Amyloid- β Aggregation: Selective Inhibition of Aggregation in Mixtures of Amyloid with Different Chain Lengths

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ABSTRACT One of the clinical manifestations of Alzheimer's disease is the deposition of the $39-43$ residue amyloid- β (A β) peptide in aggregated fibrils in senile plaques. Characterization of the aggregation behavior of $\Delta\beta$ is one of the critical issues in understanding the role of AB in the disease process. Using solution hydrodynamics, AB was observed to form three types of species in phosphate-buffered saline: insoluble aggregates with sedimentation coefficients of \sim 50.000 S and molecular masses of \sim 10 $^{\circ}$ Da, "soluble aggregates" with sedimentation coefficients of \sim 30 S and masses of \sim 10 $^{\circ}$ Da, and monomer. When starting from monomer, the aggregation kinetics of A β 1-40 (A β 40) and A β 1-42 (A β 42), alone and in combination, reveal large differences in the tendency of these peptides to aggregate as a function of pH and other solution conditons. At pH 4.1 and 7.0-7.4, aggregation is significantly slower than at pH 5 and 6. Under all conditions, aggregation of the longer AB42 was more rapid than AB40. Oxidation of Met-35 to the sulfoxide in AB40 enhances the aggregation rate over that of the nonoxidized peptide. Aggregation was found to be dependent upon temperature and to be strongly dependent on peptide concentration and ionic strength, indicating that aggregation is driven by a hydrophobic effect. When AB40 and AB42 are mixed together, AB40 retards the aggregation of A1342 in a concentraton-dependent manner. Shorter fragments have a decreasing ability to interfere with $A\beta$ 42 aggregation. Conversely, the rate of aggregation of $A\beta$ 40 can be significantly enhanced by seeding slow aggregating solutions with preformed aggregates of AB42. Taken together, the inhibition of AB42 aggregation by AB40, the seeding of AB40 aggregation by AB42 aggregates, and the chemical oxidation of AB40 suggest that the relative abundance and rates of production of different-length A β and its exposure to radical damage may be factors in the accumulation of A β in plaques in vivo.

INTRODUCTION

The formation of extracellular deposits of neuritic (senile) plaques is one hallmark of Alzheimer's disease (AD). The major component of these plaques is amyloid- β $(A\beta)$, a 39-43-residue peptide (Glenner and Wong, 1984; Kang et al., 1987). The sequence of \overrightarrow{AB} 1-42 is: DAEFR⁵HDSGY¹⁰EVHHQ¹⁵KLVFF²⁰AEDVG²⁵SNKGA³⁰-IILGLM³⁵VGGVV⁴⁰IA. A β is derived by proteolytic cleavage of the transmembrane region of the 110-135-kDa amyloid precursor protein (BPP; Goldgaber et al., 1987; Kang et al., 1987; Kitaguchi et al., 1988; Ponte et al., 1988; Tanzi et al., 1988). Evidence suggests that accumulation of $\mathbf{A}\mathbf{\beta}$ and formation of the neuritic plaques may play a pathological role in the disease (Kowall et al., 1991; Yankner, 1992; Krafft, 1993; Selkoe, 1993). Reports from in vitro toxicity studies have suggested that soluble \overrightarrow{AB} is nontoxic, whereas aggregated \overrightarrow{AB} is toxic (Pike et al., 1991; Burdick et al., 1992; Mattson and Rydel, 1992; Yankner, 1992; Pike et al., 1993; Giordano et al. 1994). Soluble \overrightarrow{AB} is present as a normal extracellular product in a variety of cell lines (Haass et al., 1992) and is found at comparable levels in the cerebrospinal fluid of age-matched AD and normal patients (Seubert et al., 1992; Shoji et al., 1992).

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 $\Delta\beta$ forms antiparallel β -pleated sheets that aggregate into amyloid fibrils that exhibit positive Congo Red staining (Glenner, 1980; Kirschner et al., 1987; Turnell and Finch, 1992). Anumber of techniques, including circular dichroism, nuclear magnetic resonance (NMR), and infrared, have been employed to characterize the secondary molecular structure and conformation of \overrightarrow{AB} (Masters et al., 1985; Halvserson et al., 1990; Fraser et al., 1991; Hilbich et al., 1991; Spencer et al., 1991; Barrow et al., 1992; Fraser et al., 1992; Lansbury, 1992; Zagorski and Barrow, 1992). The degree of β -sheet character and transitions to either α -helix or random coil have proven to be strongly dependent upon the solution characteristics. Observations of molecular structural variability have been attributed to a number of physical and environmental characteristics, including the length of the \overrightarrow{AB} fragment, peptide concentration, age of the sample, presence of organic solvents, temperature, solution pH, and ionic strength (Fraser et al., 1991; Hilbich et al., 1991; Barrow et al., 1992; Fraser et al., 1992; Zagorski and Barrow, 1992; Otvos et al., 1993).

The fibrillar structure of $A\beta$ aggregates has been investigated with electron microscopy, x-ray diffraction, and light scattering (Gorevic et al., 1986; Kirschner et al., 1987; Halvserson et al., 1990; Caputo et al., 1992; Fraser et al., 1992; Caputo et al., 1993; Inouye et al., 1993). Reports indicate that the fibrils formed from purified \overrightarrow{AB} are relatively straight with a diameter of 5 nm and periodic twists (Fraser et al., 1992). These structures have generally correlated with the structures observed of fibrils in senile plaques from AD brains (Kirschner et al., 1986).

It is reasonable to assume, a priori, that the ability of $A\beta$ to accumulate in senile plaques in vivo strongly depends on

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at least two factors, local concentration and the kinetics of aggregation. If \overrightarrow{AB} aggregation is slow in vivo, it may be cleared by proteolytic degradation before its deposition (Hyman et al., 1993; Ladror et al., 1993, 1994, Suzuki et al., 1994). Conversely, if the seeded aggregate structure becomes resistant to proteolysis in vivo more rapidly than it is degraded, the seeds will grow into larger aggregates and senile plaques could form. There have been several investigations of the kinetics of \overrightarrow{AB} aggregation (Tomski and Murphy, 1992; Jarrett and Lansbury, 1993; Jarrett et al., 1993; Shen et al., 1993; Snyder et al., 1993a,c). Most of the work has focused on kinetic events that occur over the course of hours to days. In general, conditions that favor β -sheet structure also enhance aggregation rates (Tomski and Murphy, 1992; Jarrett and Lansbury, 1993; Jarrett et al., 1993).

Observations regarding aggregate size and structure, as well as the kinetics of aggregation, have exhibited considerable variability as a result of different peptide-handling procedures and techniques employed to monitor and characterize aggregation behavior (Knauer et al., 1992; Simmons et al., 1993, 1994; Snyder et al., 1993b,c). One cause of the discrepancy regarding $\Delta\beta$ aggregation and toxicity is the method of dissolving and handling $\mathbf{A}\mathbf{\beta}$. Typically, experiments have been performed by directly transferring \overrightarrow{AB} from a lyophilized solid to the solution conditions employed for aggregation, structure, or toxicity studies (Hilbich et al., 1991; Burdick et al., 1992; Tomski and Murphy, 1992). There has been no consideration for the effect of high local $\Delta\beta$ concentrations on aggregation behavior during the nonhomogeneous solvation process. At high concentrations of synthetic $\Delta\beta$, variations in acid or water content may accentuate the nonhomogeneous distribution during mixing of the lyophilized solid. Furthermore, little regard has been shown for potential aggregation in intermediate \overrightarrow{AB} solutions used between concentrated stock solutions and dilute final solutions. At intermediate dilutions, \overrightarrow{AB} remains relatively concentrated, whereas organic solvent concentrations are reduced, which can lead to rapid aggregation. Besides variations in \overrightarrow{AB} solvation, differences exist in the techniques employed to characterize the degree of \overrightarrow{AB} aggregation. The sensitivity of dye staining such as thioflavine T to either small soluble aggregates or rapidly formed aggregates with little structural integrity remains unclear (LeVine, 1993). The effect of SDS on the stability of \overline{AB} aggregates precludes gel electrophoresis as a reliable quantitative technique for assessing aggregation. Finally, a variety of studies have been conducted with the implicit presumption that all aggregated A β is removed by centrifugation at 10,000-100,000 \times g (Burdick et al., 1992; Waite et al., 1992; LeVine, 1993).

A paradigm for studying amyloid aggregation depends upon the ability to define an initial solute physical state, to monitor the transition process from an initial state to a final state, and to define the final (equilbrium) state (Snyder et al., 1993a-c). Rates of aggregation, in vivo, that are so sluggish that they preclude accumulation in competition with proteolysis cannot be considered relevant (Hyman et al., 1993; Ladror et al., 1993, 1994; Suzuki et al., 1994). Therefore, we have undertaken a systematic investigation of the propensity

of \overrightarrow{AB} to aggregate under conditions in which peptide accumulation would be expected to compete with physiological degradation. In this work, we describe the aggregation of \overline{AB} from a hydrodynamically defined, monomeric starting state to ^a fibrillar final state. We find that kinetics are strongly dependent on fragment length, pH, concentration, seeding, and ionic strength. We further demonstrate that aggregation kinetics of the more hydrophobic \overrightarrow{AB} 1-42 (A \overrightarrow{AB} 42) can be selectively inhibited, in a specific and dose-dependent fashion, by the more soluble $\mathbf{A}\mathbf{\beta}$ 1-40 ($\mathbf{A}\mathbf{\beta}$ 40). In addition, we demonstrate that oxidation of the single Met-35 residue in AB40 to the more polar sulfoxide form, (AB40 M[O]), enhances aggregation rate. From the dependence of aggregation kinetics on relative concentrations of $A\beta40$ and $A\beta42$, we suggest that selectivity of cleavage in the carboxy terminus of APP and the potential for Met-35 oxidation may be factors in the accumulation of AB in senile plaques.

MATERIALS AND METHODS

Peptide synthesis and purification

The methods used for peptde synthesis and the characterizaion of the resulting peptides are briefly summarized. Solid-phase peptide synthesis was carried out on an Applied Biosystems (Foster City, CA) Model 430A peptide synthesizer operating with Fmoc chemistry based on dicyclohexylcarbodiimide-catalyzed formation of 1-hydroxytriazole ester in N-methylpyrolidone (NMP) and dichloromethane (DCM) co-solvent. Fmoc removal (deprotection of amino groups) was achieved with 20% piperidine in NMP. The side chain protecting groups were as follows: Ser and Tyr, O-t-Bu; Asn and Gln, C(O)-NH-Trityl; Asp and Glu, CO₂-t-Bu; His, Trityl; Lys, Boc-NH; Arg, N^G -(2,2,5,7,8-pentamethylchroman-6-sulfonyl). All natural amino acids were purchased from ABI. Fmoc-Met oxide for the synthesis of A β 40 Met-35[O] (A β 40 M[O]) was either prepared by oxidation of Fmoc-Met with m-chloroperbenzoic acid in DCM or purchased from Bachem (Torrance, CA). ABI p-hydroxymethylphenoxymethyl resin with ^a substitution level of 0.85 mmol/g was used for synthesis. A standard double-loading cycle involving coupling in the presence of p-dimethylaminopyridine was used to load the first residue on to the resin. Coupling of all subsequent resdues was achieved using standard double-couplng cycles with acetyl capping supplied with the instrument. In our hands syntheses performed as described above exhibited a typical coupling efficiency of 99.6% by ninhydrin analysis.

Upon completion of ^a synthesis, the peptide resin was treated with ^a mixture of trifluoroacetic acid (TFA, 93%) and a scavenger cocktail (7%) composed of ethylene dithiol, anisole, and ethylmethyl sulfide in a 1:3:3 ratio for $3-4$ h. The cleavage reagents were typically used at 20 ml/g of peptide resin At the end of cleavage the resin was removed by filration and the solvents were evaporated. The crude peptide was precipitated with diethyl ether and collected. The amount of crude peptide obtained typically corresponded to \sim 95% of the expected theoretical yield based on the amount of resin used. The crude peptides were routinely analyzed by reversed phase high-performance liquid chromatography (RP-HPLC) and mass spectrometry. Preparative peptide isolatons were performed using a 40-mm C8 column (300 Å, 12 μ m) at 45 ml/min. Before elution of each peptide the acetonitrile (ACN) gradient was reduced to 0.6% ACN/min to broaden the eluting peak. Only the center of each peak was collected (\sim 85% of peak area). The pooled HPLC fractions were lyophilized and the products further analyzed by analytical RP-HPLC and electrospray ionization mass spectrometry (ESI-MS) to establish purity. Typical purity values were >95% for $A\beta40$ and $>85\%$ for $A\beta42$.

Sample preparation

 $A\beta$ samples were stored in lyophilized form at room temperature, and were dissolved in stock solutions in either dimethyl sulfoxide (DMSO), 30% ACN with 0.1% TFA (ACN/TFA), hexafluoroisopropanol (HFIP), or H₂O at concentrations up to 30 mg/ml (\sim 6.5 mM). Dilution was accomplished in one step from the concentrated stocks into the final buffer, avoiding intermediate solutions with high AB concentrations between the starting stock and final solutions. Samples were dissolved in either of two buffers: phosphate-buffered saline (PBS) composed of phosphate (10-50 mM), NaCl (0-500 mM, pH 7.40); or a wide-range pH buffer composed of HOAc (20 mM), MES (20 mM), Tris (20 mM), glycine (20 mM), NaCl (150 mM, pH 3-9).

Analytical ultracentrifugation measurements

Sedimentation equilibrium and velocity measurements were performed on ^a Beckman (Palo Alto, CA) XL-A analytical ultracentrifue with an An6OTi rotor (Holzman and Snyder, 1994). Most experiments were carried out at 23.0 $^{\circ}$ C. Equilibrium runs were performed on 110- μ l samples over the rotor velocity range 3000-60,000 rpm. Samples were centifuged for at least 20 h to reach equilibrium and signals were averaged 4 to 16 times. Data were analyzed for solute molecular weights as recently described (Holzman and Snyder, 1994). Velocity runs were performed on 300-450-µl samples over the rotor velocity range of 1000-30,000 rpm. Analysis of velocity data for sedimentation and diffusion coefficients for single solutes and multiple, noninteracting solutes were based on a form of Faxen's two-component solution to the Lamm equation, as described by Fujita (1962). The useful expression is:

$$
c = \left(\frac{c_0 e^{-\tau}}{2}\right) \left[1 - \Phi\left(\frac{1 - (xe^{-\tau})^{1/2}}{\left[\epsilon(1 - e^{-\tau})\right]^{1/2}}\right)\right]
$$
(1)

where $x = (r/r_0)^2$, $\tau = 2s\omega^2 t$, $\epsilon = 2D/s(\omega r_0)^2$, Φ is the error function of the term enclosed in brackets, r is the radial position, r_0 is the radial position of the meniscus, ω is the radial rotor velocity, t is the time, and s and D are the sedimentation and diffusion coefficients, respectively. The sedimentation coefficient is reported in Svedbergs $(S, 10^{-13} s^{-1})$ and the diffusion coefficient in Ficks (10^7 cm²/s). Under suitable conditions (Fujita, 1962), Eq. ¹ can be used to approximate the profile of a sedimenting boundary (Holzman and Snyder, 1994). For heterogeneous samples or samples with multiple sedimenting components with different values of s and D , the sedimenting boundary can be represented as a linear sum of terms identical to Eq. 1, where each term represents a component with specific value of ^s and D (Holzman and Snyder, 1994). A sampe with multiple sedimenting components of similar hydrodynamic propertes can be fit to a model that assumes only one sedimenting species. The simplified model will yield an average sedimentation coefficient and an overestimated diffusion coefficient that compensates for the spreading sedimenting boundary.

When s and D are well defined, the molecular mass and the shape of the sedimenting species can be determined by:

$$
Mw = \frac{sRT}{D(1 - \bar{v}\rho)}\tag{2}
$$

where R is the universal gas constant, \bar{v} is the partial specific volume of the sedimenting species and ρ is the solvent density. With a distribution of sedimentig specis, large uncertaintes in the diffusion coefficient exist, and average sedimentaton coefficients can be employed to estimate average molecular masses:

$$
Mw \propto 6000s^{3/2} \tag{3}
$$

Eq. 3 is an empirical relationship employed to estimate molecular masses of aqueous solutions of proteins (Chervenka, 1973).

Stafford (1992a,b) has developed another method for calculating the apparent sedimentation coefficient distribution, $g^*(s)$, for sedimenting species. This method does not retain any information regarding the diffusion coefficient of the sedimenting species. We employ the algorithm "dcdt" developed by Stafford to determine $g^*(s)$ _r.

Dynamic light scattering

Dynamic light scatering (DLS) was performed on a Nicomp (Santa Barbara, CA) 370 instument equipped with a Coherent (Santa Clara, CA) 304 argon ion laser. Samples were centrifuged to remove large material, and samples were analyzed for \sim 10 min. The results are presented as a mean Gaussian diameter (MGD). The cubic dependence of scattering on particle size (Andreu and Timasheff, 1986) causes the MGD to be biased toward larger-sized particles.

Kinetic measurements of aggregation

Aggregation kinetics were monitored after rapid manual dilution/mixing of the A β sample from a 30-mg/ml (6.5 mM) stock solution in DMSO or HFIP into the desired buffer. After dissolving the $\mathbf{A}\mathbf{\beta}$ sample in DMSO, the solution was centrifuged at $10,000 \times g$ for 5 min to remove undissolved material. Mixing was accomplished in the cuvette by rapidly drawing up and delivering the solution 10 to 15 times with a pipette equipped with a smallbore $200-\mu l$ disposable tip or by vortexing the sample immediately upon dilution. Final A β concentrations were kept in the range of 0.05-2.0 mg/ml (10-450 μ M), with most measurements at 0.2 mg/ml (45 μ M). Coaggregation and aggregation inhibition measurements were accomplished by premixing the stock DMSO solutions before dilution into the desired buffer. Seeding experiments were accomplished by mixing the seed \overrightarrow{AB} sample into the desired buffer as described, allowing aggregation to occur, and then mixing in the secondary $\mathsf{A}\mathsf{\beta}$ stock solution (dissolved in DMSO) as before.

Aggregaton was monitored by folowing the change in turbidity with a Hewlett Packard (Palo Alto, CA) 8452 diode array spectrophotometer. Turbidity was monitored at 350 nm on unagitated samples in a cuvette with a 05-1.0-cm path length over the temperature range, 10-37C. Unless otherwise noted, dilution of A β from its stock solution was accomplished immediately before the start of data collection (within ¹ min). Turbidity measurements were compared with Rayleigh light-scattering measurements and similar behavior was observed.

Electron microscopy

Samples were collected from the aggregation kinetics experiments about one week after mixing. Samples $(20 \,\mu\text{J})$ were placed onto formvar carbon-coated specimen grids negatively stained with 2% phosphotungstic acid, and examined with ^a CM12 tansmission electron microscope (TEM) operating at 80 kV accelerating voltage and 60,000 × magnification.

RESULTS AND DISCUSSION

A paradigm for examining the aggregation of purified synthetic AB

The method we employ for monitoring \overrightarrow{AB} aggregation behavior is to proceed from a clearly defined, monomeric starting state to ^a fibrillar final state. We start by characterizing the initial and final states and continue by monitoring the transition between these two states. In this approach the effects of added agents on the aggregation process are monitored during the transition.

RP-HPLC and ESI-MS were used as primary analytical methods to establish the purity of the peptide. Excellent synthetic results were obtained for the synthesis of $A\beta40$ with the desired product constituting at least 95% of the crude product. The purity level is equal to or better than the $A\beta40$ samples employed in various studies where analytical data for the peptides were given and comparisons could be made (Burdick et al., 1992). The synthesis of $A\beta42$ was more problematic, as unpurified peptide contained 80-85% of the desired material, with the remainder being truncated peptides. Routine purification of this peptide by HPLC to ^a single sequence was unreliable because of its extraordinarily poor

solubility and propensity to aggregate. These results are consistent with the results of others in which AB42 samples were produced by continuous solid-phase synthesis (Burdick et al., 1992). As a test of purity water-soluble and water-insoluble fractions of AB42 were compared by mass spectroscopy after centrifugation at $10,000 \times g$. No discernible differences between the samples were observed. These results indicate that our aggregation experiments are monitoring AP42 at the stated purity, not selectively monitoring more soluble impurities.

To assess the degree of aggregation of $A\beta42$ in potential purification solvents, we determined their MGD values by DLS (Table 1). The MGD provides ^a qualitative indication of aggregation but is strongly affected by presence of larger species, even at low concentrations. In DMSO the ¹⁰ mg/ml $A\beta$ 42 solution was >99% monomeric with an equivalent diameter of 2.4 nm. However, MGD values were skewed by a small population of large aggregates to yield mean values of 378 nm. Therefore the $A\beta$ DMSO solutions were centrifuged for 10 min at 10,000 \times g before use. When diluted into the other solvents, $A\beta42$ tended to aggregate with time. In either H₂O/TFA or ACN this trend of growing aggregate size was observed. Aggregation was particularly severe in solvent systems with trifluoroethanol exhibiting large size and rapid growth. The mixture, 50% ACN and 50% 2-propanol (2-Pr), yielded the smallest aggregate sizes and the most stable behavior. We are currently investigating ACN/2-Pr as ^a purification solvent for $A\beta42$.

One possible strategy considered for improving the purity of synthetic $A\beta42$ is a convergent fragment-coupling method rather than continuous solid-phase synthesis (Hendrix and Lansbury, 1992; Hendrix et al., 1992). The stated advantage of this approach is that the smaller component fragments can be highly purified before condensation, thereby limiting the

TABLE 1 Mean Gaussian diameter of 1 mg/ml AB42 in organic solvents at various ages

Solvent	Fresh (nm)	1.5 _h (nm)	24 h (nm)
DMSO*			378 [‡]
H ₂ O/0.1% TFA	36	96	263
ACN	27°	53	80
$2-PT$	80 ⁶	96	187
TFE	134		180
50% ACN/50% 2-Pr	15		20
50% ACN/50% TFE	138		90
50% 2-Pr/50% TFE	47		87
10% TFE/0.1% TFA/H,O	29	108	1747
50% TFE/0.1% TFA/H,O	1010^5	406 ¹	410
70% TFE/0.1% TFA/H,O	٠	\bullet	529

 $*$ In DMSO A β 42 = 10 mg/ml. All other samples were prepared by diluting this starting solution tenfold with the indicated solvent. Therefore the $A\beta$ 42 = 1 mg/ml and there is 10% DMSO remaining.

[‡] Analysis indicated that 99% of the sample had a diameter of 2.4 nm, which is probably monomer and the remainder distributed in the range 18-1000 am.

⁵ Scattering intensity increased continuously, indicating rapid aggregation. 'ifluoroethanol

It is likely that a large aggregate sedimented out of the cuvette and has been excluded from the measurement.

** Unstable scattering, probably due to severe aggregation during measurement

number of peptides lacking one or two residues. In practice, however, fragment-coupling approaches suffer from both poor efficiency and yield. Finally, the potential for peptide racemization during consecutive condensations must also be addressed.

Dissolution of the AB peptide and hydrodynamic characteristics of the initial and aggregated states

The aggregation states of $\mathbf{A}\mathbf{\beta}$ stock solutions were characterized by analytical ultracentrifugation. Sedimentation equilibrium and velocity measurements for $A\beta$ were compared in a series of stock solutions: DMSO, ACN/TFA, and H₂O (Figs. 1 and 2). Both A β 40 and A β 42 remained monomeric in DMSO over ^a wide concentration range (Fig. 1, A and B). After dispersion of solid peptide in ACN/TFA, a solvent composition commonly employed by researchers (Waite et al., 1992; Yankner et al., 1990), large aggregates were observed initially and increased in size over the course of several days (Fig. 1, C and D). Attempts to dissolve $\mathsf{A}\mathsf{B}\mathsf{4}0$ in distilled H₂O did not yield monomeric solutions; within 1-2 days molecular masses of \sim 8.5 \times 10⁵ Da developed with contributions from monomer representing less than 1% of the total content (Fig. $2 \text{ } A$). A sample that was aged for one month exhibited $s \sim 55$ S, which represents a molecular mass on the order of 2×10^6 Da (Fig. 2 B). The nonzero baseline in Fig. 2 B indicates that smaller species were also present, but they were not analyzed for size or contribution.

The aggregation states of $A\beta40$ and $A\beta42$ were further characterized in perdeuterated solvents, DMSO and ACN/ DCl, by NMR $(1 D)$. NMR spectra of A β 40 in deuterated DMSO exhibited sharp lines that were concentration independent (in DMSO) over the range of 5-18 mg/ml (not shown). In comparison, in 30% deutrated ACN/0.1% DCl/ D₂O, spectral lines were broad and concentration dependent across the same concentration range. These results are consistent with a monomeric form of $A\beta$ in DMSO in comparison with an aggregated form in acidified ACN.

We also performed DLS measurements on solutions of $A\beta$ 40 and $A\beta$ 42 in HFIP (Pike et al., 1993), given that the solvent density of HFIP is too high ($\rho = 1.6$) to perform hydrodynamic measurements. At 30 mg/ml (6.5 mM), both $A\beta$ 40 and $A\beta$ 42 had diameters in the range 1.5-2 nm indicating that both $A\beta40$ and $A\beta42$ remained monomeric in HFIP. To date, HFIP and DMSO are the only solvents that we have observed to yield monomeric $\mathbf{A}\boldsymbol{\beta}$ solutions reliably.

When an AB40 sample was aged in PBS at 450 μ M (2) mg/ml), several ranges of species sizes were observed by hydrodynamic analysis (Fig. 3). At 3000 rpm (650 \times g), large aggregates sedimented with $s \sim 50,000$ S (Fig. 3 A). These aggregates have molecular masses on the order of 10^{10} Da and are probably visible to the naked eye. Upon increase of the rotor velocity to 30,000 rpm (65,000 \times g), a second species sedimented with $s \sim 30$ S (Fig. 3 B). This represents a smaller aggregate with a molecular mass of $10⁶$ Da, and therefore an aggregate of 1000 A β monomers. These latter aggregates are not removable from solution by a typical

FIGURE 1 Sedimentation analyses of AB in different solvents. (A) Sedimentation equilibrium analysis of AB40 dissolved in DMSO at 3 mg/ml (690) μ M), centrifuged at 60,000 rpm (250,000 × g) for 64 h (6-h intervals between scans) at 23°C. The spike at about 6.15 cm is the solution meniscus. To calculate the molecular weight for a sedimenting component, independent determination of the partial specific volume (\bar{v}) of the protein is required. A search of Chemical Abstracts (Chemical Abstract Seravices, American Chemical Society, Columbus, OH) did not reveal any earlier reports of determinations for proteins in DMSO. When we used the monomeric molecular weight observed by ESI-MS (4325 Da) for A β 40 we calculated = 0.859 for monomer. To obtain dimer (8650 Da) required $\bar{v} = 0.884$. (B) Sedimentation equilibrium analysis of A β 42 dissolved in DMSO at 3 mg/ml (670 μ M) under the same conditions as in (A) (at 4-h intervals). As with A β 40 we used the molecular weight from ESI-MS (4511 Da) to estimate that $\bar{v} = 0.858$ for A β 42 in DMSO. Dimeric AB42 would require that $\bar{v} = 0.883$. (C) Sedimentation velocity analysis of AB40 freshly dissolved in 30% ACN/0.1% TFA at 3 mg/ml centrifuged at 30,000 rpm (65,000 \times g) for 1 h (at 12-min intervals) at 23°C. (D) Sedimentation velocity analysis of AB42 freshly dissolved in 30% ACN/0.1% TFA at 3 mg/ml centrifuged at 3000 rpm (650 \times g) for 1 h (4-min intervals) at 23°C. The large amount of noise on the raw data could be attributed to oil deposits on the optical system of the XL-A ultracentrifuge. This noise limits our ability to estimate parameter uncertainties on the measurements, but does not perturb the trends in the results that we present.

microfuge centrfugation employed to remove insoluble material. We consider these species to be "soluble aggregates" that form an optically clear solution and can be easily mistaken for monomeric $A\beta$. Some material did not sediment at the higher rotor velocity; note that the baseline did not reach 0 at 30,000 rpm (Fig. 3 B). Analysis of the nonzero baseline indicated that the remaining material was monomeric.

As a comparison, $A\beta40$ was dissolved in DMSO and then diluted into PBS. After 3 days, the 230 μ M A β solution exhibited an $s \sim 30$ S (data not shown), very similar to the soluble aggregates observed in the solution aged after direct dissolution in PBS. This size probably represents a size limit of "soluble aggregates" before larger structures were formed.

In a more detailed analysis (Fig. 4), the sedimentation velocity data at 30,000 rpm were fit to the model of Fujita (1962). The data could be fit better by a model that considered two sedimenting species rather than one (compare Fig. $4 A$ with $4 B$). The two-component model yielded diffusion coefficients that correlated better with values expected from

the aggregates sizes estimated from the sedimentation coefficients. Uncertainties in calculating the diffusion coefficient arise because the one component model must overestimate the diffusion coefficient to account for the boundary broadening that actually develops from the size distribution of aggregates (Holzman and Snyder, 1994). A comprehensive model of the aggregate sedimentation velocity behavior would likely encompass a Gaussian distribution of aggregate sizes based on polymer chain elongation (Demas and DeGraff, 1993). However, the signal-to-noise ratio for the $\Delta\beta$ sedimentation data was insufficient for such an approach, and it was not attempted.

The data were subjected to the analysis methods of Stafford (1992a,b) to calculate the apparent sedimentation coefficient distributions ($g^*(s)$; Fig. 5). The distribution exhibited a broad maximum in the region of $s = 27$ S with a full-width-half-maximum over the range, 17-42 S. Contributions decreased steadily with increasing s, and there was very little contribution from species with s <15 S. These

FIGURE 2 Sedimentation analyses of AB40 dissolved in distilled H₂O. (A) Sedimentation equilibrium analysis of 350 μ M A β 40 aged in H₂O for ¹ day, centifuged at 3000 rpm for 22 h at 23°C. Fitted acrve through the data gave an Mw value of 8.5×10^5 . (B) Sedimentation velocity analysis of 900 μ M A β 40 aged 1 month in H₂O analyzed at 3000 rpm, 23°C. Optical transients were collected at 4-h intervals at the indicated times. Solid thick lines through the data indicate the single-component fits to Eq. 1.

results suggest that the "soluble aggregate" forms a quasi-stable species with a finite distribution of aggregate sizes, and therefore that a distribution of aggregate sizes does not exist.

The form of the final aggregated state

Samples for transmission electron microscopy were taken directly from the samples prepared for analysis of aggregation kinetics. Densely packed fibrils were observed with $A\beta$ 40, A β 40 M[O], and A β 42. Fibrils had diameters of about ⁵ nm and lengths of about 100 nm (Fig. 6). In comparison, the reverse sequence 40-1 exhibited large amorphous globules when handled with identical procedures. The fibrillar structure for $A\beta40$ was similar at pH 4.1 and pH 7.4 (not shown).

Kinetics of amyloid aggregation.

Monitoring $\Delta\beta$ aggregation by turbidity measurements provides a picture of the overall concentration of aggregated peptide. Choice of wavelength affects the subset of sizes that are monitored (Doty and Steiner, 1950), but little information regarding the number, size, or shape of the aggregates can be discerned from single-wavelength, single-angle presentation. However, from the time-dependent change in the signal,

FIGURE 3 A β 40 (2 mg/ml, 450 μ M) dissolved and aged in PBS (50 mM phosphate, ¹⁵⁰ mM NaC, pH 7.40), 23°C. Optical transients collected at 280 nm. (A) Rotor velocity of 3000 rpm (650 \times g) presented at 6-min intervals showing the sedimentation of large aggregates. Sedimentation analysis of these aggregates gave a sedimentation coefficient of 50,000 S. (B) Rotor velocity of 30,000 rpm (65,000 \times g) presented at 4-min intervals showing the sedimentation of smaller, "soluble" aggregates. Analysis yielded $s \sim 30$ S. From the indicated absorbance the relative contributions of large aggregates, soluble aggrgates, and small species can be estimated.

the rate that small \overrightarrow{AB} species enter the aggregated state can be followed. We present these results without modeling the kinetics as a guide to monitoring \overrightarrow{AB} aggregation behavior.

In Fig. 7, we present ^a comparative pH study of the aggregation kinetics of the AB40, AB40 M[O], and AB42. For A β 40, aggregation was rapid (seconds) at pH 5 and 6, whereas at pH 4 it was slow (hours). At pH 7.0 and 7.40, aggregation was extremely slow (days). AB40 M[O] exhibited similar behavior as its unmodified analog, but kinetics were faster in all cases. $A\beta42$ aggregated more rapidly than $A\beta$ 40 over the entire pH range investigated; complete aggregation was observed within ¹ min at all pH values studied. The aggregation kinetics of \overrightarrow{AB} 1-43 were very similar to $A\beta$ 42 (data not shown).

The dramatic enhancement of aggregation rate observed with A β 42, in comparison with A β 40, suggests that the hydrophobic carboxy terminus of \overrightarrow{AB} plays a critical role in aggregation. Lansbury and co-workers (Spencer et al., 1991; Jarrett and Lansbury, 1993; Jarrett et al., 1993) have suggested that structural ordering of the carboxy terminus is the rate-determining step for \overrightarrow{AB} aggregation. The pH dependence of the kinetics reveals that the charged amino terminus and central region of the peptide must also be involved in

FIGURE 4 Analysis of sedimentation velocity data for 2 mg/ml (450 μ M) Aß40 dissolved and aged in PBS (50 mM phosphate, 150 mM NaCl, pH 7.40), 30,000 rpm (65,000 \times g), 23°C (5-min intervals). (A) Solid thick lines through the data indicate the single component fits. (Inset) Analysis of data of (poor) single-component fits for sedimentation and diffusion coefficients according to Eq. 1. Sedimentation coefficient, in Svedbergs \Box) and diffusion coefficient (O) in Ficks. The analysis yielded an average $s = 32$ S and an average $d = 72$ F. The magnitude of the diffusion coefficient does not correlate well with the sedimentation coefficient. (B) Reanalysis (solid thick lines) of the identical data with a two-cmonent fit for sedimentation and diffusion coefficients according to Eq. 1. (Inset) Analysis of data from two-component fits of sedimentation and diffusion coefficients according to Eq.1. Solid thick lines through the data indicate the (good) two-component fits. The analysis yielded two components with a 2:1 contribution with $s =$ 28 and 64 S, respectively. The diffusion coefficients were still overestimated $(35$ and 110 F), indicating that although the fit quality seemed satisfactory, there was a failure to fit a model with discrete components.

aggregation. Given our findings that $A\beta40$ M[O], which contains a more polar group in the middle of the hydrophobic region, aggregates faster than the normal peptide, it may be premature to focus solely on the conformation of the carboxy terminal residues as controlling the rate of aggregation. Aggregation likely requires interactions along much of the $A\beta$ chain. An antiparallel β -sheet requires head-to-tail orientation so the carboxy terminus cannot exclusively control aggregation.

We have other corroborating evidence indicating that aggregation is dependent upon much of the \overrightarrow{AB} sequence. Chemical modification of $A\beta40$ inhibited aggregation under conditions where unmodified $A\beta40$ readily aggregated. Both

FIGURE 5 Apparent sedimentation coefficient distribution ($g^*(s)$) as a function of sedimentation coefficient. The data from Fig. 4 were fit using "dcdt" from Stafford (1992a,b) over the time range 38-63 min with $\Delta t =$ 15 min. $g^*(s)$, exhibited a broad maximum near $s = 27$ S and a full-widthhalf-maximum over the range 17-42 S. The analysis is uncorrected for diffusion.

conjugation of fluorescein to the amino terminal Asp-1 and iodination of Tyr-10 inhibited aggregation (data not shown). These modifications are remote from the carboxyl terminus of \overrightarrow{AB} and further point to the involvement of the entire molecule in controlling aggregation.

To understand further the factors that control $\mathbf{A}\boldsymbol{\beta}$ aggregation, we studied the starting solvent, concentration, temperature, and ionic strength effects on aggregation kinetics. In Fig. 8, we show that $\mathbf{A}\mathbf{B}40$ aggregation kinetics exhibit a strong nonlinear dependence on peptide concentration. Aggregation exhibits threshold-type behavior, where rates are dramatically enhanced once a given sample concentration is reached. This behavior indicates that the rate-determining step is the formation of a multimeric seed or initiator (Hofrichter et al., 1974; Jarrett and Lansbury, 1992, 1993).

When starting from HFIP, a solvent in which $A\beta40$ remains monomeric, aggregation kinetics increased by a factor of \sim 10 in comparison with DMSO (Fig. 8 B). In HFIP, AB is reported to be a mixture of random coil and α -helix with little-to-no β -sheet character (Hilbich et al., 1991; Barrow et al., 1992). Increased aggregation probably arises from the decreased hydrogen bonding, and therefore, decreased solvation by HFIP. This variation in aggregation behavior portends the difficulties in correlating $\mathbf{A}\mathbf{\beta}$ aggregation and structure to toxicity.

The dependence of $A\beta$ 40 aggregation on solution ionic strength is presented in Fig. 9 for a series of NaCl concentrations (0-500 mM). Aggregation is strongly accelerated by increasing salt concentration, again revealing the dependence of aggregation properties on handling conditions. In addition, aggregation is weakly dependent upon temperature, increasing as the temperature is raised from 10 to 37° C (data

FIGURE 6 Transmission electron micrographs of (A) Aβ40, (B) Aβ40 M[O], (C) Aβ42, and (D) 40-1 peptide. Samples were diluted out of DMSO into the wide-range pH buffer at pH 4.1 and aged for 1 week at 45 μ M. Individual samples were placed on form var carbon specimen grids and negatively stained with 2% phosphotungstic acid for 1 min. All grids were examined with a CM12 TEM operating at 80 kV and 60,000× magnification. Intertwined fibrils of about 5 nm diameter and variable lengths (\sim 100 nm) were observed in all three A β samples. With the reverse sequence 40-1, only amorphous globs were observed.

not shown). Taken together, the ionic strength and temperature dependence indicate that aggregation is driven by a hydrophobic effect (Hilbich et al., 1991).

Inhibition of AB42 aggregation and seeding of AB40 aggregation. Given the large differences in aggregation rates for $A\beta40$ and $A\beta42$ under identical conditions, we investigated the aggregation rates when $A\beta40$ and $A\beta42$ were mixed at several pH values (Fig. 10 A) and peptide concentrations (Fig. ¹⁰ B). A significant concentration-dependent decrease in rate was observed for $A\beta42$ aggregation when the two were mixed. With the mixture, the turbidity signal increased from an early time level near baseline without the rapid rise observed for AB42 by itself. These results cannot be attributed to rapid aggregation of $A\beta42$ followed by a

FIGURE 7 Aggregation kinetics of (A) A β 40, (B) A β 40 M[O], (C) AB42 at several pH values. Samples were diluted out of DMSO at 30 mg/ml (6.5 mM) to a final concentration of 0.2 mg/ml (45 μ M) in either the widerange pH buffer (pH 4.1, 5.0, 6.0, and 7.0) or PBS (10 mM phosphate, 150 mM NaCl, pH 7.40) and rapidly mixed. Turbidity was monitored in 0.5-cm
path length cells at 37°C with an HP8452 diode array spectrophotometer Dilution from DMSO into buffer was perfomed about 30 ^s before the start of data collection. In cases where aggregation was rapid (seconds), shifts in turbidity were frequently observed (e.g., AB40 M[O] at pH 5.0), which can probably be attributed to settling of large aggregates.

seeding of AB40 aggregation by aggregated AB42. Instead, the rate retardation observed with a mixture of $A\beta A2$ and $A\beta$ 40 must be attributed to inhibition of $A\beta$ 42 aggregation when the two are mixed together.

We continued these mixing experiments by investigating the effect of several A β fragments (1-28, 25-35, 30-40, and 30-42) or the reverse sequence peptide (40-1) on aggregation kinetics of $\mathsf{A}\beta42$ (Fig. 11). Only a slight inhibition of aggregation was observed in most cases. This is probably due to nonspecific interactions between intact $A\beta42$ and the fragments (or 40-1). There was also only a slight inhibition of aggregation in the presence of 20% bovine serum albumin (data not shown). A β 1-28 was intermediate in its effectiveness at inhibiting $A\beta42$ aggregation (Fig. 11). A combination of A β fragments, 1-28 and 30-40, (also 30-42), did not retard $A\beta42$ aggregation to any greater extent than the separate fragments; in fact, inhibition was less than that observed for intact $\Delta \beta 40$. Taken together these data suggest that both specific inhibition of aggregation, and aggregation itself, required interactions along the whole peptide sequence.

FIGURE 8 Concentration dependence of aggregation kinetics of AB40 in PBS (10 mM phosphate, 150 mM NaCl, pH 7.40). Turbidity was monitored in 1.0-cm path length cells at 350 nm at 20° C. (A) A β 40 was diluted out of DMSO at 30 mg/ml to the indicated concentrations, $45-430 \mu M$ (0.2->2 mg/ml). (*Inset*) The low concentration regime (\leq 220 μ M) is expanded to reveal the lack of aggregation at the low concentrations. Aggregation exhibited a strong nonlinear dependence upon concentration, indicating that a threshold exists for rapid aggregation. (B) A β 40 was diluted out of HFIP (6.5 mM) to the indicated concentrations, $10-200 \mu M$ (0.04-0.8 mg/ml). (*Inset*) The low concentration regime ($\leq 20 \mu M$) was expanded to reveal the lack of aggregation at low concentrations. Aggregation from HFIP exhibited similar threshold behavior, but at concentrations that were an order of magnitude less than that from DMSO.

From the mixing experiments it is apparent that $A\beta40$ and $A\beta$ 42 interacted during the aggregation process. To study the interactions between aggregated and aggregating peptide, we studied the ability of preformed aggregates of $A\beta$ 42 to seed the aggregation of 45 μ M A β 40 (Fig. 12). By itself A β 40 aggregates very slowly (Fig. 12A). In the presence of 11 μ M aggregated $A\beta42$, the rate of $A\beta40$ aggregation increased dramatically (minutes, Fig. $12 B$), and in the presence of 45 μ M A β 42, A β 40 aggregated in seconds (Fig. 12 C). In Fig. 12 D we show that the increase in turbidity observed in Fig. 12 C cannot be attributed to agitation of aggregated $AB42$ that has deposited in the cuvette. Therefore, aggregation of AB40 is enhanced by several orders of magnitude in a dosedependent fashion when seeded with aggregated $\mathbf{A}\mathbf{B}42$. As we first noted (Snyder et al. 1993a) and as confirmed by Jarrett et al. (1993) , aggregated A β 42 is capable of initiating the polymerization of $A\beta40$.

FIGURE 9 Ionic strength dependence of the aggregation kinetics of $A\beta40$ diluted from HFIP into PBS (10 mM phosphate, pH 7.40) and varying concentrations of NaCl (0-500 mM). Turbidity was monitored in 1-cm path length cells at 350 nm at 20° C at 68 μ M AB40. Aggregation was strongly dependent upon salt concentration, again exhibiting threshold behavior. The salt concentration required for rapid aggregation was much smaller at higher AB40 concentrations (data not shown).

FIGURE 10 Aggregation kinetics of A β 42 mixed with A β 40. The two $A\beta$ samples were mixed in DMSO (each at 15 mg/ml) and diluted into either the wide-range buffer or PBS (10 mM phosphate, 150 mM NaCl, pH 7.40). Turbidity was monitored in 0.5-cm path length cells at 37°C. (A) Dependence of inhibition of aggregation on pH at 4.1 , 5.0 , 6.0 , 7.0 , and 7.4) on samples with 0.2 mg/ml (45 μ M) of both AB40 and AB42. (B) Concentration dependence of the inhibition of aggregation at pH 7.0. A β 42 concentrations were held at 0.2 mg/ml, whereas A β 40 concentrations were varied between 0.1-0.6 mg/ml (23-140 μ M).

Factors controlling the aggregation/polymerization process

The rate of $\mathbf{A}\boldsymbol{\beta}$ aggregation is controlled by two distinct factors. First, solution conditions that decrease solubility and/or

FIGURE 11 Inhibition of AB42 aggregation by the indicated AB fragments (or the 40-1 peptide) mixed in DMSO and diluted into pH 7.0 widerange buffer. Turbidity was monitored in 0.5 -cm path length cells at 37° C. All peptide concentrations were held at 50 μ M. The control had A β 42 without any added fragments. A β 40 had the most dramatic effect on A β 42 aggregation. $\mathbf{A}\mathbf{\beta}$ 1-28 had an intermediate effect, and the smaller $\mathbf{A}\mathbf{\beta}$ fragments and 40-1 had only small effects. The combination of $\mathbf{A}\mathbf{\beta}$ 1-28 and 30-40 inhibited A β 42 aggregation to the same degree as A β 1-28 by itself.

FIGURE 12 Seeding of 0.2 mg/ml (45 μ M) A β 40 aggregation by A β 42 in PBS (10 mM phosphate, 150 mM NaCl, pH 7.40). AB42 was diluted from DMSO (30 mg/ml) and allowed to aggregate for 1 h at 0.2 mg/ml (45 μ M) in PBS at 37° C. A β 40 was diluted from DMSO (30 mg/ml) into the indicated solutions. Turbidity was monitored on 1.0-cm path length cells at 23°C. A) A β 40 diluted into PBS without A β 42. B) A β 40 diluted into 0.05 mg/ml (11 μ M) A β 42 (aggregated at 0.2 mg/ml). (C) A β 40 diluted into 0.2 mg/ml (45 μ M) AB42. Aggregation kinetics of AB40 are enhanced by the presence of aggregated A β 42 in a dose-dependent manner. (D) The aggregated 0.2 mg/ml (45 μ M) AB42 solution was remixed in the same fashion as AB40 was added, but no addition of concentrated AB40 was performed. This remixing of aggregated $A\beta42$ did not increase the signal as observed with addition of nonaggregated $A\beta40$.

increase β -sheet character accelerate aggregation kinetics; aggregation is controlled by the ability of the appending monomer to acquire the required stucture for polymerization. Lansbury (1992) has suggested that the two additional

residues on AB42, Ile-Ala, drive the carboxy terminus toward an extended β -sheet structure that is limited by a *cis*amide isoform at Gly37-Gly38 (Spencer et al., 1991). This can be seen in the accentuated aggregation rates of $A\beta42$ in comparison with AB40.

Second, aggregation rates are controlled by the number of sites available for elongation. \overrightarrow{AB} aggregation/ polymerization exhibits lag time and threshold behavior observed with polymerization processes (Hofrichter et al., 1974; Jarrett and Lansbury, 1992, 1993). Once nucleating sites are available, \overrightarrow{AB} aggregates rapidly. In the experiments with mixed A β 40 and A β 42, aggregation kinetics were inhibited because $A\beta40$ prevented nuclei of $A\beta42$ multimers from forming, by a competitive binding mechanism. This effect is transient in nature because, once the nucleating species are formed, both AB42 and AB40 aggregate. In fact, when more $A\beta40$ is present, kinetics are retarded, but the overall turbidity signal rises well above samples without $AB40.$

From the dependence of \overrightarrow{AB} aggregation kinetics on the ratio of $A\beta$ 40 and $A\beta$ 42, we speculate that the amount of accumulated peptide might correlate more closely with either the relative ratio of the longer to shorter forms of \overline{AB} than to overall $\Delta\beta$ concentration. Cerebrospinal fluid concentrations of A340 are in the range from high picomolar to low nanomolar (Seubert et al., 1992; Shoji et al., 1992), significantly below threshold concentrations required for rapid aggregation (\sim 350 μ M). Considering its sluggish aggregation rates, unless high concentrations of $A\beta40$ develop in localized regions, it is unlikely that a significant amount of $A\beta40$ would aggregate by itself. On the other hand, aggregates of $A\beta$ 42 or mixtures of $A\beta$ 42 and $A\beta$ 40 that aggregate in the seconds-to-minutes time regime would more readily develop in vivo. This leads to questions regarding cleavage specificity of the carboxy terminus of β PP. Slight changes in differential processing of the carboxy terminus could have dramatic effects on the amount of \overrightarrow{AB} aggregation and accumulation.

Another factor that can affect aggregation rates is the degree of Met-35 oxidation in A β 40 (or possibly A β 42). In a comparison of aggregation rates for AB40 versus AB40 M[O] (Fig. 7), Met oxidization enhanced aggregation rates. Oxidation of $A\beta$ by radical damage has been suggested as a causative agent to $\Delta\beta$ toxicity (Behl et al., 1992; Dyrks et al., 1992; Hensley et al., 1994); increased aggregation rates could contribute to increased toxicity.

Much of the variance observed in \overrightarrow{AB} toxicity could be due to the extreme sensitivity of the aggregation process to handling conditions. We have shown that several factors (i.e. \overrightarrow{AB} concentration, pH, and ionic strength) require only slight modification to change aggregation rates dramatically. The trends in aggregation behavior that we have presented are a paradigm, but ultimately $\mathbf{A}\boldsymbol{\beta}$ toxicity should be correlated with the aggregation state of the specific samples investigated. Consideration of the aggregation process during experimental design will avail the investigator increased reproducibility in toxicity assays.

CONCLUSIONS

We have developed ^a paradigm for studying the aggregation behavior of AB as it proceeds from a monomeric starting state to a fibrillar final state. A β 40 and A β 42 remain monomeric in DMSO or HFIP up to millimolar concentrations but aggregate heavily in water, PBS, or ACN/TFA, at submillimolar concentrations. In PBS, aggregated $A\beta40$ forms several types of species, including large, probably visible, aggregates with a sedimentation coefficient of \sim 50,000 S, small, soluble aggregates with $s \sim 30$ S, and monomer. Aggregation kinetics are strongly dependent upon sample and environmental conditions. Aggregation is very rapid (seconds) near the pl of the peptide (pH 5-6). Outside of this range, aggregation of $A\beta42$ remains rapid (minutes), whereas A β 40 aggregation slows (hours to days). A β aggregation exhibits ionic strength and temperature dependence indicative of an aggregation being driven by a hydrophobic effect. In addition, aggregation of AB40 displays threshold-type behavior, which indicates that the ratedetermining step is the formation of a multimeric seed. When mixed together as monomers, $A\beta40$ (or other $A\beta$ fragments) and $A\beta$ 42 aggregate at a rate much slower than $A\beta$ 42 by itself. This retardation of aggregation rate is dose dependent and is observed most specifically for $A\beta40$. As less of the intact \overrightarrow{AB} structure is retained, peptides are less competent to inhibit $A\beta$ 42 aggregation. In addition, preformed aggregates of $A\beta42$ are capable of seeding $A\beta40$ aggregation in a dose-dependent fashion. The interplay in the aggregation kinetics of $A\beta40$ and $A\beta42$ suggests that relative concentrations of $A\beta42$ could be a factor in $A\beta$ deposition.

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