- **Non-edible plant seeds of** *Acacia farnesiana* **as a new and effective source for biofuel**
- **production**
- 3 Inam Ullah Khan<sup>1\*</sup>, Abdul Haleem<sup>1,2\*</sup> Assad Ullah Khan<sup>3</sup>
- *<sup>1</sup> Department of Chemistry, Quaid-i-Azam University, Islamabad 45320, Pakistan*
- *<sup>2</sup>Department of Chemistry, Faculty of Natural Science, The University of Haripur, Haripur,*
- *KPK 22620, Pakistan*
- *<sup>3</sup>Department of Economics, University of Science and Technology Bannu, Bannu, KPK 28100,*
- *Pakistan*
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- \*Corresponding authors: Inam Ullah Khan & Abdul Haleem
- E-mail: [khanqau123@yahoo.com](mailto:khanqau123@yahoo.com) and haleem0300@gmail.com

#### **Supporting Materials**

### **S1. Plant description**

 In this study, *Acacia farnesiana* (AF) is chosen as the inedible raw material to produce biodiesel. Its scientific name is *Acacia farnesiana,* Family *Leguminosae (Mimosoideae*), native to North America. This tall semi-evergreen native shrub or small tree is commonly referred to as sweet acacia, Huisache, etc., with soft, medium-green feather-like, finely divided small leaves. The slightly thick stem is rich in chocolate brown or grey, with long and pointed needles. The small, puff-like yellow flowers are very fragrant, appear in clusters in late winter, and then occasionally spread out after each new flush, providing nearly four seasons of flowering. An area of about one hectare wills 91,500 kg of seeds yield, and the efficiency of oil per hectare is approximately 21,250 kg. The fruit is an elongated pod, 3 to 6 inches long, dry, and covered with hard skin, brown. Green colour attracts birds; squirrels and other mammals have no obvious littering problems and stick to the trees, which is very beautiful. The long-lasting fruit has a smooth appearance and contains seeds cherished by birds and other wildlife.

### S2. **Mechanical extraction of** *Acacia farnesiana* **seed**

 The mechanical extraction of AF seeds was done by two different electric oil expeller machines, FANGTAI SHIBAYOUFANG FL-S2017 China (less power extractor) and FANGTAI SHIBAYOUFANG J508, China (high power extractor). Pre-treatment of seed is essential for mechanical extraction, which can increase the amount of oil recovery. After 2-3 revolutions, a large yield of crude AFSO was obtained. Through mechanical extraction,8.7 wt.% oil content occurs. The oil removed from the seed by mechanical presses desires additional handling of extraction and filtration to produce a purer raw feedstock. The oil production of AFSO was calculated by the following equation (1).

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 Conversion % =   
Total seed weight  
Total seed weight × 100 (1)

 Further following steps were done to get the AFOB, filtration, rotary evaporation for access methanol, heating, trans-esterification, settling, separation, and washing.

### **S3. GC-MS Procedure**

 The obtained AF biodiesel results were checked and tested by GCMS (QP2010SE, Shimadzu, 44 Japan), furnished with a capillary column: PEG-20M (30 m  $\times$  0.32 mm  $\times$  1 um film thickness). Helium gas flow rate 1.2 mL/min; split ratio 40:1; the injector temperature and injection volume were 220 ˚C and 1 uL; Furnace heat up mode was 100 °C for 1 min, then 47 from 100 °C rises to 210 °C at the increase rate of 10 °C/min. Sensor heat mode was 210 °C, 48 and then for 20 min, the temperature was continuing at 210 °C; ion source temperature of 200 ˚C; for electron impact 70 eV ionization mode used; mass range of 35-500 m/z. The AF FAMEs were identified with the mass spectrometry fragmentation design provided by the GCMS system software, as matched with those stored in the mass spectrometry library NIST14, and their fatty acid identity was further verifying by matching with known standards values.

### **S4. ICP-OES procedure for AFOB elemental analysis**

 For the presence of metals in the AFSO biodiesel, it was explored through Inductively Coupled Plasma Spectrometer (Spectro-blue, Germany) and Elemental Analyzer (Vario EL CUBE, Germany). For the ICP-OES test, we take 1 g of oil sample for incinerating. The ashing process is as follows: Increase the oven temperature to 200 ˚C in one hour, then increase the heat to 500 ˚C and kept for 2 h, and finally increase to 800 ˚C and kept for 5 h. 60 The ash was dissolved in 10 mL of 2 % HNO<sub>3</sub>. The prepared sample was used for elements finding and concentration test of the KP biodiesel (AFBD).

### **S5. Elemental analyzer (EA) procedure for AFOB elemental analysis**

 Procedure for EA sample preparation: Element analyzer (Vario EL CUBE, Germany), the instrument was used todetecting the H, N, C, and O concentration of AF biodiesel. We take 0.5 mL of AFBD, 3 mL of concentrated HCl and 1 mL of Nitric acid in a tube and put them for 10-15 min rest, to dissolve the oil in the solution. Fresh reagents can be used for sample preparation. The aqua regia amount would be double than the sample. Then we take 1 mL of prepared solution in a new tube and add deionized water up to 5 mL. We repeated the same technique 2-3 times until the sample becomes clean and bright and use for C, H, N, and O concentration testing.

## 72 **Table S1. Source collection, oil extraction and transesterification of non-edible AF seed**

### 73 **oil as biodiesel**



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### 76 **Table S2. Catalysts effect on FAMEs conversion yield**



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# 78 **Table S3.** AF FAMEs detail process of optimization

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83 **Table S5.** <sup>1</sup>H NMR spectroscopic data showing the chemical composition of various methyl 84 esters (Methoxy proton) in AF biodiesel (FAMEs)

Integration value	<b>Chemical</b> shift ppm	<b>Multiplicity</b>	<b>Inferences</b>		
$\overline{3}$	0.88	Multiplet	$CH3$ is attached to the aliphatic group.		
16	1.27	Multiplet	A long aliphatic chain is present.		
2	1.61	Quartet	$CH2$ group is attached to terminal $CH3$ .		
3	2.03	Multiplet	$CH2$ of long-chain aliphatic (Saturated) group.		
2	2.29	Triplet	$CH2$ group is attached with CH of long aliphatic (unsaturated/Olefinic group).		
	2.77	Triplet	CH group is attached with an electron-withdrawing carbonyl group.		
3	3.66	Singlet	Methoxy $(OCH3)$ group attached with an electron- withdrawing carbonyl group.		
3	5.33	Multiplet	Olefinic hydrogen of a long-chain unsaturated aliphatic group		

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 **Table S6.** <sup>13</sup>C NMR spectroscopic data showing the chemical shift values corresponding to various structural features in AF (Methoxy carbon) FAMEs







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95 **Table 8.** AF FAMEs EA (elemental analysis) study for C, H, N, and O

Ultimate analysis	AF-BD	pistachio shell <sup>1</sup>	Peach Stone <sup>2</sup>	Apricot kernel shells $3$	Cherry Stones <sup>4</sup>	Mahua Seed <sup>5</sup>
$C\%$	76.37	42.41	45.92	47.33	52.48	61.24
H%	13.34	5.64	6.09	6.37	7.58	8.40
$N\%$	2.18	0.070	0.580	0.370	4.54	4.12
$O\%$	8.11	51.87	47.38	45.93	35.30	25.50
Higher heating	23.39	22.21	24.07	24.29	24.11	25.30
value $(MJ/kg)$						

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## 97 **References**



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