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Supplementary Materials for

Photocatalytic production of ethylene and propionic acid from plastic waste by titaniasupported atomically dispersed Pd species

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Figs. S1 to S18 Tables S1 to S10 References

Fig. S1. Morphology characterizations. High-resolution transmission electron microscopy (HRTEM) images of (**A**) TiO² and (**B**) Pdn-TiO2. High-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) images of (**C**) TiO₂ and (**D**) Pd_n-TiO₂.

Fig. S2. Nitrogen (N2) adsorption analysis. (**A**) N² adsorption-desorption isotherms and (**B**) the corresponding pore size distributions for Pd_1-TiO_2 and Pd_n-TiO_2 .

Fig. S3. Atomic structure characterizations. (**A**) Pd K-edge X-ray absorption near edge structure spectra and (**B**) Fourier-transformed k^2 -weighted extended X-ray absorption fine structure (EXAFS) spectra for Pd foil, PdO and Pd₁-TiO₂.

fig. S3B exhibits a shoulder for PdO reference, which is closely aligned with the Pd foil. The EXAFS fitting in table S2 indicates that the shoulder peak can be assigned to Pd-Pd coordination.

Fig. S4. CO adsorption diffuse reflectance infrared Fourier transform spectroscopy (DRIFTS) spectra. (A) Pd_1 -TiO₂ and **(B)** Pd_n -TiO₂.

Fig. S5. Pd 3d X-ray photoelectron spectroscopy (XPS) spectra. (A) Pd_n-TiO_2 and (B) Pd_1 -TiO2.

Fig. S6. C² hydrocarbon (C2Hx) production for bare TiO² and a series of TiO² catalysts modified with metal species following 3 h of photoreaction.

Fig. S7. Characterization of Pd1-TiO2-0.5 and Pd1-TiO2-2. (**A**) X-ray diffraction (XRD) patterns for TiO₂, Pd₁-TiO₂-0.5 and Pd₁-TiO₂-2. (**B**) CO adsorption DRIFTS spectra of Pd₁-TiO₂-0.5 and Pd1-TiO2-2. (**C**) HAADF-STEM image and (**D**) Energy dispersive spectroscopy **(**EDS) mapping of Pd₁-TiO₂-0.5. (**E**) HAADF-STEM image and (**F**) EDS mapping of Pd₁-TiO₂-2.

The XRD patterns for $Pd_1-TiO_2-0.5$ and Pd_1-TiO_2-2 exhibit the diffraction peaks for anatase TiO_2 without Pd-related features (fig. S7A). For the CO adsorption, a typical band for linearly adsorbed CO is observed at $2050 \sim 2150 \text{ cm}^{-1}$ (fig. S7B). The result indicates the atomic dispersion of Pd species on $Pd_1-TiO_2-0.5$ and Pd_1-TiO_2-2 . This is also confirmed by the HAADF-STEM images (fig. $S7$, C to F), in which atomic Pd sites are dispersed on TiO₂ nanosheets.

Fig. S8. Control experiments. (**A**) Summary of experimental control conditions for photocatalytic substrate oxidation over Pd₁-TiO₂. (**B**) Photocatalytic generation of C_2 hydrocarbons on Pd₁-TiO₂ by converting succinic acid in the presence of tert-butanol or by using different starting substrates such as propionic acid, CO_2 , and ethane (C_2H_6) . C_2 hydrocarbon production is expressed per mass of photocatalyst.

Fig. S9. Material characterization of the post-reaction sample. (**A**) XRD pattern, (**B**) Pd 3d XPS spectra, (**C**) HRTEM and (**D**) HAADF-STEM images of Pd₁-TiO₂.

Fig. S10. Pd 3d XPS spectrum of the recovered Pd1-TiO² after illumination and vacuum drying.

Fig. S11. UV-vis absorption spectra of succinic acid substrate solution, diluted PE decomposition solution, and pure polyethylene (PE) decomposition solution.

Fig. S12. The PE-to-single product (C2H⁴ or propionic acid) conversion achieved via oxidation-photocatalysis and high-temperature thermocatalysis. Catalysts and reaction processes for reported data are as follows: Y zeolite pyrolysis (*72*), HZSM-5 pyrolysis (*73*), Al(OH)³ pyrolysis (*74*), HZSM-11 pyrolysis (*75*), blend with naphtha for pyrolysis-steam cracking (*76*), biomass co-gasification (*77*), HZSM-5 pyrolysis-steam cracking (*78*), non-catalysis pyrolysis (*79*) and microwave assisted chemical oxidation (*80*).

Selected reports on thermocatalytic conversion of plastic waste into C_2H_4 /propionic acid were added in fig. S12 for comparison with our low-temperature oxidation-photocatalysis. Pyrolysis of PE waste requires high temperatures (>450 °C) and yields the major products of C_5-C_{20+} hydrocarbons as well as C_1-C_4 hydrocarbons. High temperatures, fluidized bed systems and catalysts were explored to improve C_2H_4 recovery. Gasification of PE is conducted at >600 $^{\circ}$ C to convert carbon-based feedstocks into primarily gaseous products. Steam gasification of PE has been reported to produce C_2H_4 at relatively high temperature (900 °C). Two step processes, including gasification-FT synthesis, pyrolysis-steam cracking, can achieve a high yield of light olefins. Propionic acid has been rarely reported to be generated from PE waste. Microwaveassisted chemical oxidation of PE yields a series of carboxylic acids including a portion of propionic acid.

Fig. S13. Energy band structure characterizations. (**A**) Mott-Schottky (MS) plot, (**B**) XPS valence band (VB) spectrum and (**C**) schematic for energy band structure for TiO2. (**D**) MS plot, (**E**) XPS VB spectrum and (**F**) schematic for energy band structure for Pd_1-TiO_2 .

Fig. S14. Transient surface photovoltage spectrum for Pdn-TiO2.

Fig. S15. XPS spectra. (**A**) An enlarged view of Pd 3d XPS spectrum and (**B**) O 1s XPS spectrum for Pd_1-TiO_2 in dark and under illumination.

Fig. S16. DRIFTS characterizations. DRIFTS spectra for different concentrations of (**A**) succinic acid and (B) propionic acid on Pd_1-TiO_2 in the dark. (C) In situ DRIFTS spectra for the substrate conversion on Pd_n-TiO₂.

Fig. S17. Electron paramagnetic resonance (EPR) charcaterizations. (**A**) In situ EPR spectra for TiO² with and without reaction substrates under light irradiation. (**B**) In situ EPR spectra for hydroxyl radical (\cdot OH) detection over TiO₂, Pd₁-TiO₂ and Pd_n-TiO₂ without reaction substrates under light irradiation.

Fig. S18. XPS spectra. (A) C 1s XPS spectra for Pd₁-TiO₂ before and after photoreaction. (**B**) In situ high-resolution Pd 3d XPS spectra for Pd₁-TiO₂ with the substrate and illumination.

Sample	Pd $(wt. \%)$	Surface area $(m^2 g^{-1})$	Average pore size (nm)
Pd_1-TiO_2	0.64	176	9.9
Pd_n-TiO_2	0.70	199	10.7

Table S1. Physicochemical properties of Pd1-TiO² and Pdn-TiO2.

Table S2. EXAFS fitting results for Pd1-TiO² and PdO. CN is the coordination number, R distance between absorber and backscatter atoms and σ^2 Debye-Waller factor.

Sample	Shell	CN	$\mathbf{R}(\mathbf{A})$	$\sigma^2(\AA^2)$
Pd_1 -TiO ₂	Pd-O	2.9	2.05	0.006
	Pd-Pd	3.0	2.75	0.011
	Pd-Ti	2.1	2.94	0.012
PdO	$Pd-O$	1.8	2.02	0.003
	Pd-Pd (shoulder)	1.1	2.92	0.004
	Pd-Pd	0.8	2.96	0.002

Table S3. Photocatalytic generation of C² hydrocarbons from succinic acid substrate at different pH values over Pd1-TiO2.

pH value	C_2H_4 production $(\mu \text{mol g}_{cat}^{-1} \text{h}^{-1})$	C_2H_6 production $(\mu \text{mol g}_{cat}^{-1} \text{h}^{-1})$	
	192.51	124.04	
$\overline{4}$	531.16	501.84	
7	4.59	6.85	
10	N/A	N/A	

Temperature $({}^{\circ}C)$	C_2H_4 production $(\mu \bar{m} \bar{d} g_{cat}^{-1} h^{-1})$	C_2H_6 production (μ mol g_{cat}^{-1} h ⁻¹)
30	531.16	501.84
50	498.41	440.06
70	444.88	417.24

Table S4. Photocatalytic generation of C² hydrocarbons from succinic acid substrate over Pd1-TiO² at 30^oC, 50^oC and 70^oC.

Table S5. Inductively coupled plasma optical emission spectrometry. The Pd loading in Pd1- TiO² before and after photoreactions.

Table S6. The amounts of H² and CO² evolved. Photocatalytic substrate conversion over TiO2, Pd₁-TiO₂ and Pd_n-TiO₂ following 3 h light irradiation.

Table S7. Solar-driven upcycling of plastic waste for selected state-of-the-art catalysts.

Generation of valuable major products are included.

Selected reports on photocatalytic treatment of plastic waste are added in table S7, including (1) plastic photoreforming, (2) chemical oxidation-decarboxylation, (3) photocatalytic degradation- $CO₂$ reduction as well as (4) homogeneous catalytic C-C/C-H activation. (1) Photoreforming of plastic waste involves: i) decomposition of plastic waste into monomers; ii) photocatalytic hydrogen evolution coupled with oxidation of monomers into oxygenates. Advanced CdS-based photocatalysts exhibit excellent performance with a hydrogen evolution of \sim 40 mmol g_{cat}^{-1} h⁻¹. However, the oxidation reaction still suffers from low selectivity towards a single high-value product and overoxidation to $CO₂$. (2) The reported PE upcycling via chemical oxidationdecarboxylation represents an emerging strategy to simultaneously generate valuable light olefins and single carboxylic acid with high selectivity. Side products generated from chemical oxidation may compete with the main reaction and reduce its activity. (3) One-pot photodegradation coupled with CO₂ reduction can decompose plastic waste with a conversion of nearly 100%, while enabling CO² photoreduction. The two-step process can be carried out under mild conditions, but generally requires tens of hours of irradiation to achieve complete decomposition of plastic waste. (4) Upcycling of aromatic polymers has been reported using homogeneous photocatalysts and $O₂$. Photo-driven hydrogen atom transfer followed by C-C cleavage enable the direct conversion of plastic waste into aromatic oxygenates with high yields (> 40%). Organic solvents are employed to dissolve plastics but make the reaction system complex and toxic.

Additionally, other solar-driven chemical recycling methods are also reported in table S7, including photo-biocatalysis, photothermal catalysis and photoelectrocatalysis. The biotic-abiotic hybrid methanation of microplastics exhibits excellent stability (up to 4 months) and high selectivity to CH₄, but the CH₄ yield needs to be improved. Photothermal catalysis can utilize sunlight to heat up the reaction system and boost plastic conversion, but it also aggravates overoxidation. The photothermal effect is a promising strategy that can be applied to thermocatalytic plastic conversions. The current studies on photoelectrocatalysis focus on the reforming of plastics into H_2 and chemicals. Compared to photoreforming, plastic monomer oxidation on the photoelectrode surface can be regulated to achieve high selectivity (up to 90%) to a single valuable oxygenate.

	Concentration (5-fold diluted) (mg mL^{-1})			
Conditions	Succinic acid	Acetic acid	Glutaric acid	Adipic acid
160° C 8 h	1.98	0.30	0.89	0.01

Table S8. Quantification of components of PE decomposition solution following pretreatment.

Table S9. C² hydrocarbon evolution on Pd1-TiO² in PE solutions with ultrapure water, seawater, rainwater, and simulated nitric acid wastewater as solvents. C₂ hydrocarbon production is expressed per mass of photocatalyst.

Sample	Solvent	C_2H_4 production (μ mol gcat ⁻¹ h ⁻¹)	C_2H_6 production (μ mol g _{cat} ⁻¹ h ⁻¹)
Pd_1-TiO_2	Ultrapure water	23.28	32.73
	Seawater	13.65	19.16
	Rainwater	15.42	18.80
	Simulated wastewater	17.85	20.20

Table S10. Pd 3d5/2 XPS of Pd1-TiO² in dark and under illumination.

Samples	Peak	Positions (eV)	FWHM	Percentage
In dark	Pd^0	336.20	2.00	68%
	Pd^{2+}	337.42	1.90	32%
Light irradiation	Pd^0	336.18	2.00	73%
	Pd^{2+}	337.40	1.90	27%

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