SUPPLEMENTAL MATERIAL

Text S1

Thermodynamic symbols and units

aq = aqueous state

 $\Delta_r ATP(l) =$ change in ATP for reaction $l \pmod{l}$

 $c_{i,t}$ = concentration of reactant *i* at time *t* (*M*)

 $C_{pm}^{\circ}(j)$ = standard molar heat capacity of species *j* (J/mol/K) $C_{pm}^{0}(j)$ = standard transformed molar heat capacity of species *j* (J/mol/K) *I* = ionic strength (*M*) g = gaseous state

 $\Delta_{f}G_{j}^{0} = \text{standard Gibbs energy of formation of species } j \text{ (kJ/mol)}$ $\Delta_{f}G_{j}^{0} = \text{standard transformed Gibbs energy of formation of species } j \text{ (kJ/mol)}$ $\Delta_{f}G_{l}^{0} = \text{standard transformed Gibbs energy of formation of reactant } i \text{ (kJ/mol)}$ $\Delta_{r}G^{0}(l) = \text{standard transformed Gibbs energy of reaction } l \text{ (kJ/mol)}$ $\Delta_{f}H_{j}^{0} = \text{standard enthalpy of formation of species } j \text{ (kJ/mol)}$ $\Delta_{f}H_{j}^{0} = \text{standard transformed enthalpy of formation of species } j \text{ (kJ/mol)}$ $\Delta_{f}H_{i}^{0} = \text{standard transformed enthalpy of formation of species } j \text{ (kJ/mol)}$ $\Delta_{r}H_{i}^{0} = \text{standard transformed enthalpy of reaction } l \text{ (kJ/mol)}$ $\Delta_{r}H_{i}^{0} \text{ enthalpy of reaction at time } t \text{ (kJ/mol)}$ $\Delta_{r}H_{l} \text{ enthalpy of reaction at time } t \text{ (kJ/mol)}$

 $\Delta_r H_t$ (cal) = enthalpy change in the calorimetric experiment at time *t* (kJ/mol) N' = number of reactants

 $N_{C}(j)$ = number of carbon atoms in species *j* (mol/mol) $\overline{N}_{C}(i)$ = number of carbon atoms in reactant *i* (mol/mol) $N_{\rm H}(j)$ = number of hydrogen atoms in species j (mol/mol) $\overline{N}_{H}(i)$ = number of hydrogen atoms in reactant *i* (mol/mol) $\Delta_r N_H(l)$ = change in binding of hydrogen atoms in reaction *l* (mol/mol) q = heat flow into a system (kJ) dq_t Vdt = rate of heat production (W/L) dq_t^* Vdt = rate of heat production corrected for protonation of buffer (W/L) $\frac{q_t}{V}$ = integrated heat production (kJ/L) $\frac{q_t^*}{V}$ = integrated heat production corrected for protonation of buffer (kJ/L) $r_j = \text{mol fraction of species } i \text{ in a reactant (mol/mol)}$ T = temperature (K) V =volume (L) $v'_i(l)$ = stoichiometric number of reactant *i* in reaction *l* (mol/mol) z_j = charge number of species

Reactant	Species or linkage	z_j	$N_{H}(j)$	$N_{C}(j)$	$\Delta_{f}G_j^\circ$	$\Delta_{f} {H}_j^\circ$	Source	$C_{pm}^{\circ}(j)$	Source
Acetate	CH ₃ COO ⁻ (aq)	-1	3	2	-369.32	-486.01	(1)	86.19	(1)
	CH ₃ COOH(aq)	0	4	2	-396.48	-485.76	(1)	169.70	(1)
Butyrate	CH ₂ (CH ₂) ₂ COO ⁻ (aq)	-1	7	4	-354.18	-538.19	(1)	133.05	(1)
	CH ₂ (CH ₂) ₂ COOH(aq)	0	8	4	-381.62	-535.34	(1)	127.61	(1)
$CO_2(g)$	$CO_2(g)$	0	0	1	-394.36	-393.5	(2)	37.11	(3)
CO ₂ tot	$CO_2(aq) + H_2O(l)$	0	2	1	-623.16	-699.64	(2)	318.29	(4)
	$CO_{3}^{-2}(aq)$	-2	0	1	-527.81	-677.14	(2)	-55.00	(5)
	HCO ₃ -(aq)	-1	1	1	-586.77	-691.99	(2)	-302.00	(5)
	$H_2CO_3(aq)$	0	2	1	-606.33	-694.91	(2)	69.00	(5-6)
Fructose	$C_{6}H_{12}O_{6}(aq)$	0	12	12	-915.51	-1259.38	(2)	369.00	(7)
Galactose	$C_{6}H_{12}O_{6}(aq)$	0	12	12	-908.93	-1255.20	(2)	319.00	(7)
Glucose	$C_{6}H_{12}O_{6}(aq)$	0	12	6	-915.90	-1262.19	(2)	336.30	(7)
H^{+}	H ⁺ (aq)	1	1	0	0.00	0.00	(2)	0.00	(3)
$H_2(g)$	$H_2(g)$	0	2	0	0.00	0.00	(2)	28.82	(3)
$H_2(aq)$	$H_2(g)$	0	2	0	0.00	0.00	(2)	28.82	(3)
H ₂ O	$H_2O(l)$	0	2	0	-237.19	-285.83	(2)	75.29	(3)
Lactate	CH ₃ CH(OH)COO ⁻ (aq)	-1	5	2	-516.72	-686.64	(2)	211.29	(8)
Mannose	$C_6H_{12}O_6(aq)$	0	12	12	-910.00	-1258.66	(2)	342.00	(7)
$CH_4(g)$	CH ₄ (g)	0	4	1	-50.72	-74.81	(2)	35.31	(3)
CH ₄ (aq)	CH ₄ (aq)	0	4	1	-34.33	-89.04	(2)	0.00	NA^b
Propionate	CH ₃ CH ₂ COO ⁻ (aq)	-1	5	3	-363.09	-513.08	(1)	110.88	(1)
	CH ₃ CH ₂ COOH(aq)	0	6	3	-390.99	-512.41	(1)	253.13	(1)
Reserve carbohydrate	Glucose-glucose ($\alpha 1 \rightarrow 4$) linkage	0	0	0	-15.65	4.53	(9-10)	39.50	(9)

TABLE S1 Thermodynamic properties of species and linkages relevant to glucose use in rumen microbes $(T = 25^{\circ}C, pH = 0, I = 0)^{a}$

	Glucose-glucose ($\alpha 1 \rightarrow 6$) linkage	0	0	0	-7.06	-5.80	(11-12)	0.00	NA
Valerate	CH ₃ (CH ₂) ₃ COO ⁻ (aq)	-1	9	5	-345.72	-562.25	(1)	160.25	(1)
	CH ₃ (CH ₂) ₃ COOH(aq)	0	10	5	-373.38	-559.36	(1)	260.66	(1)

^{*a*}See Text S1 in the supplemental material for symbols and units ^{*b*}Not available and assumed to be 0

Reactant	Species or linkage	$C'^0_{pm}(j)$	$\Delta_{f} {G'}_j^0$	$\Delta_{f} {H'}^0_j$	r _j
Acetate	CH ₃ COO ⁻ (aq)	75.48	-241.09	-485.93	0.995
	CH ₃ COOH(aq)	148.29	-227.46	-485.64	0.005
Butyrate	$CH_2(CH_2)_2COO^-(aq)$	100.93	-57.88	-539.71	0.994
	CH ₂ (CH ₂) ₂ COOH(aq)	84.79	-44.62	-538.07	0.006
$CO_2(g)$	$CO_2(g) + H_2O(l)$	37.11	-394.43	-392.98	1.000
CO ₂ tot	$CO_2(aq) + H_2O(l)$	307.59	-537.31	-696.31	0.161
	$CO_{3}^{-2}(aq)$	-33.59	-524.34	-675.65	0.014
	HCO ₃ (aq)	-302.00	-541.29	-696.22	0.837
	$H_2CO_3(aq)$	58.29	-519.75	-695.07	0.000
Fructose	C ₆ H ₁₂ O ₆ (aq)	304.77	-399.30	-1260.51	1.000
Galactose	$C_6H_{12}O_6(aq)$	254.77	-395.31	-1257.32	1.000
Glucose	$C_6H_{12}O_6(aq)$	272.07	-405.06	-1264.25	1.000
$H_2(g)$	$H_2(g)$	18.12	82.45	-0.72	1.000
$H_2(aq)$	$H_2(aq)$	-10.71	101.09	-5.33	1.000
H_2O	$H_2O(l)$	64.59	-152.49	-285.90	1.000
Lactate	CH ₃ CH(OH)COO ⁻ (aq)	189.88	-303.61	-685.94	1.000
Mannose	$C_6H_{12}O_6(aq)$	277.77	-390.75	-1260.02	1.000
CH ₄ (g)	CH ₄ (g)	13.90	115.32	-76.57	1.000
CH ₄ (aq)	CH ₄ (aq)	-21.41	133.17	-91.30	1.000
Propionate	CH ₃ CH ₂ COO ⁻ (aq)	89.47	-150.84	-513.79	0.993
	CH ₃ CH ₂ COOH(aq)	221.01	-138.06	-512.24	0.007
Reserve	Glucose-glucose ($\alpha 1 \rightarrow 4$) linkage	39.50	-16.62	5.08	NA ^c
carbohydrate	Glucose-glucose ($\alpha 1 \rightarrow 6$) linkage	0.00	-7.12	-5.80	NA
valerate	$CH_3(CH_2)_3COO(aq)$	11/.42	54.55	-364.51	0.993
	CH ₃ (CH ₂) ₃ COOH(aq)	207.13	47.52	-561.35	0.007

TABLE S2 Thermodynamic properties of species and linkages relevant to glucose use in rumen microbes $(T = 39^{\circ}C \text{ unless otherwise noted}, \text{pH} = 6.8, I = 0.25)^{a,b}$

^{*a*}See Text S1 in the supplemental material for symbols and units

 ${}^{b}T = 25^{\circ}\text{C for } C'^{0}_{pm}(j)$

^cNot applicable

-39 C, pH -0.8 , $I - 0.23$)				
Reactant	$\Delta_{f} G'^0_i$	$\Delta_{f} {H'}^0_i$	$\overline{N}_{H}(i)$	$\overline{N}_C(i)$
Acetate	-241.11	-485.93	3.01	2.00
Butyrate	-57.90	-539.70	7.01	4.00
$CO_2(g)$	-394.43	-392.98	0.00	1.00
CO ₂ tot	-541.45	-696.20	2.00	1.00
Fructose	-399.30	-1260.51	12.00	6.00
Galactose	-395.31	-1257.32	12.00	6.00
Glucose	-405.06	-1264.25	12.00	6.00
$H_2(g)$	83.05	-0.72	2.00	0.00
H ₂ (aq)	101.69	-5.33	2.00	0.00
H ₂ O	-152.49	-285.90	2.00	0.00
Lactate	-303.61	-685.94	5.00	3.00
Mannose	-390.75	-1260.02	12.00	6.00
$CH_4(g)$	116.52	-76.57	4.00	1.00
CH ₄ (aq)	134.37	-91.30	4.00	1.00
Propionate	-150.86	-513.78	5.01	3.00
Reserve carbohydrate	-268.60	-973.94	10.00	6.00
Valerate	34.53	-564.49	9.01	5.00

TABLE S3 Thermodynamic properties of reactants relevant to glucose use in rumen microbes ($T = 39^{\circ}$ C, pH = 6.8, I = 0.25)^{*a*}

^{*a*}See Text S1 in the supplemental material for symbols and units



FIG S1 Use of carbohydrate energy by microbes. Adapted from (13).



FIG S2 Cell components of mixed rumen microbes in response to 20 mM glucose dosed at 20 min. (A) Reserve carbohydrate. (B) Protein. (C) DNA. (D) RNA. Reserve carbohydrate was expressed in g/L (for comparison to other components) and mM (for comparison to concentration of glucose dosed), both in monomeric glucose equivalents. Data represent one experiment, and each datum point represents one sample that was analyzed in triplicate.

FIG S3 Example illustration of the calculations and overall approach used to quantify energyspilling from mixed ruminal microbes from cow 472 dosed with 20 mM of glucose. Panel A (reserve carbohydrate) appears in the main text as Fig. 1D. The units of reserve carbohydrate concentration are expressed in monomeric glucose equivalents to be in same units as the glucose dose. From these data, the slope corresponding with each 1-s time increment was plotted in panel B and designated as the numerical derivative of reserve carbohydrate with respect to time. Fermentation products over time are presented in Panel C, which appears in the main text as Fig. 1H. The molar heat of reserve carbohydrate synthesis over time (Panel D) was calculated when individual measured values of end-products from Panel C and the parameter values in Table 1 were inputted into Equation 7 from the text. The rate of heat production accounted by reserve carbohydrate synthesis is shown in Panel E. At 1-s time intervals, these points were calculated by multiplying values illustrated in Panel B by absolute values illustrated in Panel D. The integrated heat production accounted by reserve carbohydrate synthesis (Panel F) was calculated using the rectangle method for each 1-s time increment. The rates of total heat production after glucose dosage and from endogenous metabolism are both shown in Panel G (which also appears in the main text as Fig. 1J). Total rate of total heat production is output from the calorimeter. The rate of endogenous heat production was set equal to the average rate of heat production prior to dosing. It was assumed that this would not remain constant over the incubation, but it would decline by 7.3%/h (see Results). At each 1-s time increment, these rates were integrated using the rectangle rule. These integrated heat production values over time are illustrated in Panel H (which also appears as Fig. 3B in the main text). The integrated heat production accounted by reserve carbohydrate synthesis (i.e., the area from Panel F) was stacked on top of endogenous heat production in Panel G. The estimate of energy spilling was determined by difference of the integrated total heat production minus the integrated heat production that was accounted by endogenous metabolism minus the integrated heat production that was accounted by reserve carbohydrate synthesis.



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