

# Supporting Information: Mixed-Matrix Membranes Formed from Imide-Functionalized UiO-66-NH<sub>2</sub> for Improved Interfacial Compatibility

*Qihui Qian, Albert X. Wu, Won Seok Chi, Patrick A. Asinger, Sharon Lin, Asia Hypsher and  
Zachary P. Smith\**

\* Email address: zpsmith@mit.edu

Department of Chemical Engineering, Massachusetts Institute of Technology, Cambridge, MA  
02139, United States

**Section A: Supporting characterization results for the Pure MOF and PSM-MOF**

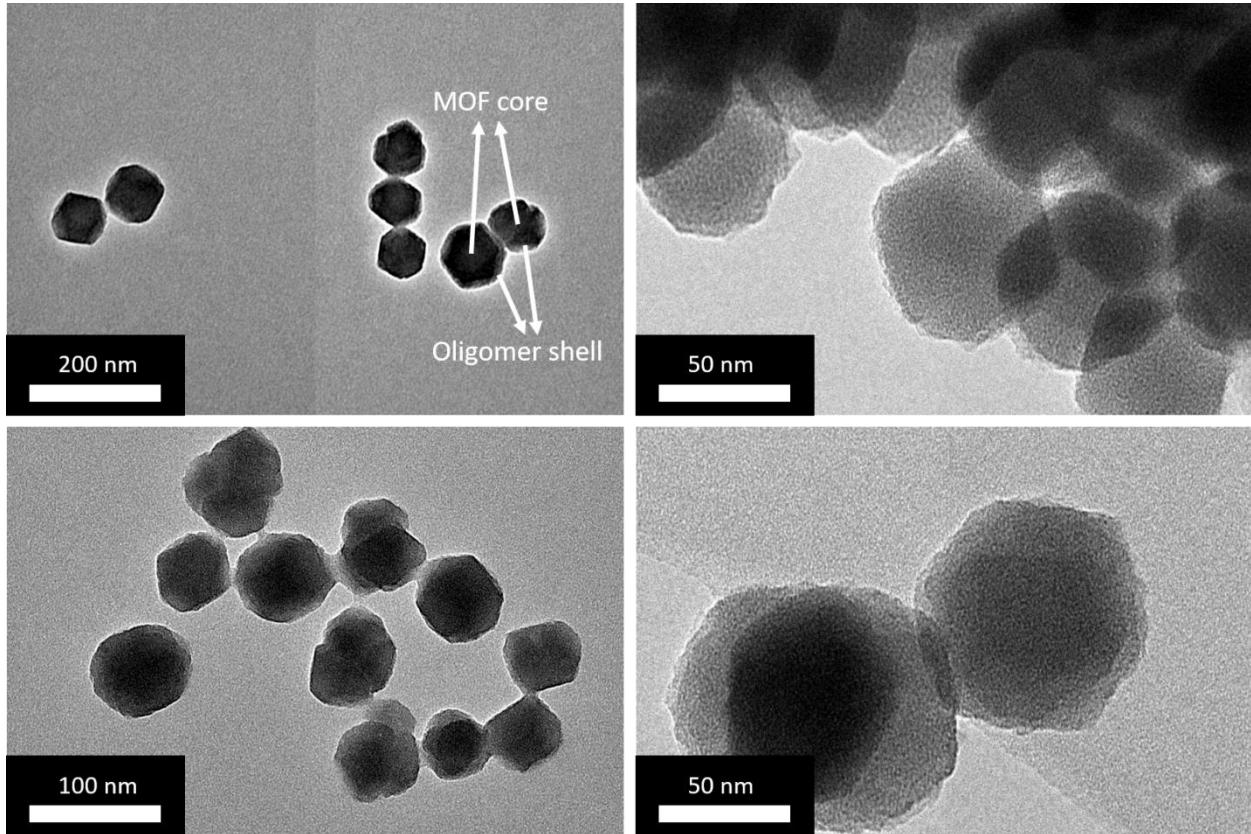


Figure S1. TEM images of oligomer-coated  $\text{UiO-66-NH}_2$  under different magnifications. MOF core and oligomer shell are labeled in the left top image. Different surface structures can be observed between these PSM-MOF structures and the pure-MOF structures, as shown in Figure 2.

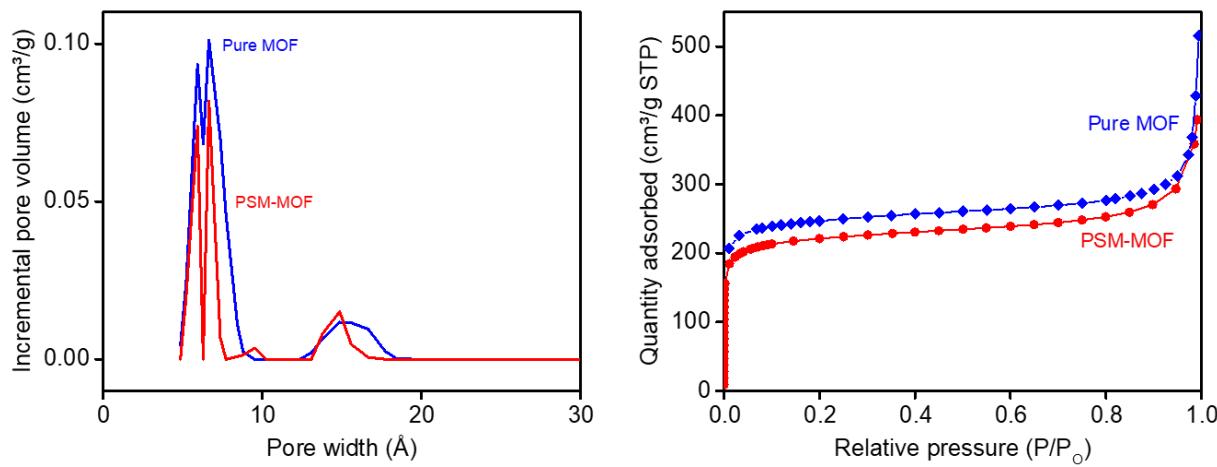


Figure S2. Pore size distribution and N<sub>2</sub> adsorption isotherms for Pure MOF and PSM-MOF. Pore size distribution was calculated using the built-in function of Micromeritics 3Flex Share software based on N<sub>2</sub>@Tarazona NLDFT Model.

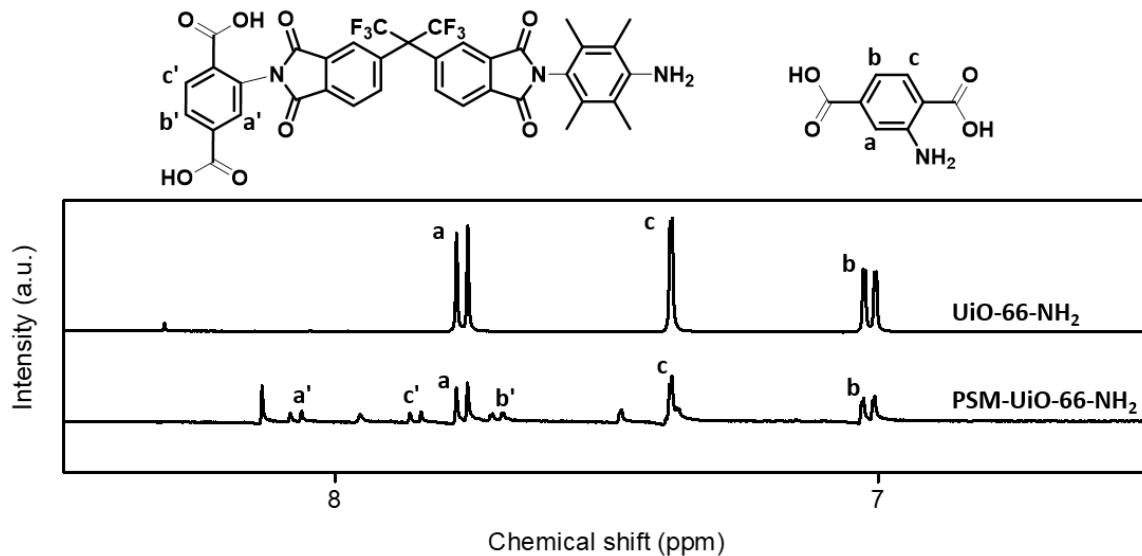


Figure S3. <sup>1</sup>H NMR spectra change upon 6FDA-Durene oligomer PSM of UiO-66-NH<sub>2</sub>. Peaks were assigned according to the literature<sup>10</sup>. Unassigned peaks may result from coupling and exchange effects from HF and 6FDA-Durene oligomer.

## Section B: Supporting characterization results for the MMMs and upper bound plots

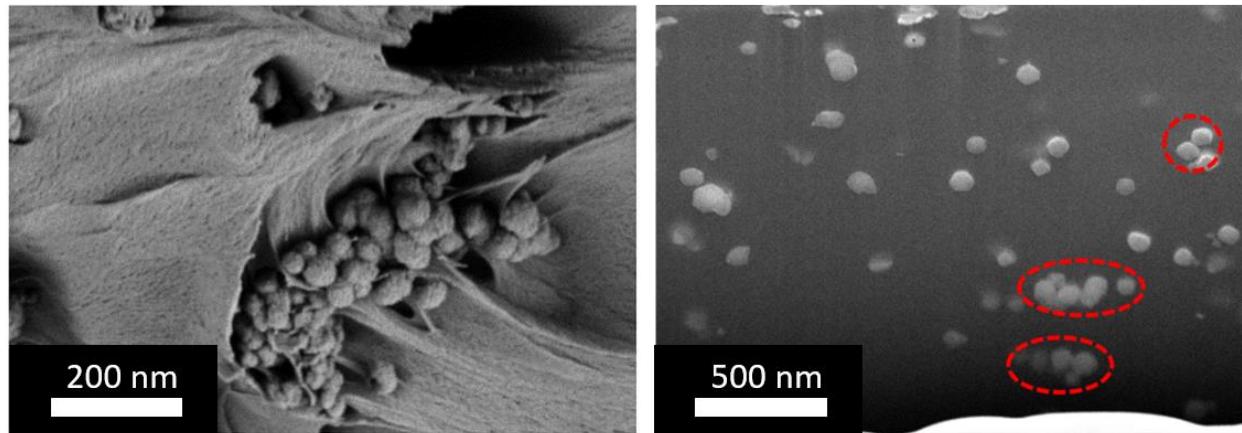


Figure S4. Cross-sectional FESEM (left) and FIB-SEM (right) images of 10% Pure MOF MMM. Both images show more serious particle aggregation than for the PSM-MOF MMMs.

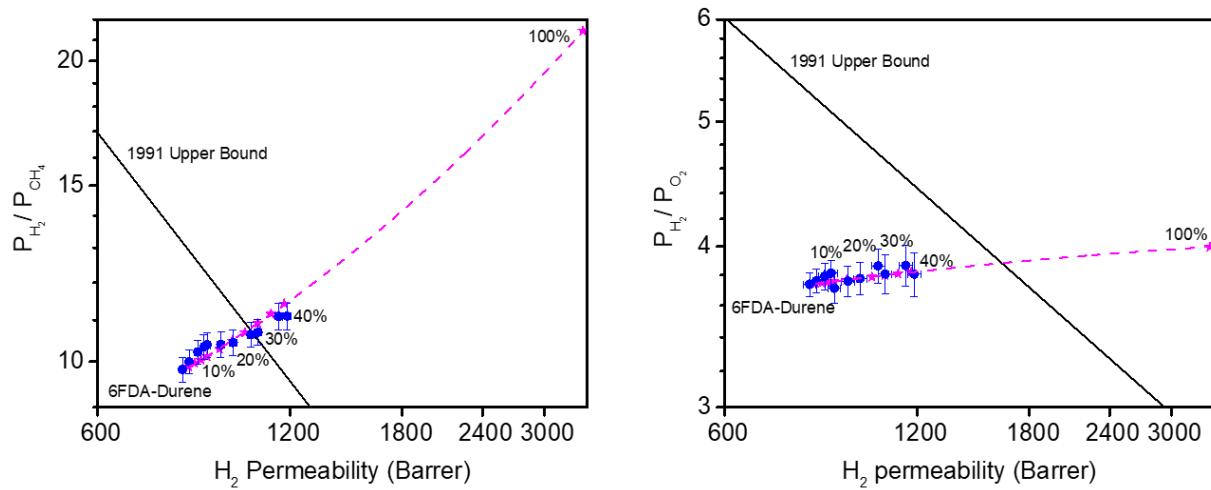


Figure S5.  $\text{H}_2/\text{CH}_4$  and  $\text{H}_2/\text{O}_2$  upper bound plots (blue circles: experimental data; pink stars: Maxwell Model predictions)

Table S1. CO<sub>2</sub>/CH<sub>4</sub> separation data for MOF-based MMMs from the literature

MOF	Loading (wt%)	Polymer	Pressure (bar)	CO <sub>2</sub> permeability (Barrer)	Selectivity CO <sub>2</sub> /CH <sub>4</sub>	Ref.
6FDA-Durene/ UiO-66-NH <sub>2</sub>	40	6FDA-Durene	1	1890	17.7	This work
NH <sub>2</sub> -UiO-66-ABA	30	Matrimid®	9	37.9	47.7	Vankelecom, 2015 <sup>1</sup>
UiO-66-NH <sub>2</sub>	30	PAO-PIM-1	N.A.	8126	18.4	Jin, 2017 <sup>2</sup>
UiO-66-NH <sub>2</sub>	20	PIM-1 (in-situ crosslinking)	2	15815	19.1	Kaliaguine, 2018 <sup>3</sup>
PEG@UiO-66-NH <sub>2</sub>	40	PEBAX®	3	425	56	Qiao, 2017 <sup>4</sup>

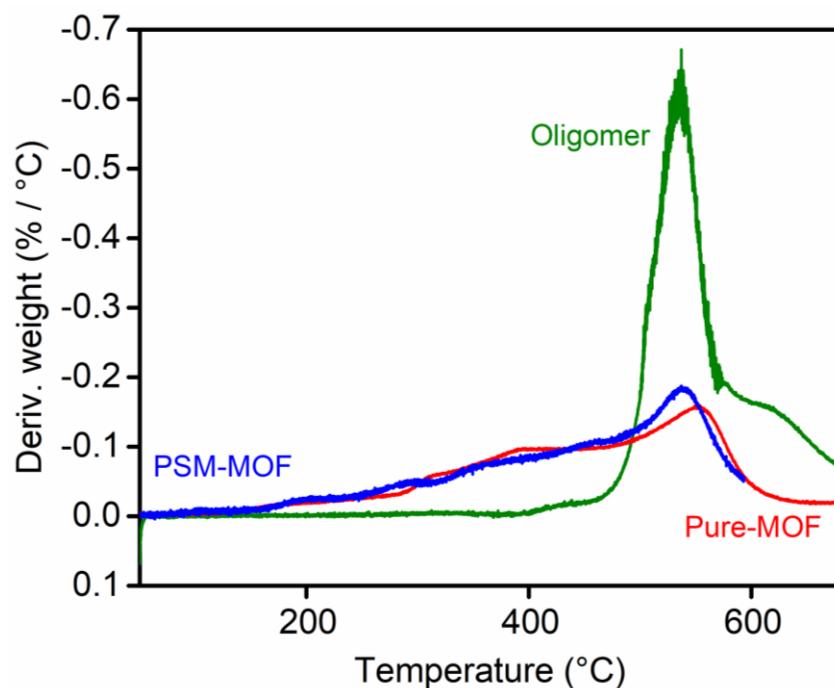


Figure S6. Derivative Thermal Gravimetric Analysis of the oligomer, Pure-MOF and PSM-MOF. Different stages of weight loss can be observed for the oligomer and the Pure-MOF.

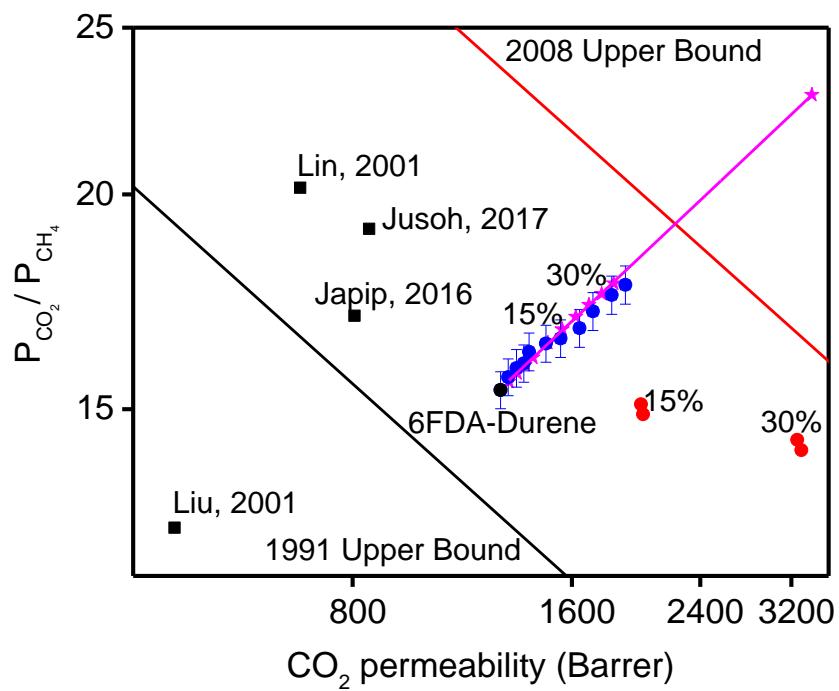


Figure S7.  $\text{CO}_2/\text{CH}_4$  upper bound plot with comparative literature data for 6FDA-Durene (black circle: experimental data for 6FDA-Durene; blue circles: experimental data for PSM-MOF MMM; pink stars: Maxwell Model predictions; red circles: experimental data for Pure MOF MMM; black squares: literature data for 6FDA-Durene<sup>6-9</sup>). The difference in reported transport properties for 6FDA-Durene relates to differences in casting conditions and the temperature/pressure at which data were obtained.

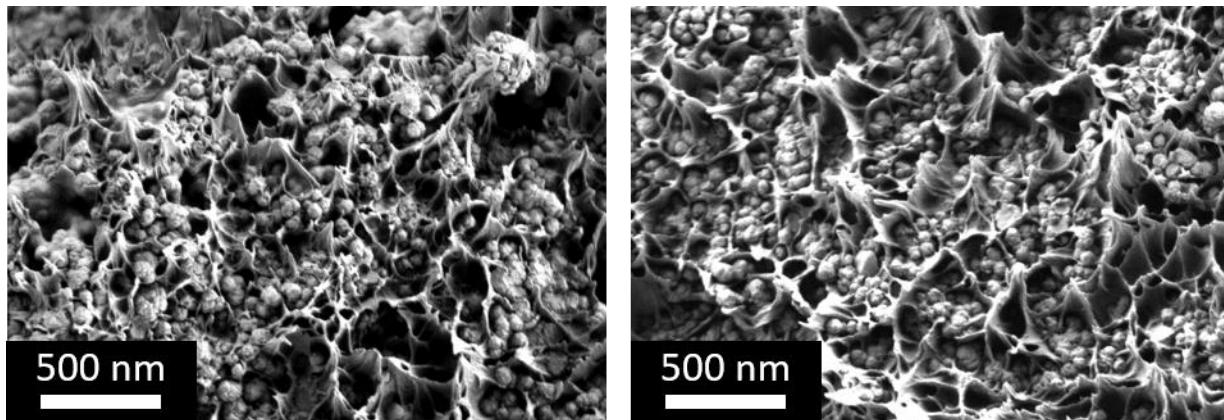


Figure S8. Cross-sectional SEM images of 40% PSM-MOF MMM taken near the top surface (left) and bottom surface (right).

Table S2. Permeation results for independently prepared samples of 6FDA-Durene and corresponding MMMs to evaluate reproducibility.

Loading (wt%)	Permeability (Barrer)									
	CH <sub>4</sub>		N <sub>2</sub>		O <sub>2</sub>		H <sub>2</sub>		CO <sub>2</sub>	
	Trial 1	Trial 2	Trial 1	Trial 2	Trial 1	Trial 2	Trial 1	Trial 2	Trial 1	Trial 2
<b>0%</b>	83±3	81±3	86±3	85±3	218±7	210±7	820±20	810±20	1280±40	1250±40
<b>2.5%</b>	84±3	84±3	86±3	88±3	222±7	228±7	840±30	860±30	1310±40	1340±40
<b>5%</b>	84±3	86±3	86±3	87±3	227±7	232±7	860±30	870±30	1340±40	1360±40
<b>7.5%</b>	85±3	85±3	87±3	88±3	231±7	232±7	880±30	880±30	1370±40	1370±40
<b>10%</b>	86±3	88±3	87±3	89±3	240±7	250±7	890±30	890±30	1400±40	1410±40
<b>15%</b>	90±3	88±3	92±3	90±3	249±7	249±7	940±30	930±30	1470±40	1450±40
<b>20%</b>	94±3	92±3	97±3	95±3	259±8	254±8	980±30	960±30	1540±40	1510±40
<b>25%</b>	98±3	99±3	103±3	106±3	270±9	280±9	1040±30	1060±30	1640±50	1670±50
<b>30%</b>	100±3	104±3	106±3	109±3	281±9	288±9	1070±30	1090±30	1710±50	1760±50
<b>35%</b>	104±3	102±3	108±3	106±3	300±10	295±10	1150±40	1130±40	1810±60	1800±60
<b>40%</b>	107±3	106±3	109±3	107±3	310±10	308±10	1180±40	1160±40	1890±60	1870±60

Table S3. Permeation results for Pure MOF MMMs

Loading (wt%)	Permeability (Barrer)		Selectivity CO <sub>2</sub> /CH <sub>4</sub>
	CH <sub>4</sub>	CO <sub>2</sub>	
<b>15%</b>	132	1990	15.1
<b>30%</b>	226	3260	14.4

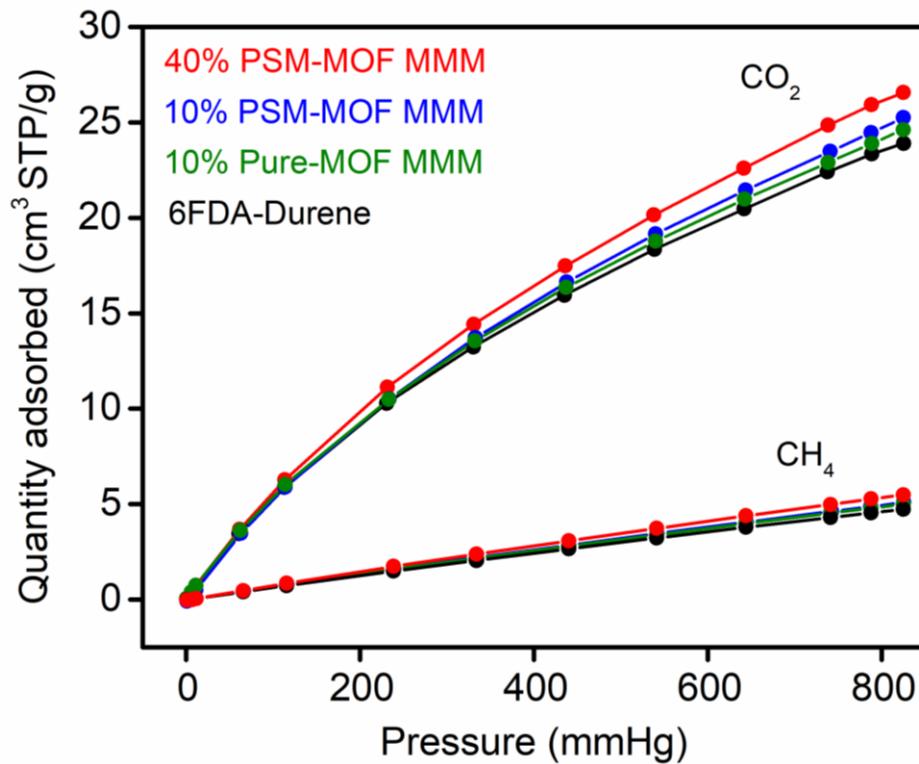


Figure S9. CO<sub>2</sub> and CH<sub>4</sub> sorption isotherms for 6FDA-Durene and corresponding MMMs.

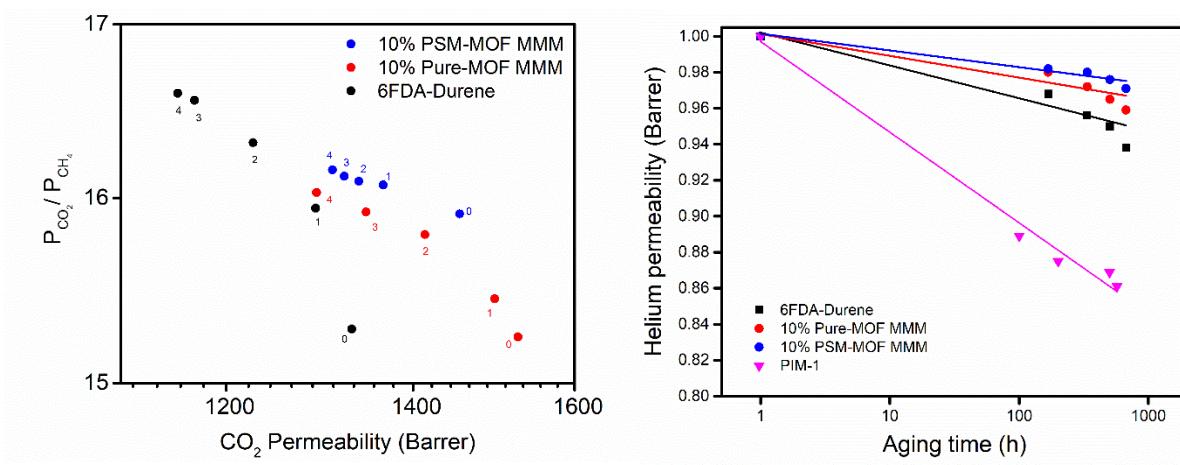


Figure S10. Physical aging of 6FDA-Durene and corresponding MMMs shown in CO<sub>2</sub>/CH<sub>4</sub> upper bound plot (left) and normalized helium permeability plot (right). The number indicates the week number of a specific test. PIM-1 aging data was added as a reference.

## **Section C: Using the Maxwell model to predict transport in MMMs and volume fraction calculation**

### *C1. Gas transport prediction using the Maxwell Model*

Experimental data ( $P_{\text{MMM}}$ ) at low loadings (below 20 wt%) were first used to calculate pure MOF permeability ( $P_f$ ) for each gas. These values ( $P_{\text{MMM}}$  at loadings below 20 wt% and  $P_f$ ) were then used together with the pure polymer permeability ( $P_p$ ) to predict MMM permeabilities at all loadings. Volume fractions of MOF loading were calculated as described in section C2.

### *C2. Volume fraction calculation*

TGA with an air sweep flow was used to determine the weight fraction of MOF fillers in MMMs. TGA profiles show that 6FDA-Durene decomposes completely under air flow at 700 °C (weight loss = 100%). Therefore, equation (1) was used to calculate the weight fraction of the MOF in the MMM:

$$\text{MOF loading (wt\%)} = \frac{\text{wt\% remained of MMM at } 700 \text{ } ^\circ\text{C}}{\text{wt\% remained of pure MOF at } 700 \text{ } ^\circ\text{C}} \quad (1)$$

To convert weight fraction to volume fraction, densities of the pure MOF and MMM are required. A crystal density of 1.36 g cm<sup>-3</sup> for the pure UiO-66-NH<sub>2</sub> was taken from Mason *et al.*<sup>5</sup> Density of MMMs can be measured using a density kit attached to a Mettler Toledo mass balance (30029886). Equation (2) was then used to convert weight fraction to volume fraction:

$$\text{MOF loading (vol\%)} = \frac{\text{MOF loading (wt\%)}}{\rho_{\text{MOF}}} \rho_{\text{MMM}} \quad (2)$$

where,  $\rho_{\text{MOF}}$  and  $\rho_{\text{MMM}}$  are the densities of the MOF and MMM, respectively.

## References

- (1) Anjum, M. W.; Vermoortele, F.; Khan, A. L.; Bueken, B.; Vos, D. E. De; Vankelecom, I. F. J. Modulated UiO-66-Based Mixed-Matrix Membranes for CO<sub>2</sub> Separation. *ACS Appl. Mater. Interfaces*, 2015, 7, 25193–25201.
- (2) Wang, Z.; Ren, H.; Zhang, S.; Zhang, F.; Jin, J. Polymers of Intrinsic Microporosity/Metal–organic Framework Hybrid Membranes with Improved Interfacial Interaction for High-Performance CO<sub>2</sub> Separation. *J. Mater. Chem. A*, 2017, 5, 10968–10977.
- (3) Tien-Binh, N.; Rodrigue, D.; Kaliaguine, S. In-Situ Cross Interface Linking of PIM-1 Polymer and UiO-66-NH<sub>2</sub> for Outstanding Gas Separation and Physical Aging Control. *J. Memb. Sci.*, 2018, 548, 429–438.
- (4) Xie, K.; Fu, Q.; Kim, J.; Lu, H.; He, Y.; Zhao, Q.; Scofield, J.; Webley, P. A.; Qiao, G. G. Increasing Both Selectivity and Permeability of Mixed-Matrix Membranes: Sealing the External Surface of Porous MOF Nanoparticles. *J. Memb. Sci.*, 2017, 535, 350–356.
- (5) Mason, J. A.; Veenstra, M.; Long, J. R. Evaluating Metal-Organic Frameworks for Natural Gas Storage. *Chem. Sci.*, 2014, 5, 32–51.
- (6) Lin, W. H.; Chung, T. S. Gas Permeability, Diffusivity, Solubility, and Aging Characteristics of 6FDA-Durene Polyimide Membranes. *J. Memb. Sci.*, 2001, 186, 183–193.
- (7) Liu, S. L.; Wang, R.; Liu, Y.; Chng, M. L.; Chung, T. S. The Physical and Gas Permeation Properties of 6FDA-Durene/2,6-diaminotoluene Copolyimides. *Polymer*, 2001, 42, 8847-8855.
- (8) Jusoh, N.; Yeong, Y. F.; Lau, K. K.; Shariff, A. M. Enhanced Gas Separation Performance Using Mixed Matrix Membranes Containing Zeolite T and 6FDA-Durene Polyimide. *J. Memb. Sci.*, 2017, 525, 175-186.
- (9) Japip, S.; Xiao, Y.; Chung, T. S. Particle-Size Effects on Gas Transport Properties of 6FDA-Durene/ZIF-71 Mixed Matrix Membranes. *Ind. Eng. Chem. Res.*, 2016, 55, 9507–9517.
- (10) Nagata, S.; Kokado, K.; Sada, K. Metal-Organic Framework Tethering PNIPAM for ON-OFF Controlled Release in Solution. *Chem. Commun.*, 2015, 51, 8614-8617.