Elucidating Oxygen Reduction Active Sites in Pyrolyzed Metal-Nitrogen Coordinated Non-Precious Electrocatalyst Systems.

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Table S1: Electrochemical parameters of carbon supported polymer-metal composites-PVAG-Fe and xBPEI-Fe and developed by UNM Fe-8AAPyr with the sacrificial support method whose high performance has been previously reported by Serov et al¹, compared to Tanaka Pt/C. (RDE in 0.1M HClO₄: Scan rate: 20mV/s. Loading of MNC catalysts: $0.6mg/cm^2$ on 5.61mm glassy carbon disc electrode. Loading of Pt/C: catalyst $25\mu g_{Pt}/cm^2$

Catalyst	Tafel slope	i _{lim}	i @ 0.8V (vs.
	[mV/decade]	$[mA/cm^2]$	RHE)
			[mA/cm ²]
30% Pt/C, 25μ g/cm ²	61	4.4	3.6
UNM Fe8AAPyr, 0.6mg/cm ²	56	6.3	1.0
NEU PVAGFe, 0.6mg/cm ²	60	6.8	0.5
NEU xBPEIFe, 0.6mg/cm ²	58	5.6	0.4

Table S2: Potential dependent FT EXAFS fitting results of PVAG-Fe catalyst collected insitu at Fe K-edge (7112eV) in O₂ saturated 0.1M HClO₄: Fitting results of theoretical FEFF8 calculations of the Fe-N_x/O peak, where CN = coordination number, and R = Fe-N bond length [Å].

Potential	CN _{Fe-N/O}	R _{Fe-N} (Å)
0.3V	4.2+/-0.5	2.08+/-0.02
0.9V	4.9+/-0.8	2.05+/-0.02

Figure S1: ORR polarization curves at 0.12 mg/cm^2 and 0.6 mg/cm^2 catalyst loading in 0.1M HClO₄ (a) and 0.1M KOH (b), and c) RDE polarization curves of oxygen (ORR) and hydrogen peroxide (HRR) reduction in 0.1M HClO₄ (black) and 0.1 M KOH (blue) (RDE: RHE ref., GC 0.2472cm², 900rpm, 20mV-s and 0.6 mg/cm² catalyst loading)



Figure S1a-b represents ORR polarization curves and yield of peroxide intermediate (as inset) in 0.1M HClO₄ (a) and 0.1M KOH (b). The improvement in kinetics with the loading observed in acid (Figure S2b), a typical behavior of pyrolyzed MNC's, is a result of increased density of active sites in the catalyst. The consistently low relative yield of peroxide intermediate (1%) even in low loading suggests that the PVAG-Fe catalyst facilitates ORR mainly through overall 4e mechanism. Considering however the apparent electron transferred between 3.2e-4e obtained by Koutecky-Levich at low and high loading respectively, the PVAG-Fe forms both water and peroxide as ORR final products suggesting 2x2e ORR mechanism. This discrepancy can be explained by disproportionation of some of the peroxide product before its further electroreduction know to occur in acid environment. On the hand, no change in kinetics upon increased catalyst loading in alkaline with the negligible yield of H₂O₂ (based on ring current and Koutecky-Levich equation) is consistent with true overall 4e ORR mechanism believed to take place in high pH media facilitated by catalyst with Fe-N₂₊₂ type active centers 2,3 . Fe-N₂₊₂ sites are able to facilitate efficient single site oxygen reduction to water through stabilization of peroxide intermediate (HO_2^{-}) on the catalytic surface (Figure S1c). The much smaller peroxide reduction currents in acid, suggest that only a small fraction of the intermediate undergo a direct reduction to water before it desorbs from the catalytic site. As already mentioned, the remaining H₂O₂ which detaches from the Fe center before its further reduction and is subjected to disproportionation or one-electron reduction ⁴ as shown below:

$$\frac{\text{H}_2\text{O}_2 \rightarrow \text{H}_2\text{O} + \frac{1}{2}\text{O}_2(2)}{\text{Fe}_{\text{surf}}^{2+} + \text{H}_2\text{O}_2 \rightarrow \text{Fe}_{\text{surf}}^{3+} + \text{HO}^{\bullet} + \text{HO}^{\bullet}(2-1)}$$
$$\text{HO}^{\bullet} + \text{H}_2\text{O}_2 \rightarrow \text{HOO}^{\bullet} + \text{O}_2(2-2)$$
$$\text{HOO}^{\bullet} + \text{Fe}_{\text{surf}}^{3+} + e^{-} \rightarrow \text{Fe}_{\text{surf}}^{2+} + \text{H}^{+} + \text{O}_2(2-2)$$

Figure S2: Effect of catalyst distortion on Koutecky-Levich plots (solid line represents initial performance, and dotted line represents post-treatment performance (a), and relative peroxide yield change versus level of $Fe^{0}/Fe_{x}O_{y}$ destruction (b). The vertical red arrow indicates increase of peroxide yield with higher level of destruction as the concentration of the external H₂O₂ increased between 0, 0.03, 0.06, 0.12, 0.15 mmol/L (RRDE: 0.1M HClO₄, catalyst loading 0.12mg/cm²).



Figure S3: Theoretical XANES and delta-mu signatures of Fe-N₄C₁₀ and Fe-Fe janin cluster (representing Fe_{NPs} when the O interacts with the Fe atom at fcc position) plotted individually (a), and as linear combination of the two (Fe-N₄C₁₀ /Fe_{NPs}) at various ratios (b). % of each of the Fe-forms in the PVAG-Fe was estimated by comparing ratio between the positive delta-mu features (cm_{max1})/(cm_{max2}) of the experimental data with the theoretical delta-mu signatures of (c). The best agreement with the experimental delta mu signature was obtained with the theoretical model containing 93%Fe-N₄C₁₀+7%Fe_{NPs} (shown in the main manuscript, Figure 4). Note that the structural models were utilized for delta-mu analysis using FEFF8 simulation. Theoretical Delta-mu signatures were obtained by subtracting the model XANES signatures according to $\Delta\mu$ (Fe-N₄C₁₀) = μ (O-Fe-N₄C₁₀) - μ (Fe-N₄C₁₀); and $\Delta\mu$ (Fe_{NPs}) = μ (O-Fe_{NPs}) - μ (Fe_{NPs}).



References:

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