

# SO<sub>2</sub> Poisoning of Cu-CHA deNO<sub>x</sub> Catalyst: The Most Vulnerable Cu Species Identified by X-ray Absorption Spectroscopy

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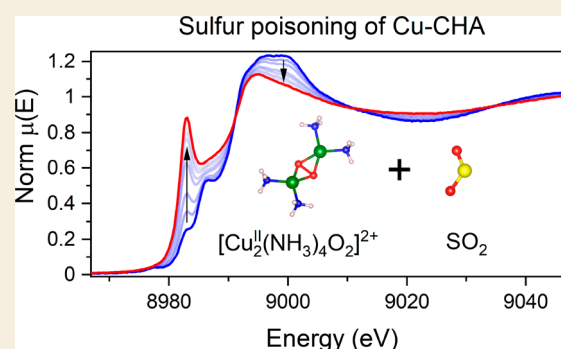
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**ABSTRACT:** Cu-exchanged chabazite zeolites (Cu-CHA) are effective catalysts for the NH<sub>3</sub>-assisted selective catalytic reduction of NO (NH<sub>3</sub>-SCR) for the abatement of NO<sub>x</sub> emission from diesel vehicles. However, the presence of a small amount of SO<sub>2</sub> in diesel exhaust gases leads to a severe reduction in the low-temperature activity of these catalysts. To shed light on the nature of such deactivation, we characterized a Cu-CHA catalyst under well-defined exposures to SO<sub>2</sub> using *in situ* X-ray absorption spectroscopy. By varying the pretreatment procedure prior to the SO<sub>2</sub> exposure, we have selectively prepared Cu<sup>I</sup> and Cu<sup>II</sup> species with different ligations, which are relevant for the NH<sub>3</sub>-SCR reaction. The highest reactivity toward SO<sub>2</sub> was observed for Cu<sup>II</sup> species coordinated to both NH<sub>3</sub> and extraframework oxygen, in particular for [Cu<sup>II</sup><sub>2</sub>(NH<sub>3</sub>)<sub>4</sub>O<sub>2</sub>]<sup>2+</sup> complexes. Cu species without either ammonia or extraframework oxygen ligands were much less reactive, and the associated SO<sub>2</sub> uptake was significantly lower. These results explain why SO<sub>2</sub> mostly affects the low-temperature activity of Cu-CHA catalysts, since the dimeric complex [Cu<sup>II</sup><sub>2</sub>(NH<sub>3</sub>)<sub>4</sub>O<sub>2</sub>]<sup>2+</sup> is a crucial intermediate in the low-temperature NH<sub>3</sub>-SCR catalytic cycle.

**KEYWORDS:** selective catalytic reduction, Cu-CHA, deNO<sub>x</sub> catalysis, sulfur poisoning, X-ray absorption spectroscopy, X-ray adsorbate quantification, XAS, XAQ



The emission of nitrogen oxides (NO<sub>x</sub>) from diesel vehicles is a global environmental challenge.<sup>1,2</sup> State of the art exhaust gas aftertreatment systems contain catalysts for selective catalytic reduction of NO<sub>x</sub> by ammonia (NH<sub>3</sub>-SCR), capable of reducing well over 90% of the NO<sub>x</sub> emitted by the engine. In the NH<sub>3</sub>-SCR reaction, NO reacts with NH<sub>3</sub> in the presence of O<sub>2</sub> to form N<sub>2</sub> and H<sub>2</sub>O. At present, Cu-exchanged chabazites (Cu-CHA) are the preferred catalysts for NH<sub>3</sub>-SCR, due to their superior low-temperature activity (150–350 °C)<sup>3,4</sup> and hydrothermal stability.<sup>5,6</sup> The temperature dependence of the NH<sub>3</sub>-SCR activity of Cu-CHA catalysts shows a minimum at around 350 °C, which indicates that the reaction mechanism at low temperatures is different from that at higher temperatures.<sup>7</sup>

The NH<sub>3</sub>-SCR reaction cycle for the low-temperature activity is a redox cycle, consisting of a series of oxidation and reduction steps, in which the oxidation state of Cu changes between Cu<sup>I</sup> and Cu<sup>II</sup>. The NO and NH<sub>3</sub> coordinate to Cu in the zeolite, giving rise to a variety of Cu species along the NH<sub>3</sub>-SCR cycle.<sup>8–11</sup> The low-temperature activity of Cu-CHA catalysts originates from the ability to form mobile Cu<sup>I</sup>(NH<sub>3</sub>)<sub>2</sub> complexes under SCR conditions. Pairs of these species constitute the active Cu sites capable of O<sub>2</sub> activation via the

formation of [Cu<sup>II</sup><sub>2</sub>(NH<sub>3</sub>)<sub>4</sub>O<sub>2</sub>]<sup>2+</sup> dimers around 200 °C, which is a crucial step in the NH<sub>3</sub>-SCR reaction cycle.<sup>12,13</sup>

In practice, the application of Cu-CHA catalysts for the NH<sub>3</sub>-SCR is restricted to ultralow-sulfur diesel fuels, due to the fact that a few ppm of SO<sub>2</sub> present in the exhaust gas drastically reduces the activity at low temperatures.<sup>3,4,14</sup> Multiple studies show that SO<sub>2</sub> affects the Cu mobility, the amount of Cu active sites,<sup>14</sup> and the redox behavior of the Cu in the NH<sub>3</sub>-SCR cycle.<sup>9,15</sup> Most studies have focused on the overall effect of SO<sub>2</sub> on the performance of the catalysts,<sup>14–21</sup> while the chemistry behind SO<sub>2</sub> poisoning at the molecular level remains poorly understood. To determine a mechanism for SO<sub>2</sub> poisoning, one must identify the species in the Cu-CHA catalysts that interact with SO<sub>2</sub>. To this end, we have selectively prepared well-defined Cu<sup>I</sup> and Cu<sup>II</sup> species with

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**Table 1. Pretreatment Procedures and Resulting Cu Species**

procedure	conditions	dominant Cu state	designation in the text and figures	ref
1	1% H <sub>2</sub> at 400 °C; cooling to 200 °C in He	fw-Cu <sup>I</sup>	fw-Cu <sup>I</sup>	24
2	500 ppm of NO + 600 ppm of NH <sub>3</sub> at 200 °C	mobile [Cu <sup>I</sup> (NH <sub>3</sub> ) <sub>2</sub> ] <sup>+</sup>	[Cu <sup>I</sup> (NH <sub>3</sub> ) <sub>2</sub> ] <sup>+</sup>	24
3	500 ppm of NO + 600 ppm of NH <sub>3</sub> at 200 °C; heating to 550 °C in He; cooling back to 200 °C in He	fw-Cu <sup>I</sup> (after thermal treatment of [Cu <sup>I</sup> (NH <sub>3</sub> ) <sub>2</sub> ] <sup>+</sup> )	[Cu <sup>I</sup> (NH <sub>3</sub> ) <sub>2</sub> ] <sup>+</sup> + T	24
4	10% O <sub>2</sub> at 200 °C	fw-Cu <sup>II</sup>	fw-Cu <sup>II</sup>	25
5	500 ppm of NO + 600 ppm of NH <sub>3</sub> at 200 °C; He purge; 10% O <sub>2</sub> at 200 °C	mobile [Cu <sup>II</sup> <sub>2</sub> (NH <sub>3</sub> ) <sub>4</sub> O <sub>2</sub> ] <sup>2+</sup> dimer	[Cu <sup>II</sup> <sub>2</sub> (NH <sub>3</sub> ) <sub>4</sub> O <sub>2</sub> ] <sup>2+</sup>	13
6	600 ppm of NH <sub>3</sub> at 200 °C	mixed <sup>a</sup>	Cu <sup>II</sup> + NH <sub>3</sub>	this work

<sup>a</sup>Procedure 6 results in a mixture of two NH<sub>3</sub>-coordinated Cu species, as discussed further in the text.

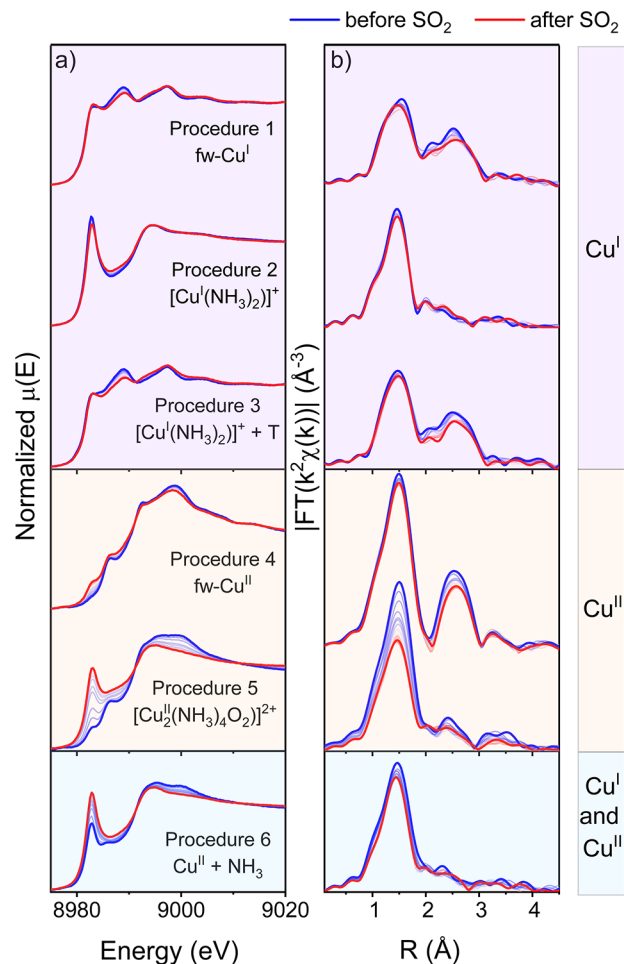
different ligands inside the pores of the Cu-CHA catalyst and exposed them to SO<sub>2</sub> under well-defined conditions. We monitored the changes in the Cu K-edge X-ray absorption spectra (XAS) during the absorption of SO<sub>2</sub>. This allowed us to determine the chemical state of the Cu that interacts with SO<sub>2</sub>. The results were corroborated by X-ray emission spectroscopy (XES) and measurements of the SO<sub>2</sub> uptake using temperature-programmed desorption (TPD) of SO<sub>2</sub>.

The Cu-CHA catalyst used in this study had a Si/Al ratio of 6.7 and a Cu loading of 3.2 wt % (Cu/Al = 0.24). The Cu K-edge XAS and Cu Kβ valence-to-core XES measurements were carried out at the BM23<sup>22</sup> and ID26<sup>23</sup> beamlines of the European Synchrotron Radiation Facility (ESRF), respectively. Sample treatment protocols consisted of three distinct steps. First, all samples were heated to 550 °C in a 10% O<sub>2</sub>/He flow, removing water and forming Cu<sup>II</sup> species bound to the framework of the zeolite (fw-Cu<sup>II</sup>). Then, the specific state of Cu was prepared, using one of the six different pretreatment procedures summarized in Table 1. Finally, the catalyst was exposed to 400 ppm SO<sub>2</sub>/He flow at 200 °C for 3 h until no visible changes in the spectra occurred. Further experimental details are given in the Supporting Information.

The Cu species formed with the pretreatments differ in three aspects: (1) the oxidation state of Cu (Cu<sup>I</sup> or Cu<sup>II</sup>), (2) the coordination of the Cu (NH<sub>3</sub> or/and O), and (3) the interaction of the Cu with the framework (fw-coordinated or mobile species).

Figure 1 shows the evolution of Cu K-edge XANES and EXAFS spectra during the exposure of the pretreated Cu-CHA catalyst to 400 ppm SO<sub>2</sub>/He flow at 200 °C. For all Cu<sup>I</sup> species and fw-Cu<sup>II</sup> species (procedures 1–4 in Table 1), only minor changes are observed upon SO<sub>2</sub> exposure, indicating that these species are not very reactive toward SO<sub>2</sub>. In contrast, for Cu<sup>II</sup> species in the presence of NH<sub>3</sub> (procedures 5 and 6) significant changes are observed in the spectra. In these cases, the exposure to SO<sub>2</sub> results in a pronounced increase of the XANES peak at 8983 eV, characteristic for linear Cu<sup>I</sup> complexes,<sup>9,26,27</sup> and a decrease in the intensity of the first shell in the EXAFS FT. This means that some of the Cu<sup>II</sup> species are reduced to Cu<sup>I</sup> upon interaction with SO<sub>2</sub>. The decrease in the first-shell intensity indicates a reduction of the coordination number for the Cu ions, which is also in line with the formation of a linear Cu<sup>I</sup> species.

The species obtained in procedure 5 are the oxygen-bridged diamine dicopper complexes [Cu<sup>II</sup><sub>2</sub>(NH<sub>3</sub>)<sub>4</sub>O<sub>2</sub>]<sup>2+</sup>, which are formed by the reaction of O<sub>2</sub> with a pair of [Cu<sup>I</sup>(NH<sub>3</sub>)<sub>2</sub>]<sup>+</sup> complexes.<sup>13</sup> In the reaction cycle for the low-temperature NH<sub>3</sub>-SCR reaction,<sup>11,13,28</sup> the [Cu<sup>II</sup><sub>2</sub>(NH<sub>3</sub>)<sub>4</sub>O<sub>2</sub>]<sup>2+</sup> complexes react with NO, which eventually leads to the production of N<sub>2</sub>

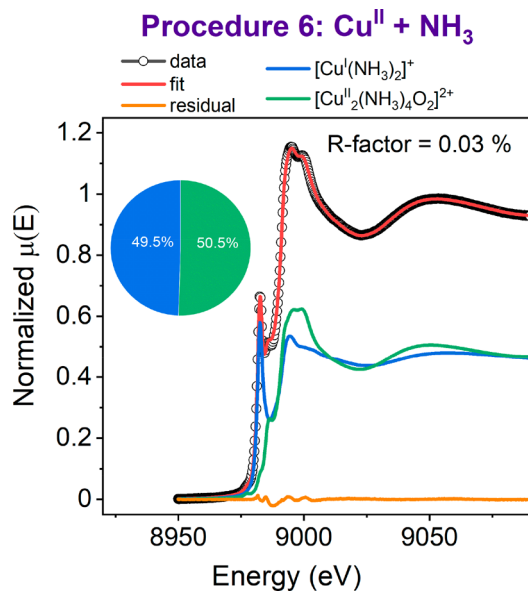


**Figure 1.** Cu K-edge XANES (a) and FT-EXAFS spectra (b) collected *in situ* during the exposure of Cu species obtained in procedures 1–6 to SO<sub>2</sub> at 200 °C.

and H<sub>2</sub>O. The observation that the [Cu<sup>II</sup><sub>2</sub>(NH<sub>3</sub>)<sub>4</sub>O<sub>2</sub>]<sup>2+</sup> complexes are reactive toward SO<sub>2</sub> is therefore a good explanation for the SO<sub>2</sub>-induced deactivation of Cu-CHA catalysts for NH<sub>3</sub>-SCR: the reaction with SO<sub>2</sub> interrupts the NH<sub>3</sub>-SCR cycle, thereby decreasing the activity of the catalyst.

The other case where Cu reacts with SO<sub>2</sub> is obtained in procedure 6 by exposure of the fw-Cu<sup>II</sup> species to NH<sub>3</sub>. Previously, a similar pretreatment resulted in a mixture of linear [Cu<sup>I</sup>(NH<sub>3</sub>)<sub>2</sub>]<sup>+</sup> and either square-planar [Cu<sup>II</sup>(NH<sub>3</sub>)<sub>4</sub>]<sup>2+</sup> complexes or mixed-ligand [Cu<sup>II</sup>O<sub>x</sub>(NH<sub>3</sub>)<sub>y</sub>]<sup>2+</sup> moieties.<sup>9,24</sup> For the sample reported in this work, the mixed-ligand configuration is more likely. Indeed, linear combination fits

of the XANES data on the basis of references for the linear  $[\text{Cu}^{\text{I}}(\text{NH}_3)_2]^+$  complex and pure  $\text{Cu}^{\text{II}}(\text{NH}_3)_4$  groups (aqueous  $[\text{Cu}^{\text{II}}(\text{NH}_3)_4]^{2+}$  or solid-state  $[\text{Cu}^{\text{II}}(\text{NH}_3)_4]\text{SO}_4 \cdot \text{H}_2\text{O}$ ) resulted in visible discrepancies with the data (Figure S7 in the Supporting Information). A better agreement is obtained when the spectrum of oxygen-bridged diamine dicopper complex  $[\text{Cu}^{\text{II}}_2(\text{NH}_3)_4\text{O}_2]^{2+}$  is used as a  $\text{Cu}^{\text{II}}$  reference in combination with  $[\text{Cu}^{\text{I}}(\text{NH}_3)_2]^+$ , with approximately equal weights for each component (Figure 2). The necessary stock of available oxygen

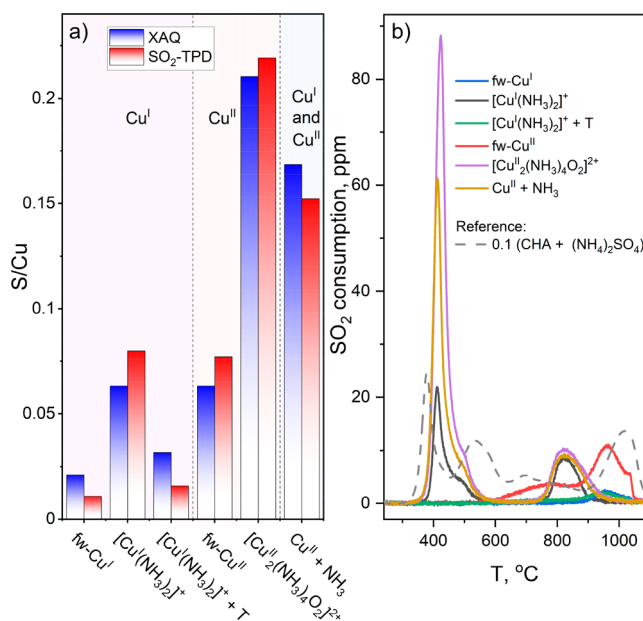


**Figure 2.** Linear combination fit of Cu K-edge XANES spectra obtained in Cu-CHA after exposing fw- $\text{Cu}^{\text{II}}$  species to  $\text{NH}_3$  at 200 °C ( $\text{Cu}^{\text{II}} + \text{NH}_3$  pretreatment).

needed for the formation of the mixed-ligand species is expected to be present in the sample, as a wavelet analysis of the EXAFS collected after heating to 550 °C and cooling to 200 °C in 10%  $\text{O}_2/\text{He}$  flow reveals the presence of Cu–Cu scattering usually attributed to the oxygen-containing dimers<sup>29,30</sup> (Figure S8 in the Supporting Information), which may be susceptible to form mixed-ligand species upon exposure to  $\text{NH}_3$ .

The evolution of XANES spectra upon interaction with  $\text{SO}_2$  shows that the most susceptible species are  $\text{Cu}^{\text{II}}$  with mixed  $(\text{NH}_3)_x\text{O}_y$  ligation, whereas  $\text{Cu}^{\text{I}}$  species or  $\text{Cu}^{\text{II}}$  in the absence of  $\text{NH}_3$  are much less affected. These findings are supported by X-ray adsorbate quantification (XAQ) data,<sup>31</sup> collected simultaneously with the XAS measurements during the exposure to  $\text{SO}_2$ , and a TPD analysis of a parallel set of catalyst samples, exposed to the same pretreatments used in XANES experiments (Figure 3a). We find the highest sulfur content ( $S/\text{Cu}$  ratio) for the  $[\text{Cu}^{\text{II}}_2(\text{NH}_3)_4\text{O}_2]^{2+}$  and  $\text{Cu}^{\text{II}} + \text{NH}_3$  procedures. The sulfur uptake of the  $[\text{Cu}^{\text{I}}(\text{NH}_3)_2]^+$  and fw- $\text{Cu}^{\text{II}}$  moieties was ca. 3 times lower, and for the bare fw- $\text{Cu}^{\text{I}}$  species, it was ca. 6 times lower. These results show that the reaction between the  $[\text{Cu}^{\text{II}}_2(\text{NH}_3)_4\text{O}_2]^{2+}$  species and  $\text{SO}_2$  contributes the most to the accumulation of  $\text{SO}_2$  in the Cu-CHA catalyst.

Interestingly, the sulfur content in the  $\text{Cu}^{\text{II}} + \text{NH}_3$  sample lies between those for samples with pure  $[\text{Cu}^{\text{I}}(\text{NH}_3)_2]^+$  and  $[\text{Cu}^{\text{II}}_2(\text{NH}_3)_4\text{O}_2]^{2+}$  species, which in combination with the linear combination fit shown in Figure 2 suggests that the

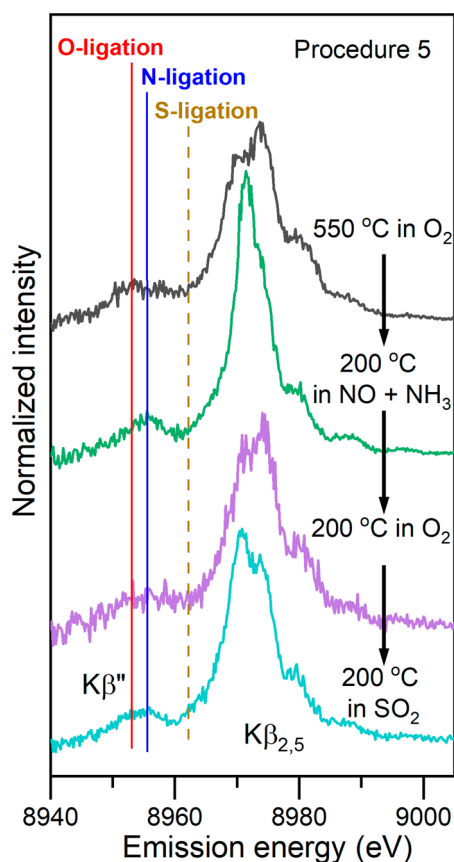


**Figure 3.** (a)  $S/\text{Cu}$  ratios in the samples after exposure to  $\text{SO}_2$  obtained from  $\text{SO}_2$ -TPD and XAQ. (b)  $\text{SO}_2$ -TPD profiles collected after exposure of the species obtained in procedures 1–6 to  $\text{SO}_2$  in comparison to a reference  $\text{SO}_2$ -TPD curve of a CHA zeolite without Cu impregnated with 20 wt %  $(\text{NH}_4)_2\text{SO}_4$ , downscaled  $\times 10$ .

reactivity of the  $\text{Cu}^{\text{II}}(\text{NH}_3)_x\text{O}_y$  species obtained after  $\text{Cu}^{\text{II}} + \text{NH}_3$  treatment toward  $\text{SO}_2$  is similar to that of  $[\text{Cu}^{\text{II}}_2(\text{NH}_3)_4\text{O}_2]^{2+}$ .

By comparing the  $\text{SO}_2$ -TPD curves of Cu-CHA samples with that of  $(\text{NH}_4)_2\text{SO}_4$  adsorbed on Cu-free CHA (Figure 3b), we can also deduce that the elevated sulfur content in the samples with the  $\text{Cu}^{\text{II}}(\text{NH}_3)_x\text{O}_y$  species is due to the reactivity toward  $\text{SO}_2$  and not to the formation of  $(\text{NH}_4)_2\text{SO}_4$  in a reaction of  $\text{SO}_2$  with  $\text{NH}_3$  and  $\text{NH}_4^+$  groups stored in the zeolite framework. For the adsorbed  $(\text{NH}_4)_2\text{SO}_4$ , we observe  $\text{SO}_2$  desorption at around 380, 530, and 1000 °C (gray curve in Figure 3b). The desorption at 380 °C matches the known thermal decomposition of  $(\text{NH}_4)_2\text{SO}_4$ ,<sup>32</sup> the other two peaks are probably due to the interaction of either  $(\text{NH}_4)_2\text{SO}_4$  or products of its decomposition with the zeolite, their precise interpretation being beyond the scope of the present argument. For all three Cu-CHA samples containing  $\text{NH}_3$  before exposure to  $\text{SO}_2$  ( $[\text{Cu}^{\text{I}}(\text{NH}_3)_2]^+$ ,  $[\text{Cu}^{\text{II}}_2(\text{NH}_3)_4\text{O}_2]^{2+}$ , and  $(\text{Cu}^{\text{II}} + \text{NH}_3)$  procedures), we observe  $\text{SO}_2$  desorption at around 420 °C (Figure 3b). As this does not match any of the observed desorption characteristics of  $(\text{NH}_4)_2\text{SO}_4$  in Cu-free Cu-CHA, the  $\text{SO}_2$ -TPD feature at 420 °C reflects an interaction of Cu with  $\text{SO}_2$ . Interestingly, the  $\text{SO}_2$ -TPD curve for the sample with the dominant fw- $\text{Cu}^{\text{II}}$  species shows a significant  $\text{SO}_2$  desorption peak close to 1000 °C, which, together with the lack of changes in Cu K-edge XANES upon exposure to  $\text{SO}_2$ , indicates the formation of some sulfur deposits not directly coordinated to Cu.

The presence of Cu–N and Cu–O bonds in the  $[\text{Cu}^{\text{II}}_2(\text{NH}_3)_4\text{O}_2]^{2+}$  complex has been independently confirmed by valence-to-core XES.<sup>27,33,34</sup> XES spectra at different stages of pretreatment leading to the formation of  $[\text{Cu}^{\text{II}}_2(\text{NH}_3)_4\text{O}_2]^{2+}$  dimers are reported in Figure 4. The origin of the  $K\beta'$  satellite peak is the transition from the ligand s orbitals to Cu 1s, which makes its position sensitive to the species directly coordinated to Cu and allows it to discriminate



**Figure 4.** Background-subtracted Cu  $K\beta$  valence-to-core XES spectra for different stages of procedure 5 leading to the formation of the  $[\text{Cu}^{\text{II}}_2(\text{NH}_3)_4\text{O}_2]^{2+}$  complex and its exposure to  $\text{SO}_2$ .

among Cu–O, Cu–N, and Cu–S bonds.<sup>35–37</sup> Figure 4 shows that after heating in  $\text{O}_2$  Cu is predominantly coordinated by oxygens (as expected for the fw- $\text{Cu}^{\text{II}}$  species), whereas after exposure to  $\text{NO} + \text{NH}_3$  N ligands are dominating, as expected for a  $[\text{Cu}^{\text{I}}(\text{NH}_3)_2]^+$  linear complex. After subsequent exposure to  $\text{O}_2$  and formation of  $[\text{Cu}^{\text{II}}_2(\text{NH}_3)_4\text{O}_2]^{2+}$  dimers, the peak broadens, confirming the presence of both Cu–N and Cu–O bonds. These bonds remain after exposure to  $\text{SO}_2$ , while no significant contribution from Cu–S bonds<sup>38</sup> is observed, suggesting that the possible  $\text{SO}_2$  binding to the Cu is carried out through an oxygen atom.

In conclusion, the *in situ* XAS and XES measurements of different Cu intermediates formed in a Cu-CHA catalyst exposed to  $\text{SO}_2$  demonstrate that  $\text{Cu}^{\text{II}}$  species with mixed  $\text{NH}_3$  and O ligation of Cu are particularly reactive toward  $\text{SO}_2$ , whereas  $\text{Cu}^{\text{I}}$  species and  $\text{Cu}^{\text{II}}$  without  $\text{NH}_3$  are much less affected by it. In particular, the  $[\text{Cu}^{\text{II}}_2(\text{NH}_3)_4\text{O}_2]^{2+}$  complex, which is formed upon activation of  $\text{O}_2$  in the  $\text{NH}_3$ -SCR cycle, shows a clear reaction with  $\text{SO}_2$ , resulting in a partial reduction of the  $\text{Cu}^{\text{II}}$  and accumulation of sulfur in the zeolite. Therefore, we conclude that this reaction is responsible for the poisoning of Cu-CHA catalysts in  $\text{NH}_3$ -SCR by  $\text{SO}_2$ .

## ■ ASSOCIATED CONTENT

### Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/jacsau.2c00053>.

Experimental details, XANES linear combination fits before  $\text{SO}_2$  exposure, wavelet transform analysis of the sample heated in  $\text{O}_2$ , and EXAFS fitting results (PDF)

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### Notes

The authors declare no competing financial interest.

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