

ADVANCED HEALTHCARE MATERIALS

Supporting Information

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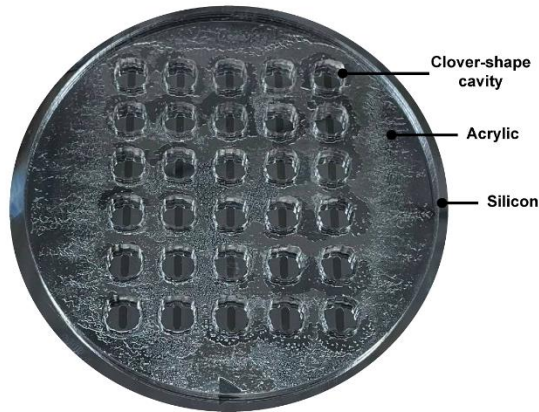
The Modular μ SiM Reconfigured: Integration of Microfluidic Capabilities to Study In Vitro Barrier Tissue Models under Flow

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Supporting Information

S1. Molds for the fabrication of flow module and seeding stencil

(A) Silicon mold with acrylic divider



(B) Aluminum mold with acrylic divider

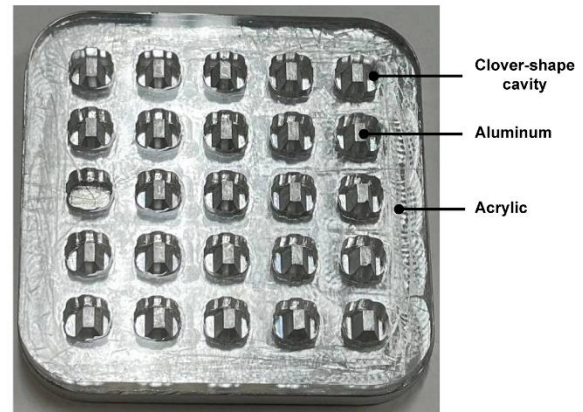


Figure S1. (A) Silicon mold with microchannel features bonded to an acrylic divider for fabricating clover-shape flow modules. (B) Machined aluminum mold with tapered features bonded to an acrylic divider for fabricating clover-shape seeding stencils. Both dividers comprise cavities that confine PDMS to get a clover-shape during curing on the hot plate.

S2. Flow circuit

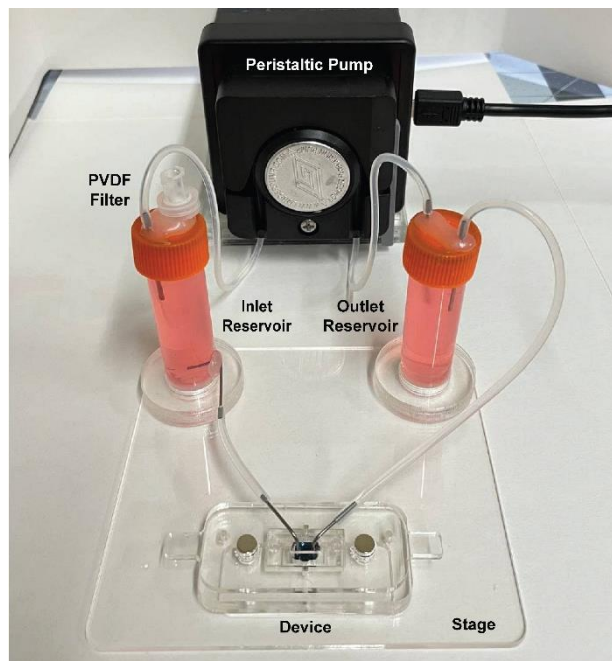
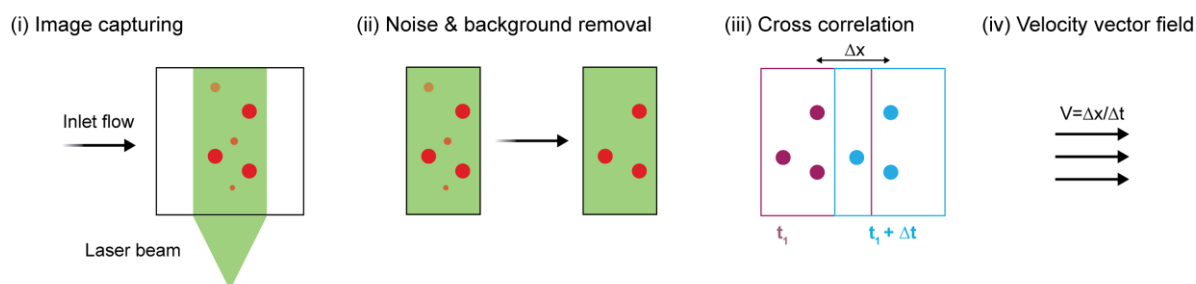


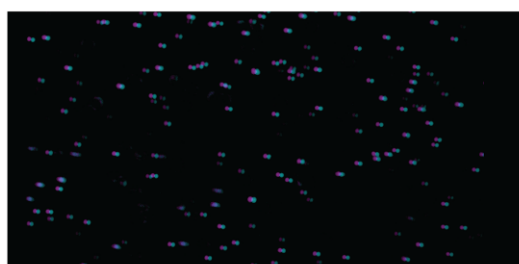
Figure S2. Custom-made flow circuit for experiments with continuous fluid flow. The setup includes a peristaltic pump for media circulation throughout the system, two reservoirs for supplying cell media and damping flow fluctuations, and an acrylic stage to hold the components in place. The PVDF filter is used to equilibrate cell media with environmental conditions in the incubator.

S3. Particle image velocimetry (PIV)

(A) Experimental measurement of velocity using PIV



(B) A pair of image captured with Δt interval



(C) Obtained vector field using cross correlation

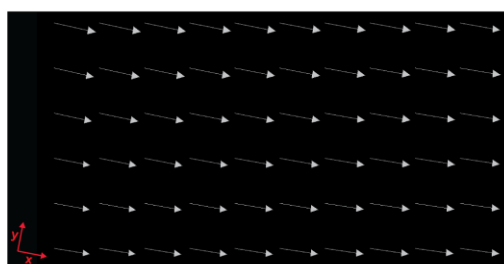
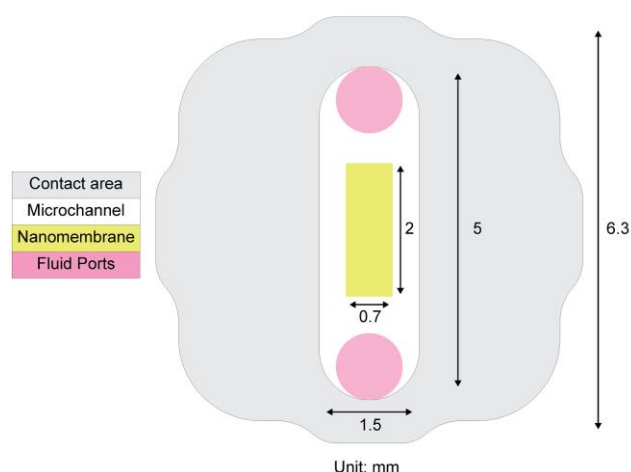


Figure S3. Schematic illustration of the experimental flow analysis using particle image velocimetry technique. (A) (i) Laser beam excites fluorescent beads in the region of interest and several pairs of images are captured. (ii) Noise and out-of-focus beads are removed from each image using image processing algorithms. (iii) Cross-correlation is applied to images of beads to find displacement between the two paired images. (iv) Velocity vectors are calculated on a structured grid for each pair of images and the mean velocity among all pairs is demonstrated as the velocity vector field. (B) A pair of image captured with a time interval of 100 μ s. (C) Generated vector field using average velocity obtained from 50 pair of images.

S4. Geometry and dimensions of the flow module

(A) Bottom view of the flow module



(B) 3D image of the flow module

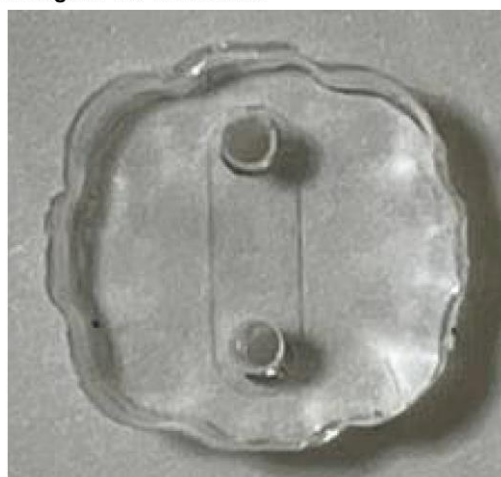
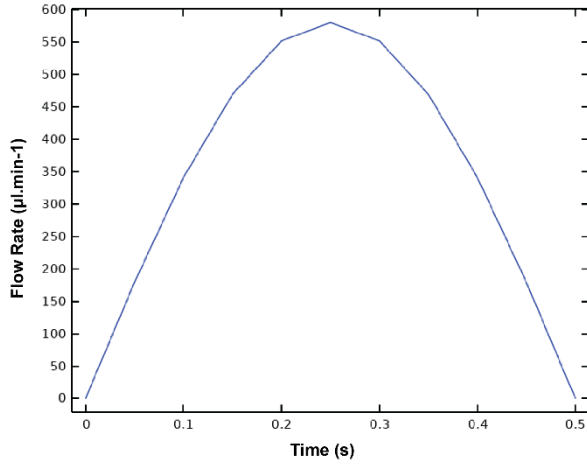


Figure S4. (A) Schematic illustration of the contacting interface between m- μ SiM membrane chip and the flow module. The fluid flow enters and exits the microchannel from fluid ports shown in pink. (B) 3D image of the PDMS flow module. Both m- μ SiM well and the flow module have a clover-shape to promote self-alignment. All dimensions are in mm.

S5. Introduction of a sinusoidal waveform as an inlet flow rate

(A) Sinusoidal flow rate as the inlet boundary condition



(B) Shear stress at the culture region (membrane surface)

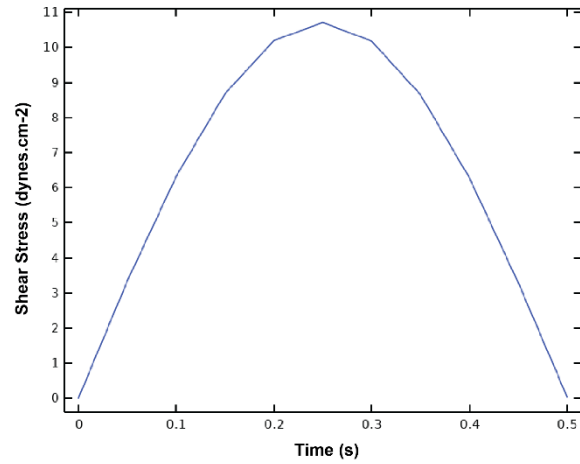


Figure S5. (A) Sinusoidal flow rate as an inlet boundary condition of the flow module. (B) Resulted shear stress at the culture region as a function of time.

S6. Neutrophil introduction and deposition onto the membrane

As a particle moves through the microchannel along with the flow, it spends a certain amount of time over the membrane (**Figure S6**). This parameter is called “residence time“ (t_f) and can be calculated by equation (S1) where L is the length of the membrane and V_f is the velocity of the fluid at the given height of the particle with respect to the membrane. There is another time scale called “settling time“ (t_s) that describes the time it takes for a particle to settle from a position h onto the membrane surface which can be calculated by equation (S2). H is the height of the particle with respect to the membrane and V_s is the settling velocity of the particle which can be calculated using Stokes’ law as described by equation (S3).

$$\text{Residence time: } t_f = \frac{L}{V_f} \quad (\text{S1})$$

$$\text{Settling time: } t_s = \frac{H}{V_s} \quad (\text{S2})$$

$$\text{Settling velocity: } V_s = \frac{gd^2(\rho_p - \rho_m)}{18\mu} \quad (\text{S3})$$

Parameters d , ρ_p , ρ_m , μ represent particle diameter, particle density, medium density, and medium viscosity, respectively.

In a situation where the settling time is less than the residence time ($t_s < t_f$), the particle can settle onto the membrane before it is swept past the membrane. To compare settling and residence times of particles at different heights, we obtained V_f from the COMSOL simulation and calculated V_s using Stokes’ Law for different flow rates. Assuming that neutrophils are distributed uniformly in the solution, our calculations showed that an inlet

flow rate of $10 \mu\text{L}\cdot\text{min}^{-1}$ results in the deposition of 20 % of neutrophil onto the membrane, which provides an adequate number of neutrophils on the membrane for transmigration study. This is an acceptable flow rate since it prevents neutrophil activation while providing adequate neutrophil deposition. Higher flow rates lead to neutrophil activation and lower flow rates result in the settlement of the majority of neutrophils in the tubing. If more neutrophils are desired on the membrane surface, we suggest increasing the neutrophil concentration in the initial solution or increasing the time the flow is maintained (introduction time).

Stokes' law for particle settlement

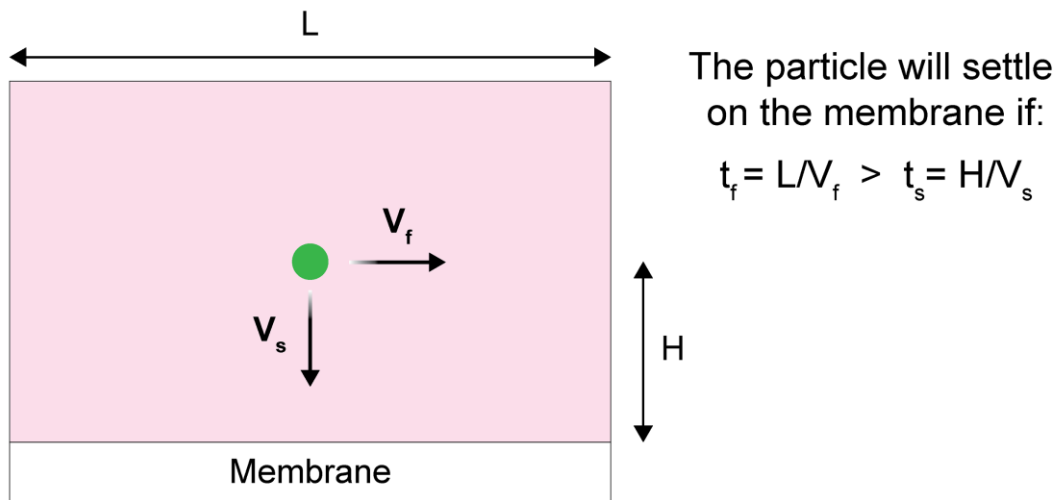


Figure S6. Schematic demonstration of Stokes' law for a spherical particle that follows the fluid velocity. When the fluid is incompressible and the flow is fully developed, Stokes' law provides a mathematical model for calculating the settling velocity of the particle and approximating the required time for the particle to settle on the surface, t_s . We compare this to the time required to move through the flow module, t_f , as an estimate of the likelihood of a particle settling onto the membrane.

S7. Quantification of neutrophil activation using flow cytometry

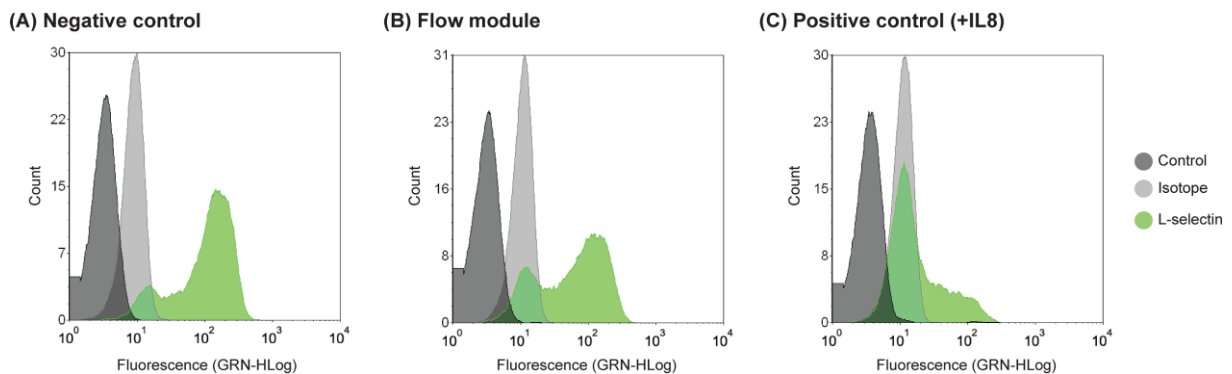


Figure S7. Flow cytometry analysis of neutrophils using L-selectin as an activation biomarker. (A) Post isolation stock as the negative control, (B) neutrophils flowed through the device showing a similar trend to the negative control, (C) IL8 treated neutrophils as the positive control showing loss of L-selectin due to activation.

S8. Mimicking tissue side in the bottom channel of m- μ SiM by incorporating collagen I

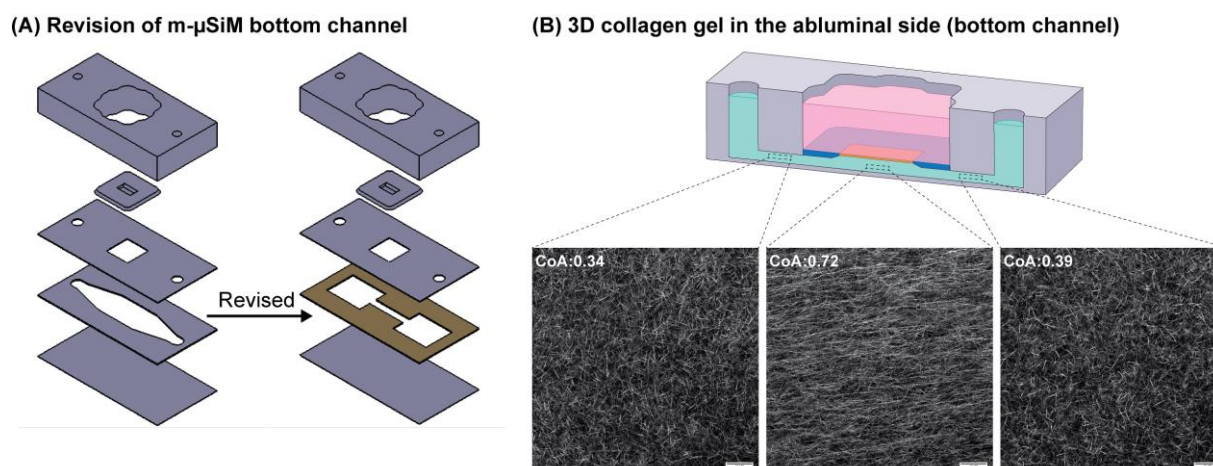
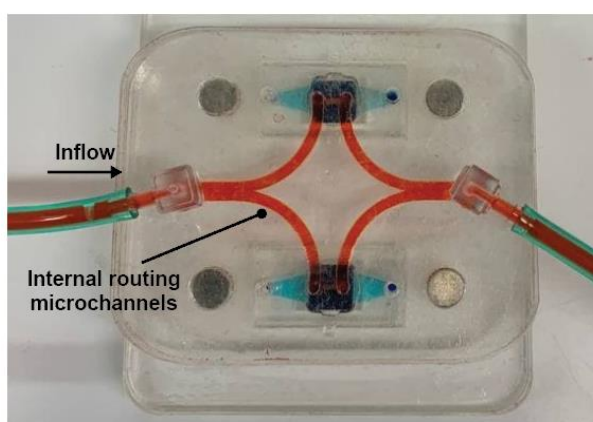


Figure S8. Customization of the m- μ SiM component to incorporate 3D gel with aligned collagen fibers below the membrane. (A) The bottom channel of the m- μ SiM is revised into a segmented channel to align collagen fibers based on extensional strain. (B) Demonstration of fibers at three different locations across the bottom channel. CoA represents the coefficient of fiber alignment (COA=0: complete randomness, COA=1: complete alignment).

S9. Multiplexing and scalability of the platform

(A) Functional lid design with integrated routing channels



(B) Schematic of the stencil carrier

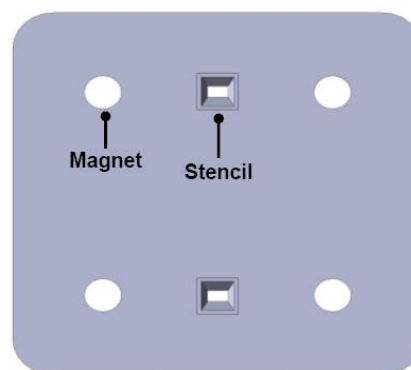


Figure S9. (A) Prototype of the functional lid with the capability of supplying two devices. The lid comprises two flow modules that are integrated into a common upper housing. In this design, the media is introduced to the system through a 90-degree elbow connector and is transferred to the devices through routing channels. Media in the routing channels and luminal side of the device is shown as red and media in the abluminal side is shown as blue. (B) Schematic of the stencil carrier containing two stencils which can be added to a corresponding array of open wells simultaneously.

S10. Characteristics of the fluid flow in the flow module

Table S1. Characteristics of fluid flow within the flow module at different flow rates

Inlet flow rate ($\mu\text{l}\cdot\text{min}^{-1}$)	Average V at midline of the flow path-PIV ($\text{mm}\cdot\text{s}^{-1}$)	Average V at midline of the flow path-COMSOL ($\text{mm}\cdot\text{s}^{-1}$)	Shear stress on the membrane surface ($\text{dynes}\cdot\text{cm}^{-2}$)	Maximum shear stress within the flow path ($\text{dynes}\cdot\text{cm}^{-2}$)
10	0.89 ± 0.07	0.83	0.18	0.40
100	8.73 ± 0.1	8.31	1.85	3.93
200	15.01 ± 1.09	16.62	3.69	7.96
500	40.39 ± 0.84	41.55	9.23	20.89
1000	86.57 ± 4.49	83.10	18.45	42.49