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S1. Experimental Section

S1.1. Chemicals

Methanol (≥ 99.5%), *N*, *N*-Dimethylformamide (DMF, ≥ 99.8%), isopropanol (≥ 99.5%), and *N*-methyl-2 pyrrolidone (NMP, 99.9%) were obtained from Makclin Chemistry (Shanghai, China). Zinc acetate dihydrate $(Zn(OAc)_2·2H_2O, 99%)$, 2-methylimidazole (MeIm, 98%) and sodium molybdate (Na₂MoO₄, 99%) were purchased from Aladdin Chemistry (Shanghai, China). Polyvinylidene fluoride (PVDF 6020), carbon black (Super P), and Nafion solution (5 *wt.*%) were provided by Sigma-Aldrich (Merck, Shanghai, China). Bulk molybdenum carbide (MoC, 99.95%) for the comparison was obtained from Aladdin Chemistry (Shanghai, China). All chemicals were used as purchased without further processing.

S1.2. Construction of ZIF-8 RDs

For a typical synthesis of ZIF-8 RDs [S1, S2], 1.0 mmol (219.5 mg) of $Zn(OAc)$; 2H₂O was dissolved into 10 mL of ultrapure water to form a homogeneous Zn^{2+} solution. 10 mmol (821.1 mg) of MeIm was dissolved into 10 mL of ultrapure water to prepare another solution. The Zn^{2+} solution was quickly added into the MeIm solution. After vigorously stirring for 5 min, the mixture solution was kept at room temperature for 24 h to obtain the white precipitates. The white precipitates were separated by centrifugation and thoroughly washed with water and methanol for several times, and dried in vacuum oven at 60 °C overnight to harvest ZIF-8 RDs.

S1.3. Preparation of MOF/MoO4-x

MOF/MoO₄-*x* (*x* stands for the mass ratio of Na₂MoO₄ to ZIF-8, $x=0.25, 0.5$, and 1) were prepared according to the previous report [S1] with some modifications. Briefly, 200 mg of the ZIF-8 RDs were ultrasonically dissolved into 20 mL of DMF. Following this, 100 mg of $Na₂MoO₄$ with the mass ratio of 0.5 was added into the above ZIF-8 RDs solution to synthesis $MOF/MoO₄-0.5$. Under stirring for 20 min, the mixture solution was transferred into a Teflon-lined stainless steel autoclave and kept at 150 ℃ for 6 h. After cooling down to ambient temperature, the $MOF/MoO₄-0.5$ was collected by centrifugation and washed by DMF and methanol for several times, and finally dried in vacuum oven.

Another two amounts of Na_2MoO_4 (50 and 200 mg) with the mass ratios of 0.25 and 1 were also added into the ZIF-8 RDs solution (200 mg in DMF) for the construction of MOF/MoO₄-0.25 and MOF/MoO₄-1 by using the similar procedures as described above, respectively.

S1.4. Synthesis of NC/MoyC-x

The above MOF/MoO₄-*x* precursors were placed into a ceramic boat and thermally carbonized under nitrogen gas flow in a tube furnace, yielding NC/Mo_{*v*}C-*x* (*y* represents the atomic ratio of Mo to C, $y=1$ or 2; *x* stands for the mass ratio of Na_2MoO_4 to ZIF-8, $x=0.25$, 0.5, and 1). During the carbonization process, the MOF/MoO₄-*x* were firstly heated from room temperature to 400 °C with a heating rate of 2 °C min⁻¹ and keep for 3 h. Subsequently, the temperature was further improved from 400 to 800 ℃ with the same heating rate (2 ℃ min-1) and also kept for another 3 h. After cooling down to room temperature, the NC/Mo*y*C-*x* products were obtained. Specifically, the MOF/MoO₄-0.25 and MOF/MoO₄-0.5 precursors were converted into NC/MoC-0.25 and NC/MoC-0.5 with the single-phased MoC nanocrystals, while the MOF/MoO₄-1 precursor was transformed to the dual-phased NC/MoC/Mo₂C-1 after the thermal pyrolysis [S1-S3]. For comparison, ZIF-8 RDs were pyrolyzed to yield the carbonaceous materials, denoted as ZIF-8-C.

S1.5. Characterizations

The structure and morphology of the MOF/MoO4-*x* and NC/Mo*y*C*-x* were observed by field emission scanning electron microscopy (SEM, Hitachi SU-8000, Japan) with an accelerating voltage of 10.0 kV. Transmission electron microscopy (TEM), high-resolution TEM (HRTEM) images, and elemental mapping analysis were performed using a JEM-2100F (JEOL, Japan) operated at 200 kV. X-ray photoelectron spectroscopy (XPS) spectra were collected on a PHI Quantera SXM (ULVAC-PHI, Japan) instrument with an Al K*α* radiation, and the binding energies were calibrated by referencing them to the C 1*s* (284.5 eV) binding energy. X-ray diffraction (XRD) patterns were examined by using a Rigaku Rint 2000 X-ray diffractometer (Tokyo, Japan) with monochromatic Cu Kα radiation (40 kV, 40 mA) at a scanning rate of 2° min⁻¹. Nitrogen adsorptiondesorption isotherms were obtained by using an Autosorb-iQ Automated Gas Sorption System (Quantachrome, USA) at 77 K. The specific surface area was evaluated by the multipoint Brunauer-Emmett-Teller (BET) method based on the adsorption data. The pore-size distributions were calculated from the adsorption branches of isotherms based on the density functional theory method. Fourier-transformed infrared spectra (FT-IR) were obtained using a Bruker Alpha spectrometer (Ettlingen, Germany) in the range of 500- 2000 cm⁻¹. The concentration of NaCl solution was continuously measured by a REX DDSJ-308F conductivity meter (INESA Scientific Instrument, Shanghai, China).

S1.6. Electrocatalysis measurements

All electrochemical measurements were carried out in 1 M NaCl aqueous electrolyte at room temperature with a three-electrode system on Chenhua CHI 760E electrochemical workstation (Shanghai, China). The Pt/C electrode and KCl-saturated Ag/AgCl were adopted as counter electrode and reference electrode, respectively. The working electrode slurry was prepared by ultrasonically dispersing 2 mg of as-synthesized samples in a mixed solution consisting of 950 µL of isopropanol and 50 µL of Nafion solution (5.0 *wt*.%).

The specific capacitances (C, F, g^{-1}) are calculated by the following eqn [1] from the GCD curves [S4, S5]:

$$
c = \frac{I \times \Delta t}{m \times V}
$$
 [1]

where *I* is the current (A), Δt is the discharge time (s), *m* is the mass of sample (g), and *V* is the voltage window (V) .

The correlation between the measured current (*i*) and the scanning rate (*v*) can be expressed by the following eqn [2] and [3]:

$$
i = av^b \tag{2}
$$

$$
\log i = b \log v + \log a \tag{3}
$$

where the modulatory parameters *a* and *b*, obtained from the fitted curves, can indicate whether the process is diffusion-controlled (when *b* approaches 0.5) or capacitive-controlled (when *b* is close to 1.0) [S6, S7].

The contribution mechanisms of various charging and discharging processes are calculated by the following eqn [4] [S6, S7]:

$$
i(V) = k_1 v + k_2 v^{1/2}
$$
 [4]

where k_1v and $k_2v^{1/2}$ represent the capacitive-controlled contribution and diffusion-controlled contribution, respectively.

S1.7. Desalination performance measurements

The CDI measurements were carried out in a continuous cycle system including a peristaltic pump, constant current power supply, stirring device, a tank and a CDI unit consisting of a pair of working electrodes (2.5 \times 2.5 cm²) and a pair of ion exchange membranes. The CDI electrodes were fabricated by a slurry mixing in NMP solution of the NC/Mo*y*C-*x*: carbon black: PVDF=8: 1: 1. The slurry was coated on graphite paper (2.5 \times 2.5 cm²) and dried overnight at 80 °C in a vacuum. In the CDI experiments, the ion conductivity meter was used to monitor and measure the real-time change of NaCl concentration at the outlet of CDI device under different concentrations (100, 250, 500, 750, and 1000 mg L-1) and voltages (0.8, 1.0, 1.2, 1.4, and 1.6 V). The volume of NaCl solution was 32 mL, and the flow rate was 20 mL min⁻¹. The salt adsorption capacity (SAC, mg g^{-1}) and salt adsorption rate (SAR, mg g^{-1} min⁻¹) at *t* min are calculated as following eqn [5] and [6]:

$$
\text{SAC} = \frac{(C_0 - C_t) \times V_s}{m}
$$
\n
$$
\text{SAR} = \frac{\text{SAC}}{t}
$$
\n
$$
\text{[5]}
$$

where C_0 and C_t are the NaCl concentrations at initial stage and *t* min (mg L⁻¹), respectively; V_s is the solution volume (L); and *m* is the total mass (16 mg) of the electrode materials on the working electrodes [S8, S9].

The charge efficiency (*Λ*) is calculated according to eqn [7] [S10, S11]:

$$
A = \frac{\Gamma \times F}{\Sigma} \tag{7}
$$

where *Γ* represents the desalination capacity (mol g⁻¹), *F* denotes the Faraday constant (96485 C mol⁻¹), and *Σ* stands for the integral of the current-time curve (C g^{-1}).

The energy consumption (E, Whg^{-1}) is obtained according to eqn [8] [S10, S11]:

$$
E = \frac{v \times \int idt}{3.6 \times (C_0 - C) V}
$$
 [8]

where the *v* indicated a driven potential, ∫*idt* corresponded to the integrated value of the current transient *vs*. running time plot, and V (mL) was the rotational solution volume. C_0 and C (mg L⁻¹) were initial and final concentrations, respectively.

The Langmuir isotherm model (eqn [9]) is adopted to simulate the experimental SAC data of ion adsorption on the electrode [S12, S13]:

$$
q = \frac{q_m K_L C}{I + K_L C}
$$
 [9]

where q is the SAC (mg g^{-1}), K_L is the Langmuir constant related to the heat of adsorption, q_m is the maximum SAC (mg g⁻¹) corresponding to complete monolayer coverage, and C is the equilibrium concentration (mg L^{-1}).

S2. DFT Calculation Methods

TheCambridge sequential total energy package (CASTEP) module in DFT-based Material Studio was utilized to perform all calculations [S14, S15]. Perdew-Burke-Ernzerhof (PBE) within the generalized gradient approximation (GGA) is employed to calculate the exchange-correlation potential. The cutoff energy is set to be 400 eV. All structures were optimized until the energy converged to 1.0×10^{-5} eV and the force reached 0.02 eV Å-1 .

Fig. S1. SEM images of (a) MOF/MoO₄-0.25, (b) MOF/MoO₄-1, and their-derived (c) NC/MoC-0.25, and (d)

NC/MoC/Mo₂C-1.

Fig. S2. (a1) HRTEM, (a2) inverse fast Fourier transformation (IFFT) image, and (a3) corresponding line scan of NC/MoC-0.25. (b1) HRTEM, and (b2-b4) IFFT images and corresponding line scans of NC/MoC/Mo2C-1, including (b2, b4) IFFT images and (b3, b5) corresponding line scans.

Fig. S3. Pore size distributions of (a) ZIF-8 RDs and MOF/MoO₄-*x* (*x*=0.25, 0.5, and 1) and (b) their derived ZIF-8-C, NC/MoC-0.25, NC/MoC-0.5, and NC/MoC/Mo2C-1.

Fig. S4. The Mo contents in NC/MoC-0.25, NC/MoC-0.5, and NC/MoC/Mo2C-1.

Fig. S5. (a) CV and (b) GCD curves for ZIF-8-C.

Fig. S6. (a) CV and (b) GCD curves of NC/MoC-0.25.

Fig. S7. (a) CV and (b) GCD curves of NC/MoC/Mo₂C-1.

Fig. S8. CDI Ragone plots of NC/MoC-0.5 with an initial NaCl concentration of 500 mg L-1 at various voltages

from 0.8 to 1.6 V.

Fig. S9. SAC versus deionization time plots of the (a) ZIF-8-C, (b) NC/MoC-0.25, and (c) NC/MoC/Mo2C-1 electrodes with initial concentration of 500 mg L-1 using different voltages. The corresponding CDI Ragone plots for (d) ZIF-8-C, (e) NC/MoC-0.25, and (f) NC/MoC/Mo₂C-1.

Table S1. Comparisons of the transition metal carbides/dichalcogenides or MOFs-derived carbons for their

CDI performance.

^a **MoC@CNFAs**: Molybdenum carbide nanoparticle-embedded carbon nanofiber aerogels; **WC@GNFs**: Tungsten carbide@graphene nanoflakes; **CoCr7C3@CNFs**: CoCr7C³ metallicemetallic carbides@carbon nanofibers; **T-MoS2**: Defectrich MoS₂; MoS₂-S180: Oxygen-incorporated MoS₂ that synthesized at 180 °C; MoS₂-CNT: Molybdenum disulfide /carbon nanotube; MoS_2/PDA : $\text{MoS}_2/\text{polydopamine}$; $\text{MoS}_2\text{-rGO}$: 3D flower-like $\text{MoS}_2/\text{reduced graphene oxide composite}$; $\text{MoS}_2/\text{g-}$ **C₃N₄:** MoS₂/graphitic carbon nitride composite; **MoS₂/NOMC**: MoS₂/nitrogen-doped highly ordered mesoporous carbon; Ce-MoS₂: Chemically exfoliated multi-layer MoS₂ nanosheets; NC@GC/CNTs: Nitrogen-doped carbon@graphitic carbon/carbon nanotubes; **NPC/rGO**: Porous N, P-doped carbon/reduced graphene oxide; **CNFZIF**: Carbon nanofiber@ZIF-8 derived N-rich porous carbon nanosheets; **NHPC**: Hierarchical porous ZIF-8 derived carbon; **NC-800**: ZIF-8 derived Ndoped carbon by the pyrolysis at 800 ºC; **NP-EHPC**: N, P co-doped eave-like hierarchical porous carbon; **P-CNFA**: P-doped carbon nanofiber aerogels.

Fig. S10. (a, b) SEM, (c, d) TEM, (e) HRTEM (Insert: the IFFT image), and (f) XRD pattern of NC/MoC-0.5 after the 200 CDI cycles (Applied voltage: 1.2 V; NaCl concentration: 500 mg L-1).

Fig. S11. The structure models of (a) MoC, (b) NC, and (c) NC/MoC [S34, S35].

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