

Cover Page for Supplementary

Manuscript title:

Improvement of Sludge Dewaterability by Ultrasound-Initiated Cationic Polyacrylamide with Microblock Structure: Role of Surface-Active Monomers

Author list:

Chuanliang Zhao ^{1,2}, Huaili Zheng ^{1,2,*}, Li Feng ^{1,2}, Yili Wang ³, Yongzhi Liu ^{1,2}, Bingzhi Liu ^{1,2} and Badradine Zakaria Djibrine ^{1,2}

¹ Key laboratory of the Three Gorges Reservoir Region's Eco-Environment, State Ministry of Education, Chongqing University, Chongqing 400045, P.R. China

² National Centre for International Research of Low-carbon and Green Buildings, Chongqing University, Chongqing 400045, P.R. China

³ College of Environmental Science and Engineering, Research Center for Water Pollution Source Control and Eco-remediation, Beijing Forestry University, Beijing 100083, P.R. China

* Correspondence: zhl@cqu.edu.cn; Tel.: +86 23 65120827

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Figure S1. Determination of AM and DMC reactivity ratios by the Fineman–Ross method

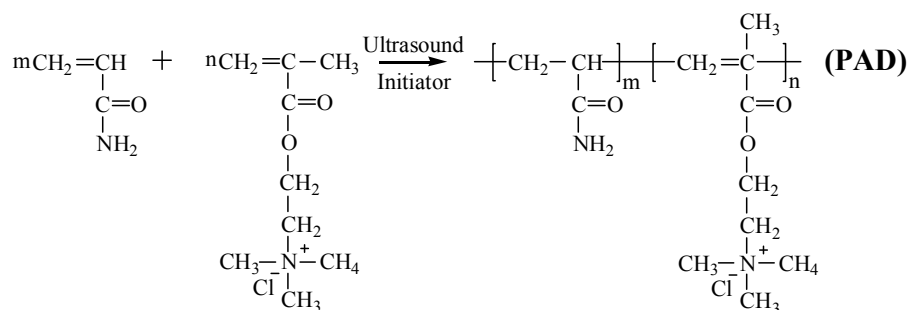
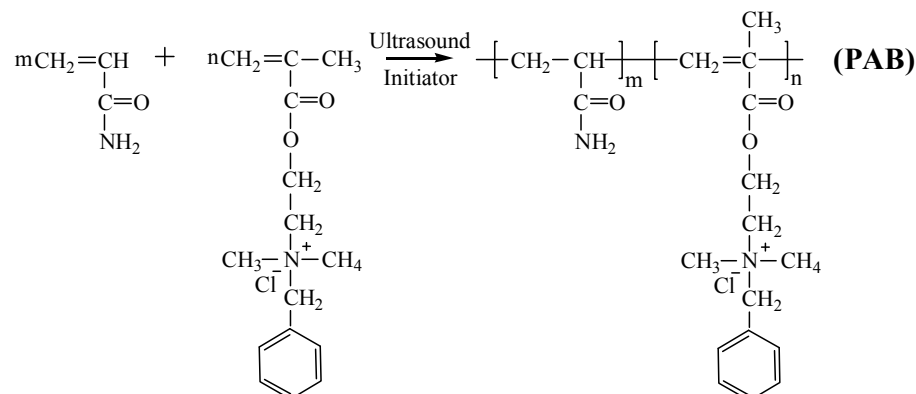
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Scheme:

Scheme S1. Proposed reaction scheme of the synthesis of PAB and PAD.



Text:

Text S1. Fineman–Ross method.

$$\begin{aligned}
 G &= r_{AM}H - r_{CM} \\
 G &= \frac{R(\rho - 1)}{\rho}; H \\
 &= \frac{R^2}{\rho} \quad \text{(S1)}
 \end{aligned}$$

In the above formulae, r_{AM} is the reactivity ratio of AM monomer in AM and cationic monomer pair, r_{CM} is analogous to r_{AM} , R is the molar ratio of AM and cationic monomers in the raw material before the polymerization reaction, and ρ is the molar ratio of AM and cationic monomers in the polymers at low conversion. After the G and H of each point were obtained, the linear fitting curve relating to G and H could be plotted, and the r_{AM} and r_{CM} can be obtained through the slope and intercept of straight line.

Text S2. Kelen–Tüdö method.

$$\begin{aligned}
 \eta &= (r_{AM} + \frac{r_{CM}}{\delta})\xi - \frac{r_{CM}}{\delta} \\
 \eta &= \frac{G}{\delta + H}; \xi = \frac{H}{\delta + H}; \delta \\
 &= \sqrt{H_{\min} \times H_{\max}} \quad \text{(S2)}
 \end{aligned}$$

η and ξ could be obtained based on the results of Fineman–Ross method and formula S2. Then, the linear fitting curve relating to η and ξ could be plotted, and the r_{AM} and r_{CM} were calculated through the slope and intercept of straight line.

Text S3. Y–B–R method.

$$r_{AM} = \frac{A_2 C_1 + n C_2}{A_1 A_2 - n^2}, \quad r_{CM} = \frac{A_1 C_2 + n C_1}{A_1 A_2 - n^2}$$

$$A_1 = \sum_{i=1}^n \frac{X_i^2}{Y_i}; \quad A_2 = \sum_{i=1}^n \frac{Y_i}{X_i^2}; \quad C_1 = \sum_{i=1}^n X_i \left(1 - \frac{1}{Y_i}\right); \quad C_2 = \sum_{i=1}^n \frac{Y_i}{X_i} \left(\frac{1}{Y_i} - 1\right) \quad (S3)$$

In the above formulae, n is the number of test groups; X is the molar ratio of AM to cationic monomers before polymerization; and Y is the molar ratio of AM units to cationic units in copolymers at low conversion.

Text S4. The composition equations of PAB and PAD.

$$F_{BDMDAC-PAB} = 1 - \frac{-0.44f_{BDMDAC}^2 - 0.12f_{BDMDAC} + 0.56}{0.08f_{BDMDAC}^2 + 0.88f_{BDMDAC} + 0.56} \quad (S4)$$

$$F_{DMC-PAD} = 1 - \frac{-0.36f_{DMC}^2 - 0.28f_{DMC} + 0.64}{-0.96f_{DMC}^2 + 0.72f_{DMC} + 0.64} \quad (S5)$$

In the above formulae, F is the molar ratio of the units of one monomer to the total copolymer units, and f is the molar ratio of one monomer to all material monomers before polymerization.

Text S5. The calculating formulae of sequence distribution of PAB and PAD.

$$(p_1)_x = p_{11}^{x-1}(1 - p_{11}), \quad (p_2)_x = p_{22}^{x-1}(1 - p_{22})$$

$$p_{11} = \frac{r_{AM}(1 - CD)}{CD}, \quad p_{22} = \frac{r_{CM}CD}{1 - CD} \quad (S6)$$

In the above formulae, x is the number of monomer units in the segment. $(p_1)_x$ is the probability of generating the x AM segment which possesses x successive AM monomer units, it equals to the percentage of x AM segments in all AM segments in the copolymer. $(p_2)_x$ is analogous to $(p_1)_x$; and p_{11} is the probability of generating the 2AM segment which possesses two successive AM monomer units. p_{22} is analogous to p_{11} .

Text S6. Analytical methods for FCMC.

The filter cake was placed into a crucible and dried for 24 h at 105 °C in a thermostatic drying oven. FCMC can be calculated by formulae S7:

$$FCMC = \frac{M_1 - M_2}{M_1 - M_0} \quad (S7)$$

where M_1 is the total weight of the filter cake without drying and crucible, M_2 is the total weight of the filter cake after drying and crucible, and M_0 is the weight of the crucible.

Text S7. Analytical methods for SRF.

The SRF of sludge can be calculated using formulae S8.

$$\text{SRF} = \frac{2bPA^2}{\mu C} \quad (\text{S8})$$

where P is the filtering pressure (N/m²), A is the filtering area (m²), μ is the kinetic viscosity (N s/m²), b is the slope of the filtration curve (S9), and C is the filter cake weight per unit volume filter (kg/m³), which can be obtained by formulae 10.

$$\frac{t}{v} = bv + a \quad (\text{S9})$$

where t is the filtering time (s), and v is the filtrate volume (m³).

$$C = \frac{1}{\frac{C_i}{100 - C_i} - \frac{C_f}{100 - C_f}} \quad (\text{S10})$$

where C_i is the moisture content of the initial sludge, and C_f is the moisture content of the filter cake.

Table:

Table S1. Fineman–Ross and Kelen–Tudos parameters for AM/BDMDAC copolymerization system initiated by ultrasound.

No.	R	ρ	G	H	ζ	η	δ
1	9	5.22	7.28	15.52	0.85	0.40	2.67
2	4	2.07	2.07	7.73	0.75	0.20	
3	2.33	1.59	0.86	3.41	0.56	0.14	
4	1.5	1.01	0.01	2.23	0.46	0.003	
5	1	0.65	-0.54	1.54	0.37	-0.13	
6	0.67	0.4	-1.01	1.12	0.30	-0.27	
7	0.43	0.3	-1.00	0.62	0.19	-0.31	
8	0.25	0.14	-1.54	0.45	0.15	-0.50	

Table S2. Fineman–Ross and Kelen–Tudos parameters for AM/DMC copolymerization system initiated by ultrasound.

No.	R	ρ	G	H	ζ	η	δ
1	9	6.57	7.63	12.33	0.90	0.56	1.31
2	4	3.04	2.68	5.26	0.80	0.41	
3	2.33	2.35	1.34	2.31	0.64	0.37	
4	1.5	1.38	0.41	1.63	0.55	0.14	
5	1	1.25	0.20	0.80	0.38	0.09	
6	0.67	0.86	-0.11	0.52	0.29	-0.06	
7	0.43	0.69	-0.19	0.27	0.17	-0.12	
8	0.25	0.45	-0.31	0.14	0.10	-0.21	

Table S3. The sequence distributions of monomer segments of PAB and PAD (1: AM, 2: cationic monomer) under $f_2 = 0.2$.

x	(P _{PAB1}) _x	(P _{PAB2}) _x	(P _{PAD1}) _x	(P _{PAD2}) _x
1	0.31	0.72	0.28	0.91

2	0.21	0.20	0.20	0.08
3	0.15	0.05	0.15	0.01
4	0.10	0.02	0.10	0
5	0.07	0.01	0.07	0
6	0.05	0	0.05	0
7	0.03	0	0.04	0
8	0.02	0	0.03	0
9	0.02	0	0.02	0
10	0.01	0	0.01	0

Table S4. The sequence distributions of monomer segments of PAB and PAD (1: AM, 2: cationic monomer) under $f_2=0.4$.

x	$(P_{PAB1})_x$	$(P_{PAB2})_x$	$(P_{PAD1})_x$	$(P_{PAD2})_x$
1	0.54	0.50	0.51	0.79
2	0.25	0.25	0.25	0.17
3	0.11	0.13	0.12	0.03
4	0.05	0.06	0.06	0.01
5	0.02	0.03	0.03	0
6	0.01	0.02	0.01	0
7	0.01	0.01	0.01	0
8	0	0	0	0
9	0	0	0	0
10	0	0	0	0

Table S5. The sequence distributions of monomer segments of PAB and PAD (1: AM, 2: cationic monomer) under $f_2=0.6$.

x	$(P_{PAB1})_x$	$(P_{PAB2})_x$	$(P_{PAD1})_x$	$(P_{PAD2})_x$
1	0.73	0.31	0.70	0.63
2	0.20	0.21	0.21	0.23
3	0.05	0.15	0.06	0.09
4	0.02	0.10	0.02	0.03
5	0	0.07	0.01	0.01
6	0	0.05	0	0.01
7	0	0.03	0	0
8	0	0.02	0	0
9	0	0.02	0	0
10	0	0.01	0	0

Table S6. The sequence distributions of monomer segments of PAB and PAD (1: AM, 2: cationic monomer) under $f_2=0.8$.

x	$(P_{PAB1})_x$	$(P_{PAB2})_x$	$(P_{PAD1})_x$	$(P_{PAD2})_x$
1	0.88	0.14	0.86	0.39
2	0.11	0.12	0.12	0.24
3	0.01	0.10	0.02	0.15
4	0	0.09	0	0.09
5	0	0.08	0	0.05

6	0	0.07	0	0.03
7	0	0.06	0	0.02
8	0	0.05	0	0.01
9	0	0.04	0	0.01
10	0	0.04	0	0

Figure:

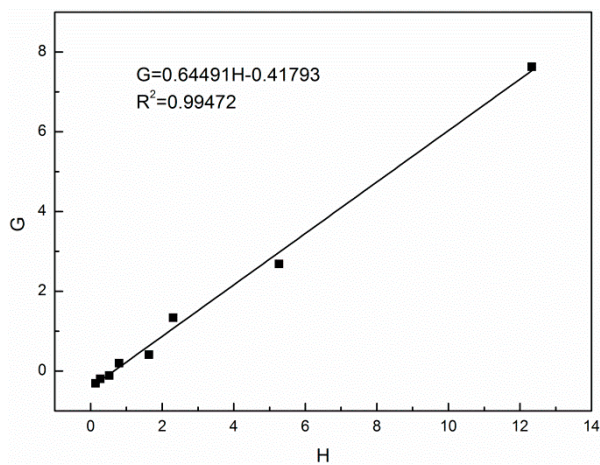


Figure S1. Determination of AM and DMC reactivity ratios by the Fineman-Ross method.

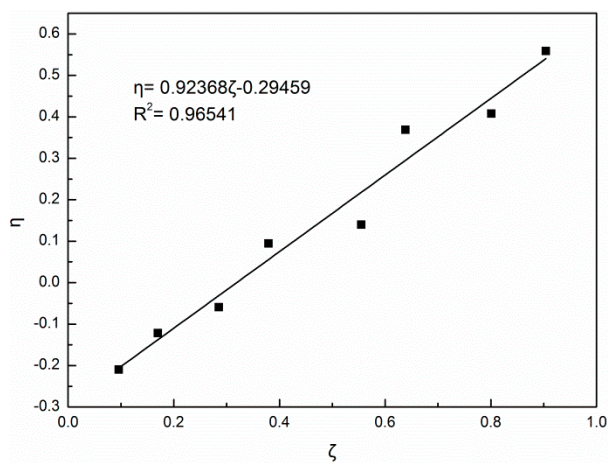


Figure S2. Determination of AM and DMC reactivity ratios by the Kelen-Tüdö method

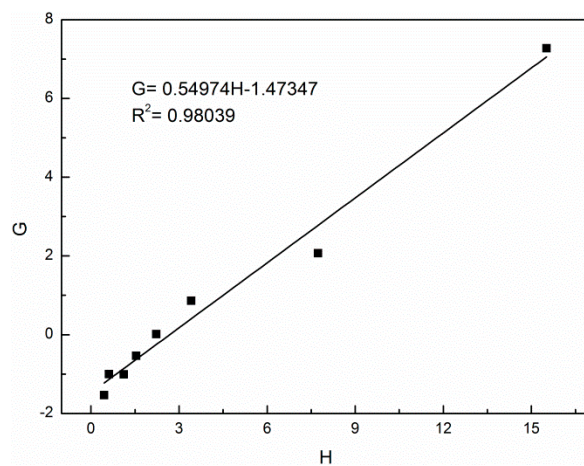


Figure S3. Determination of AM and BDMDAC reactivity ratios by the Fineman–Ross method.

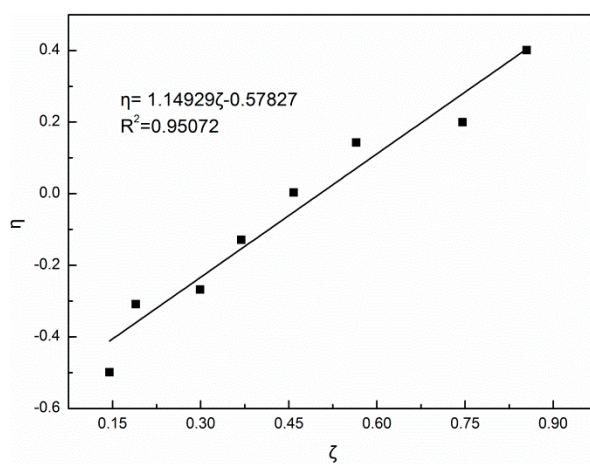


Figure S4. Determination of AM and BDMDAC reactivity ratios by the Kelen–Tüdö method.