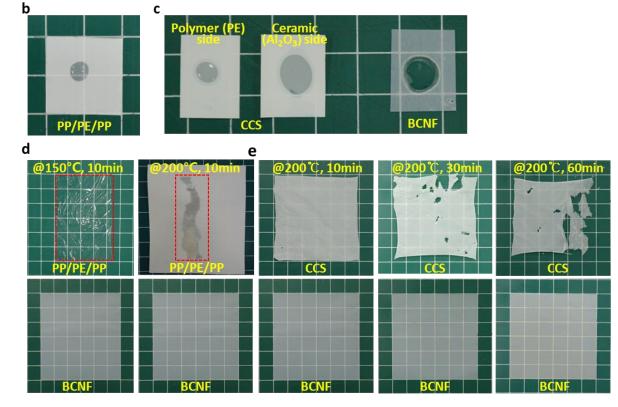
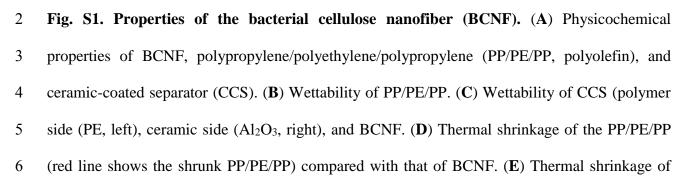
A Safe and Sustainable Bacterial Cellulose NanoFiber Separator for Lithium Rechargeable Batteries

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Park⁴, Chanhee Lee⁴, Seungyeon Lee⁴, Woo Sung Jeon⁴, Woo Dae Jang⁶, Hyun Uk Kim⁶, Sang
Yup Lee⁶, Dongmin Im¹, Seok-Gwang Doo⁴, Sang Yoon Lee⁴, Hyun Chul Lee^{2,*} & Jin Hwan
Park^{3,*}

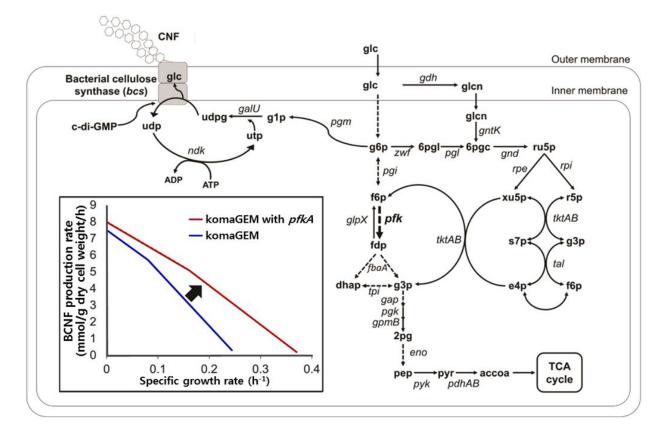
Properties of separator	BCNF	PP/PE/PP**	CCS***
Thickness (µm)	12	20	18
Porosity (%)	77	39	n.d.
Tensile strength (MPa) (MD/TD*)	63.5 / 49.9	182.3 / 13.1	83.5 / 94.4
Elongation (%) (MD/TD)	7 / 6	84 / 1220	268 / 220
Air permeability (sec per 100 cm ³)	199	547	206
Pin-puncture strength (N)	0.76	3.86	4.63
Impedance (Ω)	0.2	1.4	1.3

*MD (machine direction), TD (transverse direction), **Celgard2320, ***CK1819, Toray

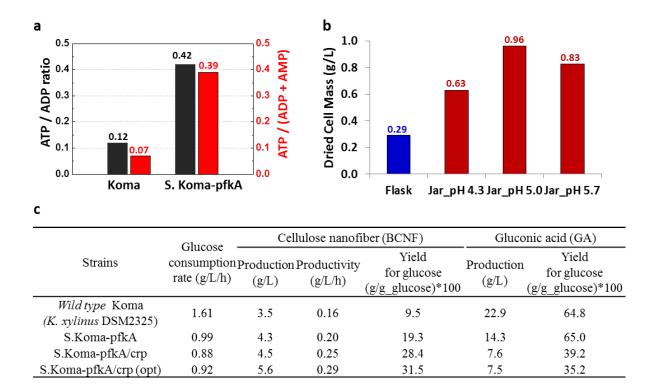




- and CCS (e) compared with that of BCNF. The BCNF possesses low thermal shrinkage of less
- than 1% at 200 °C



2 Fig. S2. Genome scale metabolic model (GEM) of Komagataeibacter xylinus DSM 2325 3 (Koma) and the simulated effect of *pfkA* gene expression on the CNF production. A GEM of 4 Koma was reconstructed using the genome annotation data (i.e. GenBank files) of this bacterium. 5 The complete GEM of Koma, named as komaGEM, contains information on 688 genes, 6 corresponding to 1,712 metabolites and 1,810 reactions. Apart from transporter reactions, 7 reactions involved in 'Amino acid metabolism' (11.1% of the total number of reactions), 'Glycan 8 metabolism' (10.9%), 'Metabolism of cofactors and vitamins' (10.3%), and 'Carbohydrate 9 metabolism' (8.8%) contributed to more than 40% of the reactions in the GEM. The kxyGEM 10 was used to predict the effects of the pfkA gene expression on the CNF production and cell 11 growth (inset).



2 Fig. S3. Production of cellulose nanofibers. (A) Intracellular adenosine triphosphate 3 (ATP)/adenosine diphosphate (ADP) ratio and ATP/(ADP + adenosine monophosphate (AMP)) 4 ratio in Koma and S. Koma-pfkA strains. S. Koma-pfkA showed much higher ATP/ADP ratio 5 (3.5 times) and ATP/(ADP+AMP) ratio (5.6 times) than those in Koma strain. (B) Effect of pH 6 on the cell mass in the high seed cell process. (C) Cellulose nanofiber production from the Koma 7 and optimised S.Koma-pfkA/crp (opt) strains in batch fermentation. The S.Koma-pfkA/crp strain 8 with optimised fermentation exhibited increased BCNF production (from 3.5 to 5.6 g/L), 9 productivity (from 0.16 to 0.29 g/L/h), and the highest yield reported so far (31.5%) with a 10 sharply decreased yield (from 64.8 to 35.2%) of by-product, gluconic acid (GA) compared with 11 those in wild type Koma strain.

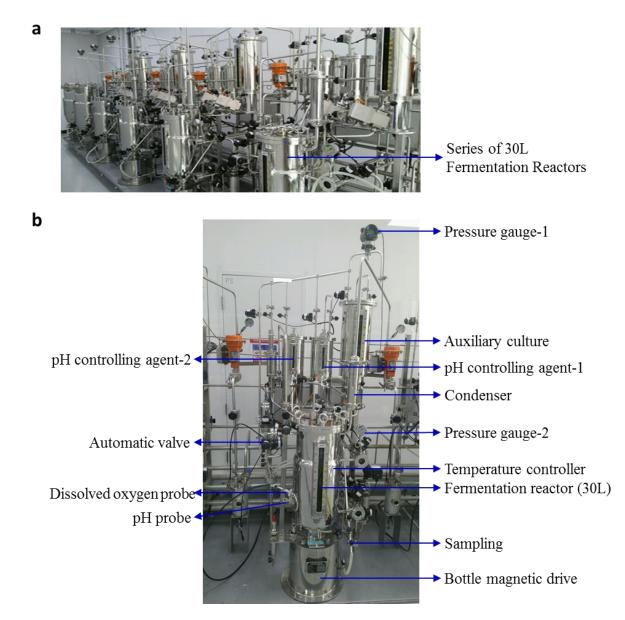


Fig. S4. Scale-up of fermentation. Mass-production of BCNF in a series of 30-L fermentation
reactors. The pressure, temperature, pH, and dissolved oxygen (DO) are monitored during the
fermentation.

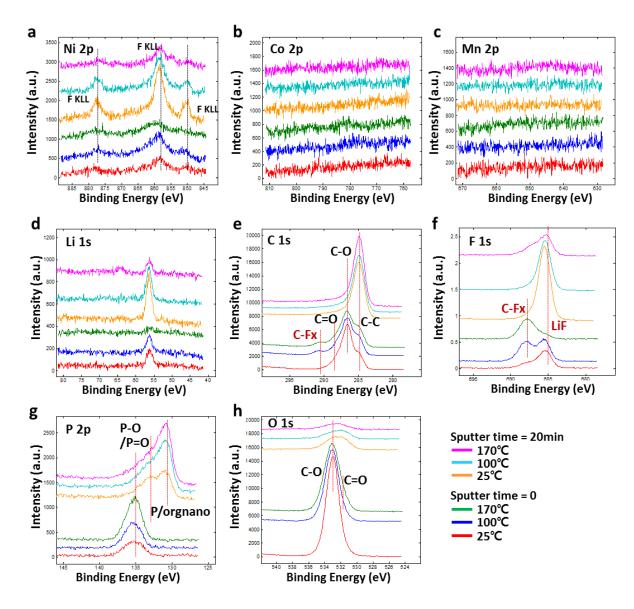


Fig. S5. X-ray photoelectron spectroscopy spectra of BCNF after heat-exposure at 170 °C.
(A) Ni 2p spectra. (B) Co 2p spectra. (C) Mn 2p spectra. (D) Li 1s spectra. (E) C 1s spectra. (F)
F 1s spectra. (G) P 2p spectra. (H) O 1s spectra. The BCNF separator was obtained from the Li
ion battery (LIB) full cell, which was exposed to 170 °C, and then analysed with different
sputtering times (0 and 20 min).

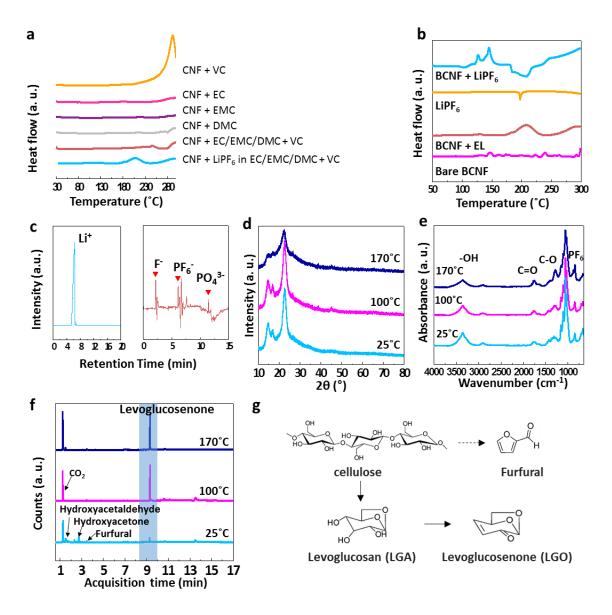
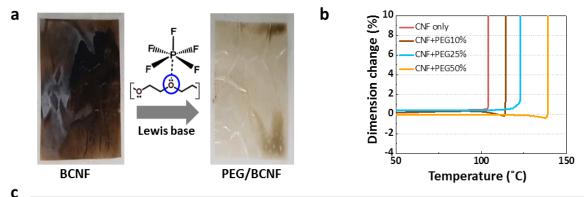
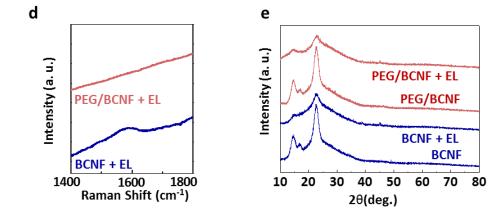


Fig. S6. Thermal safety performances and characterization of BCNF. (A) Differential scanning calorimetry thermograms of BCNF with each component of the electrolyte (ethylene carbonate (EC), ethyl methyl carbonate (EMC), dimethyl carbonate (DMC), vinylene carbonate (VC), and lithium hexafluorophosphate (LiPF₆)). An exothermic reaction occurred below 200 °C, only when LiPF₆ was used. (B) Differential scanning calorimetry (DSC) thermograms of BCNF and its reactivity with lithium hexafluorophosphate (LiPF₆) and the electrolyte (EL) including

1	LiPF ₆ . Exothermic peaks appear only in the presence of LiPF ₆ , while no exothermic peaks in
2	pure BCNF or LiPF ₆ . (C) Ionic species determined via ion chromatography of the carbonised
3	BCNF at 170 °C. (D) X-ray diffraction patterns of the BCNF. The crystallinity of BCNF
4	decreased from 83 to 21% as the heat-exposure temperature increased from 25 to 170 °C in ex-
5	situ hot-box tests. (E) Fourier-transform infrared (FT-IR) spectra. The intensity of the -OH bond
6	of the BCNF decreased and those of both of the C–O bonds caused by the decomposition of the
7	cellulose structure and PF ₆ peak from LiPF ₆ , increased as the heat-exposure temperature
8	increased from 25 to 170 °C. (F) Pyrolysis-gas chromatography-mass spectroscopic analysis at
9	350 °C of BCNF after <i>ex-situ</i> heat-exposure in the presence of the electrolyte including LiPF ₆ at
10	25, 100, and 170 °C, respectively. (G) Possible pathways for the transformation of BCNF to the
11	pyrolysed products.



C	Materials		Thinkness (µm)	Air permeability (sec per 100 cm³)	Pin-puncture strength (N)	Tensile strength (MPa) (MD)
	CNF only		14	172	0.56	40.4
		10%	14	186	0.50	36.9
	PEG(%)/BCNF	25%	16	224	0.58	35.0
		50%	18	520	0.64	32.0



1

Fig. S7. Characterization of PEG/BCNF. (A) Photographs of a BCNF membrane in a battery with LiPF₆ in comparison with that in an electrolyte containing polyethylene glycol (PEG) as well. It was observed that the carbonisation of BCNF was alleviated, when PEG was added to the electrolyte (25%). (B) TMA analysis of the BCNF and PEG/BCNFs mixed with an electrolyte. The PEG was directly added into the BCNF during membrane manufacture process. When mixed with the electrolyte, BCNF exhibited a sharp decrease in thermal resistance to 104 °C, compared to BCNF only (338 °C in Fig. 3D). The thermal resistance improved up to 140 °C as

the amount of PEG added was increased (up to 50%). (C) Properties of the PEG/BCNF with 1 2 different amounts of PEG (10, 25, and 50%). The PEG(25%)/BCNF membrane exhibited 3 reasonable properties such as tensile strength of ~35 MPa, air-permeability of 224 s/100 cm⁻³, 4 and applied as a separator in LIB. (D) Raman spectra of BCNF and PEG/BCNF. The C-C bond on the carbonised BCNF decreased on the PEG/BCNF. (E) X-ray diffraction patterns of BCNF 5 6 and PEG(25%)/BCNF. After heat-treating at 170 °C in the presence of an electrolyte including 7 LiPF₆, the decrease in the crystallinity (67 to 46%) of the PEG(25%)/BCNF membrane was 8 much more mitigated than that of the BCNF membrane (83 to 21%).

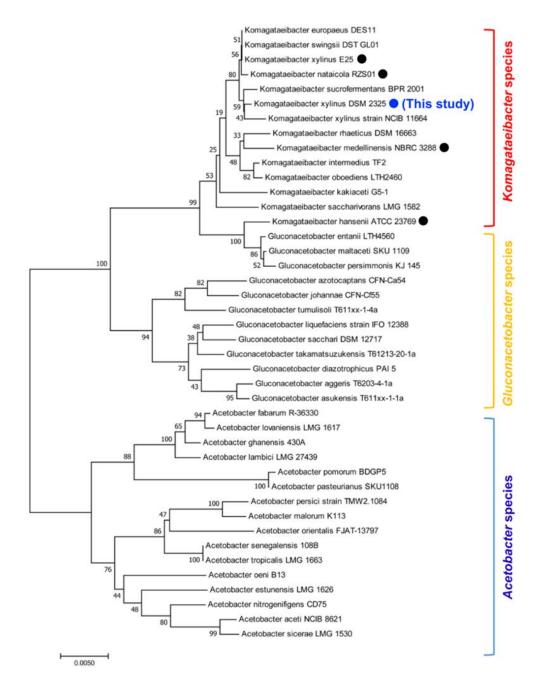


Fig. S8. Phylogenetic relationship of bacteria belonging to the Acetobacteraceae family based on their 16S rRNA sequences. Genome of *Komagataeibacter xylinus* DSM 2325 was newly sequenced in this study (blue dot). The four *Komagataeibacter* species with black dots have complete genome sequences. The 16S rRNA gene based-phylogenetic tree was constructed using the neighbour-joining method¹ of MEGA 7.0². The sequences were aligned using

MUSCLE³ within MEGA 7.0. Percentages of replicate trees for the associated taxa clustered
together in the bootstrap test (1,000 replicates) are shown next to the branche⁴. Evolutionary
distances were computed using the p-distance method in units of the number of base
substitutions per site⁵.

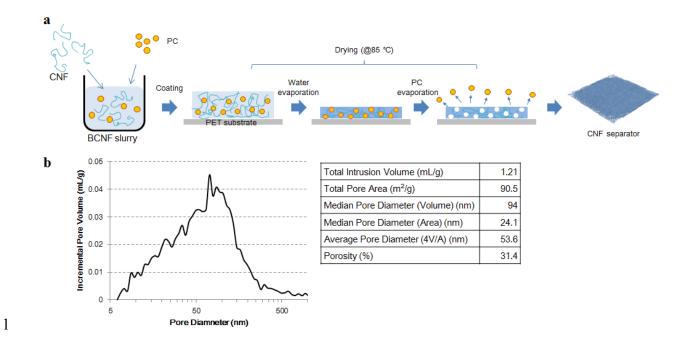


Fig. S9. Preparation and characterization of BCNF non-woven separator. a, The Slurry of BCNF mixed with PC, as foam making agent, was coated on PET substrate. During drying, as water evaporates first, the matrix of BCNF was constructed and then PC, which has lower volatility, evaporates to form pores. Fully dried BCNF film is easily detached from substrate. b, The pore size distribution and porosimetric values of BCNF separator from mercury porosimeter analysis (Autopore IV9500, Micromeritics).

1 Table S1. Koma strains and plasmids constructed and used in this study

Strains and plasmids	Genotype & Descriptions	Reference
Strains		
Koma (K. xylinus DSM 2325)	Wild-type strain	DSMZ
S.Koma- $\Delta 2760$	DSM 2325, Δ2760	This work
S.Koma-pfkA	DSM 2325, Δ 2760_P _{tac} ::pfkA (from E. coli MG1655)	This work
S.Koma-Δ0648	S. Koma-pfkA, Δ0648	This work
S.Koma-pfkA/crp	S. Koma-pfkA, Δ0648_P _{tac} ::crp	This work
Plasmids		
pMSK+	Vector for cloning; Kan ^R	This work
pTSK+	Vector for allelic exchange in K. xylinus; tetA	This work
pTSa	Shuttle vector for K. xylinus; tetA	This work
pTSa-EX1	Vector for overexpression under the control of tac promoter; tetA	This work
pTSa-EX2	Vector for overexpression under the control of gapA promot er; tetA	This work
pTSa-pfkA	Cloning pfkA gene into BamHI site of pTSa-EX1; tetA	This work
pTSa-pgi	Cloning pgi gene into BamHI site of pTSa-EX1; tetA	This work
pTSa-pgk	Cloning pgk gene into BamHI site of pTSa-EX1; tetA	This work
pTSa-fba	Cloning fba gene into BamHI site of pTSa-EX1; tetA	This work
pTSa-tpi	Cloning tpi gene into BamHI site of pTSa-EX1; tetA	This work
pTSa-gap	Cloning gap gene into BamHI site of pTSa-EX1; tetA	This work
pTSa-gpm	Cloning gpm gene into BamHI site of pTSa-EX1; tetA	This work
pTSa-pck	Cloning pck gene into BamHI site of pTSa-EX1; tetA	This work
pTSa-mae	Cloning mae gene into BamHI site of pTSa-EX1; tetA	This work
pTSK-Δ2760	Vector for deletion of Gene_2760 of the K. xylinus DSM 2 325	This work
pTSK-∆2760-Ec.pfkA	Vector for integration of E. coli pfkA gene; tetA	This work
pIN01	Vector for deletion of Gene_0648 of the K. xylinus DSM 2 325; cm^{R}	This work
pIN01-crp	Vector for integration of crp (Gene_2117) under the control of gapA promoter; cm ^R	This work

1 Table S2. Primers used for gene clonin	g and deletion
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Primer	Sequence
	•
MD-058	5'-TATTGAAAAAGGAAGAGTATGATTGAACAAGATGGATTGCACGCAGGT-3'
MD-059 MD-060	5'-AGTAAACTTGGTCTGACATCAGAAGAACTCGTCAAGAAGGCGATAGAA-3' 5'-ACTCTTCCTTTTTCAATATTATTGAAGCA-3'
	5'-TGTCAGACCAAGTTTACTCATAT-3'
MD-061 P1646	
P1646 P1647	5'-CTTGATATCGAATTCTTCTCATGTTTGACAGCTTATCATC-3' 5'-GGGCTGCAGGAATTCGAATTTCTGCCATTCATCCGC-3'
P1662	5'-CTTGATATCGAATTAGGCCTGTCATCGTCTATATACG-3'
P1663 P1664	5'-CGTGTTGTTCGAATTCGATGGATATTCCTCCAGTATCATGTG-3'
P1665	5'-CATCGAATTCGAACAACACGCCGATGTATGAC-3' 5'-ACATGAGAAGAATTGACAGATCCGGTCAGTTCACATTATC-3'
	5'-CGTACCCGGGGATCCATGATTAAGAAAATCGGTGTGTGTG
Ec.pfkA_F Ec.pfkA_R	5'-GACTCTAGAGGATCCTTAATACAGTTTTTTCGCGCAGTC-3'
pgi_F	5'-TCCTCTAGAGTCGACATGAGTGCGCGTGAATCTG -3'
	5'-TGCCTGCAGGTCGACTCAGACCGCGTGGGCGATATC -3'
pgi_R pgk_F	5'-TCCTCTAGAGTCGACATGGGTGCGGCAAGCTTC-3'
pgk_F pgk_R	5'-TGCCTGCAGGTCGACTCAGATGGGCATGGCCCG-3'
fba_F	5'-TCCTCTAGAGTCGACATGCCTATTGATCAGATGCGCC -3'
fba_R	5'-TGCCTGCAGGTCGACTCAGACCTTTTGCGTCGAAG -3'
tpi_F	5'-TCCTCTAGAGTCGACATGAAACAGATCATTGTTGGCAAC-3'
tpi_F	5'-TGCCTGCAGGTCGACTCACGATGCGCGGGCGG-3'
gapA_F	5'-TCCTCTAGAGTCGACATGGCTGTTAAAGTCGCAATAAAC-3'
gapA_R	5'-TGCCTGCAGGTCGACTTACAGGGCACCGAATACG-3'
pgk_F	5'-TCCTCTAGAGTCGACATGGGTGCGGCAAGCTTC-3'
pgk_R	5'-TGCCTGCAGGTCGACTCAGATGGGCATGGCCCG-3'
gpm_F	5'-TCCTCTAGAGTCGACATGAACGACCATGAATCGATGAAC-3'
gpm_R	5'-TGCCTGCAGGTCGACTCAGGATGGCGTGGACC-3'
pck_F	5'-TCCTCTAGAGTCGACATGACCGAAGCCGCCGC-3'
pcK_R	5'-TGCCTGCAGGTCGACTTAGCCAAAAGCGCCAACATG-3'
mae_F	5'-TCCTCTAGAGTCGACATGTCGGACACAGTGCG-3'
mae_R	5'-TGCCTGCAGGTCGACTCAGGCTTTTTCGTACGGG-3'
P1678	5'-ATATCCATCGAATTCGGAGCTTATCGACTGCACG-3'
P1679	5'-GTGTTGTTCGAATTCAAAAGGCCATCCGTCAGG-3'
0648up_infF	5'-GACGGCCAGTGAATTTGGCACCATACATTCCGGTTTCCC-3'
0648up_infR	5'-CGACCTGCACAGCCAAGACCATGCCTTGCCCGTTATCG-3'
0648dn_infF	5'-TGGCCTTTTTGCCTTAGGCATCCGTTCGCACGATACCTG-3'
0648dn_infR	5'-ATGATTACGCCAGCTTAATATGGCAGCCATCAATACCCC-3'
Ptac_F	5'-GGCTGTGCAGGTCGTAAATCACTGC-3'
Dian D	5'-TITICICCATCAATAGCICGICCCICCTICITICIAGAGAGCICGGIACCCGGAGATCIATGITICCIGIGIGAAATIG-
Ptac_R	3'
Cat-F	5'-CGAGCTATTGATGGAGAAAAAATCACTGG-3'
Cat-R	5'-GGGCACCAATAACTGCCTTAAAA -3'
P-mcs-infF	5'-CAGTTATTGGTGCCCAACGAATCACCTGTAAGTCGGACGC -3'
P-mcs-infR	5'-AAGGCAAAAAGGCCATCCGTCAGG -3'
2117-infF	5'-TAGAGTCGACCTGCATGAAAGTGAATTGGAAATTATC-3'
2117-infR	5'-GCTTGCATGCCTGCACTAGCCGTTGCCTGCGGCCAG -3'
pUC19-F	5'-ACACGGTGCCTGACTGCGTTAGCAATTTAACTGTG -3'
pUC19-R	5'-ATGGAAGCCGGCGGCACCTCGCTAACGGATTCACCACTCCAAG -3'
Tet-F	5'-CGCAGTCAGGCACCGTGTATGAAATCTAACAATGCGCTCATCGTCATCCTC-3'
Tet-R	5'-GGTGCCGCCGGCTTCCATTCAGGTCGAGGTGGCCCGGCTCCATG-3'
pSa-F	5'-GCCAGCAAGACAGCGATAGAGGGTAGTTATCCACGTGAAAC -3'
pSa-R	5'-CGACTTACAGGTGATCGGAAATCCAGAAGCCCGAGAGGTTG -3'
EX1_infF	5'-CTGACGGATGGCCTTTTTGCCTTCCGCTTCCTCGCTCACTGACTC-3'
EX1_infR	5'-TCTACGCCGGACGCATCGCGTCCGACTTACAGGTGATCGGAAAT-3'
Ptac_infF	5'-CGATGCGTCCGGCGTAGAGGATCCGGAGCTTATCGACTG -3'
Ptac_infR	5'-CGAGCTCOGTACCCAATCAATAGCTCGTCCCTGIGTGAAATTIGTTATCCGCTCAC-3'
EX1-MCS_infF	5'-ATTGGGTACCGAGCTCGAATTCGTACCCGGGGATCCTCTAGAGTCGAC -3'
TrrnB_infR	5'-GCAAAAAGGCCATCCGTCAGGATGGCC -3'
EX2_infR	5'-CGGGCGCCGCAGTTGCGTCCGACTTACAGGTGATCGGAAAT-3'
PgapA_infF	5'-AACTTCGGCGGCGCCCGAGCGTGAACAGCAC-3'
PgapA_infR	5'-CGAGCTCGGTACCCAATTTTCTTATTTTCTCCGTAAGGTCTGAC-3'

1 Table S3. Number of genes from *Komagataeibacter xylinus* DSM 2325 for each clusters of

COG functional category	Number of genes	% of total	Description
А	0	0.00	RNA processing and modification
В	0	0.00	Chromatin structure and dynamics
С	168	6.65	Energy production and conversion
D	22	0.87	Cell cycle control, cell division, chromosome partitioning
E	218	8.62	Amino acid transport and metabolism
F	77	3.05	Nucleotide transport and metabolism
G	135	5.34	Carbohydrate transport and metabolism
Н	110	4.35	Coenzyme transport and metabolism
Ι	59	2.33	Lipid transport and metabolism
J	150	5.93	Translation, ribosomal structure and biogenesis
Κ	140	5.54	Transcription
L	282	11.16	Replication, recombination and repair
М	174	6.88	Cell wall/membrane/envelope biogenesis
Ν	4	0.16	Cell motility
0	106	4.19	Posttranslational modification, protein turnover, chaperones
Р	175	6.92	Inorganic ion transport and metabolism
Q	34	1.34	Secondary metabolites biosynthesis, transport and catabolism
R	0	0.00	General function prediction only
S	513	20.29	Function unknown
Т	76	3.01	Signal transduction mechanisms
U	47	1.86	Intracellular trafficking, secretion, and vesicular transport
V	38	1.50	Defence mechanisms
W	0	0.00	Extracellular structures
Y	0	0.00	Nuclear structure
Ζ	0	0.00	Cytoskeleton
	2,528		·

2 orthologous groups (COG) functional category using eggNOG-mapper^{6,7}

locus_tag ID		KEGG orthology (KO)	^c Definition
Bacterial synthesis	cellulose		
^a GENE ^a GENE ^a GENE GENE ^a GENE	02677 00599 01096 02507	K00694 K20541	Cellulose synthase (UDP-forming) (BcsA) Cellulose synthase operon protein B (BcsB)
^ª GENE_ ^ª GENE_ ^ª GENE_	00602	K20543	Cellulose synthase operon protein C (BcsC)
^a GENE_	02679	No KO assigned	Cellulose synthase operon protein D (BcsD)
^a GENE_	_00600	No KO assigned	BcsX
^a GENE_	00601	No KO assigned	Putative membrane-bound transacylase (BcsY)
Regulation of cellulose synth			
^a GENE_ GENE_	-	K01179	Endoglucanase
^a GENE_ GENE_	-	K01188	Beta-glucosidase
^b GENE ^b GENE ^b GENE ^b GENE GENE GENE GENE GENE	00259 00422 01580 01742 00123 00656 00991	K13069	Diguanylate cyclase
^b GENE_ ^b GENE_ ^b GENE_ ^b GENE_ ^b GENE_ ^b GENE	00260 00421 01578 01579	K07181	Phosphodiesterase

1 Table S4. Genes associated with the bacterial cellulose biosynthesis

2 3 4

^a Genes found in *bcs* operons
^b Genes found in *cdg* operons
^c Enzyme names retrieved from KEGG database

COG functional category	Number of genes	% of total	Description	
А	0	0.00	RNA processing and modification	
В	0	0.00	Chromatin structure and dynamics	
С	118	7.33	Energy production and conversion	
D	18	1.12	Cell cycle control, cell division, chromosome partitioning	
E	143	8.88	Amino acid transport and metabolism	
F	61	3.79	Nucleotide transport and metabolism	
G	85	5.28	Carbohydrate transport and metabolism	
Н	102	6.34	Coenzyme transport and metabolism	
Ι	40	2.48	Lipid transport and metabolism	
J	135	8.39	Translation, ribosomal structure and biogenesis	
Κ	76	4.72	Transcription	
L	89	5.53	Replication, recombination and repair	
Μ	119	7.39	Cell wall/membrane/envelope biogenesis	
Ν	2	0.12	Cell motility	
Ο	90	5.59	Posttranslational modification, protein turnover, chaperones	
Р	98	6.09	Inorganic ion transport and metabolism	
Q	20	1.24	Secondary metabolites biosynthesis, transport and catabolism	
R	0	0.00	General function prediction only	
S	313	19.44	Function unknown	
Т	49	3.04	Signal transduction mechanisms	
U	30	1.86	Intracellular trafficking, secretion, and vesicular transport	
V	22	1.37	Defence mechanisms	
W	0	0.00	Extracellular structures	
Y	0	0.00	Nuclear structure	
Z	0	0.00	Cytoskeleton	
	1,610			

Table S5. Number of core genes from the five *Komagataeibacter* species for each COG functional category using eggNOG-mapper^{6, 7}

Table S6. Maximal titers, yields, and productivity levels of BCNF-producing strains as
 described previously.

Strains	C-source	CNF Production (g/L)	Yield per reduced sugar (wt%)	Fermentation Time (hr)	Fermentation Type	Reference
S.Koma-pfkA/crp	Glucose	5.6	31.5	19.5	30L Batch Fermentor	In this study
Acetobacter xylinum BPR2001	Fructose	8	20	67	50L Internal- Loop Airlift Reactor	8
Acetobacter xylinum BRC 5	Glucose	15.3	26	50	5L Fed batch Fermentor	9.
Acetobacter xylinum ssp. sucrofermentans BPR2001	Fructose	10.4	11.6	52	50L internal- loop airlift reactor	10
Gluconacetobacter xylinus ATCC 23770	Fiber sludges	10-11	30	168	Static culture	11

1 Methods

2 Bacterial strains, culture media, and conditions

The Koma strains and plasmids used and constructed in this study are listed in table S1. The wild-type *Komagataeibacter xylinus* DSM 2325 (Koma) strains were obtained from the Leibniz Institute DSMZ (German Collection of Microorganisms and Cell Cultures) (Braunschweig, Germany). The Koma strains were usually grown in the Hestrin-Schramm (HS) medium (0.5% yeast extract, 0.5% peptone, 0.375% Na₂HPO₄, 0.115% citric acid, pH 4.5) supplemented with 2% glucose, and then cultured at 30 °C. For the production of cellulose nanofibers, 1% (v/v) ethanol was added to the HS medium.

10 Construction of plasmids

11 The oligonucleotides used in this study are listed in table S2. For the construction of pMSK+, the kan^R gene from pK19-mobsacB and vector backbone from pBluescript II SK (+) 12 13 (Stratagene) were amplified using two pairs of oligonucleotides designated as MD-058 / MD-059 14 and MD-060 / MC-061, respectively. After purification, the PCR fragments were cloned using In-Fusion[®] HD Cloning Kit (Clonetech). For the construction of pTSK+, the tetA gene from 15 16 pBR322 (ATCC) was amplified using the P1646/P1647 primer set. The obtained PCR fragment was purified and cloned into EcoRI restriction site of the pMSK+ vector using the In-Fusion[®] 17 18 HD Cloning Kit. For the construction of pTSa shuttle vector, the pUC origin from puc19 and 19 tetA resistance gene from pBR322 (ATCC) DNA fragments were amplified using two pairs of 20 oligonucleotides designated as pUC19-F/R and tet-F/R, respectively. After purification, the PCR fragments were cloned using the In-Fusion[®] HD Cloning Kit, which resulted in pUC-tet. pSa 21 22 originating from pUCD2 (ATCC) was amplified using pSa-F/R primers. After purification, the

PCR fragments were cloned into the EcoRI restriction site of pUC-tet the using In-Fusion® HD 1 2 Cloning Kit. The pTSa-EX1 and pTSa-EX2 were constructed for the overexpression of genes 3 under the control of tac or gapA promoter. To construct the pTSa-EX1 vector, the vector region 4 of pTSa and Ptuf::MCS::TrrnB DNA fragments from the pTac15K vector were amplified using 5 EX1 infF/R, Ptac infF/R, and EX1-MCS infF/TrrnB infR primer sets, respectively. After purification, the PCR fragments were cloned using the In-Fusion[®] HD Cloning Kit. For the 6 construction of the pTSa-EX2 vector, the vector region of pTSa-EX1 and gapA promoter from K. 7 8 xylinus DSM 2325 were amplified using two pairs of oligonucleotide designated as EX1-9 MCS infF/EX2 infR and PgapA infF/R, respectively. After purification, the PCR fragments were cloned using the In-Fusion[®] HD Cloning Kit. For the overexpression of *pfkA from E. coli* 10 11 MG1655, pgi, pgk, fba, tpi, gap, pgk, gpm, pck, and mae genes from K. xylinus DSM 2325, ORFs 12 were amplified using oligonucleotide pairs and cloned into BamHI or SalI restriction site of the 13 pTSa-EX1 vector using the In-Fusion[®] HD Cloning Kit. For the construction of pTSK- $\Delta 2760$, 14 the region up- and down-stream of the Gene 2760 were amplified using two pairs of 15 oligonucleotides designated as P1662/P1663 and P1664/P1665, respectively. After purification, the PCR fragments were cloned into EcoRI restriction site of pTSK+ using In-Fusion® HD 16 17 Cloning Kit. The pTSK-A2760 Ec.pfkA was constructed for the integration of the E. coli pfkA 18 gene. The tac promoter, pfkA gene, and rrnB terminator were amplified from pTSa-Ec.pfkA 19 using the P1678 and P1679 primer sets. After purification, the PCR fragments were cloned into EcoRI restriction site of pTSK-Δ2760 using the In-Fusion[®] HD Cloning Kit. The pIN01 was 20 21 constructed for the deletion of the Gene 0648 gene. The region up- and down-stream of the 22 Gene 0648 were amplified using two pairs of oligonucleotides designated as 0648up infF/R and 23 0468dn infF/R, respectively. The tac promoter from pTSa-EX1, chloramphenicol resistance

gene from pBR322, and PgapA-MCS-TrrnB cassette from pTSa-EX2 were amplified using
Ptac_F/R, cat_F/R, and P-mcs-infF/R primer sets, respectively. After purification, the PCR
fragments were cloned into EcoRI and HindIII restriction site of pUC19 using the In-Fusion[®]
HD Cloning Kit. For the construction of pIN01-crp, the crp gene (Gene_2117) from *K. xylinus*DSM 2325 was amplified using the 2117_infF/R primer set. After purification, the PCR
fragments were cloned into PstI restriction site of pIN01 using the In-Fusion[®] HD Cloning Kit.

7 Abbreviations of gene and metabolites

8 Genes

9 gdh: glucose dehydrogenase; zwf: glucose 6-phosphate 1-dehydrogenase; pgl: 6-10 phosphogluconolactonase; gnd: 6-phosphogluconate dehydrogenase; rpe: ribulose-phosphate 3-11 epimerase; rpi: 6-phosphogluconate dehydrogenase; tkt: transketolase; tal: transaldolase; pgi: 12 glucose-6-phosphate isomerase; pfkA: 6-phosphofructokinase A; fbaA: fructose bisphosphate 13 aldolase A; tpi: triosephosphate isomerase; gap: glyceraldehyde 3-phosphate dehydrogenase; pgk: 14 phosphoglycerate kinase; gpmB: 2,3-bisphosphoglycerate-independent phosphoglycerate mutase 15 B; eno: enolase; pyk: pyruvate kinase; pdhAB: pyruvate dehydrogenase AB; pgm: 16 phosphoglucomutase; ugp: UTP-glucose-1-phosphate uridylyltransferase; ndk: nucleoside-17 diphosphate kinase.

18 Metabolites

glc: glucose; glcn: gluconate; g6p: glucose 6-phosphate; 6pgl: 6-phosphogluconolacton;
6pgc: 6-phosphogluconate; ru5p: ribulose-5-phosphate; r5p: ribose-5-phosphate; xu5p: xylulose5-phosphate; s7p: sedoheptulose; e4p: erythrose 4-phosphate; g3p: glyceraldehyde-3-phosphate;
f6p: fructose 6-phosphate; f16p: fructose-1,6-diphosphate; dhap: dihydroxyacetone phosphate;

1 2pg: 2-phosphoglyceric acid; pep: phosphoenol pyruvate; pyr: pyruvate; g1p: glucose 1-2 phosphate; udpg: UDP-glucose; c-di-GMP: cyclic diguanylate.

3

Genome sequencing of Komagataeibacter xylinus DSM 2325

4 Genome sequencing of Koma revealed that this bacterium has the genome of 3,727,795 5 base pairs (bp), consisting of a circular chromosome (3,353,346 bp) and two plasmids (369,140 6 and 5,309 bp), with an average guanine (G) + cytosine (C) content of 58.9%. Comparative 7 genome analysis was performed on Koma and other five *Komagataeibacter* species (table S3 to 8 S5). A result of the classification of genes according to the clusters of orthologous groups (COG) 9 functional categories revealed that 'Replication, recombination, and repair' (11.2%) and 'Amino 10 acid transport and metabolism' (8.6%) were the two subsystems associated with the greatest 11 number of genes with the exception of 'Function unknown' (20.3%) (table S3). Genes associated 12 with the CNF biosynthesis were also found in the genome of Koma, including glk encoding glucokinase, pgm encoding phosphoglucomutase, galU encoding UTP-glucose-1-phosphate 13 14 uridylyltransferase, and bcs operon (bcsABCD genes) (table S4).Genome analysis also confirmed that the wild-type Koma does not have the phosphofructokinase (pfkA) gene in 15 16 glycolysis, but has a full set of genes for pentose phosphate pathway (PPP). The genome was 17 sequenced using Illumina HiSeq 2500 (Illumina, San Diego, CA) and PacBio RS II system 18 (Pacific Biosciences, Menlo Park, CA). Illumina and PacBio reads were assembled using SPAdes¹² and HGAP¹³, respectively. The assembled contigs from the two sequencing 19 approaches were merged using GARM¹⁴. Among a total of 48,560,562 Illumina reads generated, 20 21 47,301,277 reads (97.41%) were mapped to the assembled genome, which validated the quality of the finished genome sequence. Genome annotation was implemented using PGAP¹⁵. 22

2

Sequences of one chromosome and two plasmids of the wild-type Koma have been deposited in the NCBI GenBank under the accession numbers, CP025269 to CP025271 (fig. S8).

3

Construction of metabolically engineered strains and plasmids

4 The metabolically engineered Koma strains were constructed by a homologous recombination procedure, as described previously¹⁶. To construct S. Koma-*A*2760, S. Koma-5 pfkA, and S. Koma-pfkA/crp, 10 µL of a plasmid DNA (pTSK-Δ2760, pTSK-Δ2760-Ec.pfkA, 6 7 or pIN01-crp) was added to 100 μ L of competent cells. Then, the cell/DNA mixture was 8 transferred to a cold 2-mm electroporation cuvette and a pulse was applied. Cells were 9 transferred to 1 mL of an HS medium containing 0.2% cellulase in a 14-mL round tube and 10 incubated overnight at 30 °C with shaking. Subsequently, the cells were spread on a HS agar 11 plate supplemented with tetracycline (10 μ g/mL) or chloramphenicol (200 μ g/mL). The primers 12 used for gene cloning and deletion are listed in Table S2. Detailed procedures for the 13 construction of plasmids and the abbreviations of the genes and metabolites are provided in the Supporting Information. All DNA manipulations were carried out using standard protocols¹⁷. 14

15 Computational fluid dynamics methodology and kLa measurement

16 Computational fluid dynamics (CFD) can be used to simulate and optimise mixing, 17 shear stress, and mass transfer coefficients. CFD was performed using NX (3D CAD) and 18 FLOW-3D (general-purpose CFD package software). The model system consisted of a 2.5-L 19 standard stirred tank reactor filled with 1.4 L of the fermentation medium. Among the various 20 multiphase models, the Volume of Fluid (VOF) model was chosen to model the turbulence 21 between fermentation medium and air using the momentum and volume fraction equations. The 22 reactor model contained grids with a total of up to 6×10^5 . The impellers and reactor walls were

1 treated as non-slip boundaries with standard wall functions. Impeller rotation was simulated 2 using general moving objects (GMO) model in steady state simulations. From multiphase 3 simulations using the VOF model, the turbulent energy and shear stress were predicted for 4 various impeller types (Rushton, Pitch-blade, modified pitch-blade), agitation speeds (50-350 5 rpm), and viscosity (1–40 cP). The volumetric oxygen-transfer coefficient ($k_L a$) represents the 6 capacity of the oxygen supply, which is related to the impeller type, reactor configuration, 7 agitation speed, and aeration rate. The k_{La} was determined by a dynamic (unsteady-state) method. 8 In this method, the reactor is first deoxygenated by sparging nitrogen gas until DO reaches below 9 20% saturation level. Then, the air is reintroduced into the fermenter while the DO reaches about 10 80% saturation value. The $k_{\rm I}$ a was determined at an agitation speed of 50–350 rpm, aeration rate 11 of 1.4 L/min, temperature of 30 °C, and viscosity of 1-40 cP.

12

 $dDO/dt = k_L a (DO_{sat} - DO)$

13 BCNF production by CMC-based fermentation

14 The high seed cell process, which is one of the most cost-effective means of achieving high CNF productivity, was performed to maximise the cell mass and activity by adjusting the 15 culture conditions, including temperature, pH, and medium. A maximum dry cell mass of 0.96 16 g/L was obtained at a seed pH of 5.0 (fig. S3). The seed culture was prepared by a two-step 17 18 fermentation process. In the first seed culture process, Koma strain grown in HS agar medium, 19 was inoculated into a 250-mL Erlenmeyer flask containing 100 mL of the HS medium at 150 20 rpm for 10 h. The temperature was maintained at 30 °C in all the cultures, unless otherwise 21 indicated. The second seed culture was performed in a 1.0-L jar fermenter (HANIL science; 22 South Korea) containing 0.7 L of a medium composed of 35 g/L glucose, 1 g/L yeast extract, 2

1 g/L monosodium glutamate (MSG), 0.5 g/L MgSO₄·7H₂O, 1.0 g/L KH₂PO₄, 1.15 g/L citric acid, 2 10 mM sodium acetate buffer (pH 4.7), and 10 g/L Na-CMC under 250 rpm and aeration rate of 3 0.7-1.0 L/min. Most of fermentation parameters were assessed in a 2.5-L jar fermenter (New 4 Brunswick Fermentation systems Bioflo 310, USA) containing 1.4 L of the medium under 5 250–350 rpm and an aeration rate between 1.4 and 2.1 L/min, depending on the culture time. The 6 pH was controlled at 5.0 using a 3 N KOH solution. The supplementation of oxygen-enriched air 7 plays an important role in the production of CNF from glucose. Therefore, fermentations were 8 carried out to determine the optimal oxygen composition (0-50%). The optimal oxygen 9 composition for CNF production was found to be 25%. For the mass production of BCNF, we used a series of 30-L-scale fermenters (KoBio Tech, KF-30, South Korea) under the same culture 10 11 condition used with the 2.5-L jar fermenter.

12 **Fibrillation and purification**

13 After the fermentation process, the resulting broth including BCNFs was homogenised 14 using a general homogeniser (Homogenizer HG-15A, Daehan Science, Republic of Korea). Then, 15 the homogenised fermentation broth was passed through a microchannel (size 200 μ m, 16 Interaction chamber) of a nano disperser (ISA-NH500, Ilshin autoclave, Republic of Korea) 17 under a pressure of 1500 bar. The well-homogenised BCNF solution was centrifuged under high 18 pressure to obtain a cellulose precipitate. The precipitate was heated for 2 h in 0.1 N NaOH 19 aqueous solution at 90 °C to hydrolyse the cells and impurities existing between the BCNFs, and 20 the resulting mixture was washed thoroughly with distilled water to obtain purified BCNFs via 21 repeated centrifugation until the conductivity of the supernatant became less than 10 µS/cm.

22 **Preparation of the BCNF separator**

1 Considering the large scale roll-to-roll process of battery manufacturing, the introduction 2 of an appropriate pore forming agent should be carefully considered, that can provide uniform 3 pore formation and have excellent compatibility with other battery components. In order to easily 4 produce large quantities of uniform non-woven BCNF membranes, purified BCNF was mixed 5 with propylene carbonate (PC) serving as a foaming agent and carboxymethylcellulose (CMC) 6 (MW ~90 kDa) could also be added to control the air permeability of the separator by 7 interrupting hydrogen bonding between CNFs. Remarkably, most of the reported pore-forming 8 agents induced aggregation of fibrillated CNFs or required further washing with toxic solvents. 9 However, PC, which is known as a common electrolyte component, is well-soluble in a CNF 10 suspension and mostly evaporates during the drying process. The pore forming mechanism is 11 thought to be due to the difference of vapour pressure between water and PC. As the water 12 evaporates first, the hydrogen bonds are built between CNFs in the presence of PC, and then, 13 the pores are formed as PC evaporates, as shown in fig. S9. The BCNF slurry was prepared as 14 follows: a solution of BCNF (0.6 g) in H₂O (120 g) was mixed with PC (2.4 g) and CMC (0.12 g) 15 to obtain high air permeability, below 200 s/100 cm³. Then, the resulting slurry was coated on a 16 polyethylene terephthalate (PET) film (240 mm × 300 mm) using a micrometre applicator. The 17 coated slurry was dried in an oven for 90 min. Subsequently, the BCNF separator was detached 18 from the PET substrate and its tensile strength and air permeability was evaluated using an LRX-19 PLUS Universal Testing Machine (Lloyd instruments, UK) and Oken Type Air Permeability 20 Tester EGO-1-55-1MR (ASAHI SEIKO CO., LTD, Japan), respectively. The porosity (31.4 %) 21 and average pore size (53.6 nm) of as-obtained BCNF membrane were measured by mercury 22 porosimeter (Autopore IV9500, Micromeritics) (fig. S9).

23 Characterization of the BCNF separator

1 After filtering the cultivated supernatant using a 0.22-um syringe filter, glucose and 2 extracellular metabolites were quantified using a HPLC instrument (Waters) equipped with an 3 Aminex HPX-87H column (300 mm × 7.8 mm, Bio-Rad). A mobile phase of 2.5 mM H₂SO₄/0.9% (v/v) acetonitrile at a flow rate of 0.5 ml/min was used. Products were detected by refractive 4 5 index measurement and a diode array detector. For the quantification of cellulose, the cellulose 6 pads were washed with 0.1 N NaOH and rinsed several times with water and freeze-dried at -807 °C to determine the production and yield. The thermal behaviour of the separators was analysed 8 up to 400 °C with a heating rate of 10 °C/min using a thermomechanical analyser (TMA Q400, 9 Waters). X-ray diffraction was carried out on a Bruker D8 Advance X-ray diffractometer under 10 Cu Ka radiation in the 2θ range of 10–70°. The morphology of the BCNF was observed via 11 field-emission scanning electron microscopy (Nova NanoSEM 450, FEI), operated at 5 kV and transmission electron microscopy (Tecnai G², FEI), operated at 200 kV. X-ray photoelectron 12 13 spectroscopy was carried out on a PHI Quantera II (ULVAC-PHI, Inc.) using Al $K\alpha$ X-ray (hv =14 1486.6 eV). Fourier-transform infrared spectra were collected on a Varian 670-IR FT-IR 15 spectrometer (Agilent Technologies Inc.) in the attenuated total reflectance mode. Raman spectra 16 were obtained using an inVia Raman microscope (Renishaw) equipped with a 514-nm excitation 17 laser source (~1 mW power). Differential scanning calorimetry was performed on Discovery DSC (TA instruments) in the temperature range of 25–300 °C at a heating rate of 5 °C min⁻¹. 18 19 Solid-state NMR spectroscopy was performed on Bruker Avance HD-III consoles corresponding 20 to ¹H Larmor frequency of 700.13 MHz (AVANCE HD-III, 16.4T). ¹³C cross polarization magic 21 angle spinning NMR experiments were performed with a spinning frequency of 15 kHz. Under 22 the ¹³C cross polarization condition, a cross polarization contact time of 2000 µs and delay time 23 of 5.0 s were used. Pyrolysis-gas chromatography-mass spectroscopy was performed using a PY-

2020iD double-shot pyrolyser (Frontier Lab) connected to an Agilent 7890B series gas
 chromatograph (Agilent Technologies) coupled with an Agilent 5977A MSD series mass
 spectrometer (Agilent Technologies). An Agilent 7890A series gas chromatograph (Agilent
 Technologies) coupled with an Agilent 5975C MSD series mass spectrometer (Agilent
 Technologies) was used for the evolved gas analysis (EGA).

6 Electrode and electrolyte preparation for the battery

7 The positive electrode materials, $LiNi_{0.6}Co_{0.2}Mn_{0.2}O_{2}$ (NCM622) and 8 LiNi_{0.85}Co_{0.10}Al_{0.05}O₂ (NCA), were purchased from Ecopro Co. LTD. (South Korea) and used as 9 a mixture with NCM622: NCA ratio of 8:2. A slurry was prepared with the weight ratio of 10 positive electrode material, denka black, and polyvinylidene fluoride (PVDF) of 96: 1.8: 2.2 and 11 cast on both sides of a 12-µm Al foil, and then dried at 120 °C for 2 h in a vacuum oven. After 12 pressing, a 129-µm-thick positive electrode tape was obtained. The loading level of the casted positive electrode was 40.7 mg/cm². Similarly, a negative electrode was prepared via a 13 14 conventional tape-casting process. The weight ratio of graphite, styrene-butadiene rubber (SBR), 15 and carboxymethyl cellulose (CMC) in the slurry was 97.5:1.5:1.0. The mixed slurry was coated 16 on both sides of an 8-µm Cu foil and dried at 80 °C for 2 h in a vacuum oven. The full cell was 17 designed with a negative/positive (N/P) ratio of 1.13. The electrolyte used in this study consisted 18 of 1.15 M lithium hexafluorophosphate (LiPF₆) in ethylene carbonate/ethyl methyl 19 carbonate/dimethyl carbonate (EC/EMC/DMC, 2:4:4 v/v/v) and 0.5% vinylene carbonate (VC).

20 **18650 cell preparation**

Mini-sized 18650 cells with 500 mAh capacity were built using a semi-automatic winder
 using 54-mm-wide and 150-mm-long cathodes, 58-mm wide and 190-mm long anodes, 65-mm-

1 wide CNF separators. The anode tab was spot-welded to the bottom of the 18650-can through the 2 central mandrel hole and the can was grooved just above the roll to prevent the roll from sliding 3 out of the can. After attaching the header, the cells took approximately 3.0 mL of the electrolyte. 4 After filling, the cells were crimped. The cells were subjected to galvanostatic charge-discharge 5 cycling (at 60 °C) using a Toyo system (Toscat-3100U). The cells were typically cycled between 2.8 and 4.3 V (versus Li/Li⁺) at 1.0 C rate. 1 C corresponds to 600 mA g⁻¹. A constant voltage 6 7 (CV) was applied until 0.05 C was achieved at 4.3 V and held for 10 min at both 2.8 V and 4.3 V. 8 The DC-IR was determined after every 100 cycles at 25 °C. Before each experiment, the state of 9 charge (SOC) was adjusted to 50% by drawing a 0.2 C charging current. After discharging for 10 10 s with a current of 1 A, DC-IR was calculated from the electric voltage difference.

11 Full-pouch cell preparation and Hot-box test

12 For hot-box test, 1.5 Ah full-pouch cells with a size of 4 mm \times 40 mm \times 70 mm were 13 assembled. Prior to filling the electrolyte, the stacked cells were dried overnight at 80 °C in a 14 vacuum oven to remove residual moisture. The assembled cells were charged up to 3.6 V, and 15 then the cells were cut open to release the generated gas. After degassing, the cells were vacuum-16 sealed again and discharged to 3.0 V. The cells were formed by charging (CC/CV)/discharging 17 (CC) between 4.3 and 2.8 V at the C/5 rate for 3 cycles. In the CC/CV step, CV was fixed at 18 C/20. Finally, the formed cells were fully charged for the hot-box test. To evaluate the battery 19 safety performance, the fully charged cells were placed in an oven connected to a battery tester. 20 The temperature of the oven was linearly increased from room temperature to 170 °C at the rate of 5 °C min⁻¹ and maintained there. At the same time, the cell voltage was monitored using the 21 22 battery tester (Toyo, Toscat-3000U) during the test.

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