# Supplementary Information

Probabilistic Thermodynamic Analysis of Metabolic Networks

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### 1 Methods

#### 1.1 Probabilistic Metabolic Optimization (PMO)

We solved PMO problems using the Gurobi Optimizer v9.0.1 (Gurobi Optimization, Beaverton, OR). Eq. (1) summarizes the constraints:

$$
\mathbf{t} := \begin{bmatrix} \ln c \\ \Delta_{\mathbf{r}} \mathbf{G}'^{\circ} \\ \Delta_{\mathbf{r}} \mathbf{G}' \end{bmatrix} = \mathbf{Qm} + \mu_{\mathbf{t}}
$$
  
\n
$$
\|\mathbf{m}\| \leq \chi_n^2(\alpha)
$$
  
\n
$$
\mathbf{S} \cdot \mathbf{v} = 0
$$
  
\n
$$
\mathbf{lb} \leq \mathbf{v} \leq \mathbf{ub}
$$
  
\n
$$
M_f \mathbf{d} - \mathbf{v_{con}} \leq 1 \cdot (M_f - \epsilon_f)
$$
  
\n
$$
M_f \mathbf{d} - \mathbf{v_{con}} \geq 1 \cdot \epsilon_f
$$
  
\n
$$
M_r \mathbf{d} + \Delta_{\mathbf{r}} \mathbf{G}' \leq 1 \cdot (M_r - \epsilon_r)
$$
  
\n
$$
M_r \mathbf{d} + \Delta_{\mathbf{r}} \mathbf{G}' \geq 1 \cdot \epsilon_r
$$

Here, the vector of integers **d** in  $\{0,1\}^{\gamma}$  denotes if a reaction has positive (1) or negative (0) flux and the relationship between free energies and fluxes has been rewritten in the  $Biq-M$  formulation [20].  $M_f (M_r)$  are the big-M values and  $\epsilon_f$  ( $\epsilon_r$ ) are the minimum magnitudes for fluxes (reaction energies). These values must be chosen carefully as  $Big-M$ constraints are often a source of numerical errors. In most cases, the range of coefficients should not span more than 9 orders of magnitude. We choose  $M_r = 1000 \frac{kJ}{mol}$  as it is larger than the  $\Delta_r G^{\prime\circ}$  of any reaction in the model and  $\epsilon_r = 0.1 \frac{kJ}{mol}$  since smaller values imply high enzyme cost and are thus unlikely. For fluxes, we set  $M_f$  larger than the highest flux magnitude (1000 in iML1515-CAN) and  $\epsilon_f = 10^{-8} \cdot M_f$ . Additionally we set the Gurobi parameters FeasibiltyTol =  $10^{-9}$  and IntFeasTol =  $10^{-9}$  to ensure that sign constraints are not violated.

The objective depends on the application: for quantitative assessment of the models we minimize  $\|\mathbf{m}\|_2$  (i.e. we maximize the probability of **), while for searching initial points for the sampler we maximize and minimize reaction** fluxes. We used  $\alpha = 0.95$  as confidence level.

The matrix  $\bf{Q}$  and the vector of z-scores **z** of a solution **m** are computed from the truncated eigenvalue decomposition of  $\Sigma_{\rm t}$ 

$$
\Sigma_{\mathbf{t}} = \mathbf{U}\Lambda \mathbf{U}^{\mathsf{T}} \approx \mathbf{U}_{\mathbf{q}} \Lambda_{\mathbf{q}} \mathbf{U}_{\mathbf{q}}^{\mathsf{T}} = \mathbf{U}_{\mathbf{q}} \Lambda_{\mathbf{q}}^{1/2} \cdot \left( \mathbf{U}_{\mathbf{q}} \Lambda_{\mathbf{q}}^{1/2} \right)^{\mathsf{T}} , \qquad (2)
$$

where U is an orthogonal matrix containing the eigenvectors of  $\Sigma_t$  and  $\Lambda$  is a diagonal matrix containing the eigenvalues of  $\Sigma_t$ . U<sub>q</sub> and  $\Lambda_q$  are submatrices of U and  $\Lambda$  that represent eigenvectors and eigenvalues for which the eigenvalue is larger than  $10^{-3}$ . Given the decomposition,  $\mathbf{Q} = \mathbf{U}_{\mathbf{q}} \Lambda_{\mathbf{q}}^{-1/2}$  and  $\mathbf{z} = \mathbf{U}_{\mathbf{q}} \mathbf{m}$ .

#### 1.2 Thermodynamics and Flux Sampling (TFS)

The algorithm for sampling  $\mathcal T$  (see main text) relies on the ability to quickly verify whether an orthant in thermodynamic space is feasible, i.e. there is a steady state flux solution that satisfies the directionality constraint of the orthant. We achieve fast feasibility verification with the following optimizations:

1. First, we test a simple condition that is necessary but not sufficient at steady state: for each metabolite, there must be at least one in-flux and one out-flux. This is the case when the system of equations

$$
|\mathbf{S} \cdot sign(\mathbf{v})| < \sum_{j} |\mathbf{S_j}| \,, \tag{3}
$$

where  $S_i$  are the columns of  $S$ , is satisfied.

- 2. We maintain a fixed-size cache  $(10^5 \text{ entries})$  with Least Recently Used (LRU) policy that stores the results of the linear program. If a set of directions has been already tested and the result is present in the cache, we use the result directly without calling the solver.
- 3. If Eq. (3) and the cache cannot determine the feasibility of an orthant, we verify feasibility with a linear program

$$
\begin{array}{ll}\n\max_{\mathbf{v}} & \mathbf{0} \\
\text{s.t.} & \mathbf{S} \cdot \mathbf{v} = 0 \\
& \text{lb}_{\text{orth}} \le \mathbf{v} \le \text{ub}_{\text{orth}} \,,\n\end{array} \tag{4}
$$

where the  $\cdot$ <sub>orth</sub> subscript indicates the original flux bounds restricted to the directions of the orthant. The optimization problem can be solved quickly because (1) setting the objective to zero, the solver only needs to find one feasible point instead of the optimum and (2) we reuse the same model object for each orthant and only modify the flux bounds. This way the solver can use information from the previous solution.

For each simulation on iML1515-CAN we run 200 chains (starting from different modes of the thermodynamic space) for  $2 \cdot 10^8$  steps. The first half of the random walk is treated as warm-up and discarded. From the remaining steps, we collect at regular intervals a total of  $10^5$  samples of  $\Delta_r G'$  and  $10^8$  direction samples. We then use the samples of  $\Delta_{\mathbf{r}}\mathbf{G}'$  to conditionally sample metabolite concentrations and  $\Delta_{\mathbf{r}}\mathbf{G}'^{\circ}$ . However, due to memory requirements it is more efficient to characterize the probability of each orthant using the signs of the reversible reactions only. These are stored efficiently in a hashmap were the keys are binary serializations of the sign pattern of the reversible reactions and the values indicate the number of times an orthant was sampled.

#### 1.2.1 Validation

We implemented two samplers for TFS: A non-convex, non-uniform sampler for  $\mathcal T$  and a convex uniform sampler based on Coordinate Hit and Run with Rounding (CHRR) for sampling orthants of  $\mathcal F$ . The samplers are implemented in C++, and elementary operations (ray-polytope intersections, ray-ellipsoid intersection, sampling from 1D uniform distribution, sampling from 1D truncated normal distribution) are covered by unit tests. To verify that the implementations sample from the correct distributions we performed a set of validations against established approaches:

- 1. Uniform sampling: we uniformly sampled the *e-coli-core* model and iML1515-CAN (growth on glucose) using our implementation and the COBRA Toolbox implementation. We used the same number of chains, samples, warmup steps and total steps for both implementations. Figure SI 2 shows that the two implementations have similar convergence properties and predict the same distributions.
- 2. Multivariate Normal (MVN) sampling: we sampled MVN distributions of different dimensions with random means and covariances using our implementation and the built-in MATLAB function mvnrnd. Figure SI 3 shows that samples generated with our sampler are as good as samples generated using mynrnd.
- 3. **Sampling of**  $\mathcal{T}$ : we sampled a toy network using TFS and a simple rejection-based approach. In the latter, we generated random samples of free energies using mvnrnd and then used a simple linear program (based on the constraints in Eq. (1), where the integer variables are already fixed by the reaction energies) to reject samples that did not satisfy the steady state condition. Figure SI 4 shows that, for the toy network, both implementations generate comparable sets of samples. In this example with only five internal reactions, the rejection rate was 88.2%. We can assume that each additional irreversible reaction reduces the steady-state thermodynamic space by half, thus doubling the number of rejections, and the example shows that reversible reactions increase the number of rejections as well. Thus, rejection sampling quickly becomes prohibitive even for core models and cannot be used to evaluate results obtained with TFS on iML1515-CAN. However, the comparison on the toy network combined with the asymptotic guarantees of hit-and-run [2] and the practical convergence results (Section SI 3.1) suggest that TFS samples the thermodynamic space correctly even for large models such as iML1515-CAN.
- 4. Sampling the flux space in TFS: since sampling of the flux space is achieved by uniformly sampling multiple orthants independently, this step is validated through point (1).

#### 1.3 Models

The condition-specific models used in the analysis (iML1515-CAN) were generated with the following steps:

1. We used NetworkReducer 's lossy reduction [5] allowing removal of the reactions, metabolites in the following subsystems: Cell Envelope Biosynthesis, Glycerophospholipid Metabolism, Lipopolysaccharide Biosynthesis / Recycling, Membrane Lipid Metabolism, Cofactor and Prosthetic Group Biosynthesis, Folate Metabolism, Murein Biosynthesis, Murein Recycling. Additionally, we allowed for removal of transport and exchange reactions for

metabolites that are present exclusively in the subsystems above. During reduction, we protected the model's capability of reproducing the measured growth and exchange rates. Reducing the level of detail in these subsystems was necessary to make the model computationally tractable and to ignore parts of the network where the thermodynamic model could be unreliable (e.g. different phase and poorly defined metabolites in lipid metabolism).

- 2. We manually removed/lumped reactions that only participate to secretion of metabolites or energy-wasting loops in the subsystems above.
- 3. We removed reactions related to oligosaccharides (glycogen and maltose) as their production and degradation form unfeasible cycles at steady state and the annotated directionalities are thermodynamically inaccurate.
- 4. PFK 3 and FBA3 were removed to make fluxes in the pentose phosphate pathway comparable to the 13C estimates.
- 5. We integrated experimental data (metabolite concentrations when required and measured growth/exchange rates).
- 6. The model was further reduced using NetworkReducer lossless compression. We protected all reactions in carbon, amino acid and nucleotide metabolism, which we believed were the most important in the growth conditions (minimal media).
- 7. As we require non-zero flux through all reactions modeled with thermodynamic constraints, we removed all blocked reactions.

The resulting models maintain an intact description of carbon, amino acid and nucleotide metabolism. Intracellular metabolomics data were only used for model assessment (glucose and acetate conditions) and in the  $M+$  conditions. In all conditions we set extracellular concentrations according to the composition of M9 media.

### 2 Thermodynamic assessment of iML1515-CAN

Table SI 1 lists the irreversible reactions that we had to make reversible to avoid thermodynamic inconsistencies. The same inconsistencies were found in all growth conditions. Table SI 2 shows the anomalies found for the growth on glucose and acetate, together with the explanation we found based on literature and the curation steps. We curated the model only in presence of support from literature. It is possible that some of the irreversibility annotations that we removed during the curation process were added to the model because it is known that  $E$ , coli does not actively use these reactions in the opposite direction. This is an intentional choice, as thermodynamic reversibility and regulatory choices are two different kinds of constraints. While knowledge of the preferred direction of a reaction can be added on top of a thermodynamically constrained model (e.g. for further reducing the number of modes predicted by TFS), this should not be used as a thermodynamic constraint.

Solving the PMO optimization problem took a time varying between 1 and 4 minutes on a Intel® i7-8700K processor depending on the growth condition and whether the results of the curation were applied or not.

### 3 Sampling iML1515-CAN

#### 3.1 Convergence and performance

For all six conditions, the random walks satisfied recommended convergence metrics [6] (split-R  $\leq 1.1$  and  $ESS < 5 \cdot n_c$ ) where  $n_c$  is the number of chains). Note that we computed these statistics on the split-chains, meaning that, after discarding the warm-up steps, we split each chain in two halves and treated each half as a chain. This is recommended to detect systematic trends in the chains. After sampling the thermodynamic space, we randomly selected  $10<sup>4</sup>$  modes according to their probabilities and used our implementation of CHRR to sample their flux spaces. The number of flux samples drawn for each orthant was proportional to its probability.

Table SI 3 shows a comparison of the runtimes of Uniform Sampling (US) and TFS sampling a core model and iML1515-CAN. Benchmarks were executed on our HPC cluster consisting of 26 nodes, each equipped with two Intel® Xeon® E5-2697 processors (year 2013, 12 cores at 2.70 GHz) and 128 GB of memory. On this system we used 8 cores when sampling the core model and 200 cores when sampling iML1515-CAN. We chose to simulate 200 chains (one per core) for iML1515-CAN to have higher chances of detecting issues in their convergence. However, this is not a general requirement and fewer chains can be simulated on smaller systems, as long as there is sufficient confidence that the sampler is not missing large portions of the space (e.g. for models as large or smaller than iML1515-CAN and with a similar fraction of reversible reactions). TFS simulations take significantly longer than US, increasing the runtime from a few minutes to almost a day for iML1515-CAN. Most of the runtime of TFS was spent simulating hit-and-run, a task that unfortunately can not be parallelized for individual chains. However, sampling a core model required less

than 5 minutes, suggesting that sampling models containing few hundred reactions is computationally affordable on simple desktop computers. Moreover, the runtime depends mostly on the dimensionality of the thermodynamics space and less on the dimensionality of the flux space. If an application requires investigation of specific areas of the network only, one can apply thermodynamic constraints only to the corresponding reactions, resulting in faster simulations.

### 3.2 Prediction of directions and flux distributions

Table SI 4 shows the number of orthants in each condition. These cover a wide range of behaviors, which reflect on the flux distributions of individual reactions (Figure SI 5, Figure SI 6). Interestingly, US overlooks many of the capabilities of the network. This is likely an artifact of representing the flux space with a polytope. In high dimensions, most of the volume lies in the center of the space and orthants that only appear close to the boundary of the polytope are too unlikely to be found, independent of their thermodynamic probability.

Table SI 5 summarizes the results of the validation of precision and accuracy of US and TFS against 13C estimates. However, 13C estimates have limited coverage and there were several cases where US and TFS predicted the irreversibility of a reaction but in different directions. We manually validated the predicted directions using EcoCyc [11] (Table 6 and 7) and found that in all verifiable cases TFS predicts the correct direction.

### 3.3 Prediction of metabolite concentrations

For comparisons against TMFA we used the matTFA [16] implementation, modified to use  $\Delta_{\mathbf{r}}\mathbf{G}^{\prime\circ}$  estimates from eQuilibrator. We constrained the estimates of metabolite concentrations and  $\Delta_{\mathbf{r}}\mathbf{G}^{\prime\circ}$  to their 95% confidence interval. Figure SI 7 shows the predicted TFS distributions and Thermodynamics-based Metabolic Flux Analysis (TMFA) ranges for each metabolite with measured concentration. TMFA could not constrain the concentration of any of those metabolites. This is consistent with the results obtained by the authors of TMFA, which showed constrained metabolite ranges only assuming no error in the standard reaction energies [9].

# 4 Supplementary figures and tables



Reaction	Reason
ACCOAL	Enforces unfeasible internal cycle.
ACt4pp	Conflicts with ACt2rpp and NAt3pp.
GLYCLTt4pp	Conflicts with GLYCLTt2rpp and NAt3pp.
PPAt4pp	Prevents excretion of propionate, enforcing an unfeasible internal cycle.
PPCSCT	Enforces unfeasible internal cycle.
PROt4pp	Conflicts with PROt2rpp and NAt3pp.
PTA2	Enforces unfeasible internal cycle.

Table SI 2: Interpretation of the PMO results. NA denotes values that are not available because the metabolite was removed after model curation.



Table SI 2: Interpretation of the PMO results. NA denotes values that are not available because the metabolite was removed after model curation.

Metabolite		$z$ -score		Concentration (mM)	Explanation		
	Before	After	Before	After			
$5caiz_c$ 5aizc_c	2.0 $-2.0$	ΝA 0.0	14.6 0.004	NA $\rm 0.25$	We hypothesize channeling of 5caiz_c between AIRC2 and AIRC3, since the respective enzymes purK and purE have been shown to bind in $E.$ coli [17]. Note that this is controversial [15]. Action: Convert AIRC2 and AIRC3 to the lumped reaction AIRC2_AIRC3.		
$O2_{-}C$	$-1.7$	$-1.7$	0.008	0.008	Expected. Limited by extracellular o2 concentration. Action: None.		
$3pg-c$ $3$ php_ $c$	$1.6\,$ $-1.6$	0.26 $-0.26$	6.4 0.010	0.42 $\rm 0.15$	PGCD alone is thermodynamically unfavorable. SerA has been shown to couple 3pg dehydrogenation to akg reduction in <i>Pseudomonas</i> . The same mechanism is likely employed by $E.$ coli as well [22]. Action: Make PGCD reversible. Add reactions for the proposed mechanism: $3pg_c + akgc \rightleftharpoons$ $3php_c + r2hglut_c$ and $akg_c + q8h2_c$ $\implies$ $r2hglut_c + q8_c$ .		
$acg5p_c$ acglu.c	$-1.5$ $1.5\,$	0.0 ΝA	0.012 $5.2\,$	$\rm 0.25$ NA	Channeling of acglu between ACGS and ACGK has been shown experimen- tally in S. cerevisiae [1], we hypothesize a similar mechanism in E. coli. $Ac$ - tion: Convert ACGS and ACGK to the lumped reactions ACGS_ACGK.		
$glu5p_c$	$-1.5$	ΝA	0.012	NA	Channeling of glu5p from GLU5K to G5SD is experimentally supported in E. coli [14]. Action: Convert GLU5K and G5SD to the lumped reaction $\mathrm{GLU5K\_G5SD}.$		
$4$ abut_ $c$ sucsal_c	1.5 $-1.5$	0.0 ΝA	5.1 0.013	$\rm 0.25$ NA	Physical interaction between the enzymes catalyzing ABTA and SSAL <sub>x</sub> has been shown experimentally in mitochondria [8]. We hypothesize a similar interaction in E. coli leading to channeling of sucsal for both SSALx and SSALy. Action: Convert ABTA, SSALx and SSALy to the lumped reactions ABTA_SSALx and ABTA_SSALy		
$ser\_L_c$ 2amsa.c	1.5 $-1.5$	0.0 ΝA	4.7 0.014	0.25 NA	Artifact of the steady-state constraint. 2amsa is a required intermediate for the synthesis of D-serine from L-serine. However, it is unlikely that E. coli actively synthesizes D-serine as it is not involved in any cellular function. Ac- tion: Remove 2amsa <sub>c</sub> and ser <sub>compare</sub> to avoid imposing unrealistic constraints on the concentration of L-serine.		
succoa_c $coa_c$ $sl2a6o_c$ thdp <sub>-c</sub>	1.3 $-1.2$ $-1.1$ 1.1	0.60 $-0.33$ 0.0 ΝA	$3.2\,$ 0.0245 0.027 2.4	0.83 0.13 $\rm 0.25$ NA	Inaccuracies in group contribution estimates. DHDPS is a ring-forming re- action synthesizing 23dhdp, which is then converted to thdp. THDPS then opens the thdp ring, forming sl2a6o. Both 23dhdp and thdp are not in- volved in any reaction in TECRDB, thus their formation energy must be estimated from group contribution, which is known to be unreliable for ring al- terations $ 4 $ . <b>Action:</b> Ignore the ring thermodynamics by replacing DHDPS, DHDPRy and THDPS with the lumped reaction DHDPS_DHDPRy_THDPS.		
ptrc_c $4$ abutn_ $c$	1.3 $-1.2$	1.1 $-1.1$	$3.1\,$ 0.021	$2.3\,$ 0.027	STRING predicts possible binding between PatA an PatD. However, we could not find further evidence supporting substrate channeling between the two enzymes. Action: None.		
$\mathrm{gcald}_c$ 4hthr_c $gly_c$	$1.1\,$ $-1.1$ 1.1	0.20 ΝA 0.0	2.5 0.026 2.5	0.39 NA 0.25	As 4hthr does not participate in any essential pathway and its maximum flux is very low, the validity of the constraints from the directions of 4HTHRA and 4HTHRK is questionable. <i>in-vivo</i> those may be affected by transport and dilution. Action: Remove 4HTHRA and 4HTHRK to avoid imposing unrealistic constraints on the concentration of glycine.		
acon_c	$-1.0$	$-1.0$	0.030	0.030	(1) Citrate dehydratase is an unfavourable reaction, while the previous step (citrate synthase) is predicted to be highly favourable $(\Delta_r G' - 40.5 \frac{kJ}{mol})$ , suggesting channeling of citrate between the two reactions. Indeed there is experimental evidence for a mitochondrial enzyme complex including malate dehydrogenase, citrate synthase and aconitase $[3, 21]$ . We hypothesize a simi- lar interaction in $E.$ coli, leading to the channeling of oxaloacetate and citrate. (2) It is not clear whether aconitate is channeled between the two aconitase steps, since it must be released from the enzyme and turn $180^{\circ}$ before binding again. [13] We conservatively assume it is. <b>Action:</b> Add lumped reactions for the potential channels (1) MDH <sub>-to-CS</sub> , CS <sub>-to-ACONT</sub> , MDH <sub>-to-ACONT</sub> and (2) ACONTa_ACONTb.		
	Additional metabolities with concentration $\geq 10mM$ for growth on glucose.						
$cl\_p$	0.57	$0.3\,$	75.5	6.0	The annotated irreversibility of CLt3 <sub>-2pp</sub> is thermodynamically inaccurate and implies high periplasmic concentrations of cl.L. <b>Action:</b> Make CLt3.2pp reversible.		
$glu$ <sub>--L</sub> $p$	0.46	0.0	26.2	0.25	The annotated irreversibilities of GLUt4pp, GLUABUTt7pp and ABUTt2pp are thermodynamically inaccurate and imply high periplasmic concentrations of glu <sub>rbarr</sub> Make GLUt4pp, GLUABUTt7pp and ABUTt2pp re- versible.		

Additional metabolites with  $|z| \geq 1$  for growth on acetate.

Table SI 2: Interpretation of the PMO results. NA denotes values that are not available because the metabolite was removed after model curation.

Metabolite	$z$ -score		Concentration (mM)		Explanation
	Before	After	<b>Before</b>	After	
$glyc_c$ $g3p_c$ $dha_c$	$2.2\,$ $-1.5$ 1.4	0.36 $-1.7$ $-0.36$	19.9 0.012 4.2	0.52 0.007 0.12	Glucone ogenesis appears unfavourable at the given intracellular concentra- tions. <i>in-vivo</i> , unfavourable reactions could be overcome by substrate chan- neling (see main text). To make unfavourable reactions feasible, they would need to be coupled with favourable steps (PPCK and FBP). <b>Action:</b> Based on evidence from literature and predicted requirements we hypothesised two complexes performing substrate channeling: (1) PPCK, ENO, PGM, PGK, GAPD, TPI (or any subset starting from PPCK) and (2) FBP, FBA, TPI (or any subset starting from FBP). The thermodynamics of glycolysis is highly influenced by magnesium ions [19], currently not accounted for by eQuili- brator. While it is likely that some form of channeling involving FBP and PPCK occurs in the pathway, the exact composition of the enzyme complexes is hard to determine. The predicted complexes are thus possibly larger than the actual ones.
$ac_{-}c$	$1.5\,$	1.3	4.8	3.6	Plausible given the growth condition. Action: None.
$g1p_c$	$-1.2$	$-1.2$	0.022	0.023	STRING predicts possible binding between Pgm an Pgi, but we could not find further literature evidence supporting substrate channeling between the two enzymes. Moreover, glucose-6-phosphate isomerase operates close to equilib- rium, thus substrate channeling between the two enzymes would not bring any thermodynamic advantage. Action: None.
sucgsa <sub>_c</sub> sucorn_c	$-1.0$ 1.0	$-0.87$ 0.87	0.032 2.0	0.044 1.4	STRING predicts possible binding between AstC an AstD, however we could not find further literature evidence supporting substrate channeling between the two enzymes. Action: None.



Figure SI 1: Overview of the predicted reaction energies in gluconeogenesis. The concentrations of the metabolites highlighted in orange, as well as all cofactors other than CO2 and phosphate were constrained by measurements. Phosphate is constrained to literature values. Reactions predicted to be unfavorable are shown in red. An example of hypothetical net reactions caused by substrate channeling is shown in blue.



Figure SI 2: Comparison between our implementation of CHRR (PTA) and the implementation in the COBRA Toolbox (CT) for the e<sub>colication</sub> and iML1515-CAN (growth on glucose) models. (A) Both implementations have similar convergence properties, as shown by the Potential Scale Reduction Factors (PSRFs). (B, C) Both implementations predict the same mean and standard deviation for the probability distribution of each flux. (D) Kolmogorov-Smirnov (KS) distance between the distributions predicted by the two implementations for each flux.



Figure SI 3: Validation of our sampler for MVN distributions. For samples obtained with our sampler (PTA) and with the built-in MATLAB function mvnrnd we compare  $(A)$  the Mahalanobis distance between the true means and the means estimated from samples and (B) the Frobenius norm between the true covariance and the covariance estimated from the samples, normalized by the Frobenius norm of the true covariance. Error bars represent the standard deviation over 10 replicates, each with random mean and covariance.



Figure SI 4: Validation of TFS sampling the thermodynamic space of a hypothetical toy network (left). The four metabolites (glucose 6-phosphate (g6p), glucose 1-phosphate (g1p), fructose 6-phosphate (f6p), fructose 1-phosphate (f1p)) have similar formation energies, thus all reaction energies are distributed around zero. However, steady state imposes additional constraints on the reaction energies. For example, if conversion of g6p to f1p through reactions A and B is favourable, then conversion through D and C must be favourable as well. We show the distribution of the samples for each reaction energy (diagonal) and pair of reaction energies (off-diagonal) predicted by our sampler (PTA, blue) and by a simple rejection sampling approach (RS, orange).

Table SI 3: Runtime of TFS (including individual steps of the pipeline) and US. Benchmarks show the average over the six  $M+$  conditions for iML1515-CAN and a core model based on e\_coli\_core and modified to include reactions for the measured exchanges [7]. For both models, the number of reactions for TFS and US differ because some results of thermodynamic curation would have allowed additional internal or ATP-generating cycles and were thus not applied for US.

	e_coli_core (modified)	iML1515-CAN	
Number of cores	8	200	
Number of chains	100	200	
Number of reactions (US)	$89 - 92$	$864 - 871$	
Number of reactions (TFS)	$101 - 104$	$875 - 883$	
<b>TFS</b>	$4 \text{ min } 43 \text{ s} + 7 \text{ s}$	$23h$ 46 min $+54$ min	
Sampling $\mathbf{\Delta}_r \mathbf{G}'$	$4 \text{ min } 22 \text{ s} + 4 \text{ s}$	$19h$ 47 min $+$ 47 min	
• Finding initial points	$29s+4s$	$4 h 3 min + 33 s$	
• Iterative rounding	$2 \text{ min } 35 \text{ s } \pm 5 \text{ s}$	$2h1min + 6min$	
$\bullet$ Hit-and-run	$49s + 1s$	$12h$ 47 min $+32m$ in	
Sample ln c	$22s+1s$ $0s + 0s$		
Sampling flux orthants	$22 s \pm 11 s$	$3h\,58\,\mathrm{min} \pm 17\,\mathrm{min}$	
US	$3.4s + 0.3s$	$4 \text{ min } 54 \text{ s} + 30 \text{ s}$	

Table SI 4: Number of orthants found in each condition. The last column shows the minimum number of orthants required to cover 95% of the thermodynamic space.





Figure SI 5: Selected examples comparing the flux distributions predicted by US and TFS (M−, growth on fructose). (A) Large variability in the flux through the pentose phosphate pathway. (B) A "branched TCA" (inactive or reverse fumarase) is themodynamically realistic. (C) E. coli has two paths for synthesizing glutamate. The path through glutamate synthase requires more ATP than the path through glutamate dehydrogenase, but may be the only thermodynamically feasible option in low-nitrogen conditions. (D) The flux through oxidative phosphorylation can vary significantly depending on the directions selected in the rest of the network.

				ALATA		
					<b>CYSTL</b>	
				EX_als_D_o EX skg.o	DXYLTD EX_ca2	EX_cl_s
					EX.R.A	
	EX. Ins. 6 DOM: EX lac_D_s	EX_lou_L_o EX.lysL.e	EX_nb4_e EX_met_L_s EX_mg2_e	EX 02.0	EX_pinc_e EX_pyt_e EX_so4_e	
	GLYCK	GLYCKZ		GLYCTOJ		
			LCARS			
	NTD10 NTD1		NTD	NTDS		
PAPSR2						
PPA2 PPAKe PPCK PPCSCT PSP 1 $P\overset{\sim}{\mathbf{SERT}}$ PTA2	PPK2 $\begin{array}{c} 0.005 & 0 \\ \textbf{PTA} & \\ \textbf{100} \end{array}$ PTRCabcpp	FUNPT $PTRC$ lex $\texttt{PTRCL2pp}$ <b>PTRCTA</b>	PUNP4 PUNPS PUNP3	PUMP? PUNPE PYK PYK2	Prise PYKS PYKS PYROX PYNP2r tr2rpp <sup>-p-y</sup> Rte	
nor alla $\frac{10}{100}$ K RISBPK RSPP QMO3 QMO2	RBK	$n$ $n$ RNDR1 RNDR2 RNDR1b	RNDR3b <b>RNDR4</b> RNDR2b RNDR3	RNTR1c2 RNTR3c2 RNDR4b RNTR2c2	RNTR4c2 SADH SADT2 Ã	$s$ c $\sigma$ os
SERAT SOPTA SERD_D SERD_L <b>SER</b> t2rpp	<b>SERMpp</b> stropp SERtex	3000 s <sub>cos</sub> <b>SGSAD</b> $\frac{1}{2}$	竈 9611 504(2pp	$_{\tt SOTA}$ sms 504tex SPMDs3pp	$s_{\text{SALX}}$ <b>SSALy</b> $\mathsf{sp}\,\mathsf{com}$ <b>SUCCITIPP</b> <b>SUCASPIpp</b>	SUCCI2_2pp
$\frac{0.20}{\text{SUCClex}}$ $_{\rm{svch}}$ SUCCI2_3pp sucrumpp SUCMALIPP	$\frac{0.02}{\text{SILabcpp}}$ $_{\text{surr}}$ $5UCOAS$	mors $\frac{0.06}{\text{THD2pp}}$ $\frac{0.05}{1}$ TARTt2_3pp $\mathbf{A}$	T H O R D N THRA $\begin{array}{c} 0.1 \\ \text{D\_copy2"TMMD} \end{array}$	$rac{0.001}{11005}$ TMRA2 THRabcpp mBD $mRD_L$ $\mathbf{H}$	$\begin{array}{c} 0.2 \\ \text{TRt2pp} \end{array}$ $\frac{0.1}{1000(2\pi pp)}$ THRIGH THTML3pp THRMpp	$\frac{1}{10}$
TMOS TMDK1 TMDPP $\mathbb{TP}1$ 骂	TRDR TREEPH TREGPP	TRESPS TREH TRPS1 TRPAS2	TRPS3 TRP52 TRPCrpp	$\overline{\text{TRSARr}}$ $_{\rm TME}$ TRPIEX TRPtipp Ctex"TTRCYCtpp"	TYRTA TYRI2rpp TYRIes	UGLYCH
$up_{R}$ $\frac{1}{\text{URAtax}}$ <b>UMPK</b> URACPAN URAI2pp	URAipp URDGLYCD <b>EX'UREA</b>	$_{\rm URIK2}$ <b>URK1</b> utic $_{\text{URIM}}$	VALabopp VALIZIPP p_copy2"URiter"	<b>VALTA</b> VALtex <b>XAND</b> VPAMT VALtIpp	$x$ ANt2pp <b>XPPT</b> XANtex XANtpp <b>XTSNH</b> t2rpp"XTS	
$x + 12$ ZN213pp 2N21pp <b>ZNabcpp</b>	GLCDpp EX glc_D_s GLCabcpp	GLCNIER GLCptspp GLCt2pp	ABTA SSALy GLCtex_copy2 ABTA_SSALx	ACGS_ACGK AIRCZ_AIRC3 ACONTa_ACONTb ARHGDE <b>ID_DHDPS_DHDP</b>	$\frac{-0.01}{\text{CPGCD}}$ $\sum_{k=1}^{n}$ PK ASAD HSD LUTION acon C. H.	EX pps a
$\frac{1}{\text{MDH} \cdot \text{log} \cdot \text{CZ}}$ PIK to FBA GLUSK_GSSD MDH_to_ACONT FBA_to_FBP	POK 10 POM PFK to TPI PIGrpp H2PO4 depp*PPAtex	PPCK to GAPD PPCK to PGK PPCK to PGM PPCK to END	PPS to GAPD PPS to END	030 035 0 2 PPS_to_PGK PPS_to_PGM PPS_to_TPI ு - மான் ப PTS to PGI	$\frac{US}{TFS}$	

Figure SI 6: Fluxes for all the reactions in iML1515-CAN (growth on glucose,  $M+$ ) predicted with US and TFS.

0.00 0.05 0.10 0.15 0.20 0 2 0 2 4 0 2 4 0 2 4 0 10 0.0 0.5 −0.5 0.0 0.00 0.05 0.10 0.00 0.05 0.10 0.00 0.05 0.10 0.0 0.1 0.0 0.1 0.0 0.1 0.0 0.1 0.0 0.1 0.0 0.1 0.00 0.05 0.10 0 5

Table SI 5: Comparison of precision and accuracy of different methods (see main text). Counts (percentages) are given as range (mean) over all conditions. The last two rows report the number (percentage relative to the reversible reactions) of reactions for which US and TFS predicted irreversibility in different directions.



Table SI 6: Evaluation of the predicted directions of reactions for which US and TFS predicted irreversibilities in opposing directions (M−). Predictions that are correct according to EcoCyc [11] are highlighted in green. Light green indicates predictions that we believe are correct but could not be confirmed. We did not seek validation for transporters (gray) as their exact stoichiometry is often unclear. Moreover, we ignored reactions already validated against 13C data and reactions that are potentially involved in substrate channeling (in that case, the direction of the reaction does not reflect the direction of the net flux).



Table SI 7: Evaluation of the predicted directions of reactions for which US and TFS predicted irreversibilities in opposing directions  $(M+)$ . Predictions that are correct according to EcoCyc [11] are highlighted in green. Light green indicates predictions that we believe are correct but could not be confirmed. We did not seek validation for transporters (gray) as their exact stoichiometry is often unclear. Moreover, we ignored reactions already validated against 13C and reactions that are potentially involved in substrate channeling (in that case the direction of the reaction does not reflect the direction of the net flux).





Figure SI 7: Distributions (orange) and 95% confidence intervals (red) of TFS predictions, predicted TMFA ranges (blue) and mean and 95% confidence intervals of the metabolomics data (black) are shown for all metabolites measured in [7]. Some concentrations could not be predicted because all the related reactions were blocked.

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