

Supporting Information (SI)

Enhanced removal of heavy metal ions from aqueous solution using manganese dioxide-loaded biochar: Behavior and mechanism

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The SI contains 12 total pages with 4 Figures.

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Figure captions:

Figure S1: (a) N₂ adsorption-desorption isotherms and (b) pore size distributions of the samples.

Figure S2: Fitting kinetics of heavy metal ions adsorption onto BC@MnO₂-26.6 using (a) the pseudo-first-order model, (b) the pseudo-second-order model and (c) the Webber-Morris model.

Figure S3: Effect of co-existing ions on heavy metal ions onto BC.

Figure S4: XPS spectra of BC@MnO₂-26.6 after the sorption of Cu(II), Cd(II) and Zn(II). (a) Cu 2p, (b) Cd 3d and (c) Zn 2p.

Sorption kinetic models:

The kinetic data of Pb(II), Cd(II), Cu(II) and Zn(II) sorption onto BC@MnO₂-26.6 were analyzed using two widely used kinetic models, the pseudo-first-order model, the pseudo-second-order model and the Webber-Morris model. The pseudo-first-order kinetic model is described as equation (1) [1]:

$$\log(q_e - q_t) = \log q_e - k_1 t \quad (1)$$

where q_e (mg g⁻¹) and q_t (mg g⁻¹) are the amount of Pb(II), Cd(II), Cu(II) and Zn(II) adsorbed at equilibrium and at time t (min), respectively. k_1 (min⁻¹) is the first-order sorption kinetic constant.

The pseudo-second-order equation is as following [2]:

$$\frac{t}{q_t} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} t \quad (2)$$

where q_e (mg g⁻¹) and q_t (mg g⁻¹) are adsorption capacities of Pb(II), Cd(II), Cu(II) and Zn(II) at equilibrium and at time t (min), respectively, and k_2 (g mg⁻¹ min⁻¹) is the second-order sorption rate constant.

The Webber-Morris model is described as equation (3) [3]:

$$q_t = k_{id} t^{1/2} + C_i \quad (3)$$

where q_t (mg g⁻¹) is the amount of adsorbed Pb(II), Cd(II), Cu(II) or Zn(II) at time t (min), k_i (mg g⁻¹ min^{-1/2}) is the diffusion rate constant and C_i is the intercept which provides an idea of the boundary layer thickness.

Langmuir isotherm model:

The isotherm data of Pb(II), Cd(II), Cu(II) and Zn(II) sorption onto adsorbents were fitted to the Langmuir model according to the equation (4) [4]:

$$\frac{C_e}{q_e} = \frac{1}{K_L q_m} + \frac{1}{q_m} C_e \quad (4)$$

where q_e (mg g^{-1}) is the amount of adsorbed metal at equilibrium, C_e (mg L^{-1}) is the equilibrium concentration of heavy metal ions in aqueous solution, q_m (mg g^{-1}) is the maximum adsorption capacity of heavy metals on adsorbents, K_L (L mg^{-1}) is a binding constant.

Thomas model:

The Thomas model is used to predict the column breakthrough capacities. The linearized form of the Thomas model is as equation (5) [5]:

$$\ln\left(\frac{C_{\text{in}}}{C_{\text{out}}} - 1\right) = \frac{k_{\text{Th}} q_m m}{Q} - k_{\text{Th}} C_{\text{in}} t \quad (5)$$

where C_{in} and C_{out} are the influent and effluent, respectively, k_{Th} is the Thomas rate constant ($\text{ml min}^{-1} \text{mg}^{-1}$), q_m is the maximum adsorption capacity (mg g^{-1}), Q is the flow rate (mg min^{-1}), m is the mass of adsorbent (g), and t is the adsorption time (h).

Mn(IV) content determination procedures:

Firstly, total Mn content was measured by dissolving 0.2 g of BC@MnO₂ sample in 50 ml of 0.25 mol L⁻¹ hydroxylamine hydrochloride, then the resulting Mn(II) content in the solution was diluted with water and was measured by atomic absorption spectrometry (AAS) (Perkin Elmer 2380, USA). Another 0.1 g of BC@MnO₂ sample was completely dissolved in 10 ml of 0.5 mol L⁻¹ H₂C₂O₄ and 10 ml of 1 mol L⁻¹ H₂SO₄ to reduce Mn(III) and Mn(VI) to Mn(II) at 75°C. The excess C₂O₄²⁻ was measured by back-titration with a standardized KMnO₄ solution. According to the results of above experiments, the Mn(IV) content in BC@MnO₂ adsorbent were calculated. All

chemical analyses for each sample were performed three times and the mean was recorded.

Figure S1

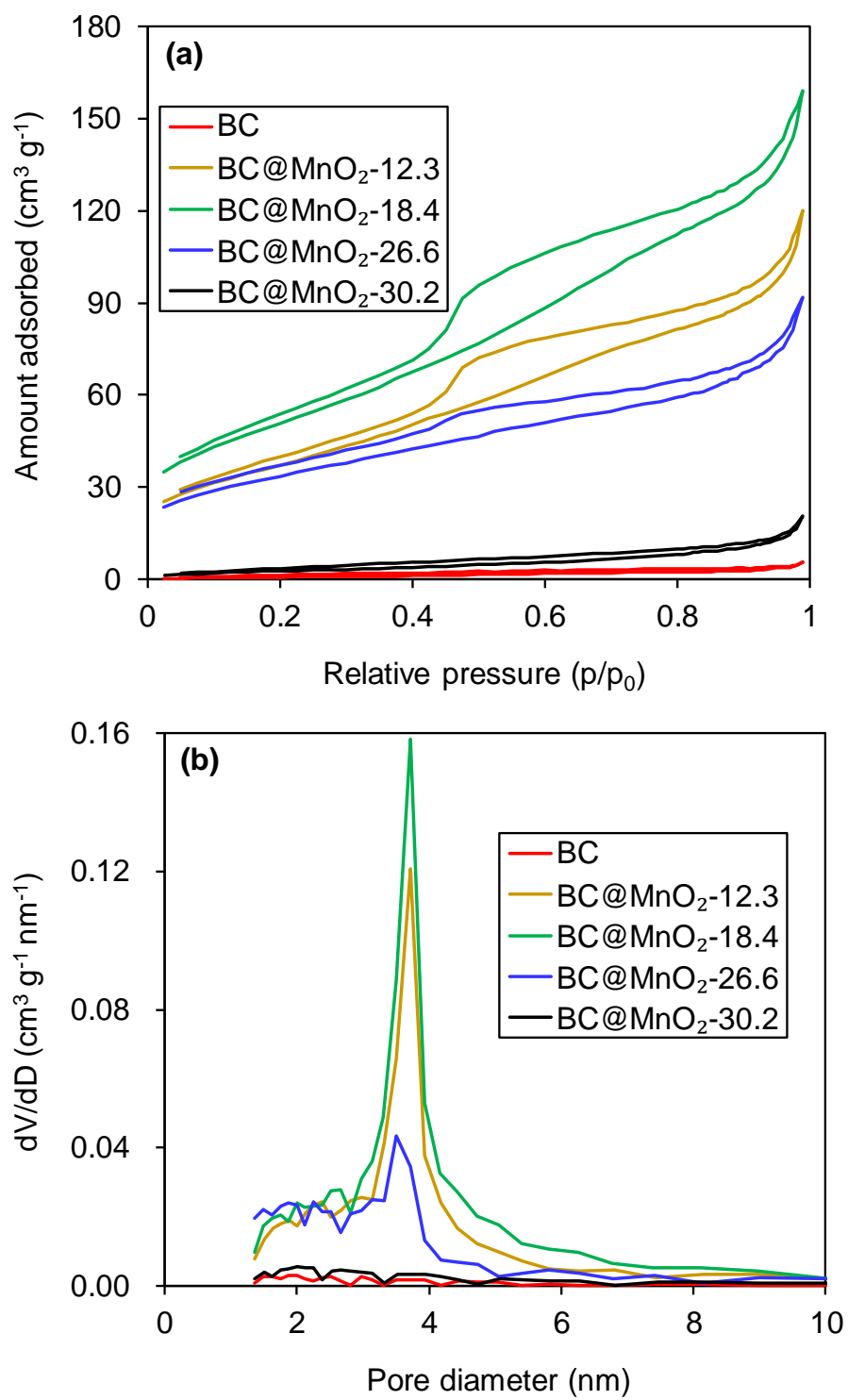
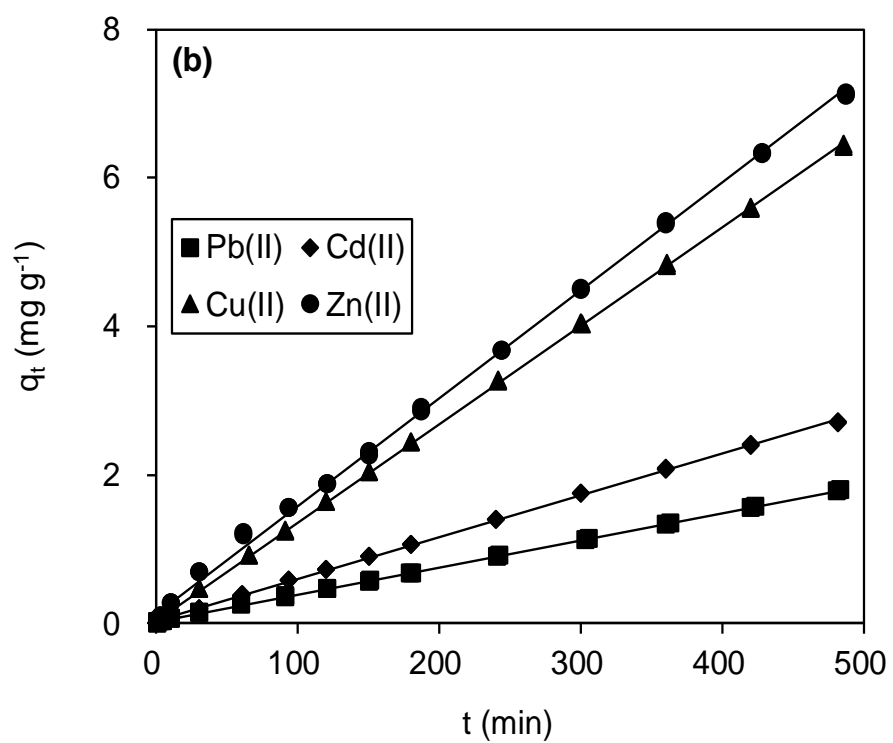
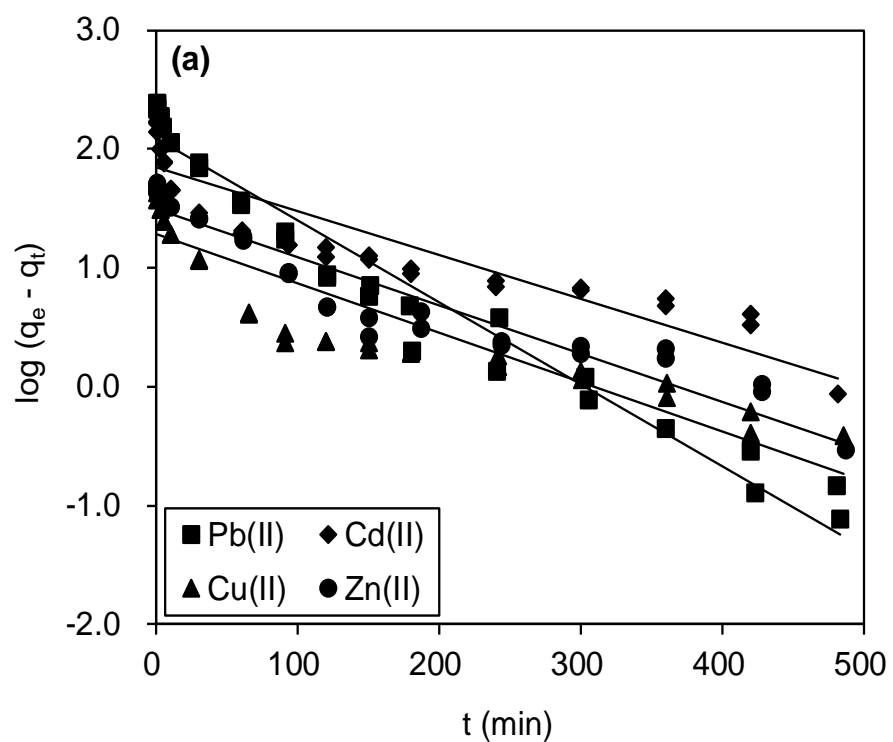


Figure S2:



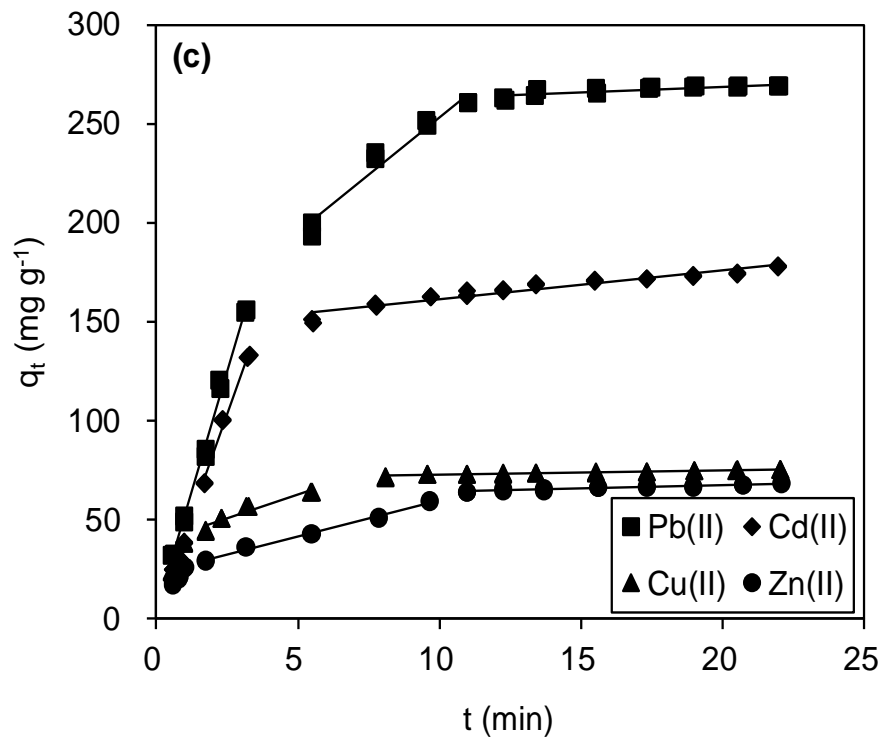


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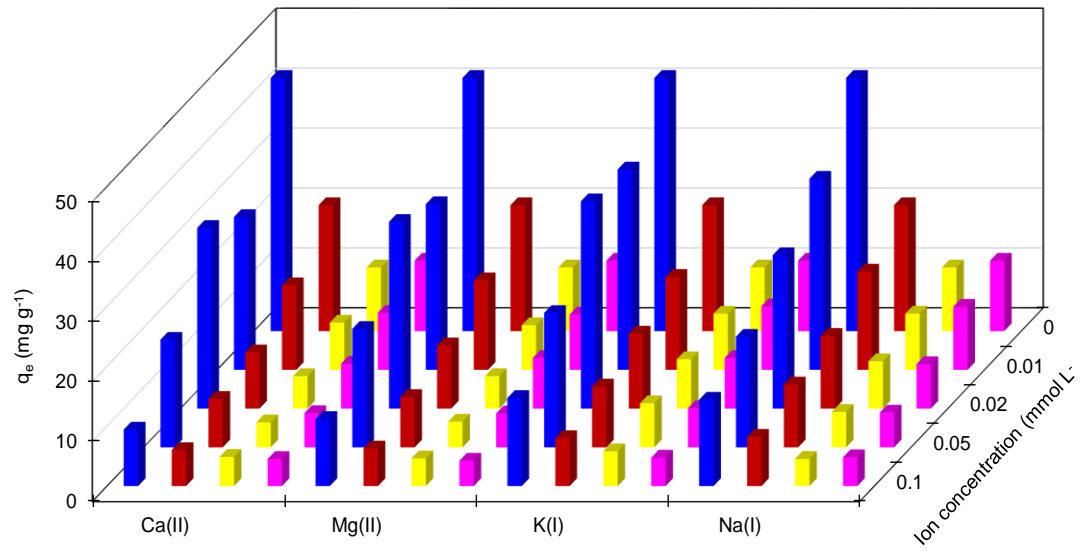
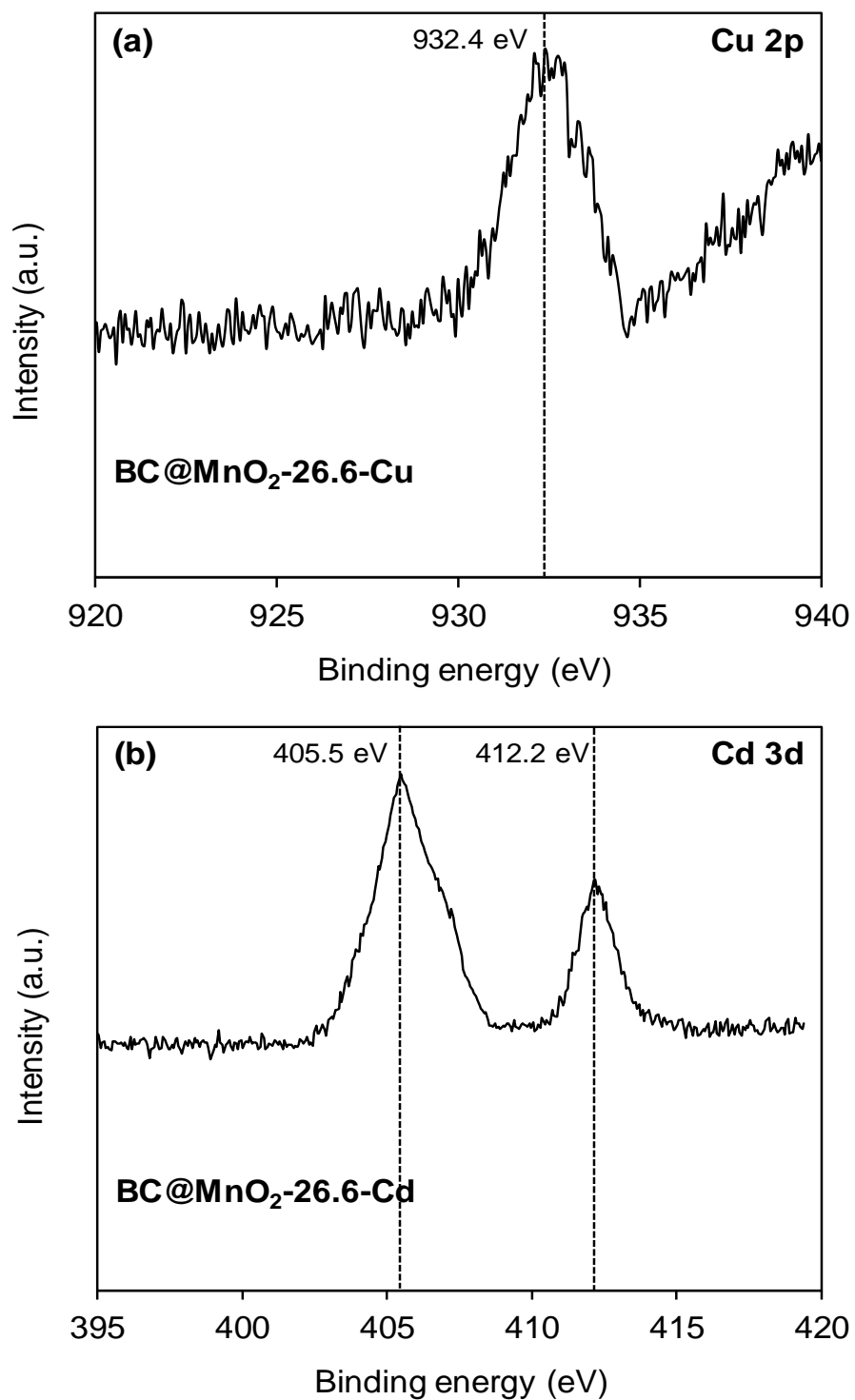
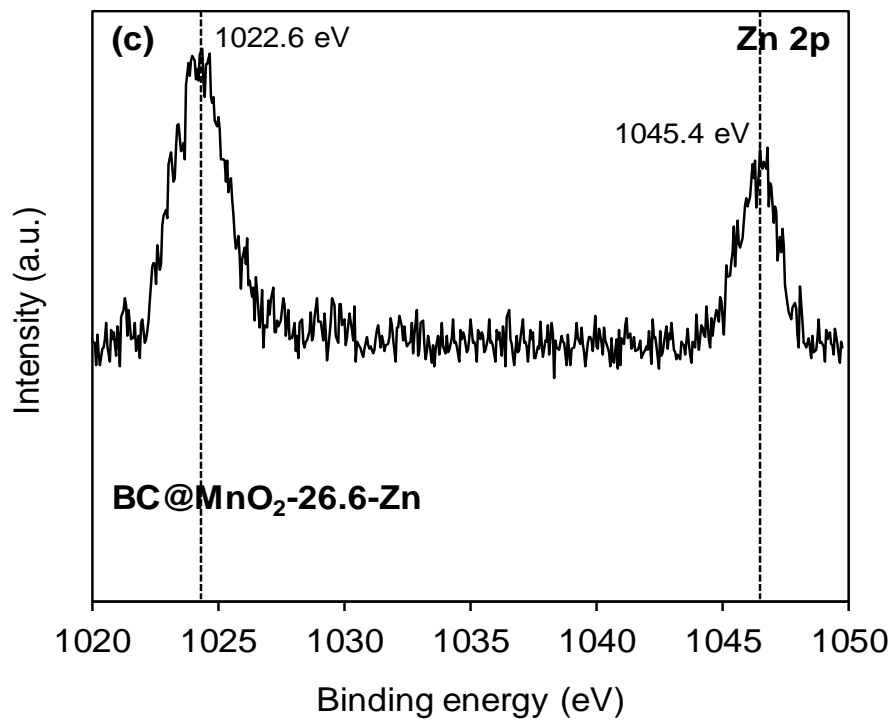


Figure S4:





References

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