Electronic Supplementary Material (ESI) for RSC Advances. This journal is © The Royal Society of Chemistry 2019

Supporting Information

Enhanced phosphate sequestration by Fe(III) modified

biochar derived from coconut shell

Zhenxing Zhong¹, Guowen Yu¹, Wenting Mo², Chunjie Zhang¹, Hao Huang^{1,3}, Shengui Li², Meng Gao⁴, Xiejuan Lu^{1*}, Beiping Zhang¹, Hongping Zhu⁵

¹ School of Environmental Science and Engineering, Huazhong University of Science and Technology, Wuhan 430074, China

²Department of Urban Construction, Wuchang Shouyi University, Wuhan, 430064, China

³ Wuhan Planning and Design Company, Wuhan, 430014, China

⁴ Huangshi Institute of Environmental Protection, Huangshi, 435000, China

⁵School of Civil Engineering & Mechanics, Huazhong University of Science and Technology, Wuhan 430074, China

*Corresponding author: luxiejuanhust@163.com (X.J Lu); Tel: +27-87792155

Appendix A

Table S1 List of isotherm models and kinetic models in this study

Kinetic models [1]	Parameters	Isotherm models [2]	Parameters	
First-order:		Freundlich		
$\frac{dq_t}{dt} = k_1(q_e - q_t)$	$q_e, q_t, k_1, R^2;$	$q_{_e} = K_{_f}C_{_e}^{_{1/n}}$	$K_{F,} n, R^{2};$	
$\ln(q_e - q_t) = \ln q_e - k_1 t$				
Second-order:		Langmuir		
$\frac{dq_t}{dt} = k_2 (q_c - q_t)^2$	$q_{e}, q_{t}, k_{2}, R^{2};$	$q_{\perp} = \frac{K_{I}q_{m}C_{e}}{K_{I}}$	$K_{L} q_{m} R^{2};$	
$\frac{t}{q_t} = \frac{l}{k_2 q_e^2} + \frac{t}{q_e}$		$1 + KC_e$, - ,	
Richie n-th-order:		Langmuir- Freundlich		
$\frac{dq_{t}}{dt} = k_{n}(q_{e} - q_{t})^{n}$ $q_{t} = q_{e} - ((n-1)k_{n}t + q_{e}^{1-n})^{\frac{1}{1-n}}$	$\begin{array}{c} q_e,q_t,k_n,\\ n,R^2; \end{array}$	$q_e = \frac{K_{IF}q_m C_e^n}{1 + K_{IF} C_e^n}$	$K_{LF,} q_{m,} n, R^2;$	
Elovich:				
$\frac{dq_{t}}{dt} = aexp(-bq_{t})$ $q_{t} = \frac{1}{b}ln(abt + 1)$	a, b, q _t , R ²			

Adsorbents	$\begin{array}{c} K_{p1} \\ (mg/g {\scriptstyle \bullet } h^{1/2}) \end{array}$	C ₁ (mg/g)	R ²	$\begin{array}{c} K_{p2} \\ (mg/g {\scriptstyle \bullet } h^{1/2}) \end{array}$	C ₂ (mg/g)	R ²
CSB	1.023	0.463	0.797	0.049	1.886	0.895
Fe-CSB	0.806	1.212	0.905	0.323	2.092	0.923

Table S2 Kinetic parameters of phosphate sorption to CSBs based on the intra-particle diffusion model [3]

The intraparticle diffusion model: $q_t = k_p \cdot t^{1/2} + C_{,}$ where K_p is the intraparticle diffusion rate constant (mg/g \cdot h^{1/2}), and C is a constant that reflects the thickness of the boundary layer.

Materials T (K)	T(V)	Parameters					
	1 (K)	K ₀ (L/mg)	$\Delta G^0 (kJ/mol)$	$\Delta H^0(kJ/mol)$	$\Delta S^0(J/mol/K)$		
	298	0.13	-12.06				
CSB	308	0.15	-12.82	21.58	111.43		
	318	0.20	-14.01				
	298	1.43	-18.00				
Fe-CSB	308	1.54	-18.79	26.54	82.11		
	318	1.63	-19.56				

Table S3 Thermodynamic parameters of P adsorption for CSB and Fe-CSB

Thermodynamic parameters are determined by the following equations [4]:

 $K_{0} = \frac{q_{e}}{C_{e}} \frac{1}{(1); \Delta G} = -RT \ln K_{0}(2); \Delta G = \Delta H - T\Delta S^{0}(3); \ln K_{0} = \frac{\Delta H^{0}}{RT} - \frac{\Delta S^{0}}{R} \frac{1}{(4);}$ where K₀ is the adsorption coefficient, R is gas constant (kJ/mol K), and T is the absolute temperature (K),

respectively.

Adsorbents	Solution pH	Contact time (h)	Temperature (℃)	Fe (wt %)	Equilibrium Ce (mg/g)	Max q _m (mg/g)	Ref.
Fe-CSB	7.0	24	25	11.2%	2-100	36.0	This work
Fe(III)-Bentonite	7.0	96	25	2.78%	0.05-5.0	11.2	[5]
Granulated ferric hydroxide	5.5	24	20	31.4%	0.3-4.0	23.3	[6]
Magnetic water hyacinth biochar	7.0	24	25	15.0-27.1%	0.2-150	5.1	[7]
Fe-impregnated woodchip biochar	5.6	24	24	2-4%	10-200	3.2	[8]
Fe-doped activated carbon	7.0	24	RT ^a	18.6%	15-640	8.1	[9]
Fe ³⁺ /Fe ²⁺ modified WAS biochar	7.0	2	22	24.2%	5-1000	34.2	[10]
Magnetic Fe-Zr binary oxide	4.0	24	25	26.62%	0-100	13.7	[11]
Ferrihydrite	7.0	24	25	31.4%	0-250	22.2	[12]

Table S4 Comparison of maximum P sorption capacities for various Fe-based materials

a: RT, room temperature;

Solid formed	med Chemical equation		Ref.
Ferric phosphate	$Fe^{3+} + PO3-4 \leftrightarrow FePO_{4(s)}$	21.9	[13]
Iron (III) hydrogen phosphate	$2Fe^{3+} + 3HPO2-4 \leftrightarrow Fe_2(HPO_4)_{3(s)}$	30.9	[14]
Iron (II) dihydrogen phosphate	$Fe^{3+} + 3H_2PO-4 \leftrightarrow Fe(H_2PO_4)_{3 (s)}$	26.6	[14]
Aluminum phosphate	$\mathrm{Al}^{3+} + \mathrm{PO3-4} \leftrightarrow \mathrm{Al}\mathrm{PO}_{4(\mathrm{s})}$	21.0	[13]
Aluminum hydrogen phosphate	$2\mathrm{Al}^{3+} + 3\mathrm{HPO2}\text{-} 4 \leftrightarrow \mathrm{Al}_2(\mathrm{HPO}_4)_{3(s)}$	Particles	[15]
Calcium hydrogen phosphate	Ca^{2+} +HPO2- 4 \leftrightarrow CaHPO _{4(s)}	6.66	[16]
Calcium dihydrogen phosphate	$Ca^{2+} + 2H_2PO-4 \leftrightarrow Ca(H_2PO_4)_{2(s)}$	1.14	[16]
Tricalcium phosphate	$3Ca^{2+} + 2PO3-4 \leftrightarrow Ca_3(PO_4)_{2(s)}$	24.0	[16]
Hydroxyapatite	$5Ca^{2+}+3PO3-4+OH-\leftrightarrow Ca_5(PO_4)_3OH_{(s)}$	55.9	[16]
Magnesium phosphate	$3Mg^{2+}+2PO3-4 \leftrightarrow Mg_3(PO_4)_{2(s)}$	25.2	[1]
Magnesium hydrogen phosphate	Mg ²⁺ +HPO2- 4 ↔ MgHPO $4_{(s)}$	5.82	[1]
Magnesium dihydrogen phosphate	$Mg^{2+}+2H_2PO-4 \leftrightarrow Mg(H_2PO 4)_{2(s)}$	Particles	[1]

Table S5 Chemical reactions between phosphate and metal ions in this study



 $$_{\rm pH}$$ Fig. S1 Linear correlations between the initial pH and the P adsorption amount of CSB and Fe-CSB





Fig. S3. The adsorption capacity of phosphate by Fe-CSB during five successive cycles

References:

- 1. Y. Yao, B. Gao, J. Chen, L. Yang, Environ Sci Technol, 2013, 47, 8700-8708.
- 2. L. Zeng, X. Li, J. Liu, Water Research, 2004, 38, 1318-1326.
- 3. V Kuroki, G E. Bosco, P S. Fadini, Journal of Hazardous Materials, 2014, 274, 124-131.
- 4. P. Liao, S. Yuan, W. Xie, W. Zhang, M. Tong, K. Wang, Journal of Colloid and Interface Science, 2013, 390, 189-195.
- 5. M. Zamparas, A. Gianni, P. Stathi, Y. Deligiannakis, I. Zacharias, Applied Clay Science, 2012, 62–63, 101–106.
- 6. A. Genz, A. Kornmuller, M. Jekel, Advanced phosphorus removal from membrane filtrates by adsorption on activated aluminium oxide and granulated ferric hydroxide, Water Research, 38 (2004) 3523–3530.
- 7. R. Cai, X. Wang, X.H Ji, B. Peng, C.Y. Tan, X. Huang, Journal of Environmental Management, 2017, 187, 212-219.
- 8. B. Micháleková-Richveisová, V. Frišták, M. Pipíška, L. Ďuriška, E. Moreno-Jimenez, G. Soja, *Environ Sci Pollut Res*, 2017, 24, 463–475.
- 9 Y. Yao, B. Gao, M. Inyang, A. R. Zimmerman, X.D Cao, P. Pullammanappallil, L.Y. Yang, *Journal of Hazardous Materials*, 2011, 190, 501–507.
- 10. Q. Yang, X.L. Wang, W. Luo, J. Sun, Bioresource Technology, 2018, 247, 537-544.
- 11. F. Long, J.-L. Gong, G.-M. Zeng, L. Chen, X.-Y. Wang, J.-H. Deng, Q.-Y. Niu, H.-Y. Zhang, X.-R. Zhang, *Chemical Engineering Journal*, 2011, 171, 448-455.
- 12. J. Yan, T. Jiang, Y. Yao, S. Lu, Q. Wang, S. Wei, Journal of Environmental Sciences, 2016, 42, 152-162.
- 13. G W Yu, B P Zhang, X J Lu, Arab J Geosci, 2015, 8, 3491–3499.
- 14. D. Rich, [D], Northwestern International University, 2005.
- 15. H R Liu, W L Jiang, G M Su, Modern Paint & Finishing, 2010, 13, 10-12 (Chinese).
- 16. T Hiemstra, J Antelo, R Rahnemaie, Geochimica et Cosmochimica Acta, 2010, 74, 41-58.