

Supplementary Note 1. Methods

1.1 Characterizations

 Linear coefficients of thermal expansion (CTE) of PEHF were measured from 0 30 to 100 °C at a heating rate of 3 °C min⁻¹ using a thermomechanical analyzer (TMA, Q400 system, TA instruments). Because the thermal expansion of employed 32 polyethylene hollow fibre is anisotropic¹, the axial and the radial coefficients of thermal expansion were tested individually. For each experiment, three heating scans and two cooling scans were conducted. The linear CTE along each direction was calculated based on the thermomechanical analysis results.

 Two-dimensional wide-angle X-ray scattering (2D WAXS) experiments were 37 performed at a sample-to-detector distance of 100 mm using CuK α radiation ($\lambda = 1.54$) Å) by deploying a D8 Discover system (Bruker, Germany) equipped with a 2D HI-Star detector and a 1.6 kW generator. Parallel PEHF were assembled, using a video microscope to ensure that the X-ray beam irradiated the centers of the fibres. The image acquisition time was 600 s. One-dimensional wide-angle X-ray scattering 42 (1D WAXS) experiments were performed using CuK α radiation and a 2 θ scanning 43 rate of 5° min⁻¹ on a Rigaku Smart Lab system (Japan) equipped with a 3.0 kW generator.

1.2 Calculation of the degree of orientation of crystals using WAXS analysis

 Despite inserting twists into a polymer fibre, the highly oriented semicrystalline form is also the key to provide a fibre the actuation capability. The Herman's orientation parameter (*f*) is employed to represent the polymer chain alignment of the 49 fibre, where $f = 1$ means that the polymer chains orient along the fibre axis 50 direction completely; $f = -0.5$ means that the polymer chains orient vertically to 51 the fibre axis direction completely. For a non-oriented sample, f equals to 0.

52 The Herman's orientation parameters $(f_a, f_b, \text{ and } f_c)$ for the a-axis, b-axis, and c-axis, for a unit cell of polyethylene crystallite with orthorhombic symmetry, were 54 calculated as 0.12, -0.30 , and 0.18, respectively, according to the literatures.²⁻³ These values provide the evidences that the fibres are in highly oriented semicrystalline

56 form.

57 The calculation details are as follows.

58 The Herman's orientation parameter (*f*) is defined as:

 $f = \frac{3\langle \cos^2{\phi} \rangle - 1}{2}$ 59 $f = \frac{3(\cos \theta)^{-1}}{2}$ (1.1),

60 where $\langle \cos^2 \Phi \rangle$ is an orientation factor defined as:

$$
61 \qquad \qquad
$$

 $\langle \cos^2 \Phi \rangle = \frac{J_0}{\int_0^{\pi} I_\Phi \sin \Phi d\Phi}$ (1.2), 62 where I_{Φ} represents the diffraction intensity. The azimuthal curve obtained by integration of diffraction intensity in the 2D WAXS pattern is used in Eq. (1.2) to 64 calculate $\cos^2 \Phi$ by the numerical integration process. Then the values of $\cos^2 \Phi$ are used in Eq. (1.1) to calculate the orientation function value *f* of the semicrystalline polymers.

 $\langle \cos^2 \Phi \rangle = \frac{\int_0^{\pi} I_\Phi \cos^2 \Phi \sin \Phi d\Phi}{\int_0^{\pi} I_\Phi \sin \Phi d\Phi}$ $\bf{0}$

 $\int_0^{\pi} I_{\Phi}$

67 For polyethylene with orthorhombic symmetry of the unit cell, the a-axis (f_a) and 68 b-axis (f_b) orientation parameters were calculated from the intense reflections of (200) 69 and (020) planes based on the relation:

 $\langle \cos^2 \Phi_{110} \rangle = 0.692 \langle \cos^2 \Phi_{020} \rangle + 0.308 \langle \cos^2 \Phi_{200} \rangle$ (1.3),

71 where $\langle \cos^2 \Phi_{110} \rangle$ and $\langle \cos^2 \Phi_{200} \rangle$ are obtained from the azimuthal intensity 72 measurements on the (110) and (200) reflections, respectively. The parameter f_c is estimated based on the orthogonal symmetry relationship: $f_a + f_b + f_c = 0$. 73

74 The detailed calculations for f_a , f_b , and f_c are as follows. First, an azimuthal curve was obtained by integration of diffraction intensity in the 2D WAXS pattern over the azimuthal angle using the software of the GADDS (general area detector 77 diffraction system) for diffraction angles $(2\theta_d)$ of 21.6° (110 plane) and 24° (200 plane), as shown in Supplementary Fig. 1c. Two identical peaks were observed in the azimuthal curve (Supplementary Fig.1d) because of the symmetric diffraction pattern 80 in 2D WAXS. The f_a , f_b , and f_c of the PEHF are respectively 0.12, -0.30, and 0.18, which indicate that the fibres are in highly oriented semicrystalline form.

83 **Supplementary Note 2. Thermomechanical modeling of hollow fibre actuator**

84 *1.1 Transient heat conduction analysis*

 The temperature change of the hollow fibre actuator is contributed by the forced convection of the internal flowing water as well as the natural convection of the ambient (external) air. To study this transient heat conduction problem, we establish a two-step model. First, we model the radial heat conduction at an arbitrary cross-section of the hollow fibre actuator. Second, we build a simple axial heat conduction model based on the assumption that heat conduction rate along the hollow fibre axis is much slower compared to the water flow rate and the rate of heat conduction in the radial direction. With this two-step model, we determine the hollow fibre actuator temperature as a function of radial and axial coordinates and time.

 The DSC results showed that there was no observable phase transition in the PEHF for the investigated temperature range (Supplementary Fig. 1b), we assume that there is no contribution of the phase transition to the volume change and the heat transfer contributed to the volume expansion.

98 First, the governing equation of the transient heat conduction in radial direction 99 at an arbitrary cross-section of the hollow fibre is given by

100
$$
\frac{\partial^2 \theta}{\partial r^2} + \frac{1}{r} \frac{\partial \theta}{\partial r} = \frac{1}{\alpha} \frac{\partial \theta}{\partial t} \quad \text{in} \quad R_i \le r \le R_o,
$$
 (2.1)

101 where θ (*r*, *t*) is the temperature, R_i and R_o are the inner and outer radius of the hollow 102 fibre, respectively. Thermal diffusivity α is defined by

$$
\alpha = \frac{k}{\rho c_p},\tag{2.2}
$$

104 in which *k* is the thermal conductivity, ρ is the mass density, c_p is the specific heat 105 capacity⁵⁻⁶. For PE, we have $k = 0.33$ W $(m \cdot K)^{-1}$, $\rho = 920$ kg m⁻³, $\epsilon_p = 2300$ J 106 $(kg \cdot K)^{-1.8}$.

107 The convective boundary conditions at the interior and exterior surfaces of the 108 hollow fibre are given by

$$
k\frac{\partial \theta}{\partial r}\bigg|_{r=R_i} = h_w \bigg(\theta\big|_{r=R_i} - \theta_w\bigg),\tag{2.3}
$$

$$
-k\frac{\partial\theta}{\partial r}\bigg|_{r=R_o} = h_a\Big(\theta\big|_{r=R_o} - \theta_a\Big),\tag{2.4}
$$

where h_w and h_a are the heat transfer coefficients of water and air, respectively. 111 112 Similarly, θ_w and θ_a are respectively the temperatures of water and air. The heat 113 transfer coefficient of water depends on many factors such as hollow fibre internal 114 geometry, surface roughness, water physical properties as well as the flow state 115 (laminar or turbulent), *etc*. In this work, we employ $h_w = 2000 \text{ W } (m^2 \cdot \text{K})^{-1}$, which 116 provides the best fit of theoretical predictions to the experimental measurements.

117 The initial condition is

$$
\color{red}118
$$

-

$$
\theta(t=0) = \theta_0, \qquad (2.5)
$$

119 where θ_0 is the initial temperature of the hollow fibre actuator.

 The above 1D radial transient heat conduction equations can be solved either analytically using methods of separation of variables and superposition, which are well documented in ref. 10, or using numerical methods such as finite difference or finite element. In this work, we solved this 1D partial differential equation (PDE) 124 using the PDE solver provided by MATLAB^{*}.

 Next, we assume that the axial heat conduction rate is much lower compared to the water flow rate. As such, the heat transfer in the axial direction is mainly contributed by the flowing water and the radial conduction. Therefore, by substituting 128 water temperature as a function of axial coordinate and time, i.e. $\theta_w = \theta_w(x,t)$, in 129 which x is the axial coordinate, into the above radial heat conduction equations, we can solve the hollow fibre temperature distribution in the axial direction.

131 Water temperature θ_w (*x*, *t*) depends on a few factors, such as initial water 132 temperature, water flow rate, heat loss due to transfer to hollow fibre actuator and

^{*}https://www.mathworks.com/help/matlab/math/partial-differential-equations.html

133 eventually to the ambient air, *etc*. For simplicity, we assume that the heat loss is 134 relatively low when the flow rate is high. Therefore, we can write the water 135 temperature as

$$
\theta_{w}(x,t) = \theta_{w0}H(vt-x), \qquad (2.6)
$$

137 where θ_{w0} is the initial water temperature, *v* is the water flowrate and $H(\cdot)$ is the 138 Heaviside step function.

139

140 *2.2 Torsional actuation modeling*

141 Torsional actuation mechanism of the twisted polymer fibres was studied in ref. 142 10 and 11. The hollow fibre length *l*, the hollow fibre outer diameter *d*, and the 143 helically oriented polymer chain length λ are related through

$$
\lambda^2 = \left[\left(\pi dT \right)^2 + 1 \right] l^2, \tag{2.7}
$$

145 where T is the twist density.

 Upon heating, polymer chains will expand in the radial direction and contract in the axial direction, which can be accommodated by the changes in the hollow fibre length, the diameter and the twist density. In ref. 10, the change of hollow fibre length is considered small and the following equation for untwisting can be obtained by

$$
\Delta T = \left(\frac{\Delta \lambda}{\lambda} \frac{1}{\cos^2 \alpha_f} - \frac{\Delta d}{d}\right) T, \qquad (2.8)
$$

151 where bias angle $\alpha_f = \tan^{-1}(\pi dT)^{12}$.

152 Ref. 11 further assumed that λ is also constant. Therefore, the untwist ΔT is 153 linearly proportional to the change in the hollow fibre diameter, i.e.

$$
\Delta T = -\frac{\Delta d}{d}T,\tag{2.9}
$$

155 In this work, we employ Eq. (2.8) for torsional actuation modeling. It can be 156 rewritten as

$$
\Delta T = \left(\alpha_{\lambda} \frac{1}{\cos^2 \alpha_f} - \alpha_d\right) \Delta \theta \cdot T\,,\tag{2.10}
$$

158 where α_{λ} and α_{d} are the coefficients of thermal expansion of polymer chain in the 159 axial direction and that of the hollow fibre in the radial direction, respectively. The $\Delta\theta$ 160 is the temperature change obtained from the previous transient heat conduction 161 analysis. In this work, the average exterior hollow fibre temperature change is 162 employed as the actuation temperature $\Delta \theta$. Axial and radial coefficients of thermal 163 expansion of PEHFs were employed as $\alpha_{\lambda} = -(5.3 \pm 0.4) \times 10^{-4} \text{ K}^{-1}$ and 164 $\alpha_d = (5.2 \pm 0.7) \times 10^{-4} \text{ K}^{-1}$, which were obtained from thermomechanical analysis 165 (TMA).

- 166
- 167 *2.3 Tensile actuation modeling*

168 The tensile actuation mechanism of the twisted, mandrel-coiled polymer fibre is 169 well documented in ref. 10, which is adopted in this work. The equation for tensile 170 actuation is

$$
\frac{\Delta L}{L} = \frac{l^2}{NL} \Delta T \quad , \tag{2.11}
$$

172 where *L* is the coil length, *l* is the twisted hollow fibre length, *N* is the number of coil 173 turns and ΔT is the amount of untwisting that can be obtained from Eq. (2.10).

174

175 **Supplementary Note 3. The analysis for the optimum hollow fibre geometry**

 To provide an estimation of the optimum configuration of the hollow fibre, we assume steady heat solution and constant temperature due to the small thickness of the hollow fibre. Based on the linear elastic solution for a thin-walled hollow fibre under 179 – pure torsion¹³, the generated torque *M* is related to the twist through

180 $M = 2\pi GJT$, (3.1)

181 in which *G* is shear modulus, *J* is the polar second moment of area. For the hollow fibre section $J=\frac{\pi}{2}$ 182 fibre section $J = \frac{\pi}{2} (r_o^4 - r_i^4)$ where r_i and r_o are the inner and outer radius of the 183 hollow fibre, respectively.

184 Applying Eq. (3.1) to the hollow fibre configurations before and after the

torsional actuation provides the torque release *∆M*:

186
$$
\Delta M = \pi G A_0 (r_i^2 + r_o^2) [(I + \alpha_d \Delta \theta)^4 (T + \Delta T) - T], \qquad (3.2)
$$

187 in which A_0 is the cross-section area of the hollow fibre.

We now introduce a simplified version of torsional actuation based on Ref. 10 :

$$
\Delta T = \left(\frac{d_0}{d} - 1\right)T.\tag{3.3}
$$

Substituting Eq. (3.3) into (3.2) gives

191
$$
\Delta M = \pi G A_0 (r_i^2 + r_o^2) [(1 + \alpha_d \Delta \theta)^3 - 1]T.
$$
 (3.4)

 Based on Eq. (3.4), we conclude that the optimum geometry for maximizing the 193 torque output is to maximize $(r_i^2 + r_o^2)$, assuming that the cross-section area A_0 (or equivalently the material consumption) is constant. This means that the material should be distributed as far away as possible from the center of the cross-section, which justifies the use of hollow fibre over solid cross-sections. It should be noted that the above theoretically derived optimum geometry is subjected to the constraint that the hollow fibre will not buckle under the applied torque. Thus, in practice a hollow fibre with finite thickness should be used for the proposed actuation application.

204 **Supplementary Figure 1.** (a) The stress-strain curve of the PEHF₅₈₀₋₉₉₀. The gauge 205 length was 34 mm, and the extension rate was 20 mm min⁻¹. (b) Differential scanning 206 calorimetry (DSC) curve of the PEHF₅₈₀₋₉₉₀ with a heating rate of 5° C/min in N₂ 207 atmosphere. The melting enthalpy $(H_m=126.4 \text{ J g}^{-1})$ was obtained by integration of the 208 endothermic melting peak. By considering that the melting enthalpy of the 100% 209 crystalline polyethylene was $H_c=287.3 \text{ J g}^{-1}$ ¹⁴, we can obtain the crystallinity of 210 low-density polyethylene (χ_c) from the equation $\chi_c=H_m/H_c=44\%$. (c) The intensity of 211 diffraction peaks versus Bragg angle (2 θ) in WAXS for PEHF₅₈₀₋₉₉₀. (d) 2D WAXS 212 diffraction pattern for PEHF₅₈₀₋₉₉₀ showing anisotropic structure. (e, f) The azimuthal 213 curves of (110) and (200) planes in $PEHF_{580-990}$ were obtained from (d).

215 **Supplementary Figure 2.** The torsional actuation of the PEHF₅₈₀₋₉₉₀ actuator by 216 flowing hot water at 1.72 g s^{-1} at different actuation conditions: (a) at different 217 environment temperatures, (b) at different environmental relative humidity, and (c) at 218 different wind speed. (d) The torsional actuation of the $PEHF_{580-990}$ actuator by 219 flowing different types of 40 °C liquid at a flow rate of 1.72 g s⁻¹. The δ and $\Delta\delta$ are the 220 rotation angle during actuation and its change. If not specified, the room temperature 221 is 25 °C, the environmental relative humidity is 40%, and the water flow rate is 1.72 g 222 $s⁻¹$. If not specified, error bars in this figure and in the following figures indicate 223 standard deviations. EtOH: ethanol; EA: ethyl acetate; DMSO: dimethyl sulfoxide; 224 THF: tetrahydrofuran; DMF: N, N-dimethylformamide; DCM: dichloromethane; 225 IPA: iso-propanol; PE: petroleum ether.

228 **Supplementary Figure 3**. (a) Contraction and hollow fibre surface temperature as a 229 function of time for a homochiral PEHF₅₈₀₋₉₉₀ actuator by flowing 95 °C water with 230 different flow rates. (b) Response time and hollow fibre surface temperature as a 231 function of water flow rate for a homochiral PEHF₅₈₀₋₉₉₀ actuator by flowing 95 \degree C 232 water. (c) Coil length and actuation stroke of the homochiral $PEHF_{580-990}$ actuator by

233 flowing 25 °C water at different flow rates. The spring index was 4.0, and the inserted 234 twist density was 200 turns m^{-1} .

235

236 **Supplementary Figure 4**. (a) The initial coil length and actuation stroke of the 237 homochiral PEHF₅₈₀₋₉₉₀ actuator by flowing 25 \degree C glycerol/water solution with 238 different viscosity. (b) Actuation stroke of the PEHF₅₈₀₋₉₉₀ actuator by flowing 80 °C 239 glycerol/water solution with different viscosity. (c) The initial coil length and 240 actuation stroke of the PEHF₅₈₀₋₉₉₀ actuator by flowing 25 \degree C aqueous NaCl solution 241 with different densities. (d) Actuation stroke of the $PEHF_{580-990}$ actuator by flowing 242 80 °C aqueous NaCl solution with different densities. The spring index was 4.0, and 243 the twist density was 200 turns m^{-1} .

245 **Supplementary Figure 5**. The contraction as a function of temperature for 246 PEHF₅₈₀₋₉₉₀ actuator driven by consecutively flowing hot water and cold water with a 247 temperature range. The spring index was 4.0, the inserted twist density was 200 turns

248 m ⁻¹, and the flow rate was 1.72 g s⁻¹. The solid symbols indicate the heating process, and the open symbols indicate the cooling process.

 Supplementary Figure 6. (a, b) Serial infrared images of the homochiral 252 PEHF₃₈₀₋₁₀₉₀ (a) and PEHF₂₈₀₋₆₄₀ (b) actuators by flowing 95 °C water at different time (0 s, 0.2 s, 0.4 s, and 0.6 s). (c) Experimental results and theoretical analysis of the actuation strain and surface temperature of the PEHF actuators as a function of time.

 Supplementary Figure 7. (a) Maximum actuation stroke for ten consecutive 257 heating/cooling cycles for heterochiral and homochiral load-free $PEHF_{580-990}$ actuators 258 driven by alternatively flowing hot water and $25 \degree C$ water. (b) Maximum actuation

259 stroke as a function of twist density for load-free $PEHF_{580-990}$ homochiral actuators 260 with different spring indexes driven by 80 °C flowing water.

262 **Supplementary Figure 8.** (a) Maximum contraction at different mass of the load for 263 ten consecutive heating/cooling cycles of homochiral $PEHF_{580-990}$ actuators with a 264 spring index of 4.0 and an inserted twist of 100, 150, 200, 250 and 300 turns m^{-1} by 265 alternatively flowing 90 °C and 25 °C water. (b) The actuation stroke and the work

266 capacity as a function of the mass of the applied load for the homochiral $PEHF_{580-990}$ actuators with different twist densities, which were derived from graphs in (a).

 Supplementary Figure 9. (a) Comparison of the work capacity at different isobaric 270 stress for the homochiral PEHF₅₈₀₋₉₉₀ actuator driven by 90 °C water and for the PE 271 solid fibre actuator driven by 90 °C water. (b) Comparison of the time-dependence of 272 work capacity for the homochiral PEHF₅₈₀₋₉₉₀ actuator driven by 90 $^{\circ}$ C water and for 273 the PE solid fibre driven by 90 \degree C air at the stress of 107 kPa, and the inset was the 274 comparison of power density. The twist density was turns m^{-1} , and the spring index was 4.0. The isobaric stress was calculated as the weight of the load divided by the cross-sectional area of sheath of the hollow fibre.

 Supplementary Figure 10. (a) Schematic diagram of a conventional microfluidic manipulation system containing liquid sensing, transporting and actuating devices. Optical images (b) and schematic illustration (c) of the contractile hollow fibre actuators used for sensing the liquid temperature and sorting the liquid into the

 desired vessels. (d) The length of the hollow fibre actuators as a function of the 283 temperature of the flowing water for the homochiral $PEHF_{580-990}$ actuators.

 Supplementary Figure. 11 Schematic of the twisted and coiled hollow-fibre actuators

 Supplementary Figure 12. The twist loss of the hollow fibre after twist insertion, 290 thermal annealing with both-end tethered at $108 \degree C$ for 1h, and cooling down to room temperature and removing the tethering.

293 **Supplementary Tables:**

294 **Supplementary Table 1**. Response time and actuation parameters of the torsional 295 PEHF actuators in this work.

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297 **Supplementary Table 2**. Response time and actuation parameters of the tensile PEHF

298 actuators in this work.

299

Supplementary Table 3. Resolution and the coil parameters of the homochiral PEHF

Fibre Length	Coil Length	Number of	Twist density	Resolution
(l, mm)	(L, mm)	Turns (N)	$(T,$ turns mm ⁻¹)	$(l^2 \Delta T/NL, 10^{-3})$
200	105	11	0.30	$-3.0%$
200	105	11	0.25	$-2.0%$
200	105	11	0.20	$-1.3%$
200	105	11	0.15	$-0.78%$
200	105	11	0.10	$-0.43%$
200	115	12	0.30	$-2.5%$
200	115	12	0.25	$-1.7%$
200	115	12	0.20	$-1.1%$
200	115	12	0.15	$-0.66%$
200	115	12	0.10	$-0.36%$
200	130	15	0.25	$-1.2%$
200	130	15	0.20	$-0.78%$
200	130	15	0.10	$-0.26%$
200	145	18	0.20	$-0.58%$
200	145	18	0.10	$-0.19%$

hollow fibre actuators in this work.

self-nucleation/annealing thermal fractionation. J. Appl. Polym. Sci. 94, 1710-1718 (2004).