

Supporting Information

A multi-gram synthesis to pure HMF and BHMF

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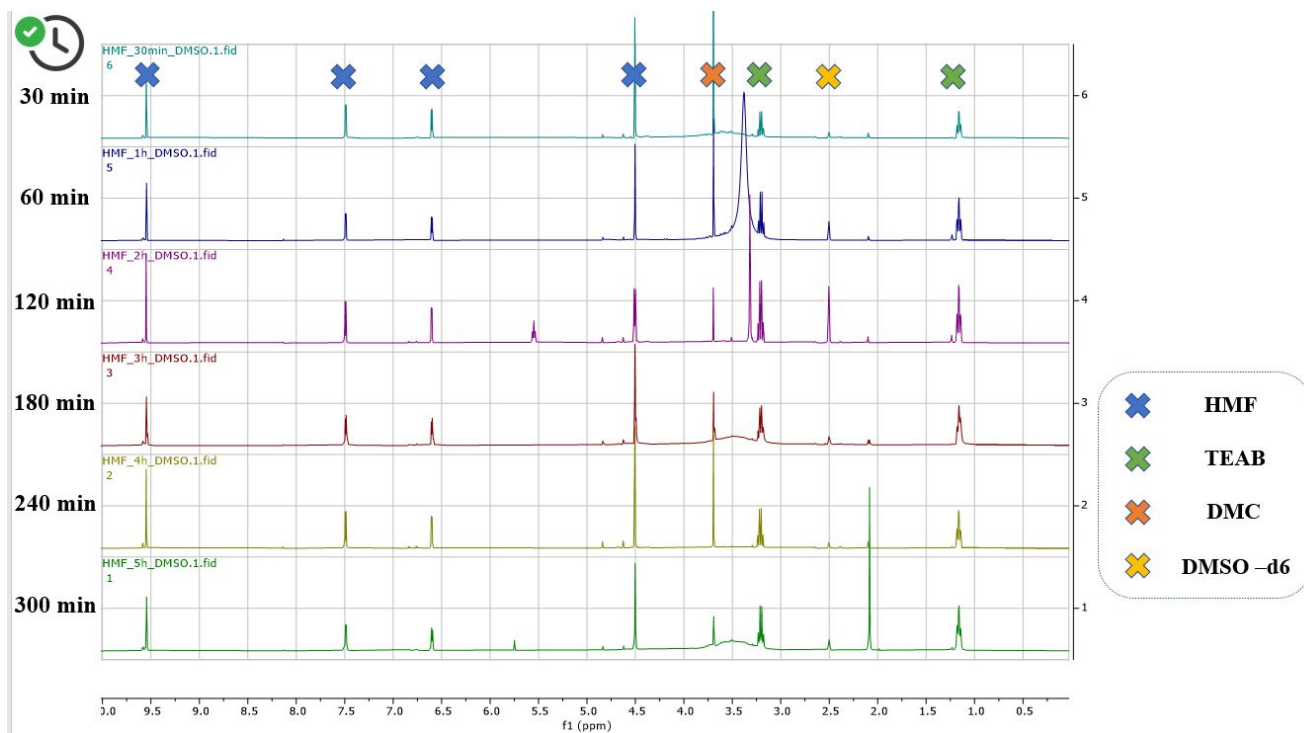
Catalysts properties overview

Table S1. Purolites and Amberlysts properties.

	Amberlyst-15	Amberlyst-36	CT151	CT269	CT275
Polymer structure	Macroporous polystyrene crosslinked with divinylbenzene				
Appearance	Spherical Beads				
Functional Group	Sulfonic Acid				
Ionic Form	H ⁺ form				
Particle Size Range	< 300 μm	600-850 μm		425 - 1200 μm	
Dry Weight Capacity	≥ 4.7 eq/kg (H ⁺ form)	≥ 5.4 eq/kg (H ⁺ form)	5.1 eq/kg (H ⁺ form)	5.2 eq/kg (H ⁺ form)	5.2 eq/kg (H ⁺ form)
Moisture Retention	≤ 1.6% (H ⁺ form)	51 - 57 % (H ⁺ form)	54 - 59 % (H ⁺ form)	51 - 57 % (H ⁺ form)	51 - 59 % (H ⁺ form)
Surface Area	53 m ² /g	33 m ² /g	15 - 25 m ² /g	35 - 50 m ² /g	20 - 40 m ² /g
Pore Volume	0.40 mL/g	0.20 mL/g	0.15 - 0.30 mL/g	0.30 - 0.50 mL/g	0.40 - 0.60 mL/g
Average Pore Diameter	300 Å	240 Å	250 - 400 Å	250 - 425 Å	400 - 700 Å
Temperature Limit	120 °C	150 °C	150 °C	130 °C	130 °C

a) All Purolite® information is available on <https://www.purolite.com/index>. All Amberlyst-15 information are available on the DuPont (<https://www.dupont.com/content/dam/dupont/amer/us/en/watersolutions/public/documents/en/45-D00927-en.pdf>).

^1H -NMR spectra of a typical HMF synthesis at different times (samples taken from #6 Table 1 reaction)

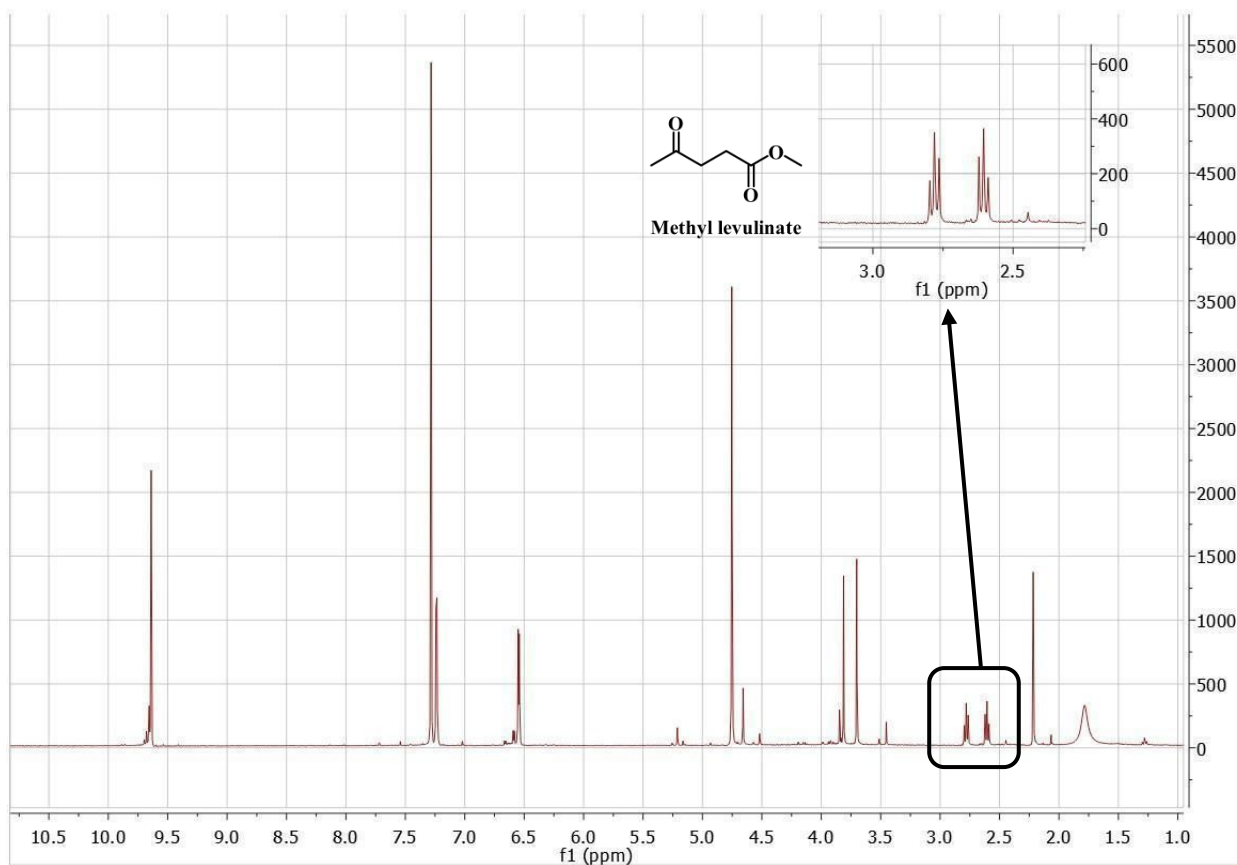


Additional reactions for the synthesis of HMF in autoclave

Table S2. Synthesis of HMF in autoclave with temperatures higher than 110 °C.

#	DMC [mL]	TEAB [%]	Purolite CT275DR [%]	T [C°]	Time [h]	¹ H-NMR Selectivity [%]			HMF ¹ H-NMR Yield [%]
						HMF	ML	Other	
1	40	10% wt.	5% wt.	120	2	97	3	0	68
2	40	10% wt.	5% wt.	130	2	96	4	0	70
3	40	10% wt.	5% wt.	150	2	68	18	16	46
4	40	10% wt.	5% wt.	150	4	71	4	25	60

¹H-NMR of #3, Table S2 in CDCl₃.



Crystallization/Purification of HMF

Table S3. Solvents used in the HMF crystallization trials.^a

#	Solvent	HMF crystals	Crystal yield %	Crystals
1 ^b	Et ₂ O	✓	ca. 50	Bubble-shape, yellow crystals 
2 ^{b,d}	Et ₂ O + Hexane	✓	ca. 30	Needle-shape, yellow-orange crystals. 
3 ^c	t-butyl methyl ether (TBME)	✗	/	/
4 ^c	THF	✗	/	/
5 ^c	2-MeTHF	✗	/	/
6 ^c	Hexane	✗	/	/
7 ^b	Acetone + Hexane	✗	/	/
8 ^{b,e}	AcOEt + Hexane	✓	ca. 30	Needle-shape, yellow-orange. They melt faster. 
9 ^c	AcOEt	✗	/	/

^a After obtaining the dark brown reaction crude, solvent(s) was added, the organic phase was collected in a beaker and put in freezer for 48h; ^b Separation between organic phase and dark brown crude oil; ^c Solvent dissolves the dark brown crude oil; ^d 10 mL of Et₂O were poured in the reaction crude, then hexane was added until the formation of a white-yellow powder; this procedure repeated two more times, the recovered organic phase were then put in the freezer for 48h; ^e Dark brown oil dissolved in 5 mL of AcOEt, then hexane was added until the formation of a white-yellow powder; this procedure repeated two more times, the recovered organic phase were then put in the freezer for 48h.

Green metrics evaluation

Explanation of waste-related Green Metrics:

- E-kernel: Mass contribution to the total E-factor from reaction by-products, reaction side products, and unreacted starting materials;
- E-reaction solvent (E-rxn solv): Mass of reaction solvent necessary for the synthesis of the target product;
- E-catalyst (E-cat): Mass of the catalyst necessary for the synthesis of the target product;
- E-workup: Mass of the reagents used in the work-up procedures necessary to obtain the target product;
- E-purification (E-purif): Mass of the reagents used in purification procedures necessary to obtain the pure target product;

Comprehensive table for the evaluation of green metrics

Table S4. Environmental assessment of different procedures with PMI lower than 100 (#1-17) and higher than 100 (#18-25).

#	Method ^b	D-Fructose [g]	Catalyst	Rxn solvent	Yield [%]	E-kernel	E-rxn solv.	E-cat	E-workup	E-purif	E-total	PMI	Ref.
1*	B	0.64	CeP ₃ ^c	DMC-water	68	1.11	44.43	0.33	39.6	0	85.47	86.47	Dibenedetto <i>et al.</i> ²⁸
2 ^d	C	1	HCl 0.25M	MIBK	74.3	0.92	23.02	21.54	0	0	45.48	46.48	Brasholz <i>et al.</i> ²⁹
3*	B	1	FeCl ₃ /Et ₄ NBr	NMP ^e	78	0.83	18.83	0.55	67.29	0	87.5	88.5	Tong <i>et al.</i> ³⁰
4* ^f	B	1.8	HBr/silica	THF	95	0.5	88.8	4.01	0.83	>>0	94.14	95.14	Rajmohan <i>et al.</i> ³¹
5 ^d	B	2.1	Ti/Si500	Dist water/TEAC	95.2	0.5	7.14	0.14	5.64	0	13.42	14.42	Novamont ³²
6 ^g	B	5	[PPFPy][HSO ₄]	DMSO	82.7	0.73	30.4	0.92	7.6	0	39.65	4.17 ^h	Shi <i>et al.</i> ³³
7	B	5	[PPFPy][HSO ₄]	DMSO	82.7	0.73	30.4	0.92	7.6	0	39.65	40.65	Shi <i>et al.</i> ³³
8 ^g	B	5	[PPFPy][HSO ₄]	DMSO	84.4	0.69	29.79	0.9	59.58	0	90.97	57.34 ^h	Shi <i>et al.</i> ³³
9	B	5	[PPFPy][HSO ₄]	MIBK/water	83	0.72	28.86	0.92	5.49	0	35.99	36.99	Shi <i>et al.</i> ³³
10 ^{f,i}	A	5	CO ₂	H ₂ O	92	0.55	5.59	0	0	0	6.14	7.14	Motokucho <i>et al.</i> ³⁴
11 ^{d,i}	B	10	H ₂ SO ₄ /LiBr	DMAc	45.3	2.15	29.56	3.26	21.34	0	56.31	57.31	Kovash <i>et al.</i> ³⁵
12 ^g	A	10	Pur CT275DR	DMC	50.3	2.03	12.96	0.45	27.3	6.49	49.24	14.25	This work
13	A	10	Pur CT275DR	DMC	72	0.98	8.45	0.3	17.8	0	27.53	5.13	This work
14* ^f	B	10	Amb-15	CH ₃ CN:TEAC	78	0.82	21.27	2.18	7.19	0	31.46	32.46	Brown <i>et al.</i> ³⁶
15*	B	20	Amb-15	DMC:TEAB	70	1.04	17.45	0.61	5.52	0	24.62	25.62	Musolino <i>et al.</i> ¹⁴
16*	B	20	Amb-15	water	91	0.57	0.7	7.28	86.84	0	95.39	96.39	Simeonov <i>et al.</i> ⁹
17*	B	20	BF ₃ OEt ₂	DMC	76	0.89	16.14	0.53	2.55	0	20.11	21.11	Musolino <i>et al.</i> ¹⁴
18 ^{m,i,g}	B	1.5	H ₂ SO ₄	[BMIM][Cl]	78	0.83	8.55	0.02	605.74	34.68	649.81	650.81	Galkin <i>et al.</i> ²²
19 ^m	B	1.5	H ₂ SO ₄	[BMIM][Cl]	78	0.83	8.55	0.02	605.74	0	615.13	616.13	Galkin <i>et al.</i> ²²
20*	B	9	Cationic resin/activate carbon	water	48	1.97	49.5	19.8	260.4	0	331.67	332.67	Vinke <i>et al.</i> ³⁷
21*	B	18	BF ₃ OEt ₂	DMSO-toluene	60	1.37	26.41	0.29	67.74	153.79	249.60	250.60	Musau <i>et al.</i> ³⁸
22 ^{m,i,g}	B	18	H ₂ SO ₄	[BMIM][Cl]	72.9	0.96	7.83	0.02	647.79	37.03	693.69	694.69	Galkin <i>et al.</i> ²²
23 ^m	B	18	H ₂ SO ₄	[BMIM][Cl]	72.9	0.96	7.83	0.02	647.79	0	656.61	657.61	Galkin <i>et al.</i> ²²
24* ⁿ	C	70	WCl ₆ /HY	[BMIM]Cl/THF	55	1.62	170.04	0.27	0	0	171.93	172.93	Chan <i>et al.</i> ³⁹

^a E-excess is not reported in the table as its value was zero for all the synthetic procedure reported; the reported metrics do not consider the preparation of the catalyst; procedures signed by a star were already reported in our previous article [13] ^b A = Autoclave, B = Batch, C = Continuous flow; ^c CeP₃ is Cerium Phosphate catalyst with formula [(Ce(PO₄)1.5(H₂O)(H₃O)0.5(H₂O)_{0.5})]₃; ^d Amounts of work-up and/or purification materials are not reported in the original article; ^e NMP = N-Methyl-2-pyrrolidone; ^f Excluding column chromatography; ^g Including purification; ^h DMSO is partially recovered; ⁱ Reaction conducted for 148 h; ^j NHC is 1,3-bis(2,6-diisopropylbenzyl)imidazolyliidene; ^m Aqueous solution of NaCl/NaHCO₃ not included; ⁿ Reaction conducted in continuous biphasic system over a 42 h period where 7 cycles of 10 g each of D-fructose run at 6 h intervals were combined.

Ecoscale evaluation

Table S5. Ecoscale scores for the selected procedures for HMF synthesis and isolation.

Reference	Amount of D-fructose g	Ecoscale value	Comments
Brasholz <i>et al.</i> ²⁹	1.00	56	Continuous flow reaction
Galkin <i>et al.</i> ²²	1.5	76	Purification included
Novamont ³²	2.10	89	Ti/Si 500 (catalyst) not included
		67	Reagent for catalyst synthesis included [PPFPy][HSO ₄] not included, DMSO recovered by distillation from reaction crude
Shi <i>et al.</i> ³³	5.00	83	Reagent for catalyst synthesis included [PPFPy][HSO ₄] not included, DMSO recovered by distillation from reaction crude
		36	Reagent for catalyst synthesis included [PPFPy][HSO ₄] not included, DMSO recovered by distillation from reaction crude; purification by AcOEt/H ₂ O extraction
Shi <i>et al.</i> ³³	5.00	81	Reagent for catalyst synthesis included
		34	MIBK/water extraction
Shi <i>et al.</i> ³³	5.00	82	Reagent for catalyst synthesis included
		32	Reaction performed for 168 h in autoclave; amount of CO ₂ employed not specified
Motokucho <i>et al.</i> ³⁴	5.00	80	HMF isolated as yellow liquid
Kovash <i>et al.</i> ³⁵	10	43	Purolite not available in the database (Amb-15 used instead of Purolite)
This work with purif. (50 % yield)	10	60	Purolite not available in the database (Amb-15 used instead of purolite)
This work, no purif. (72% yield)	10	71	Large-scale reaction in rotatory evaporator
Galkin <i>et al.</i> ²²	18	71	

Comparison of Yield, E-factor and PMI of reactions with PMI > 100.

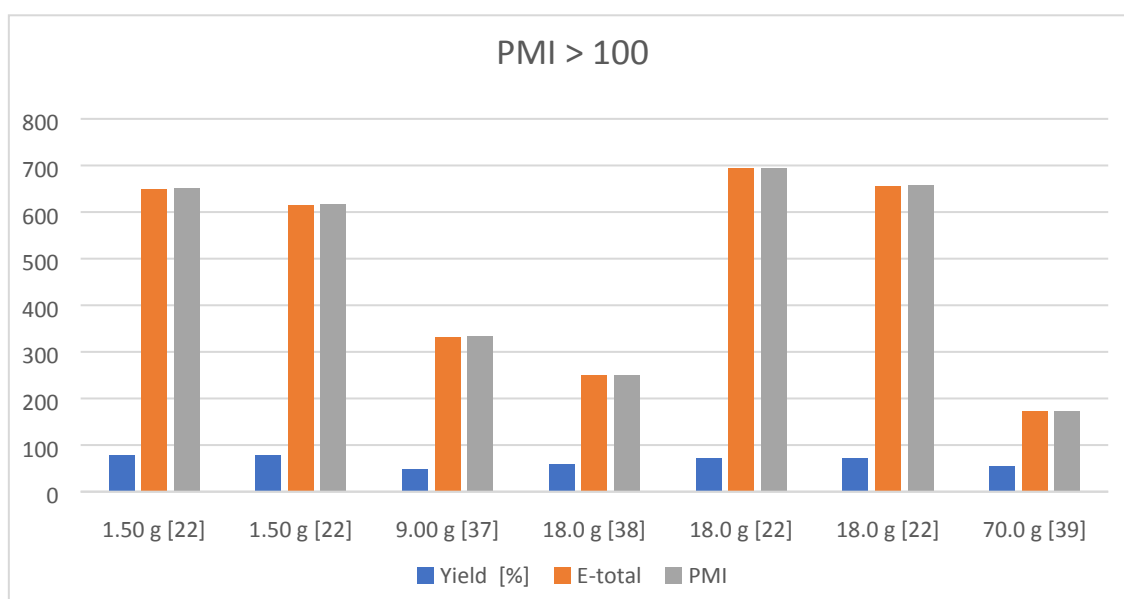
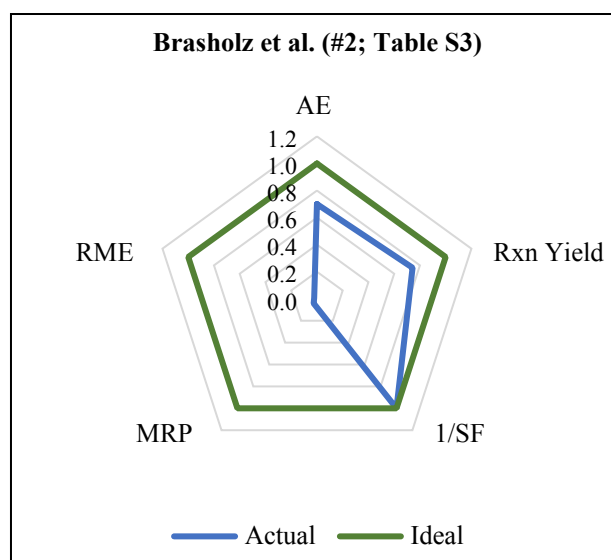
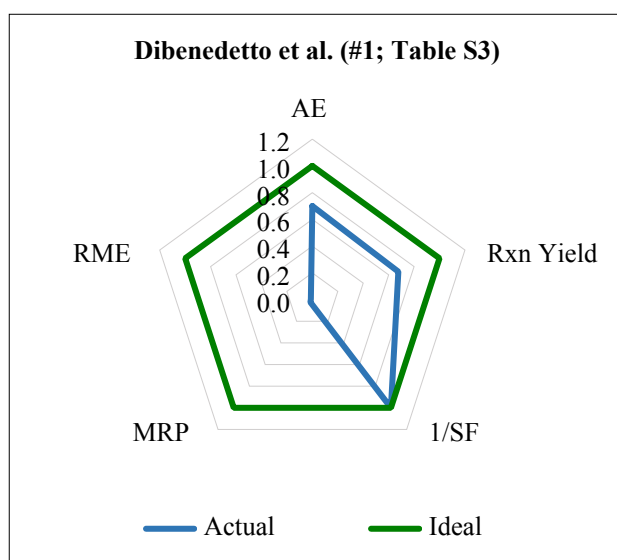
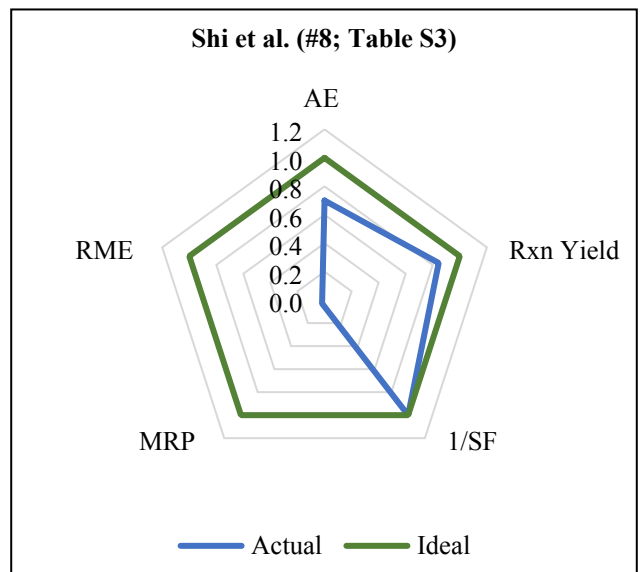
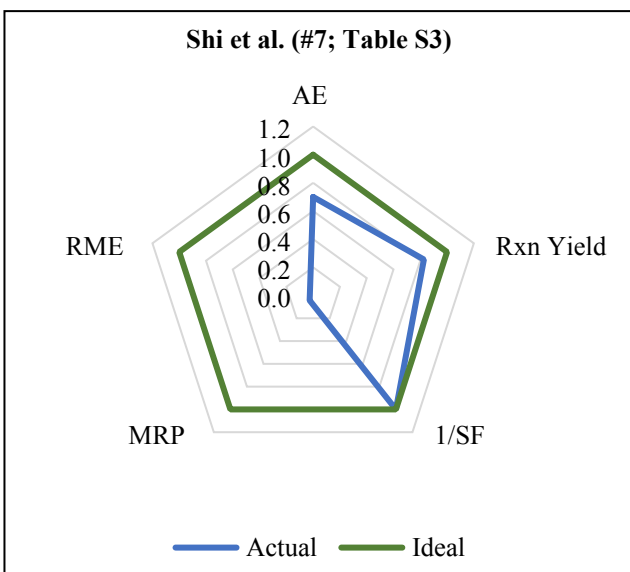
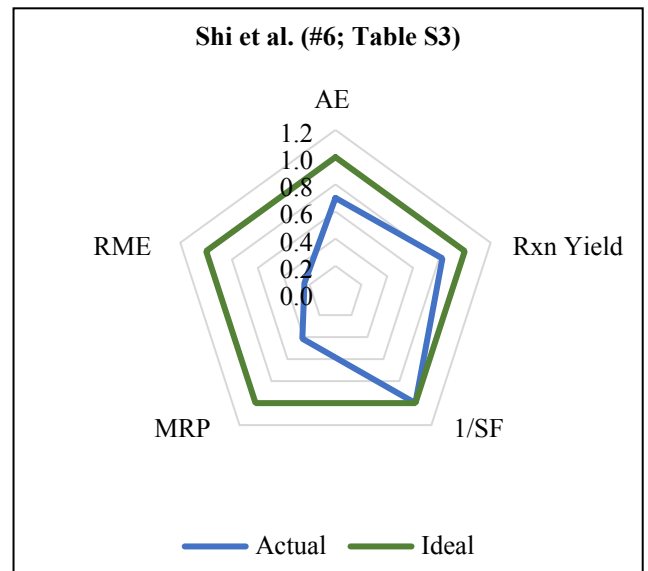
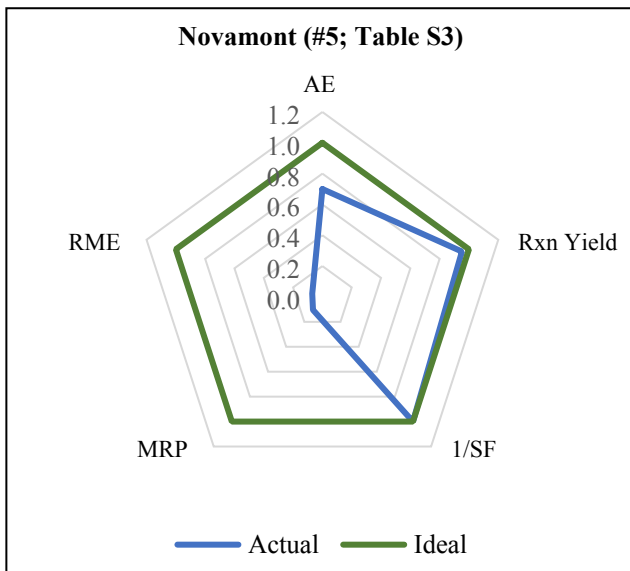
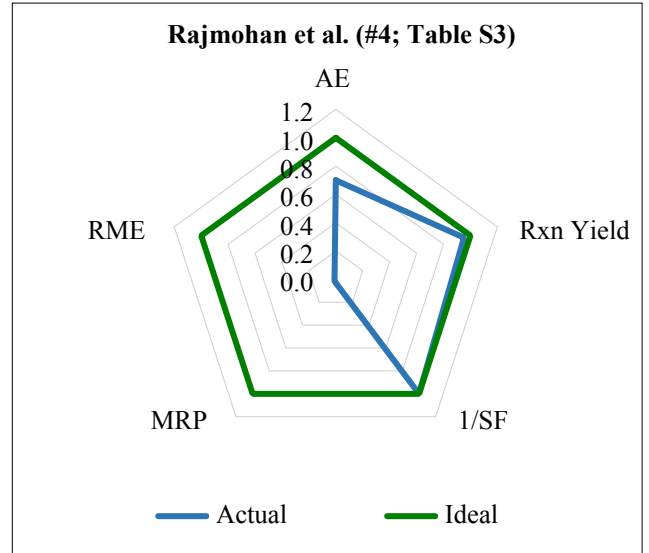
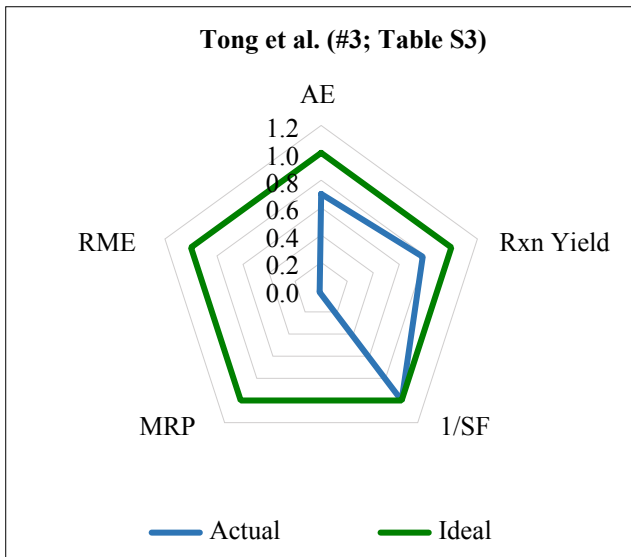
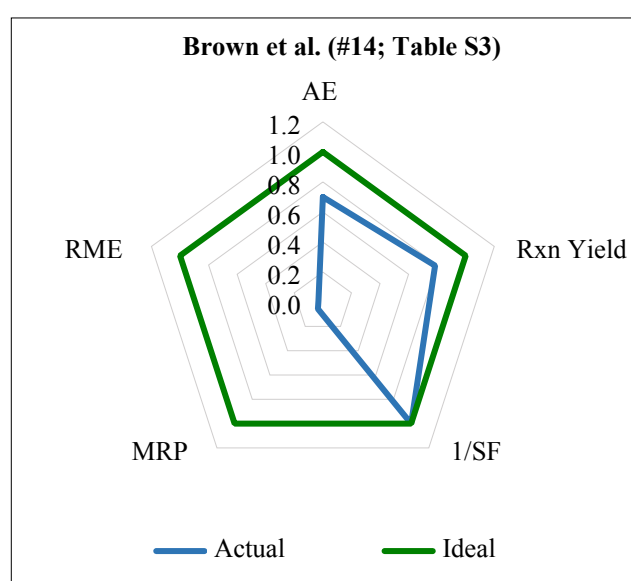
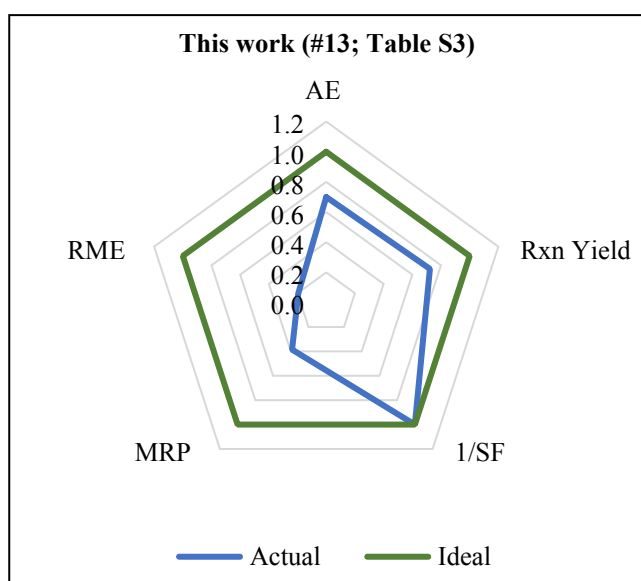
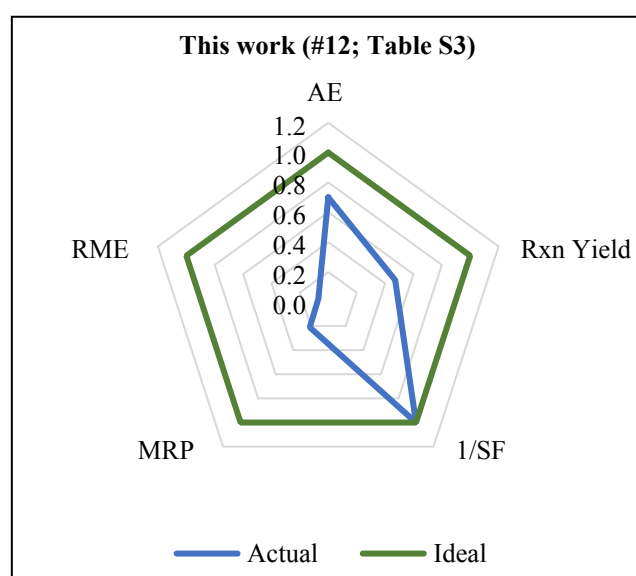
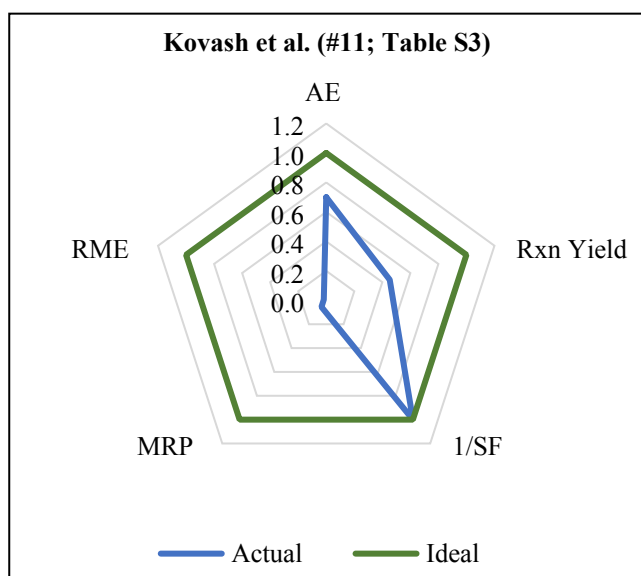
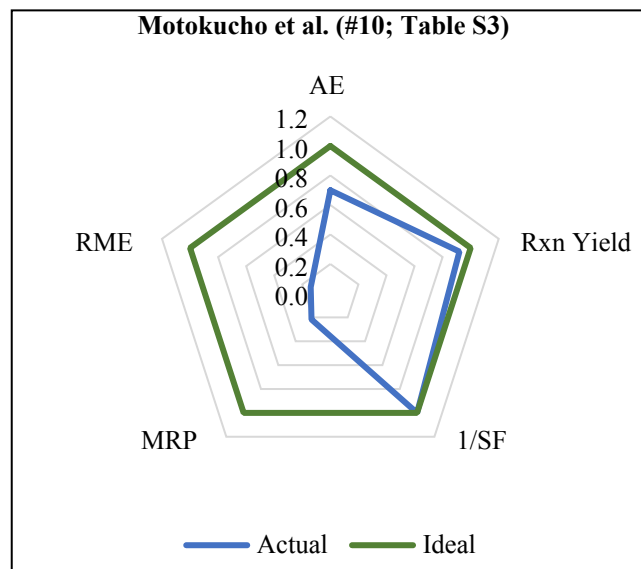
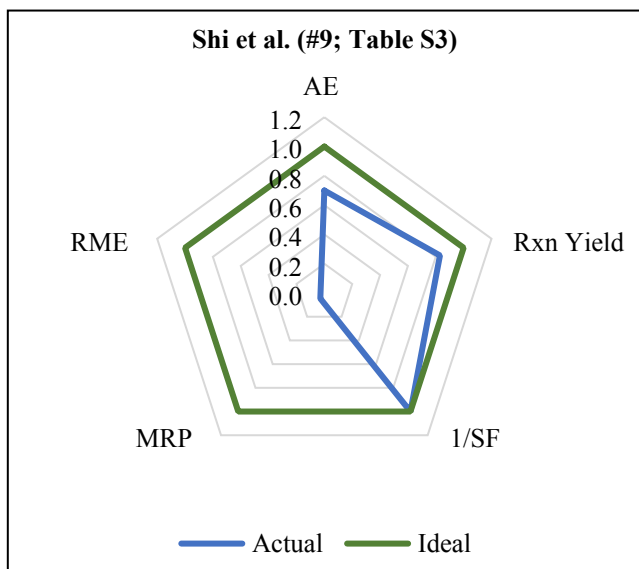


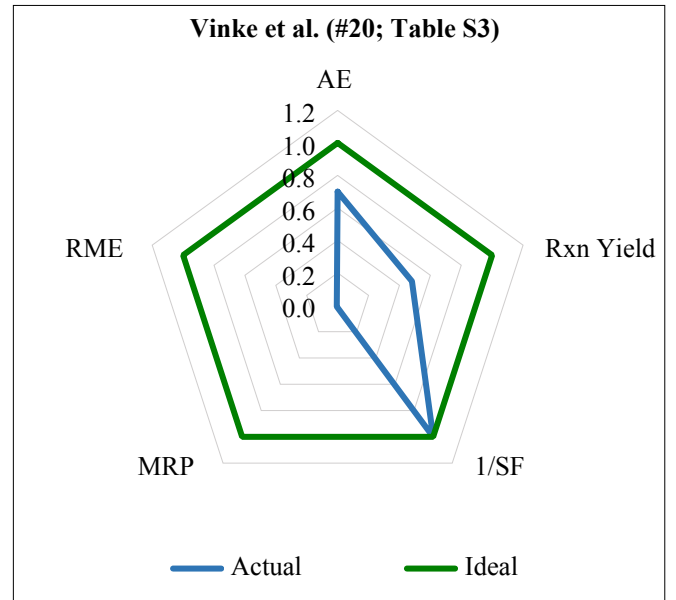
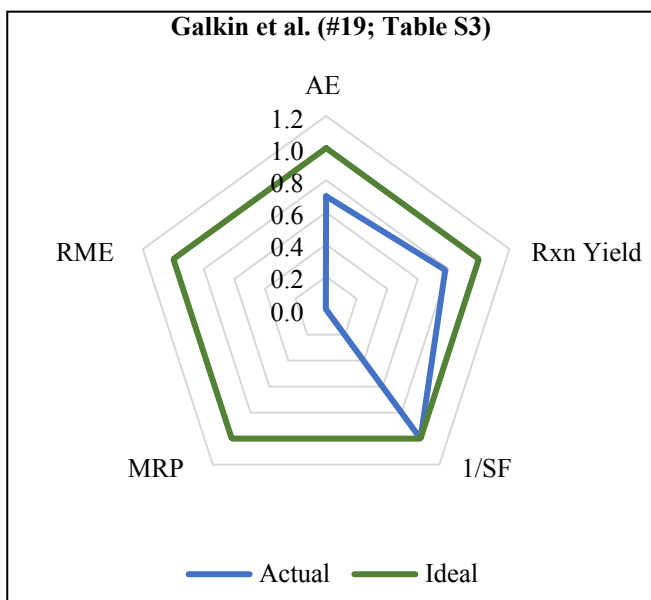
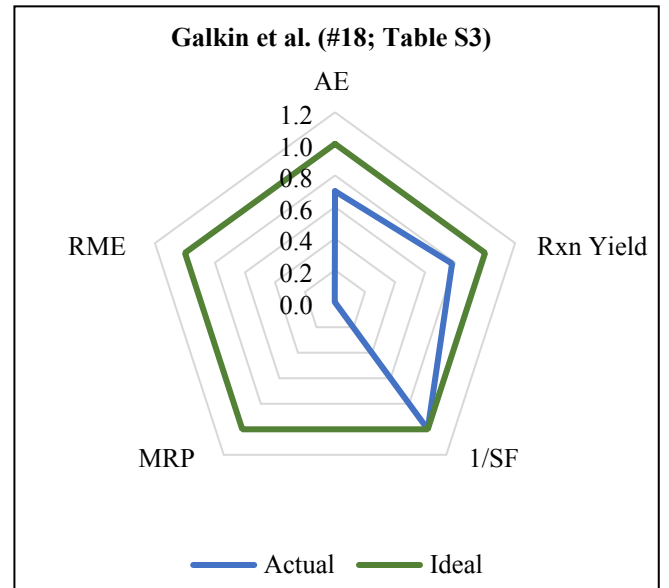
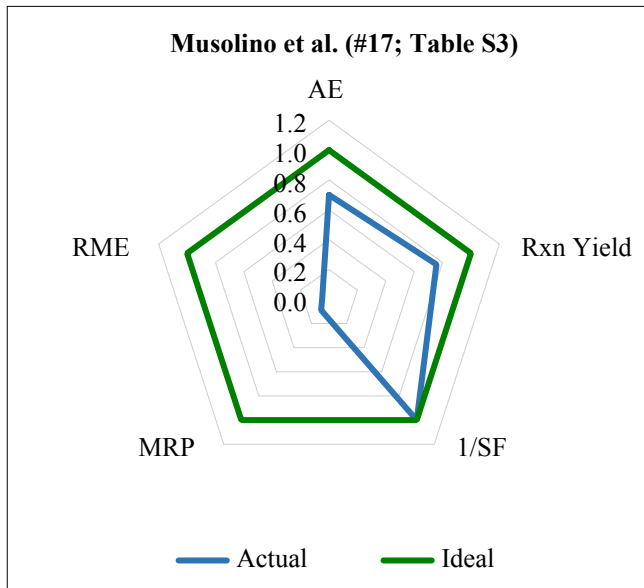
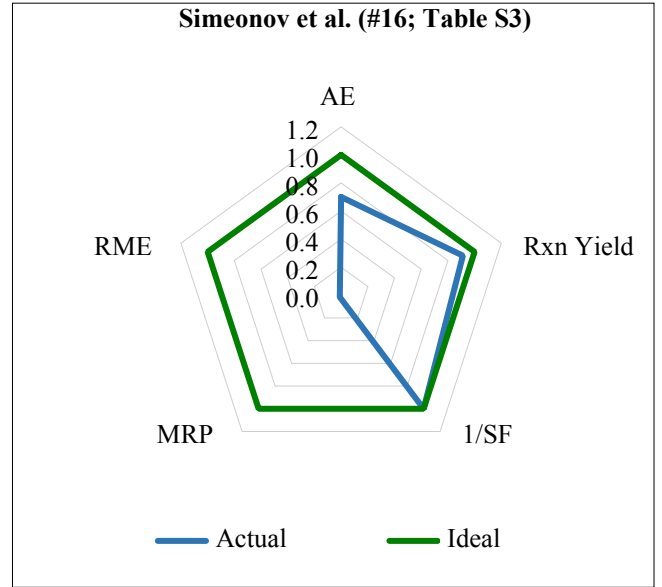
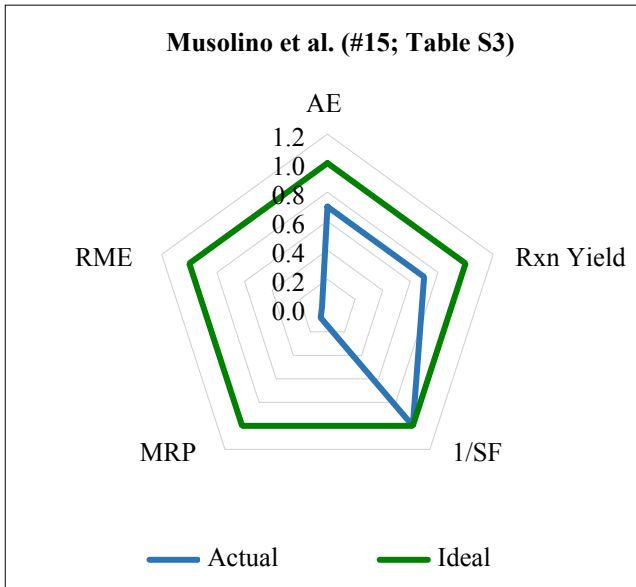
Figure S1. Comparison of yield %, E-total and Process Max Intensity (PMI) of procedures with PMI higher than 100; with the amount of D-Fructose employed below each set of bars.

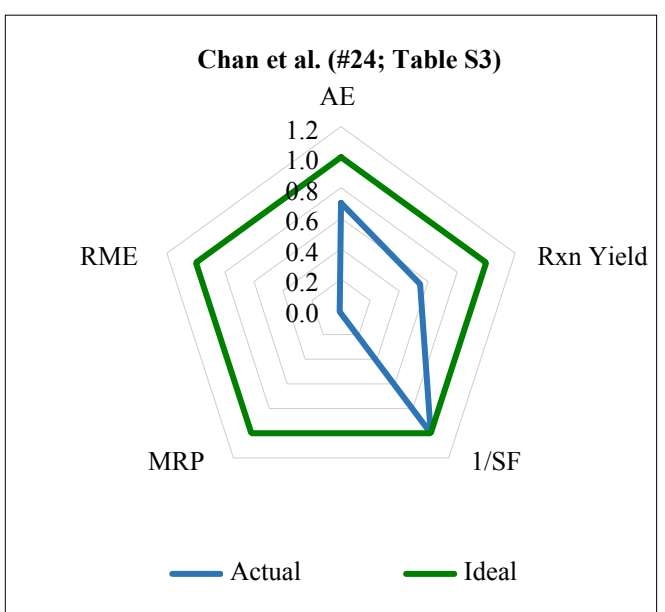
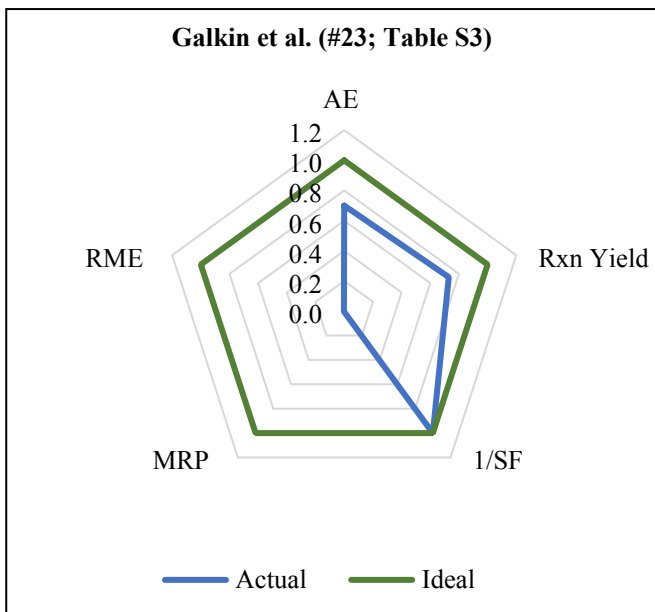
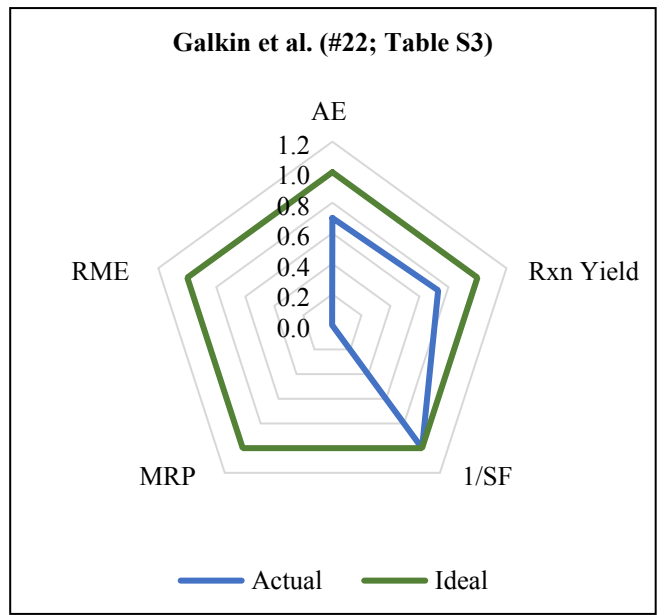
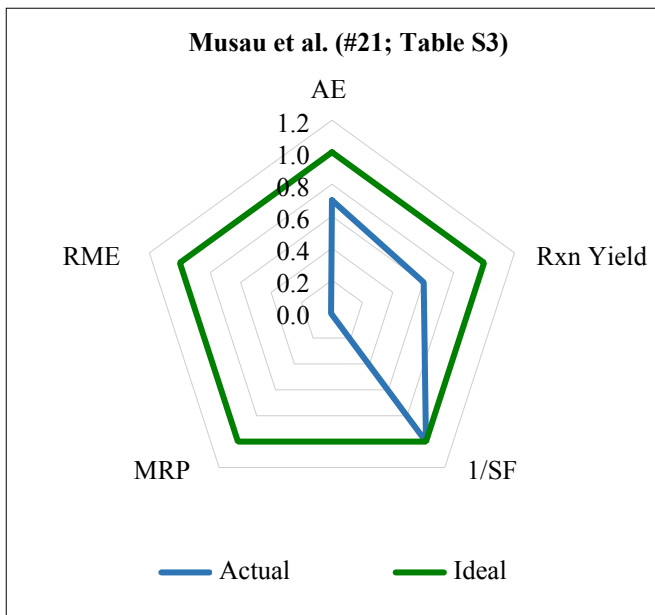
Radical pentagon analysis





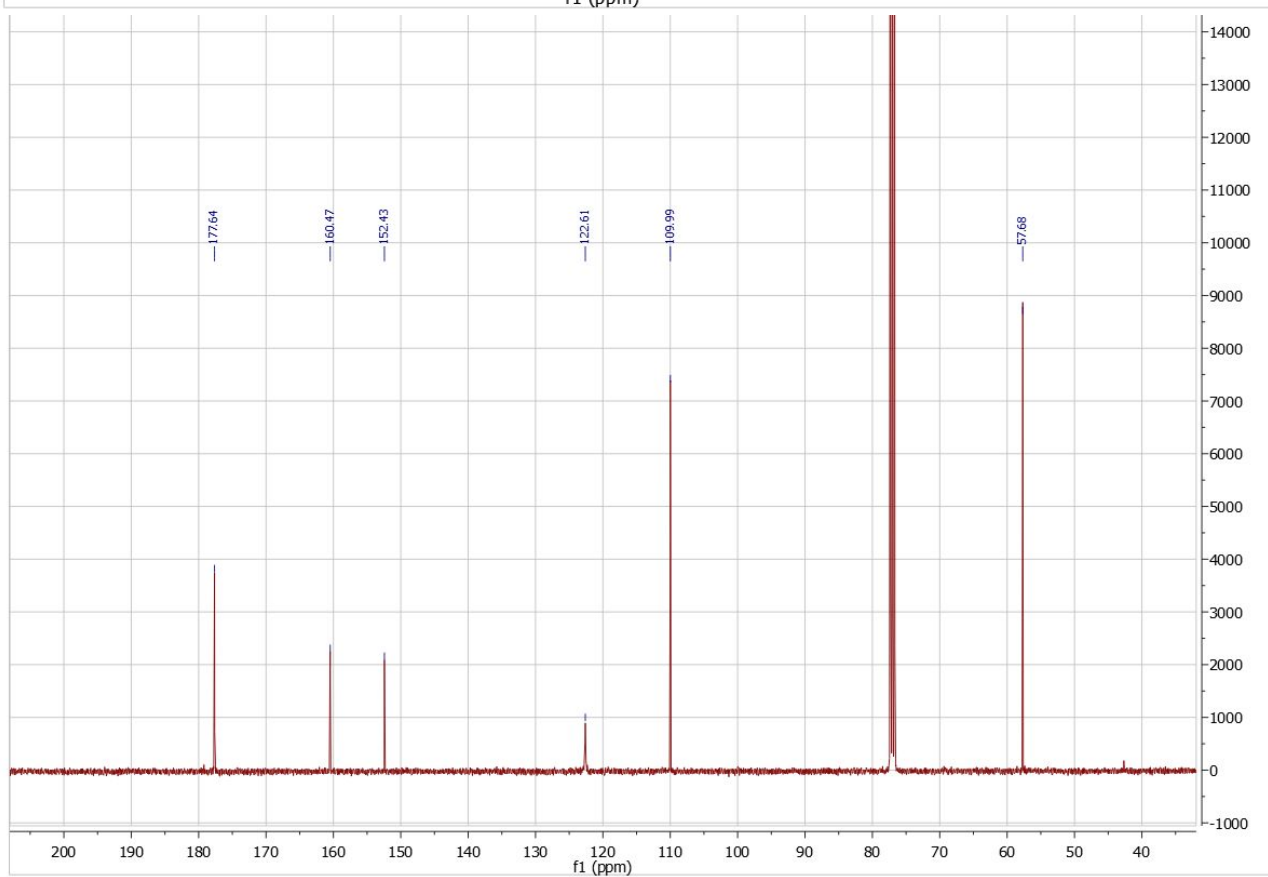
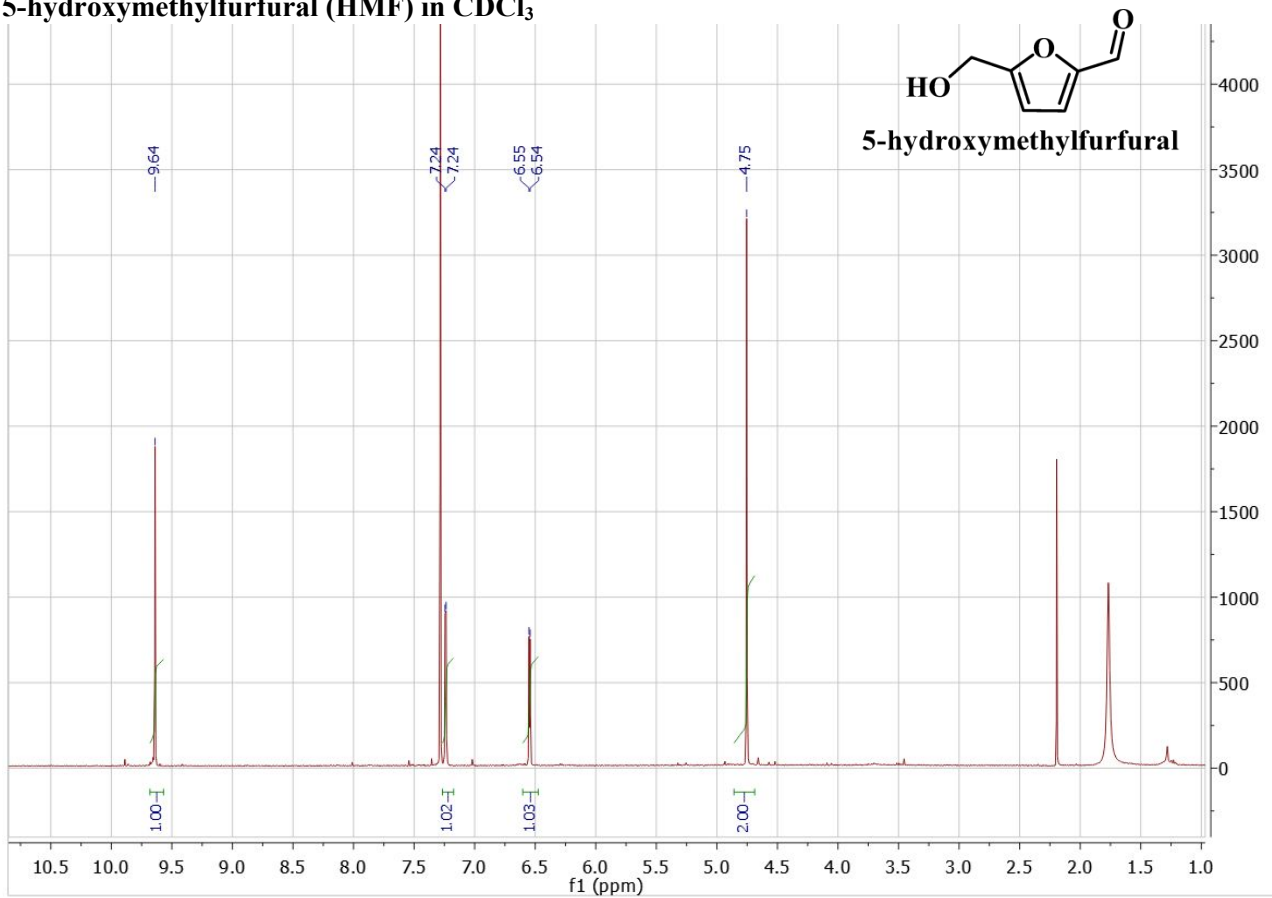




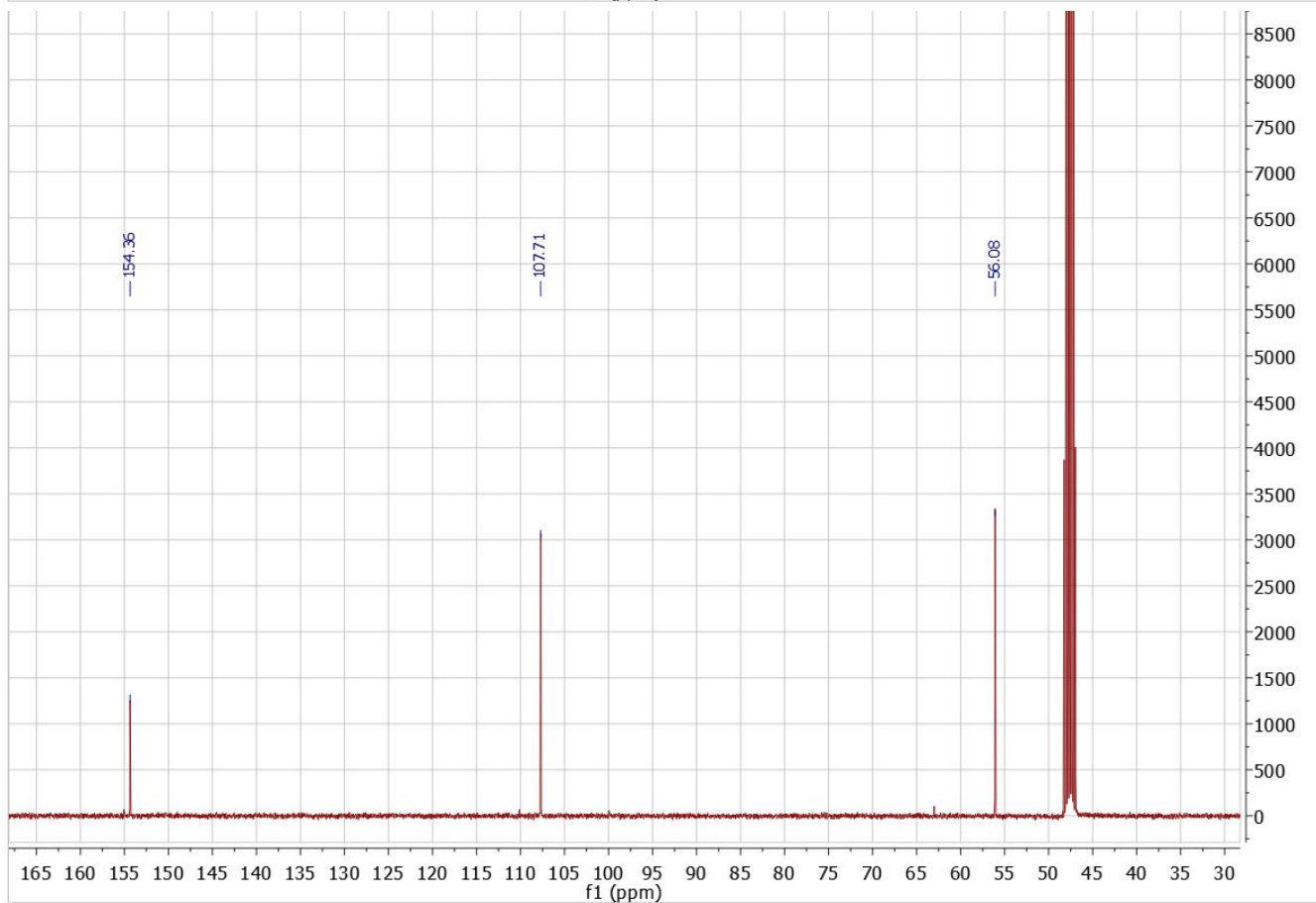
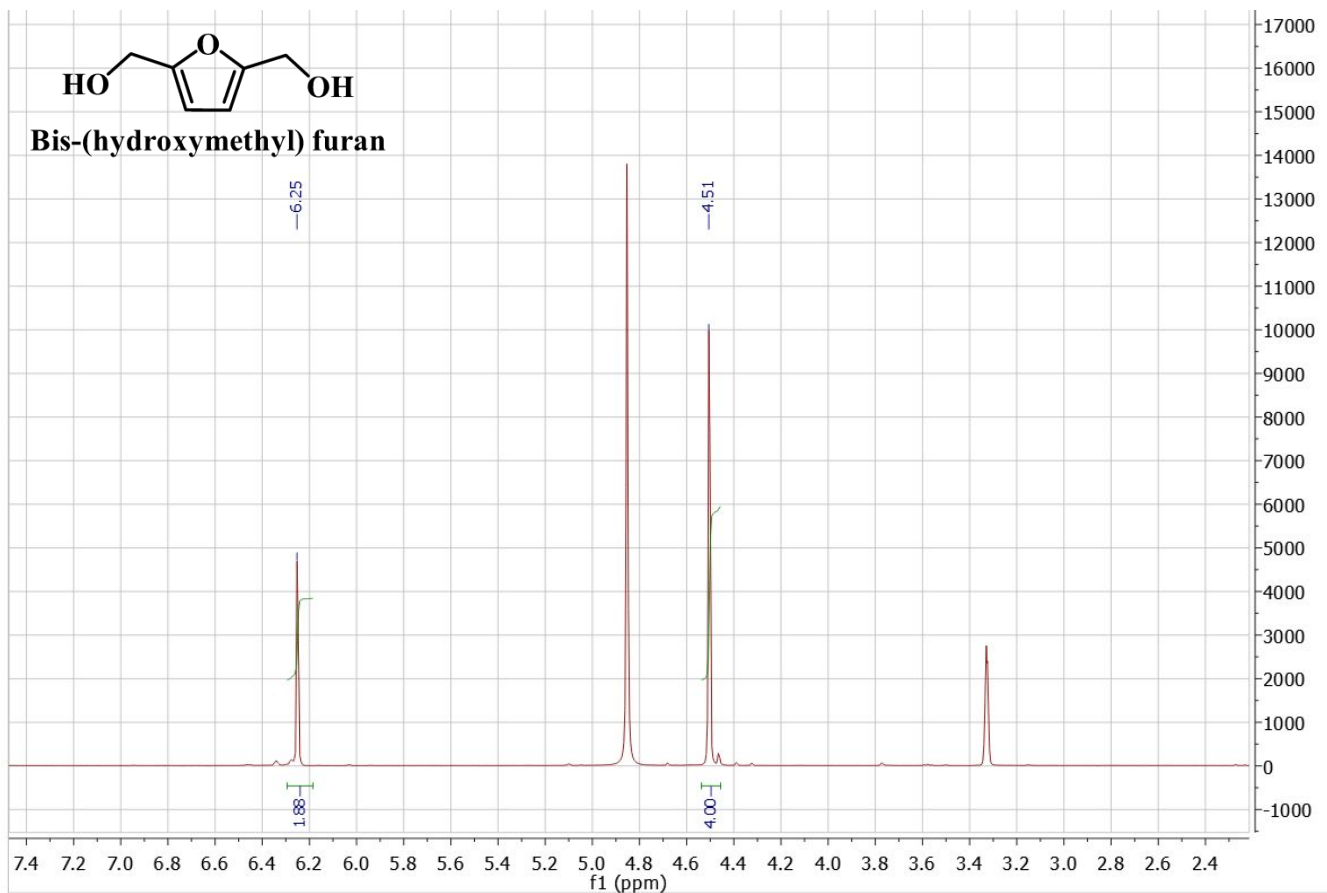


^1H -NMR and ^{13}C -NMR spectra

5-hydroxymethylfurfural (HMF) in CDCl_3



Bis-(hydroxymethyl)furan (BHMF) in MeOD



Dark-brown HMF-rich oil in CDCl₃

