

1 **Supplementary information: Flow-through stable isotope probing (Flow-SIP) minimizes**  
2 **cross-feeding in complex microbial communities**

3

4 **Supplementary text**

5 **Materials and experimental setup**

6 Schemes of the incubation setup of recirculated and flow-through approaches are shown in Figure 1.  
7 For the flow-through approach, the screw caps of the medium reservoir and the waste collection bottle  
8 were equipped with two ports, one for the tubing inlet and one for sterile pressure equalization using  
9 a membrane filter (0.2  $\mu\text{m}$ ). For the recirculated approach, a small bottle was used as medium reservoir  
10 with two ports, from which medium was withdrawn and recirculated back, respectively. For both  
11 approaches, the medium reservoir was connected to the top of the filter holder (stainless steel, 47  
12 mm, Sartorius) and a peristaltic pump was placed after the filter holder. To open and close the filter  
13 holder as well as to remove aliquots of the medium for chemical analysis during the incubation, a  
14 three-way valve was connected to the bottom of the filter holder. Material used for both recirculated  
15 and flow-through approaches are given in Table S1. All material except for the three-way-valves was  
16 sterilized by autoclaving, three-way valves were sterilized by rinsing in 70% ethanol and autoclaved  
17 distilled water. Mineral medium was prepared according to Palatinszky *et al.* [1], with some  
18 modifications: instead of 4 g L<sup>-1</sup> CaCO<sub>3</sub>, we used 0.01 g L<sup>-1</sup> (1 mM, as a calcium source), and, as substrate  
19 for autotrophic C-fixation, we added <sup>13</sup>C-NaHCO<sub>3</sub> (98 atom%) with a final concentration of 2 mM,  
20 resulting in a final <sup>13</sup>C-labelling percentage of approximately 66 atom%. For batch and recirculated  
21 incubations, 20 ml of medium were inoculated. We accounted for the dead volume of the filter holder  
22 and tubing (9 ml) and thus only 11 ml medium were added to the medium reservoir of the recirculated  
23 approach. In the flow-through incubations, approximately 624 ml of medium were supplied over 24 h  
24 (i.e., flow rate of 26 mL h<sup>-1</sup>).

25 Activated sludge was sampled from the nitrification basin of the municipal wastewater treatment plant  
26 Aalborg West (luftningstanke, Renseanlæg Vest), Denmark, on March 16<sup>th</sup> and 18<sup>th</sup>, 2016. Sludge was  
27 disrupted by sonication to yield single cells or colonies to reduce diffusive cross-feeding due to the  
28 large 3D-structure of the flocs. 20 ml aliquots of sludge (diluted 1:5 in mineral medium) were sonicated  
29 on ice for 120 s using 20% power and 1x cycle settings (Bandelin HD2200, probe MS73), and were  
30 allowed to settle for 10 min. The top 15 ml of the sludge suspensions, containing smaller flocs or single  
31 colonies and cells, were filtered through 20 µm nylon mesh membrane filters (Magna, Fisher Scientific)  
32 to remove residual large flocs. To remove residual substrates from the filtrate, cells were pelleted by  
33 centrifugation (20 min, 10°C, 4 200 g), supernatant was discarded, and cells were gently resuspended  
34 in mineral medium with <sup>12</sup>C-NaHCO<sub>3</sub> and without ammonium. To avoid the use of storage compounds  
35 during the incubation, cells were exposed to a starvation period of approximately 8 - 10 h before start  
36 of the incubation. To determine optimal cell density for the incubations, different volumes of  
37 sonicated, washed cells were filtered onto 0.2 µm filters, stained by DAPI and inspected by an  
38 epifluorescence microscope.

39 Under sterile conditions, support filters (for E1, glass fibre filters, Advantec, GC50, 47mm, and for E2  
40 nylon membrane filters Magna, Fisher Scientific, 47mm) and membrane filters (0.2µm polycarbonate,  
41 Nucleopore Whatman 47mm) were placed into filter holders (backpressure grids were omitted) fitted  
42 with a valve at the filter holder outlet. Filter holders were then filled bubble-free with mineral medium  
43 and closed off until cells were applied onto the filter membrane. Using syringes, sonicated, starved  
44 cells were gently filtered onto the membranes, discarding the flow-through. To ensure even settling of  
45 cells on the membrane surface, additional 20 ml mineral medium (with <sup>12</sup>C-NaHCO<sub>3</sub> and without  
46 ammonium) were gently pushed through the filter holder, discarding the flow-through. Shortly before  
47 the start of the incubation, the medium in the filter holder was replaced by medium containing <sup>13</sup>C-  
48 NaHCO<sub>3</sub> (but no ammonium). Filter holders were then connected to sterile tubing of the incubation  
49 setup (Figure 1). The same amount of biomass as in the recirculated and flow-through incubations  
50 were added to the batch incubations. At the start of the incubation, ammonium was added from a  
51 stock solution to batch incubation bottles and into the medium reservoir and fresh medium bottle of

52 the recirculated and flow-through approaches, respectively. Incubations were done in the dark for 24h  
53 at *in situ* temperature of the nitrification basin in Aalborg Vest (14°C). Immediately after the setup of  
54 the incubation, and after approximately 12, 18 and 24 h, subsamples were collected for concentration  
55 measurements of ammonium, nitrite and nitrate. In both flow-through and recirculated incubations,  
56 samples were collected at the filter holder outlet, and from batch incubations, bulk samples were  
57 collected, and cells were removed by centrifugation. Samples were stored at -20°C until analysis.

58 At the end of the incubation, filter holders were closed off using the valve at the filter outlet,  
59 disconnected from the tubing, and cells on the membrane filter inside the filter holders were fixed  
60 with formaldehyde (3% formaldehyde in 1x phosphate buffered saline; PBS). To avoid disturbing the  
61 cells' position on the membrane filter, 20 ml formaldehyde solution were gently pushed through the  
62 filter holders, thereby replacing medium. Filter holders were then closed using the valve connected at  
63 the filter holder outlet and incubated for 30 min at room temperature. Formaldehyde was removed  
64 by pushing 20 ml 1x PBS through the filter holder, followed by 20 ml distilled water. After pushing out  
65 all liquid, filter holders were disassembled, and membrane filters were air-dried and frozen at -20°C  
66 until FISH and nanoSIMS analyses. Batch incubation samples were also filtered on a membrane filter,  
67 fixed and stored the same way as the flow-through and recirculated samples.

68 Nitrification activity was monitored by ammonium consumption, and nitrite and nitrate production.  
69 Ammonium, nitrite and nitrate concentrations were quantified after 0, 12, 18 and 24 h by a  
70 colorimetric procedure as described in Hood-Nowotny *et al.* [2] and Garcia-Robledo *et al.* [3].

#### 71 **FISH and nanoSIMS analyses**

72 In addition to cells fixed after incubation, bulk activated sludge samples were fixed with formaldehyde  
73 as previously described [4]. These samples were used to screen for presence of nitrifier populations by  
74 FISH using probes for AOB (probes NEU, [5]; Nso1225, [6]; Nmv/Ncmob [7]; Ncom1025, [8]; Cl6a192,  
75 [9]) and NOB (Nit3, [5]; Ntspa1431 and Ntspa1151, [10]; Ntoga122, [11]). We detected AOB  
76 populations related to *Nitrosomonas oligotropha* (targeted by probe Cl6a192) and *Nitrosomonas*  
77 *eutropha/europea/urea* (targeted by probe NEU). We further detected *Nitrotoga*-affiliated NOB and

78 lineage 1 and 2 *Nitrospira* (targeted by probe Ntspa 1431 and 1151, respectively). Previous  
79 metagenomic analyses showed that WWTP Aalborg West does not harbor comammox *Nitrospira* [12,  
80 13], whose presence would have confounded the results of our study, as comammox *Nitrospira* are  
81 able to oxidize ammonia but are not distinguishable from the canonical lineage 2 *Nitrospira* by FISH.  
82 For all combined FISH and nanoSIMS analyses, we used probe mixes for AOB (Cl6a192 and NEU) and  
83 NOB (Ntoga122, Ntspa1431 and Ntspa1151).

84 Before FISH analysis, laser markings were made on membrane filters using a laser microdissection  
85 microscope (Leica LMD 7000, Germany). FISH on sections of the incubated filters was done as  
86 previously described by Daims [4]. All FISH probes were double labelled with FitC (AOB in E1; NOB in  
87 E2), Cy3 (NOB in E1), or Cy5 (AOB in E2) fluorophores [14]. We observed strong non-specific binding of  
88 the fluorophores, especially of Cy3 and Cy5, to the membrane filter surface. This non-specific binding  
89 was overcome by using CARD-FISH hybridization buffer [15] instead of normal FISH hybridization buffer  
90 in hybridizations of E1 samples. Filter sections of E2 were pre-incubated in 1:10 diluted blocking  
91 reagent before hybridization [15]. After FISH, cells were counterstained with DAPI before fluorescent  
92 images were acquired on a confocal laser scanning microscope (SP7, Leica, Germany, equipped with a  
93 white light laser).

94 For nanoSIMS analyses, selected filter sections were attached to antimony-doped silicon wafer  
95 platelets (7.1 x 7.1 x 0.11 mm, Active Business Company, Brunthal, Germany) by a commercially  
96 available superglue (Loctide®, Henkel, Ireland), and coated with AuPd thin films (30 nm nominal  
97 thickness) using a sputter coater (K550X Emitech, Quorum Technologies Ltd., Ashford, UK). In the flow-  
98 through incubations, a thin, yellow layer of salt crystals was formed on the filter membranes, which  
99 strongly reduced the conductivity of the sample surfaces upon sputtering with AuPd. To remove this  
100 layer prior to AuPd coating, we tested washing the filter membrane sections from experiment E2, flow-  
101 through incubation in either 1N HCl or 1N HNO<sub>3</sub> for 10 min. Both acid treatments successfully removed  
102 the yellow layer and rendered the samples sufficiently conductive for nanoSIMS analyses. We  
103 subsequently used HCl for washing all other samples. After acid treatment, samples were rinsed with  
104 water (Milli-Q, >18.2 MΩm, Millipore) and 70% ethanol. For maintaining comparability and to remove

105 possible  $^{13}\text{C}$ -bicarbonate contamination, samples on filter membranes from batch and recirculated  
106 incubations were also washed with 1N HCl in the same way.

107 NanoSIMS measurements were performed on a NanoSIMS 50L (Cameca, Gennevilliers, France) at the  
108 Large-Instrument Facility for Environmental and Isotope Mass Spectrometry at the University of  
109 Vienna. Prior to data acquisition, analysis areas were pre-sputtered utilizing a high-intensity, slightly  
110 defocused  $\text{Cs}^+$  ion beam (400 pA beam current,  $\sim 1,5 \mu\text{m}$  spot size). Data were acquired as multilayer  
111 image stacks by sequential scanning of a finely focused  $\text{Cs}^+$  primary ion beam (approximately 80 nm  
112 probe size at 2 pA beam current) over areas between  $36 \times 36$  and  $74 \times 74 \mu\text{m}^2$  at  $512 \times 512$  pixel image  
113 resolution and a primary ion beam dwell time of 5 to 10 ms/(pixel\*cycle). The detectors were  
114 positioned to enable parallel detection of  $^{12}\text{C}_2^-$ ,  $^{12}\text{C}^{13}\text{C}^-$ ,  $^{12}\text{C}^{14}\text{N}^-$ ,  $^{31}\text{P}^-$  and  $^{32}\text{S}^-$  secondary ions and the mass  
115 spectrometer was tuned to achieve a mass resolving power (MRP) of  $>9\,000$  (according to Cameca's  
116 definition) for detection of  $\text{C}_2^-$  and  $\text{CN}^-$  secondary ions, respectively.

117 NanoSIMS images were processed using the software WinImage version 2.0.8 (Cameca, France). Prior  
118 to stack accumulation, the individual images were aligned to compensate for positional variations  
119 arising from primary ion beam and/or sample stage drift. Secondary ion signal intensities were dead  
120 time corrected on a per-pixel basis. C isotope composition images displaying the  $^{13}\text{C}/(^{12}\text{C}+^{13}\text{C})$  isotope  
121 fraction, designated as  $^{13}\text{C}$  atom%, were inferred from the  $\text{C}_2^-$  secondary ion signal intensity  
122 distribution images via per-pixel calculation of  $^{13}\text{C}^{12}\text{C}^-/(2 \cdot ^{12}\text{C}_2^- + ^{13}\text{C}^{12}\text{C}^-)$  intensity ratios.

123 Regions of interest (ROIs), referring to individual cells, were manually defined utilizing the nitrogen-,  
124 phosphorus- and sulfur-related secondary ion signal intensity distribution maps as indicators of  
125 biomass and the respective FISH image. These ROIs were cross-checked by the  
126 topographical/morphological appearance of the sampled areas in secondary electron intensity  
127 distribution images that were recorded simultaneously with the secondary ion images. Statistical  
128 significance of the difference of the  $^{13}\text{C}$ -enrichment between groups within each approach was  
129 analyzed by the Kruskal-Wallis test followed by a non-parametric multiple comparison test (Dunn's  
130 test), using the R package "dunn.test" [16].

131 **Nitrite diffusion model**

132 In order to determine nitrite distributions surrounding the AOB colonies and to quantify the potential  
133 exchange rates with NOB colonies, the flow-condition around a single AOB colony on the Flow-SIP filter  
134 was simulated.

135 The steady-state Navier-Stokes equations are given by:

136

$$137 \quad \rho(\mathbf{u} \cdot \nabla)\mathbf{u} = -\nabla p + \mu \nabla^2 \mathbf{u}$$

138

139 With the continuity equation for incompressible fluids:

140

$$141 \quad \nabla \cdot \mathbf{u} = 0,$$

142

143 where  $\rho$  is the density,  $\nabla$  is the del operator,  $\mu$  the dynamic viscosity of water,  $p$  the pressure and  $\mathbf{u}$   
144 the velocity vector. The time-dependent advection-diffusion equation is given by:

145

$$146 \quad \frac{\partial C}{\partial t} = -D \nabla^2 C + \mathbf{u} \cdot \nabla C,$$

147

148 where  $C$  is the nitrite concentration and  $D = 1.7 \cdot 10^{-9} \text{ m}^2 \text{ s}^{-1}$  is the isotropic diffusion of nitrite. The  
149 equations were solved in the COMSOL Multiphysics® software.

150 Simulating the full 3-dimensional complexity as found on the Flow-SIP filter is numerically expensive  
151 and requires precise information about the cell and colony structures. Therefore, certain assumptions  
152 were made when generating the model domain. First, it is assumed that the AOB colonies are of  
153 spherical shape with a radius that can be estimated from measured volumes. For AOB colonies  
154 exceeding 50 cells, it was shown that the colony volume can be empirically described using:  $V_{col} =$   
155  $n_{cell}^{1.56} e^{-3.28}$ , where  $n_{cell}$  is the cell number [17]. For colonies with fewer cells no empirical relation  
156 exists. Therefore, the volume for 50 cells was linearly scaled down to a theoretical volume of a single

157 cell multiplied with the cell number:  $V_{col} = \frac{50^{0.56} e^{-3.28}}{50} \cdot n_{cell}$ , which is valid for 1-50 cells. Finally, within  
158 the domain the reactive, spherical AOB colony was centered in a cylinder. To minimize wall-effects,  
159 the radius of the cylinder was adjusted to 120  $\mu\text{m}$ , which is more than 20 times the radius of the AOB  
160 colony.

161 To mimic conditions of the experimental setup, a symmetric outer boundary with a constant inlet flow  
162 velocity  $U_0$  and a no-slip boundary condition along the colony's surface was assumed. The inflow  
163 nitrite-concentration was adjusted to 0  $\mu\text{mol l}^{-1}$ . To simulate the nitrite production of the AOB colonies,  
164 a constant normal flux ( $J_n$ ) was imposed at the surface of the colony, which was calculated based on  
165 the cell specific volumetric rates and normalized to the surface area:

166

$$167 \quad J_n = \frac{n_{cell} \cdot R_{cell}}{S_{col}}$$

168

169 With a cell specific volumetric rate of  $R_{cell} = 2.6 \text{ fmol cell}^{-1} \text{ h}^{-1}$  [17–20] and a surface area of  $S_{col} =$   
170  $4\pi r_{col}^2$ . The described approach reduces the decisive parameters to cell numbers and flow velocity.

171 In more than 200 stationary model runs ( $\frac{dC}{dt} = 0$ ), cell numbers were varied between  $n_{cell} =$   
172 5, 50, 500 cells and the imposed flow velocity was sequentially increased from  $U_0 = 0.1 - 100 \mu\text{m s}^{-1}$  in  
173  $1.25 \mu\text{m s}^{-1}$  steps.

174 Post-processing was performed in Matlab (Mathworks 2017b). Briefly, nitrite concentrations were  
175 extracted along the equator up to a distance of 100  $\mu\text{m}$  of the colony surface. This procedure was  
176 repeated for all imposed flow velocities and subsequently interpolated to an equidistant grid.  
177 Subsequently, contour lines were extracted.

178 Additionally, time-dependent nitrite accumulation around AOB colonies without flow ( $\mathbf{u} = 0$ ), i.e. in a  
179 diffusion-controlled system, were simulated in the same domain as described above. After a simulation  
180 time of 24 hours, nitrite profiles along the equator were extracted for 5, 50 and 500 cells (Figure S2).

181 **Supplementary references**

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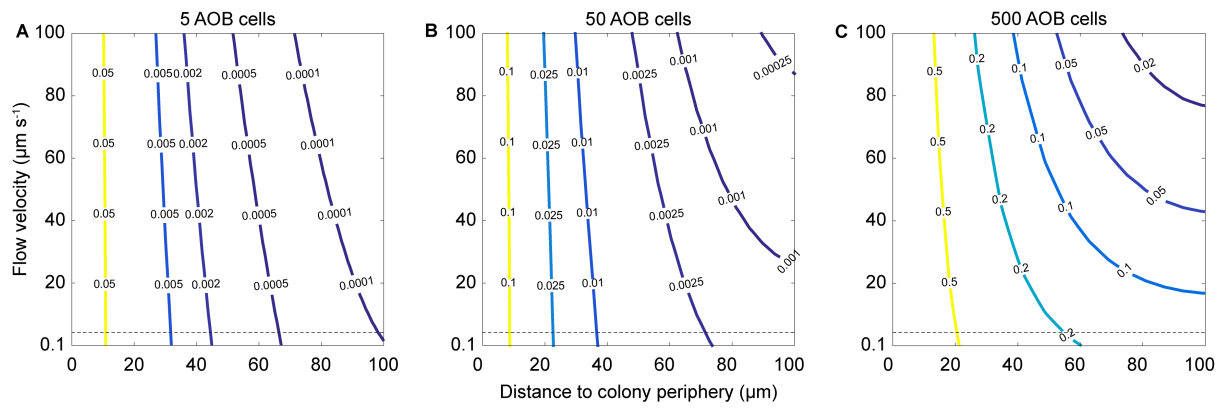


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- 238

239 **Supplementary figures**

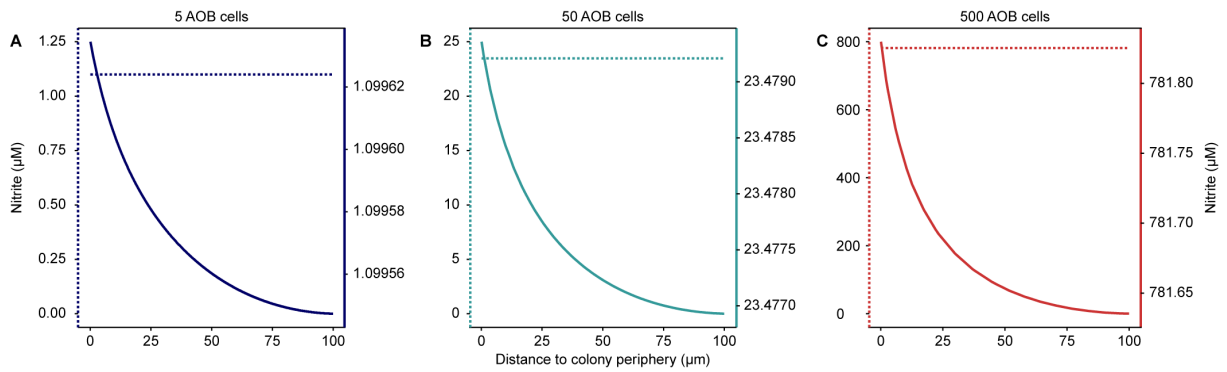
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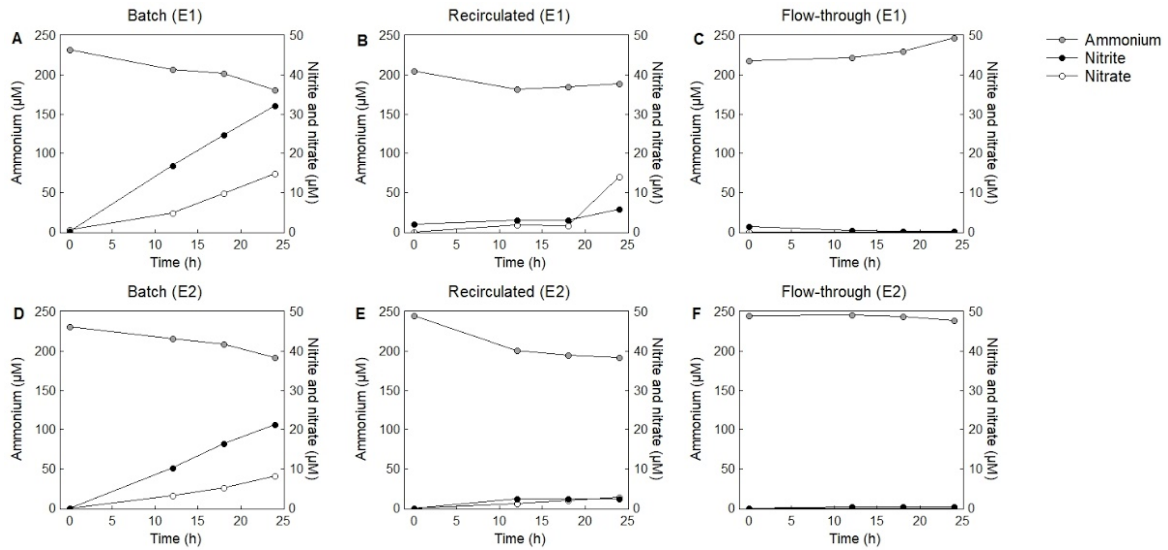
242 **Figure S1.** Nitrite diffusion model showing spatial distribution of nitrite concentrations ( $\mu\text{M}$ ) around  
243 AOB colonies on the membrane filter in the flow-through approach, considering different flow  
244 velocities from  $0.1 - 100 \mu\text{m s}^{-1}$ . The flow rate of  $26 \text{ ml h}^{-1}$  used in our experiment corresponds to a  
245 flow velocity of  $4.2 \mu\text{m s}^{-1}$  (horizontal dashed grey line). The model was run for three different AOB  
246 colony sizes, consisting of either (A) 5, (B) 50 or (C) 500 cells. We analyzed AOB colonies ranging from  
247 single cell to approximately 250 cells in our experiments. The distance to the periphery of an AOB  
248 colony of  $0 - 100 \mu\text{m}$  corresponds approximately to the distances between AOB and NOB colonies that  
249 we have observed. The contour lines represent nitrite concentration ( $\mu\text{M}$ ).

250



251

252 **Figure S2.** Spatial distribution of nitrite concentrations ( $\mu\text{M}$ ) in absence of any flow surrounding AOB  
253 colonies after 24h of incubation. The model was run for three different AOB colony sizes, consisting of  
254 either (A) 5, (B) 50 or (C) 500 cells. Note the different scales on the y-axes – the solid lines (right y-axis)  
255 were added to depict very minor changes in nitrite concentrations with distance to the AOB colony  
256 peripheries (solid lines). At distances of 0-100  $\mu\text{m}$ , modeled nitrite concentrations around AOB colonies  
257 were very stable. Specifically, predicted nitrite concentrations over this distance around AOB colonies  
258 consisting of 5 cells were approx. 1.1  $\mu\text{M}$ , around AOB colonies of 50 cells 23  $\mu\text{M}$ , and around AOB  
259 colonies of 500 cells 780  $\mu\text{M}$  after 24 h, as depicted by the dotted lines.



260

261 **Figure S3.** Nitrification activity in batch, recirculated and flow-through incubations of E1 (A-C) and E2

262 (D-F). Nitrification activity was monitored over the course of the incubation by ammonium

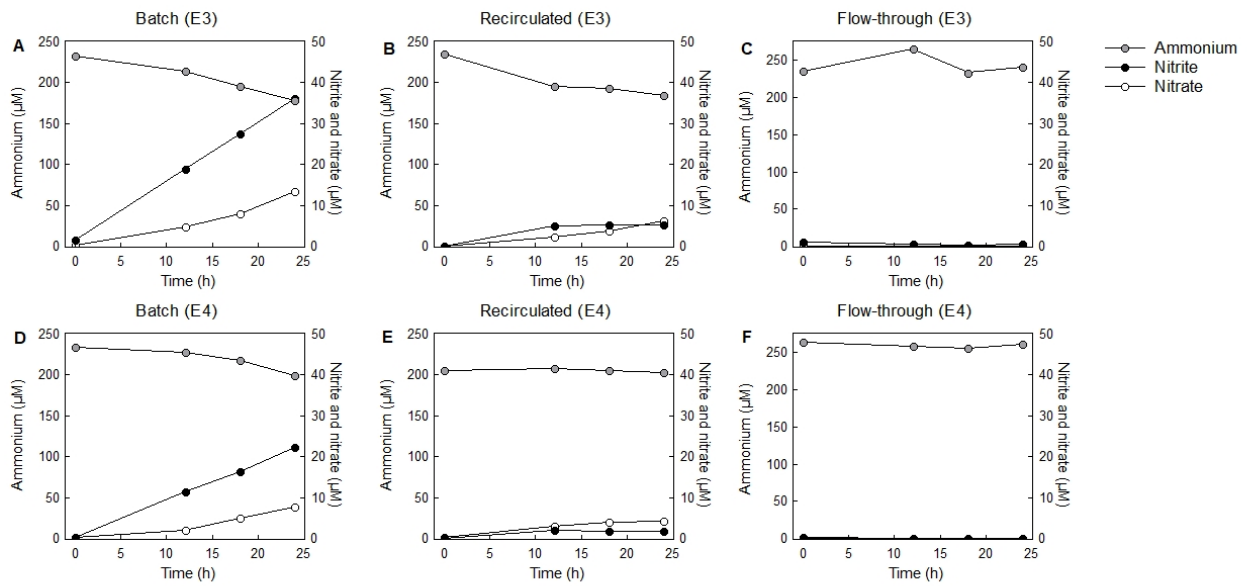
263 consumption, and nitrite and nitrate production. Note that the drop in the ammonium concentration

264 in the recirculated treatment between 0 and 12h was not due to ammonium consumption, but due to

265 dilution by ammonium-free medium that was present in the tubing and filter holder at the beginning

266 of the incubation. Nitrite and nitrate were not detectable in the flow-through incubation due to the

267 strong dilution by the constant medium supply.



268  
 269 **Figure S4.** Nitrification activity in batch, recirculated and flow-through incubations of two additional  
 270 experiments (E3 and E4) to further support reproducibility of the Flow-SIP method. Nitrification activity  
 271 was monitored over the course of the incubation by ammonium consumption, and nitrite and nitrate  
 272 production. Note that the drop in the ammonium concentration in the recirculated treatment between  
 273 0 and 12h was not due to ammonium consumption, but due to dilution by ammonium-free medium  
 274 that was present in the tubing and filter holder at the beginning of the incubation. Nitrite and nitrate  
 275 were not detectable in the flow-through incubation due to the strong dilution by the constant medium  
 276 supply.

277 **Supplementary tables**

278 **Table S1.** Material used in flow-through and recirculated approaches. Schemes of the setup of both  
 279 approaches are given in Figure 1.

Item	Comment	Manufacturer	Article number
Ismatec REGLO ICC digital peristaltic pump; 4-channel, 8-roller		Ismatec	ISM4408
Pump tubing, PharMed® Ismaprene, 1.6 mm inner diameter, 4.8 mm outer diameter, 1.6 mm wall thickness		Ismatec	MF0010
2-stop tubing, PharMed® Ismaprene, 1.65 mm inner diameter		Ismatec	SC0331
In-line stainless steel filter holder, 47 mm		Sartorius	16254
Luer lock connector for filter holders		Sartorius	16881
Whatman® Nuclepore™ Track-Etched Membranes; 47 mm diameter, 0.2 µm pore size, polycarbonate		Whatman	WHA111106
Advantec Grade GC50 Glass Fiber Filters, 47 mm diameter, 0.5 µm pore size	Support filter for E1	Advantec	GC5047MM
GVS Life Sciences Magna™ Nylon Membrane Filters, 47 mm diameter, 0.5 µm pore size	Support filter for E2, Nylon provides a smoother filter surface than the glass fibre support filters used for E1	GVS	1213776
Glass bottle, 1.5 cm inner diameter, 10 cm height, GL25 thread	Medium reservoir for recirculated incubations; custom-made		

280

281 **Table S2.** Test of statistical significance of differences in <sup>13</sup>C-enrichment between microbial groups  
 282 within each approach and differences between approaches within each microbial group. Shown are  
 283 results of Kruskal-Wallis test and non-parametric multiple comparison test (Dunn's test, see pairwise  
 284 comparisons column); \*P < 0.05, \*\*P < 0.01, \*\*\*P < 0.001, n.s. not significant.

Within approach		Kruskal-Wallis Test			Dunn's Test, pairwise comparison		
		$\chi^2$	df	P-value	AOB – NOB	NOB – other cells	AOB – other cells
E1	Batch	182.6	2	< 0.001	***	***	***
	Recirculated	134.7	2	< 0.001	***	***	***
	Flow-through	65.1	2	< 0.001	***	n.s.	***
E2	Batch	185.4	2	< 0.001	***	***	***
	Recirculated	193.8	2	< 0.001	***	***	***
	Flow-through	327.6	2	< 0.001	***	n.s.	***

Within microbial group		$\chi^2$	df	P-value	Pairwise comparison		
					Batch – Recirc.	Recirc. – Flow-thr.	Batch – Flow-thr.
E1	AOB	157.0	2	< 0.001	***	*	***
	NOB	184.5	2	< 0.001	***	***	***
	Other cells	7.9	2	0.019	*	*	n.s.
E2	AOB	375.0	2	< 0.001	***	***	***
	NOB	98.2	2	< 0.001		***	***
	Other cells	20.3	2	< 0.001	***	***	n.s.

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