Description of Supplementary Files

File Name: Supplementary Information Description: Supplementary Figures, Supplementary Tables and Supplementary References

File Name: Peer Review File



Supplementary Figure 1 | **SEM images and XRD patterns of ZIF-8 membranes. a**, Top view SEM image of ZIF-8 membrane. The sample was prepared with sol concentration of 1 U, coating time of 2 s and deposition time of 2 h. **b**,**c**, Energy dispersion spectroscopy (EDS) mapping of the ZIF-8 membrane corresponding to image **a**. Top view SEM image of **d**, the inner surface and **e**, the ZIF-8 layer on inner surface of the PVDF hollow fibre. **f**, XRD patterns of the simulated ZIF-8 and the ZIF-8 membrane on inner surface of the PVDF hollow fibre.



Supplementary Figure 2 | Powder XRD patterns of Zn-based gel and experimental ZIF-8 powder. The Zn-based gel and bulk ZIF-8 powder were synthesized without substrate. The simulated XRD pattern of ZIF-8 is shown for reference. This result indicates that gel has been transformed to ZIF-8, and the prepared ZIF-8 shows intact crystalline structure.



Supplementary Figure 3 | FTIR spectrums of Zn-based gel and prepared ZIF-8.

The Zn-based gel and bulk ZIF-8 powder were synthesized without substrate. This result shows the change of chemical structure after vapour deposition, demonstrates the formation of ZIF-8.



Supplementary Figure 4 | XRD patterns of ZIF-8 membranes with different deposition time (top) and calcinated ZIF-8 membranes with different deposition time (bottom). The simulated XRD pattern of ZIF-8 is shown for reference. There are no characteristic peaks of ZnO in calcinated ZIF-8 membranes, which verifies that all Zn-based gel has been transformed to ZIF-8.



Supplementary Figure 5 | **Cross-sectional view SEM images of ZIF-8 membranes with various coating times. a**, 5 s, **b**, 10 s and **c**, 30 s. These ZIF-8 membranes were prepared with sol concentration of 1 U and deposition time of 2 h. The thickness of the membrane increases with the coating time.



Supplementary Figure 6 | **Cross-sectional view SEM images of ZIF-8 membranes with various sol concentrations. a**, 0.1 U, **b**, 1.5 U and **c**, 2 U. These ZIF-8 membranes were prepared with coating time of 2 s and deposition time of 2 h. The thickness of membrane increases with the sol concentration.



Supplementary Figure 7 | **Schematic diagrams and top view SEM images. a,c**, Schematic diagram and **b,d**, top view SEM image of **a,b**, the noncontinuous ZIF-8 membrane fabricated with sol concentration of 0.05 U and **c,d**, the continuous ZIF-8 membrane fabricated with sol concentration of 0.1 U. These ZIF-8 membranes were prepared with coating time of 2 s and deposition time of 2 h. The small concentration means the low viscosity, which leads to the small loading and spread in internal substrate of Zn-based sol. Because the surface of porous substrate is composed of nanoparticles with diameter of 20-50 nm, the formed membrane has some cracks.



Supplementary Figure 8 | AFM images of Zn-based gel layer and ZIF-8 membrane. AFM analysis of a,c, Zn-based gel layer and b,d, ZIF-8 layer on PVDF hollow fibres. The samples were prepared with sol concentration of 0.1 U and coating time of 2 s. The vapour deposition time was 2 h. Root mean square roughness (R_q): a, 3.6 nm, b, 5.8 nm c, 7.0 nm, d, 9.3 nm. Arithmetic average roughness (R_a): a, 2.8 nm, b, 4.7 nm c, 5.5 nm, d, 7.3 nm.



Supplementary Figure 9 | Comparison of the prepared ZIF-8 membranes with polymer membranes reported in previous studies for H₂/N₂ and H₂/CH₄ systems. The black line is the Robeson's upper-bound of polymeric membranes reported in 2008. The permeance is calculated from permeability by assuming membrane thickness of 1 μ m. In H₂/N₂ and H₂/CH₄ systems, the performance of our membranes can surpass the Robeson's upper-bound.



Supplementary Figure 10 | Single gas permeation behaviour of various gases through ZIF-8 membranes with various coating times of 2 s, 5 s, 10 s and 30 s. These ZIF-8 membranes were prepared with sol concentration of 1 U and deposition time of 2 h. Blue square is gas permeance. H_2/X_n , CO_2/X_n and C_3H_6/X_n selectivities are depicted in red circle, dark yellow rhombus and dark cyan hexagon, respectively. X_n represents various gases. Red arrow shows the increasing direction of coating time. Gas permeances decreased with increases of coating time.



Supplementary Figure 11 | Gas permeation behaviours of additional three ZIF-8 membranes. These ZIF-8 membranes were prepared with sol concentration of 1 U, coating time of 2 s and deposition time of 2 h. The H₂ permeances of these three membranes were 106.5, 122.9 and 126.7 ×10⁻⁷ mol m⁻² s⁻¹ Pa⁻¹, and the corresponding selectivities of H₂/C₃H₈-C₃H₆/C₃H₈ were 2701-67.2, 2845-64.4 and 3012-68.9, respectively. The results demonstrate the good reproducibility of the membranes. In binary mixture separation of additional ZIF-8 membrane 3, the similar permeances (117.8 ×10⁻⁷ mol m⁻² s⁻¹ Pa⁻¹ for H₂ in H₂/C₃H₈ separation and 2.8 ×10⁻⁷ mol m⁻² s⁻¹ Pa⁻¹ for C₃H₆ in C₃H₆/C₃H₈ separation) and selectivities (3126 for H₂/C₃H₈ and 73.4 for C₃H₆/C₃H₈) were achieved.



Supplementary Figure 12 | Effect of feed pressure on separation performance of C₃H₆/C₃H₈ mixture. The membrane was the additional ZIF-8 membrane 3, as shown in Supplementary Figure 11. The selectivity and the C₃H₆ permeance both decreased with the increase of feed pressure due to the gate opening of window of ZIF-8 structure and the competitively diffusion of the C₃H₆ and C₃H₈ through the membrane. However, membrane still showed good C₃H₆/C₃H₈ selectivity of 22.7 and C₃H₆ permeance of 2.0 ×10⁻⁷ mol m⁻² s⁻¹ Pa⁻¹ at 9 bar.



Supplementary Figure 13 | Schematic diagram of in situ production of MOF membrane module (left) and crystallization process (right). Blue arrows present the diffusion of ligand vapour.



Supplementary Figure 14 | Optical photographs of membrane module and coated membrane module. a, membrane module and b, coated membrane module. The change of colour should be explained by the reaction between polymer and ethanolamine.

Supplementary Table 1 Comparison of ZIF-8 membranes here with polymeric
zeolite and other MOF membranes reported in previous studies for H2/N2
H ₂ /CH ₄ and H ₂ /C ₃ H ₈ systems.

	Substrate	Thickness (100 nm)	Permeance ×10 ⁻⁸ mol m ⁻² $s^{-1} Pa^{-1}$	Selectivity			
Membrane				H_2/N_2	H ₂ /CH ₄	H_2/C_3H_8	Ref
ZIF-8	Al_2O_3	80	20.8	10.3	10.4	149.6	1
ZIF-8	Al_2O_3	200	18.0	16.2	31.5	712.6	2
ZIF-8	Al_2O_3	20	43.2	11.1	12.1	-	3
ZIF-8/LDH	Al_2O_3	200	14	10	12.5	-	4
ZIF-8/LDH	Al_2O_3	11	4.1	16.8	54.1	-	5
ZIF-8	PES	72	40.0	9.2	8.7	-	6
ZIF-8	PSF	200	11.1	22.7	-	-	7
ZIF-8-annealing	P84	13	3.5	-	103	-	8
ZIF-93-annealing	P84	26	1.10	-	97.2	-	9
ZIF-8/GO	AAO	1	5.46	11.1	11.2	405.0	10
ZIF-90- modification	Al ₂ O ₃	200	28.5	-	70.5	458.0	11
ZIF-95	Al_2O_3	300	193.0	10.1	11.0	59.7	12
NH ₂ -MIL-53	Glass	150	151.7	23.9	20.7	-	13
CuBTC	Al_2O_3	130	3.2	8.7	6.2	-	14
CuBTC	PVDF	30	201.0	6.5	5.4	-	15
CuBTC/MIL-100	PVDF	200	8.8	217	336	-	16
PIM	-	1810	1.4	14.8	11.1	-	17
PIM	-	1570	0.5	9.4	4.9	-	17
Zeolite	Al_2O_3	75	16	8.6	6.5	19.3	18
ZIF-8	PVDF	0.17	2154	15.1	17.9	1145	
ZIF-8	PVDF	0.87	1190	22.4	27.3	2894	This
ZIF-8	PVDF	1.14	949	23.1	28.7	3088	
ZIF-8	PSF	2.80	354	24.1	30.7	3212	work
ZIF-8	PVDF	7.57	273	24.8	31.2	3401	

Membrane	Substrate	Thickness	Permeance	Selectivity	Ref	
		(100 nm)	$\times 10^{-8} \text{ mol m}^{-2} \text{ s}^{-1} \text{ Pa}^{-1}$	$C_{3}H_{6}/C_{3}H_{8}$		
ZIF-8	Al_2O_3	22	2.0-3.7	28.0-45.0	19	
ZIF-8	Al_2O_3	15	2.0	55.0	20	
ZIF-8	Al_2O_3	50-200	0.7	30.0	21	
ZIF-8	Al_2O_3	800	0.3	59.0	22	
ZIF-8	Al_2O_3	15	2.0	40.0	23	
ZIF-8	Al_2O_3	25	1.1	30.1	24	
ZIF-8	Al_2O_3	200	0.35	14.6	3	
ZIF-8	Al_2O_3	16	0.06	3.5	25	
ZIF-8/GO	AAO	1	0.16	12	10	
ZIF-8	BPPO	20	1.5	27.8	26	
ZIF-8	Torlon	90	1.2	12.0	27	
ZIF-8	Torlon	50	2.2	65	28	
ZIF-8	Torlon	81	1.5	180	29	
Cabron	Al_2O_3	3	0.75	16	30	
Cabron	Al_2O_3	3	0.87	17	30	
Cabron	Al_2O_3	3	1.4	23	30	
ZIF-8	PVDF	0.17	83.7	44.5		
ZIF-8	PVDF	0.87	27.6	67.2	This	
ZIF-8	PVDF	1.14	20.8	67.8		
ZIF-8	PSF	2.80	7.6	69.5	work	
ZIF-8	PVDF	7.57	5.7	70.8		

Supplementary Table 2 | Comparison of ZIF-8 membranes here with carbon and

other MOF membranes reported in previous studies for C₃H₆/C₃H₈ system.

Supplementary References

- 1. Zhang, X. F. *et al.* A simple and scalable method for preparing low-defect ZIF-8 tubular membranes. *J. Mater. Chem. A* **1**, 10635-10638 (2013).
- Liu, Q., Wang, N., Caro, J. & Huang, A. Bio-inspired polydopamine: A versatile and powerful platform for covalent synthesis of molecular sieve membranes. *J. Am. Chem. Soc.* 135, 17679-17682 (2013).
- Huang, K., Dong, Z. Y., Li, Q. Q. & Jin, W. Q. Growth of a ZIF-8 membrane on the inner-surface of a ceramic hollow fiber via cycling precursors. *Chem. Commun.* 49, 10326-10328 (2013).
- Liu, Y., Wang, N. Y., Pan, J. H., Steinbach, F. & Caro, J. In-situ synthesis of MOF membranes on ZnAl-CO₃ LDH buffer layer-modified substrates. *J. Am. Chem. Soc.* 136, 14353-14356 (2014).
- 5. Liu, Y. *et al.* Remarkably enhanced gas separation by partial self-conversion of a laminated membrane to metal-organic frameworks. *Angew. Chem. Int. Ed.* **54**, 3028-3032 (2015).
- Ge, L., Zhou, W., Du, A. J. & Zhu, Z. H. Porous polyethersulfone-supported zeolitic imidazolate framework membranes for hydrogen separation. J. Phys. Chem. C 116, 13264-13270 (2012).
- 7. Su, P. *et al.* Metal based gels as versatile precursors to synthesize stiff and integrated MOF/polymer composite membranes. *J. Mater. Chem. A* **3**, 20345-20351 (2015).
- Cacho-Bailo, F. *et al.* MOF-polymer enhanced compatibility: post-annealed zeolite imidazolate framework membranes inside polyimide hollow fibers. *RSC Adv.* 6, 5881-5889 (2016).

- Cacho-Bailo, F. *et al.* High selectivity ZIF-93 hollow fiber membranes for gas separation. *Chem. Commun.* 51, 11283-11285 (2015).
- Hu, Y. X. *et al.* Zeolitic imidazolate framework/graphene oxide hybrid nanosheets as seeds for the growth of ultrathin molecular sieving membranes. *Angew. Chem. Int. Ed.* 55, 204-2052 (2016).
- Huang, A., Wang, N., Kong, C. & Caro, J. Organosilica-functionalized zeolitic imidazolate framework ZIF-90 membrane with high gas-separation performance. *Angew. Chem. Int. Ed.* 51, 10551-10555 (2012).
- Huang, A. *et al.* A highly permeable and selective zeolitic imidazolate framework ZIF-95 membrane for H₂/CO₂ separation. *Chem. Commun.* 48, 10981-10983 (2012).
- 13. Zhang, F. *et al.* Hydrogen selective NH₂-MIL-53(Al) MOF membranes with high permeability. *Adv. Funct. Mater.* **22**, 3583-3590 (2012).
- 14. Zhou, S. Y. *et al.* Challenging fabrication of hollow ceramic fiber supported Cu₃(BTC)₂ membrane for hydrogen separation. *J. Mater. Chem.* **22**, 10322-10328 (2012).
- 15. Mao, Y. Y. *et al.* Pressure-assisted synthesis of HKUST-1 thin film on polymer hollow fiber at room temperature toward gas separation. *ACS Appl. Mater. Interfaces* **6**, 4473-4479 (2014).
- Li, W. *et al.* Transformation of metal-organic frameworks for molecular sieving membranes.
 Nature Commun. 7, 11315 (2016).
- Carta, M. *et al.* An efficient polymer molecular sieve for membrane gas separations. *Science* 339, 303-307 (2013).
- 18. Huang, A., Wang, N. & Caro, J. Synthesis of multi-layer zeolite LTA membranes with enhanced gas separation performance by using 3-aminopropyltriethoxysilane as interlayer.

Microporous Mesoporous Mater. 164, 294-301 (2012).

- 19. Pan, Y., Li, T., Lestari, G. & Lai, Z. Effective separation of propylene/propane binary mixtures by ZIF-8 membranes. *J. Membr. Sci.* **390**, 93-98 (2012).
- Kwon, H. T. & Jeong, H. K. In situ synthesis of thin zeolitic-imidazolate framework ZIF- 8 membranes exhibiting exceptionally high propylene/propane separation. *J. Am. Chem. Soc.* 135, 10763-10768 (2013).
- Shah, M. N., Gonzalez, M. A., McCarthy, M. C. & Jeong, H. K. An unconventional rapid synthesis of high performance metal-organic framework membranes. *Langmuir* 29, 7896-7902 (2013).
- 22. Hara, N. *et al.* Diffusive separation of propylene/propane with ZIF-8 membranes. *J. Membr. Sci.* **450**, 215-223 (2014).
- 23. Kwon, H. T. & Jeong, H. K. Highly propylene-selective supported zeolite-imidazolate framework (ZIF-8) membranes synthesized by rapid microwave-assisted seeding and secondary growth. *Chem. Commun.* **49**, 3854-3856 (2013).
- 24. Liu, D., Ma, X., Xi, H. & Lin, Y. S. Gas transport properties and propylene/propane separation characteristics of ZIF-8 membranes. *J. Membr. Sci.* **451**, 85-93 (2014).
- Shekhah, O. *et al.* The liquid phase epitaxy approach for the successful construction of ultra-thin and defect-free ZIF-8 membranes: pure and mixed gas transport study. *Chem. Commun.* 50, 2089-2092 (2014).
- Shamsaei, E. *et al.* Aqueous phase synthesis of ZIF- 8 membrane with controllable location on an asymmetrically porous polymer substrate. *ACS Appl. Mater. Interfaces* 8, 6236-6244 (2016).

- 27. Brown, A. J. *et al.* Interfacial microfluidic processing of metal-organic framework hollow fiber membranes. *Science* **345**, 72-75 (2014).
- Eum, K. *et al.* Fluidic processing of high-performance ZIF-8 membranes on polymeric hollow fibers: Mechanistic insights and microstructure control. *Adv. Funct. Mater.* 26, 5011-5018 (2016).
- Eum, K., Ma, C., Rownaghi, A., Jones, C. W. & Nair, S. ZIF- 8 membranes via interfacial microfluidic processing in polymeric hollow fibers: efficient propylene separation at elevated pressures. ACS Appl. Mater. Interfaces 8, 25337-25342 (2016).
- Ma, X., Lin, Y. S., Wei, X. & Kniep, J. Ultrathin carbon molecular sieve membrane for propylene/propane separation. *AIChE J.* 62, 491-499 (2016).