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## **Supplemental Information**

# Measuring Cell Viscoelastic Properties Using a Microfluidic Exten-

### sional Flow Device

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#### Measuring cell viscoelastic properties using a microfluidic extensional flow device

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#### SUPPORTING MATERIAL

#### SUPPORTING RESULTS

#### Derivation of the normalized entrance velocity $\xi$ that best matches experimental measurements

Experimental values for  $\xi$  will lie between  $\xi_{min}$  and  $\xi_{max}$ , provided that we restrict our analysis to objects that are near the center of the channel. In such instances, the objects will be spread in the vertical axis between the heights r and h-r, where r is the radius of the spherical object. Indeed, it is not possible for a spherical object's center to get closer to the channel walls than r. We show an example in Figure 1B (dotted black line) where r = h/16, corresponding to an experimental case in which the channel height is 200 µm and the object's radius is at least 25 µm. To obtain those  $\xi$  values, we take the mean velocity along the heights considered using the velocity profile provided in Ref. (26). We find using these formulas that for our devices and objects (both dextran beads and cells), the analytical values for  $\xi$  are close to 1.5 (between 1.48 and 1.62). We also experimentally measure object velocities in the cross-slot, and find that they are about 1.5 times the mean velocity in the channel. Therefore, for simplicity, we use the value  $\xi = 1.5$  in our experimental analysis.

#### Cells do not perturb the flow sufficiently to modify the strain rate in the device

For the calculations of strain rate in the cross-slot, it is assumed that the flow field is unaffected by suspended cells. To determine if the presence of cells in the fluid flow affects the fluid velocity and gradients, we inspect the Stokes number of the suspended cells, which is the ratio of particle momentum relaxation time (i.e. exponential decay of particle velocity due to drag) to the characteristic time scale of the continuum fluid phase. For neutrally buoyant particles with a small particle Reynolds number (Re<sub>p</sub> = Re(d<sub>p</sub><sup>2</sup>/D<sup>2</sup>) =  $\rho U d_p^{2/}(\mu D) < 0.013$ ), the momentum relaxation time scale is independent of density and can be expressed as  $\tau_{mom} = d_p^{2/}(18v_c)$  where  $v_c = \mu_c/\rho_c$  is the kinematic viscosity of the continuum fluid phase and  $d_p$  the diameter of the dispersed particles. Cells with a typical diameter of 10  $\mu$ m and suspended in 20% w/v PEG20000/PBS ( $\rho_c \sim 1040 \text{ kg/m}^3$ ,  $\mu_c \sim 0.04 \text{ Pa} \cdot \text{s}$ ) thus have a momentum relaxation time of  $\tau_{mom} = 1.4 \cdot 10^{-7}$  seconds. The characteristic flow time scale is taken to be the inverse of the velocity gradient in the cross-slot region,  $\Omega$ . The smallest strain rate in our cell cross-slot experiments is  $\Omega = 34 \text{ s}^{-1}$ , leading to a maximum characteristic flow field time scale of  $\tau_{flow} = 5 \cdot 10^{-6} << 1$ . Thus, the suspended cells follow the flow field streamlines instantaneously, and the strain rate in a cross-slot device  $\Omega$  is undisturbed by the presence of the cells.

#### Uncertainty in cell strain measurements: User bias and small strains

We verified that the manual strain measurement was accurate within 2% strain by having different individuals analyze the same set of cells and set of cross-slot experiments (Supporting Figure S3). Observed cell strains were small at the lower strain rates, so that the difference in length of the major and minor axes was close to 1 pixel. We mitigated the limitation of resolving small deformations by measuring several cells per data point ( $10 \le n \le 30$ ), which resulted in a clear trend of increasing strain with increasing strain rate for both cell types and all pharmacological conditions.

#### Viscous forces acting on cell surface in planar extensional flow

The suspending fluid that is considered to be a Newtonian fluid has a Cauchy stress tensor of the form  $\mathbf{T} = -\text{grad}(\mathbf{p}) + \mu(\text{grad}(\mathbf{v}) + \text{grad}(\mathbf{v})^T)$  where p is the fluid pressure,  $\mu$  the dynamic viscosity, and **v** the fluid velocity. Assume that the perturbations to the fluid velocity field due the presence of the cell are small, which is reasonable for our system as argued above. Due to the uniform velocity gradient in planar extensional flow  $\text{grad}(\mathbf{v}) = [-\Omega \ 0 \ 0; \ 0 \ \Omega \ 0; \ 0 \ 0 \ 0]$  where  $\Omega$  is the extensional strain rate, the viscous contribution to the fluid stress tensor is independent of location in the extensional flow field. Therefore, the force from the fluid (traction vector  $\mathbf{t} = \mathbf{Tn}$ ) acting on the cell surface only depends on the local outward unit normal vector  $\mathbf{n}$  of the cell surface. The viscous force vectors on the equator of a sphere and ellipsoid located anywhere in planar extensional flow, not just the stagnation point, are shown in Supporting Figure S7. The magnitude of each fluid force vector is proportional to  $\mu\Omega$  and the z-component of the normal vector.



**Supporting Figure S1.** Macroscale rheologic measurements of PEG20000/PBS solutions used in cell cross-slot deformation experiments. Black line indicates 40% w/v PEG20000 in PBS, dark grey line indicates 30% w/v and light grey line 20% w/v. After initial transients at the experiment start-up, the viscosity is constant for strain rates of  $1-2000 \text{ s}^{-1}$  indicating the fluid is Newtonian. The reported viscosities for each batch are the average of 2 independent rheometry measurements.



**Supporting Figure S2.** Ratio of local strain rate  $\dot{\epsilon} = du/dx$  to maximum strain rate at the crossslot stagnation point as a function of the distance along the central inlet streamline as predicted in Hele-Shaw simulations. This streamline corresponds to the x-axis (cf. Figure 1A). The strain rate is approximately constant within a distance D (the channel half width) of the stagnation point, an

indication that the flow field is indeed hyperbolic extensional flow. Thus, objects in the stagnation point region experience a constant strain rate.



**Supporting Figure S3.** Impact of user bias on cell strain measurements is negligible. Left: Independent strain measurements performed by two users of a set of individual cells from a single cross-slot experiment (TIC control case, flow rate 300  $\mu$ L/hr). Right: Independent cell strain measurements for several flow rates for control TICs by two users. Each marker is the average strain of  $n \ge 10$  cells and the error bars indicate  $\pm$  standard error of the mean. Users independently selected qualifying cells to analyze and manually fitted ellipses in order to measure cell strain. User 2 systematically measures larger cell strain but agrees closely with User 1. For the results reported in the manuscript, User 1 performed most of the measurements.



**Supporting Figure S4.** Histogram of cell radii. All analyzed cells are included. (A) Both TIC and 3T3 cells, in both control and drug conditions, are included (n = 3,357 cells). (B) Only TICs in control case are included (n = 1,288 cells). (C) Only 3T3 cells in control case are included (n = 321 cells).



Supporting Figure S5. Cell deformation increases as they enter the cross-slot's central region  $|\mathbf{x}| \leq D$  (blue dots), up until the point where they leave the central region and the deformation starts decreasing (red dots). Frame 0 marks the entry of the central region of the cross-slot. Cell deformation was tracked from the moment they entered the central region. Frame rate is approximately 40 fps. The cells in this example are 3T3 cells in control case at a flow rate of 250  $\mu$ l/hr, with n = 8 cells tracked in this example.



**Supporting Figure S6.** Cell cross-slot measurements including error bars reflecting the uncertainty in strain measurements (standard error of the mean). Error propagation (49) was used to plot these uncertainties for the quantity  $\log(\epsilon/\mu)$ :  $\sigma_{\log(\epsilon/\mu)} = [d(\log(\epsilon/\mu))/d\epsilon]^2 \cdot (\sigma_{\epsilon})^2 = \sigma_{\epsilon}/\epsilon$ .



**Supporting Figure S7.** Viscous fluid forces acting on the surface of a sphere (left) and ellipsoid (right) in planar extensional flow that is unperturbed by the presence of the object. The force vectors in the x-y plane at the equator have a uniform magnitude equal to  $2\mu\Omega$  ( $\mu$  fluid viscosity,  $\Omega$  extensional strain rate) and different directions.

**Supporting Table S1.** Range for various experimental parameters over all experimental conditions tested for the glioblastoma tumor initiating cells (TIC) and 3T3 fibroblast cells. U =  $Q/(h \cdot w)$  is the average flow velocity in the channels based on the specified flow rate Q and channel cross-sectional dimensions (width  $w = 2 \cdot D$ , height  $h = 30 \mu m$ ). The suspending fluid viscosity  $\mu$  was measured before each set of experiments (sample measurements Supporting Figure S1). The flow Reynolds number Re is based on microchannel dimensions, fluid properties, and flow rate. n is the number of cells used to determine the average strain  $\varepsilon$  that makes up each data point in Figure 4(B,C).

Cell Type	μ	W	U	$Re = \rho UD/\mu$	ξU/D	n	$\varepsilon = (a-b)/(a+b)$
- <b>J F</b> -	[mPa·s]	[µm]	[mm/s]		$s^{-1}$		<i>a</i> )/( <i>a b</i> )
TIC	$36 \le \mu \le$	w = 70,	$7 \le U \le$	$0.0057 \le \text{Re}$	$283 \le \xi U/D$	$10 \le n$	$0.029 \le \epsilon \le$
	42	100	159	$\leq 0.19$	$\leq 6800$	$\leq 27$	0.18
3T3	$37.5 \le \mu$	w = 100	$9 \le U \le$	$0.013 \leq \text{Re} \leq$	$278 \leq \xi U/D$	$10 \le n$	$\geq$ 3 $\geq$ 900.0
	$\leq$ 38.3		148	0.20	$\leq$ 4440	$\leq$ 30	0.12

**Supporting Table S2**. Statistical significance (p-values) of multiple regression analysis of covariance.

Comparison Groups	3T3 p-value	TIC p-value
Control vs. CytoD	0.012	0.0002
Control vs. PFA	0.0094	0.0015
CytoD vs. PFA	0.0004	$8.5 \cdot 10^{-6}$

**Supporting Table S3.** Raw data for glioblastoma tumor initiating cells (TIC) mechanical measurements. The uncertainty ( $\sigma_{\epsilon}$ ) in the average strain measurement ( $\epsilon$ ) at each experimental condition is the standard error of the mean.

TIC	Fluid viscosity μ	Channel wideth w = 2·D	Mean flow velocity U	Flow Reynolds number Re = ρUD/μ	Extensional strain rate ξU/D	Number of cells n	Average strain ε = (a- b)/(a+b)	Strain uncertainty σ <sub>ε</sub>
	mPa∙s	μm	mm/s		S <sup>-1</sup>			std error of mean
TIC CO	NTROL							
			6.61	0.0057	283	14	0.029	0.007
			13.23	0.0115	567	15	0.047	0.006
Day 1	42	70	39.68	0.0344	1701	12	0.06	0.01
			79.37	0.0688	3401	16	0.10	0.02
			132.28	0.1146	5669	15	0.16	0.02
			23.15	0.0334	694	11	0.036	0.004
			46.30	0.0669	1389	15	0.07	0.01
Dav 2	36	100	69.44	0.1003	2083	15	0.086	0.006
			92.59	0.1337	2778	15	0.082	0.009
			111.11	0.1605	3333	14	0.09	0.01
			129.63	0.1872	3889	11	0.087	0.006
		70	6.61	0.0064	283	12	0.037	0.005
	37.6		13.23	0.0128	567	18	0.035	0.004
Day 3			33.07	0.0320	1417	20	0.062	0.006
,			66.14	0.0640	2834	20	0.11	0.01
			99.21	0.0960	4252	27	0.102	0.007
_			132.28	0.1281	5669	22	0.136	0.008
TIC CY	TOCHALASIN	D	22.45	0.0004			0.005	0.000
	36	100	23.15	0.0334	694	18	0.065	0.006
Day 2			46.30	0.0669	1389	20	0.09	0.01
Day 2			69.44	0.1003	2083	15	0.16	0.01
	37.6	70	0.01	0.0064	283	14	0.063	0.005
			13.23	0.0128	507 1417	10	0.069	0.005
Day 3			55.07	0.0320	1417	20	0.077	0.005
			00.14	0.0040	2034	20	0.130	0.008
			122.22	0.0900	4232	20	0.10	0.01
	<u> </u>		132.20	0.1281	5009	20	0.18	0.02
TIC PF/	42	70	12.22	0.0115	567	20	0.020	0.007
			20.69	0.0113	1701	10	0.025	0.007
Day 1			39.08	0.0344	2401	19	0.00	0.01
			132.28	0.0000	5669	10	0.072	0.005
			66 14	0.0640	2834	20	0.10	0.01
	37.6	70	99.21	0.0040	2004 4252	20	0.07	0.01
Day 3			132.28	0.1281	5669	20	0.08	0.01
			158.73	0.1537	6803	20	0.10	0.01

**Supporting Table S4.** Raw data for 3T3 fibroblast cell mechanical measurements. The uncertainty ( $\sigma_{\epsilon}$ ) in the average strain measurement ( $\epsilon$ ) at each experimental condition is the standard error of the mean.

3T3	Fluid viscosity μ	Channel wideth w = 2∙D	Mean flow velocity U	Flow Reynolds number Re = ρUD/μ	Extensional strain rate ξU/D	Number of cells n	Average strain ε = (a- b)/(a+b)	Strain uncertainty $\sigma_{\epsilon}$
	mPa∙s	μm	mm/s		s⁻¹			std error of mean
3T3 CC	ONTROL							
			23.15	0.0319	694	16	0.047	0.006
			46.30	0.0638	1389	11	0.047	0.006
Day 1	37 75	100	69.44	0.0957	2083	22	0.058	0.003
Dayı	57.75	100	111.11	0.1531	3333	15	0.071	0.008
			129.63	0.1786	3889	25	0.10	0.01
			148.15	0.2041	4444	27	0.099	0.007
			23.15	0.0314	694	10	0.043	0.005
			46.30	0.0629	1389	10	0.065	0.006
Dav 2	38.3	100	69.44	0.0943	2083	11	0.056	0.009
			92.59	0.1257	2778	10	0.072	0.008
			111.11	0.1509	3333	10	0.069	0.009
			129.63	0.1760	3889	19	0.09	0.01
			23.15	0.0321	694	10	0.035	0.007
Day 3	37.5	100	46.30	0.0642	1389	10	0.051	0.004
			69.44	0.0963	2083	14	0.06	0.01
			92.59	0.1284	2778	13	0.07	0.01
			9.26	0.0128	278	10	0.020	0.007
Day 4	37.5	100	23.15	0.0321	1280	18	0.031	0.006
			46.30	0.0642	1389	10	0.035	0.006
272.0			129.05	0.1798	2009	12	0.07	0.01
313 C1		1	0.26	0.0129	270	21	0.022	0.005
			9.20	0.0128	270	21	0.033	0.003
			25.15	0.0519	1290	20	0.074	0.007
			40.30	0.0058	2083	12	0.003	0.003
Day 1	37.75	100	92 59	0.0937	2083	10	0.083	0.008
			111 11	0.1273	3333	27	0.005	0.007
			129.63	0.1331	3889	10	0.000	0.007
			148.15	0.2041	4444	20	0.12	0.01
			9.26	0.0126	278	17	0.023	0.006
	38.3	3 100	23.15	0.0314	694	16	0.06	0.01
			46.30	0.0629	1389	12	0.07	0.01
Day 2			69.44	0.0943	2083	20	0.093	0.009
			92.59	0.1257	2778	21	0.079	0.007
			111.11	0.1509	3333	26	0.09	0.01
3T3 PF	A	•	•					
	37.5	100	9.26	0.0128	278	15	0.016	0.005
Day 2			46.30	0.0642	1389	15	0.028	0.005
Day 3			69.44	0.0963	2083	15	0.031	0.009
			111.11	0.1541	3333	15	0.055	0.006
	37.5	100	9.26	0.0128	278	11	0.009	0.005
			23.15	0.0321	694	15	0.027	0.007
			46.30	0.0642	1389	15	0.034	0.007
Day 4			69.44	0.0963	2083	15	0.029	0.007
			92.59	0.1284	2778	14	0.038	0.008
			111.11	0.1541	3333	15	0.05	0.01
			129.63	0.1798	3889	15	0.05	0.01