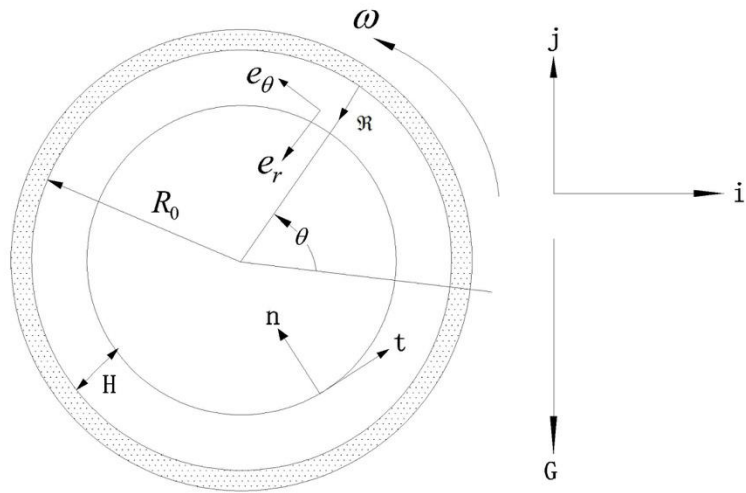
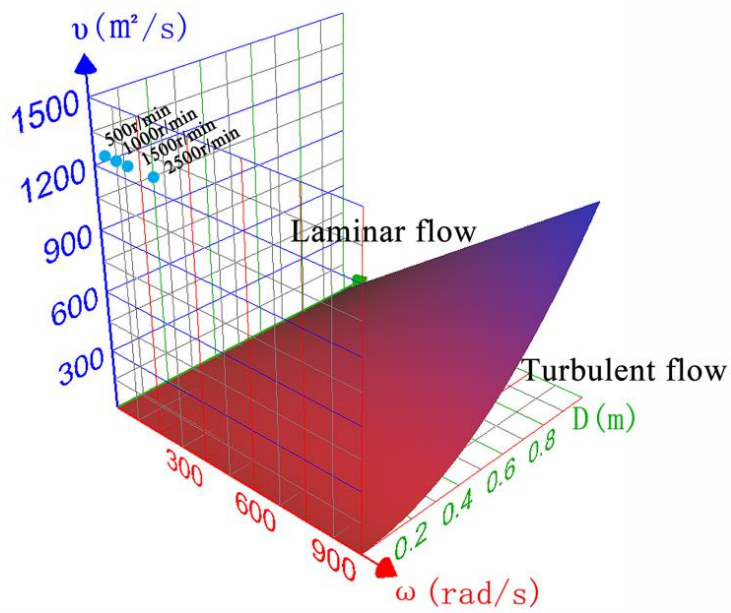


**Efficient and scalable synthesis of highly aligned and compact two-dimensional nanosheets films with record performances**

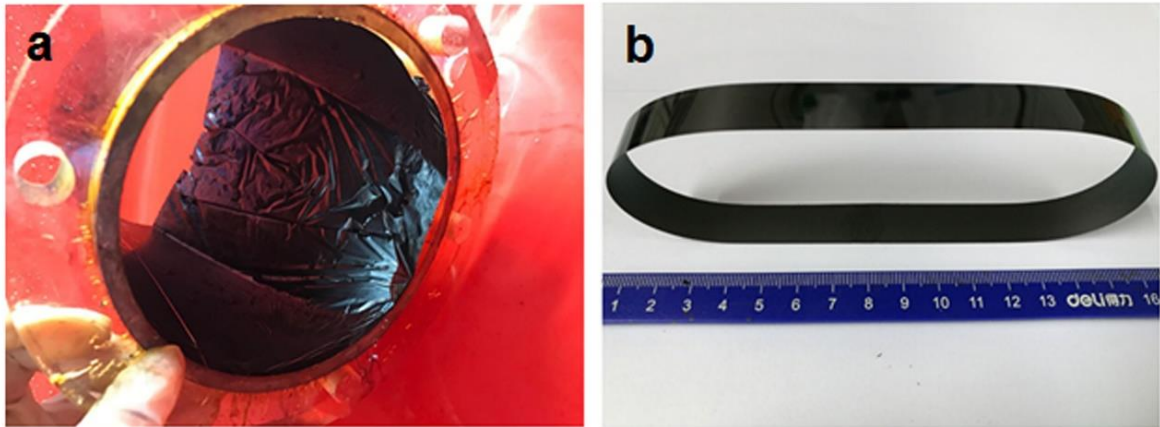
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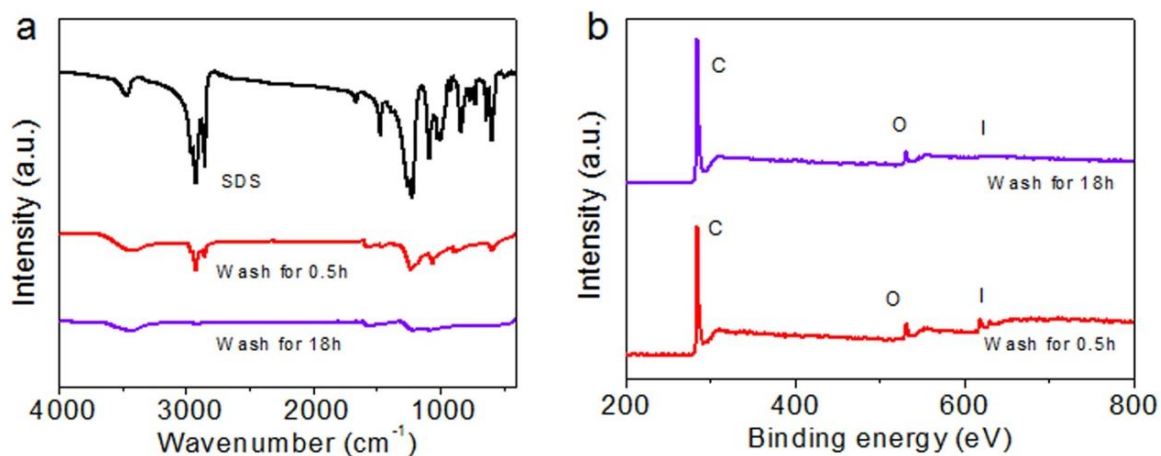
**Supplementary Figure 1. Schematic of a rotating hollow cylinder partially filled with a liquid layer.** The meanings of all the symbols are shown in Supplementary Note 1.



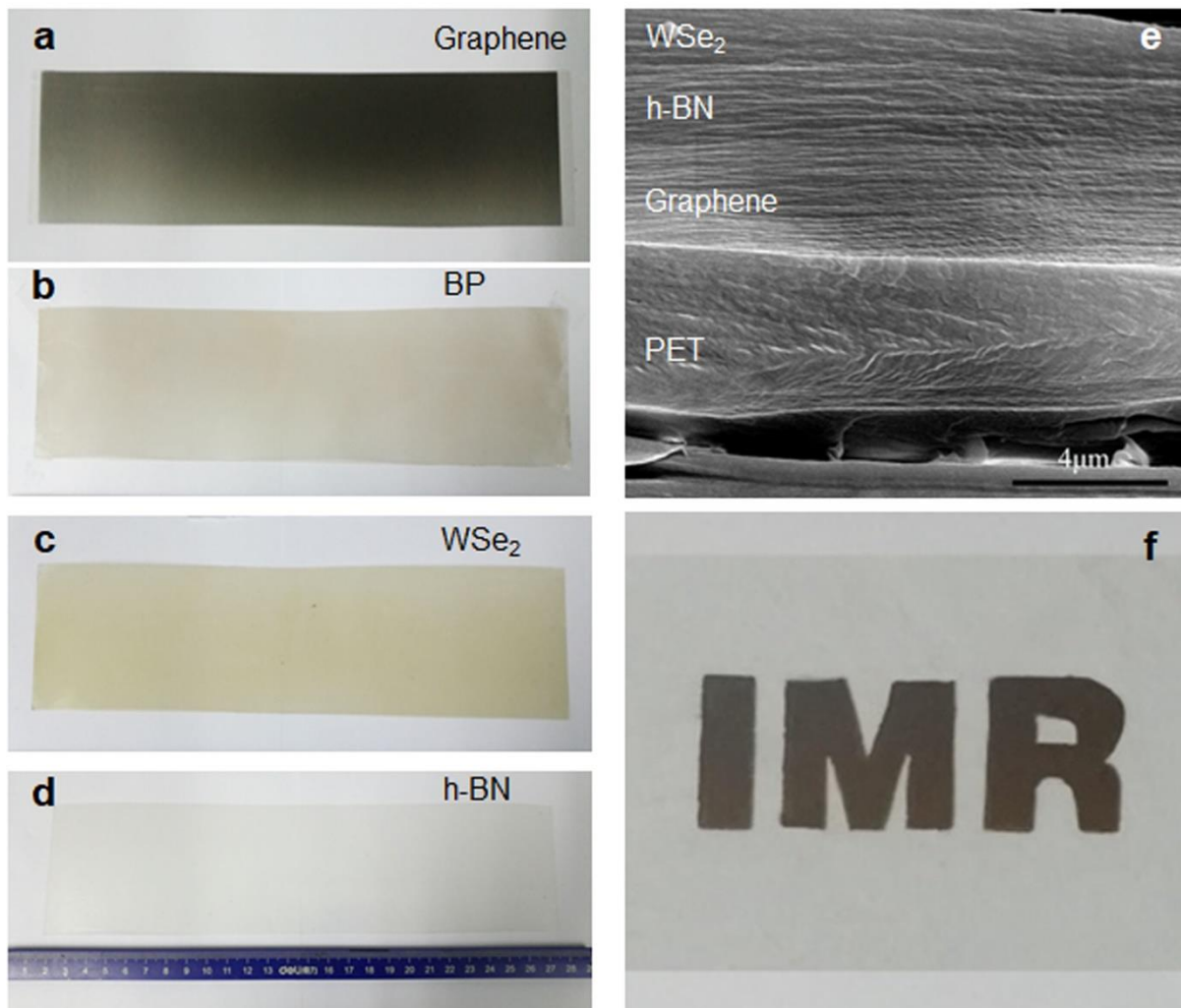
**Supplementary Figure 2. The phase diagram for the laminar and turbulent phase.** The bottom-right and up-left corresponds to the turbulent flow and laminar flow, respectively. The blue dots represent the experimental conditions (viscosity of 1.26 Pa.s, corresponding to the concentration of GO dispersion of  $\sim 8 \text{ mg mL}^{-1}$ ) that are used in our study. In fact, the real viscosity should be much higher than the original value because of the water evaporation caused by heating during the CCC process. Therefore, these blue dots should move further away from the phase transition interface.



**Supplementary Figure 3. rGO films synthesized by CCC method. a,** A hydrophobic rGO film with part immersing into water, showing that it can be easily separated from the silica tube. **b,** A rGO bracelet directly cut out of a continuous rGO film and peeled off from the silica tube.



**Supplementary Figure 4. Characterization of the residual SDS and iodine in the rGO/SWCNT hybrid films.** FTIR (a) and XPS (b) spectra of the rGO/SWCNT hybrid film soaked in DI water for different time (0.5 h, 18 h) followed by ethanol washing for 2 h. The peaks at 2853 cm<sup>-1</sup> and 2992 cm<sup>-1</sup> correspond to the vibrational modes of methyl and methylene group in SDS, respectively, which were used to measure qualitatively the amount of residual SDS, and both of the two peaks diminish with increasing the soaking time in water.



**Supplementary Figure 5. 2D nanosheet films and heterostructures synthesized by CCC method on PET substrate. a-d**, Photos of a graphene film (a), black phosphorus (BP) film (b), WSe<sub>2</sub> film (c), and hexagonal boron nitride (h-BN) film (d). **e**, SEM image of a vertical graphene/h-BN/WSe<sub>2</sub> heterostructure film. **f**, Patterned graphene films.

**Supplementary Table 1.** Comparison of the GO films synthesized by different methods with different GO nanosheets.

Synthesis method	lateral size of GO nanosheets ( $\mu\text{m}$ )	C/O ratio of GO nanosheets	Interlayer Spacing ( $\text{\AA}$ )	FWHM (degree)	Reference
VF	1-2	1.2	8.04	0.69	1
VF	1-2	1.2	8.05	0.55	1
VF	1-5	NA	8.03	2.06	2
VF	NA	NA	8.3	NA	3
VF	0.5	NA	7.96	1.71	4
VF	NA	NA	9.4	0.74	5
BCO	40	NA	9.07	0.75	6
SC	NA	0.96	8.6	1.71	7
SE	NA	1.49	7.01	0.95	8
SCO	44	NA	9.42	2.74	9
VS	1	2.38	8.50	2.01	10
VF	5 ( $5^\circ\text{C}$ )	2.25	7.90	1.09	11
VF	5 ( $35^\circ\text{C}$ )	2.26	7.5	0.54	11
VF	5	2.32	9.40	0.75	12
VF	33	2.4	9.50	0.95	12
VF	60	2.45	9.10	1.31	12
VF	93	2.61	8.58	0.86	12
CCC@2500	1	1.7	7.5	0.55	This work

VF = Vacuum filtration

NA = Not available

BCO = Bar coating

SC = Solvent casting

SE = Solvent evaporation

SCO = Spin coating

VS = Vacuum suction.

CCC = Continuous centrifugal casting

**Supplementary Table 2.** Structure, strength and electrical conductivity comparison of the rGO films synthesized by different methods.

Synthesis method	lateral size ( $\mu\text{m}$ )	XRD Peak (degree)	FWHM (degree)	Strength (MPa)	Conductivity ( $\text{S cm}^{-1}$ )	Reference
VF	5	NA	NA	20	190	12
VF	33	NA	NA	24	380	
VF	60	NA	NA	26	480	
VF	93	NA	NA	28	500	
SA	5	24.4	1.31	162	298	13
VF	1.3	23.37	4.97	150	40	14
VF@220°C	1.3	25.66	1.7	293	120	
VF@500°C	1.3	26.15	1.55	90	295	
SE	2.5	NA	NA	117	45	15
ESD	NA	24.12	3.5	66	26	16
SA	22	24.62	3.56	170	210	17
VF	NA	NA	NA	118	50	18
CCC@1500	20	25.7	1.13	591	602	This work
CCC@2500	20	25.94	1.02	662	647	

SA = Self assembly

ESD = electro-spray deposition



**Supplementary Table 3.** Capacitance comparison of the all-solid-supercapacitors based on different electrode materials.

Electrode material	Specific capacitance ( $F g^{-1}$ )	Volumetric capacitance ( $F cm^{-3}$ )	Discharge rate	Reference
Graphene/CNT	508	300	$26.7 mA cm^{-3}$	19
Graphene/CNT	~237	158	$0.1 mA cm^{-2}$	20
MWCNT/PEDOT	119	179	$10 mV s^{-1}$	21
CF/MnO <sub>2</sub>	1	2.5	$20 mA cm^{-3}$	22
Co <sub>3</sub> O <sub>4</sub> @Ni Wire/Graphene	0.3	2.1	$20 mA cm^{-3}$	23
CF@ZnO@MnO <sub>2</sub> <sup>+</sup>	<0.64	0.325	$50 mA cm^{-3}$	24
CNT/MnO <sub>2</sub> Yarn <sup>++</sup>	<17	25.4	$10 mV s^{-1}$	25
N-doped CF	260	4.3	$500 mA cm^{-3}$	26
B, N co-doped graphene aerogels	62	49.6	$5 mV s^{-1}$	27
Undoped graphene aerogels	43	34.4	$5 mV s^{-1}$	27
N-doped graphene aerogels	52	41.6	$5 mV s^{-1}$	27
B-doped graphene aerogels	55	44	$5 mV s^{-1}$	27
Graphene paper <sup>+++</sup>	29	23.2	$5 mV s^{-1}$	27
Laser scribing graphene	202	0.45	$1 A g^{-1}$	28
Activated CC	0.003	0.0088	$10 mV s^{-1}$	29
Coaxial fiber of aligned CNT fiber and sheet	59	32.09	$46 mA cm^{-3}$	30
GF@3D-G fiber	40	9.2	$142 \mu A cm^{-2}$	31
CF@ZnO@MnO <sub>2</sub> *	0.033	0.066	$100 mV s^{-1}$	32
CF@MnO <sub>2</sub> /CF@Fe <sub>2</sub> O <sub>3</sub>	91.3	1.5	$2 mA cm^{-2}$	33
N-doped CF <sup>++++</sup>	77.4	38.7	$25 mV s^{-1}$	34
Graphene hydrogel	187	31	$10 mV s^{-1}$	35
rGO/SWCNT	255	407	$114 mA cm^{-3}$	This work

+ The author did not provide the specific capacitance directly, which was estimated by assuming the density of the electrode as  $2 \text{ g cm}^{-3}$ .

++The specific capacitance was estimated by assuming the density of the electrode as  $1.5 \text{ g cm}^{-3}$ .

+++ The volumetric capacitance was estimated by assuming the density of the electrode as  $0.8 \text{ g cm}^{-3}$ .

++++ The volumetric capacitance was estimated by assuming the density of the electrode as  $0.1 \text{ g cm}^{-3}$ .

\* The author did not provide the specific capacitance directly, which was estimated by the given geometrical size and density of the plastic wire by  $2 \text{ g cm}^{-3}$ .

## Supplementary Note 1. Analysis of fluid dynamics during CCC process

In a liquid flow, shear stress is generated when there is velocity gradient in the direction that is perpendicular to the velocity direction. In our method, when the hollow tube is rotated, the first liquid layer that is adjacent to the tube inner surface will stick on the tube according to the non-slippery boundary condition, and thus has the same linear velocity with the inner surface of the rotating tube. The second liquid layer is then pulled by the first liquid layer to move along because of the viscosity of the liquid. Such disturbance generated by the tube rotation thus propagates from the liquid-solid interface (tube inner surface) deep into the liquid flow. The transient shear rate distribution at the beginning of the tube rotation (at 1 microsecond) was investigated by the software of CONSOL. As shown in Fig. 1b in the main text, the disturbance transports from the liquid-solid boundary into liquid immediately once the tube starts to rotate, generating uniform shear rate around the tube inner surface.

As discussed in the main text, the liquid layer around the inner surface of a rotating hollow tube, typically considered as rimming flow, is a non-trivial example of a steady, two-dimensional, viscous flow with a free surface. As shown in Supplementary Fig. 1, we considered a horizontally placed circular hollow cylinder with inside radius  $R_0$ , which rotates at a constant angular velocity ( $\omega$ ) around its axis. Polar coordinates were used:  $\Theta$  and  $\mathfrak{R}$  are the angular azimuthal coordinate and radial coordinate, respectively, and  $\mathbf{e}_\theta$  and  $\mathbf{e}_r$  are the corresponding unit tangent vectors. The cylinder is partially filled with Newtonian liquid which is distributed in a layer around the inner wall. Strictly speaking, the thickness of the liquid layer varies with the cylinder and is a function of  $\theta$ , that is  $H(\theta)$ , because of the influence of the local gravitational acceleration (which is denoted as  $\mathbf{G}$  along the vertical direction of  $\mathbf{j}$ ). Since the gas occupying the rest of the volume in the cylinder is inviscid, the viscous stress exerted by the relatively rarefied gas at the gas/liquid interface is negligible, and thus can be modeled as by a uniform pressure  $\mathbf{P}_a$ .

Based on the above analysis, this trimming flow can be modeled mathematically as follows:

$$\left\{ \begin{array}{l} \mathbf{V} \cdot \nabla \mathbf{V} = -\rho^{-1} \nabla \mathbf{P} + \nu \nabla^2 \mathbf{V} - \mathbf{Gj} \\ \nabla \cdot \mathbf{V} = 0. \end{array} \right\} \quad (1)$$

where  $\mathbf{V}(R)$  and  $\mathbf{P}(R)$  are liquid velocity and pressure fields, respectively. The density  $\rho$ , viscosity  $\mu$ , kinematic viscosity  $\nu = \mu/\rho$  and surface tension  $\sigma$  of the liquid are all assumed uniform.

The no-slip boundary condition at the liquid-wall interface is:

$$\mathbf{V} = \omega R_0 \mathbf{e}_\theta \quad \text{at} \quad \mathbf{R} = -R_0 \mathbf{e}_r \quad (2)$$

The balance of traction at the liquid/gas interface gives the boundary condition:

$$(P - P_a) \mathbf{n} - \mu \left[ \nabla \mathbf{V} + (\nabla \mathbf{V})^T \right] \cdot \mathbf{n} + 2\sigma K \mathbf{n} = 0 \quad \text{at} \quad \mathbf{R} = -(R_0 - H) \mathbf{e}_r. \quad (3)$$

where  $\mathbf{n}$  is the unit normal to the interface, directed to the gas, and  $K$  is the mean curvature of the interface:

$$K = \frac{1+2[H_\theta/(R_0-H)]^2+H_{\theta\theta}/(R_0-H)}{2(R_0-H)\{1+[H_\theta/(R_0-H)]^2\}^{\frac{3}{2}}} \quad (4)$$

Since no liquid can cross the interface, the velocity along the normal direction should be zero:

$$\mathbf{V} = \omega R_0 \mathbf{e}_\theta \quad \text{at} \quad \mathbf{R} = -R_0 \mathbf{e}_r \quad (5)$$

It is obvious that the solution for the above equations must be periodic with respect to the coordinate of  $\theta$  with a period of  $2\pi$ .

The average thickness of the liquid layer ( $D$ ) is given by

$$2R_0 D - D^2 = \frac{1}{2\pi} \int_0^{2\pi} (2R_0 H - H^2) dX \quad (6)$$

For the high rotation rate,  $G$  can be neglected, and thus we assume  $G = 0$ .

An analytical solution can be obtained:

$$\left. \begin{array}{l} \mathbf{V} = \omega(R_0 - Y) \mathbf{e}_\theta, \\ P - P_a = \rho \Omega^2 \left[ R_0(D - Y) - \frac{1}{2}(D^2 - Y^2) \right] - \frac{\sigma}{R_0 - D}, \\ H = D. \end{array} \right\} \quad (7)$$

The derived shear stress for this Newtonian flow is:

$$\boldsymbol{\sigma}_{\text{shear}} = \mu\omega\mathbf{e}_{\theta} \quad (8)$$

During the continuous centrifugal casting process, the 2D nanosheets are also subjected to centrifugal force at the same time. The centrifugal stress that is applied on 2D nanosheets is given by:

$$\boldsymbol{\sigma}_{\text{centrifugal}} = \rho_g t_g R_0 \omega^2 \mathbf{e}_r \quad (9)$$

where  $\rho_g$  and  $t_g$  are the density and thickness of 2D nanosheets, respectively.

## **Supplementary Note 2: Discussion on the data shown in Supplementary Table 1**

Dip coating, spin coating, and spray coating were also reported for the synthesis of GO film, but the films obtained are mostly used for transparent conductive films and the XRD data were not provided. In Supplementary Ref. 11, authors synthesized GO at two different temperatures (5 °C and 35 °C) to control the defects. The GO nanosheets synthesized at 5 °C show much less defects than those synthesized at 35 °C. As shown in Supplementary Ref. 12, the lateral size of GO nanosheets plays an important role in the interlayer spacing and alignment of the films. The relatively small interlayer spacing shown in Supplementary Ref. 8 is probably due to the large lateral size of the GO nanosheets and the annealing at 80 °C for 8 hours, and the relatively small FWHM shown in Supplementary Ref. 11 is probably due to the large lateral size of the GO nanosheets as well.

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