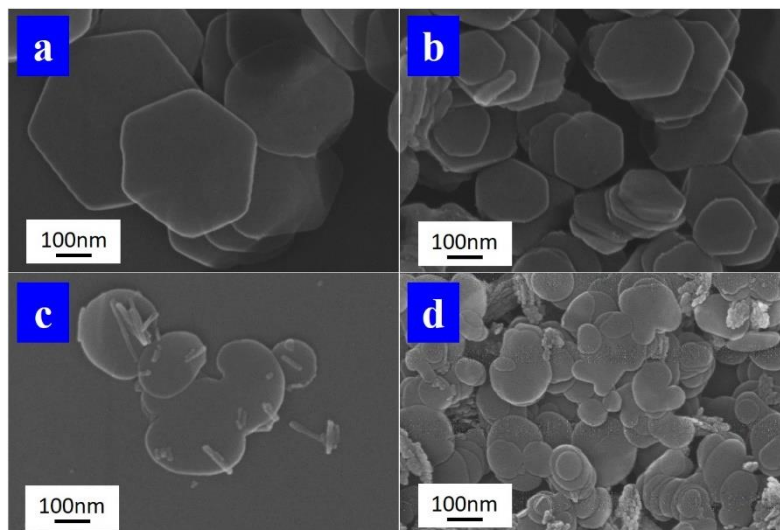


Supplementary Information for

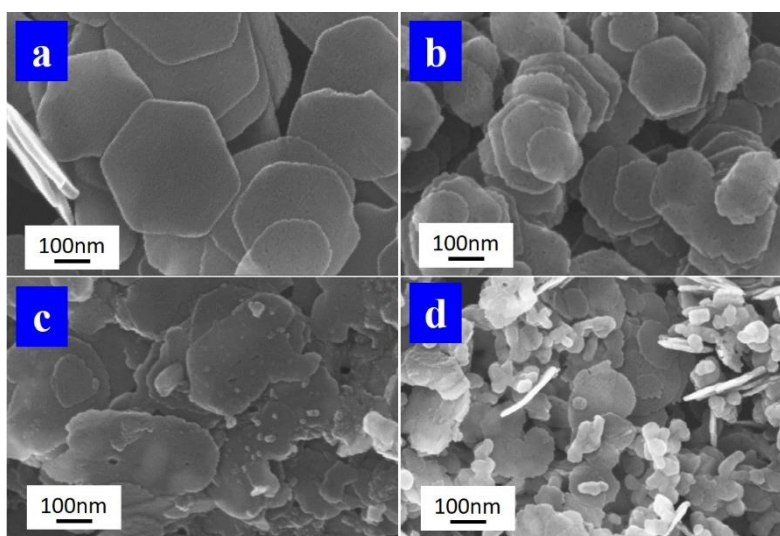
**Interfacial Fe₅C₂-Cu catalysts toward Low-Pressure Syngas
Conversion to Long-Chain Alcohols**

Li et al.

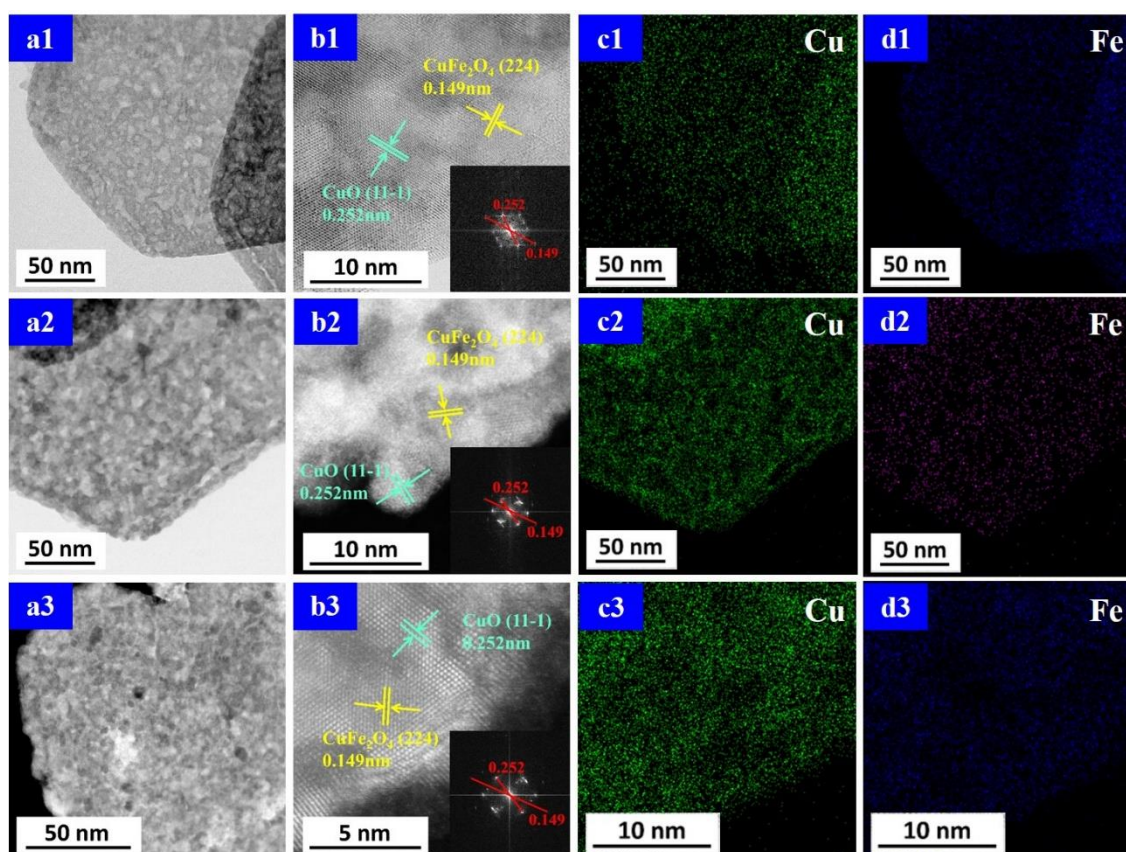
Supplementary Figures and Tables



Supplementary Figure 1. Morphology of $\text{Cu}_x\text{Fe}_y\text{Mg}_4\text{-LDH}$. SEM images of (a) $\text{Cu}_1\text{Fe}_1\text{Mg}_4\text{-LDH}$, (b) $\text{Cu}_2\text{Fe}_1\text{Mg}_4\text{-LDH}$, (c) $\text{Cu}_4\text{Fe}_1\text{Mg}_4\text{-LDH}$ and (d) $\text{Cu}_6\text{Fe}_1\text{Mg}_4\text{-LDH}$.



Supplementary Figure 2. Morphology of $\text{Cu}_x\text{Fe}_y\text{Mg}_4\text{-MMO}$. SEM images of Calcined sample: (a) $\text{Cu}_1\text{Fe}_1\text{Mg}_4\text{-MMO}$, (b) $\text{Cu}_2\text{Fe}_1\text{Mg}_4\text{-MMO}$, (c) $\text{Cu}_4\text{Fe}_1\text{Mg}_4\text{-MMO}$ and (d) $\text{Cu}_6\text{Fe}_1\text{Mg}_4\text{-MMO}$.



Supplementary Figure 3. Morphology of $\text{Cu}_x\text{Fe}_y\text{Mg}_4\text{-MMO}$. TEM images of Calcined sample: (a1–a3) $\text{Cu}_1\text{Fe}_1\text{Mg}_4\text{-MMO}$, $\text{Cu}_2\text{Fe}_1\text{Mg}_4\text{-MMO}$ and $\text{Cu}_4\text{Fe}_1\text{Mg}_4\text{-MMO}$. (b1–b3) HRTEM images selected from (a1–a3) and their Fourier transform patterns of the selected region (inset), respectively. (c1–c3) and (d1–d3) EDS mapping of elemental distribution for Cu and Fe.

Supplementary Table 1. Physicochemical properties of various catalysts

Sample	BET surface area ($\text{m}^2 \text{g}^{-1}$)	Surface C content (%)	Cu/Fe ratio ^a	Cu/Fe ratio ^b	Cu Crystallite size ^c (nm)	Mean Cu particle size ^d (nm)
Cu_1Fe_1	32.49	33.53	0.63	0.99	15.7	13.4
Cu_2Fe_1	22.07	36.39	1.24	1.96	18.4	17.9
Cu_4Fe_1	15.96	35.43	2.37	3.84	21.7	21.0
Cu_6Fe_1	10.38	29.99	4.47	5.67	25.1	-

^a Cu/Fe ratio was determined by XPS.

^b Cu/Fe ratio was determined by inductively coupled plasma-atomic emission spectroscopy (ICP-AES).

^c Crystallite size was determined by XRD with the Scherrer equation.

^d Mean Cu particle size was determined by TEM images.

Supplementary Table 2. Catalytic performances of samples with various calcination temperatures

Catalysts ^{a,b,c}	Conv. [%]	Selectivity[mol%]				Alcohols distribution[%] ^d				
		CH ₄	C ₂₊ H	ROH	CO ₂	MeOH	EtOH	PrOH	BuOH	C ₅₊ OH
Cu ₄ Fe ₁ Mg ₄ -MMO(800)	17.3	11.3	44.7	5.2	38.8	21.3(1.1)	59.2(3.1)	12.0(0.6)	5.7(0.3)	1.8(0.1)
Cu ₄ Fe ₁ Mg ₄ -MMO(500)	48.7	2.8	48.0	15.6	33.6	6.0(0.9)	31.7(4.9)	5.8(0.9)	2.5(0.4)	54.0(8.5)
Cu ₄ Fe ₁ Mg ₄ -MMO(400)	43.2	4.3	47.8	19.0	28.9	10.9(2.1)	43.5(8.3)	10.6(2.0)	5.2(1.0)	30.8(5.6)
Cu ₄ Fe ₁ Mg ₄ -MMO(350)	44.9	3.1	43.4	18.8	34.7	5.9(1.0)	49.8(9.3)	9.2(1.7)	4.3(0.8)	31.8(6.0)
Cu ₄ Fe ₁ Mg ₄ -LDH	42.1	9.8	50.3	18.7	21.2	26.6(4.9)	45.3(8.4)	14.1(2.6)	6.2(1.2)	7.8(1.6)

^a Activation conditions: 1 g precursor, H₂: CO: CO₂=1: 1: 2 (40 mL min⁻¹), 2 °C min⁻¹, 300 °C 2 h + 350 °C 1 h.

^b Reaction conditions: 3 MPa, 260 °C, H₂/CO=2, 2400 mL g_{cat}⁻¹ h⁻¹.

^c Various calcination temperatures of Cu₄Fe₁Mg₄-LDH in brackets.

^d Normalized data to S_{ROH}, mol% in brackets.

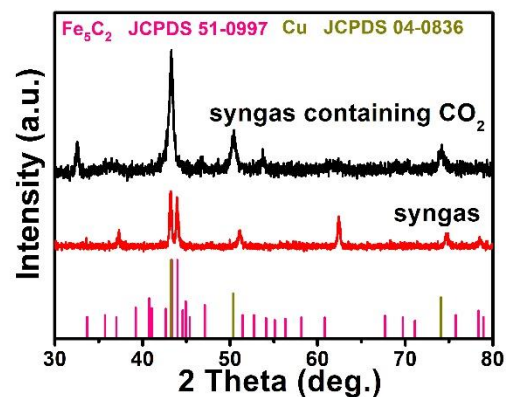
Supplementary Table 3. Catalytic performances of samples with various activation steps

Entry ^{a,b}	Conv. [%]	Selectivity[mol%]				Alcohols distribution[%] ^c				
		CH ₄	C ₂₊ H	ROH	CO ₂	MeOH	EtOH	PrOH	BuOH	C ₅₊ OH
500°C 20h	4.8	5.6	41.8	45.2	7.4	85.4(38.6)	1.9(0.8)	1.5(0.7)	0.8(0.4)	10.4(4.7)
350°C 2h	33.1	1.7	64.2	7.2	26.9	8.4(0.6)	18.4(1.3)	7.2(0.5)	1.3(0.1)	64.7(4.7)
350°C 10h (H ₂ :CO:CO ₂ :N ₂ =1:1:2:8, 100 ml min ⁻¹)	12.8	2.3	63.9	13.2	20.6	20.8(2.7)	25.3(3.3)	5.4(0.7)	1.2(0.2)	47.3(6.3)
300°C 2h + 350°C 1h	48.7	2.8	48.0	15.6	33.6	6.0(0.9)	31.7(4.9)	5.8(0.9)	2.5(0.4)	54.0(8.5)

^a Activation conditions : Cu₄Fe₁Mg₄-MMO, 1 g precursor, H₂:CO:CO₂=1:1:2 (40 ml min⁻¹), 2 °C min⁻¹.

^b Reaction conditions: 3 MPa, 260 °C, H₂/CO=2, 2400 mL g_{cat}⁻¹ h⁻¹.

^c Normalized data to S_{ROH}, mol% in brackets.

**Supplementary Figure 4.** XRD patterns of the reduced and passivated samples in syngas or syngas containing CO₂ of Cu₄Fe₁Mg₄-MMO.

Supplementary Table 4. Catalytic performances of samples with various activation atmosphere

Activation atmosphere ^{a,b}	Pressure [MPa]	Conv. [%]	Selectivity[mol%]				Alcohols distribution[%] ^c				
			CH ₄	C ₂₊ H	ROH	CO ₂	MeOH	EtOH	PrOH	BuOH	C ₅₊ OH
50.0% CO ₂	1	53.2	3.7	36.5	29.8	30.0	8.7(2.6)	28.8(8.5)	8.2(2.4)	5.2(1.5)	49.1(14.8)
	2	39.9	2.8	60.3	17.9	19.4	10.4(1.8)	41.7(7.4)	9.9(1.7)	9.1(1.6)	28.9(5.4)
	3	48.7	2.8	48.0	15.6	33.6	6.0(0.9)	31.7(4.9)	5.8(0.9)	2.5(0.4)	54.0(8.5)
Pure syngas	1	39.3	7.6	46.6	20.7	25.1	21.6(4.4)	45.1(9.3)	14.2(2.9)	7.3(1.5)	11.8(2.6)
	2	39.7	7.8	44.8	23.0	24.4	19.2(4.4)	43.1(9.9)	13.4(3.1)	10.2(2.3)	14.1(3.3)
	3	48.9	7.8	48.7	19.2	24.3	15.0(2.9)	36.5(7.0)	10.0(1.9)	5.2(1.0)	33.3(6.4)

^a Activation conditions: Cu₄Fe₁Mg₄-MMO, 1 g precursor, 40 mL min⁻¹, 2 °C min⁻¹, 300 °C 2 h + 350 °C 1 h.

^b Reaction conditions: 260 °C, H₂/CO=2, 2400 mL g_{cat}⁻¹ h⁻¹.

^c Normalized data to S_{ROH}, mol% in brackets.

Supplementary Table 5. Catalytic performances of samples with various H₂/CO ratios in reaction gas

H ₂ /CO ratio ^{a,b}	Conv. [%]	Selectivity[mol%]				Alcohols distribution[%] ^c				
		CH ₄	C ₂₊ H	ROH	CO ₂	MeOH	EtOH	PrOH	BuOH	C ₅₊ OH
1/1	26.5	4.8	34.8	12.6	47.8	12.4(1.6)	38.3(4.8)	11.2(1.4)	11.4(1.4)	26.7(3.4)
2/1	48.7	2.8	48.0	15.6	33.6	6.0(0.9)	31.7(4.9)	5.8(0.9)	2.5(0.4)	54.0(8.5)

^a Activation conditions: Cu₄Fe₁Mg₄-MMO, 1 g precursor, H₂: CO: CO₂=1: 1: 2 (40 mL min⁻¹), 2 °C min⁻¹, 300 °C 2 h + 350 °C 1 h.

^b Reaction conditions: 3 MPa, 260 °C, 2400 mL g_{cat}⁻¹ h⁻¹.

^c Normalized data to S_{ROH}, mol% in brackets.

Supplementary Table 6. Catalytic performances of samples with various reaction temperatures

Reaction temperature ^{a,b}	Conv. [%]	Selectivity[mol%]				Alcohols distribution[%] ^c				
		CH ₄	C ₂₊ H	ROH	CO ₂	MeOH	EtOH	PrOH	BuOH	C ₅₊ OH
220	4.6	4.7	39.9	53.8	1.6	12.2(6.6)	16.1(8.7)	10.7(5.7)	5.4(2.9)	55.6(29.9)
260	48.7	2.8	48.0	15.6	33.6	6.0(0.9)	31.7(4.9)	5.8(0.9)	2.5(0.4)	54.0(8.5)
300	55.4	7.4	57.3	13.7	21.6	80.3(11.0)	5.0(0.7)	3.6(0.5)	1.7(0.2)	9.4(1.3)

^a Activation conditions: Cu₄Fe₁Mg₄-MMO, 1 g precursor, H₂: CO: CO₂=1: 1: 2 (40 mL min⁻¹), 2 °C min⁻¹, 300 °C 2 h + 350 °C 1 h.

^b Reaction conditions: 3 MPa, H₂/CO=2, 2400 mL g_{cat}⁻¹ h⁻¹.

^c Normalized data to S_{ROH}, mol% in brackets.

Supplementary Table 7. Catalytic performances of samples with various reaction pressure

Catalysts ^{a,b}	Pressure [MPa]	Conv. [%]	Selectivity[mol%]				Alcohols distribution [%] ^d				
			CH ₄	C ₂ +H	ROH ^c	CO ₂	MeOH	EtOH	PrOH	BuOH	C ₅ +OH
Cu ₁ Fe ₁	1	28.1	6.7	50.8	25.4 (30.6)	17.1	19.0 (4.8)	38.5 (9.8)	15.1 (3.8)	7.3 (1.8)	20.1 (5.2)
	2	33.5	3.8	59.1	21.8 (25.7)	15.3	12.8 (2.8)	44.1 (9.6)	14.2 (3.1)	7.5 (1.6)	21.4 (4.7)
	3	58.2	3.3	52.3	12.9 (18.8)	31.5	6.8 (0.9)	47.6 (6.1)	10.1 (1.3)	4.6 (0.6)	30.9 (4.0)
Cu ₂ Fe ₁	1	28.8	2.1	44.8	23.6 (33.5)	29.5	10.9 (2.6)	31.0 (7.3)	13.4 (3.2)	8.8 (2.1)	35.9 (8.4)
	2	32.1	5.8	48.4	23.0 (29.7)	22.7	20.6 (4.7)	20.8 (4.8)	12.4 (2.8)	7.5 (1.7)	38.7 (9.0)
	3	38.4	2.4	60.9	16.8 (21.0)	19.9	21.4 (3.6)	21.6 (3.6)	9.3 (0.9)	5.3 (0.4)	43.4 (7.3)
Cu ₄ Fe ₁	1	53.2	3.7	36.5	29.8 (42.6)	30.0	8.7 (2.6)	28.8 (8.5)	8.2 (2.4)	5.2 (1.5)	49.1 (14.8)
	1 ^e	31.6	8.4	47.3	20.2 (26.6)	24.1	15.1 (3.1)	22.5 (4.5)	13.2 (2.6)	10.6 (2.1)	38.6 (7.9)
	2	39.9	2.8	60.3	17.9 (22.2)	19.4	10.4 (1.8)	41.7 (7.4)	9.9 (1.7)	9.1 (1.6)	28.9 (5.4)
	3	48.7	2.8	48.0	15.6 (23.5)	33.6	6.0 (0.9)	31.7 (4.9)	5.8 (0.9)	2.5 (0.4)	54.0 (8.5)
Cu ₆ Fe ₁	1	17.2	5.7	43.6	7.1 (12.6)	43.6	4.1(0.3)	14.7(1.0)	3.9(0.3)	2.1(0.1)	75.2(5.4)
	1 ^f	30.5	6.4	46.3	3.2 (5.7)	44.1	10.1 (0.3)	15.5 (0.5)	9.2 (0.3)	5.6 (0.2)	59.6 (1.9)
	2	27.5	3.1	45.2	9.8 (16.8)	41.9	9.1(0.9)	19.8(1.9)	6.8(0.6)	3.5(0.3)	60.8(6.1)
	3	61.5	10.7	38.0	8.9 (15.4)	42.4	9.7(0.9)	29.6(2.6)	8.2(0.7)	4.2(0.3)	48.3(4.4)

^a Activation conditions: 1 g precursor, H₂: CO: CO₂=1: 1: 2 (40 mL min⁻¹), 2 °C min⁻¹, 300 °C 2 h + 350 °C 1 h.

^b Reaction conditions : 260 °C, H₂/CO=2, 2400 mL g_{cat}⁻¹ h⁻¹.

^c S_{ROH} excluding CO₂ in brackets.

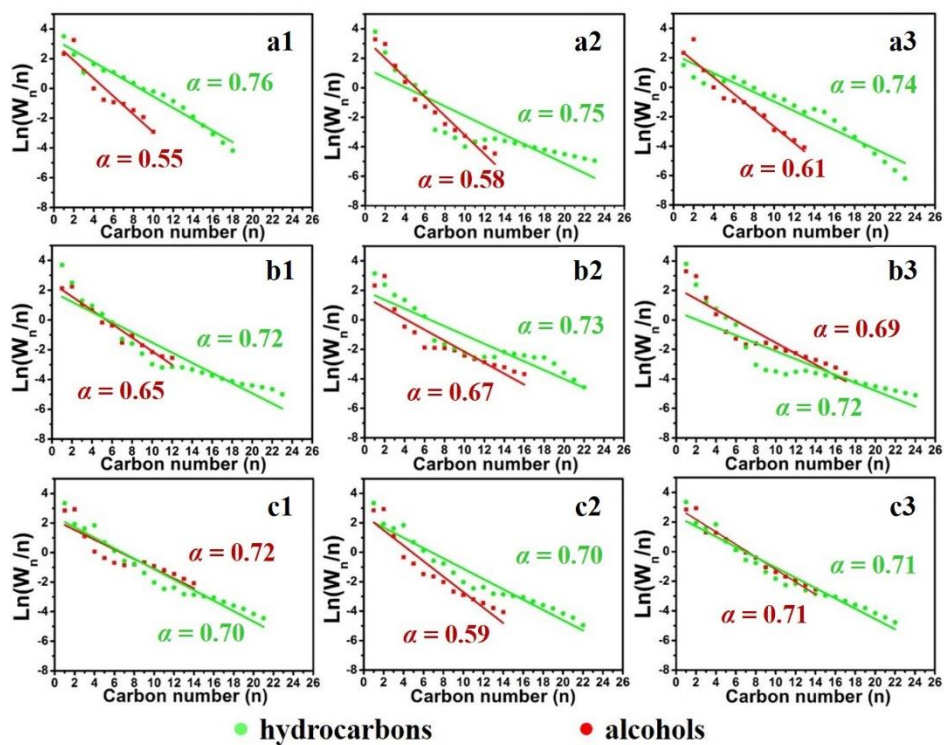
^d Normalized data to S_{ROH}, mol% in brackets.

^e WHSV = 4800 mL g_{cat}⁻¹ h⁻¹

^f WHSV = 1200 mL g_{cat}⁻¹ h⁻¹

Supplementary Table 8. Space time yield of various products calculated from Table S7

Catalysts	Pressure [MPa]	Space time yield [$\text{g g}_{\text{cat}}^{-1} \text{h}^{-1}$]					
		CH ₄	C ₂₊ H	CO ₂	ROH	MeOH	C ₅₊ OH
Cu ₁ Fe ₁	1	0.017	0.116	0.122	0.130	0.025	0.026
	2	0.012	0.166	0.135	0.141	0.018	0.030
	3	0.018	0.254	0.481	0.141	0.010	0.040
Cu ₂ Fe ₁	1	0.006	0.106	0.218	0.111	0.014	0.042
	2	0.014	0.109	0.159	0.122	0.024	0.045
	3	0.009	0.200	0.205	0.131	0.027	0.053
Cu ₄ Fe ₁	1	0.012	0.111	0.285	0.201	0.018	0.101
	2	0.010	0.205	0.207	0.140	0.014	0.040
	3	0.014	0.210	0.462	0.141	0.009	0.076



Supplementary Figure 5. Anderson-Schulz-Flory (A-S-F) plots for the distribution of alcohols and hydrocarbons. (a) Cu_1Fe_1 , (b) Cu_2Fe_1 and (c) Cu_4Fe_1 . (a1–c1) at 1 MPa, (a2–c2) at 2 MPa, (a3–c3) at 3 MPa.

Supplementary Table 9. Catalytic performance data for a variety of modified F–T catalysts used in LAS

Catalyst	H ₂ /CO ratio	Temperature /°C	Pressure /MPa	GHSV	CO conversion/%	Total alcohol Selectivity/%	Long-chain alcohol selectivity/%	Total alcohols STY ^a	Long-chain alcohols STY ^a	reference
Cu ₄ Fe ₁	2	260	1	2400 mL g _{cat} ⁻¹ h ⁻¹	53.2	29.8	49.1	0.201	0.101	This work
CuZnFeMn	2	260	4	6000 h ⁻¹	52.62	31.04	3.65	0.24	0.016	<i>Catal. Commun.</i> 2008 , 9, 1869-1873
3DOM Cu ₂ Fe ₁	1	260	4.8	2000 h ⁻¹	57.5	33.6	52.4	0.20	0.100	<i>ChemCatChem</i> 2014 , 6, 473-478
CF _{0.5}	2	260	4	5000 h ⁻¹	17.99	20.77	2.5	0.05	0.001	<i>J. Colloid Interface Sci.</i> 2016 , 470, 162-171
CNF-2-0.005	1.5	240	5	32000 mL g _{cat} ⁻¹ h ⁻¹	11	39		0.53		<i>ACS Catal.</i> 2018 , 8, 9604-9618
CuFe NPs	2	220	6	6000 h ⁻¹	17.1	21.9	64	0.14	0.085	<i>J. Mol. Catal. A: Chem.</i> 2013 , 378, 319-325
0.5%K-FeCuMnZnO	2	260	4	6000 h ⁻¹	27.3	49.3	3	0.29		<i>Appl. Energy</i> 2015 , 138, 584-589
CoGa-ZnAl-LDO/ Al ₂ O ₃	2	260	3	2000 h ⁻¹	43.5	59	37.7	0.24	0.091	<i>J. Catal.</i> 2016 , 340, 236-247
CoMn CuZnAlZr	2	230	6	2000 mL g _{cat} ⁻¹ h ⁻¹	17.8	46.1	57.1	0.04	0.023	<i>Angew. Chem., Int. Ed.</i> 2019 , 58, 4627-4631
CoCu/MoO _x	1	270	4	120000 mL g _{cat} ⁻¹ h ⁻¹	<2	46		0.03		<i>Angew. Chem., Int. Ed.</i> 2014 , 53, 6397-6401
(Cu ₁ Co ₂) ₂ Al/CNT	2	230	3	3900 mL g _{cat} ⁻¹ h ⁻¹	45	62	13.8	0.34	0.05	<i>J. Mater. Sci.</i> 2016 , 51, 5216-5231
CuFeCo	2	350	5.5	6000 h ⁻¹	72	12.5	6	0.25	0.015	<i>Appl. Catal. A</i> 2015 , 503, 51-61

Fe/K/ Mo₂C(Fe/Mo= 1/14)	2	320	7	4000 h ⁻¹	50.25	22.69	0.62	0.14	0.001	<i>Catal. Lett.</i> 2010 , 136, 9-13
S2-CuFeMg-Cat	2	300	4	2000 h ⁻¹	56.89	49.07	11.25	0.28	0.032	<i>Catal. Sci. Technol.</i> 2013 , 3, 1324-1332
CuFeK0.5M	2	320	5	6000 h ⁻¹	53	61		0.32		<i>Fuel Process. Technol.</i> 2017 , 159, 436-441
Fe-CuMnZrO₂(I)	2	310	8	8000 h ⁻¹	45.5	26.2	3	0.45	0.014	<i>J. Mol. Catal. A: Chem.</i> 2004 , 221, 51-58
Fe-Cu/Al₂O₃ (Al₂O₃ loading: 89.3%)	2.68	380	4	10000 h ⁻¹		62.3		0.044		<i>J. Nat. Gas Chem.</i> 2008 , 17, 327-331
Cu-Fe-K-M₈₀	2	320	5	6000 h ⁻¹	56	63		0.35		<i>Energy Procedia</i> 2015 , 75, 767-772
Cu₂₀Fe₃₀K₁M	2	320	5	6000 h ⁻¹	46	53		0.35		<i>Catal. Today</i> 2014 , 234, 278-284
K-CoMoS₂/Al₂O₃	2	300	5	5000 h ⁻¹	9	47	47	0.30	0.141	<i>Energy Fuels</i> 2013 , 277, 3769-3777
Co₄Mn₁K_{0.1}	5	220	4	3600 h ⁻¹	34	44	22	0.20	0.044	<i>Nat Commun.</i> 2016 , 7, 13058-13064
CoCuMn	2	200	6	3600 h ⁻¹	3	52	65	0.12	0.078	<i>J. Am. Chem. Soc.</i> 2013 , 135, 7114-7117
Co₁Mo₁K_{0.05-12%} (4.2% Co/MWCNT)	2	290	5	8000 mL g _{cat} ⁻¹ h ⁻¹	21.1	85		0.33		<i>Appl. Catal. A</i> 2008 , 340, 87-97

^a g g_{cat}⁻¹ h⁻¹

Supplementary Table 10. Catalytic performances of Cu₄Fe₁ with three runs

Entry ^{a,b}	Conv. [%]	Selectivity[mol%]				Alcohols distribution[%] ^c				
		CH ₄	C ₂₊ H	ROH	CO ₂	MeOH	EtOH	PrOH	BuOH	C ₅₊ OH
1	53.2	3.7	36.5	29.8	30.0	8.7(2.6)	28.8(8.5)	8.2(2.4)	5.2(1.5)	49.1(14.8)
2	50.1	3.4	34.3	31.2	30.1	9.6(3.0)	29.6(9.2)	8.7(2.7)	6.4(1.9)	45.7(14.4)
3	51.2	2.3	38.6	28.0	31.1	7.5(2.1)	28.0(7.8)	8.1(2.3)	6.0(1.7)	50.4(14.1)

^a Activation conditions: 1 g precursor, H₂: CO: CO₂=1: 1: 2 (40 mL min⁻¹), 2 °C min⁻¹, 300 °C 2 h + 350 °C 1 h.

^b Reaction conditions: 1 MPa, 260 °C, H₂/CO=2, 2400 mL g_{cat}⁻¹ h⁻¹.

^c Normalized data to S_{ROH}, mol% in brackets.

Supplementary Table 11. Catalytic performances of samples with different preparation methods and composition

Catalysts ^{a,b}	Conv. [%]	Selectivity[mol%]				Alcohols distribution[%] ^c				
		CH ₄	C ₂₊ H	ROH	CO ₂	MeOH	EtOH	PrOH	BuOH	C ₅₊ OH
Cu ₄ Fe ₁	53.2	3.7	36.5	29.8	30.0	8.7(2.6)	28.8(8.5)	8.2(2.4)	5.2(1.5)	49.1(14.8)
Cu ₄ Fe _{1-co}	37.1	13.4	31.3	35.2	20.1	9.6(3.4)	79.6(28.0)	6.7(2.3)	2.4(0.8)	1.7(0.7)
Cu ₄ Fe _{1-im}	9.7	19.9	52.0	10.5	17.6	81.2(8.5)	9.6(1.0)	5.3(0.6)	3.9(0.4)	–
Cu ₄	5.9	23.1	2.1	70.5	4.3	92.0(64.8)	3.9(2.7)	2.7(1.9)	1.4(1.1)	–
Fe ₁	19.2	21.3	38.6	–	40.1	–	–	–	–	–
Cu ₄ /Fe ₁ ^d	7.8	25.5	21.7	27.6	25.2	85.6(23.6)	8.8(2.4)	5.6(1.6)	–	–
Cu ₄ +Fe ₁ ^e	6.2	21.7	47.8	15.0	15.5	89.1(13.3)	7.3(1.1)	3.6(0.6)	–	–
Fe ₁ +Cu ₄ ^f	6.5	27.3	34.3	19.6	18.8	90.6(17.7)	7.6(1.5)	1.8(0.4)	–	–

^a Activation conditions: 1 g precursor, H₂: CO: CO₂=1: 1: 2 (40 mL min⁻¹), 2 °C min⁻¹, 300 °C 2 h + 350 °C 1 h.

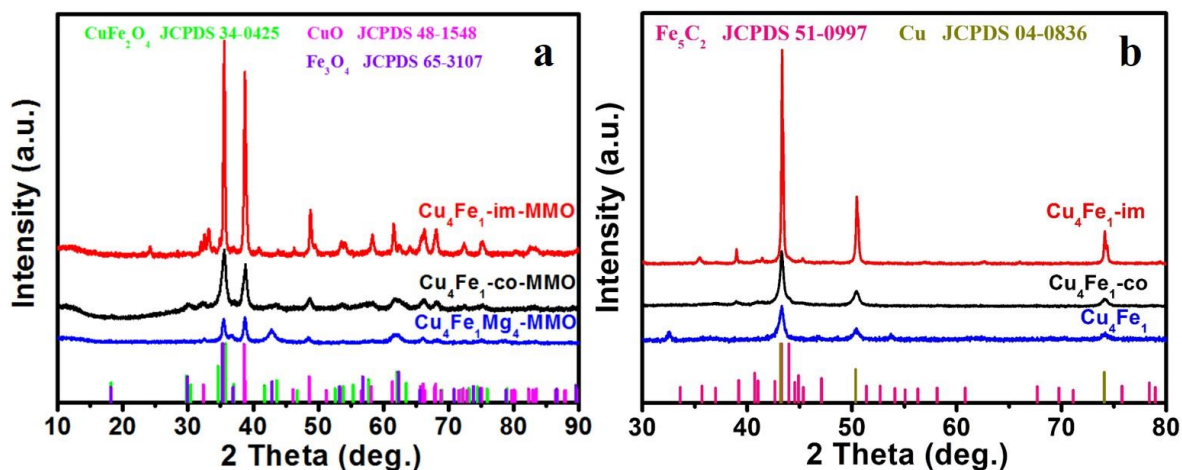
^b Reaction conditions: 1 MPa, 260 °C, H₂/CO=2, 2400 mL g_{cat}⁻¹ h⁻¹.

^c Normalized data to S_{ROH}, mol% in brackets.

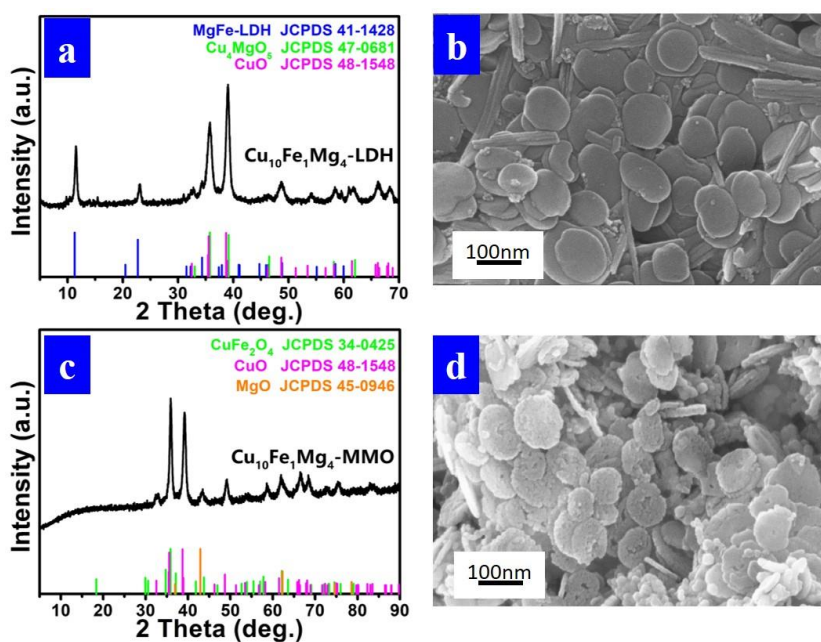
^d Physical mixture of Cu₄ and Fe₁

^e Fe₁ is located separately below Cu₄ by an inert layer of quartz wool.

^f Cu₄ is located separately below Fe₁ by an inert layer of quartz wool.



Supplementary Figure 6. Structure of control samples. XRD patterns of the calcined samples (a) $\text{Cu}_4\text{Fe}_1\text{-im-MMO}$, $\text{Cu}_4\text{Fe}_1\text{-co-MMO}$, $\text{Cu}_4\text{Fe}_1\text{Mg}_4\text{-MMO}$ and the reduced samples (b) $\text{Cu}_4\text{Fe}_1\text{-im}$, $\text{Cu}_4\text{Fe}_1\text{-co}$, Cu_4Fe_1 .



Supplementary Figure 7. Structure and morphology of $\text{Cu}_{10}\text{Fe}_1\text{Mg}_4\text{-LDH}$. XRD patterns of (a) $\text{Cu}_{10}\text{Fe}_1\text{Mg}_4\text{-LDH}$ precursors and calcined (c) $\text{Cu}_{10}\text{Fe}_1\text{Mg}_4\text{-MMO}$ precursors. SEM images: (b) $\text{Cu}_{10}\text{Fe}_1\text{Mg}_4\text{-LDH}$ and (d) $\text{Cu}_{10}\text{Fe}_1\text{Mg}_4\text{-MMO}$.

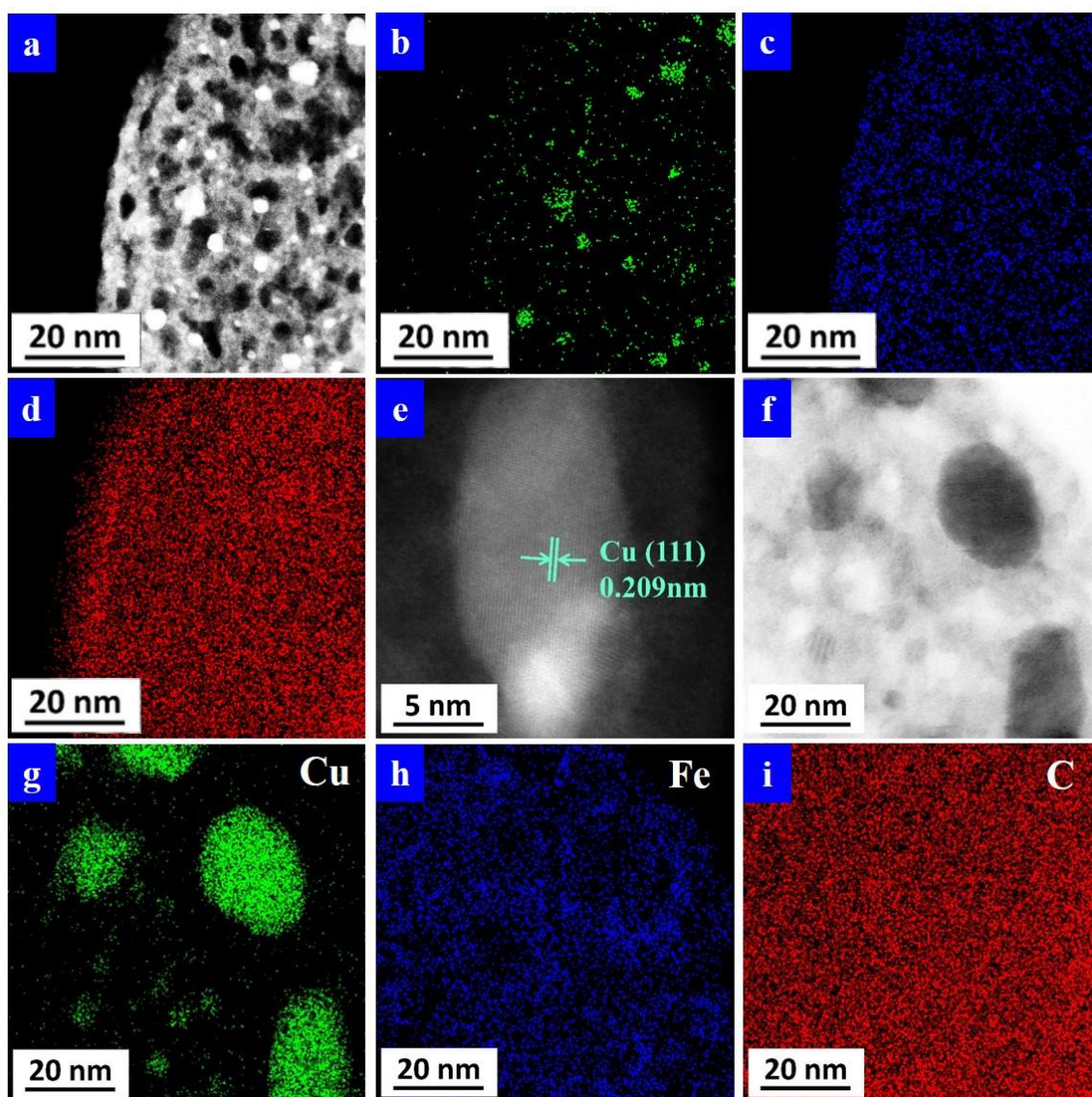
Supplementary Table 12. Catalytic performances of samples with Cu/Fe ratio 10/1

Catalysts ^{a,b}	Pressure [MPa]	Conv. [%]	Selectivity[mol%]				Alcohols distribution[%] ^c				
			CH ₄	C ₂₊ H	ROH	CO ₂	MeOH	EtOH	PrOH	BuOH	C ₅₊ OH
Cu ₁₀ Fe ₁	1	17.4	9.7	41.1	5.4	43.8	11.1(0.6)	21.2(1.1)	6.3(0.3)	3.2(0.2)	58.2(3.2)
	2	32.4	5.8	45.0	10.2	39.0	12.9(1.3)	25.5(2.6)	7.2(0.7)	3.6(0.4)	50.8(5.2)
	3	61.2	15.2	26.9	10.1	47.8	11.1(1.1)	24.0(2.4)	7.4(0.7)	4.1(0.4)	53.4(5.5)

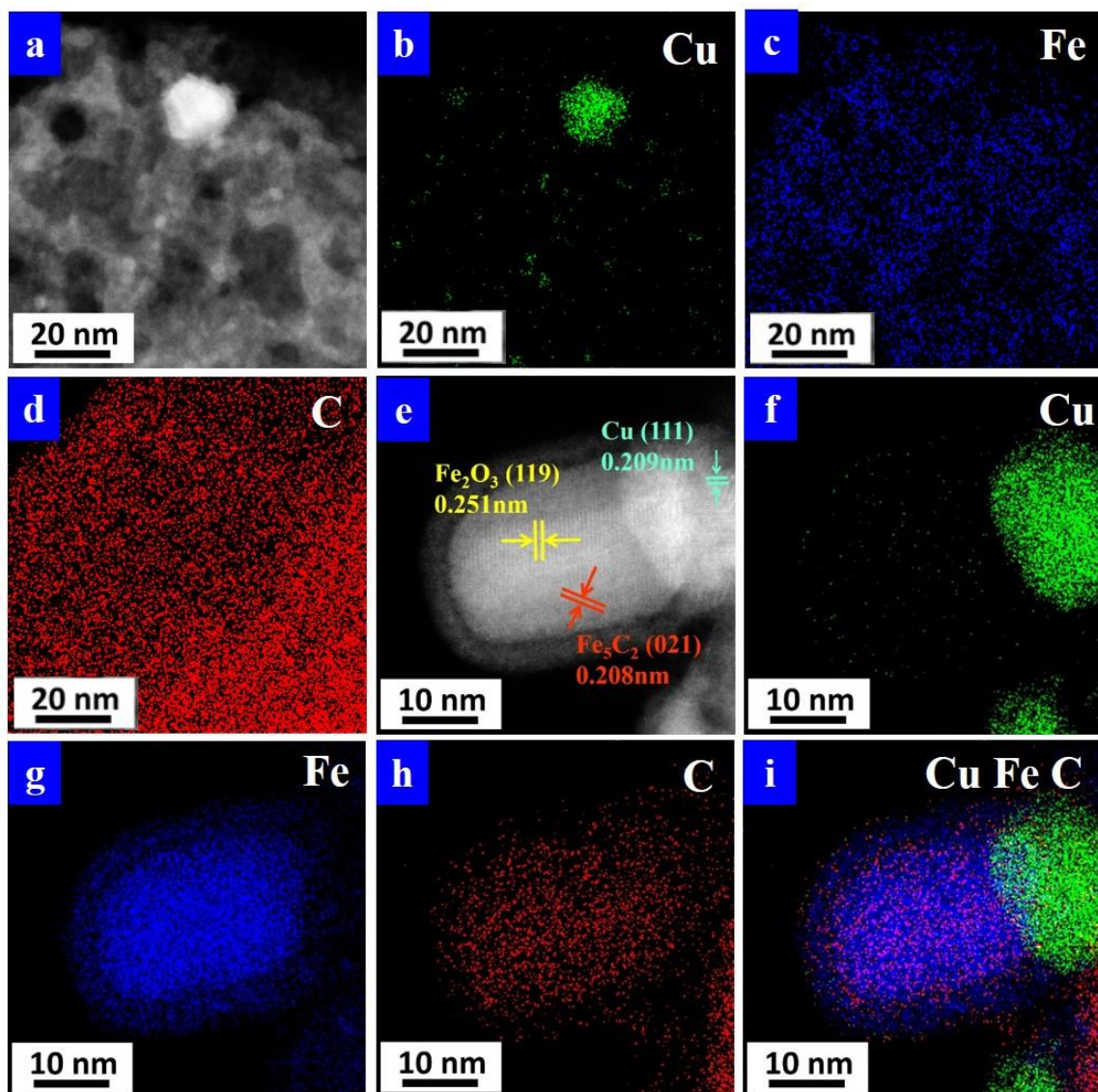
^a Activation conditions: 1 g precursor, H₂: CO: CO₂=1: 1: 2 (40 mL min⁻¹), 2 °C min⁻¹, 300 °C 2 h + 350 °C 1 h.

^b Reaction conditions: 260 °C, H₂/CO=2, 2400 mL g_{cat}⁻¹ h⁻¹.

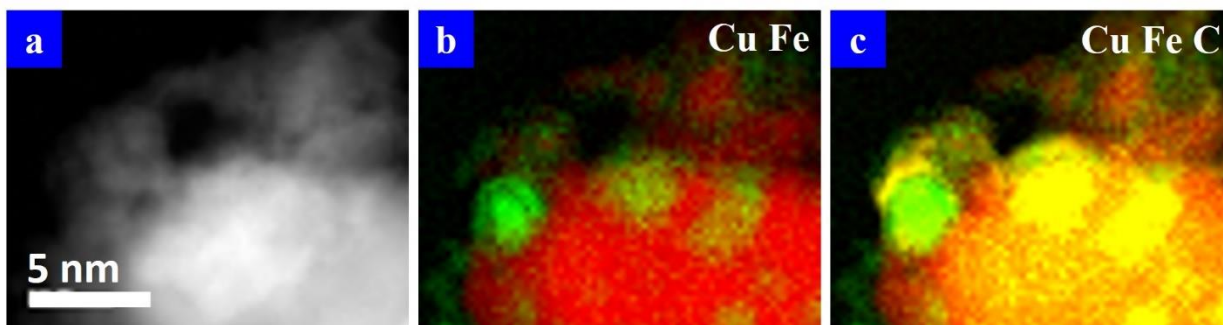
^c Normalized data to S_{ROH}, mol% in brackets.



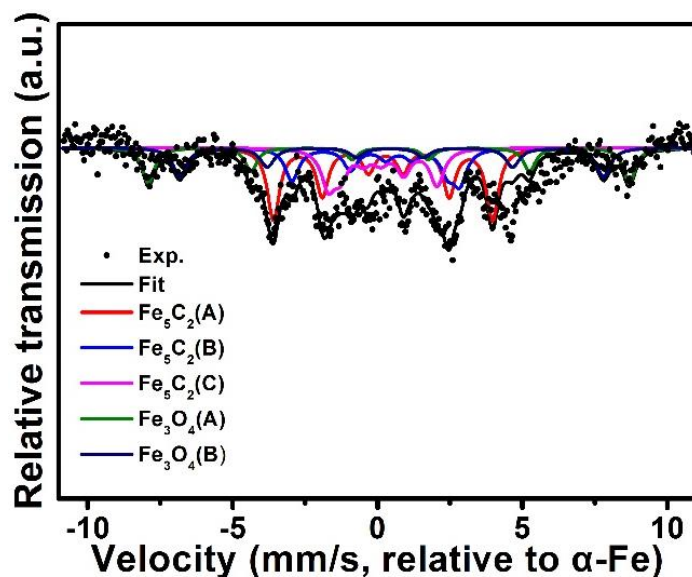
Supplementary Figure 8. Morphology of Cu_1Fe_1 catalyst. (a, e and f) TEM images of Cu_1Fe_1 catalyst (reduced and passivated). (b, c, d, g, h and i) EDS mapping of elemental distribution for Cu, Fe and C, respectively.



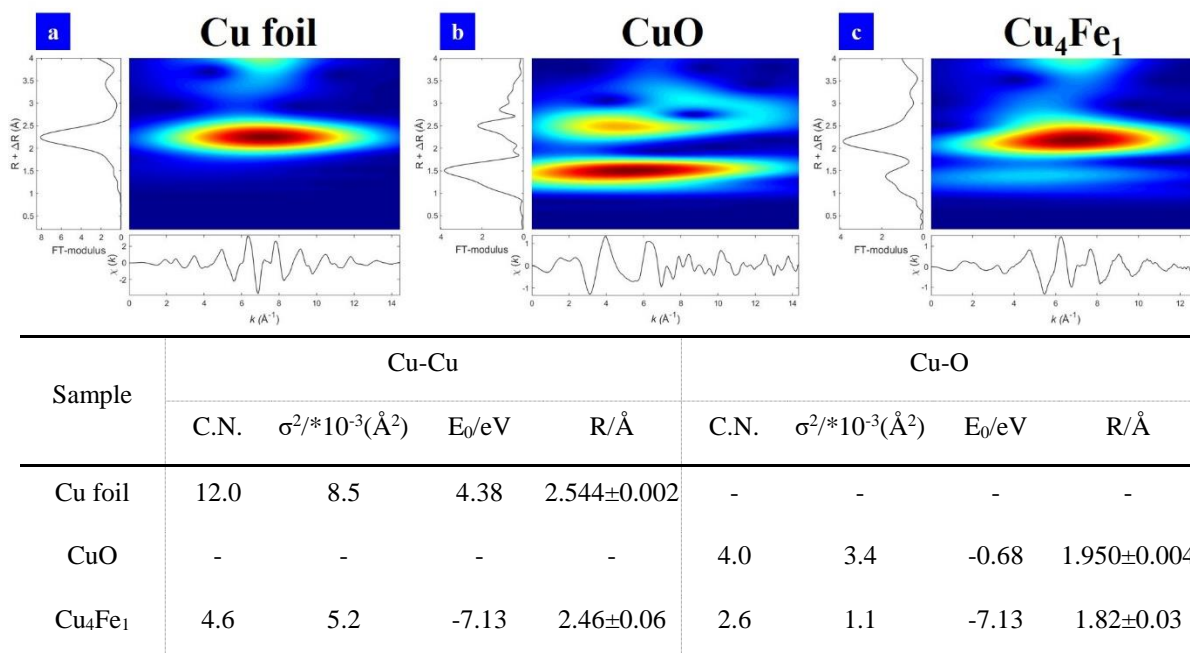
Supplementary Figure 9. Morphology of Cu_2Fe_1 catalyst. (a, e) TEM images of Cu_2Fe_1 catalyst (reduced and passivated). (b, c, d, f, g, h and i) EDS mapping of elemental distribution for Cu, Fe and C, respectively.



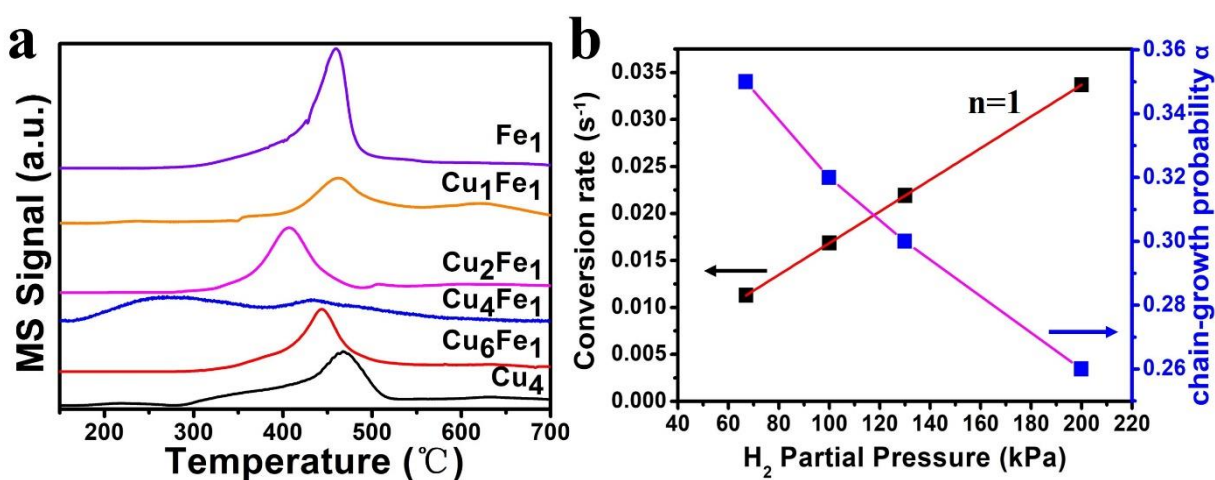
Supplementary Figure 10. Morphology of Cu_4Fe_1 catalyst. (a) HAADF-STEM image and (b, c) corresponding EELS mapping of Cu (red), Fe (green) and C (yellow).



Supplementary Figure 11. Mössbauer spectrum of Cu_4Fe_1 sample (reduced and passivated) (Exp.: experimental data; Fit: fitting data).



Supplementary Figure 12. Structure of Cu_1Fe_1 catalyst. Wavelet transformation of (a) Cu foil, (b) CuO and (c) Cu_4Fe_1 . The fitting results are listed in the table.



Supplementary Figure 13. H_2 activation of Fe_1 , Cu_4 and Cu_xFe_y samples. (a) H_2 -TPD profiles of Fe_1 , Cu_4 and Cu_xFe_y samples. (b) Kinetic orders of H_2 and the corresponding chain-growth probability at various H_2 partial pressures over Cu_4Fe_1 .