

# Non aqueous Li-mediated nitrogen reduction: Taking control of potentials – Supplementary Information

*Romain Tort,<sup>a,b</sup> Olivia Westhead,<sup>b</sup> Matthew Spry,<sup>b</sup> Bethan J. V. Davies,<sup>b</sup> Mary P. Ryan,<sup>b</sup>  
Maria-Magdalena Titirici,<sup>a</sup> and Ifan E. L. Stephens<sup>b</sup>*

<sup>a</sup> Department of Chemical Engineering, Imperial College London, SW7 2AZ London, UK

<sup>b</sup> Department of Materials, Imperial College London, SW7 2AZ London, UK

**Corresponding Author: Ifan E. L. Stephens – Department of Materials, Imperial  
College London, SW7 2AZ London, UK; Email: [i.stephens@imperial.ac.uk](mailto:i.stephens@imperial.ac.uk)**

## TABLE OF CONTENTS

<b>1</b>	<b>MATERIALS AND METHODS</b>	<b>3</b>
<b>1.2.</b>	<b>Reference electrode preparation</b>	<b>3</b>
1.2.1.	Coin cell assembly	3
1.2.2.	Lithiation/Delithiation procedures	4
<b>1.3.</b>	<b>Setup for electrochemical experiments</b>	<b>4</b>
<b>1.4.</b>	<b>Measuring the drift in potential of a studied reference electrode</b>	<b>4</b>
<b>1.5.</b>	<b>Chronoamperometric electrolysis procedure</b>	<b>5</b>
<b>1.6.</b>	<b>Ammonia quantification</b>	<b>5</b>
1.6.1.	Reagents preparation for ammonia quantification	5
1.6.2.	Ammonia quantification method	6
<b>2</b>	<b>FIGURES</b>	<b>8</b>

Figure S 1. (a) Coin cell assembly method for  $\text{LiFePO}_4$  or  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  conditioning, wetting the separator with  $70\mu\text{L}$   $\text{LiNTf}_2$  1M in THF, at  $20^\circ\text{C}$ . (b,c) Typical chronovoltammograms for galvanostatic (b)  $\text{LiFePO}_4$  partial delithiation and (c)  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  partial lithiation at  $10\text{mA}\cdot\text{g}^{-1}_{\text{active material}}$ , showing the obtention of a stable potential of  $+ 3.428 \pm 0.003$  V vs. Li and  $+ 1.564 \pm 0.001$  V vs. Li, respectively. Procedure described in 1.2. 9

Figure S 2. (a) Electrochemical cell assembly diagram: 4mL electrolyte capacity,  $1\text{cm}^2$  working and counter electrodes surface areas, 1.7cm distance between each electrode, gas-tight with gas flow at ambient pressure (b) Assembled cell picture, (c) Cell in operation in a glovebox, closed gas line equipped with a THF bubbler to saturate inlet gas with THF. 9

Figure S 3. Typical quantification experiment as described in 1.6.2 – data analysis: (a) samples preparation volumes, (b) resulting UV-vis spectra and (c) reported maxima vs. added  $\text{NH}_4\text{Cl}$ . 10

Figure S 4. (a,b) CVs of ferrocene 10mM in 1M  $\text{LiNTf}_2$  in THF/EtOH 99:1 v/v at different times of aging at open circuit, using (a) Pt and (b)  $\text{LiFePO}_4$  as reference electrodes (Corresponding  $U_{Fc}/F_c$  + reported in Table S 2). (c) Peak potentials difference ( $U_{a, max} - U_{c, max}$ ) vs. time at open circuit used to calculate  $U_{Fc}/F_c$  + (Figure 2b). (d) Working electrode potential recorded between ferrocene cycling steps, showing partial to full relaxation to OCP between each experiment. 10

Figure S 5. (a,b) Examples of impedance spectra of the (a) working and (b) counter electrodes for the cell assemblies made for electrolysis experiments plotted in figure 3. Recorded by potentiodynamic electrochemical impedance spectroscopy (PEIS) at open circuit voltage, with an oscillation amplitude of 20 mV at frequencies ranging from 200 kHz to 500 smHz. The ohmic drop correction was performed manually after the experiments by correcting potentials with the formula  $U_{eff} = U_{recorded} - Rele_i$  where  $U_{eff}$  is the corrected electrode potential,  $U_{recorded}$  is the raw potential measured during experiments and  $i$  is the current passed during experiments.  $Rele$  is the uncompensated resistance between the working (or counter) and reference electrode, collected from the PEIS measurements.  $Rele$  is obtained here through fitting of the experimental data to a suitable equivalent circuit. (c) Equivalent circuit used to fit the impedance spectra and extract  $Rele$  as well as other impedance contributions such as:  $R_{ct}$  the charge transfer resistance,  $C_{dl}$  the double-layer capacitance, and  $ZW$  the warbug impedance describing diffusion processes. 11

Table S 1. Comparison of Faradaic efficiency to  $\text{NH}_3$  after a 10 C electrolysis at  $2\text{mA}\cdot\text{cm}^{-2}$  of a  $\text{LiNTf}_2$  1M electrolyte in THF/EtOH 99:1 v/v using Pt,  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  or  $\text{LiFePO}_4$  as a reference electrode – Showing the interference of  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  in  $\text{N}_2$  reduction experiments. 12

Table S 2. Ferrocene/Ferrocenium potential drift records for Pt, and  $\text{LiFePO}_4$  across time at OCV using different salts in THF/EtOH 99:1 v/v electrolytes. 13

Table S 3. Relation between current density, working/counter electrodes potentials and faradaic efficiency to ammonia after 10C electrolysis of a  $\text{LiNTf}_2$  1M electrolyte in THF/EtOH 99:1 v/v at a corresponding current applied. 14

Table S 4. Summary of Table S 3 (mean & errors): relation between current density, electrodes potentials, Faradaic efficiency, and partial current density to  $\text{NH}_3$ . 15

## 1 Materials and Methods

### 1.1. Materials

Mo foil (99.9 %, 125  $\mu\text{m}$  thick), Cu foils (99.9 %, 0.5 mm thick), Pt foil (99.95 %, 25  $\mu\text{m}$  thick) and Pt mesh (99.9 %, 60  $\mu\text{m}$  thick) were purchased from Goodfellow Cambridge.  $\text{LiFePO}_4$  and  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  18 mm diameter discs were cut out of pre-coated commercial sheets:  $\text{LiFePO}_4$  coated on Al sheets (BR0188,  $135\text{mA}\cdot\text{h}\cdot\text{g}^{-1}$  capacity,  $28\text{mg}\cdot\text{cm}^{-2}$  loading) purchased from MSE supplies, and  $\text{Li}_4\text{Ti}_5\text{O}_{12}$  coated on Cu sheets (Nanomyte® BE-10E, 90% active material, 5% PVDF, 5% Super P  $170\text{mA}\cdot\text{h}\cdot\text{g}^{-1}$  capacity,  $7.3\text{mg}\cdot\text{cm}^{-2}$  loading), purchased from NEI Corp. Lithium bis(trifluoromethanesulfonyl)imide ( $\text{LiNTf}_2$ , 99.9 %, < 20 ppm  $\text{H}_2\text{O}$ ) was purchased from Solvionic. Ethanol (99.5 %, Extra Dry, absolute, AcroSeal™) was bought from Thermofischer™. THF (anhydrous,  $\geq 99.9\%$ , inhibitor-free), Ferrocene (98 %), HCl (30 %, Suprapur®) and coin cell separators (Whatman® glass microfiber filters, Grade GF/A) were purchased from Merck KGaA Darmstadt (Sigma Aldrich). Sodium salicylate, sodium hydroxide and sodium nitroprusside were purchased from VWR. Separators were dried overnight under dynamic vacuum before use. 15 mm diameter Lithium discs, coin cell cases, spacers and wave-springs were purchased from Pi-Kem.

## 1.2. Reference electrode preparation

### 1.2.1. *Coin cell assembly*

Within an Ar-filled glovebox, a Li disc was mounted on stainless steel spacer and spring, placed in the negative case of a coin cell. A 18 mm diameter disc was cut out of the active materials sheets (LiFePO<sub>4</sub> or Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub>), then placed in the opposite positive case and covered with a separator, which was wetted with 70-100  $\mu$ L electrolyte (1 M LiNTf<sub>2</sub> in THF). (Figure S 1a) Cell was closed with a 7-bar press.

### 1.2.2. *Lithiation/Delithiation procedures*

Partial lithiation (for Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub>) or delithiation (for LiFePO<sub>4</sub>) methods were reproduced and adapted from La Mantia *et al.*<sup>20</sup> and Costard *et al.*<sup>21</sup> LiFePO<sub>4</sub>/Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> materials assembled cells were discharged (1.56 mA.g<sup>-1</sup><sub>LiFePO<sub>4</sub></sub>, 0.01C rate) / charged (10 mA.g<sup>-1</sup><sub>Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub></sub>, 0.06C rate) respectively, until a cut-off voltage of 4.0 or 1.3 V vs. Li, respectively. The cell was then left to relax to a potential plateau (+3.428  $\pm$  0.003 V vs. Li for LiFePO<sub>4</sub>, +1.564  $\pm$  0.002 V vs. Li for Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub>), stable for days in the coin cell. (Figure S 1).

## 1.3. Setup for electrochemical experiments

The 3-electrode sandwich cell used in this work consists of: (i) a 1 cm<sup>2</sup> Mo foil working electrode, polished, dipped in 4 M HCl and sonicated in ethanol for 10 min, (ii) a Pt mesh counter electrode on a 1 cm<sup>2</sup> Pt foil, (iii) a reference electrode – either a Pt wire or the previously prepared LiFePO<sub>4</sub> or Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> disc, shaped into a ring by punching a 8 mm diameter hole at its centre –. Within an Ar-filled glovebox, the cell was assembled, with the reference midway through the two other electrodes (1.8 cm between each). Gas-tight compartments were filled with 4 mL electrolyte, and leak tested by passing Argon through. The cell was then saturated with THF-pre-saturated N<sub>2</sub>, bubbling for 30 min at a rate of 4

mL.min<sup>-1</sup> before any experiment, then turned down to 1 mL.min<sup>-1</sup>. All the electrochemistry was performed in the Argon glovebox. After experiments, cell was cleaned with EtOH out of the glovebox and boiled in ultrapure water (>18.2 M $\Omega$ , Sartorius), then dried in an oven at 70°C.

#### 1.4. Measuring the drift in potential of a studied reference electrode

To assess the extent of an undesired drift in reference electrode potential, we use the ferrocene-ferrocenium redox couple, an internal reference redox system with a defined 1 electron redox equilibrium (Figure 2a), approved as a reference for non-aqueous systems.<sup>36</sup> In every test condition, a voltammogram of a 1 M LiNTf<sub>2</sub> and 10 mM ferrocene in THF electrolyte was recorded, at a 50 mV.s<sup>-1</sup> rate.  $U_{Fc/Fc^+}$ , the average *between* the potentials at which peak cathodic and anodic currents are reached (Figure 2a), is an estimate of its half-peak potential.<sup>36</sup> An important sidenote: during electrolysis, an unavoidable passivation layer forms at the working electrode (Figure 1). To avoid resistive contribution of this layer to  $U_{Fc/Fc^+}$ , post-electrolysis measurements (Figure 2d) were done after replacing the working electrode with a fresh one.

#### 1.5. Chronoamperometric electrolysis procedure

After cell assembly, the cell was purged with N<sub>2</sub> for 30 min at a rate of 4 mL.min<sup>-1</sup> before any experiment, then turned down to 1 mL.min<sup>-1</sup>. After assessing electrolyte resistance by impedance spectroscopy (PEIS at open circuit, 20 mV oscillation, 100 kHz to 1 Hz frequency range), voltage was swept from open circuit voltage to - 4.0 V vs. LiFePO<sub>4</sub>, with a cut-off current density corresponding to the final applied current during electrolysis. Once this current was reached, it was held at this level, passing a total of 10 C charge. Electrolyte resistance change was assessed post electrolysis using the same method as before, then the cell was purged

with Argon for 30 min at 4 mL.min<sup>-1</sup> flow rate before disassembly. Ohmic drop was corrected manually post experiment during data processing, using PEIS data (Figure S 5).

## 1.6. Ammonia quantification

### 1.6.1. *Reagents preparation for ammonia quantification*

A sodium hypochlorite alkaline solution was prepared by mixing sodium hypochlorite 14 % w/w and sodium hydroxide 0.4 M in a 1:9 v/v ratio. This solution must be done shortly before every quantification experiment as the stock solution stability is limited in time.

A “salicylate – catalyst” solution was prepared by dissolving 40 g sodium salicylate powder in 50mL ultrapure water, to which 1 mL of a 50 mM aqueous sodium nitroprusside ( $\text{Na}_2[\text{Fe}(\text{CN})_5\text{NO}] \cdot 2\text{H}_2\text{O}$ ) solution was added. Volume was completed to 100 mL in a volumetric flask, to yield a solution containing 2.5 M sodium salicylate and 0.5 mM sodium nitroprusside catalyst. The solution was stored at 5°C in the dark for several months.

Sometimes, the sodium salicylate powder was contaminated with ammonia salts impurities. To purify it from these interferents, 40 g sodium salicylate was dissolved in 300 mL DI water, to which 50 mL of 6 M aqueous HCl was added dropwise under constant stirring. The salicylic acid precipitate was filtered and washed with three times 200 mL ultrapure water, then dried under vacuum at 40°C. For 20 g of obtained salicylic acid, the solid was dissolved in 35 mL sodium hydroxide 4 M, to which were added 580 mL of sodium nitroprusside 50 mM solution, then completed with ultrapure water to 58 mL.

### 1.6.2. *Ammonia quantification method*

Electrolyte post electrolysis was collected, with its total volume measured. 3 x 400 µL were collected alongside 400 µL of previously saved pristine electrolyte blank in separate vials. 20 µL 4 M aqueous HCl was added to each one of the four vials to trap NH<sub>3</sub> as NH<sub>4</sub>Cl, which

were then placed in a 70°C water bath for 1 h to evaporate solvents. Concentrates were then redissolved in 2 mL ultrapure water.

Resulting samples were dispatched in 1 mL portions in UV-vis cuvettes, to quantify ammonia via the salicylate method: a colorimetric detection method based on the complexation of ammonia with sodium salicylate to create a blue dye. For this method, a 1 mL sample was diluted to a volume of 2 mL with ultrapure water. Then, 280 µL of the “salicylate – catalyst” solution was added, followed with 280 µL of the sodium hypochlorite alkaline solution. Samples were left to age in the dark for 45 min, then characterised by UV-vis absorption spectroscopy, measuring absorbance of light between 500 nm and 900 nm wavelengths, and measuring the difference in absorbance between the maximum (655 nm) and baseline (900 nm).

In this work, we couple this quantification experiment to the quantification method of standard addition,<sup>33</sup> spiking sequential amounts of a NH<sub>4</sub>Cl standard solution (500 ppm, 9.35 mM) to the as prepared 1 mL samples and performing the salicylate quantification method to each one of these samples. By doing a linear regression on the obtained measurements, one can trace back to the ammonia present in the electrolyte, corresponding to negative of the intercept between the linear plot and the x axis (or the ratio between the slope  $m$  of the linear regression and its intercept  $b$ ) (see equations (1 – 3) and Figure S 3).  $[NH_3]$  is the ammonia concentration in the electrolyte,  $V_{ele}$  is the electrolyte volume,  $F$  is the Faraday constant,  $C$  is the total charge passed during the experiment,  $FE$  is the Faradaic Efficiency to ammonia,  $A$  is the working electrode geometric surface area.

$$(1) [NH_3] = \frac{b}{m} \quad (2) FE = \frac{3[NH_3]V_{ele}F}{C} \quad (3) Yield Rate = \frac{[NH_3]V_{ele}}{A \cdot Exp\ time}$$

Variations ( $\sigma_k^2$ ) and standard errors ( $s_k$ ) in measurements are estimated using the below statistical equations.  $A_i$  is the absorbance of sample with concentration  $c_i$ ,  $\bar{A}$  and  $\bar{c}$  are the mean absorbance and concentration, respectively.  $m$  and  $b$  are the slope and intercept of the fitted linear regression.  $N$  is the overall number of measurements.

$$\sigma_A^2 = \sum_i (A_i - \bar{A})^2 - m^2 \sum_i (c_i - \bar{c})^2 \quad \sigma_m^2 = \frac{\sigma_A^2}{\sum_i (c_i - \bar{c})^2} \quad \sigma_b^2 = \sigma_A^2 \frac{\sum c_i^2}{\sum_i (c_i - \bar{c})^2}$$

$$s_k = \sqrt{\frac{\sigma_k^2}{N-1}} \quad (k = A, m, b) \quad s_{c,NH_3} = \sqrt{\frac{\sigma_{c,NH_3}^2}{N-1}} = C_{NH_3} \sqrt{\left(\frac{s_b}{b}\right)^2 + \left(\frac{s_m}{m}\right)^2}$$



## 2 Figures

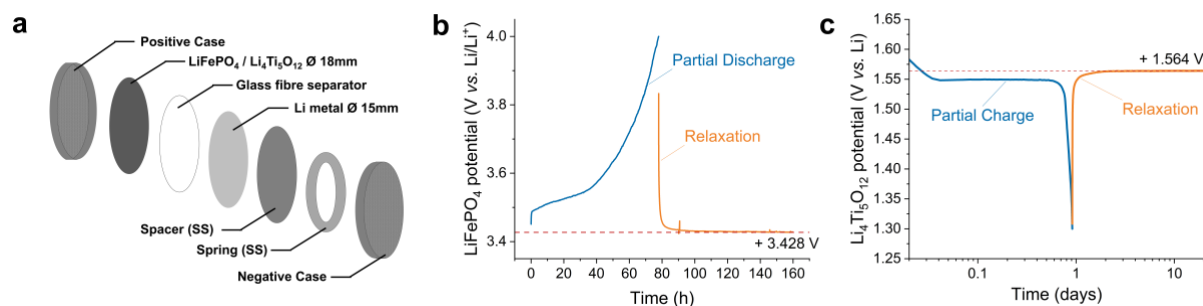


Figure S 1. (a) Coin cell assembly method for LiFePO<sub>4</sub> or Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> conditioning, wetting the separator with 70  $\mu$ L LiNTf<sub>2</sub> 1M in THF, at 20°C. (b,c) Typical chronovoltammograms for galvanostatic (b) LiFePO<sub>4</sub> partial delithiation and (c) Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> partial lithiation at 10mA.g<sup>-1</sup> active material, showing the obtention of a stable potential of + 3.428  $\pm$  0.003 V vs. Li and + 1.564  $\pm$  0.001 V vs. Li, respectively. Procedure described in 1.2.

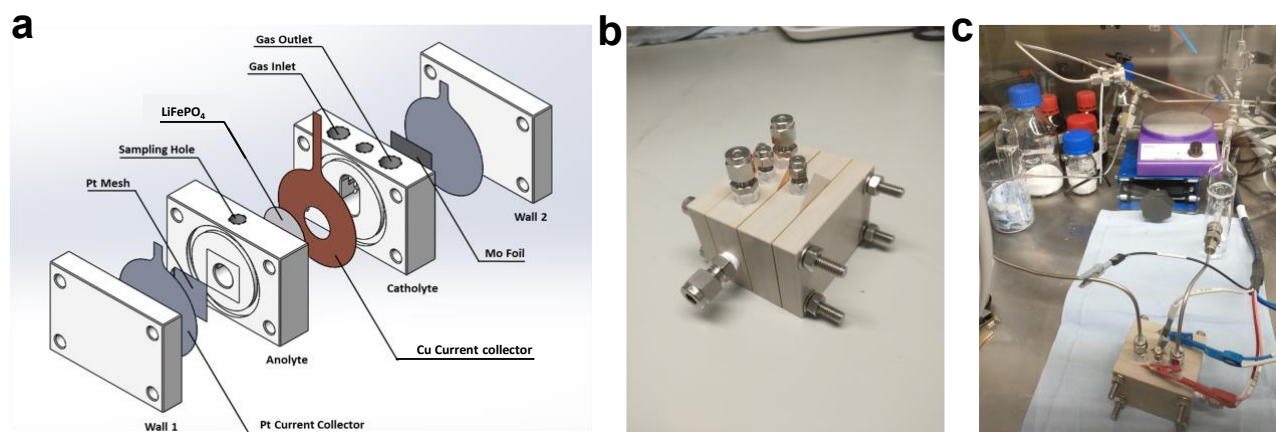


Figure S 2. (a) Electrochemical cell assembly diagram: 4mL electrolyte capacity, 1cm<sup>2</sup> working and counter electrodes surface areas, 1.7cm distance between each electrode, gas-tight with gas flow at ambient pressure (b) Assembled cell picture, (c) Cell in operation in a glovebox, closed gas line equipped with a THF bubbler to saturate inlet gas with THF.

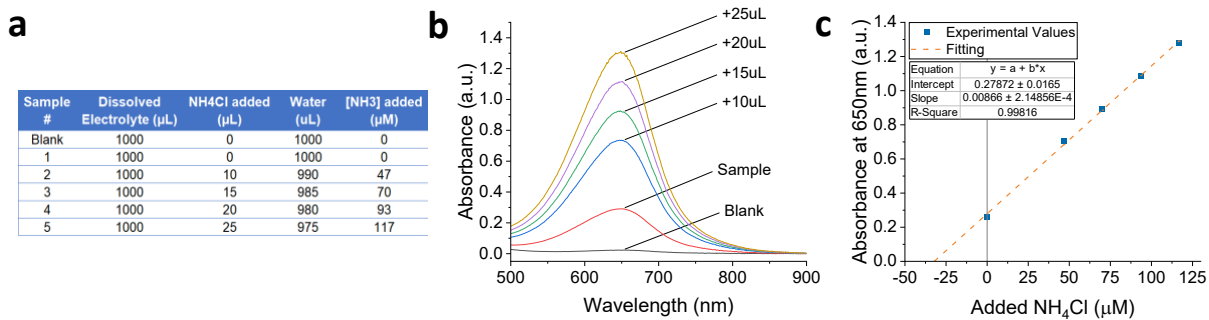


Figure S 3. Typical quantification experiment as described in 1.6.2 – data analysis: (a) samples preparation volumes, (b) resulting UV-vis spectra and (c) reported maxima vs. added NH<sub>4</sub>Cl.

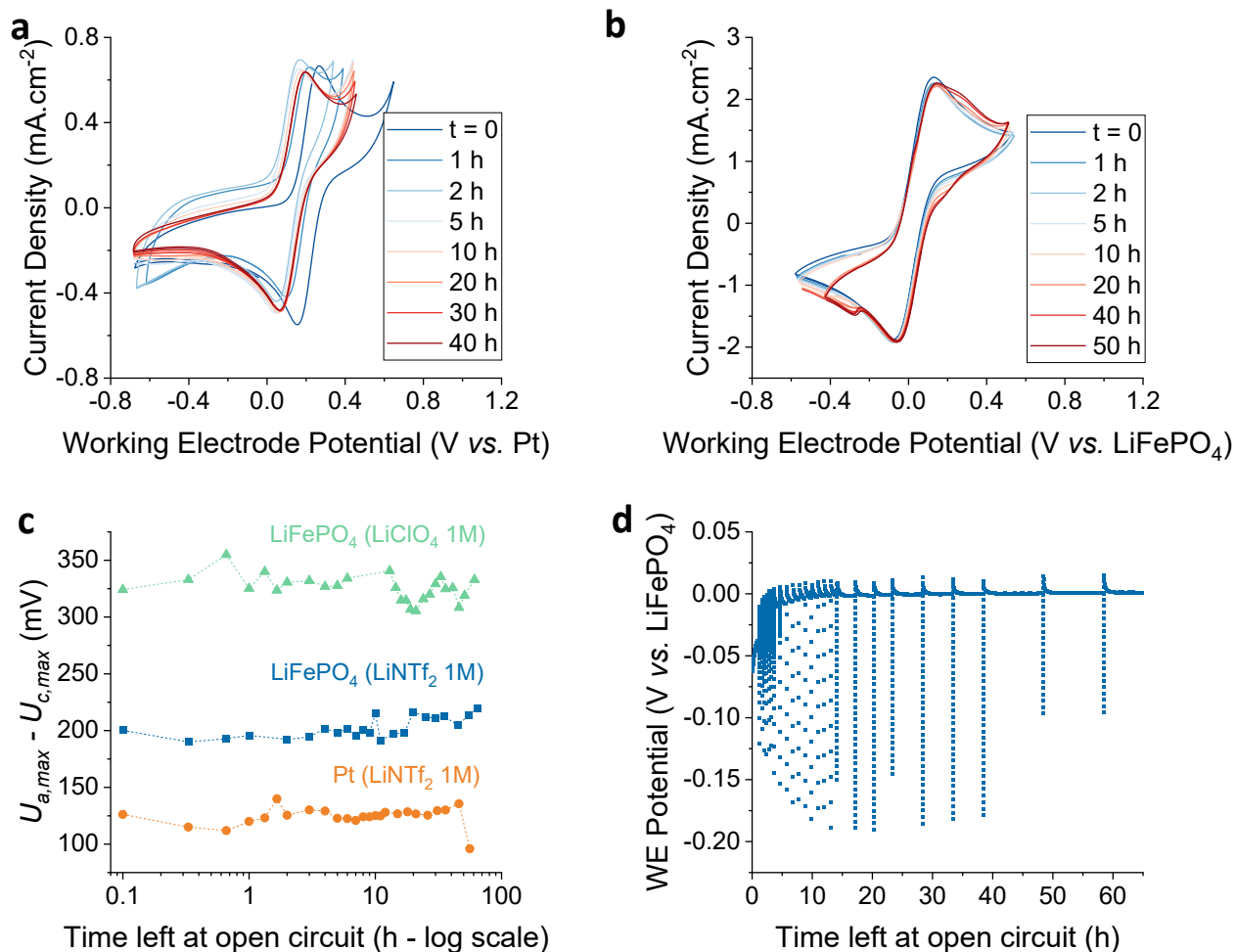


Figure S 4. (a,b) CVs of ferrocene 10mM in 1M LiNTf<sub>2</sub> in THF/EtOH 99:1 v/v at different times of aging at open circuit, using (a) Pt and (b) LiFePO<sub>4</sub> as reference electrodes (Corresponding  $U_{Fc/Fc^+}$  reported in

Table S 2). (c) Peak potentials difference ( $U_{a,max} - U_{c,max}$ ) vs. time at open circuit used to calculate  $U_{Fc/Fc^+}$  (Figure 2b). (d) Working electrode potential recorded between ferrocene cycling steps, showing partial to full relaxation to OCP between each experiment.

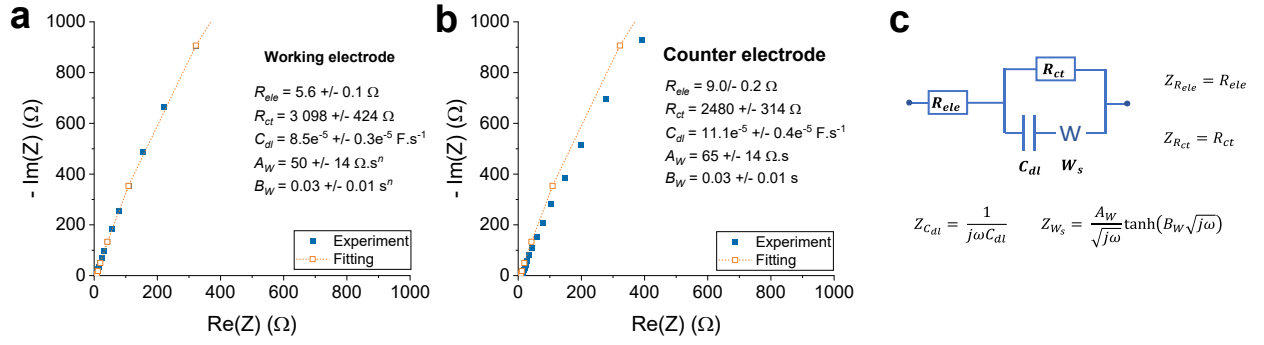


Figure S 5. (a,b) Examples of impedance spectra of the (a) working and (b) counter electrodes for the cell assemblies made for electrolysis experiments plotted in figure 3. Recorded by potentiodynamic electrochemical impedance spectroscopy (PEIS) at open circuit voltage, with an oscillation amplitude of 20 mV at frequencies ranging from 200 kHz to 500 smHz. The ohmic drop correction was performed manually after the experiments by correcting potentials with the formula  $U_{eff} = U_{recorded} - R_{ele}i$  where  $U_{eff}$  is the corrected electrode potential,  $U_{recorded}$  is the raw potential measured during experiments and  $i$  is the current passed during experiments.  $R_{ele}$  is the uncompensated resistance between the working (or counter) and reference electrode, collected from the PEIS measurements.  $R_{ele}$  is obtained here through fitting of the experimental data to a suitable equivalent circuit. (c) Equivalent circuit used to fit the impedance spectra and extract  $R_{ele}$  as well as other impedance contributions such as:  $R_{ct}$  the charge transfer resistance,  $C_{dl}$  the double-layer capacitance, and  $Z_W$  the warbug impedance describing diffusion processes.

### 3 Tables

Table S 1. Comparison of Faradaic efficiency to ammonia resulting from the electrolysis of a LiNTf<sub>2</sub> 1M electrolyte in THF/EtOH 99:1 v/v at 2mA.cm<sup>-2</sup> passing 10 C of charge, using Pt, Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> or LiFePO<sub>4</sub> as a reference electrode – Showing the interference of Li<sub>4</sub>Ti<sub>5</sub>O<sub>12</sub> in N<sub>2</sub> reduction experiments.

Reference used	FE to NH <sub>3</sub> (%) (run 1)	FE to NH <sub>3</sub> (%) (run 2)	FE to NH <sub>3</sub> (%) (run 3)	FE to NH <sub>3</sub> (%) (mean)
Pt wire	7.6 ± 0.5	6.9 ± 0.2	7.8 ± 0.9	7.4 ± 0.2
Li <sub>4</sub> Ti <sub>5</sub> O <sub>12</sub>	4.1 ± 0.3	4.0 ± 0.4	3.6 ± 0.5	3.9 ± 0.1
LiFePO <sub>4</sub>	7.8 ± 0.2	6.7 ± 1.0	7.0 ± 0.9	7.2 ± 0.3

Table S 2. Ferrocene  $U_{Fc/Fc^+}$  drift records for Pt, and LiFePO<sub>4</sub> across time at OCV using different salts in THF/EtOH 99:1 v/v electrolytes (plotted in Figure 2b)

<b>Reference Electrode</b>	<b>Pt wire</b>	<b>LiFePO<sub>4</sub></b>	<b>LiFePO<sub>4</sub></b>
<b>Salt – concentration</b>	<b>LiNTf<sub>2</sub> – 1M</b>	<b>LiNTf<sub>2</sub> – 1M</b>	<b>LiClO<sub>4</sub> – 1M</b>
<b>Time (h)</b>			
0	0	0	0
0.33	-48.9	-2.5	-2.3
0.66	-61.9	-1.7	-0.7
1	-70.9	1.5	-0.7
2	-91.6	0.2	-7.8
3	-98.9	3.5	-3.3
4	-99.5	4.2	-8.6
5	-93.3	7.3	-4.6
6	-90.2	8.7	-4.3
7	-88.4	9.1	-
8	-86.9	6.2	-
9	-83.9	7.3	-
10	-83.5	-3.6	-
11	-80.3	7.2	-
14	-77.3	9.3	0.1
17	-75.1	10.5	3.7
20	-71.2	1.4	-0.1
25	-69.7	2.2	4.2
30	-71.3	1.8	-1.2
35	-74.6	5.5	-1.4
45	-73.0	6.1	2.9
50	--	10.0	-2.6
60	-83.9	8.2	-0.3

Table S 3. Relation between current density, electrodes potentials and faradaic efficiency to NH<sub>3</sub> after electrolysis at constant current, passing 10 C of charge in a LiNTf<sub>2</sub> 1M electrolyte in THF/EtOH 99:1 v/v.

Current (mA.cm <sup>-2</sup> )	$U_{working\ electrode}$ (V vs. LiFePO <sub>4</sub> )			$U_{counter\ electrode}$ (V vs. LiFePO <sub>4</sub> )			FE to NH <sub>3</sub> (%)		
	run 1	run 2	run 3	run 1	run 2	run 3	run 1	run 2	run 3
0.1	- 3.438	- 3.421	- 3.402	+ 0.676	+ 0.669	+ 0.712	4.1 ± 0.4	6.6 ± 1.0	6.0 ± 0.8
0.2	- 3.342	- 3.430	- 3.380	+ 0.936	+ 0.751	+ 0.774	1.5 ± 2.0	4.5 ± 0.2	3.5 ± 0.2
0.5	- 3.442	- 3.380	- 3.372	+ 0.921	+ 0.913	+ 0.988	8.2 ± 0.5	6.9 ± 0.8	5.9 ± 1.5
1	- 3.410	- 3.402	- 3.403	+ 1.023	+ 1.152	+ 1.005	7.5 ± 3.3	7.1 ± 0.6	6.8 ± 0.3
2	- 3.437	- 3.434	- 3.432	+ 1.057	+ 1.062	+ 1.056	7.8 ± 0.2	6.7 ± 1.0	7.0 ± 0.9
5	- 3.427	- 3.462	- 3.459	+ 1.219	+ 1.142	+ 2.748	9.3 ± 0.6	7.6 ± 1.3	6.9 ± 0.3
10	- 3.407	- 3.434	- 3.402	+ 2.069	+ 5.131	+ 1.501	8.7 ± 0.8	7.7 ± 0.5	7.2 ± 1.1

Table S 4. Summary of Table S 3 (mean & errors): relation between current density, electrodes potentials, Faradaic efficiency, and partial current density to NH<sub>3</sub> (plotted in Figure 3).

Current (mA.cm <sup>-2</sup> )	$U_{working\ electrode}$ (V vs. LiFePO <sub>4</sub> )	$U_{counter\ electrode}$ (V vs. LiFePO <sub>4</sub> )	FE to NH <sub>3</sub> (%)	Partial current to NH <sub>3</sub> (μA.cm <sup>-2</sup> )
0.1	- 3.420 ± 0.010	+ 0.686 ± 0.013	5.6 ± 0.7	5.6 ± 0.8
0.2	- 3.384 ± 0.025	+ 0.821 ± 0.059	4.4 ± 0.5	8.8 ± 0.9
0.5	- 3.398 ± 0.022	+ 0.941 ± 0.024	7.0 ± 0.7	35.0 ± 3.3
1	- 3.405 ± 0.002	+ 1.060 ± 0.046	6.7 ± 0.5	67.3 ± 4.6
2	- 3.434 ± 0.001	+ 1.061 ± 0.002	7.2 ± 0.3	143.3 ± 6.6
5	- 3.437 ± 0.011	+ 1.705 ± 0.522	8.3 ± 0.5	413.3 ± 26.2
10	- 3.414 ± 0.010	- 2.926 ± 1.115	7.9 ± 0.4	786.7 ± 44.1