

# FTIR-Assisted Electroreduction of CO<sub>2</sub> and H<sub>2</sub>O to CO and H<sub>2</sub> by Electrochemically Deposited Copper on Oxidized Graphite Felt

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Cite This: *ACS Omega* 2022, 7, 45067–45076

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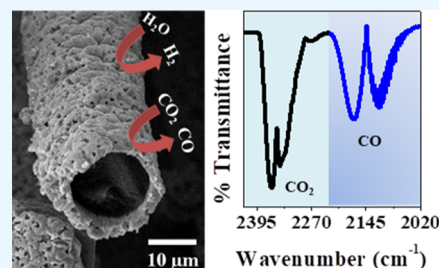


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**ABSTRACT:** Obtaining CO and H<sub>2</sub> from electrochemical CO<sub>2</sub> reduction (CO<sub>2</sub>RR) offers a viable alternative to reduce CO<sub>2</sub> emissions and produce chemicals and fuels. Herein, we report a simple strategy for obtaining polycrystalline copper deposited on oxidized graphite felt (Cu-OGF) and its performance on the selective conversion of CO<sub>2</sub> and H<sub>2</sub>O to CO and H<sub>2</sub>. For the electrode obtaining, graphite felt (GF) was first oxidized (OGF) in order to make the substrate hydrophilic and then copper particles were electrochemically deposited onto OGF. The pH of deposition was investigated, and the CO<sub>2</sub>RR activity was assessed for the prepared electrodes at each pH (2.0, 4.0, 6.0, 8.0, and 10.0). It was found that pH 2.0 was the most promising for CO<sub>2</sub>RR due to the presence of hexagonal copper microparticles. Fourier transform infrared analysis of the produced gases showed that this is a low-cost catalyst capable of reducing CO<sub>2</sub> and H<sub>2</sub>O to CO and H<sub>2</sub>, with Faradaic efficiencies between 0.50 and 5.21% for CO and 50.87 to 98.30% for H<sub>2</sub>, depending on the experimental conditions. Hence, it is possible for this gas mixture to be used as a fuel gas or to be enriched with CO for use in Fischer–Tropsch processes.



## 1. INTRODUCTION

In the search for renewable energy sources, electrochemical energy conversion has emerged as a promising alternative to the use of fossil fuels.<sup>1</sup> In this sense, the CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) emerges as an excellent alternative because it can provide sustainable fuel production.<sup>2</sup> As a widely available and inexpensive metal, copper has been extensively studied as the catalyst for CO<sub>2</sub>RR. An additional feature is the obtention of several fuels, such as hydrogen, methane, ethylene, ethanol, and methanol.<sup>3</sup> However, the costs associated with the separation of these and other CO<sub>2</sub>RR products make it difficult to implement this technology.<sup>4</sup>

In the electrochemical reduction of CO<sub>2</sub>, H<sub>2</sub> is inevitably obtained as a byproduct from the competitive hydrogen evolution reaction (HER).<sup>5,6</sup> It is, therefore, possible to obtain syngas (a mixture composed of 30–60% CO, 25–30% H<sub>2</sub>, and 5–15% CO<sub>2</sub><sup>7</sup>), which has aroused interest due to the wide range of possible applications.<sup>8</sup> For example, syngas can be used for the synthesis of chemicals and synthetic fuels through well-established industrial processes.<sup>5,9</sup> According to the H<sub>2</sub>/CO molar ratio, syngas is targeted for specific applications. For instance, an H<sub>2</sub>/CO ratio of 2:1 to 3:1 is ideal for methanol production, an H<sub>2</sub>/CO ratio of 0.25:1 is favorable for ethanol production, and an H<sub>2</sub>/CO ratio of 2:1 is suitable for Fischer–Tropsch processes.<sup>6,10–12</sup>

Aiming for an efficiency increase in syngas production by copper electrodes, several strategies have been developed. Reske and co-workers studied the effect of Cu nanoparticle (NP) size on the catalytic activity and selectivity for CO<sub>2</sub>RR. They reported a dramatic increase in selectivity for CO and H<sub>2</sub> for NPs below 5 nm.<sup>13</sup> The use of different morphologies has

also been proposed. Wang and co-workers reported the use of copper nanowire arrays and obtained a tunable H<sub>2</sub>/CO ratio according to the applied potential.<sup>9</sup> Grosse and collaborators studied nanocubic Cu and the effect of the supporting materials, such as copper and carbon. The results showed higher Faradaic efficiency (FE) for CO in copper nanocubes supported on carbon.<sup>14</sup> Another method that has been shown to increase CO production is etching copper single-crystal surfaces.<sup>15</sup> However, among the cited works, only copper nanowire arrays produced only H<sub>2</sub> and CO as gaseous products.<sup>9</sup> For this reason, the combination of copper with other materials has been studied, such as Cu/Ni(OH)<sub>2</sub>,<sup>16</sup> Cu/In<sub>2</sub>O<sub>3</sub>,<sup>5</sup> Cu/SnO<sub>2</sub>,<sup>17</sup> Cu/In,<sup>18,19</sup> Cu/Ag,<sup>20</sup> Cu/Pd,<sup>21</sup> and Cu/Au.<sup>22</sup> Modifications in the electrochemical measurements have also been shown to be effective for increasing the FE of CO<sub>2</sub>RR on copper materials, such as the use of pulsed electrolysis. Engelbrecht and co-workers reported suppression of HER, achieving 10% FE,<sup>23</sup> while Kumar and colleagues showed high selectivity for syngas by suppressing the side reactions.<sup>24</sup>

NPs and single crystals are important for understanding the mechanisms involved in CO<sub>2</sub>RR but are limited in their applicability. However, electrodeposited copper offers excellent

Received: August 25, 2022

Accepted: November 17, 2022

Published: December 1, 2022



applicability as it can be obtained with the desired geometric area. Also, it is a low-cost and simple operation process.<sup>25,26</sup> As a support material for electrodeposition, graphite felt (GF) has some outstanding properties, such as chemical resistance and good electrical and mechanical properties.<sup>27–29</sup> Nevertheless, due to its low hydrophilicity, a surface modification treatment, such as thermal activation,<sup>30</sup> nitration,<sup>31,32</sup> or anodic modification,<sup>33</sup> is required to enhance its use as an electrode in aqueous media.

Herein, we report the synthesis of low-cost copper electrodes supported on oxidized GF (Cu-OGF). GF was first oxidized, and then copper was electrochemically deposited at different pHs. Fourier transform infrared (FTIR) spectroscopy-assisted electrocatalytic experiments showed that the electrode obtained at pH 2 can be used for the selective reduction of CO<sub>2</sub> and water to CO and H<sub>2</sub>.

## 2. EXPERIMENTAL SECTION

**2.1. Chemicals.** Copper sulfate pentahydrate (CuSO<sub>4</sub>·5H<sub>2</sub>O, 99.99%, Sigma-Aldrich), citric acid (C<sub>6</sub>H<sub>8</sub>O<sub>7</sub>, 99%, Sigma-Aldrich), sodium hydroxide (NaOH, 99%, Sigma-Aldrich), carbon dioxide (CO<sub>2</sub>, 99.99%, White Martins), and nitrogen (N<sub>2</sub>, 99.999%, White Martins) were used without purification. GF was used as the support for copper microparticles, and copper foil (99.9%) was employed as the counter electrode in the copper deposition. Commercial copper foam was used as the reference material. All solutions were prepared using 18.2 MΩ cm deionized water.

**2.2. GF Surface Treatment.** In a glass reflux condenser reactor, commercial GF (4.0 cm × 1.0 cm × 0.2 cm) was soaked in a boiling mixture of 1:1 (v/v) HNO<sub>3</sub> and H<sub>2</sub>SO<sub>4</sub> in a fume hood. The GF was kept in the hot acid mixture for 5 min and then quickly immersed and stored in deionized water. This procedure was essential for obtaining good copper adhesion to the substrate and preserving its low electrical resistance.

**2.3. Copper Electrocatalyst Electrodeposition.** An electrochemical bath was prepared with a saturated CuSO<sub>4</sub> solution in 1 M citric acid. Then, the pH value was adjusted by adding sodium hydroxide (1 M) dropwise until it reached the desired pH value (2, 4, 6, 8, and 10). Using a two-electrode cell configuration, the oxidized GF (OGF) was immersed in the electrochemical bath, and 250 mA of a cathodic current was applied against copper foil at room temperature for 2 h. Subsequently, the Cu-OGF electrodes were rinsed with deionized water to remove all chemical residues.

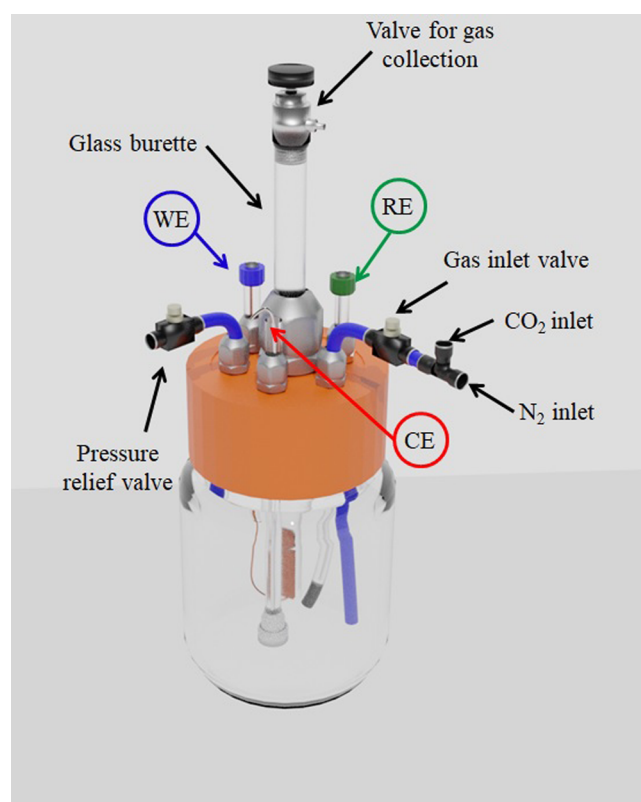
**2.4. Physical Characterization.** Scanning electron microscopy (SEM) images and energy-dispersive X-ray (EDX) elemental maps were acquired in a dual-beam FEI Scios microscope operating at 20.00 kV. Raman spectra were collected with a Witec Alpha 300 micro-Raman confocal microscope using a 532 nm excitation laser. X-ray diffraction (XRD) patterns were collected using a Shimadzu Lab X XRD6000 X-ray diffractometer equipped with a Cu Kα source (λ = 1.5406 Å).

**2.5. Electrochemical Instrumentation and Procedures.** The electrochemical experiments reported in this work were carried out at 25 °C in a three-electrode cell configuration using a 1010 B electrochemical workstation (Gamry, USA). The as-prepared Cu-OGF materials were used as working electrodes, while a platinum plate (1.0 cm × 1.0 cm × 0.1 mm) and Ag wire (0.1 mm) were used as the counter and pseudo-reference electrodes, respectively. To conduct the experiments, an H-shaped electrolysis cell with a Nafion

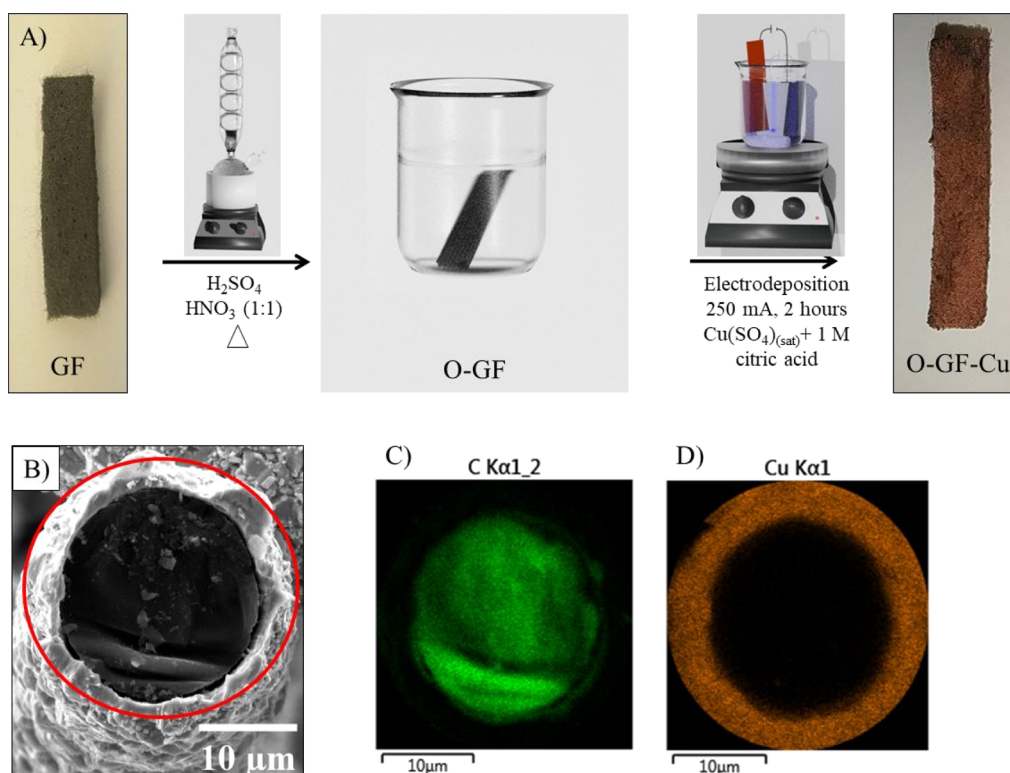
membrane was used. The membrane separates the anode and cathode compartments (Figure S1). Each compartment of the H-type cell was filled with 100 mL of 0.1 M NaHCO<sub>3</sub> and 0.1 M KCl and purged with high-purity gas (N<sub>2</sub> or CO<sub>2</sub>) for at least 30 min before electrochemical measurements. CO<sub>2</sub> RR polarization curves were obtained from −0.5 to −1.0 V versus reversible hydrogen electrode (RHE) at 1 mV·s<sup>−1</sup>. CO<sub>2</sub>RR and HER currents were measured by chronoamperometry from −0.58 to −0.84 V versus RHE. Electrochemical impedance spectroscopy (EIS) was recorded in the range of 20 kHz to 10 mHz in the potentiostatic mode at −0.68 V versus RHE, with 10 mV as the DC bias voltage. Finally, Gamry Echem Analyst was used for equivalent circuit modeling (ECM). All of the applied potentials are reported versus RHE potentials according to eq 1.

$$E \text{ (vs RHE)} = E_{\text{Ag/AgCl}} + E_{\text{ref}}^{\circ} - (0.0591 \times \text{pH}) \quad (1)$$

**2.6. Analysis of Electrolysis Products.** CO and CO<sub>2</sub> can be quickly and simultaneously quantified by FTIR in a gas analysis cell.<sup>34,35</sup> The specifications of the short-path gas cell are presented in Figure S2. The quantification was done by analyzing the spectra in absorbance and comparing the areas of the respective bands with the analytical curve with excellent correlation coefficients (Figure S3). To collect the gases generated in the electrolysis, CO<sub>2</sub>RR was performed in an electrochemical cell coupled with a volumetric gas compartment built from a glass burette, as shown in Figure 1. This electrochemical cell was specially designed to collect the evolved gases from the working electrode and inject them directly into the short-path FTIR gas cell for quantification. The electrochemical cell setup consists of Ag/AgCl(s) as the



**Figure 1.** Electrochemical cell used in the quantification of gaseous products generated by FTIR spectroscopy.



**Figure 2.** A) Graphic illustration of the GF-Cu electrode synthesis procedure. (B) SEM image of the GF-Cu cross-section and EDX maps of (C) carbon and (D) copper. The photographs were taken by M.E.G.W.

reference electrode, a platinum rod ( $d = 0.1$  cm) as the counter electrode (Figure S4), and the working electrode (Cu-OGF) positioned inside the cylindric chamber. Therefore, the presence of CO and CO<sub>2</sub> was quantified using a Thermo Scientific iS10 spectrometer. As no additional signals were detected, the remaining volume was assigned to H<sub>2</sub>.

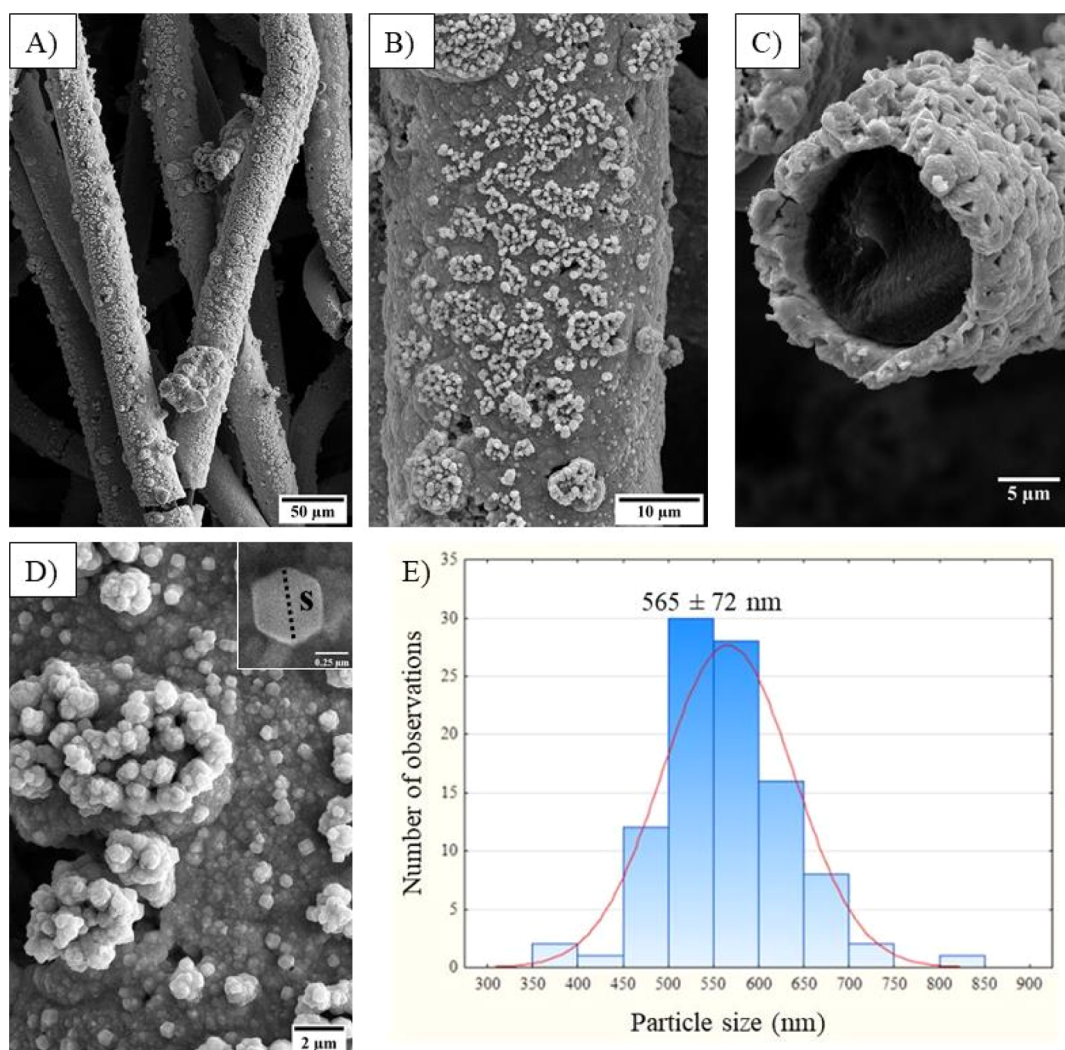
### 3. RESULTS AND DISCUSSION

In electrocatalysis, three-dimensional materials such as metals or carbonaceous foams have been used to obtain higher numbers of active sites per geometric area, either as catalysts or as supporting material. Through a two-step method, GF was successfully coated with metallic copper, as demonstrated in Figure 2. First, GF is oxidized by its immersion in a hot mixture of H<sub>2</sub>SO<sub>4</sub> and HNO<sub>3</sub> (1:1 v/v) (Figure 2A). This is necessary to make the substrate hydrophilic and thus to obtain good adhesion with copper microparticles. The change in hydrophilicity of GF with the surface treatment can be seen in Figure S5. Then, the oxidized-carbon felt was copper-coated by applying a 250 mA cathodic current for 2 h. SEM imaging coupled with EDX mapping revealed the achievement of copper-coated oxidized GF (Figure 2B–D).

**3.1. Physical Characterization.** Low-magnification SEM images of the electrode surfaces (Figures 3A,B and S6) revealed that the copper coating on oxidized GF occurred within a controlled process without affecting the fiber-like morphology. Moreover, the pH used for electrodeposition was a key factor in obtaining copper microstructures. This can be seen in the high-magnification SEM images of the materials' surfaces and by the cross-section micrographs (Figures 3C,D and S7 and S8). Therefore, the results indicate that morphology, particle sizes, roughness, and thickness of the copper layer can be tailored by the pH used. As an example,

the copper layer deposited was found to be in the range of 1.1 to 9.2  $\mu\text{m}$  (Table S1), as measured by the SEM images of the cross-section of the material (Figure S8). For the electrode deposited at pH 2 (Cu-OGF pH 2), hexagonal copper particles were found on the surface of the material (inset Figure 3D) with a size distribution of  $565 \pm 72$  nm (Figure 3E). The particle size distribution of the other electrodes is presented in Figure S9.

Raman spectroscopy was used to investigate changes in the GF structure caused by the surface treatment and for the characterization of copper oxides on the Cu-OGF pH 2 electrode (Figure 4A). The ratio of D (1352  $\text{cm}^{-1}$ ) and G (1580  $\text{cm}^{-1}$ ) bands ( $I_D/I_G$ ) of carbonaceous materials is used to evaluate defects in carbonaceous materials. Hence,  $I_D/I_G = 0.40$  was observed for GF, while  $I_D/I_G = 0.98$  for OGF. This significant increase in  $I_D$  is associated with the  $\text{sp}^2$  C–C bond breakage to form  $\text{sp}^3$  bonds.<sup>36</sup> This causes an increase in defects in the material, and therefore, the  $I_D/I_G$  reveals the high degree of defects caused by the surface treatment in the acid medium. For Cu-OGF pH 2, the Raman spectra revealed the presence of CuO at 280  $\text{cm}^{-1}$  and Cu<sub>2</sub>O at 330  $\text{cm}^{-1}$ , in addition to the carbonaceous D and G bands ( $I_D/I_G = 0.77$ ) (Figure 4A). The graphitic peaks were observed in the XRD pattern of the GF (Figure 3B). Hence, the most intense peak, and the one present in the other materials, is related to the (002) plane at  $2\theta = 26.4^\circ$ , while the less intense peaks at  $43.5$  and  $54.3^\circ$  refer to (100) and (004), respectively.<sup>37</sup> Cu<sub>2</sub>O (JCPDS 03-065-3288) diffraction peaks (111), (200), (220), and (311) were observed at  $36.7$ ,  $42.5$ ,  $61.5$ , and  $73.7^\circ$ , respectively, in the as-prepared Cu-OGF pH 2 (Figure 4B, Table S2). The presence of Cu<sub>2</sub>O and CuO, revealed by Raman spectroscopy and XRD, may be associated with the oxidation of copper due to atmospheric oxygen exposure. To

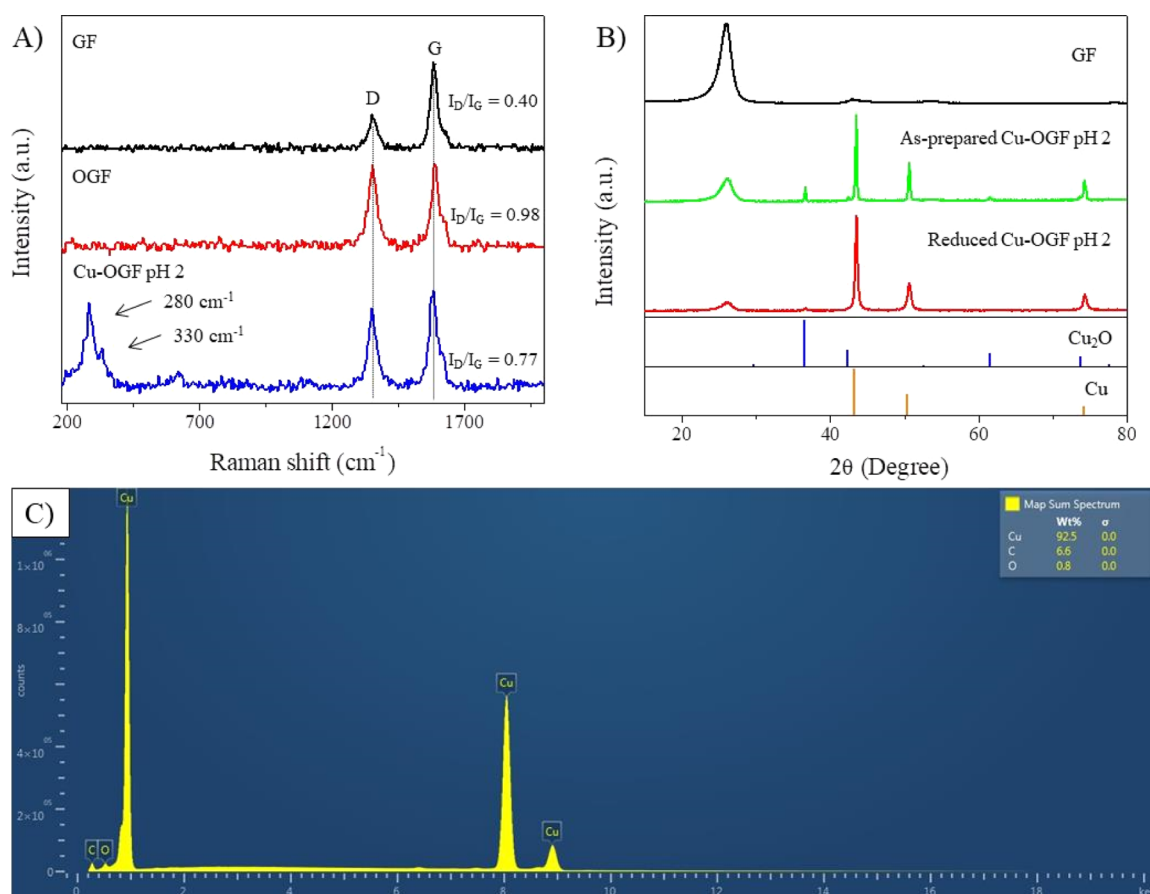


**Figure 3.** SEM results of the Cu-OGF pH 2 electrode. (A,B) Low-magnification images of the surface and (C) cross-section; (D) high-magnification image of the surface and (E) size distribution of copper particles on the surface.

understand the reduction that occurs in the first voltammetry cycles (Figure S10), the as-prepared Cu-OGF pH 2 electrode was subjected to five cycles of cyclic voltammetry in 0.1 M NaHCO<sub>3</sub> and 0.1 M KCl, N<sub>2</sub>-saturated and then characterized by X-ray diffraction. The XRD pattern of Cu-OGF reduced at pH 2 exhibited a single peak related to the (111) crystallographic plane of Cu<sub>2</sub>O with a relative intensity of 2.30% (Table S3). This incomplete reduction is similar to that seen in oxide-derived copper materials (OD-Cu). OD-Cu catalysts are formed by copper oxidation and subsequent reduction. Thus, the presence of residual oxides is believed to be responsible for the remarkable catalytic properties.<sup>9,38</sup> Additionally, the signals of cubic Cu(111), (200), and (220) were found at 43.6, 50.7, and 74.3°, respectively, in both as-prepared Cu-OGF pH 2 and reduced Cu-OGF pH 2 (JCPDS 00-004-0836). This suggests the deposition of polycrystalline copper on the surface of oxidized GF. EDX mapping was used to analyze the chemical composition of the Cu-OGF pH 2 surface (Figure 4C). The spectrum obtained revealed the presence of the elements Cu, C, and O at atomic ratios of 92.5, 6.6, and 0.8%, respectively, suggesting the Cu-rich surface of the fibers.

**3.2. CO<sub>2</sub>RR Performance.** Obtaining fuels from the electrochemical reduction of CO<sub>2</sub>, where electrical energy can be obtained from renewable sources, has attracted much

attention over the last decade. To this end, Cu-based materials have emerged as promising, cost-effective electrocatalysts for CO<sub>2</sub> reduction. Motivated by the high surface areas and different morphologies of copper particles, we investigated the catalytic activity of copper-coated oxidized GF in the electrochemical reduction of CO<sub>2</sub>. As shown in Figures 5A and S11A–D, all Cu-OGF electrodes exhibited catalytic responses for CO<sub>2</sub> superior to Cu-foam and the support material (OGF) (Figure S11E). However, the cyclic voltammograms showed significant differences in the onset potential and measured current. In both aspects, the Cu-OGF pH 2 electrode showed more promising results than others, that is, the lowest onset potential (−0.598 V for CO<sub>2</sub>RR) and the highest cathodic current (Figure 5A). This may be related to micro-structure control and the exposure of the particle edges. Changing the applied potential from −0.58 to −0.84 V versus RHE for 1 h resulted in a current variation from 8.7 μA to −1.88 mA in the absence of CO<sub>2</sub>, that is, only for HER (Figure 5B). Nevertheless, at the same applied potential range, the current variation obtained in the presence of CO<sub>2</sub> was −1.55 to −27.3 mA (Figure 5C), which indicates high catalytic activity. Moreover, for both HER and CO<sub>2</sub>RR, the current remained stable during the electrocatalysis at each given potential. In long-term chronoamperometry measurements,



**Figure 4.** Physical characterization. (A) Raman spectra of GF, OGF, and Cu-OGF pH 2; (B) XRD patterns of GF, as-prepared Cu-OGF pH 2, reduced Cu-OGF pH 2, Cu<sub>2</sub>O (JCPDS 03-065-3288), and Cu (JCPDS 00-004-0836); and (C) EDX spectra of the Cu-OGF pH 2 surface.

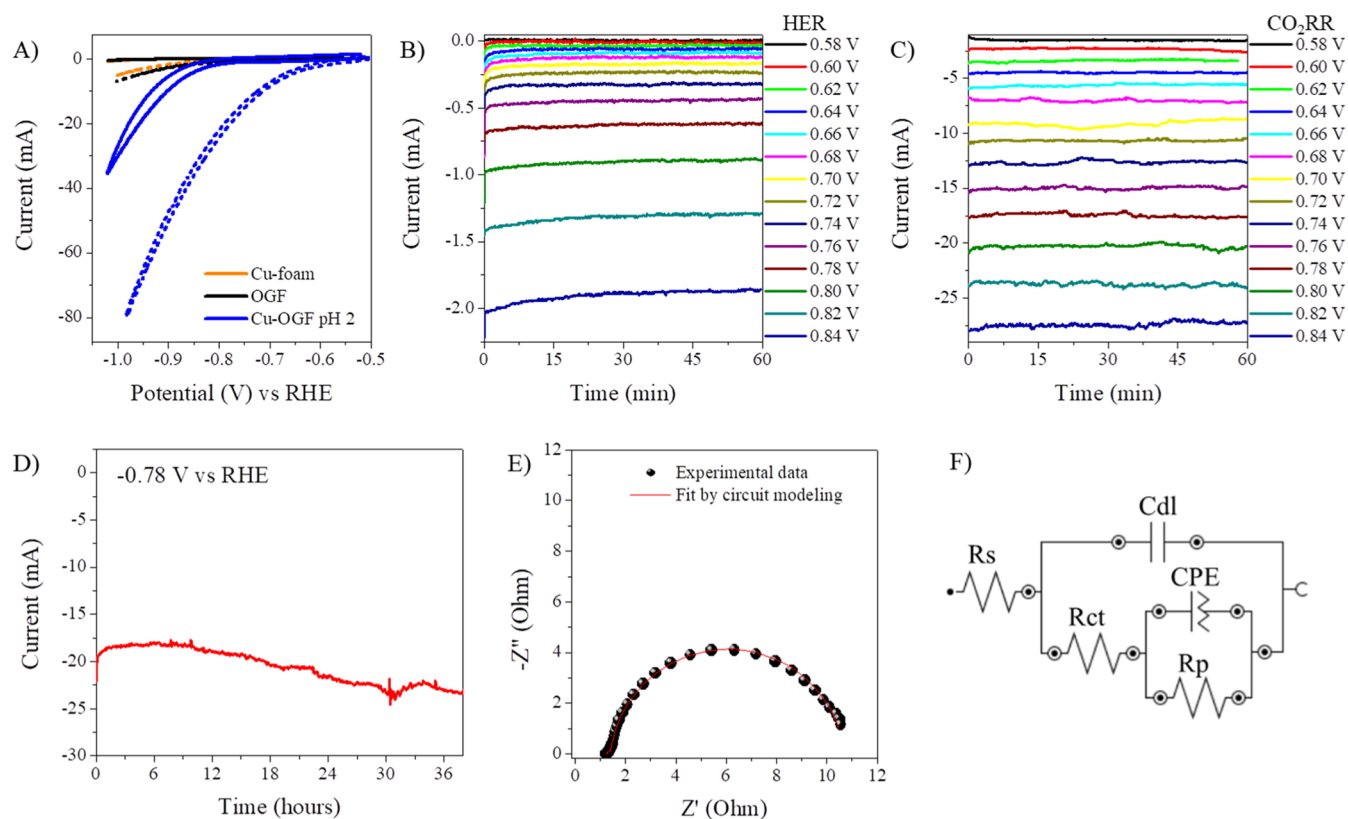
Cu-OGF pH 2 displayed excellent catalytic stability (Figure S4). Furthermore, as revealed by EIS and ECM (Figure S5,F), Cu-OGF pH 2 exhibited charge transfer and electrode polarization resistance of 0.198 and 9.239 Ω, respectively, at −0.68 V versus RHE. These values are significantly lower than those of the other Cu-OGF electrodes (Figure S12 and Table S4). All electrodes exhibited a low total impedance value (<28 Ω), which indicates good charge transfer between the Cu-oxidized GF interface and high catalytic activity. The adopted model circuit (Figure S5F) describes Faradaic reactions in the presence of one adsorbed species, in which,  $R_s$  is the electrolyte resistance,  $C_{dl}$  is the double layer capacitance,  $R_{ct}$  is the charge transfer resistance, CPE is the constant phase element (a non-ideal capacitor or a pseudocapacitance), and  $R_p$  is the electrode polarization resistance.<sup>39</sup>

### 3.3. Product Characterization and Faradaic Efficiency.

Selectivity is a big issue in CO<sub>2</sub>RR, as the formation of complex reduction products is possible, from C1 products to C2 and C3. As the focus of this work was the production of CO, the characterization of the generated gases was performed by FTIR in a short-path gas cell. Cu-OGF pH 2 was highly selective in reducing CO<sub>2</sub> and H<sub>2</sub>O to gaseous products CO and H<sub>2</sub>. Figure 6A shows the FTIR spectra of the gases generated at potentials of −1.00 to −1.35 V—no CO was detected above −1.00 V. The areas of CO (2226–2020 cm<sup>−1</sup>, Figure 6B) and CO<sub>2</sub> (2393–2227 cm<sup>−1</sup>, Figure 6C) absorbance signals were used for quantifying the CO produced and for calculating the FE. Carbon dioxide was present due to the non-Faradaic processes involved, such as desorption at the electrode surface.

The difference between the total volume of gas produced and the volumes of CO and CO<sub>2</sub> was assumed to be the volume of H<sub>2</sub>, as no other signals appeared in the FTIR spectrum (Figure 6A). The chronoamperometry curves are shown in Figure S13, and the data used to calculate the FE are presented in Table S5. From −1.00 to −1.35 V versus RHE, CO was produced with a FE of 0.58 to 3.54%, while H<sub>2</sub> had a FE of 50.87 to 85.58%, resulting in a total FE of 52.79 to 86.17% (Figure 7A), suggesting the presence of products in the liquid phase. Interestingly, even at higher potentials (more negatives than −1.25 V vs RHE), there was no detection of methane, which is the main CO<sub>2</sub>RR product reported for polycrystalline copper under these conditions.<sup>3,40</sup> However, by performing constant current measurements, the total FE toward CO and H<sub>2</sub> were improved to 92.00% at −10.0 mA and 100.25% at −7.5 mA (Figure 7B). Although the efficiency was very high for H<sub>2</sub>, the high overpotential for HER does not make it a good catalyst for H<sub>2</sub>. The FTIR spectra of the constant current measurements, the chronopotentiometry curves, and the data for calculating the FE are shown in Figure S14 and Table S6.

After finding the highest efficiency conditions (−1.15 V vs RHE for constant potential and −2.5 mA for constant current), we studied the performance and selectivity in long-duration measurements (at least 24 h). At −1.15 V versus RHE, the total evolved gas volume was 35.00 mL, resulting in five injections to the short-path gas analysis cell, in which the FE toward CO was initially 2.67% and decreased to 1.72% by the end of the experiment, while toward H<sub>2</sub>, it dropped from 97.03 to 81.29% (Figures 7C, S15, and Table S7). For comparison, at



**Figure 5.** Catalytic performance of the Cu-OGF pH 2 in the electroreduction of  $\text{CO}_2$ . (A) Cyclic voltammograms in  $\text{N}_2$ -saturated and  $\text{CO}_2$ -saturated 0.1 M  $\text{NaHCO}_3$  and 0.1 M KCl aqueous solutions. The scan rate was  $1 \text{ mV}\cdot\text{s}^{-1}$ . Chronoamperometric currents at different applied voltages in (B)  $\text{N}_2$ -saturated 0.1 M  $\text{NaHCO}_3$  and 0.1 M KCl and (C)  $\text{CO}_2$ -saturated 0.1 M  $\text{NaHCO}_3$  and 0.1 M KCl. (D) Long-term chronoamperometry at  $-0.78 \text{ V}$  vs RHE in  $\text{CO}_2$ -saturated 0.1 M  $\text{NaHCO}_3$  and 0.1 M KCl. (E) Nyquist diagram collected at  $-0.68 \text{ V}$  vs RHE in  $\text{CO}_2$ -saturated 0.1 M  $\text{NaHCO}_3$  and 0.1 M KCl and (F) model circuit used in the simulations.

$-2.5 \text{ mA}$ , the total volume of produced gas was  $41.30 \text{ mL}$  and divided into eight FTIR measurements. Initially, the FE of CO was  $4.88\%$  in the first analysis, reaching the maximum in the second ( $5.21\%$ ) and decreasing to  $3.70\%$  at the end of the experiment (Figures 7D, S16, and Table S8).

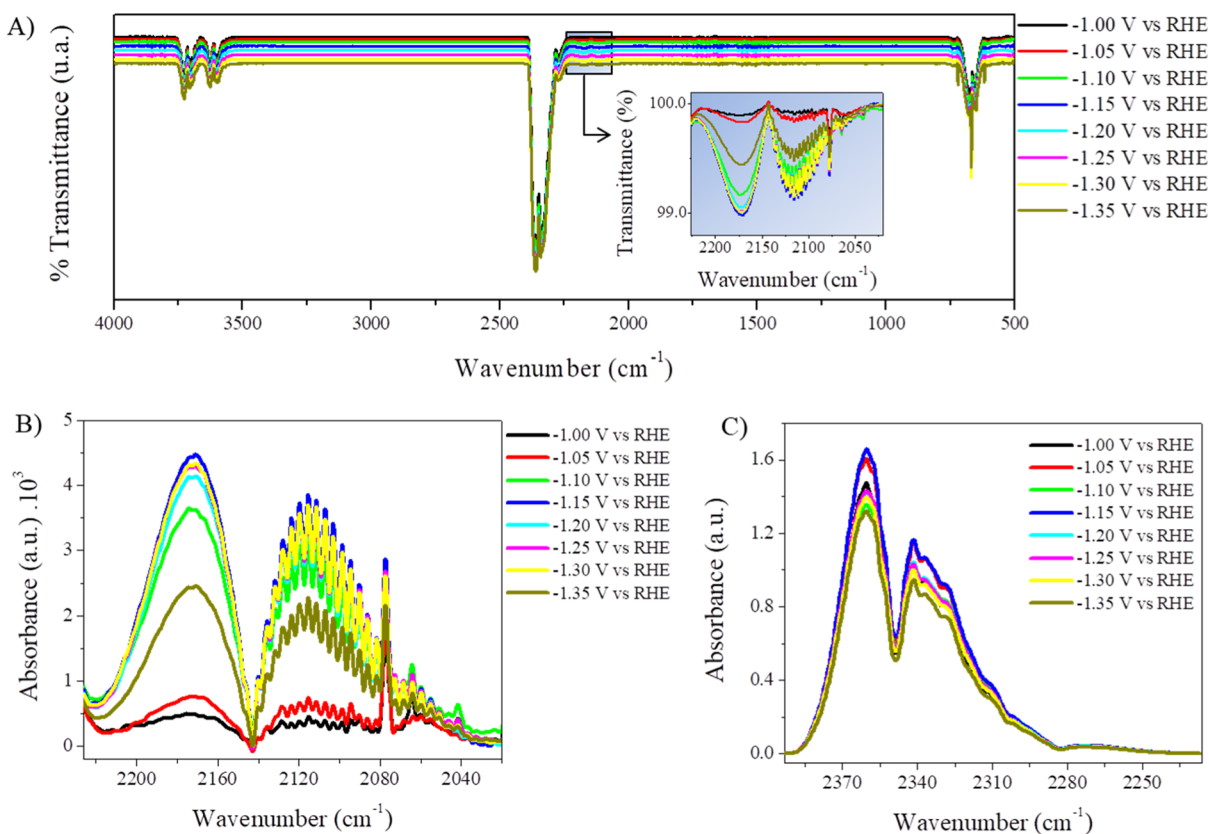
The found FE for CO ( $5.21\%$ ) is a significant value since the bulk Cu electrode gives a value of only  $1.3\%$ , exhibiting higher efficiencies for  $\text{CH}_4$  ( $33.3\%$ ) and ethylene ( $25.5\%$ ).<sup>40</sup> Compared to Cu-foam, this result was even superior ( $0.55\%$  for CO and  $3.19\%$  for  $\text{H}_2$ ) (Figure S17 and Table S9). Also, the selectivity of the Cu-OGF pH 2 electrode for CO and  $\text{H}_2$  was not expected since copper is a metal capable of producing a wide range of products from  $\text{CO}_2\text{RR}$ . For example, Kuhl and co-workers reported obtaining 16 products using copper foil as the working electrode, including the gaseous products carbon monoxide, methane, and ethylene.<sup>3</sup> Similarly, Wu and co-workers deposited Cu dendrites on carbon paper, and it showed to be active for the production of the same gaseous species.<sup>41</sup> In our experiments, only CO was detected, similar to Kumar and co-workers' results but applying pulsed-bias electrolysis.<sup>24</sup> The selectivity for syngas in DC electrolysis was recently reported by Wang and co-workers on copper and copper oxide electrodes.<sup>9</sup> They showed high efficiency for CO and  $\text{H}_2$ , but the total FE was around  $80\%$ . Although the maximum FE to CO and  $\text{H}_2$  was  $5.21$  and  $88.80\%$ , respectively, the present work reports a simple and inexpensive strategy for obtaining electrodes capable of transforming  $\text{CO}_2$  and  $\text{H}_2\text{O}$  to CO and  $\text{H}_2$  (with a total FE close to  $100\%$ ), which can be used as fuel gas or enriched with CO to achieve suitable  $\text{H}_2/\text{CO}$

ratios for the synthesis of chemicals by Fischer–Tropsch processes.

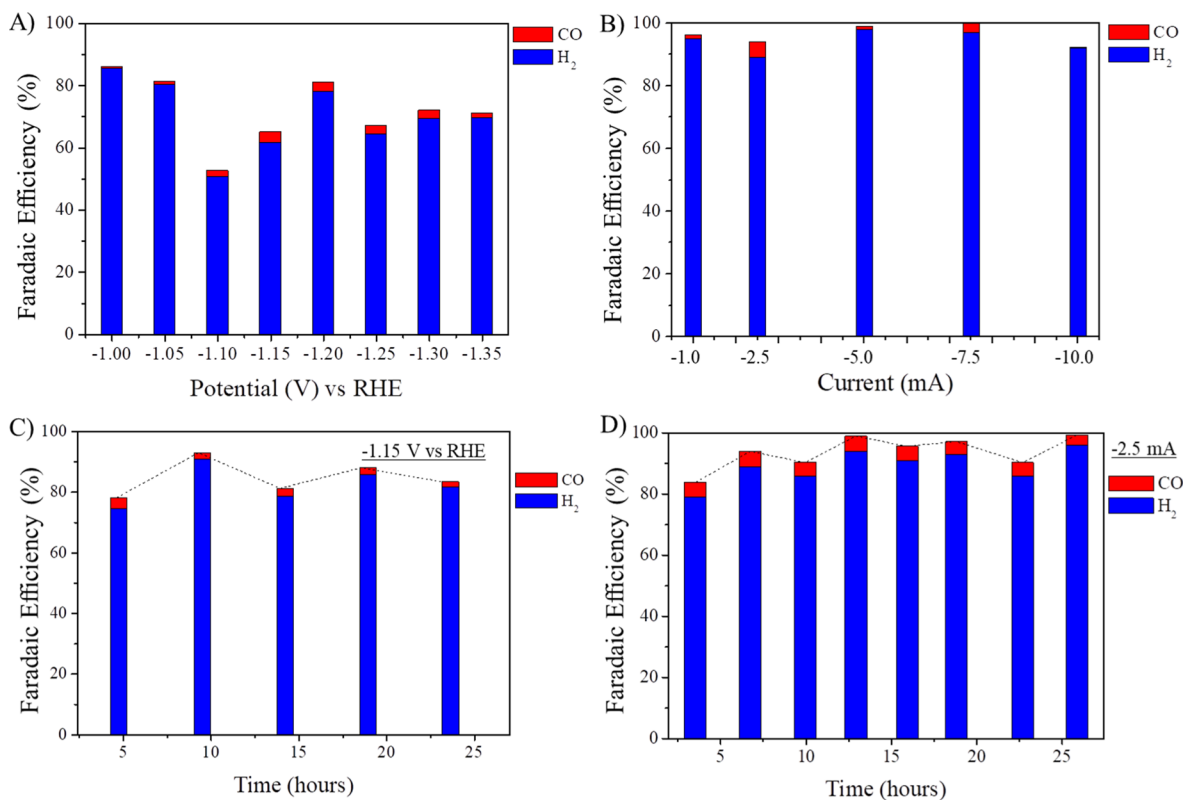
To understand the loss of electrode efficiency, the post-electrolysis electrode surface was characterized by SEM, EDX mapping, and Raman spectroscopy. SEM micrographs revealed restructuring of the electrode surface, such as the loss of hexagonal morphologies and oxidation (Figures 8A and S18). EDX mapping indicated a copper-rich surface with the presence of oxygen (Figure 8B,C), and the increase in the oxygen signal can be seen in Figure S19. The Raman spectrum revealed that the increased oxygen amount is attributable to the oxidation of copper particles to  $\text{Cu}_2\text{O}$ , as denoted by the appearance of the  $224 \text{ cm}^{-1}$  signal (Figure 8D). The processes of surface restructuring and copper oxidation are two well-known electrode deactivation phenomena.<sup>14,40,42</sup>

#### 4. CONCLUSIONS

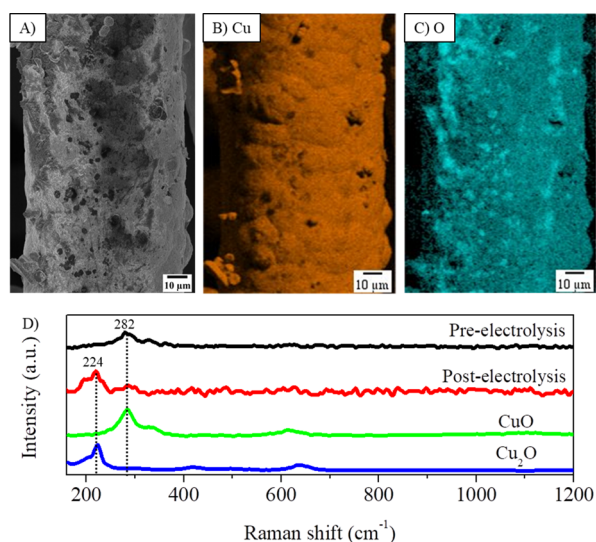
Here, a synthetic strategy has been developed to prepare copper-coated oxidized GF electrodes. A series of characterization techniques were used to study the detailed structure of the copper layer. The morphologies of copper particles, the width of the copper layer, and the particle sizes were found to be related to the pH used in the deposition. The highest performance was obtained by the electrode prepared at pH 2, reaching the lowest onset potential and the highest measured current. This could be explained by the better control of the microstructures of particles and the exposure of their edges. FTIR-assisted electrochemical measurements were performed with this electrode at a constant potential (from  $-1.00$  to



**Figure 6.** (A) FTIR spectra from 4000 to 500  $\text{cm}^{-1}$  of the gases produced at different potentials (inset: 2226–2020  $\text{cm}^{-1}$ ); (B,C) absorption regions of carbon monoxide and carbon dioxide, respectively.



**Figure 7.** CO and H<sub>2</sub> FE of Cu-OGF pH 2 in saturated sodium bicarbonate solution and CO<sub>2</sub> flux at different (A) potentials and (B) currents and in long-duration measurements at optimized (C) potential and (D) current.



**Figure 8.** Physical characterization of the post-electrolysis Cu-OGF pH 2 electrode. (A) SEM micrograph; (B,C) EDX mapping of Cu and O elements, respectively; and (D) Raman spectra.

−1.35 V vs RHE) and current (−1.0, −2.5, −5.0, −7.5, and −10 mA). It was found that the FE was between 0.50 and 5.21% for CO and 50.87 and 98.30 for H<sub>2</sub>, according to experimental conditions. Therefore, the produced gas mixture can be used as a fuel gas, or it can be CO-enriched for Fischer–Tropsch processes.

## ■ ASSOCIATED CONTENT

### SI Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acsomega.2c05486>.

Additional experimental details, methods, FTIR spectra, SEM images, particle size distribution, cyclic voltammograms, Nyquist diagrams, chronoamperometry curves, and data acquired for FE calculations (PDF)

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## Notes

The authors declare no competing financial interest.

## ■ ACKNOWLEDGMENTS

The authors are thankful for the financial support from the Coordenação de Aperfeiçoamento de Pessoal de Nível Superior, the Conselho Nacional de Desenvolvimento Científico e Tecnológico, Brazil (Proc. nos. 429548/2018-4 and 311517/2020-0), and Instituto Nacional de Ciência, Tecnologia e Inovação em Materiais Complexos Funcionais (INOMAT-Proc. no. CNPq 573644/2008-0). The authors would also like to thank the Complexo de Centrais de Apoio à Pesquisa (COMCAP) and Financiadora de Estudos e Projetos (Finep) for their instrumental support.

## ■ ABBREVIATIONS

- CO, carbon monoxide
- CO<sub>2</sub>, carbon dioxide
- CuSO<sub>4</sub>, copper sulfate
- CO<sub>2</sub>RR, carbon dioxide reduction reaction
- Cu-OGF, copper-coated oxidized graphite felt
- Cu-OGF pH 2, copper-coated oxidized graphite felt deposited at pH 2
- Cu-OGF pH 4, copper-coated oxidized graphite felt deposited at pH 4
- Cu-OGF pH 6, copper-coated oxidized graphite felt deposited at pH 6
- Cu-OGF pH 8, copper-coated oxidized graphite felt deposited at pH 8
- Cu-OGF pH 10, copper-coated oxidized graphite felt deposited at pH 10
- ECM, equivalent circuit modeling
- EDX, energy dispersive X-ray
- EIS, electrochemical impedance spectroscopy
- HER, hydrogen evolution reaction
- HNO<sub>3</sub>, nitric acid
- H<sub>2</sub>SO<sub>4</sub>, sulfuric acid
- H<sub>2</sub>, hydrogen
- H<sub>2</sub>O, water
- FE, Faradaic efficiency
- FTIR, Fourier transform infrared
- GF, graphite felt
- OGF, oxidized graphite felt
- N<sub>2</sub>, nitrogen gas
- RHE, reversible hydrogen electrode
- SEM, scanning electron microscopy
- XRD, X-ray diffraction

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