# Supporting Information

## **Superoxide kinetics**

Superoxide is involved in the following kinetically significant reactions: Its production :

> metabolism production  $\xrightarrow{k_1} O_2^{\bullet -}$ 2

Its tree ways of dismutation (by SOD, by GSH and spontaneously)

$$
O_2^{\bullet-} + H^+ \xrightarrow{k_2} \frac{1}{2} H_2 O_2 + \frac{1}{2} O_2
$$

$$
O_2^{\bullet-} + GSH + H^+ \xrightarrow{k_{GSH}} \frac{1}{2} GSSG + H_2 O_2
$$

$$
2O_2^{\bullet-} + 2H^+ \xrightarrow{k_{sp}} H_2 O_2 + O_2
$$

Those reactions lead to the following ordinary differential equation (ODE) coming from the balance between production and consumption:

$$
\frac{\mathrm{d}\left[O_2^{\bullet-}\right]}{\mathrm{d}t} = k_1
$$
\n
$$
-k_2 \left[SOD\right] \left[O_2^{\bullet-}\right] - k_{GSH} \left[GSH\right] \left[O_2^{\bullet-}\right] - 2k_{sp} \left[O_2^{\bullet-}\right]^2
$$

The kinetic constants used in this work are gathered in the table 1 (concerning superoxide) according to Imlay and Fridovich (1991).

<b>Constants</b>	Value
k <sub>1</sub>	$5.7 \times 10^{-6}$ mol·L <sup>-1</sup> ·s <sup>-1</sup>
$k_2$ [SOD]	$2.8 \times 10^4$ s <sup>-1</sup>
k <sub>2</sub>	$1.5 \times 10^9$ mol <sup>-1</sup> ·L·s <sup>-1</sup>
$k_{GSH}[GSH]$	$1.3 \times 10^{1}$ s <sup>-1</sup>
$k_{GSH}$	$2.6 \times 10^3$ mol <sup>-1</sup> ·L·s <sup>-1</sup>
$k_{sp}$	$5.0 \times 10^5$ mol <sup>-1</sup> ·L·s <sup>-1</sup>

Table 1: Kinetic constants used to describe superoxide evolution.

## **Superoxide evolution**

#### **Without exogenous stress**

#### **In the wild-type strain**

In the wild-type strain, the resolution of  $O_2^{\bullet-}$  $_{2}^{\bullet-}$  concentration gives :

$$
\left[O_2^{\bullet-}\right] \approx \left[O_2^{\bullet-}\right]_{\infty} \left(1 - e^{-k_2\left[SOD\right]t}\right)
$$

indeed  $GSH$  and spontaneous dismutation are negligible because  $k_{sp} \ll k_{GSH}$  [ $GSH] \ll$  $k_2$  [SOD] the.  $O_2^{\bullet-}$  $_{2}^{\bullet-}$  concentration rapidly reached its steady-state value, in less than 1 ms, actually the characteristic time is given by  $\frac{1}{k_2[SOD]}$  . This time, which was dependent solely on *SOD* concentration and the *SOD* catalytic degradation rate  $k_2$ , corresponds to the characteristic time require for the re-establishment of equilibrium.

If we assume that *SOD* concentration and  $O_2^{\bullet-}$  production change over time, and that their equilibrium time values are probably significantly shorter than 1 ms, then the steady-state value of  $O_2^{\bullet -}$ •<sup> $\bullet$ </sup> concentration is always reached but depends purely on  $O_2^{\bullet -}$ 2 production rate and *SOD* catalytic degradation rate  $(k_2)$ , which are time-dependent.

For each time, we can write that the  $O_2^{\bullet-}$ •<sup>-</sup> concentration is  $[O_2^{\bullet-}]$  $\left[\begin{smallmatrix}\bullet^- \ 2\end{smallmatrix}\right](t) = \frac{k_1(t)}{k_2[SOD](t)}.$  For example, with published values (Imlay and Fridovich, 1991),  $\tilde{O_2^{\bullet-}}$  $2^{\circ}$  concentration is 2.1  $\times$  $10^{-10}$  M : this value fits the Imlay prediction well, and it corresponds to the equilibrium between  $O_2^{\bullet-}$  production (parameter  $k_1$ ) and the rate of scavenging of this radical by *SOD*.

We confirmed this approximation, by comparing the analytical solution  $(\triangle)$  with the numerical solution  $(\blacksquare)$  in figure 1. Indeed this comparison help us to check whether the suggested approximations used to find an analytical expression are valid.

In a wild strain, the two major reaction involving superoxide are its production and its consumption by SOD.

#### **In a SOD(-) mutant**

In a *SOD* (-) mutant, changes in  $O_2^{\bullet-}$  $_{2}^{\bullet-}$  concentration were explained principally by the following differential equation :

$$
\frac{\mathrm{d}\left[O_{2}^{\bullet-}\right]}{\mathrm{d}t}=k_{1}-k_{GSH}\left[GSH\right]\left[O_{2}^{\bullet-}\right]
$$

The resolution of  $O_2^{\bullet-}$ •<sup>-</sup> concentration gave:  $[O_2^{\bullet-}]$  $\left[0\right] \approx \left[0\right]$ <sup>o</sup>  $\left[2\right]_{\infty}\left(1-e^{-k_{GSH}[GSH]t}\right)$ , which rapidly reached its steady-state value, in less than 0.5 s. Actually the characteristic time is  $\frac{1}{k_{GSH}[GSH]}$ . This time, which was dependent only on *GSH* concentration and the *GSH* catalytic degradation rate  $k_{GSH}$ , corresponds to the characteristic time required for the re-establishment of equilibrium.

If we assume that *GSH* concentration and  $O_2^{\bullet-}$  production can change over time, and that their equilibrium time values are probably significantly shorter than 0.5 s, then the steady state value of  $O_2^{\bullet-}$  $_{2}^{\bullet-}$  concentration is always reached but is dependent purely on  $O_2^{\bullet-}$  production rate and the *GSH* catalytic degradation rate  $k_{GSH}$ , which are time-dependent.



Figure 1: Change in  $O_2^{\bullet-}$  concentration in the *E. coli* wild-type strain. (A) corresponds to the analytical solution according to the simplified system and  $(\blacksquare)$  corresponds to whole model solved with numerical methods. Cell density has no influence on the pattern of superoxide concentration evolution. —————————————————Fig1

For each time point, we can write that  $O_2^{\bullet-}$ •<sup>-</sup> concentration is  $[O_2^{\bullet-}]$  $\begin{bmatrix} \bullet^{-} \\ 2 \end{bmatrix} (t) = \frac{k_1(t)}{k_{GSH}[GSH](t)}.$ For example, with published values (Imlay and Fridovich, 1991),  $O_2^{\bullet-}$  $_{2}^{\bullet-}$  concentration is  $4.4 \times 10^{-7}$  M. This value is consistent with the predictions of Imlay and corresponds to the equilibrium between  $O_2^{\bullet-}$  production (parameter  $k_1$ ) and the rate of scavenging of this radical by *GSH*.

For confirmation of this approximation, we compared (figure 2) the analytical solution  $(\triangle)$  with the numerical one  $(\blacksquare)$ :

#### **In a** *SOD***(-)** *GSH***(-) mutant**

In a *SOD*(-) *GSH*(-) mutant, the change in  $O_2^{\bullet-}$  $_{2}^{\bullet-}$  concentration can be explained principally by the following differential equation according to the spontaneous dismutation:

$$
\frac{\mathrm{d}\left[O_2^{\bullet-}\right]}{\mathrm{d}t} = k_1 - 2k_{sp}\left[O_2^{\bullet-}\right]^2
$$

 $O_2^{\bullet-}$  $\frac{1}{2}$  concentration obeys the function :

$$
\left[O_2^{\bullet-}\right]=\left[O_2^{\bullet-}\right]_\infty\frac{1-\mathrm{e}^{-\mathrm{t}/2\tau}}{1+\mathrm{e}^{-\mathrm{t}/2\tau}}
$$

where  $\tau = \frac{1}{\sqrt{2k}}$  $\frac{1}{2k_1k_{sp}}$  and  $\left[O_2^{\bullet -}\right]$  $\left[\begin{smallmatrix}\bullet^- \ 2\end{smallmatrix}\right]_\infty = \sqrt{\frac{k_1}{2k_{sp}}}$ 

 $O_2^{\bullet-}$ • concentration rapidly reaches its steady-state  $[O_2^{\bullet-}]$  $\left[2\atop 2\right]_\infty$  value, in less than 1 s ( $\tau$  is the characteristic time). This time, which is dependent solely on the dismutation rate  $k_{sp}$ , corresponds to the characteristic time required to re-establish equilibrium.



Figure 2: Changes in  $O_2^{\bullet-}$  concentration in a  $SOD(-)$  mutant. (A) corresponds to the analytical solution according to the simplified system and  $(\blacksquare)$  corresponds to the whole model solved with numerical methods. Cell concentration has no influence on this pattern of superoxide concentration evolution.

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If we assume that  $O_2^{\bullet -}$  production can change over time, and that the equilibrium time is probably significantly shorter than 1 s, then the steady-state value of  $O_2^{\bullet-}$  $2^{\bullet -}$  concentration is always reached but is dependent purely on  $O_2^{\bullet-}$  production rate, which is time-dependent.

For each time point, we can write that  $O_2^{\bullet-}$ •<sup>-</sup> concentration is  $[O_2^{\bullet-}]$  $\left[\begin{smallmatrix}\bullet^- \ 2\end{smallmatrix}\right](t) \;\approx\; \sqrt{\frac{k_1(t)}{2k_{sp}}}$  $\frac{\kappa_1(\iota)}{2k_{sp}}.$ With published values, the  $O_2^{\bullet-}$ • concentration is  $2.4 \times 10^{-6}$ M, a value consistent with the predictions of Imlay (2001), and corresponding to the equilibrium between  $O_2^{\bullet-}$ 2 production (parameter  $k_1$ ) and its spontaneous dismutation.

The analytical solution  $(\triangle)$  and the numerical solution  $(\blacksquare)$  are the identical because they solved the same system (figure 3).



Figure 3: Change in  $O_2^{\bullet-}$  concentration in  $SOD(-)$   $GSH(-)$  mutants. (A) corresponds to the analytical solution according to the simplified system and  $(\blacksquare)$  corresponds to the whole model with numerical methods. Cell concentration has no influence on this pattern of superoxide concentration evolution.

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### **Superoxide summary**

The table 2 summarizes the superoxide steady-state concentrations.

		$[O_2^{\bullet-}]$ (mol L <sup>-1</sup> ) In this work Imlay, Fridovich
Wild type	$2.1 \times 10^{-10}$	$2.0 \times 10^{-10}$
$SOD(-) GSH(+)$	$4.2 \times 10^{-7}$	$4.9 \times 10^{-7}$
$SOD(-)$ $GSH(-)$	$2.4 \times 10^{-6}$	$6.7 \times 10^{-6}$

Table 2: Superoxide steady-state concentration. At steady state, the internal concentration is shown for cells in LB at 37 ◦C without exogenous hydrogen peroxide. In a wild-type strain, *Fe* concentration is 10 µM, and, in a SOD<sup>−</sup> strain, *Fe* concentration is 80 µM (Keyer and Imlay, 1996).

## **References**

Imlay JA, Fridovich I, Assay of metabolic superoxide production in Escherichia coli. J. Biol. Chem. 1991;266.11: 69576965.

Keyer K, Imlay JA, Superoxide accelerates DNA damage by elevating free-iron levels. Proc. Natl. Acad. Sci. U.S.A. 1996;93.24: 13635 13640.