

Supporting Information

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Advanced Dual-Ion Batteries with High-Capacity Negative Electrodes Incorporating Black Phosphorus

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Incorporating Black Phosphorus**

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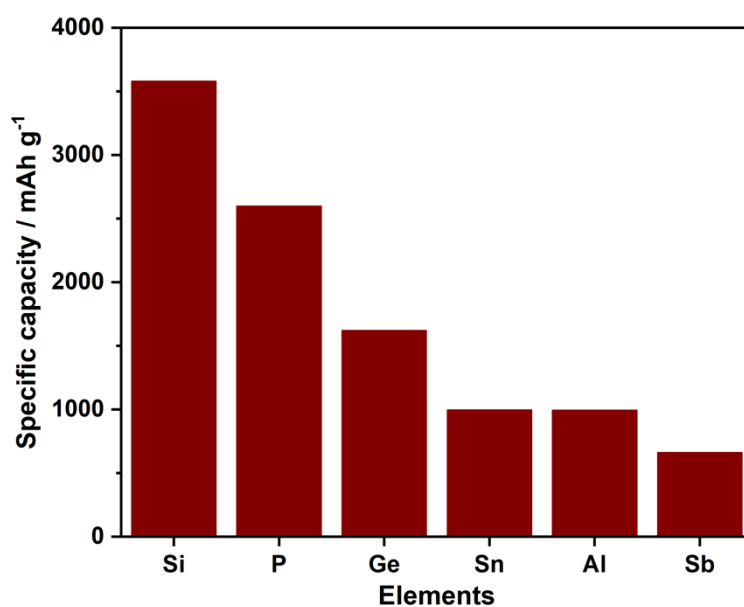


Figure S1. Theoretical specific capacities of selected materials capable of electrochemical alloying with Li⁺ ions.

Additional results

Table S1. Elemental analysis of synthesized BP-C composite via energy-dispersive X-ray spectroscopy. Weight ratios of observed elements.

Element	Weight ratio / %	
	Average	St. Dev
C	47.84	1.14
O	5.05	0.29
Na	0.17	0.05
Mg	0.10	0.03
Si	0.08	0.05
P	44.94	0.42
Cl	0.22	0.05
Ar	0.17	0.05
Cr	0.41	0.11
Fe	1.79	0.45
W	1.12	0.13
Total	101.89	

Table S2. Specific de-lithiation capacities and Coulombic efficiencies of BP-C || Li metal cells (two-electrode configuration; voltage range: 0.01V – 2V) for different electrolyte solutions.

Electrolyte	De-lithiation capacity			Capacity retention (6 th – 105 th cycle, %)	Coulombic efficiency (%)		
	1 st cycle (mAh g ⁻¹)	6 th cycle (mAh g ⁻¹)	105 th cycle (mAh g ⁻¹)		1 st cycle	6 th cycle	105 th cycle
1M LiPF₆ in EC:EMC, 3:7 by wt.	1194	1070	792	74.0	79.7	98.0	99.7
3.4M LiTFSI in DMC	1060 ± 39	897 ± 40	745 ± 32	83.0	72.9 ± 0.03	98.3 ± 0.06	99.6 ± 0.04
4M LiPF₆ in DMC	1009 ± 98	957 ± 134	706 ± 99	73.0	43.5 ± 1.5	94.6 ± 0.5	96.7 ± 0.4

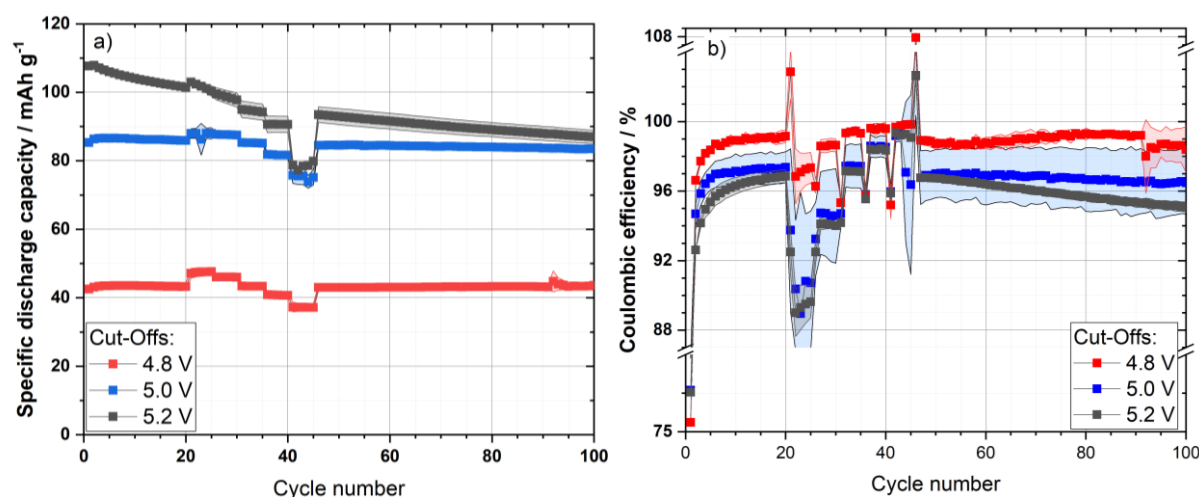


Figure S2. Electrochemical performance of graphite as positive electrode material in constant current cycling charge/discharge experiments in graphite || Li metal cells (three-electrode configuration; half-cell setup) over 100 cycles: a) Specific discharge capacity and b) C_{Eff} of a graphite WE at various specific currents and varying upper-cut-off potentials (vs. Li|Li⁺) with 3.4M LiTFSI in DMC as electrolyte in a three electrode setup (same as shown in Figure 5b,c).

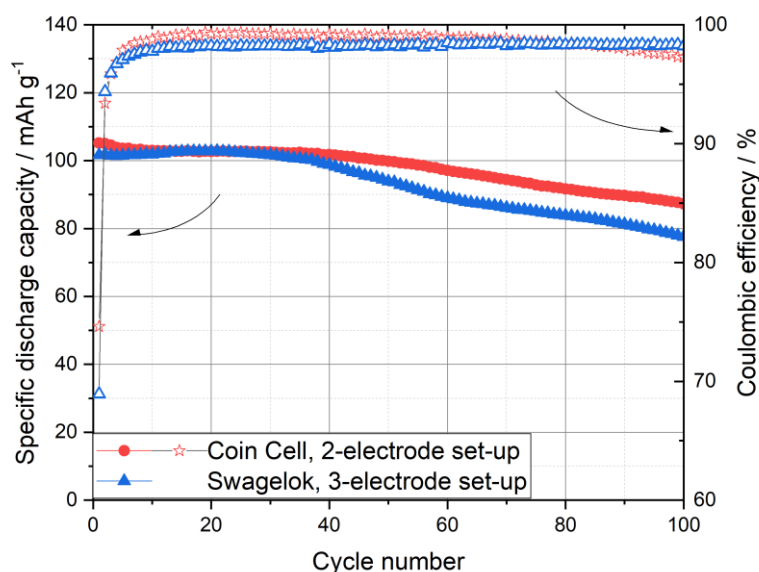


Figure S3. Comparison of the electrochemical performance of graphite || BP-C cells (two-electrode and three-electrode configuration; both in full-cell setup) in constant current cycling charge/discharge experiments with 3.4M LiTFSI in DMC as electrolyte. Cell voltage range: 2.0 - 4.7 V. Specific capacity is related to the mass of the positive electrode.

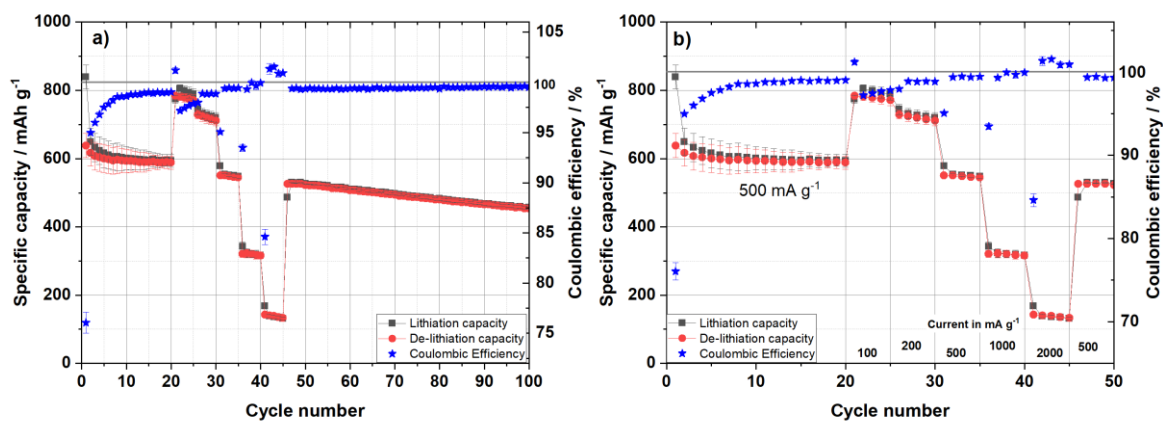


Figure S4. Electrochemical performance of BP-C composite in constant current cycling (de-)lithiation experiments in BP-C || Li cells (three-electrode configuration; half-cell setup) at various specific currents with 3.4M LiTFSI in DMC as electrolyte. Potential range: 0.5 V – 2.0 V vs. Li|Li⁺. (b) magnification of (a).

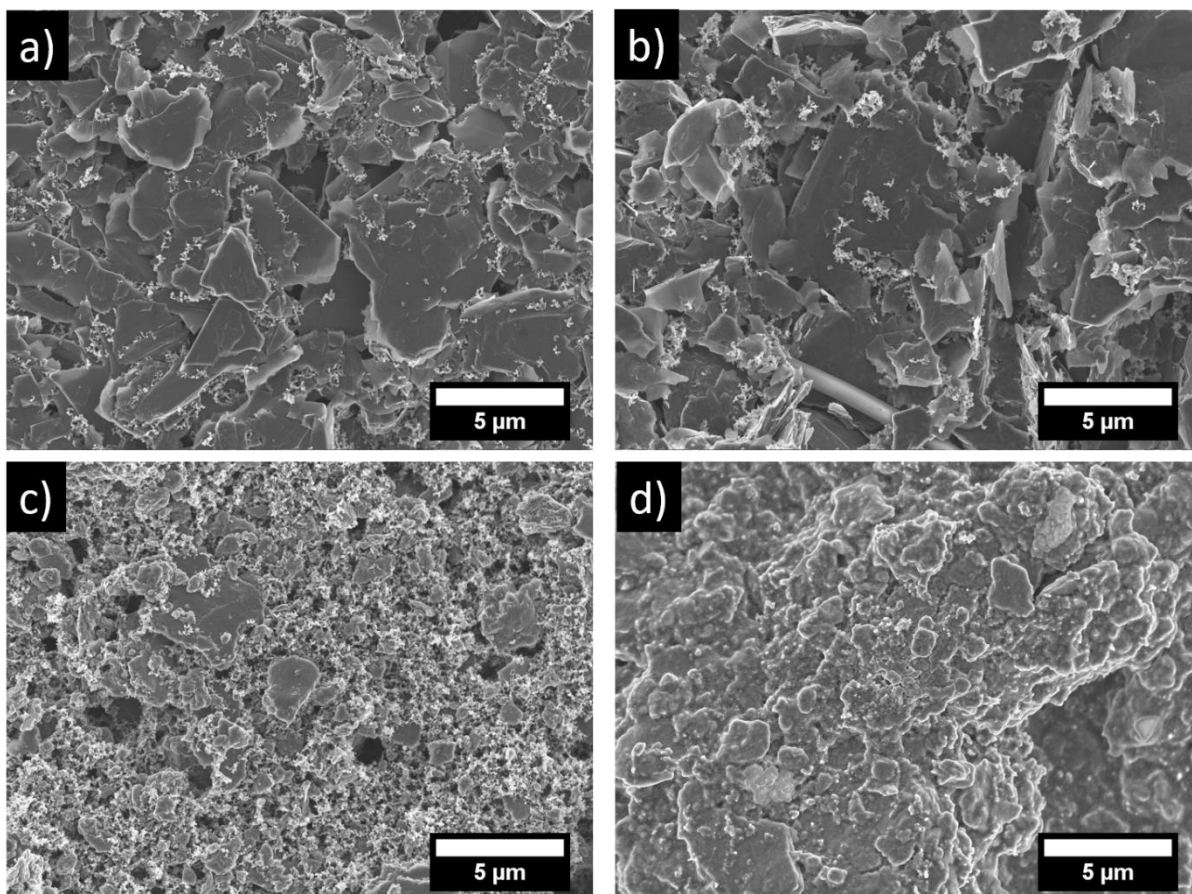


Figure S5. SEM images of a pristine graphite electrode (a), pristine BP-C electrode (c) and cycled graphite electrode (b) as well as BP-C (d) electrode after 100 cycles cycled between 2-4.7V in graphite || BP-C full-cells.

Ex situ XRD of graphite positive electrodes

During anion intercalation of anions into layered structures the arise of (00l)-reflections (with $l = 1, 2, \dots$ etc.) demonstrates the staging behavior, which is caused by the repeat unit in c-direction, whereas for anion with the size of TFSI⁻ or PF₆⁻ the (00n+1) and (00n+2)-reflections are the most dominant ones.^[1] Since the repeat distance of the unit cell $I_{Gallery}$ is the same for both reflections, the following equation can be written:

$$I_{Gallery} = (n + 1)d_{00n+1} = (n + 2)d_{00n+1} \quad (1)$$

where d_{00n} is the calculated interlayer distance, which can be calculated by Bragg's law:

$$d_{00n+1} = \frac{\lambda}{2 \sin \theta_{00n+1}} \quad (2)$$

where λ describes the X-ray length and θ the Bragg angle. By substitution of (2) in (1) the dominating stage index n can be calculated by:

$$n = \frac{1}{1 - \frac{\sin \theta_{00n+1}}{\sin \theta_{00n+2}}} - 2 \quad (3)$$

As one unit cell of a GIC consists out of $(n-1)$ stacked graphene planes, $I_{Gallery}$ can be described by

$$I_{Gallery} = h_{C-A-C} + (n - 1) 3.35 \text{ \AA} \quad (4)$$

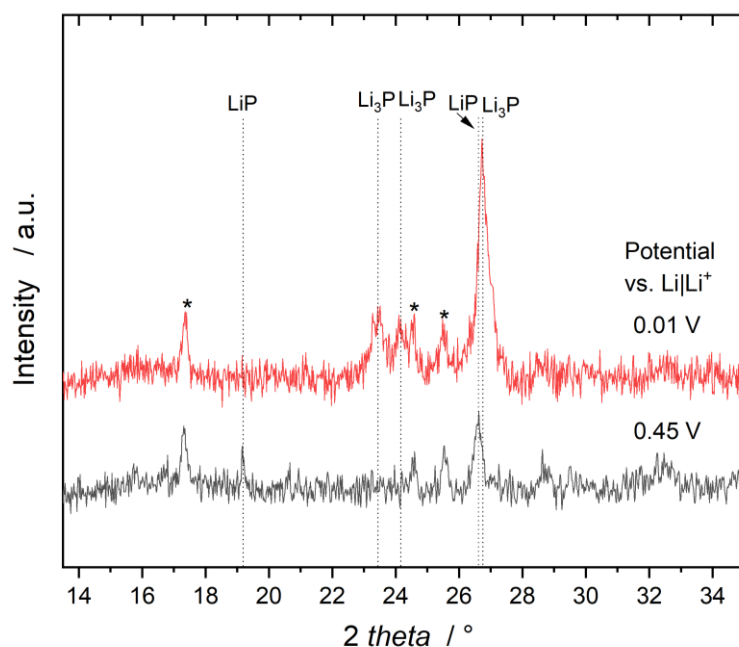
where h_{C-A-C} describes the gallery height of two intercalated graphene planes. Based on that following values in **Table S3** can be calculated.

Table S3. List of calculated parameters from the *ex situ* XRD measurement of graphite electrodes extracted from graphite || BP-C cells (three-electrode configuration, full-cell setup; **Figure 9b**).

Mode	Cell voltage	$2\theta_{00(n+1)} / ^\circ$	$2\theta_{00(n+2)} / ^\circ$	Calc. Stage	$I_{Gallery} / \text{\AA}$	$h_{C-A-C} / \text{\AA}$
Charge	3.7 V	24.00	30.71	2.66	13.54	7.99
Charge	4.3 V	22.09	33.28	1.02	8.12	8.05
Charge	4.7 V	22.25	33.49	1.03	8.095	7.99
Discharge	4.1 V	22.14	33.26	1.04	8.18	8.07
Discharge	3.7 V	22.23	33.39	1.042	8.15	8.01
Discharge	3.2 V	23.51	31.35	2.07	11.59	8.02
Discharge	2.0 V	25.10	28.97	5.62	23.44	7.98

Ex situ ^7Li MAS NMR**Table S4.** List of ^7Li chemical shifts measured *via ex situ* ^7Li NMR measurement of BP-C electrodes (**Figure 9c**).

Cell voltage	Mode	Potential vs. $\text{Li} \text{Li}^+$ / V	δ_{iso} / ppm
Pristine	-	-	-1.7
3.7 V	Charge	1.00	-1.0
4.3 V	Charge	0.70	1.0
4.7 V	Charge	0.45	2.4
4.1 V	Discharge	0.8	2.8
3.7 V	Discharge	0.95	1.3
3.2 V	Discharge	1.2	1.0

Ex situ XRD of BP-C electrodes**Figure S6.** *Ex-situ* XRD pattern of the lithiated black P-carbon composite electrode at different potentials: 0.45 (corresponding cell voltage in full cell: 4.7 V, black) and 0.01 V vs. $\text{Li}|\text{Li}^+$ (fully lithiated, red). The reflections of crystalline phases of LiP and Li_3P are clearly visible. The reflections marked with asterisk could not be assigned to phases expected in the electrodes and may originate from side reactions or from non-reactive components of the *ex situ* setup.

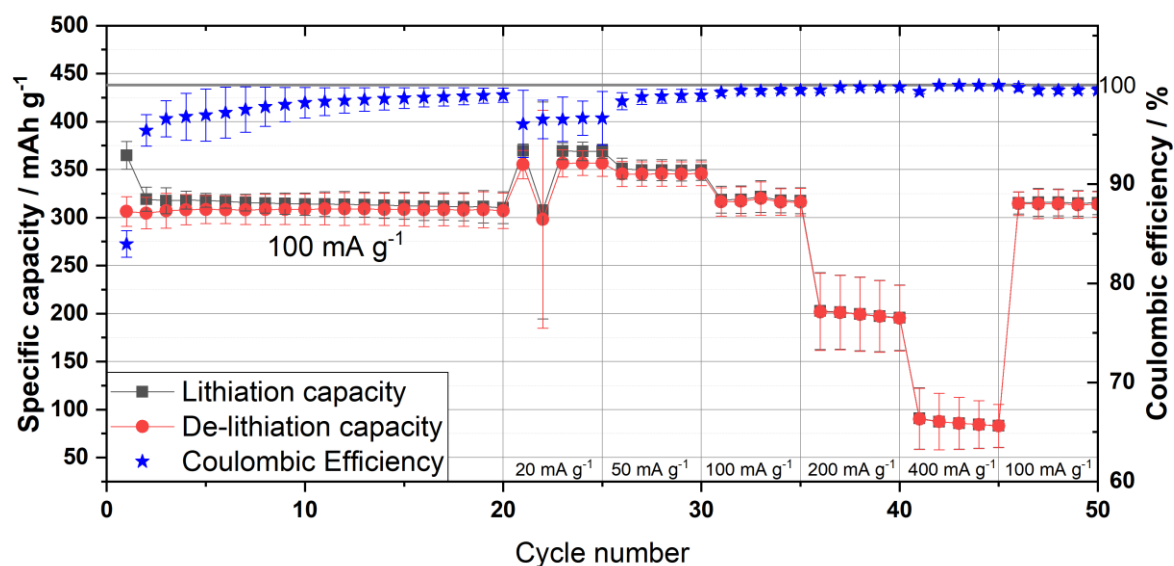


Figure S7. Electrochemical performance of graphite negative electrodes in constant current cycling lithiation/de-lithiation experiments in graphite || Li metal cells (three-electrode configuration; half-cell setup) at various specific currents with 3.4M LiTFSI in DMC as electrolyte in a potential range of 0.02 – 1.5 V vs. Li|Li⁺.

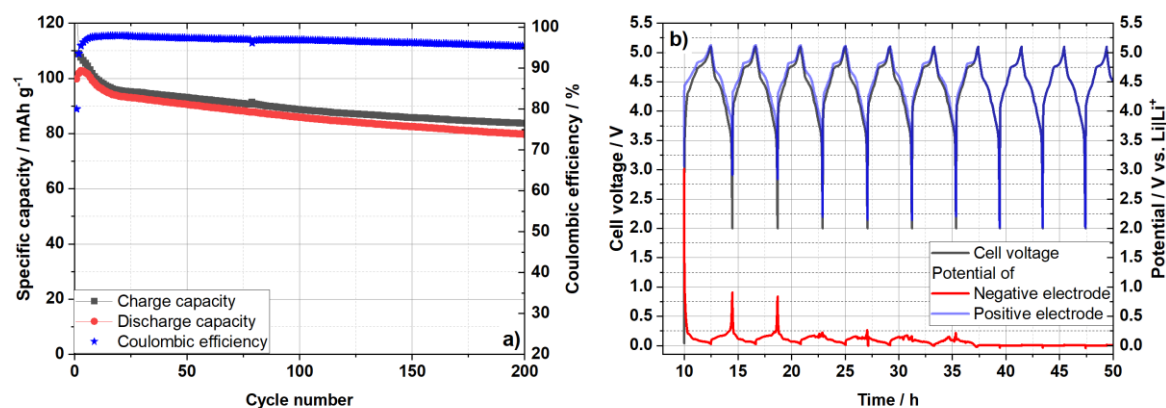


Figure S8. Electrochemical performance of graphite || graphite cells (three-electrode configuration; full-cell setup) in constant current cycling charge/discharge experiments with 3.4M LiTFSI in DMC as electrolyte in a cell voltage range of 2.0 – 5.1 V. (a) Specific charge and discharge capacity related to the mass of the positive electrode and C_{eff} ; (b) respective cell voltage and electrode potentials in the first 10 cycles of the cell shown in (a).

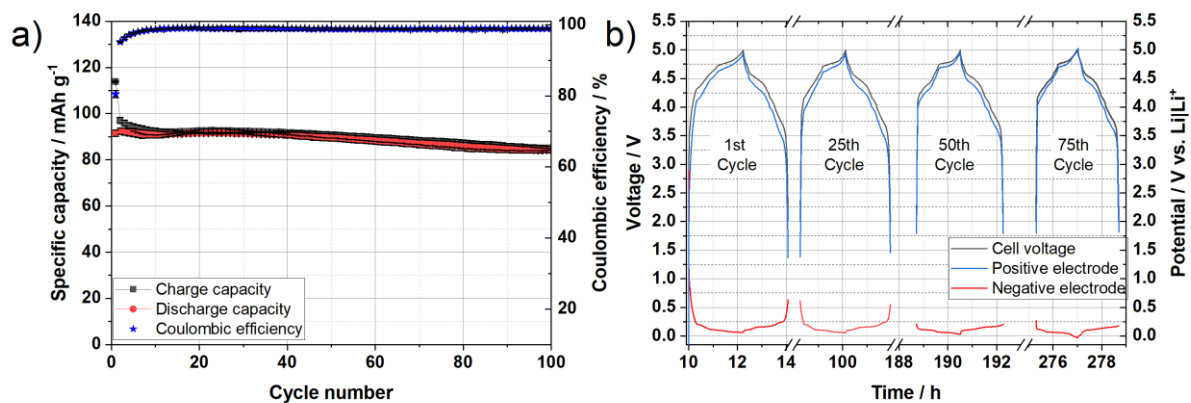


Figure S9. Electrochemical performance of graphite || graphite cells (three-electrode configuration; full-cell setup) in constant current cycling charge/discharge experiments with 3.4M LiTFSI in DMC as electrolyte in a cell voltage range of 2.0 – 5.0 V. (a) Specific charge and discharge capacity related to the mass of the positive electrode and C_{Eff} ; (two-electrode setup) (b) cell voltage and electrode potentials in different cycles.

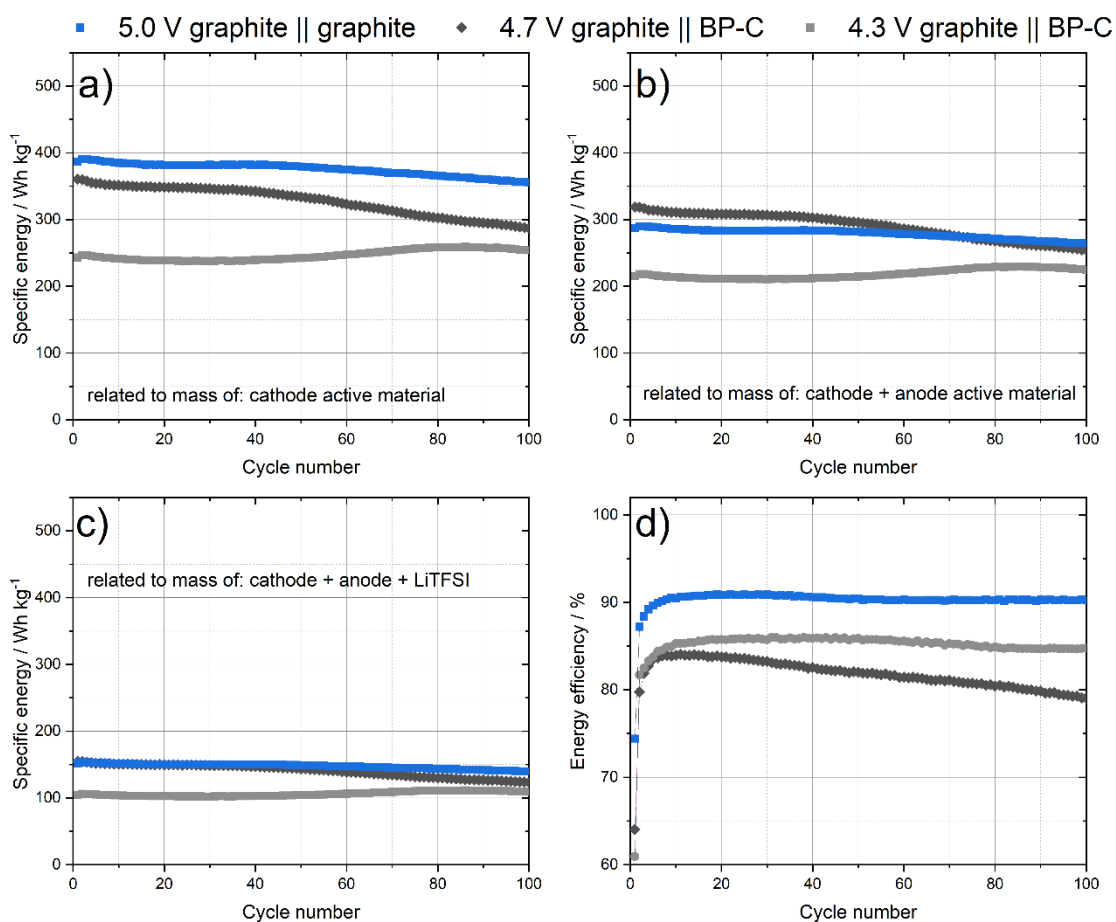


Figure S10. Specific energy of graphite || BP-C cells (two-electrode configuration; full-cell setup; cell voltage: 2.0 – 4.7 V, black, and 2.0 – 4.3 V, grey) and graphite || graphite cells (three-electrode configuration; full-cell setup; 2.0 – 5.0 V, blue) in constant current cycling experiments: Specific discharge energy related to the mass of a) the positive electrode active material; b) both electrode active materials; c) both electrode active material and mandatory LiTFSI salt for ion uptake. d) Energy efficiency. 3.4M LiTFSI in DMC as an electrolyte at a current of 50 mA g⁻¹ (related to the positive electrode).

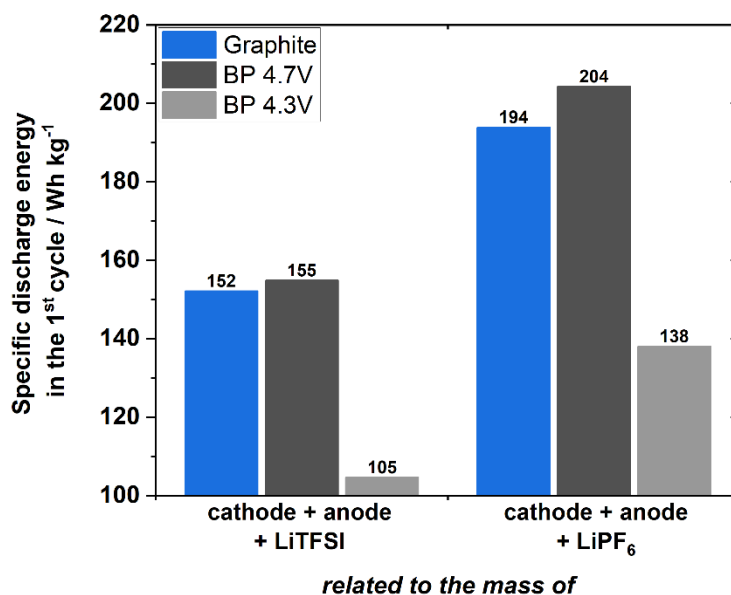


Figure S11. Specific energy of PGDIBs cells and DGB cells in the first cycle related to the mass of cathode, anode and different active lithium salts. Practical values of LiTFSI cells were calculated with LiPF₆ molar mass to show the impact of the used lithium salt on the specific energy.

In **Figure 10** the specific energy, C_{Eff} and capacity retention of different reported GDIBs are compared. **Table S5** shows the values which were taken from the respective study to calculate the specific energy per total electrode active mass.

Table S5. Overview of considered values for **Figure 10** based on reported studies.

Cell chemistry	Reported capacity C_{reported}	Factor R [including active salt]	Mean discharge voltage $U_{\text{mean discharge}}$	Calculated specific energy (including active salt)	C_{Eff} (10 th cycle)	Capacity 100th cycle	Capacity retention
Graphite Ge ^[2a]	281 mAh g ⁻¹ (per mass of N)	0.07692 (1/13) [LiPF ₆ : 0.0733; LiTFSI:0.07044]	3.7 V	79.97 Wh kg ⁻¹ (73.24 Wh kg ⁻¹)	78%	182 mAh g ⁻¹	64.8 %
Graphite Si ^[2b] (5.0V)	78.2 mAh g ⁻¹ (per mass of P)	0.891 („CB 2.2“) [LiPF ₆ : 0.569; LiTFSI:0.431]	4.15 V	289 Wh kg ⁻¹ (139.87 Wh kg ⁻¹)	90 %	78 mAh g ⁻¹	99.7 %

The specific energy per total mass of active material was calculated by:

$$E = C_{reported} * R * U_{mean discharge} \quad (6)$$

where R describes the factor to calculate the specific capacity per total active mass, which was calculated based on the given mass ratio (N/P for Ge: 1/12 and for Si:2.2/1).^[2]

For including the active salt in calculations, a XC₂₀ – GIC (X: PF₆⁻ or TFSI⁻) was used. In case of Graphite || Si,^[2b] the following formula and values for R were used to calculate the specific capacity including anode, cathode and active salt:

$$R = \left(\frac{1}{1 + \left[\frac{\frac{1}{\left(\frac{\text{spec. Capacity (Anode)}{\text{Balancing}} \right)}}{\text{spec. Capacity (Cathode)}} \right] + \left(\frac{\frac{1}{\left(\frac{M(C)}{n} \right)}}{\text{Number C-Atoms for GIC} * n(\text{Number of Anions per GIC}) * M(\text{Salt})} \right)} \right)} \quad (7)$$

$$R(\text{Si, LiTFSI}) = \left(\frac{1}{1 + \left[\frac{\frac{1}{\left(\frac{2248}{2.2} \right)}}{125} \right] + \left(\frac{\frac{1}{\left(\frac{1}{12} \right)}}{20} * 287.09 \right)} \right)$$

Comment 1:

As discussed, a somewhat smaller capacity (per mass of cathode) has been achieved in DGB cells compared to the capacity in the PGDIB cell operated at 2.0 – 4.7 V. This achieved specific capacity per mass of the cathode plays an important role in defining several important metrics including the specific energy, C_{Eff} and cycling stability. Upon a closer inspection, it is visible that a lower maximum cathode potential (≈ 5.0 V vs. $\text{Li}|\text{Li}^+$) is reached in the DGB cell than the maximum potential in the case of the graphite || BP-C cell, leading naturally to a lower capacity (see **Figure S9**). However, sticking to the chosen N/P ratio, a higher cathode potential was practically not achievable since an increased cut-off cell voltage (5.1 V) for the DBG cell leads to Li metal plating on the anode (see **Figure S8**). This effect of Li metal plating can be explained by a stronger difference in the C_{Eff} of anode and cathode in the first cycle for the two types of cells (DGB and PGDIB). In PGDIB cells the anode and cathode show nearly the same initial C_{Eff} ($\approx 75\%$, see **Figure 2** and **Figure 4**), while the anode and cathode in DGB cells show a difference of $\approx 10\%$ in the initial C_{Eff} (graphite anode: 85%; graphite cathode: 75%; refer to a comparison of **Figure S7** and **Figure 4**). This leads to accelerated Li^+ ion trapping in the anode and therefore, to faster Li metal plating. To counteract this drawback of the DGB cell and inhibiting Li metal plating, a different N/P ratio in accordance with the cell voltage and other requirements can be adapted. If the N/P ratio is therefore increased, this will affect multiple cell metrics as the total mass of active materials is changed and in turn, increase the benefit of high-capacity anodes with lowered mass.

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