Supplementary Information for

Quantifying the factors limiting rate-performance in battery electrodes

Ruiyuan Tian *et al.*

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Supplementary Tables

	$(C_{\text{eff}}/V)/\sigma_M$	σ_{0}/σ_{M}	S	β_{1}	Q_V	$C_{V,eff}$	$\sigma_{\scriptscriptstyle M}$	σ_{0}
units	s m^{-2}	$\qquad \qquad -$		$\rm s~m^{-2}$	$mAh m-3$	$F m^{-3}$	$S \, \text{m}^{-1}$	$S \, \text{m}^{-1}$
J Zhang	2.7×10^{14}	1060	3	2×10^9	2.0×10^{9}	5.6×10^{10}	1.0×10^{-4}	0.11
J Coelho	10^{15}	4000	1.4	2×10^9	2.8×10^8	7.8×10^{9}	3.9×10^{-6}	1.6×10^{-2}
B Zhang	5.5×10^{13}	4×10^6	3.5	2.2×10^{12}	5.3×10^{8}	1.5×10^{10}	1.3×10^{-4}	5.4×10^{2}
Yu	3.3×10^{11}	1.2×10^{6}	2.7	2.3×10^{9}	4.8×10^{8}	1.3×10^{10}	2.0×10^{-2}	2.5×10^{4}

Supplementary Table 1. Physical percolation properties from references (figure 3 main text).

Cohort I: Lithium ion batteries

Supplementary Table 3. Literature details for Cohort IB (data sets with varying electrode thickness)

Cohort Ⅱ**: Sodium ion batteries**

Supplementary Table 4. Literature details for Cohort II (Na-ion batteries)

Cohort Ш: Varying conductive additive Mf

Supplementary Table 5. Literature details for Cohort Ш

Supplementary Table 6. Details of electrode parameters in Figure 6.

Supplementary Notes

Supplementary Note 1. Deriving the equation for characteristic time

This parameter is a measure of R_T so is likely to be controlled by physical properties of the electrode. This data outlined above implies that τ has both resistance and diffusive contributions. In addition, we must include the effects of the kinetics of the electrochemical reaction at the electrode/electrolyte interface. This can be done *via* the characteristic time associated with the reaction, *tc*, which is primarily controlled by the exchange current density *via* the Butler-Volmer equation.⁵⁰ This characteristic time can range from ~ 0.1 to >100 s, depending on the circumstances.⁵⁰

Then, τ is the sum of the three contributing factors:

$$
\tau = \tau_{Electrical} + \tau_{Diffusive} + t_c \tag{5A}
$$

It is likely that that the diffusive component is just the sum of diffusion times associated with *cation* transport in the electrolyte, both within the separator (coefficient D_S) and the electrolytefilled pores within the electrode (coefficient D_P) as well as in the solid active material (coefficient D_{AM}).⁵⁰ These times can be estimated using $L = \sqrt{Dt}$ such that

$$
\tau_{Diffusive} = \frac{L_E^2}{D_P} + \frac{L_S^2}{D_S} + \frac{L_{AM}^2}{D_{AM}}
$$
\n(5B)

where *LE*, *L^S* and *LAM* are the electrode thickness, separator thickness and the length scale associated with active material particles respectively. We note that the value of *LAM* depends on material geometry. For a thin film of active material, *LAM* is the film thickness while for a quasi-spherical particle of radius *r*, ⁵⁰ *LAM*=*r*/3.

For the electrical contribution, we note that every battery electrode has an associated *capacitance*⁵⁵ which limits the rate at which the electrode can be charged/discharged. This effective capacitance, *Ceff*, will be dominated by charge storage but may also have contributions due to surface or polarisation effects.⁵⁵ Then, we propose $\tau_{Electrical}$ to be the RC time constant associated with the circuit. The total resistance related to the charge/discharge process is the sum of the resistances due to out-of-plane electron transport in the electrode material $(R_{E,E})$, as well as ion transport, both in the electrolyte-filled pores of the electrode $(R_{I,P})$ and in the separator respectively (R_{IS}) . Then, the RC contribution to τ is given by

$$
\tau_{Electrical} = C_{\text{eff}} (R_{E,E} + R_{I,P} + R_{I,S})
$$
\n(5C)

The overall characteristic time associated with charge/discharge is then the sum of capacitive and diffusive components and *tc*:

$$
\tau = C_{eff} (R_{E,E} + R_{I,P} + R_{I,S}) + \frac{L_E^2}{D_P} + \frac{L_S^2}{D_S} + \frac{L_{AM}^2}{D_{AM}} + t_c
$$
\n(5D)

In porous structures, only a fraction of the total volume is available for transport, thus reducing the diffusion coefficient relative to that in the bulk liquid (D_{BL}). This is dealt with *via* the Bruggeman equation which says: $D_{\text{porous}} = D_{BL}P/\tau$ where P is porosity and tau is tortuosity. This is usually simplified *via* the approximation $\tau = P^{-1/2}$ so $D_{p_{\text{orous}}} = D_{\text{BL}} P^{3/2}$ We apply this approach to relate the diffusion coefficients of ions in the separator and porous electrode (D_S) and D_P) to that in bulk liquid: $D_p = D_{BL} P_E^{3/2}$ and $D_s = D_{Bulk} P_S^{3/2}$. Here, P_E and P_S represent the porosity of the electrode and separator respectively.

We can generalise this approach to apply to ionic conductivity because the Nearnst-Einstein predicts a linear relationship between ionic conductivity and the diffusion coefficient. Then,

we can write the resistances as
$$
R_{E,M} = \frac{L_E/2}{\sigma_E A}
$$
, $R_{I,P} = \frac{L_E/2}{\sigma_{BL} P_E^{3/2} A}$ and $R_{I,S} = \frac{L_S}{\sigma_{BL} P_S^{3/2} A}$, where

 σ_{BL} is the conductivity of the bulk liquid electrolyte and A is the area of both the electrode and separator. The factor of 2 comes from that fact that, on average, ions from the electrolyte and electrons from the current collector meet at the midpoint of the electrode. Combining these expressions then gives ons then gives
 $\left[\frac{L_E}{2} + \frac{L_E}{2} + \frac{L_S}{2} + \frac{L_S}{2} + \frac{L_E^2}{2} + \$

expressions then gives
\n
$$
\tau = \frac{C_{\text{eff}}}{A} \left[\frac{L_{E}}{2\sigma_{E}} + \frac{L_{E}}{2\sigma_{BL} P_{E}^{3/2}} + \frac{L_{S}}{\sigma_{BL} P_{S}^{3/2}} \right] + \frac{L_{E}^{2}}{D_{BL} P_{E}^{3/2}} + \frac{L_{L}^{2}}{D_{BL} P_{S}^{3/2}} + \frac{L_{S}^{2}}{D_{S}} + t_{c}
$$

The effective capacitance of the electrode probably scales with electrode thickness (constant volumetric capacitance, $C_{eff} / AL_E = C_{V, eff}$) so
 $C = \begin{bmatrix} L_F^2 & L_F^2 & L_F L_S \end{bmatrix}$ L_F^2 L_F^2 L_F^2 explanance of the exercise process, b

capacitance, $C_{\text{eff}}/AL_E = C_{V,\text{eff}}$) so
 $\left[\frac{L_E^2}{2} + \frac{L_E^2}{2} + \frac{L_E L_S}{2} \right] + \frac{L_E^2}{2}$

volumetric capacitance,
$$
C_{\text{eff}} / AL_E = C_{V,\text{eff}}
$$
) so

\n
$$
\tau = C_{V,\text{eff}} \left[\frac{L_E^2}{2\sigma_E} + \frac{L_E^2}{2\sigma_{BL} P_E^{3/2}} + \frac{L_E L_S}{\sigma_{BL} P_S^{3/2}} \right] + \frac{L_E^2}{D_{BL} P_E^{3/2}} + \frac{L_S^2}{D_{BL} P_S^{3/2}} + \frac{L_{AM}^2}{D_{AM}} + t_c
$$

Which can be rearranged as
\n
$$
\tau = L_E^2 \left[\frac{C_{V,eff}}{2\sigma_E} + \frac{C_{V,eff}}{2\sigma_{BL} P_E^{3/2}} + \frac{1}{D_{BL} P_E^{3/2}} \right] + L_E \left[\frac{L_S C_{V,eff}}{\sigma_{BL} P_S^{3/2}} \right] + \left[\frac{L_S^2}{D_{BL} P_S^{3/2}} + \frac{L_{AM}^2}{D_{AM}} \right] + t_c
$$

Or alternatively, keeping electrical and diffusive terms together and writing as
$$
\Theta
$$
:
\n
$$
\Theta^{-1} = \frac{\tau}{L_E^2} = C_{V,eff} \left[\frac{1}{2\sigma_E} + \frac{1}{2\sigma_{BL} P_E^{3/2}} + \frac{L_S / L_E}{\sigma_{BL} P_S^{3/2}} \right] + \left[\frac{1}{D_{BL} P_E^{3/2}} + \frac{L_S^2 / L_E^2}{D_{BL} P_S^{3/2}} + \frac{L_{AM}^2 / L_E^2}{D_{AM}} \right] + \frac{t_c}{L_E^2}
$$

Supplementary Note 2. Calculating Percolation Parameters

The data in figure 3E is described by

$$
\tau/L_E^2 = \frac{C_{V,eff} / 2}{\sigma_M + \sigma_0 (M_f)^s} + \beta_1
$$

For fitting purposes, this can be written as

$$
\tau/L_E^2 = \frac{(C_{\text{eff}}/V)/2\sigma_M}{1+(\sigma_0/\sigma_M)(M_f)^s} + \beta_1
$$

From the fits in figure 3E and figure 5A, we obtain the parameters $(C_{\text{eff}}/V)/2\sigma_M$, σ_0/σ_M , s and β_1 as shown in table 1. The mean volumetric capacity, Q_V , can be found by multiplying *Q^M* by the electrode density which can usually be extracted/estimated from data in papers. The effective volumetric capacitance was found from $C_{V, eff} = 28 \times \rho_E C_M$ (figure 4F). This parameter can be combined with the fit parameters to yield σ_M and σ_0 (Supplementary Table 1).

The percolation exponents found ranged from 1.4 to 3.5 in good agreement with the fact that in the literature, such exponents usually fall in the range $1.4 < s < 4.56$ The σ_M parameter is a measure of the out-of-plane conductivity of the electrode in the absence of conductive additive. This parameter should be quite small, usually $<<1$ S m⁻¹ as is found below. We note that the Yu paper has a higher value of σ_M =0.18 S m⁻¹. This is as expected because the active particles making up the electrode were coated with a conductive carbon coating yielding some conductivity even in the absence of additional filler. The parameter σ_0 is roughly a measure of the out-of-plane conductivity of a network containing only the filler particles which we expect to be ~1000x lower than the in plane conductivity. σ_0 can be quite high, perhaps reaching ~10⁶ S m⁻¹ for graphite.⁵⁷ Thus, the value obtained for Yu *et al* appears plausible while the value obtained from B Zhang's paper is reasonably consistent with their in-plane conductivity which implies a value of σ_0 somewhat larger than 10⁶ S m⁻¹. Notable, the values of σ_0 found for J Zhang and J Coelho's work are very low. These papers describe electrodes with carbon nanotubes added to increase conductivity. One might expect NTs to give very good conductivity enhancements and so large values of σ_0 . However, in composites prepared by liquid processing, nanotube tend to become aligned in-plane. This can give very low out-of-

plane conductivities. For example, we previously reported and out-of-plane σ_0 value of 4 S m ¹ for a composite of single walled nanotubes mixed with $Co(OH)_2$ nanosheets.⁵⁸ This data implies that nanotubes may not be as good at enhancing rate as may have been thought.

Supplementary Note 3. Main text Fig 5 Calculations

Figure 5B

Bauer *et al*: Characteristic time *versus* porosity.

Equation:
$$
\frac{\tau}{L_E^2} = \left[\frac{C_{V,eff}}{2\sigma_{BL}} + \frac{1}{D_{BL}} \right] P_E^{-3/2} + \beta_2
$$

Fit equation:
$$
\frac{\tau}{L_E^2} = 1.27e10^* P^{\wedge} (-3/2) + 9.8e8
$$

From the fit, the square-bracketed term= 1.27×10^{10} s m⁻². Personal communication from the author showed the electrodes to have $L_E=62$ and 77 μ m for the low- and high-P samples respectively. The volumetric capacities (Q_V) were $\sim 3 \times 10^8$ mAh m⁻³. Using the relationship in figure 4F ($C_{V,eff} = 28 \times Q_V$) gives $C_{V,eff} = 8.4 \times 10^9$ F m⁻³. Then approximating $D_{BL} \approx 3 \times 10^{-10}$ m² s^{-1} yields $\sigma_{BL} = 0.45$ S m⁻¹. As typical electrolytes used in LiBs (c=1 M) typically have σ_{BL} ~0.5–1 S m⁻¹, this is as expected.

Figure 5C

Yu *et al*: Characteristic time *versus* electrolyte concentration
Equation:
$$
\frac{\tau}{L_E^2} = \left[\frac{C_{V,eff}}{2\sigma_E} + \frac{1}{D_{BL}P_E^{3/2}} \right] + \frac{t^*RT}{F^2D_{BL}c} \left[\frac{C_{V,eff}}{2P_E^{3/2}} + \frac{L_S}{L_E} \frac{C_{V,eff}}{P_S^{3/2}} \right]
$$
Fit equation;
$$
\frac{\tau}{L_E^2} = 1.6e10 + 9.1e13/c
$$
 (c in mol m⁻³)

The volumetric capacities were $\sim 3.6 \times 10^8$ mAh m⁻³. Using the relationship in figure 4F ($C_{V, \text{eff}} = 28 \times Q_V$) gives $C_{V, \text{eff}} = 10.1 \times 10^9 \text{ F m}^{-3}$.

Then approximating $t^+ \approx 1$, $P_s \approx 0.4$, $P_E \sim 0.4$ (estimated from paper=1-(2.2 g cc⁻¹)/(3.6 g cc⁻¹)) and taking $D_{BL} \approx 10^{-10}$ m² s⁻¹ and using the slope yields $L_s/L_E = 0.35$. Assuming, $L_s = 25 \mu m$, yields $L_E=71$ µm, close to the quoted value of 65 µm.

Figure 5D

This work: Characteristic time *versus* electrolyte (separator) thickness.

Equation:
$$
\frac{\tau}{L_E^2} = L_S \left[\frac{C_{V, \text{eff}}}{L_E \sigma_{BL} P_S^{3/2}} \right] + \beta_3
$$

Fit: 2.04e10+2.71e14*L^S

The volumetric capacities were $\sim 3.3 \times 10^8$ mAh m⁻³. Using the relationship in figure 4F ($C_{V, eff} = 28 \times Q_V$) gives $C_{V, eff} = 9.2 \times 10^9$ F m⁻³.

Then approximating $D_{BL} \approx 3 \times 10^{-10} \text{ m}^2 \text{ s}^{-1}$ and P_S~0.4 and taking the measured value of L_E=245 μ m gives σ_{BL} ~0.6 S m⁻¹.

Figure 5E

Ye *et al*: characteristic time versus thickness of thin active layer in porous current collector (large pores)

Equation:
$$
\tau = \frac{L_{AM}^2}{D_{AM}} + \beta_4
$$

From the fit $1/D_{AM} = 3.02 \times 10^{18}$ s m⁻² yielding $D_{AM} = 3.3 \times 10^{-19}$ m² s⁻¹.

Supplementary Methods

Electrode fabrication and electrochemical characterization performed in this work

As shown in figure 4 and 5D (main text), some electrodes were prepared and tested in this work. All such electrodes were prepared by a conventional slurry casting method using a CNT solution (Tuball, OCSiAl, 0.2 wt% SWCNT in water with ~0.2 wt% PVP as a surfactant) with various battery active materials (AM). Here we employed nano-LTO (~200 nm, Aldrich), micro-sized silicon (1−3 µm, US Research Nanomaterials), and graphene wrapped silicon (Si/Gr, Nano GCA-2000, Angstron Materials) for anodes, and NMC (NMC811, ~10 µm, Lifun Tech) for cathodes, respectively. The AM powers were directly mixed with the CNT solution and ground by a mortar and pestle to obtain a uniform slurry. The CNT contents and electrode compositions were controlled by changing the mixing ratio between CNT solution and AM power. For instance, 1 g of AM powder was mixed with 2.5 ml of CNT solution to fabricate 0.5 wt% CNT-AM electrode. Then the slurry was cast onto either Al or Cu foil using a doctor blade. The electrode thickness was also controlled by the slurry coating thickness with changing the height of the doctor blade. Then the slurry cast electrodes were slowly dried at 40 °C for 2 hours and followed by vacuum drying at 100 °C for 12 hours to remove residual water.

The electrochemical properties of the electrodes were measured in 2032-type coin cells (MTI Corp.) with a half-cell configuration. All coin cells were assembled in an Ar-filled glovebox (UNIlab Pro, Mbraun). The dried electrodes were cut into 12 mm diameter discs (area = 1.13 cm²) and paired with Li metal discs (diameter= 16 mm). Celgard 2032 (thickness = $25 \mu m$) was used as a separator. To investigate the effect of separator thickness, we also varied the number of stacked separators (1−3 stacks, thickness varying from 25−75 µm). The electrolyte was 1–1.2 M LiPF₆ dissolved in EC/DEC/FEC (3:6:1 in v/v/v, BASF) with 2 wt% vinylene carbonate. The rate-capabilities were evaluated by galvanostatic charge-discharge (GCD) test at a potentiostat (VMP3, Biologic). The voltage range was 0.005−1.2 V, 1−2.5 V and 3−4.3 V for Si, LTO, and NMC electrodes, respectively.

Capacity-rate analysis in this work

Note on fitting

All the fitting analysis has been performed by Origin software (here we used Origin version 2015-2018) using "Nonlinear Curve Fit" function, according to the model equation.

Although it seems obvious that the best way to fit data is to plot *Q/M* v *R* and use $\left[1 - (R\tau)^n \left(1 - e^{-(R\tau)^{-n}}\right)\right]$ $\int_M \left[1 - (R\tau)^n \left(1 - e^{-(R\tau)^{-n}}\right)\right]$ $\frac{Q}{M} = Q_M \left[1 - (R\tau)^n \left(1 - e^{-(R\tau)} \right) \right]$ = Q_M $\left[1 - (R\tau)^n \left(1 - e^{-(R\tau)^{-n}}\right)\right]$ to f to fit, this is not the case. The reason is that in some cases, the *Q*/*M* data can span a wide range. Then the least squares fitting routine is biased toward the larger values of *Q/M* leading to poor fits at high *R*.

To avoid this, we plotted the data as log(*Q/M*) *vs*. *R* and fitted using $\log(Q/M) = \log \left\{ Q_M \left[1 - (R\tau)^n \left(1 - e^{-(R\tau)^{-n}} \right) \right] \right\}$ *n* avoid this, we plotted the
 $Q/M = \log \left\{ Q_M \left[1 - (R\tau)^n \left(1 - e^{- (R\tau)^n} \right) \right] \right\}$ $(r^{n})^{n} (1 - e^{-(R\tau)})$ this, we plotted the data as
= $\log \left\{ Q_M \left[1 - (R\tau)^n \left(1 - e^{-(R\tau)^{-n}} \right) \right] \right\}$

The resultant smaller range of y-values results in much better fitting.

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