

# **A kinetic and thermodynamic understanding of O<sub>2</sub> tolerance in [NiFe]-hydrogenases**

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## **Supporting information**

### **S1. The Rates of O<sub>2</sub> Reaction**

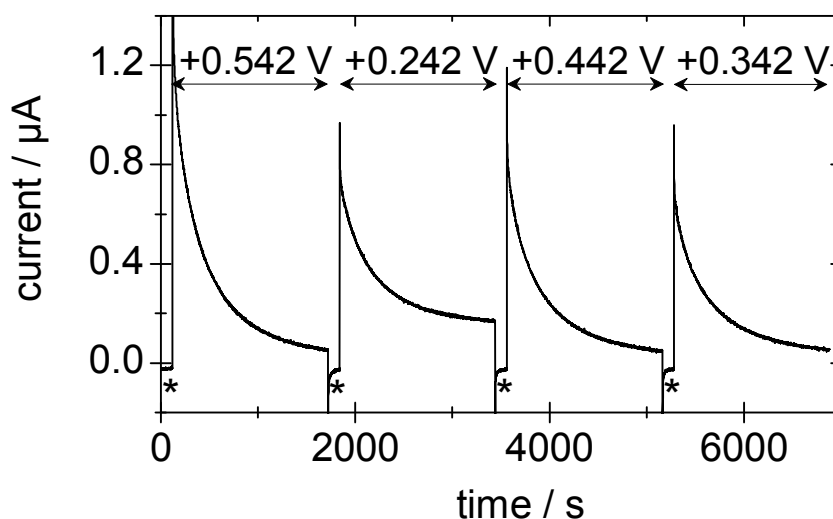
As mentioned in the text, not all O<sub>2</sub>-reaction rate data fit cleanly to a single exponential process. Data were analyzed by three methods: by fitting the entire current decay to a single exponential, by concentrating on the initial rapid decay and fitting a single exponential to this data, or by fitting to two processes, one fast and one slower. Table S1 summarizes the rates thus obtained; whilst the precise values differ significantly between analyses, the *trends* in these values are consistent between data sets.

**Table S1.** Detailed analysis of the rates of O<sub>2</sub> reaction, using three alternative methods to extract rate constants from current vs. time data. The values in bold are shown in the main text.

Potential (V vs. SHE)	+0.192	+0.262	+0.332	+0.402
Rate of O <sub>2</sub> reaction (s <sup>-1</sup> )				
<i>determined by fitting a single exponential curve to all data points</i>	0.06	0.05	0.05	0.06
<b>determined by fitting a single exponential curve to only initial, rapid current decay</b>	<b>0.11</b>	<b>0.10</b>	<b>0.10</b>	<b>0.11</b>
<i>determined by fitting two exponential curves to all data points, one with a high rate constant, one with a lower rate</i>	0.13	0.13	0.14	0.15
	0.03	0.03	0.03	0.03
<i>All values were recorded at pH 5.5, 10 °C</i>				
pH	4.5	5.5	6.5	
Rate of O <sub>2</sub> reaction (s <sup>-1</sup> )				
<i>determined by fitting a single exponential curve to all data points</i>	0.07	0.06	0.06	
<b>determined by fitting a single exponential curve to only initial, rapid current decay</b>	<b>0.12</b>	<b>0.11</b>	<b>0.11</b>	
<i>determined by fitting two exponential curves to all data points, one with a high rate constant, one with a lower rate</i>	0.15	0.13	0.12	
	0.03	0.03	0.03	
<i>All values were recorded at 10 °C, at a constant overpotential (driving force) of +523 mV relative to the thermodynamic H<sup>+</sup>/H<sub>2</sub> cell potential at each pH.</i>				
Temperature (°C)	0	10	20	30
Rate of O <sub>2</sub> reaction (s <sup>-1</sup> )				
<i>determined by fitting a single exponential curve to all data points</i>	0.04	0.06	0.10	0.09
<b>determined by fitting a single exponential curve to only initial, rapid current decay</b>	<b>0.06</b>	<b>0.11</b>	<b>0.19</b>	<b>0.31</b>
<i>determined by fitting two exponential curves to all data points, one with a high rate constant, one with a lower rate</i>	0.08	0.13	0.22	0.36
	0.02	0.03	0.03	0.02
<i>All values were recorded at pH 5.5, at a constant overpotential (driving force) of +523 mV relative to the thermodynamic H<sup>+</sup>/H<sub>2</sub> cell potential at each temperature.</i>				

## S2. The rate of anaerobic inactivation

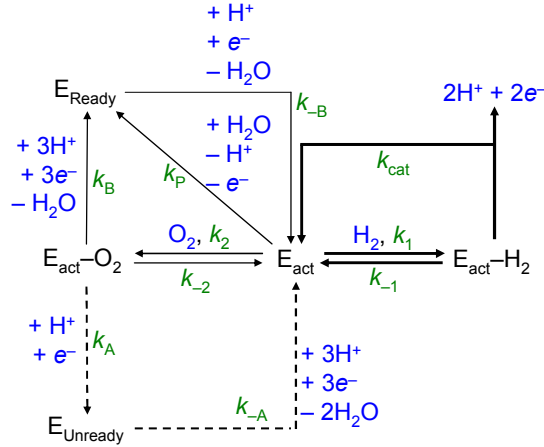
Typical experiments to measure the rate of anaerobic inactivation are shown in Figure S2. An electrode modified with *Re* H16 MBH was initially held at  $-0.508$  V vs. SHE to ensure that all the enzyme was active. The electrode was then stepped to a high potential, causing the enzyme to anaerobically inactivate. Stepping the electrode back to  $-0.508$  V reactivated the enzyme, allowing multiple experiments to be performed on the same enzyme film. The inactivation traces fitted well to a single exponential decay corresponding to an inactivation rate  $\sim 0.003$  s $^{-1}$ ; the rate was independent of the electrode potential in the range  $0.242$  V –  $0.542$  V.



**Figure S2.** A typical experiment to determine the rate of anaerobic inactivation of *Re* MBH. The electrode potential was stepped between a low value ( $-0.508$  V, indicated \*) to activate the enzyme, and a high value (indicated in the figure) at which potential the enzyme anaerobically inactivates. Experimental conditions were: pH 5.5,  $10$  °C,  $100\%$  H $_2$ , electrode rotation rate =  $2500$  rpm.

### S3. The Derivation of Equation 1

Equation 1 was derived as follows, starting from the catalytic scheme shown in the text and reproduced below (Figure S3).



**Figure S3.** The kinetic scheme used to model O<sub>2</sub> tolerance. *Re* MBH is abbreviated, for clarity, to the single initial 'E', and is described as being in its reduced, active form (E<sub>act</sub>), forming an adduct with either H<sub>2</sub> or O<sub>2</sub> (E<sub>act</sub>-H<sub>2</sub> and E<sub>act</sub>-O<sub>2</sub>, respectively) or being in either the Ready state (E<sub>Ready</sub>) or the Unready (E<sub>Unready</sub>) state.

For ease of notation, we make the following substitutions:

$$\begin{aligned}
 [E_{\text{act}}] &= \beta & [E_{\text{act}}]_0 &= \beta_0 \\
 [E_{\text{act}} - \text{H}_2] &= \alpha & [E_{\text{act}} - \text{O}_2] &= \sigma \\
 [E_{\text{Ready}}] &= \varepsilon & [E_{\text{Unready}}] &= \omega
 \end{aligned} \tag{1}$$

The steady state approximation is applied to all intermediate species, generating the following expressions for the concentrations of each:

$$\frac{d\alpha}{dt} = k_1 [\text{H}_2] \beta - (k_{-1} + k_{\text{cat}}) \alpha = 0 \quad \Rightarrow \quad \alpha = \frac{k_1 [\text{H}_2] \beta}{k_{-1} + k_{\text{cat}}} \tag{2}$$

$$\frac{d\sigma}{dt} = k_2 [\text{O}_2] \beta - (k_{\text{B}} + k_{\text{A}} + k_{-2}) \sigma = 0 \quad \Rightarrow \quad \sigma = \frac{k_2 [\text{O}_2] \beta}{k_{\text{B}} + k_{\text{A}} + k_{-2}} \tag{3}$$

$$\frac{d\varepsilon}{dt} = k_p\beta + k_B\sigma - k_{-B}\varepsilon = 0 \quad \Rightarrow \quad \varepsilon = \frac{k_p\beta + k_B\sigma}{k_{-B}} \quad [4]$$

$$\frac{d\omega}{dt} = k_A\sigma - k_{-A}\omega = 0 \quad \Rightarrow \quad \omega = \frac{k_A\sigma}{k_{-A}} \quad [5]$$

The total concentration of active enzyme is given by the difference between the initial concentration of enzyme,  $[E_{act}]_0 = \beta_0$ , and the concentration of all intermediate species, *i.e.*:

$$\beta = \beta_0 - \alpha - \sigma - \varepsilon - \omega \quad [6]$$

The Michaelis constant for  $H_2$ ,  $K_M^{H_2}$ , is defined as:

$$K_M^{H_2} = \frac{k_{-1} + k_{cat}}{k_1} \quad [7]$$

and an inhibition constant for  $O_2$  inhibition,  $K_I^{O_2}$ , is defined as:

$$K_I^{O_2} = \frac{k_B + k_A + k_{-2}}{k_2} \quad [8]$$

From equation 2:

$$\alpha = \frac{[H_2]}{K_M^{H_2}} (\beta_0 - \alpha - \sigma - \varepsilon - \omega) \quad [9]$$

and thus

$$\alpha = \frac{\beta_0 - \sigma - \varepsilon - \omega}{1 + \frac{K_M^{H_2}}{[H_2]}} \quad [10]$$

Substituting in, we obtain:

$$\alpha = \frac{\beta_0 - \sigma - \left( \frac{k_p\beta + k_B\sigma}{k_{-B}} \right) - \left( \frac{k_A\sigma}{k_{-A}} \right)}{1 + \frac{K_M^{H_2}}{[H_2]}} \quad [11]$$

Solving for  $\sigma$  leads to

$$\sigma = \frac{\beta_0 - \alpha \left( 1 + \frac{K_M^{H_2}}{[H_2]} + \frac{k_p}{k_{-B}} \frac{K_M^{H_2}}{[H_2]} \right)}{1 + \frac{k_B}{k_{-B}} + \frac{k_A}{k_{-A}}} \quad [12]$$

Similarly, from equation 3, we obtain:

$$\sigma = \frac{[O_2]}{K_I^{O_2}} (\beta_0 - \alpha - \sigma - \varepsilon - \omega) \quad [13]$$

and thus

$$\sigma = \frac{\beta_0 - \alpha - \varepsilon - \omega}{1 + \frac{K_I^{O_2}}{[O_2]}} \quad [14]$$

From Equation 10, by substituting in Equations 4 and 5, we obtain:

$$\sigma = \frac{\beta_0 - \alpha \left( 1 + \frac{k_p}{k_{-B}} \frac{K_M^{H_2}}{[H_2]} \right)}{1 + \frac{K_I^{O_2}}{[O_2]} + \frac{k_B}{k_{-B}} + \frac{k_A}{k_{-A}}} \quad [15]$$

As equations 12 and 15 are both expressions for  $\sigma$ , they must be equal to one another,

and so we write

$$\frac{\beta_0 - \alpha \left( 1 + \frac{K_M^{H_2}}{[H_2]} + \frac{k_p}{k_{-B}} \frac{K_M^{H_2}}{[H_2]} \right)}{1 + \frac{k_B}{k_{-B}} + \frac{k_A}{k_{-A}}} = \frac{\beta_0 - \alpha \left( 1 + \frac{k_p}{k_{-B}} \frac{K_M^{H_2}}{[H_2]} \right)}{1 + \frac{K_I^{O_2}}{[O_2]} + \frac{k_B}{k_{-B}} + \frac{k_A}{k_{-A}}} \quad [16]$$

Solving for  $\alpha$  yields

$$\alpha = \frac{\beta_0 \frac{K_I^{O_2}}{[O_2]}}{\frac{K_M^{H_2}}{[H_2]} \left( 1 + \frac{K_I^{O_2}}{[O_2]} + \frac{k_B}{k_{-B}} + \frac{k_A}{k_{-A}} \right) + \frac{K_I^{O_2}}{[O_2]} \left( 1 + \frac{K_M^{H_2}}{[H_2]} \frac{k_p}{k_{-B}} \right)} \quad [17]$$

The overall rate of reaction,  $v$ , is defined as

$$v = k_{\text{cat}}\alpha \quad [18]$$

and the maximum rate of reaction is obtained when  $\alpha = \beta_0$

$$v_{\text{max}} = k_{\text{cat}}\beta_0 \quad [19]$$

The relationship between the rate of catalysis and the catalytic current,  $i$ , is given by

$$i = nFA\Gamma k_{\text{cat}} \quad [20]$$

and we thus arrive at the final equation:

$$\frac{i}{i_{\text{max}}} = \frac{\frac{K_1^{\text{O}_2}}{[\text{O}_2]}}{\frac{K_{\text{M}}^{\text{H}_2}}{[\text{H}_2]} \left( 1 + \frac{K_1^{\text{O}_2}}{[\text{O}_2]} + \frac{k_{\text{B}}}{k_{-\text{B}}} + \frac{k_{\text{A}}}{k_{-\text{A}}} \right) + \frac{K_1^{\text{O}_2}}{[\text{O}_2]} \left( 1 + \frac{K_{\text{M}}^{\text{H}_2}}{[\text{H}_2]} \frac{k_{\text{p}}}{k_{-\text{B}}} \right)} \quad [21]$$