Supplementary Information for

Quantifying the factors limiting rate-performance in battery electrodes

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Supplementary Tables

	$(C_{eff}/V)/\sigma_{M}$	$\sigma_{_0}/\sigma_{_M}$	S	β_1	Q_V	$C_{V,eff}$	$\sigma_{_M}$	$\sigma_{_0}$
units	s m ⁻²	-	-	s m ⁻²	mAh m ⁻³	F m ⁻³	S m ⁻¹	S m ⁻¹
J Zhang	2.7×10^{14}	1060	3	2×10 ⁹	2.0×10 ⁹	5.6×10 ¹⁰	1.0×10 ⁻⁴	0.11
J Coelho	1015	4000	1.4	2×10 ⁹	2.8×10 ⁸	7.8×10 ⁹	3.9×10 ⁻⁶	1.6×10 ⁻²
B Zhang	5.5×10 ¹³	4×10^{6}	3.5	2.2×10 ¹²	5.3×10 ⁸	1.5×10 ¹⁰	1.3×10 ⁻⁴	5.4×10^{2}
Yu	3.3×10 ¹¹	1.2×10^{6}	2.7	2.3×10 ⁹	4.8×10 ⁸	1.3×10 ¹⁰	2.0×10 ⁻²	2.5×10^4

Supplementary Table 1. Physical percolation properties from references (figure 3 main text).

Cohort I: Lithium ion batteries

Supplementary	Table 2.	Literature	details for	Cohort IA
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Row No.	Electrode	Electrode composition	Mass loading (M _{Total} /A and M _{AM} /A)	Particle size, morphology or density	Electrode thickness	Ref.			
	NMC111 (1C = 200 mA g^{-1})								
	Carbon coated	AM: PTEF: C	6.2	Particle size: 50–200 nm					
1	NMC111	= 80: 5: 15	(AM: 5 mg cm ⁻²)	Particle size: 150 nm with 10 nm carbon coating	≈ 40 µm	1			
2	Slurry-casted NMC111 electrode	NMC111: CB: PVDF = 85: 7: 8	28 mg cm ⁻² (NMC: 24 mg cm ⁻²)	Particle size: 6–8 μm	104 µm	2			
3	Slurry-casted NMC111 electrode	NMC111: CB: graphite: PVDF =90: 3: 4: 3 Full Pouch bag cells	82 mg cm ⁻² (NMC: 73.8 mg cm ⁻²)	Commercial NMC (BASF)	305 µm	3			
		LiNi0.5Mn	$1.5O_4 (1C = 147 \text{ mA g}^{-1})$						
4	Electrospray/ spinning of LMNO	LMNO: MWCNT: PAN = 72: 3.6: 24.4	80 mg cm ⁻² (LMNO: 57 mg cm ⁻²)	Particle size: 100–500 nm	420 µm	4			
		LiCoO	$p_2 (1C = 140 \text{ mA g}^{-1})$						
5	LiCoO ₂ /CNT free- standing film by vacuum-filtration (CNT as substrate)	LCO: CB: PVDF = 77.5: 12.5: 10	16.1 mg cm ⁻² (LCO: 12.5 mg cm ⁻²)	Particle size: 5–10 μm	150 µm	5			
			97.16 mg cm ⁻²	74% of the	260 µm				
	Mechanically	Free-standing	298.96 mg cm ⁻²	crystal density (5.05 g cm^{-3})	400 μm 800 μm				
6	pressed LiCoO ₂	pellet	114.23 mg cm ⁻²	87% of the	260 µm	6			
	penet electrode		175.74 mg cm ⁻²	theoretical	400 µm				
			351.48 mg cm ⁻²	(5.05 g cm^{-3})	800 µm				
		LiFePO	$D_4 (1C = 170 \text{ mA g}^{-1})$						
7	High tap density nanoplate packed LiFePO4/C microspheres	AM: AB: PTFE = 75: 20: 5 (Symmetric charge/dischar ge rate)	$\approx 6.67 \text{ mg cm}^{-2}$ (AM: 5 mg cm ⁻²)	Secondary particle size: 0.5-2 µm Tap density for AM: 1.4 g cm ⁻³	≈50 µm	7			

8	Soft-contact conductive carbon (SCC) to LiFePO ₄	LFP: SCC: PTFE = 70: 20: 10	3.64 mg cm ⁻² (AM: 2.55 mg cm ⁻²)	Particle size: 50 nm	15 µm	8
9	Vacuum-filtrated CNF–CNT–LiFeP O4 film	LFP: CNT: CNF = 80: 15: 5	5.5 mg cm ⁻² (LFP: 4.4 mg cm ⁻²)	Particle size: 200–700 nm	≈ 60 µm	9
	Slurry-coating	LED/C·CB·	43.3 mg cm ⁻² (AM: 32.5 mg cm ⁻²)	Particle size: Unknown	330 µm	
10	LiFePO ₄ onto porous metal foam	PVDF	62 mg cm ⁻² (AM: 46.5 mg cm ⁻²)	Electrode	430 µm	10
	substrate	- 75. 15. 10	75.1 mg cm ⁻² (AM: 56.3 mg cm ⁻²)	density: 1.35 g cm ⁻³	540 µm	
		Si (1	$C = 3500 \text{ mA g}^{-1}$			
11	PEDOT: PSS + CMC binder	Si: AB: (PEDOT: PSS): CMC =70:10:10:10	1.5 mg cm ⁻² (Si: 1.05 mg cm ⁻²)	Particle size: 50–100 nm	10 µm	11
12	CVD growth of Si nanowires	Si film <i>via</i> CVD	Si: 2.47 mg cm ⁻²	Nanowires with D \approx 300nm	90 µm	12
13	Si-graphene composite by vacuum filtration	Si: graphene = 62: 38	3.7 mg cm ⁻² (Si: 2.3 mg cm ⁻²)	Particle size: ≈100 nm	28 µm	13
14	Si nanowire- graphene composites	Si: 70–80%	$\approx 8 \text{ mg cm}^{-2}$ (Si: 6 mg cm ⁻²)	Nanowires with D= 10–100 nm	40 µm	14
		Li4Ti5O	$D_{12} (1C = 175 \text{ mA g}^{-1})$			
15	Flexible and self- standing electrodes <i>via</i> vacuum filtration	LTO: MWCNTs= 85: 15	5.25 mg cm ⁻² (LTO: 4.46 mg cm ⁻²)	Particle size: 2 µm	25 µm	15
16	Mesoporous spinel Li ₄ Ti ₅ O ₁₂ nanosheets	AM: AB: PTFE = 80: 10: 10	10.6 mg cm ⁻² (AM: 8.5 mg cm ⁻²)	Mesoporous nanosheets: 150–200 nm	30 µm	16
17	$\begin{array}{c} \text{Rutile-TiO}_2\\ \text{nanocoated}\\ \text{Li}_4\text{Ti}_5\text{O}_{12}\\ \text{nanosheets} \end{array}$	AM: Super P: PVDF = 80: 10: 10	12.5 mg cm ⁻² (AM: 10 mg cm ⁻²)	Nanosheets thickness: 30–60 nm (AM: 1.5 g cm ⁻³)	≈ 100 µm (AM: 70 µm)	17
		Graphi	te (1C = 372 mA g ⁻¹)			Γ
18	Magnetically aligned graphite electrodes	Large graphite flakes: Small flakes: PVP: Super P= 15.4: 3.8: 2.4: 2.3	6.3 mg cm ⁻² (Graphite: 5 mg cm ⁻²)	Graphite size: Large flake \leq 44 µm small flakes: 7–10 µm	≈ 110 µm	18
19	Coating of graphite anode with coal tar pitch as an effective precursor	AM: SBR: CMC = 90: 5: 5	6 mg cm ⁻² (AM: 5.4 mg cm ⁻²)	particle size 10 µm Active material: 1.5 g cm ⁻³	40 µm	19

Supplementary Table 3. Literature details for Cohort IB (data sets with varying electrode thickness)

Row No.	Electrode	Electrode details	Electrolyte details	Separator thickness	Ref.			
	Theoretical density: NMC-4.77 g cm ⁻³ LFP-3.6 g cm ⁻³ Graphite-2.25 g cm ⁻³							
1	Slurry-casted NMC111/LFP electrode	NMC111 Thickness: 24–104 μm Density: 2.7 g cm ⁻³ Porosity: 44% LFP Thickness: 10–108 μm Density: 1.8 g cm ⁻³ Porosity: 50%	1 M LiPF ₆ in EC/DEC=1:1 $\sigma_{BL} \approx 0.8 \text{ S m}^{-1}$	Unknown	2			
2	Slurry-casted NMC622 or graphite electrodes with different areal capacity	NMC622 Thickness: 48–154 μm Porosity: 32–37% Graphite Thickness: 58–182 μm Porosity: 37–40%	1 M LiPF ₆ in EC/EMC (3:7 weight ratio) + additional 2 wt.% vinylene carbonate (BASF) $\sigma_{BL} \approx 0.5$ S m ⁻¹	Unknown	20			
	Nb	2O5/Graphene composite	-3.85 g cm ⁻³					
3	Three-dimensional holey- graphene/niobia composites	Electrode porosity: ≈ 60%.	1 M LiPF ₆ in EC/DMC (1:1 volume ratio, BASF) $\sigma_{BL} \approx 1.16$ S m ⁻¹	Unknown	21			
		LFP-3.6 g cm ⁻³						
4	LiFePO4 cathodes with different electrode parameters	Density: 2.2 vs. 1.55 g cm ⁻³ . Porosity: 40% vs. 57%.	0.7, 1.0, and 1.3 M LiPF ₆ in EC/DEC or EC/DMC (3:7 by volume ratio) σ_{BL} : 1 M LiPF ₆ in EC/DEC (3:7): 0.724 S m ⁻¹ 1 M LiPF ₆ in EC/DMC (3:7): 1.872 S m ⁻¹	Unknown	22			
	·	GaS - 3.86 g cm ⁻	3					

5	Liquid-phase exfoliated 2D gallium chalcogenide nanosheet/CNT composites	Thickness: 5–29 μm Density: 0.44–0.6 g cm ⁻³ Porosity: 84–89%.	1 M LiClO ₄ in EC/DMC (1:1 volume ratio) $\sigma_{BL} \approx 0.5$ S m ⁻¹	50 µm	23					
	Data collected by us									
	51-2.55 g cm ⁻³									
		NMC-4.77 g cm ⁻	3							
6	LTO/CNT	Thickness: 5–100 μm Density: 0.5 g cm ⁻³ Porosity: 85%.	1 M LiPF ₆ in EC/DEC/FEC, (3:6:1 volume ratio, BASF) with 2 wt% VC $\sigma_{BL} \approx 0.5-1.0$ S m ⁻¹	25 µm	This work					
7	NMC/CNT	Thickness: $115-540$ µm Density: $1.75-2.13$ g cm ⁻³ Porosity: 55-63 %.	Half Cell: 1 M LiPF ₆ in EC/DEC/FEC (3:6:1 volume ratio, BASF) with 2 wt% VC $\sigma_{BL} \approx 0.5 - 1.0$ S m ⁻¹	25 µm	This work					
8	SiGr/CNT	Thickness: 30–300 μm Density: 0.4 g cm ⁻³ Porosity: 83%.	1 M LiPF ₆ in EC/DEC/FEC (3:6:1 volume ratio, BASF) with 2 wt% VC $\sigma_{BL} \approx 0.5-1.0$ S m ⁻¹	25 µm	This work					
9	μSi/CNT	Thickness: 30-170 μm Density: 0.43-0.64 g cm ⁻³ Porosity: 73-82%.	1 M LiPF ₆ in EC/DEC/FEC (3:6:1 volume ratio, BASF) with 2 wt% VC $\sigma_{BL} \approx 0.5-1.0$ S m ⁻¹	25 µm	This work					

Cohort II: Sodium ion batteries

Supplementary Table 4. Literature details for Cohort II (Na-ion batteries)

Row No.	Electrode	Electrode compositio n	Mass loading (M _{Total} /A and M _{AM} /A)	Particle size, morphology or density	Electrode thickness	Ref.	
			Cathode				
		Na0.44MnO2 (1	Na4Mn9O18) (1C = 120) mA g ⁻¹)			
1	Na _{0.44} MnO ₂ nanoplate cathode	AM: Super C65: PVDF = 80: 10: 10	2 mg cm ⁻² (AM: 1.6 mg cm ⁻²)	Particle size: 6 μm in length and 2 μm in width	≈ 10–20 µm	24	
		Na ₂ Fe	$P_2O_7 (1C = 97 \text{ mA g}^{-1})$)			
		Theoret	tical density: 3.15 g cr	n ⁻³			
2	Na ₂ FeP ₂ O ₇ nanoparticles on porous carbon cloth	AM: Super P: PVDF = 70: 15: 15	1.4-2.1 mg cm ⁻² (NMC: 1-1.5 mg cm ⁻²)	Particle size: 20 – 50 nm Particles embedded in carbon	≈ 10 µm	25	
Na ₂ FePO ₄ F (1C = 124 mA g^{-1})							
		Theoret	tical density: 3.32 g cr	n ⁻³			
3	Na ₂ FePO ₄ F nanoparticles by enhancing surface carbon functionality	AM: Super P: PVDF = 70: 20: 10 (AM mixed by Na ₂ FePO ₄ F : GO = 80/20)	1–2 mg cm ⁻² (AM: 0.7–1.4 mg cm ⁻²)	Particle size: 25 nm	< 10 μm (doctor- blade 10 μm)	26	
		Na ₂ VTi	$(PO_4)_3 (1C = 147 \text{ mA})_3$	g-1)			
4	Na ₂ VTi(PO ₄) ₃ as ionic conductor structured electrode	AM: Super P: PVDF = 70: 20: 10	1.75–2.2 mg cm ⁻² (AM: 1.225–1.54 mg cm ⁻²)	Particle size: ≈ 200 nm	≈ 15–20 µm	27	
		Na ₃ V ₂ (PO_4)3 (1C = 110 mA g	-1)			
	1	Theoret	tical density: 3.21 g cr	n ⁻³			
5	Carbon-coated Na ₃ V ₂ (PO ₄) ₃ embedded in porous carbon matrix	AM: Super P: PVDF = 70: 20: 10	1.43 mg cm ⁻² (AM: 1 mg cm ⁻²)	Particle size: 60 nm	$pprox 20~\mu m$	28	
6	Hierarchical carbon framework wrapped $Na_3V_2(PO_4)_3$ as a cathode	AM: AB: PVDF = 70: 20: 10	1.43 mg cm ⁻² (AM: 1 mg cm ⁻²)	Particle size: 100–500 nm	≈ 15 µm	29	

7	Layer-by-Layer Na ₃ V ₂ (PO ₄) ₃ embedded in rGO	AM: CB: PVDF = 70: 20: 10	1.5–2.0 mg cm ⁻² (AM: 1–1.4 mg cm ⁻²)	Particle size: 200 nm	≈ 15–20 µm	30	
		NaCi	$CO_2 (1C = 110 \text{ mA g}^{-1})$	m ⁻³			
	l		lical defisity: 4.50 g ci	II *			
8	Layered O ₃ -type carbon-coated NaCrO ₂ cathode for Na-ion battery (Yu <i>et al.</i>)	AM: KS-6: Super P: PVDF = 85: 3.75: 3.75: 7.5 All samples with x wt% carbon coating (0 <x<16.6%)+7.5% (KS- 6+superP)</x<16.6% 	4.1 mg cm ⁻² (AM: 3.5 mg cm ⁻²)	Particle size: ≈ 500 nm	≈ 20 µm	31	
$FePO_4 (1C = 178 \text{ mA g}^{-1})$ Theoretical density 2.87 g cm ⁻³							
9	Mesoporous FePO ₄ nanospheres as cathode	AM: KB: PVDF = 70: 20: 10	2 mg cm ⁻² (AM: 1.4 mg cm ⁻²)	Particle size: 100 nm	$pprox 30 \mu m$	32	
			Anode				
		TiC Theoret	D ₂ (1C = 335 mA g ⁻¹) tical density: 4.23 g cr	n -3			
10	Carbon-coated anatase TiO ₂ anode	$TiO_{2}:$ $Carbon$ $coating:$ $Super C65:$ $PVDF$ $=$ $65:12:13:10$ $TiO_{2}:$ $Carbon$ $coating:$ $Super C65:$ $PVDF$ $= 65:9:16:10$ $TiO_{2}:$ $Carbon$ $coating:$ $Super C65:$ $PVDF$ $= 65:0:25:10$	1.85–2.31 mg cm ⁻² (TiO ₂ : 1.2–1.5 mg cm ⁻²) 1.85–2.77 mg cm ⁻² (TiO ₂ : 1.2–1.8 mg cm ⁻²) 1.85 mg cm ⁻² (TiO ₂ : 1.2 mg cm ⁻²)	Particle size: 11 nm Particle size: 40 nm Particle size: 15 nm	< 120 µm (doctor- blade) ≈ 20−30 µm	33	

	Carbon (1C = 372 mA g^{-1}) Theoretical density: 2.26 g cm ⁻³							
11	Hard carbon anode <i>via</i> graphene oxide	AM: PVDF	2.7 mg cm ⁻²	Without GO particle size: 30–80 µm		34		
11	as dehydration agent	= 93: 7	$(AM: 2.5 \text{ mg cm}^{-2})$	With GO particle size: 80–110 µm	40 μπ			
Graphite (1C = 372 mA g ⁻¹)								
		Theoret	tical density: 2.28 g cr	n ⁻³				
12	Expanded graphite (EG) as anode	EG: Na alginate = 85: 15	0.6 mg cm ⁻² (EG: 0.5 mg cm ⁻²)	(Unknown)	$\approx 10 \mu m$	35		
13	Natural graphite using ether-based electrolytes	AM: CB: PVDF = 70: 20: 10	4.3 mg cm ⁻² (AM: 3 mg cm ⁻²)	Particle size 100 μm	45 µm	36		
		Sb	$(1C = 660 \text{ mA g}^{-1})$					
		Theoret	tical density: 6.68 g ci	n ⁻³				
	Monodispersed Sb nanocrystals for Li-	AM: CB:	1 mg cm ⁻²	Particle size: \leq 74 µm Particle size: 10		27		
14	/Na-ion battery	$CMC = 64 \cdot 21 \cdot 15$	(AM: 0.64 mg cm ⁻ 2)	nm	10–15 µm	37		
	anodes	01.21.10	,	Particle size: 20 nm				
15	Rod-like Sb–C composite as anodes for Li-/ Na- ion batteries	AM: CB: PVDF = 70: 20: 10	3 mg cm ⁻² (AM: 2 mg cm ⁻²)	Secondary micro- rods: 6 µm in length, 2 µm in diameter Primary nanoparticles size: 200 nm	≈ 40 µm	38		

Cohort III: Varying conductive additive Mf

Row No.	Electrode	Electrode composition	Mass loading (M _{Total} /A and M _{AM} /A)	Particle size, morphology or density	Electrode thickness	Ref.	
		Li4Ti5O12 (1	$C = 175 \text{ mA g}^{-1}$				
1	LTO/SWCNT composites (Coelho <i>et al.</i>)	Different mass fractions of CNTs	AM: 0.2 mg cm ⁻²	Particle size: 174 nm	1.1 µm	39	
		Ν	IoS ₂				
2	MoS ₂ intercalated p- Ti ₃ C ₂ anode (Zheng <i>et al.</i>)	AM: AB: PVDF = 80: 10: 10	Unknown	Unknown	Unknown	40	
		MWCNT (1	$C = 400 \text{ mA g}^{-1}$				
3	CuNW-MWCNT composite anodes (Yin <i>et al.</i>)	CuNW:MWCNT = 1:1, 3:1, 5:1, and 7:1, w/w	CNT: 1.46 mg cm ⁻²	CuNW with D $\approx 100 \text{ nm}$ CNT with D = 10 nm	61–126 μm	41	
	NaTi ₂ (PO ₄) ₃ (1C = 133 mA g ⁻¹)						
4	CNT decorated NaTi ₂ (PO ₄) ₃ /C nanocomposite for Na-ion battery anode (Wang <i>et al.</i>)	AM: AB: PVDF = 80: 10: 10	2 mg cm ⁻² (AM: 1.6 mg cm ⁻²)	Particle size: < 100 nm	Unknown	42	
		SnS ₂	/MXene				
5	2D MXene/SnS ₂ composites for Na- ion battery anode (Wu <i>et al.</i>)	AM: AB: CMC = 80: 10: 10 (AM: MX/SnS ₂ = 5/1, 10/1 and 2/1)	Unknown	SnS ₂ size: 20– 25 nm	Unknown	43	
		GaS (1C =	1107 mA g ⁻¹)				
6	2D Gallium Chalcogenide Nanosheet/CNT composites (Zhang <i>et al.</i>)	Different mass fractions of CNTs (SWCNT : 5%, 10%, 20%, 30%, and 50%)	2 mg cm ⁻²	GaS NS size: 338 nm	5 µm	23	

Supplementary Table 5. Literature details for Cohort III

		NaCrO2 (10 Theoretical de	$C = 110 \text{ mA g}^{-1}$ ensity: 4.36 g cm ⁻¹	3			
7	Layered O ₃ -type carbon-coated NaCrO ₂ cathode for Na-ion battery (Yu <i>et al.</i>)	AM: KS-6: Super P: PVDF = 85: 3.75: 3.75: 7.5 All samples with x wt% carbon coating (0 <x<16.6%)+7.5 % (KS-6+superP)</x<16.6%)+7.5 	4.1 mg cm ⁻² (AM: 3.5 mg cm ⁻²)	particle size: ≈ 500 nm	≈ 20 µm	31	
		Li4Ti5O12 (10	$C = 175 \text{ mA g}^{-1}$				
8	Li4Ti5O12/Graphene anodes for Li-ion batteries	PVDF=10 wt% (fixed) Graphene contents varying from 0 to 10 wt%	Unknown	LTO rods: 1–2 µm length GNS thickness: ≈ 4.5 nm GNS diameter: ≈ 46 mm	Unknown	44	
	$LiCoO_2 (1C = 140 \text{ mA g}^{-1})$						
9	LiCoO2/Graphene/Su per P based Li-ion batteries	Different contents of graphene nanosheet (GN) together with Super-P (SP). No information about binder	Electrode: 10 mg cm ⁻²	LCO particle size: 5–10 μm	≈ 50 µm	45	
		LiFePO ₄ (10	$C = 170 \text{ mA g}^{-1}$				
10	LiFePO4/Graphene cathode for Li-ion batteries	1% GN + 9% SP. No information about binder	Unknown	LiFePO ₄ microparticle: 400–600 nm Single-layer + multi-layer GNS (3–15 layer) GN1: 1–2 µm; GN2: 3–5 µm; GN3: 10–15 µm;	Unknown	46	
		NMC111 (10	$C = 155 \text{ mA g}^{-1}$				
11	NMC/graphite/CB cathode for Li-ion batteries	AM: CB: PVDF = 92: 4: 4	Unknown	NMC111: 8.9 µm. Carbon black (Super C65): 35 nm.	Unknown	47	

	Parameters	Values	Details	Ref.
σ_{E}	Out-of-plane electrode conductivity	10 S m ⁻¹	High enough to remove resistance limitation in the electrode	This work
σ_{BL}	Bulk liquid conductivity of electrolyte	0.5 S m ⁻¹	Midpoint of the literature values $(\sigma_{BL} = 0.1 - 1 \text{ S m}^{-1})$	48
P_E	Porosity of electrode	0.5 (50 %)	Typical value from references $(P_E = 0.3 - 0.6)$	2,20,22
P_S	Porosity of separator	0.4 (40 %)	Typical porosity of the standard Celgard separator ($P_S = 0.35-0.45$)	49
L _E	Battery electrode thickness	120 µm	Typical value for electrode in commercial battery. $(L_E = 100-150 \ \mu m)$	20
L_S	Battery separator thickness	25 µm	Thickness of the standard Celgard separator	52
L _{AM}	Active material thickness	100 nm	Equivalent to particle diameter of 600 nm	50
$C_{V,eff}$	Effective volumetric capacitance associated with battery electrode	2×10 ⁴ F cm ⁻³	Roughly in midpoint of the range found from our model $(C_{V,eff} = 10^3 - 10^5 \mathrm{F cm^{-3}})$	This work
D_{BL}	Bulk liquid diffusion coefficient of electrolyte	$3 \times 10^{-10} \text{ m}^2 \text{ s}^{-1}$	Midpoint of the literature values $(D_{BL} = 1-5 \times 10^{-10} \text{ m}^2 \text{ s}^{-1})$	51-53
D _{AM}	Li ion diffusion coefficient in the solid active material	$10^{-16} \mathrm{m}^2 \mathrm{s}^{-1}$	Typical value from reference.	54
t _c	Characteristic time associated with electrochemical reaction at the electrode/electrolyte interface	25 s	Within the range of literature values	50

Supplementary Table 6. Details of electrode parameters in Figure 6.

Supplementary Notes

Supplementary Note 1. Deriving the equation for characteristic time

This parameter is a measure of R_T so is likely to be controlled by physical properties of the electrode. This data outlined above implies that τ has both resistance and diffusive contributions. In addition, we must include the effects of the kinetics of the electrochemical reaction at the electrode/electrolyte interface. This can be done *via* the characteristic time associated with the reaction, t_c , which is primarily controlled by the exchange current density *via* the Butler-Volmer equation.⁵⁰ This characteristic time can range from ~0.1 to >100 s, depending on the circumstances.⁵⁰

Then, τ is the sum of the three contributing factors:

$$\tau = \tau_{Electrical} + \tau_{Diffusive} + t_c \tag{5A}$$

It is likely that that the diffusive component is just the sum of diffusion times associated with *cation* transport in the electrolyte, both within the separator (coefficient D_S) and the electrolyte-filled pores within the electrode (coefficient D_P) as well as in the solid active material (coefficient D_{AM}).⁵⁰ These times can be estimated using $L = \sqrt{Dt}$ such that

$$\tau_{Diffusive} = \frac{L_E^2}{D_P} + \frac{L_S^2}{D_S} + \frac{L_{AM}^2}{D_{AM}}$$
(5B)

where L_E , L_S and L_{AM} are the electrode thickness, separator thickness and the length scale associated with active material particles respectively. We note that the value of L_{AM} depends on material geometry. For a thin film of active material, L_{AM} is the film thickness while for a quasi-spherical particle of radius r,⁵⁰ $L_{AM}=r/3$.

For the electrical contribution, we note that every battery electrode has an associated *capacitance*⁵⁵ which limits the rate at which the electrode can be charged/discharged. This effective capacitance, C_{eff} , will be dominated by charge storage but may also have contributions due to surface or polarisation effects.⁵⁵ Then, we propose $\tau_{Electrical}$ to be the RC time constant associated with the circuit. The total resistance related to the charge/discharge process is the sum of the resistances due to out-of-plane electron transport in the electrode material $(R_{E,E})$, as well as ion transport, both in the electrolyte-filled pores of the electrode $(R_{I,P})$ and in the separator respectively $(R_{I,S})$. Then, the RC contribution to τ is given by

$$\tau_{Electrical} = C_{eff} \left(R_{E,E} + R_{I,P} + R_{I,S} \right) \tag{5C}$$

The overall characteristic time associated with charge/discharge is then the sum of capacitive and diffusive components and t_c :

$$\tau = C_{eff} \left(R_{E,E} + R_{I,P} + R_{I,S} \right) + \frac{L_E^2}{D_P} + \frac{L_S^2}{D_S} + \frac{L_{AM}^2}{D_{AM}} + t_c$$
(5D)

In porous structures, only a fraction of the total volume is available for transport, thus reducing the diffusion coefficient relative to that in the bulk liquid (D_{BL}). This is dealt with *via* the Bruggeman equation which says: $D_{porous} = D_{BL}P/\tau$ where P is porosity and tau is tortuosity. This is usually simplified *via* the approximation $\tau = P^{-1/2}$ so $D_{porous} = D_{BL}P^{3/2}$ We apply this approach to relate the diffusion coefficients of ions in the separator and porous electrode (D_S and D_P) to that in bulk liquid: $D_p = D_{BL}P_E^{3/2}$ and $D_S = D_{Bulk}P_S^{3/2}$. Here, P_E and P_S represent the porosity of the electrode and separator respectively.

We can generalise this approach to apply to ionic conductivity because the Nearnst-Einstein predicts a linear relationship between ionic conductivity and the diffusion coefficient. Then,

we can write the resistances as
$$R_{E,M} = \frac{L_E/2}{\sigma_E A}$$
, $R_{I,P} = \frac{L_E/2}{\sigma_{BL} P_E^{3/2} A}$ and $R_{I,S} = \frac{L_S}{\sigma_{BL} P_S^{3/2} A}$, where

 σ_{BL} is the conductivity of the bulk liquid electrolyte and A is the area of both the electrode and separator. The factor of 2 comes from that fact that, on average, ions from the electrolyte and electrons from the current collector meet at the midpoint of the electrode. Combining these expressions then gives

$$\tau = \frac{C_{eff}}{A} \left[\frac{L_E}{2\sigma_E} + \frac{L_E}{2\sigma_{BL} P_E^{3/2}} + \frac{L_S}{\sigma_{BL} P_S^{3/2}} \right] + \frac{L_E^2}{D_{BL} P_E^{3/2}} + \frac{L_L^2}{D_{BL} P_S^{3/2}} + \frac{L_S^2}{D_S} + t_S^2$$

The effective capacitance of the electrode probably scales with electrode thickness (constant volumetric capacitance, $C_{eff} / AL_E = C_{V.eff}$) so

$$\tau = C_{V,eff} \left[\frac{L_E^2}{2\sigma_E} + \frac{L_E^2}{2\sigma_{BL} P_E^{3/2}} + \frac{L_E L_S}{\sigma_{BL} P_S^{3/2}} \right] + \frac{L_E^2}{D_{BL} P_E^{3/2}} + \frac{L_S^2}{D_{BL} P_S^{3/2}} + \frac{L_{AM}^2}{D_{AM}} + t_C$$

Which can be rearranged as

$$\tau = L_E^2 \left[\frac{C_{V,eff}}{2\sigma_E} + \frac{C_{V,eff}}{2\sigma_{BL} P_E^{3/2}} + \frac{1}{D_{BL} P_E^{3/2}} \right] + L_E \left[\frac{L_S C_{V,eff}}{\sigma_{BL} P_S^{3/2}} \right] + \left[\frac{L_S^2}{D_{BL} P_S^{3/2}} + \frac{L_{AM}^2}{D_{AM}} \right] + t_c$$

Or alternatively, keeping electrical and diffusive terms together and writing as Θ :

$$\Theta^{-1} = \frac{\tau}{L_E^2} = C_{V,eff} \left[\frac{1}{2\sigma_E} + \frac{1}{2\sigma_{BL} P_E^{3/2}} + \frac{L_S / L_E}{\sigma_{BL} P_S^{3/2}} \right] + \left[\frac{1}{D_{BL} P_E^{3/2}} + \frac{L_S^2 / L_E^2}{D_{BL} P_S^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{BL} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{BL} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{BL} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{BL} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{BL} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{AM} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM} P_E^{3/2}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{AM} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM} P_E^{3/2}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{AM} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM} P_E^{3/2}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{AM} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM} P_E^{3/2}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{AM} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM} P_E^{3/2}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{AM} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM} P_E^{3/2}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{AM} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM} P_E^{3/2}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{AM} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM} P_E^{3/2}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{AM} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM} P_E^{3/2}} \right] + \frac{t_c}{L_E^2} \left[\frac{1}{D_{AM} P_E^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM} P_E^{3/2}} \right]$$

Supplementary Note 2. Calculating Percolation Parameters

The data in figure 3E is described by

$$\tau / L_E^2 = \frac{C_{V,eff} / 2}{\sigma_M + \sigma_0 (M_f)^s} + \beta_1$$

For fitting purposes, this can be written as

$$\tau / L_{E}^{2} = \frac{(C_{eff} / V) / 2\sigma_{M}}{1 + (\sigma_{0} / \sigma_{M})(M_{f})^{s}} + \beta_{f}$$

From the fits in figure 3E and figure 5A, we obtain the parameters $(C_{eff} / V) / 2\sigma_M$, σ_0 / σ_M , s and β_1 as shown in table 1. The mean volumetric capacity, Q_V , can be found by multiplying Q_M by the electrode density which can usually be extracted/estimated from data in papers. The effective volumetric capacitance was found from $C_{V,eff} = 28 \times \rho_E C_M$ (figure 4F). This parameter can be combined with the fit parameters to yield σ_M and σ_0 (Supplementary Table 1).

The percolation exponents found ranged from 1.4 to 3.5 in good agreement with the fact that in the literature, such exponents usually fall in the range 1.4<s<4.56 The $\sigma_{\scriptscriptstyle M}$ parameter is a measure of the out-of-plane conductivity of the electrode in the absence of conductive additive. This parameter should be quite small, usually <<1 S m⁻¹ as is found below. We note that the Yu paper has a higher value of $\sigma_M = 0.18$ S m⁻¹. This is as expected because the active particles making up the electrode were coated with a conductive carbon coating yielding some conductivity even in the absence of additional filler. The parameter σ_0 is roughly a measure of the out-of-plane conductivity of a network containing only the filler particles which we expect to be ~1000x lower than the in plane conductivity. σ_0 can be quite high, perhaps reaching ~10⁶ S m⁻¹ for graphite.⁵⁷ Thus, the value obtained for Yu et al appears plausible while the value obtained from B Zhang's paper is reasonably consistent with their in-plane conductivity which implies a value of σ_0 somewhat larger than 10⁶ S m⁻¹. Notable, the values of σ_0 found for J Zhang and J Coelho's work are very low. These papers describe electrodes with carbon nanotubes added to increase conductivity. One might expect NTs to give very good conductivity enhancements and so large values of σ_0 . However, in composites prepared by liquid processing, nanotube tend to become aligned in-plane. This can give very low out-ofplane conductivities. For example, we previously reported and out-of-plane σ_0 value of 4 S m⁻¹ for a composite of single walled nanotubes mixed with Co(OH)₂ nanosheets.⁵⁸ This data implies that nanotubes may not be as good at enhancing rate as may have been thought.

Supplementary Note 3. Main text Fig 5 Calculations

Figure 5B

Bauer et al: Characteristic time versus porosity.

Equation:
$$\frac{\tau}{L_{E}^{2}} = \left[\frac{C_{V,eff}}{2\sigma_{BL}} + \frac{1}{D_{BL}}\right] P_{E}^{-3/2} + \beta_{2}$$

Fit equation: $\frac{\tau}{L_{E}^{2}} = 1.27 e^{10*P^{-3/2}} + (-3/2) + 9.8e^{30}$

From the fit, the square-bracketed term= 1.27×10^{10} s m⁻². Personal communication from the author showed the electrodes to have L_E=62 and 77 µm for the low- and high-P samples respectively. The volumetric capacities (Q_V) were ~3×10⁸ mAh m⁻³. Using the relationship in figure 4F ($C_{V,eff} = 28 \times Q_V$) gives $C_{V,eff} = 8.4 \times 10^9$ F m⁻³. Then approximating $D_{BL} \approx 3 \times 10^{-10}$ m² s⁻¹ yields $\sigma_{BL}=0.45$ S m⁻¹. As typical electrolytes used in LiBs (c=1 M) typically have $\sigma_{BL}\sim 0.5-1$ S m⁻¹, this is as expected.

Figure 5C

Yu et al: Characteristic time versus electrolyte concentration

Equation:
$$\frac{\tau}{L_E^2} = \left[\frac{C_{V,eff}}{2\sigma_E} + \frac{1}{D_{BL}P_E^{3/2}}\right] + \frac{t^+RT}{F^2D_{BL}c} \left[\frac{C_{V,eff}}{2P_E^{3/2}} + \frac{L_S}{L_E}\frac{C_{V,eff}}{P_S^{3/2}}\right]$$

Fit equation; $\frac{\tau}{L_E^2} = 1.6e_{10} + 9.1e_{13}/c$ (c in mol m⁻³)

The volumetric capacities were ~ 3.6×10^8 mAh m⁻³. Using the relationship in figure 4F ($C_{V,eff} = 28 \times Q_V$) gives $C_{V,eff} = 10.1 \times 10^9$ F m⁻³.

Then approximating $t^+\approx 1$, $P_s\approx 0.4$, $P_E\sim 0.4$ (estimated from paper=1-(2.2 g cc⁻¹)/(3.6 g cc⁻¹)) and taking $D_{BL}\approx 10^{-10}$ m² s⁻¹ and using the slope yields $L_s / L_E = 0.35$. Assuming, $L_s = 25$ µm, yields $L_E = 71$ µm, close to the quoted value of 65 µm.

Figure 5D

This work: Characteristic time versus electrolyte (separator) thickness.

Equation:
$$\frac{\tau}{L_E^2} = L_S \left[\frac{C_{V,eff}}{L_E \sigma_{BL} P_S^{3/2}} \right] + \beta_3$$

Fit: 2.04e10+2.71e14*Ls

The volumetric capacities were ~ 3.3×10^8 mAh m⁻³. Using the relationship in figure 4F ($C_{V,eff} = 28 \times Q_V$) gives $C_{V,eff} = 9.2 \times 10^9$ F m⁻³.

Then approximating $D_{BL} \approx 3 \times 10^{-10} \text{ m}^2 \text{ s}^{-1}$ and $P_S \sim 0.4$ and taking the measured value of $L_E=245$ µm gives $\sigma_{BL} \sim 0.6 \text{ S m}^{-1}$.

Figure 5E

Ye *et al*: characteristic time versus thickness of thin active layer in porous current collector (large pores)

Equation:
$$\tau = \frac{L_{AM}^2}{D_{AM}} + \beta_4$$

From the fit $1/D_{AM}=3.02\times10^{18}$ s m⁻² yielding $D_{AM}=3.3\times10^{-19}$ m² s⁻¹.

Supplementary Methods

<u>Electrode fabrication and electrochemical characterization performed in this work</u>

As shown in figure 4 and 5D (main text), some electrodes were prepared and tested in this work. All such electrodes were prepared by a conventional slurry casting method using a CNT solution (Tuball, OCSiAl, 0.2 wt% SWCNT in water with ~0.2 wt% PVP as a surfactant) with various battery active materials (AM). Here we employed nano-LTO (~200 nm, Aldrich), micro-sized silicon (1–3 μ m, US Research Nanomaterials), and graphene wrapped silicon (Si/Gr, Nano GCA-2000, Angstron Materials) for anodes, and NMC (NMC811, ~10 μ m, Lifun Tech) for cathodes, respectively. The AM powers were directly mixed with the CNT solution and ground by a mortar and pestle to obtain a uniform slurry. The CNT contents and electrode compositions were controlled by changing the mixing ratio between CNT solution to fabricate 0.5 wt% CNT-AM electrode. Then the slurry was cast onto either Al or Cu foil using a doctor blade. The electrode thickness was also controlled by the slurry coating thickness with changing the height of the doctor blade. Then the slurry cast electrodes were slowly dried at 40 °C for 2 hours and followed by vacuum drying at 100 °C for 12 hours to remove residual water.

The electrochemical properties of the electrodes were measured in 2032-type coin cells (MTI Corp.) with a half-cell configuration. All coin cells were assembled in an Ar-filled glovebox (UNIIab Pro, Mbraun). The dried electrodes were cut into 12 mm diameter discs (area = 1.13 cm²) and paired with Li metal discs (diameter= 16 mm). Celgard 2032 (thickness = 25 μ m) was used as a separator. To investigate the effect of separator thickness, we also varied the number of stacked separators (1–3 stacks, thickness varying from 25–75 μ m). The electrolyte was 1–1.2 M LiPF₆ dissolved in EC/DEC/FEC (3:6:1 in v/v/v, BASF) with 2 wt% vinylene carbonate. The rate-capabilities were evaluated by galvanostatic charge-discharge (GCD) test at a potentiostat (VMP3, Biologic). The voltage range was 0.005–1.2 V, 1–2.5 V and 3–4.3 V for Si, LTO, and NMC electrodes, respectively.

Capacity-rate analysis in this work

Note on fitting

All the fitting analysis has been performed by Origin software (here we used Origin version 2015-2018) using "Nonlinear Curve Fit" function, according to the model equation.

Although it seems obvious that the best way to fit data is to plot $Q/M \vee R$ and use $\frac{Q}{M} = Q_M \left[1 - (R\tau)^n \left(1 - e^{-(R\tau)^{-n}} \right) \right]$ to fit, this is not the case. The reason is that in some cases, the Q/M data can span a wide range. Then the least squares fitting routine is biased toward the larger values of Q/M leading to poor fits at high R.

To avoid this, we plotted the data as $\log(Q/M)$ vs. R and fitted using $\log(Q/M) = \log \left\{ Q_M \left[1 - (R\tau)^n \left(1 - e^{-(R\tau)^{-n}} \right) \right] \right\}$

The resultant smaller range of y-values results in much better fitting.

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