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3 **Elevated levels of diesel range organic compounds in groundwater near**
4 **Marcellus gas operations are derived from surface activities**

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27 fracturing, natural gas extraction
28

29 **Analytical Methods**

30 *Sample Collection:* Groundwater wells were purged until temperature, pH, and electrical
31 conductance readings were stable. Shallow groundwater samples were collected in pre-
32 combusted 40-mL glass volatile organic analysis (VOA) vials containing 1-mL of 50%
33 v/v hydrochloric acid (HCl), capped without headspace, and stored on ice or at 4°C until
34 analysis. Samples were collected as close to the wellhead as possible and upstream of any
35 water treatment systems.

36 *Volatile Organic Compounds (VOCs):* We used a modified version of EPA Method 624
37 and 8015D as described in Getzinger et al. (2015) [1] for quantification and qualitative
38 identification of 50 unique VOCs via GC-FID and GC-MS (Table S1). Briefly, a 5-mL
39 aliquot of groundwater was purged with helium on a purge and trap concentrator and
40 subsequently transferred to a GC-FID (quantification with retention time identity
41 confirmation) or GC-MS (confirming qualitative identification) using a Restek
42 MegaMix™ standard mixture (Restek 502.2).

43 *Gasoline Range Organic Compounds (GRO):* We quantified GRO with the sample
44 preparation techniques described for the VOC analysis and used a GRO mix standard for
45 quantification (Restek #30065), following EPA Method 8015D. Chromatographic peaks
46 eluting within the retention time window of 2-methylpentane and 1,2,4-trimethylbenzene
47 were integrated and added together for a total signal representative of the organic
48 compounds with boiling points within the defined gasoline range [2].

49 *Diesel Range Organic Compounds (DRO):* We used a liquid-liquid extraction technique
50 to quantify DRO with EPA Method 8015D, as described in Getzinger et al. (2015) [1].
51 Approximately 500 mL of groundwater was extracted with 90:10
52 dichloromethane:methanol three times before rotary evaporation down to a final volume
53 of 1-1.5 mL. Samples were quantified with a Restek DRO mix standard (Restek 31064)
54 via GC-FID. Chromatographic peaks eluting within the retention time window of decane
55 (nC_{10}) and octacosane (nC_{28}) were integrated and added together for a total signal
56 representative of the organic compounds with boiling points within the defined diesel
57 range [2].

58 *Comprehensive two-dimensional gas chromatography:* Two Leco GC×GC systems were
59 used in this study: one coupled with a time-of-flight mass spectrometer (TOF-MS; Leco
60 Pegasus 4D) and one coupled to a flame ionization detector (FID) detector. They were
61 equipped with an Agilent 6890 GC (TOF-MS) and Agilent 7890 GC (FID system) and
62 configured with split/splitless auto injectors (7683B series) and a dual stage cryogenic
63 modulator (Leco, Saint Joseph, Michigan). Samples were injected in splitless mode. Two
64 capillary GC columns were fitted in each GC×GC instrument, with a cryogenic
65 modulator between the two. The first-dimension column was a non-polar Restek Rxi-
66 1ms, (60 m length, 0.25 mm I.D., 0.25 μm film thickness) and the second-dimension
67 separations were performed on a 50% phenyl polysilphenylene-siloxane column (SGE
68 BPX50, 1.0 m length, 0.10 mm I.D., 0.1 μm film thickness). The modulator between the
69 two columns operates with a liquid N₂ cold jet and dry N₂ hot jet operated at 10-15 °C
70 above the temperature of the main GC oven. Hydrogen was used as carrier gas at a

71 constant flow rate of 0.90 mL min⁻¹ on the GC×GC-FID and helium at a flow rate of 1.00
72 mL min⁻¹ on the GC×GC-TOF.

73

74 *GC×GC-TOFMS Method:*

75 The temperature program of the main oven started isothermal at 50 °C (15 min) and was
76 then ramped from 50 to 330 °C at 1.75 °C min⁻¹. The hot jet pulse width was 0.75 s and
77 the modulation period was 10 s with a 4.25 s cooling period between stages. The second
78 dimension oven was programmed from 55 °C (15 min) to 335 °C at 1.75 °C min⁻¹. The
79 TOF-MS data were sampled at an acquisition rate of 50 spectra per second. The transfer
80 line from the second oven to the TOFMS was deactivated fused silica (0.5 m length, 0.18
81 mm I.D.), constantly held at 315 °C. The TOF detector voltage was 1335 Volts and the
82 source temperature 220 °C. The mass spectrometer employs 70 eV electron ionization
83 and operates at a push pulse rate of 5 kHz allowing sufficient signal averaging time to
84 ensure good signal-to-noise ratios while still operating at a high enough data acquisition
85 rate to accurately process (signal average) spectra from the peaks eluting from the second
86 dimension column in this high resolution separation technique (GC×GC-TOF second
87 dimension peak widths range between 50 to 200 milliseconds).

88

89 *GC×GC-FID Method:*

90 For the GC×GC-FID analysis, 1 µL of each sample solution was injected into a 300 °C
91 splitless injector with a purge time of 0.5 min. The first-dimension column and the dual
92 stage cryogenic modulator resided in the main oven, whereas the second-dimension
93 column was fitted in a separate oven, allowing for independent temperature control of all
94 three. The temperature program of the main oven started isothermal at 40 °C (10 min)
95 and was then ramped from 40 to 335 °C at 1.25 °C min⁻¹. The second dimension oven
96 was programmed to remain isothermal at 45 °C for 10 minutes and then ramped from 45
97 to 340 °C at 1.25 °C min⁻¹. The hot jet pulse width was 0.50 seconds and the modulation
98 period was 7.5 seconds with a 3.25 second cooling period between stages.

99

100 *Inorganic constituents:* Inorganic compounds were analyzed from samples collected
101 either simultaneously with or prior to sample collection campaigns for organic
102 compounds. Analyses were performed via methods described by Warner et al. (2012) [3].

103 *Methane:* Methane was analyzed from samples collected simultaneously with or prior to
104 sample collection campaigns for organic compounds. Analyses were performed via
105 methods described by Jackson et al. (2013) and Darrah et al. (2014) [4, 5].

106 *Helium concentrations and noble gases:* Helium and heavier noble gases were analyzed
107 from samples collected simultaneously with or prior to sample collection campaigns for
108 organic compounds. Analyses were performed via methods described by Jackson et al.
109 (2013) and Darrah et al. (2014) [4, 5].

110 **Field Setting**

111 Samples were collected in northeastern Pennsylvania from three aquifers (Lock Haven,
112 Catskill, and Alluvium) overlying the Marcellus Shale in the northern Appalachian Basin.
113 Extensive descriptions of the geology and hydrogeologic settings can be found elsewhere
114 [3-7].

115

116 **Groundwater Contaminant Transport Calculations**

117 Subsurface groundwater transport of bis(2-ethylhexyl) phthalate through an aquifer
118 representative of northeastern Pennsylvania hydrogeology was estimated based on
119 calculations and physical parameters (Table S2) from various sources [8-13].
120

121 The compound-specific, sorption-retarded transport velocity, v_c , is given by:
122

$$v_c = \frac{v_w}{R} \quad \text{Eq. S1}$$

123

124 where v_w is the bulk groundwater flow and R is the retardation factor given by:
125

$$R = 1 + \rho_s \frac{1 - \phi}{\phi} K_d \quad \text{Eq. S2}$$

126

127 and ρ_s is the sediment or soil bulk density, ϕ is the porosity, and K_d is the solid-water
128 distribution coefficient. Here, we assume K_d is dominated by sorption to non-black
129 carbon organic carbon phases [10], and so:
130

$$K_d = K_{oc} * f_{oc} \quad \text{Eq. S3}$$

131

132 where K_{oc} is the organic carbon partition coefficient and f_{oc} is the fraction of organic
133 carbon in the porous medium.
134
135

136 **Modeling chemical transport across a polyethylene liner**

137 We deployed an analytical solution to calculate 1-D Fickian diffusion of bis(2-
138 ethylhexyl) phthalate (DEHP; diethylhexyl phthalate) across a 4-mm polyethylene (PE)
139 film, following Crank (1975) [14] and Schwarzenbach et al. (2002) [10]:
140

$$C_{PE}(x, t) = C_{PE}^* \operatorname{erfc} \left(\frac{x}{2(D_{PE}t)^{1/2}} \right) \quad \text{Eq. S4}$$

141 where $C_{PE}(x, t)$ (mass/cm³) is the concentration in the PE x cm from the side in contact
142 with retention pond water at some time, t (s), C_{PE}^* is the concentration at the boundary of
143 the PE equilibrated with water in the retention pond, and D_{PE} (cm²/s) is the diffusivity of
144 DEHP within the PE. By neglecting the additional resistances to mass transport provided
145 by a water-side diffusive boundary layer, diffusion within the soil porous media, and
146 retardation within the PE caused by pigments (e.g., carbon black, commonly used to
147 color the black PE liners used in containment ponds), this mathematical model simulates
148 the furthest possible distance the concentrations front could reach within the PE film.
149 D_{PE} for DEHP was estimated at $10^{-11.3}$ cm²/s, based on a relationship between molar
150 volume (MV) and $\log D_{PE}$ (Eq. S5) obtained from measured D_{PE} for PAHs (polycyclic
151 aromatic hydrocarbons) and PCBs (polychlorinated biphenyls) [15] and molar volume

152 estimated using the Sparc Performs Automated Reasoning in Chemistry (SPARC)
153 chemical property estimator.
154

$$\log D_{PE} (cm^2/s) = -0.014 MV (cm^3/mol) - 6.1 \quad Eq. S5$$

155
156 Using these values, DEHP will only diffuse 1 mm into the PE liner after 4 years (and
157 only 2×10^{-27} % of the original concentration). Using an even more conservative
158 calculation, employing 100-fold faster diffusion ($D_{PE}=10^{-9.3} cm^2/s$) indicates that only 2%
159 of DEHP could cross a 4-mm thick PE liner by 12 months.

160
161 We confirmed the application of the analytical solution by running an explicit, finite-
162 difference model to simulate transport across the PE using a previously prepared Matlab
163 code modified to reflect boundary conditions relevant to a pond-PE-porous media system
164 [16].
165
166

Table S1. Detection limits for DRO, GRO, and the targeted VOCs.

<i>Compound</i>	<i>LOD (ppb)</i>	<i>Compound</i>	<i>LOD (ppb)</i>
DRO	0.09	1,2-Dibromoethane	0.17
GRO	0.03	chlorobenzene	1.8
1,1-Dichloroethene	0.84	Ethylbenzene	2.9
Methylene chloride	1.0	m-Xylene+p-xylene	5.0
1,1-Dichloroethane	0.47	o-xylene	2.4
trans-1,2-Dichloroethene	1.2	styrene	0.26
2,2-Dichloropropane	2.4	bromoform	9.0
cis-1,2-dichloroethene	2.4	1,2,3-Trichloropropane	0.32
chloroform	2.7	Bromobenzene	0.54
Bromochloromethane	1.5	1,1,2,2-Tetrachloroethane	1.2
carbon tetrachloride	0.83	n-Propylbenzene	0.34
1,1,1-trichloroethane	0.83	2-Chlorotoluene	0.39
1,1-dichloropropene	0.83	1,3,5-Trimethylbenzene	0.19
Benzene	0.20	tert-Butylbenzene	0.37
1,2-dichloroethane	0.53	1,2,4-Trimethylbenzene	0.35
Trichloroethene	1.2	sec-Butylbenzene	0.42
1,2-Dichloropropane	0.70	1,3-Dichlorobenzene	0.55
bromodichloromethane	4.2	1,4-Dichlorobenzene	0.24
Dibromomethane	4.1	4-isopropyltoluene	0.24
cis-1,3-Dichloropropene	0.91	1,2-Dichlorobenzene	0.56
toluene	0.26	n-Butylbenzene	0.50
trans-1,3-Dichloropropene	1.2	1,2-Dibromo-3-chloropropane	7.2
1,1,2-Trichloroethane	1.5	1,2,4-Trichlorobenzene	1.0
Tetrachloroethene	0.41	Hexachlorobutadiene	2.6
1,3-Dichloropropane	0.66	Napthalene	0.88
dibromochloromethane	0.10	1,2,3-Trichlorobenzene	1.1

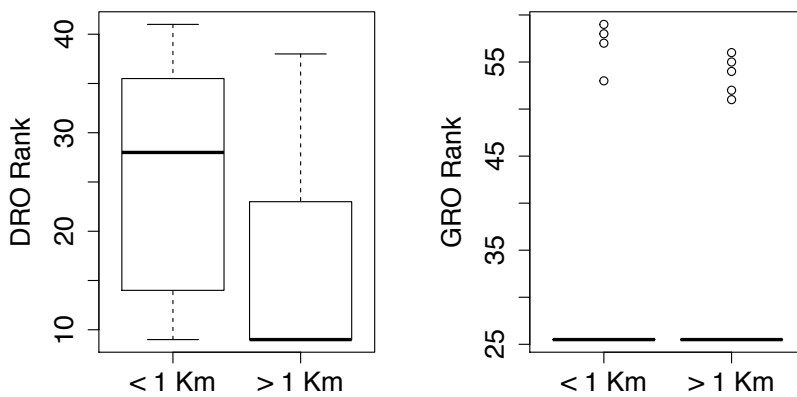
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169 **Table S2.** Parameters used for subsurface transport calculations of bis(2-ethylhexyl)
 170 phthalate.

Variable	High velocity	Low velocity
K_{oc} bis(2-ethylhexyl) phthalate	4.998	5.078
f_{oc} ($\text{kg}_{oc} \text{ kg}_{sed}^{-1}$)	0.001	0.1
ρ_s (kg L^{-1})	1.6	2.4
ϕ	0.08	0.25
v_w (km yr^{-1})	8.219	0.109
v_c (km yr^{-1})	7.527	0.0234

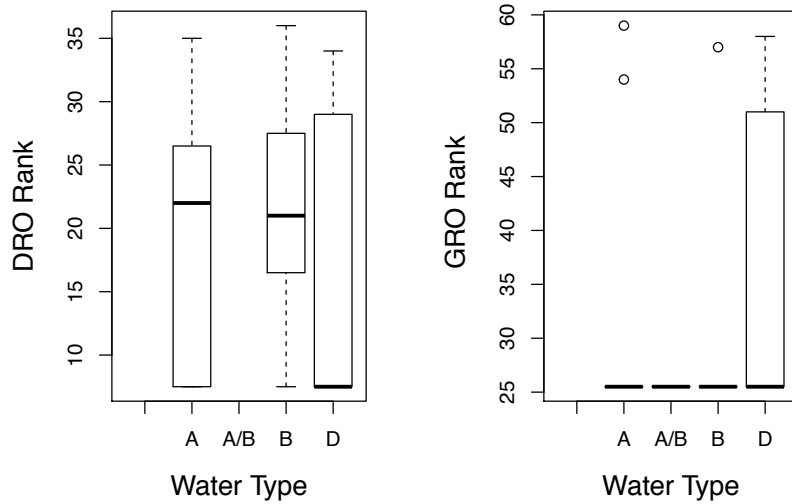
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173 **Figure S1.** Ranked comparison of DRO (left) and GRO (right) between active and non-
 174 active zones (active zone defined as < 1 km from a shale gas well). There was a statistical
 175 difference in DRO between zones ($p = 0.01$, Mann-Whitney U test) and no difference in
 176 GRO between zones ($p = 0.90$).
 177
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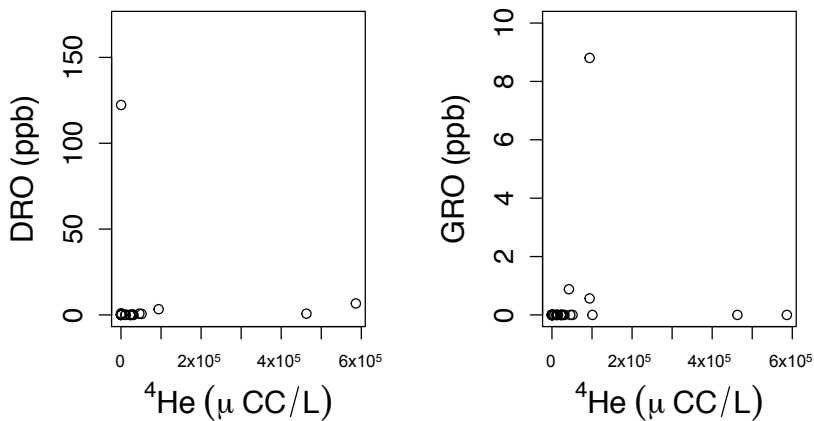
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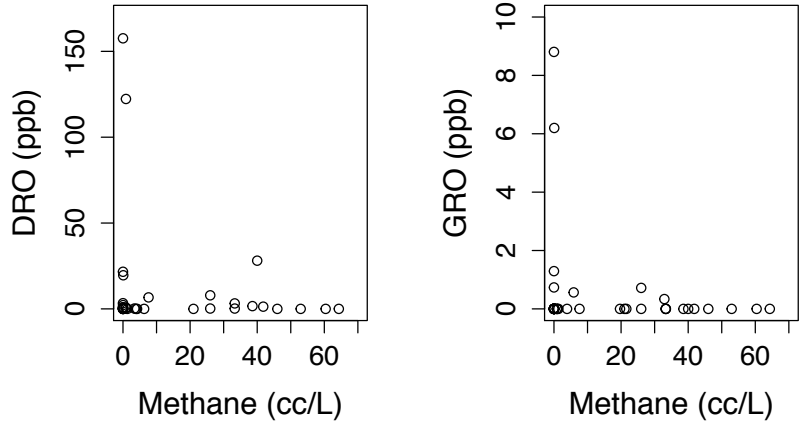
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 182 **Figure S2.** Ranked comparison of DRO (left) and GRO (right) with respect to different
 183 shallow groundwater types. Type D water has influence of Marcellus formation brine via
 184 natural connectivity [3]. There were no statistical differences in DRO or GRO between
 185 types (DRO, $p > 0.05$; GRO, $p > 0.05$; Kruskal-Wallis test).

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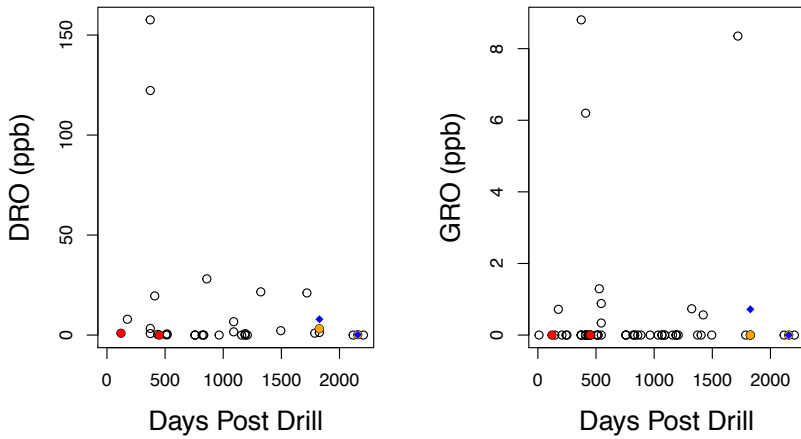
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 188 **Figure S3.** Relationship of DRO (left) and GRO (right) with respect to ^4He
 189 measurements taken either during the same sampling campaign or at a previous time.
 190 Statistical analysis showed no correlation (DRO, $p > 0.05$; GRO, $p > 0.05$, Spearman
 191 correlation).

192



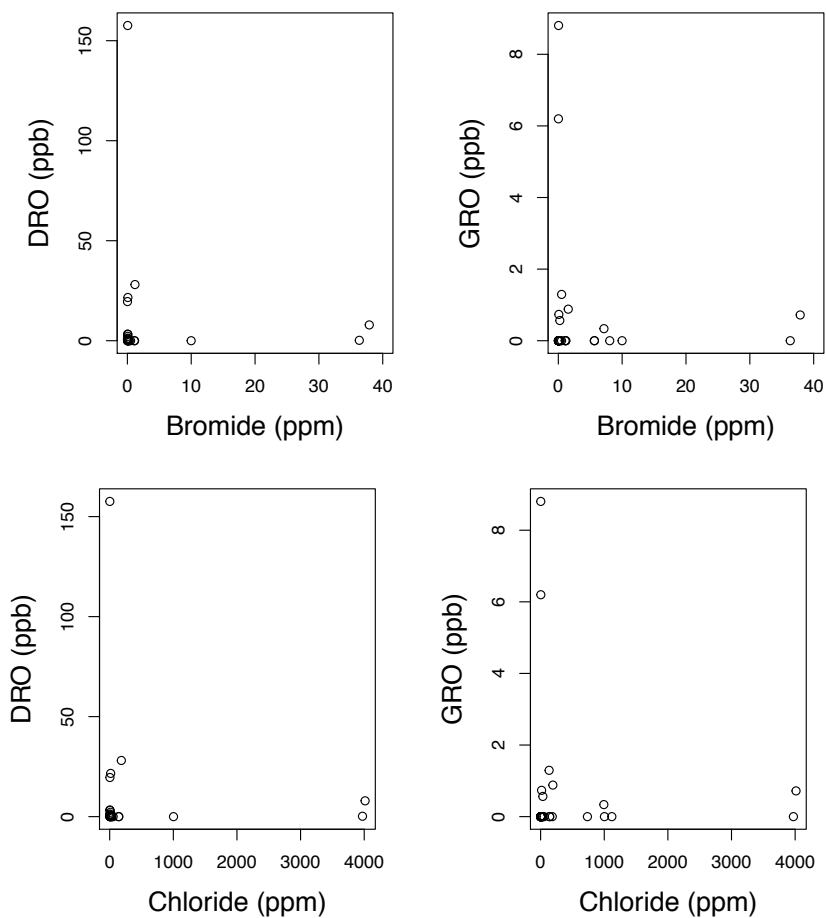
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 194 **Figure S4.** Relationship of DRO (left) and GRO (right) concentrations with respect to
 195 methane measurements taken either during the same sampling campaign or at a previous
 196 time. Statistical analyses showed no correlation (DRO, $p > 0.05$; GRO $p > 0.05$,
 197 Spearman correlation).

198



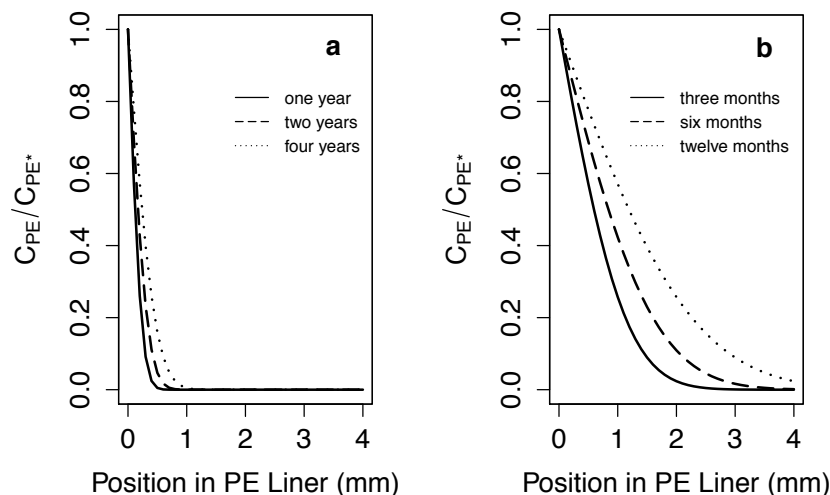
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 200 **Figure S5.** Relationship of DRO (left) and GRO (right) with the number of days since the
 201 nearest shale gas well was drilled. Statistical analyses showed no correlation (DRO, $p >$
 202 0.05 ; GRO, $p > 0.05$, Spearman correlation). Note that only three groundwater wells were
 203 sampled repeatedly over a period of time (shown in color), and most of the data are
 204 individual wells that were sampled once during our three-year period.

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Figure S6. Relationship of DRO (left) and GRO (right) with bromide (top) and chloride (bottom). Statistical analyses showed no correlation (DRO and bromide, $p > 0.05$; GRO and bromide, $p > 0.05$; DRO and chloride, $p > 0.05$; GRO and chloride, $p > 0.05$).

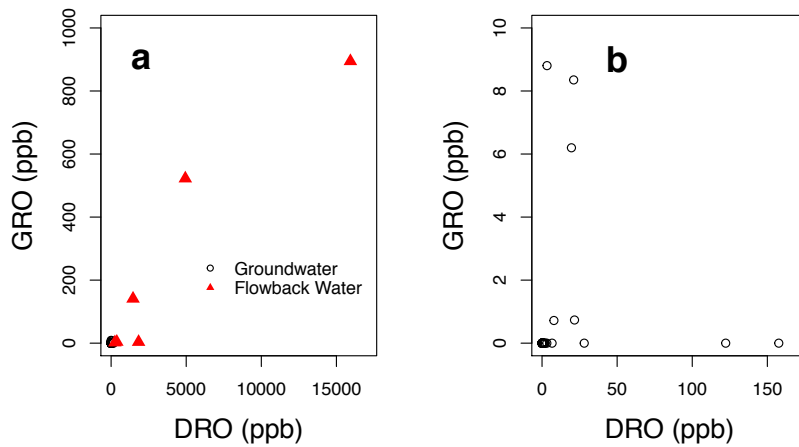


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 214 **Figure S7.** The 1-dimensional Fickian diffusion model for transport of bis(2-
 215 ethylhexyl)phthalate through a 4-mm thick polyethylene liner using a reasonable,
 216 estimated diffusivity of $10^{-11.3} \text{ cm}^2/\text{s}$ (a) and a 100-fold faster diffusion of $10^{-9.3} \text{ cm}^2/\text{s}$ (b).
 217 Note that this model represents the fastest-possible transport times, as we neglected
 218 resistances to mass transport provided by a water-side diffusive boundary layer, diffusion
 219 within the soil porous media, and retardation within the PE caused by pigments (e.g.,
 220 carbon black, commonly used to color the black PE liners used in containment ponds).

221
 222 **GRO and DRO Fingerprinting**

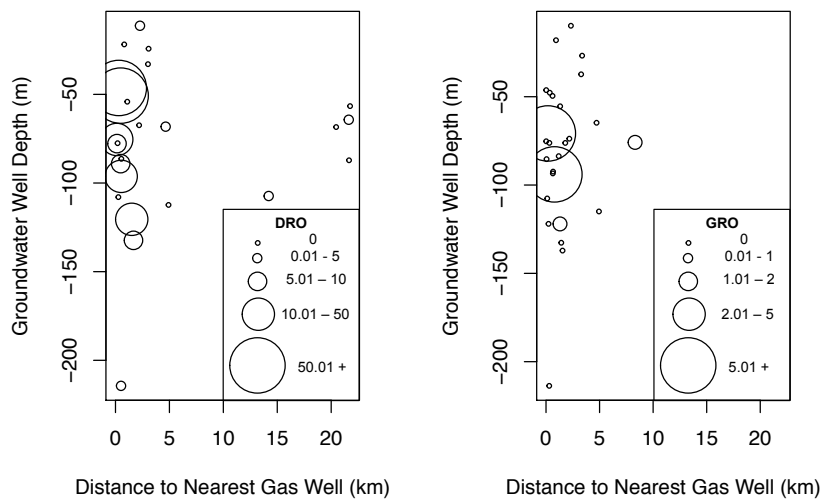
223 GRO/DRO ratios could be used as a tracer of these waters or potentially as an
 224 indicator of deep formation water migration. Noting that only a small number of samples
 225 ($n = 5$) had detectable levels of both GRO *and* DRO, it is clear that there is no
 226 discernable GRO/DRO “fingerprint” (Figure 2, inset, main text) in groundwater in from
 227 this region. Similarly, flowback water showed variable GRO/DRO ratios, with total GRO
 228 and DRO abundance much higher than that observed in groundwater (SI Fig. S8). Thus,
 229 GRO/DRO fingerprinting and enrichments are not viable candidates for tracing flowback
 230 water migration from either faulty well casings or leaking containment pits.

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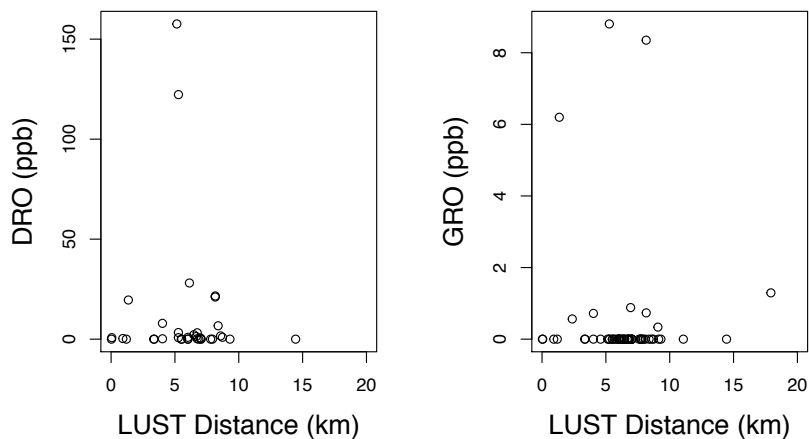
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 234 **Figure S8.** Comparison of GRO and DRO concentrations in shallow groundwater
 235 samples and flowback waters samples. Note that the flowback water samples (colored
 236 triangles) have much higher GRO and DRO (a), whereas groundwater samples (open
 237 circles) have comparatively low levels for GRO and DRO (b). There is no discernible
 238 GRO/DRO fingerprint in either groundwater or flowback water, as both exhibit a high
 239 degree of variability.

240



241
 242 **Figure S9.** Relationship of DRO (left) and GRO (right) concentrations with sampled
 243 groundwater well depth and the distance to the nearest shale gas well. There was no
 244 statistical relationship between concentration and well depth (DRO $p > 0.05$, GRO $p >$
 245 0.05). The samples with the highest concentrations were found in areas with relatively
 246 shallow well depths and close to shale gas wells.

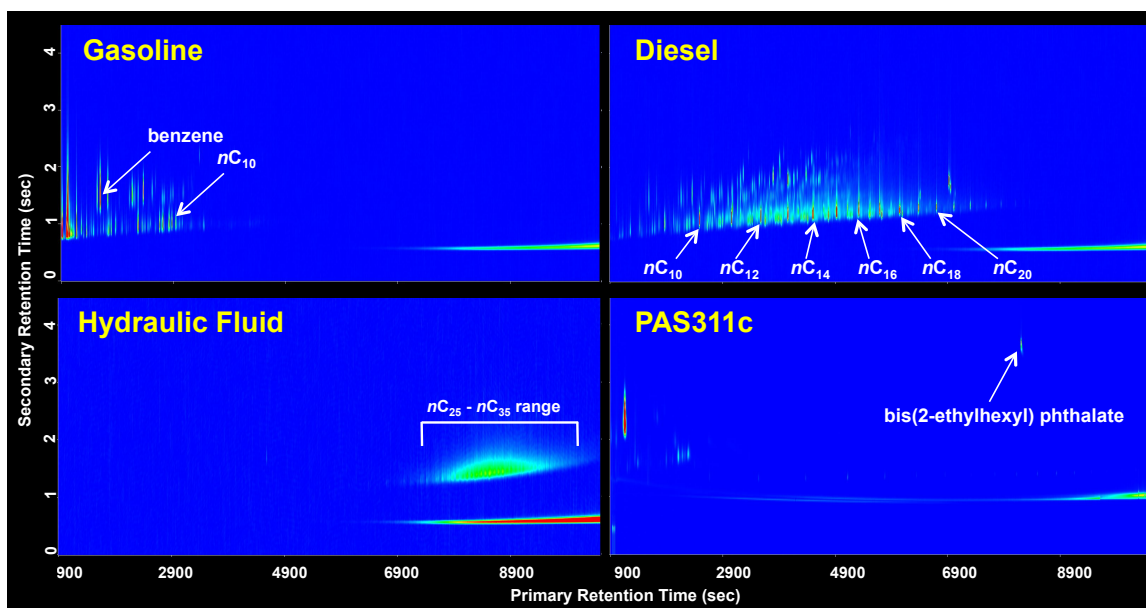
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249 **Figure S10.** Spatial relationship of DRO (left) and GRO (right) concentrations with the
 250 distance to the nearest leaking underground storage tank (LUST) as reported by
 251 Pennsylvania Department of Environmental Protection (PA DEP). Statistical analyses
 252 showed no correlation (DRO, $p > 0.05$; GRO, $p > 0.05$). LUST location data available at
 253 http://www.depreportingservices.state.pa.us/ReportServer/Pages/ReportViewer.aspx?/Cleanup/Tank_Cleanup_Incidents. Accessed on November 2, 2014.

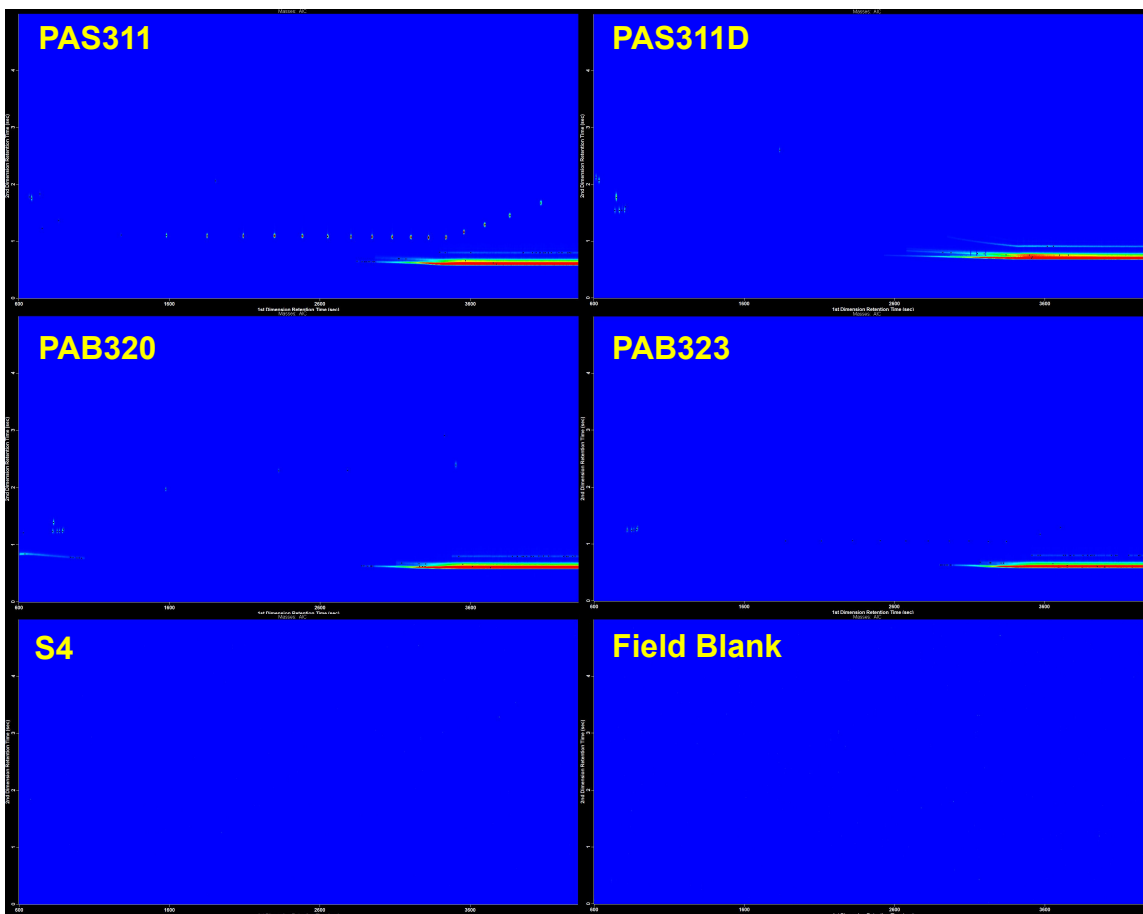
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257 **Figure S11.** GCxGC-TOFMS analysis of gasoline, diesel fuel, and a hydraulic fluid
 258 common in industrial and agricultural applications, along with a groundwater samples
 259 (PAS 311c) that contained elevated levels of DRO. Note that the instrument response in
 260 the DRO region of the groundwater sample is dominated by the phthalate and unlike
 261 those of the fuels.

262



263
 264 **Figure S12.** GCxGC-TOF-MS analysis of five (out of 23 total) low-but-detectable-DRO
 265 containing groundwater samples and a field blank indicated no detectable levels of bis(2-
 266 ethylhexyl) phthalate. These results demonstrate that phthalates, while ubiquitous in
 267 industrial products (e.g., plastics and piping material), do not often appear in groundwater
 268 in this region. The complimentary analysis of two high-DRO containing groundwater
 269 samples appears in the main text and shows the presence bis(2-ethylhexyl) phthalate.

270

271 **References**

272

273 1. Getzinger et al. (2015) Natural Gas Residual Fluids: Sources, Endpoints, and Organic
274 Chemical Composition after Centralized Waste Treatment in Pennsylvania. *Environ*
275 *Sci Technol* 49(14):8347-8355.

276

277 2. US Environmental Protection Agency (2003) *Method 8015D Nonhalogenated*
278 *Organics Using GC/FID*. (US EPA, Washington DC).

279

280 3. Warner NR, et al. (2012) Geochemical evidence for possible natural migration of
281 Marcellus Formation brine to shallow aquifers in Pennsylvania. *Proc Natl Acad Sci*
282 *USA* 109(30):11961-11966.

283

284 4. Jackson RB, et al. (2013) Increased stray gas abundance in a subset of drinking water
285 wells near Marcellus shale gas extraction. *Proc Natl Acad Sci USA* 110(28):11250-
286 11255.

287

288 5. Darrah TH, Vengosh A, Jackson RB, Warner NR, & Poreda RJ (2014) Noble gases
289 identify the mechanisms of fugitive gas contamination in drinking-water wells
290 overlying the Marcellus and Barnett Shales. *Proc Natl Acad Sci USA* 111(39):14076-
291 14081.

292

293 6. Faill RT (1997) A geologic history of the north-central Appalachians. 1. Orogenesis
294 from the mesoproterozoic through the tectonic orogeny. *Am J Sci* 297(6):551-619.

295

296 7. Faill RT (1997) A geologic history of the north-central Appalachians. 2. The
297 Appalachian basin from the Silurian through the Carboniferous. *Am J Sci* 297(7):729-
298 761.

299

300 8. Rogers JD, Burke TL, Osborn SG, & Ryan JN (2015) A Framework for Identifying
301 Organic Compounds of Concern in Hydraulic Fracturing Fluids Based on Their
302 Mobility and Persistence in Groundwater. *Environ Sci Technol Letters* 2(6): 158-164.

303

304 9. Gelhar LW, Welty C, & Rehfeldt KR (1992) A Critical Review of Data on Field-
305 Scale Dispersion in Aquifers. *Water Resour Res* 28(7):1955-1974.

306

307 10. Schwarzenbach RP, Gschwend PM, & Imboden DM. *Environmental Organic*
308 *Chemistry*. 2nd ed. 2003, Hoboken, NJ: John Wiley & Sons, Inc.

309

310 11. Todd DK & Mays LW. *Groundwater Hydrology*. 3rd ed. 2005, Hoboken, NJ: John
311 Wiley & Sons, Inc.

312

313 12. Agency for Toxic Substances and Disease Registry (ATSDR). *Toxicological Profile*
314 *for Di(2-ethylhexyl)phthalate*. Public Health Service, U.S. Department of Health and
315 Human Services, Atlanta, GA. 1993.

316

- 317 13. US Environmental Protection Agency (2015). Estimation Programs Interface Suite
318 for Microsoft® Windows, v 4.11. (US EPA, Washington DC).
319
- 320 14. Crank J. *The Mathematics of Diffusion*. 2nd ed. 1975, Bristol, England: Clarendon
321 Press.
322
- 323 15. Rusina TP, Smedes F, Klanova J, Booij K, & Holoubek I. (2007) Polymer selection
324 for passive sampling: A comparison of critical properties. *Chemosphere* 68(7):1344-
325 1351.
326
- 327 16. Fernandez LA, MacFarlane JK, Tcaciuc AP, & Gschwend PM (2009) Measurement
328 of Freely Dissolved PAH Concentrations in Sediment Beds Using Passive Sampling
329 with Low-Density Polyethylene Strips. *Environ Sci Technol* 43(5):1430-1436.