, A.; Küçük, H.; Yapar, Z. A new model for single-layer drying. *Dry Technol.* 2002, 20, 1503–1513. [CrossRef]
- 35. Wang, C.Y.; Singh, R.P. *A Single Layer Drying Equation For Rough Rice*; ASAE Paper No. 78-3001; American Society of Agricultural Engineers: St. Joseph, MI, USA, 1978.
- 36. Jain, D.; Pathare, P.B. Selection and evaluation of thin layer drying models for infrared radiative and convective drying of onion slices. *Biosyst. Eng.* **2004**, *89*, 289–296. [CrossRef]
- 37. Verma, L.R.; Bucklin, R.A.; Endan, J.B.; Wratten, F.T. Effects of drying air parameters on rice drying models. *ASAE* **1985**, *28*, 296–301. [CrossRef]
- 38. Naghavi, Z.; Moheb, A.; Ziaei-Rad, S. Numerical simulation of rough rice drying in a deep-bed dryer using non-equilibrium model. *Energy Convers. Manag.* **2010**, *51*, 258–264. [CrossRef]
- 39. Soysal, Y.; Oztekin, S.; Eren, Ö. Microwave drying of parsley: Modelling, kinetics, and energy aspects. *Biosyst. Eng.* **2006**, *93*, 403–413. [CrossRef]
- 40. Mghazli, S.; Ouhammou, M.; Hidar, N.; Lahnine, L.; Idlimam, A.; Mahrouz, M. Drying characteristics and kinetics solar drying of Moroccan rosemary leaves. *Renew. Energy* **2017**, *108*, 303–310. [CrossRef]
- 41. Crank, J. Mathematics of Diffusion, 2nd ed.; Oxford University Press: London, UK, 1975; p. 414.
- 42. Simal, S.; Femenia, A.; Garau, M.C.; Rossello, C. Use of exponential, Page's and diffusional models to simulate the drying kinetics of kiwi fruit. *J. Food Eng.* **2005**, *66*, 323–328. [CrossRef]
- 43. Kara, C.; Doymaz, I. Effective moisture diffusivity determination and mathematical modelling of drying curves of apple pomace. *Heat Mass Transf.* **2015**, *51*, 983–989. [CrossRef]
- 44. Nguyen, T.V.L.; Nguyen, M.D.; Nguyen, D.C.; Bach, L.G.; Lam, T.D. Model for Thin Layer Drying of Lemongrass (*Cymbopogon citratus*) by Hot Air. *Processes* **2019**, *7*, 21. [CrossRef]
- 45. Singleton, V.L.; Rossi, J.A. Colorimetry of total phenolics with phosphomolybdic-phosphotungstic acid reagents. *Am. J. Enol. Viticult.* **1965**, *16*, 144–153.

- 46. Gao, H.; Cheng, N.; Zhou, J.; Wang, B.N.; Deng, J.J.; Cao, W. Antioxidant activities and phenolic compounds of date plum persimmon (*Diospyros lotus* L.) fruits. *J. Food Sci. Technol.* **2014**, *51*, 950–956. [CrossRef] [PubMed]
- 47. Önder, H. Nonparametric statistical methods used in biological experiments yöntemler. *BSJ Eng. Sci.* 2018, 1, 1–6.
- 48. Genç, S.; Soysal, M.I. Parametric and nonparametric post hoc tests. BSJ Eng. Sci. 2018, 1, 18–27.
- Menges, H.O.; Ertekin, C. Thin layer drying model for treated and untreated Stanley plums. *Energy Convers. Manag.* 2006, 47, 2337–2348. [CrossRef]
- 50. Goyal, R.K.; Kingsly, A.R.P.; Manikantan, M.R.; Ilyas, S.M. Mathematical modelling of thin layer drying kinetics of plum in a tunnel dryer. *J. Food Eng.* **2007**, *79*, 176–180. [CrossRef]
- 51. Tasirin, S.M.; Puspasari, I.; Lun, A.W.; Chai, P.V.; Lee, W.T. Drying of kaffir lime leaves in a fluidized bed dryer with inertparticles: Kinetics and quality determination. *Ind. Crop. Prod.* **2014**, *6*, 193–201. [CrossRef]
- 52. Therdthai, N.; Zhou, W. Characterization of microwave vacuum drying and hot air drying of mint leaves (*Mentha cordifolia* Opiz ex Fresen). *J. Food Eng.* **2009**, *91*, 482–489. [CrossRef]
- 53. Li, B.; Lecourt, J.; Bishop, G. Advances in non-destructive early assessment of fruit ripeness towards defining optimal time of harvest and yield prediction—A Review. *Plants* **2018**, *7*, 2–20.
- 54. Zielinska, M.; Markowski, M. Color characteristics of carrots: Effect of drying and rehydration. *Int. J. Food Prop.* **2011**, *15*, 450–466. [CrossRef]
- 55. Torrez, V.; Jørgensen, P.M.; Zanne, A.E. Specific leaf area: A predictive model using dried samples. *Aust. J. Bot.* **2013**, *61*, 350–357. [CrossRef]
- 56. Doymaz, I. Drying kinetics, rehydration and colour characteristics of convective hot-air drying of carrot slices. *Heat Mass Transfer.* **2017**, *53*, 5–35. [CrossRef]
- 57. Doymaz, I. Thin-layer drying behaviour of mint leaves. J. Food Eng. 2006, 74, 370–375. [CrossRef]
- 58. Park, K.J.; Vohnikova, Z.; Brod, F.P.R. Evaluation of drying parameters and desorption isotherms of garden mint leaves (*Mentha crispa* L.). *J. Food Eng.* **2002**, *51*, 193–199. [CrossRef]
- 59. Onwude, D.I.; Hashim, N.; Janius, R.B.; Nawi, N.; Abdan, K. Evaluation of a suitable thin layer model for drying of pumpkin under forced air convection. *Int. Food Res. J.* **2016**, *23*, 1173–1181.
- 60. Hii, C.L.; Law, C.L.; Cloke, M. Modeling using a new thin layer drying model and product quality of cocoa. *J. Food Eng.* **2009**, *90*, 191–198. [CrossRef]
- Zogzas, N.P.; Maroulis, Z.B.; Kouris, D.M. Moisture diffusivity data compilation in foodstuffs. *Dry Technol.* 1996, 14, 2225–2253. [CrossRef]
- 62. Darvishi, H.; Asl, A.R.; Asghari, A.; Azadbakht, M.; Najafi, G.; Khodaei, J. Study of the drying kinetics of pepper. *J. Saudi Soc. Agri. Sci.* 2014, *13*, 130–138. [CrossRef]
- 63. Abraham, D.G.; Arolilo, A.P.; Rosimeire, M.R.; Cala, S.S.L.; Amanda, C.F. The air drying behaviour of osmotically dehydrated jackfruit. In Proceedings of the 14th International Drying Symposium, Sao Paulo, Brazil, 22–25 August 2004.
- 64. Guine, R.; Lopes, P.; Joao, B.M.; Ferreira, D. Effect of ripening stage on the solar drying kinetics and properties of S. bartolomeu pears. *Int. J. Acad. Res.* **2009**, *1*, 46–52.
- 65. Madan, A.; Pare, A.; Nanje Gowda, N.A. Mathematical modelling of thin-layer drying process of bamboo (*Bambusa bambos*) shoots at varying temperature. *Res. Rev. J. Bot.* **2014**, *3*, 1–9.
- 66. Darvishi, H.; Khoshtaghaza, M.H.; Najafi, G.; Nargesi, F. Mathematical modeling of green pepper drying in microwave-convective dryer. *J. Agri. Sci. Technol.* **2013**, *15*, 457–465.
- 67. Doymaz, I. Convective ait drying characteristics of thin layer carrots. J. Food Eng. 2004, 61, 359–364. [CrossRef]
- 68. Turhan, M.; Turhan, K.N.; Sahbaz, F. Drying kinetics of red pepper. J. Food Proc. Preserv. 1997, 21, 209–223. [CrossRef]
- 69. Önder, H.; Cebeci, Z. A Review on the permutation tests. *Biostat. Biom. Open Access J.* 2017, 3, 1–3. [CrossRef]
- López, J.; Uribe, E.; Vega-Gálvez, A.; Miranda, M.; Vergara, J.; Gonzalez, E.; Di Scala, K. Effect of air temperature on drying kinetics, vitamin C, antioxidant activity, total phenolic content, non-enzymatic browning and firmness of blueberries variety O'Neil. *Food Bioprocess Technol.* 2010, *3*, 772–777. [CrossRef]
- 71. Felipe, C.; da Silva, C.; Favaro-Trindade, S.M.; de Alencar, M.T.; Julio, C.B. Physicochemical properties, antioxidant activity and stability of spray-dried propolis. Kinetics, mineral content and colour characteristics of rosemary leave. *Energy Convers. Manag.* **2010**, *49*, 1258–1264.

- 72. Złotek, U.; Dziki, U.G.; Dziki, D.; Swieca, M.; Nowak, R.; Martinez, E. Influence of drying temperature on phenolic acids composition and antioxidant activity of sprouts and leaves of white and red quinoa. *Hindawi J. Chem.* **2019**, *2019*, 1–8. [CrossRef]
- 73. Capecka, E.; Mareczek, A.; Leja, M. Antioxidant activity of fresh and dry herbs of some *Lamiaceae* species. *Food Chem.* **2005**, *93*, 223–226. [CrossRef]
- 74. Shan, F.; Tang, H.; Wang, Y.; Guo, M. Study on flavonoids from the Peony leaves by ultrasonic extraction. *Adv. Mater. Res.* **2011**, 236–238, 2250–2254. [CrossRef]
- 75. Roshanak, S.; Rahimmalek, M.; Goli, S.A.H. Evaluation of seven different drying treatments in respect to total flavonoid, phenolic, vitamin C content, chlorophyll, antioxidant activity and color of green tea (*Camellia sinensis* or *C. assamica*) leaves. *J. Food Sci. Technol.* **2015**, *53*, 721–729. [CrossRef] [PubMed]
- 76. Azad, M.O.K.; Piao, J.P.; Park, C.H.; Cho, D.H. Far infrared irradiation enhances nutraceutical compounds and antioxidant properties in *Angelica gigas* nakai powder. *Antioxidants* **2018**, *7*, 189. [CrossRef] [PubMed]
- 77. Fernandez, N.F.; Casas, M.P.; Munoz, M.J.G.; Gonzalez, H.D. *Water Extraction of Bioactive Compounds: From Plants to Drug Devolopment*, 1st ed.; Elsevier: Amsterdam, The Netherlands, 2017; pp. 421–439.
- Olsson, M.E.; Gustavsson, K.E.; Vagen, I.M. Quercetin and isorhamnetin in sweet and red cultivars of onion (*Allium cepa* L.) at harvest, after field curing, heat treatment, and storage. J. Agric. Food Chem. 2010, 58, 2323–2330. [CrossRef] [PubMed]



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